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1	An instrument to measure fast gas phase radical kinetics
2	at high temperatures and pressures
3	
4	Daniel Stone, <sup>1</sup> Mark Blitz, <sup>1,2</sup> Trevor Ingham, <sup>1,2</sup> Lavinia Onel, <sup>1</sup> Diogo J. Medeiros <sup>1</sup>
5	and Paul W. Seakins <sup>1,2</sup>
6	<sup>1</sup> School of Chemistry, University of Leeds, Leeds, UK
7	<sup>2</sup> National Centre for Atmospheric Science, University of Leeds, Leeds, UK
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# 9 Abstract

Fast radical reactions are central to the chemistry of planetary atmospheres and combustion 10 systems. Laser-induced fluorescence is a highly sensitive and selective technique that can be used to 11 monitor a number of radical species in kinetics experiments, but is typically limited to low pressure 12 systems owing to quenching of fluorescent states at higher pressures. The design and characterisation 13 14 of an instrument is reported using laser-induced fluorescence detection to monitor fast radical kinetics (up to 25,000 s<sup>-1</sup>) at high temperatures and pressures by sampling from a high pressure reaction region 15 to a low pressure detection region. Kinetics have been characterised at temperatures reaching 740 K 16 and pressures up to 2 atm, with expected maximum operational conditions of up to ~ 900 K and ~ 5 17 atm. The distance between the point of sampling from the high pressure region and the point of 18 probing within the low pressure region is critical to the measurement of fast kinetics. The 19 instrumentation described in this work can be applied to the measurement of kinetics relevant to 20 atmospheric and combustion chemistry. 21

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23

# 25 Introduction

The kinetics of gas phase reactions involving free radicals are central to the chemistry of planetary 26 atmospheres (1), interstellar space (2,3) and combustion systems (4). A variety of experimental approaches 27 exist for the extraction of rate coefficients; for radical reactions, real-time measurements monitoring the 28 removal of reagents or generation of products following the production of radicals by laser flash photolysis 29 (LFP) is a successful approach (5). Laser-induced fluorescence (LIF) spectroscopy is commonly employed in 30 flash photolysis experiments to monitor changes in radical concentrations throughout the course of a reaction 31 in real-time, thus enabling determination of kinetic parameters. LIF is a highly sensitive and selective 32 technique, with the sensitivity to measure OH radical concentrations in the atmosphere at concentrations of 33 less than  $10^6$  cm<sup>-3</sup> (6) and the selectivity to distinguish between isotopic species such as  ${}^{16}$ OH and  ${}^{18}$ OH (7). 34 The nature of LFP-LIF, where the reaction is monitored only where the photolysis and probe lasers intersect, 35 significantly reduces the potential for the influence of heterogeneous chemistry compared to flow methods. 36 However, LIF spectroscopy is typically limited to low pressure regimes (typically < 0.5 atm) owing to 37 collisional quenching of fluorescent states at higher pressures. Whilst many bimolecular rate coefficients are 38 pressure independent, and hence results determined at low pressures can be used in chemical models (e.g. 39 combustion simulations) at higher pressures, association and dissociation reactions are pressure dependent 40 (8). Although it is sometimes possible to determine the high pressure limiting rate using isotopic (9) or proxy 41 (10) methods, determination of rate coefficients over a wide range of temperature and pressure is important 42 to verify theories of reactions (11) and provide kinetic input into models. Pressures in the 1 - 10 atm range 43 are particularly relevant in elucidating autoignition processes (4,12), a subject of topical interest due to the 44 role of autoignition in homogenous charge compression ignition (HCCI) and related engines (13,14). 45

Saturated laser-induced fluorescence (SLIF) spectroscopy has been successfully used to minimise the influence of collisional quenching on observed fluorescence signals at high pressures (15-18), and thus to enable determination reaction kinetics of reactive species at high pressures (up to 150 bar in He (15)). However, the technique requires sufficiently strong laser powers to ensure stimulated emission dominates over spontaneous emission and collisional quenching and can be affected by non-uniform saturation (15). In addition, consideration of rotational energy transfer (RET) schemes are required which can complicate data
analysis (15-17).

Absorption methods do not suffer from quenching and have the added advantage of providing 53 absolute measurements if cross-sections are known. However, simple absorption methods are significantly 54 less sensitive than LIF, although modulation methods can enhance sensitivity (19). Cavity ring down 55 spectroscopy (CRDS) generally provides a significant enhancement in sensitivity (20-22), but as with other 56 absorption techniques there are practical issues in maintaining uniform temperatures over the absorption 57 region, determining the region of overlap with photolysis, avoiding surface effects and additionally keeping 58 cavity mirrors aligned over wide pressure and temperature ranges. Thus, whilst other detection methods exist 59 (and indeed, using a variety of methods is important to identify systematic errors), LIF has significant 60 advantages in sensitivity, selectivity and minimising heterogeneous interferences. 61

In this work, we describe the use of LIF at low pressures (~ 1 Torr) in the Fluorescence Assay by Gas Expansion (FAGE) technique (23) to determine reaction kinetics of reactive species at higher pressures (> 1 atm). The FAGE technique is used by several groups worldwide (6,24-31) to measure OH radical concentrations in the atmosphere, and relies on sampling gas from a region of high pressure through a pinhole nozzle to a region of low pressure, resulting in a supersonic expansion to form a free jet. Expansion of the gas significantly reduces the rate of collisional quenching of fluorescent states, thus permitting LIF spectroscopy within the low pressure region.

Field instruments to measure the total loss rate of OH in the atmosphere (k'<sub>OH</sub>, the OH reactivity) are 69 70 currently in operation which use LFP in conjunction with LIF-FAGE to make real-time measurements of OH radical kinetics with ambient concentrations of trace gases at atmospheric pressure (31-38). 71 These instruments rely on flash photolysis of  $O_3$  (followed by the subsequent reaction of  $O(^1D)$  with water vapour) 72 to produce relatively high concentrations of OH radicals in a reaction cell containing a flow of ambient air at 73 atmospheric pressure. The subsequent OH decay, owing to reactions with trace gases in the ambient air, is 74 monitored by sampling from the atmospheric pressure reaction cell to the low pressure (~1-2 Torr) FAGE 75 cell for detection by LIF. 76

However, ambient OH reactivity is typically low compared to reaction rates used in laboratory experiments, maximum reported values of  $k'_{OH}$  reaching ~100-120 s<sup>-1</sup> even in polluted environments (37,39,40). Calibrations of OH reactivity instruments using known reactant concentrations report deviations from expected kinetics at higher reactivities, with non-exponential behaviour reported for some instruments at reactivities > 60 s<sup>-1</sup> (33). Such conditions correspond to a very small dynamic range for laboratory experiments.

In this work we present the design and characterisation of an instrument to determine fast radical kinetics at high pressure and temperatures up to 740 K by coupling flash photolysis in a high pressure reaction cell to LIF in a low pressure detection cell using the FAGE technique. The use of flash photolysis to initiate the chemistry significantly lowers the potential for interference from heterogeneous chemistry. In addition to applications in combustion chemistry, we discuss the kinetic limitations of OH reactivity instruments employing similar designs, with suggestions for potential improvements. While the focus in this work is on OH kinetics, results are widely applicable to other species observable by LIF.

90

## 91 **Experimental**

Figure 1 displays a schematic of the instrument. The high pressure reaction cell consists of a stainless 92 steel tube (304L grade) of 19 mm I.D., and length of 1 m to ensure sufficient preheating of the gas, if 93 necessary, prior to the region near the pinhole. Gases, prepared at known concentrations and pre-mixed at 94 known flow rates, as determined by calibrated flowmeters, are passed in to the reaction cell at one end 95 through a T-piece which also houses a window to enable propagation of the photolysis laser beam (Lambda 96 Physik, Compex 200 operating on either ArF at 193 nm or KrF at 248 nm, beam dimensions of 24 mm × 12 97 mm expanded to fill the diameter of the cell) through the cell to initiate chemistry and produce a uniform 98 distribution of radicals throughout the cell. Precursor concentrations in the cell are maintained sufficiently 99 low such that attenuation of the photolysis laser beam along the length of the reaction cell is negligible, 100 leading to uniform radical concentrations along the length of the cell. The repetition rate of the photolysis 101

laser was varied between 1 and 10 Hz, with no impact on the observed kinetics. Gas flows in the cell are maintained under laminar conditions (Reynold's number,  $R_e < 2300$  for laminar conditions).

At the other end of the reaction cell, the 19 mm I.D. tube is open and housed within a pressure-sealed 104 chamber (70 mm I.D. and 200 mm in length) which couples the reaction cell to the low pressure FAGE 105 detection cell. The open end of the reaction cell is 5 mm from the 0.5 mm pinhole nozzle which is mounted 106 on a flat plate and enables sampling of the gas from the high pressure reaction cell into the detection cell. 107 The flow rate of gas through the detection cell is ~ 1.2 slm (for a detection cell pressure of ~ 1 Torr), with 108 any excess gas in the reaction cell passed out through the pressure-sealed chamber, which is connected to a 109 rotary pump (Edwards 210 ED660). Control of the total pressure within the reaction cell is achieved by 110 throttling the exit valve to the pump. 111

The temperature of the gas in the reaction cell is controlled by varying the voltage applied to a heating coil (Watlow, WATROD tubular heater) surrounding the reaction cell within the pressure-sealed chamber. Pre-heating of the gas to achieve a longer residence time in the heated region can be achieved using a ceramic heater (Watlow, ceramic fiber heater, VS102A18S) situated around the reaction cell prior to the heating coil within the pressure-sealed chamber. Three K-type thermocouples (Omega) are situated along the length of the heated region of the reaction cell to monitor the temperature.

Pressure in the detection cell is maintained at ~ 1 Torr by a rotary pump (Edwards 210 ED660) 118 backed supercharger pump (EUROSERV). OH radicals in the gas flow are monitored by off-resonance 119 laser-induced fluorescence following excitation at 282 nm ( $A^2\Sigma$  (v'=1)  $\leftarrow X^2\Pi$  (v''=0), Q<sub>1</sub>(1)), generated 120 using the 532 nm output of an Nd:YAG (Spectron Laser Systems) to pump a dye laser (Spectron Laser 121 Systems) operating on Rhodamine-6-G dye. While 308 nm laser light offers the potential for higher 122 sensitivity (41,42), temporal gating would be required to discriminate the fluorescence emission from 123 scattered laser light. The 282 nm probe laser beam is passed through the detection cell perpendicular to the 124 direction of gas flow at a variable distance (between 5 and 200 mm) from the sampling point of the gas from 125 the reaction cell (i.e. from the position of the pinhole). The off-resonant OH fluorescence at ~308 nm is 126 passed through an interference filter (Barr Associates,  $308 \pm 5$  nm) and detected by a channel photomultiplier 127 (CPM, Perkin-Elmer C1943P) mounted perpendicular to the plane of the gas flow and probe laser beam. 128

The time delay between photolysis and probe laser pulses is controlled by a digital delay generator 129 (BNC DG535) and varied to enable monitoring of the OH profile as a function of time following photolysis 130 of the gas mixture. Kinetic traces typically consist of 200 data points, with each data point typically averaged 131 5-10 times. OH signals are monitored before, during and after the photolysis laser pulse at several known 132 reactant concentrations. The pseudo-first-order rate coefficient (k', where  $k' = k_{OH+X}[X]$ ) is determined by 133 fitting an exponential decay to the observed OH signal. The bimolecular rate coefficient (i.e. k<sub>OH+X</sub>) is 134 obtained from the gradient of the bimolecular plot (i.e. the plot of the pseudo-first-order rate coefficient 135 136 against [X], the known concentration of reactant X).

137

## 138 **Instrument characterisation at room temperature**

Initial experiments to characterise the instrument and optimise experimental parameters were 139 performed at a temperature of 298 K, total pressure of 1000 Torr, and a total flow rate of 18 slm to measure 140 well-known kinetics of  $OH + CH_3OCH_3$  (dimethyl ether, DME) (18,43) by flash photolysis of 141 O<sub>3</sub>/H<sub>2</sub>O/DME/O<sub>2</sub>/N<sub>2</sub> gas mixtures. O<sub>3</sub> was generated from O<sub>2</sub> by a commercial ozone generator (EASELEC, 142 Ozone Technology, ELO-3G), diluted in N<sub>2</sub> to ~ 1 % by volume and stored in an aluminium cylinder (Luxfer 143 Gas Cylinders M4141) at a total pressure of ~6000 Torr. DME (Sigma-Aldrich,  $\geq$  99 %) was diluted to a 144 known concentration in N<sub>2</sub> and also stored in an aluminium cylinder. Cylinders were stored overnight prior 145 to use to ensure complete mixing, and were used within one week of preparation. No significant differences 146 were observed between experiments using cylinders stored for different periods of time. Water vapour was 147 introduced to the gas flow by passing the carrier gas  $(N_2)$  through a bubbler containing distilled water. N<sub>2</sub> 148 (BOC, 99.99 %) and O<sub>2</sub> (BOC, 99.999 %) were used as supplied. OH radicals were produced in the reaction 149 cell by the photolysis of O<sub>3</sub> ( $\lambda$  = 248 nm), followed by the subsequent reaction of O(<sup>1</sup>D) with water vapour 150 (R1-R2). Concentrations of  $O_2$  were sufficient to ensure that any  $O({}^{3}P)$  formed was rapidly converted back 151 to O<sub>3</sub> (R3-R4). Initial OH radicals concentrations were  $\sim 1 \times 10^{12}$  cm<sup>-3</sup>, estimated from the laser fluence and 152 ozone absorption cross-section at  $\lambda = 248$  nm. DME concentrations were sufficient to ensure pseudo-first-153 order conditions for reaction with OH (R5). While there is the potential for some regeneration of OH 154 through reaction of CH<sub>3</sub>OCH<sub>2</sub> with O<sub>2</sub>, the extent of this was small at the pressures used here (44). 155

156 
$$O_3 + hv (\lambda = 248 \text{ nm}) \rightarrow O(^1\text{D}) + O_2$$
 (R1)

157 
$$O(^{1}D) + H_{2}O \rightarrow 2 OH$$
 (R2)

158 
$$O(^{1}D) + M \longrightarrow O(^{3}P) + M$$
 (R3)

159 
$$O(^{3}P) + O_{2} + M \longrightarrow O_{3} + M$$
 (R4)

160 
$$OH + CH_3OCH_3 \rightarrow CH_3OCH_2 + H_2O$$
 (R5)

Figures 2 and 3 show the observed temporal behaviour of OH and corresponding bimolecular plots 161 162 for the reaction of OH with DME. At a probe distance (i.e. the distance from the pinhole, where gas is sampled from the high pressure reaction cell, to the probe laser, as shown in Figure 1) of 5 mm, the observed 163 164 OH decay was well-described by pseudo-first-order kinetics and the bimolecular rate coefficient obtained for OH + DME,  $k_{OH+DME} = (2.6 \pm 0.1) \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$ , is in good agreement with recent determinations of 165  $k_{OH+DME} = (2.7 \pm 0.2) \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$  (18) and  $k_{OH+DME} = (2.9 \pm 0.3) \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$  (43) and literature 166 recommendations of  $k_{OH+DME} = (2.8 \pm 0.4) \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$  (45) at 298 K. The signal-to-noise ratio of the OH 167 measurements is estimated at ~50:1 (Figure 2), and can be improved through use of alternative OH radical 168 precursors not requiring the presence of large amounts of water vapour, which efficiently quenches the OH 169 fluorescent state. The sensitivity of the instrument described in this work is approximately a factor of ten 170 lower than that achieved in a standard time-resolved LIF experiment conducted at pressures up to ~100 Torr 171 ((43), for example). Although the number density of OH is reduced on expansion into the FAGE detection 172 cell, the reduction in temperature associated with the expansion results in significantly increased population 173 of the  $X^2\Pi$  (v''=0), Q<sub>1</sub>(1) state probed in the experiment, reducing the impact of the decreased number 174 density in the FAGE cell. 175

Measurements of the rate coefficients of reactions of OH with methane (CH<sub>4</sub>) (see below and supplementary information for further information (46)) and isoprene (2-methyl-1,3-butadiene,  $C_5H_8$ ) (see supplementary information for further information (46)) have also been obtained at probe distances of < 5 mm in agreement with literature values (45), with pseudo-first-order rate coefficients of up to ~25,000 s<sup>-1</sup> measured in this work. When probing the OH signal further away from the pinhole a significant rise time was noted for the OH signal (Figure 2b, Figures S1 and S3 in supplementary information (46)) and the resulting bimolecular plots (Figure 3b, Figures S2 and S4 in supplementary information (46)) produced a bimolecular rate coefficient that was approximately a factor two lower than the literature values. This is discussed further below.

186

# 187 Characterisation of temperature and pressure

Subsequent experiments were performed to characterise the instrument as a function of temperature. 188 Figure 4 shows the temperature profiles along the reaction cell, measured by a K-type thermocouple (Omega) 189 situated in the centre of the gas flow in the reaction cell at varying distances from the point at which gas is 190 sampled. Temperature profiles were found to be constant in the region of the reaction cell immediately prior 191 to the sampling point for at least 10 cm (the total heating region using the heating coil alone is ~ 18 cm in 192 length). For a gas flow of ~ 5 slm, a distance of 1 cm in the reaction cell corresponds to a residence time of ~ 193 18 ms. Temperatures are monitored throughout experiments by three K-type thermocouples situated along 194 the length of the heated region. 195

Kinetics of the reaction between OH and methane, CH<sub>4</sub>, were obtained at various temperatures and 196 pressures to characterise the instrument as a function of temperature and pressure. OH was generated by the 197 photolysis of H<sub>2</sub>O ( $\lambda$  = 193 nm) and detected at a probe distance of 5 mm from the sampling point in all 198 cases. The OH + methane reaction was chosen for validation as it is well characterised (45,47), has a strong 199 temperature dependence (hence a sensitive probe of the reaction temperature) and at low temperatures is a 200 slow reaction ( $k_{298 \text{ K}} = 6.3 \times 10^{-15} \text{ cm}^3 \text{ s}^{-1}$ ) (45); reproducing literature rate coefficients at low temperatures 201 therefore suggests an absence of interfering radical-radical reactions (47). Concentrations of CH<sub>4</sub> (BOC, 100 202 CP Grade, used as supplied) were sufficient to ensure pseudo-first-order conditions for  $OH + CH_4$  at all 203 temperatures. Total flow rates in the reaction cell were varied between 5 slm and 18 slm, with no significant 204 effect on the observed kinetics. 205

Figure 5 shows the bimolecular rate coefficients ( $k_{OH+CH4}$ ) determined in this work at temperatures in the range 298 to 740 K and pressures up to 2 atm. Results obtained with this experimental approach are in good agreement with those reported previously in the literature (48-50), and those currently recommended for use in atmospheric (45) and combustion models (51).

The maximum temperatures and pressures reported in this work are primarily a result of current safety constraints. To achieve the maximum temperature of 740 K reported in this work, the coil heater is operating at ~75 % of its maximum power, with an expected maximum achievable temperature of ~ 900 K, while current gas fittings and components within the system are specified to operate up to ~ 5 atm. It is thus expected that higher temperatures and pressures could be readily achieved with this instrument than are reported in this work.

216

# 217 Effects of probe distance

Measurements of  $k_{OH+DME}$  and  $k_{OH+CH4}$  obtained using the experimental approach described above compare favourably with previous measurements for experiments conducted here using a short ( $\leq 5$  mm) probe distance (i.e. the distance from the point of sampling from the high pressure reaction cell at the pinhole nozzle to the point at which the probe laser intersects the gas flow in the low pressure detection cell). However, the probe distance has been shown to be critical to accurate kinetic measurements, as described above and shown in Figures 2 and 3.

At longer probe distances (> 10 mm) and low reactant concentrations (i.e. with low pseudo-first-order 224 rate coefficients,  $< \sim 500 \text{ s}^{-1}$ ), the observed OH kinetics were broadly similar to literature values (Figure 3b, 225 reaction of OH with DME). However, as the reactant concentration was increased, significant deviations 226 from expected behaviour were observed when probing at longer distances. The observed OH decays at 227 higher reactant concentrations and longer probe distances appeared to display biexponential behaviour 228 (Figure 2b, reaction of OH with DME), with bimolecular rate coefficients obtained from these data 229 significantly lower than expected values (Figures 3b, reaction of OH with DME). In addition, OH signals 230 took significantly longer to appear than in experiments probing at a distance of 5 mm. 231

The differences observed between experiments probing at short distances from the sampling point and those probing at longer distances can be rationalised in terms of the behaviour of the gas sampled in to the low pressure detection region. When sampling from a high pressure region to a low pressure region, expansion of the sampled gas into the low pressure region results in the generation of a supersonic jet. Species within the jet can be characterised by low rotational temperatures, and have a narrow and welldefined velocity distribution around a relatively high mean velocity. The length of the jet can be approximated by the position of the Mach disk:

$$x_m = 0.67 d \sqrt{\frac{p_0}{p_b}}$$

where  $x_m$  is the position of the Mach disk (i.e. the length of the jet), *d* is the diameter of the pinhole nozzle and  $p_0$  and  $p_b$  are the pressures in the high pressure region and the background pressure in the low pressure region, respectively. At the Mach disk, the supersonic jet breaks down and plug flow conditions dominate. Under plug flow conditions, species have higher rotational temperatures, the mean gas velocity is much lower, and the velocity distribution is much broader and can be described by a Maxwell-Boltzmann distribution.

Thus, when the distance between the sampling point (i.e. the position of the pinhole) and the detection point (i.e. the point at which the probe laser passes across the gas flow) is short (< 10 mm), the arrival time of species travelling from the sampling point to the detection point will be relatively short, with a relatively narrow distribution. The impact of this spread in arrival times on observed first-order kinetics has been described for experiments sampling from high pressure reaction regions to low pressure detection regions using mass spectrometry, and solutions enabling exact determinations of kinetics have been reported (52).

In contrast, when the distance between the sampling point and the detection point is longer (> ~10 mm for a transition from 760 Torr to 1 Torr for a 0.5 mm pinhole), species will be probed from the plug flow region. Subsequently, arrival times at the detection point will not only be much longer, but there will also be a much more significant spread of arrival times at the detection point from species which were sampled at the pinhole at the same time. The impact of this spread in arrival times will therefore be much greater if species are probed in the plug flow region than if species are probed within the jet. Deconvolution of kinetics from transport within the detection region thus becomes more problematic under plug flow conditions, and it is not
possible to obtain an exact solution to enable extraction of kinetic parameters.

Creasev et al.(53) demonstrated that the rotational temperature determined by LIF increases sharply at 259 the expected location of the Mach disk. Figure 6 shows the LIF excitation spectra recorded for OH probed at 260 5 mm and 200 mm from the sampling point, indicating a transition from a low rotational temperature (~ 40 K 261 when compared to simulations using LIFBASE (54)) at a probe distance of 5 mm to a much higher rotational 262 temperature (~ 200 K) at a probe distance of 200 mm. Measurements of the OH LIF spectra in the detection 263 region thus indicate that probing at a distance of 5 mm from the sampling point (where the observed kinetics 264 indicate reliable measurements up to k' ~ 20,000 s<sup>-1</sup>) probes species within the supersonic jet, while probing 265 distance of 200 mm from the sampling point (where the observed kinetics deviate significantly from 266 expected behaviour) probes species outside of the supersonic jet and within the plug flow regime. 267

Figure 7 shows the expected distributions of arrival times, and impacts on temporal profiles for 268 identical pseudo-first-order reaction conditions, of species at probe regions of 5 mm from the sampling point 269 270 (i.e. within the supersonic jet, simulated using the exact solution described by Taatjes (55)) and 200 mm from the sampling point (i.e. in the plug flow region, simulated using a Maxwell-Boltzmann distribution at the 271 temperature indicated by the LIF spectra in the plug flow region). There is a clear difference in both the 272 mean arrival time and the spread in arrival times between species probed at 5 mm and those probed at 200 273 mm (Figure 7a), leading to significant impacts on observed temporal profiles (Figures 2 and 5) and 274 consequences for extraction of kinetic parameters. 275

276

#### 277 Applications

### 278 Ambient OH reactivity

Deviations from the expected pseudo-first-order behaviour at high reactivities have been reported for a number of field instruments used to measure ambient OH reactivity using laser flash photolysis coupled to FAGE detection (LFP-FAGE), which typically probe OH at distances of 120-200 mm from the sampling point (31,33,36,38,56). For some instruments, such deviations from the expected exponential behaviour are observed at reactivities above 60 s<sup>-1</sup>, potentially leading to underestimations of ambient OH reactivity in polluted environments (33,34). The use of FP-FAGE to measure ambient OH reactivity does, however, offer advantages over other techniques to measure OH reactivity, particularly in high NO<sub>x</sub> environments owing to the ability to produce OH in isolation from HO<sub>2</sub> which significantly reduces the impact of OH production from HO<sub>2</sub> + NO on the timescale of the experiment.

The observed deviations from expected behaviour at high ambient reactivities can be explained by the long probe distances typically employed in field instruments. Increased dynamic ranges for measurements of OH reactivity can thus be achieved by reducing the probe distance such that radicals are detected within the supersonic jet of the gas expansion.

292

### 293 Low temperature combustion

Real-time measurements of reactive species involved in low temperature combustion are key to the 294 elucidation of reaction mechanisms involved in autoignition processes in homogeneous charge compression 295 ignition (HCCI) engines (57). There is, however, a gap between techniques appropriate to measurements of 296 oxidation processes at temperatures and pressures relevant to the atmosphere, and those appropriate to 297 measurements of high temperature combustion processes in traditional spark ignition or diesel engines, 298 limiting experimental capabilities in the temperature range ~500-900 K (57). The lack of appropriate 299 experimental techniques for studies of low temperature combustion and the chemistry controlling 300 autoignition has thus hindered the full exploitation of biofuels and novel fuels to improve fuel security and to 301 reduce emissions of  $CO_2$ ,  $NO_x$  and soot (4,57). 302

The instrumentation described in this work will bridge the gap between techniques currently described in the literature to enable more detailed investigations of the processes controlling autoignition and low temperature combustion in real-time. Dimethyl ether (DME) is a potentially promising biofuel (58), and several groups have recently reported measurements of key markers in the low temperature combustion of DME (43,59-64). However, the mechanism of DME combustion remains unclear, and the processes leading to radical chain branching have yet to be experimentally determined. Application of the techniques described in this work to such systems will enable greater understanding of the gas phase radical chemistry involved inautoignition and low temperature combustion, and will be explored further in future work.

311

### 312 Summary

The design and characterisation of an instrument to measure fast gas phase kinetics in real-time at 313 high temperatures and pressures by sampling from a high pressure reaction region to a low pressure detection 314 region using the FAGE technique has been described. Radical generation in the high pressure reaction region 315 is achieved by laser flash photolysis, thus minimising the potential for heterogeneous chemistry. We have 316 demonstrated successful accurate measurements of kinetics over a range of temperatures and pressures. 317 However, the distance between the sampling point and the probe region is critical for accurate measurements 318 of reaction kinetics, with measurement accuracy requiring probing within the supersonic jet formed on 319 sampling from the high pressure region to the low pressure region. 320

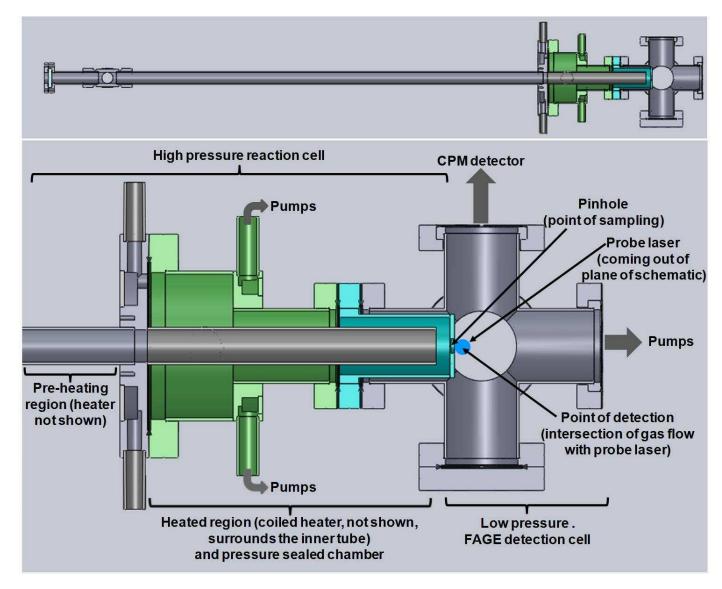
The experimental approach described in this work can be applied to measurements of fast gas phase kinetics relevant to atmospheric and combustion chemistry, and is applicable to any species exhibiting laserinduced fluorescence.

324

## 325 Acknowledgements

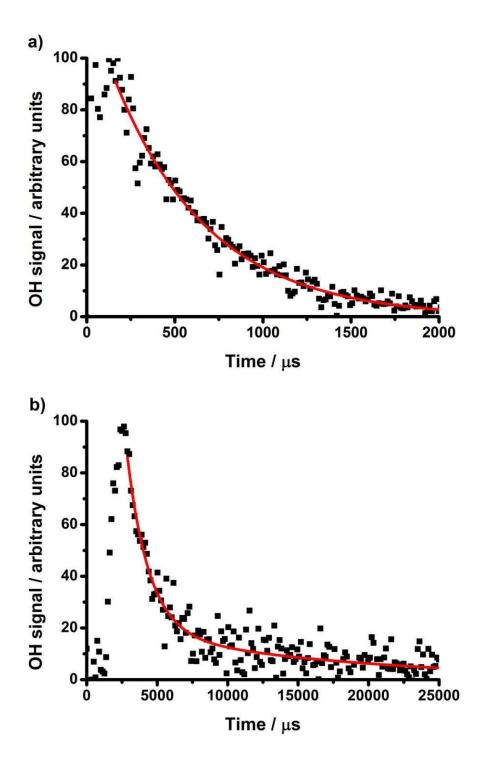
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# **Figures**



331

Figure 1: Schematic of the instrument. Upper panel shows the full instrument, with the lower panel displaying the region connecting the high pressure reaction cell and the low pressure detection cell in detail. The pinhole is incorporated within the section shown in blue, and this section is readily interchangeable if a change in pinhole diameter is required.



337 Figure 2: Temporal behaviour of OH signals for reaction of  $OH + CH_3OCH_3$  (dimethyl ether, DME) at probe 338 distances of a) 5 mm and b) 200 mm from the sampling point. For both plots, the reaction cell was at 298 K, 1000 Torr and the detection cell at 0.8 Torr. Fits to the data are shown in red. Data collected at a probe 339 distance of 5 mm (panel a,  $[DME] = 8.3 \times 10^{14} \text{ cm}^{-3}$ ) were fitted to a single exponential decay ( $\hat{k}_{obs} = (1850)$ 340  $\pm$  58) s<sup>-1</sup>), while those collected at a probe distance of 200 mm (panel b, [DME] =  $3.6 \times 10^{14}$  cm<sup>-3</sup>) were fitted 341 to a biexponential decay ( $k_{obs,fast} = (644 \pm 74) \text{ s}^{-1}$ ;  $k_{obs,slow} = (64 \pm 14) \text{ s}^{-1}$ ), with only the fast component of 342 the decay observed to display any dependence on [DME] and used in the bimolecular plots in Figure 3. 343 Additional kinetic results obtained for  $OH + CH_4$  at probe distances of < 5 mm and 50 mm, and for OH +344  $C_5H_8$  at a probe distance < 5 mm, are shown in the supplementary information. 345

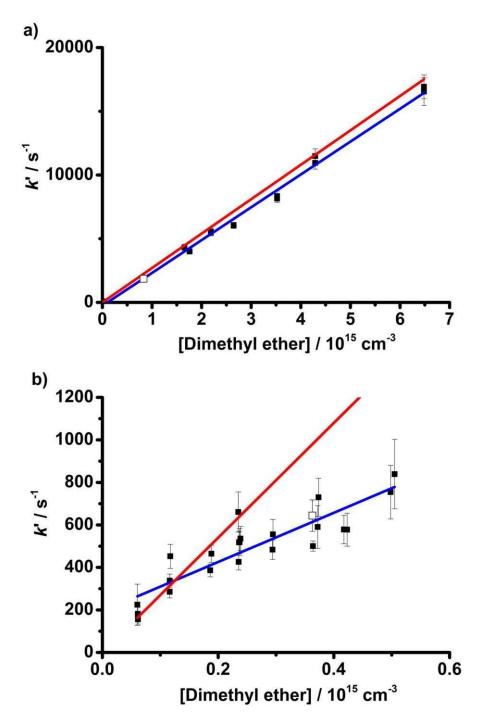


Figure 3: Bimolecular plots of observed OH decay kinetics at 298 K and 1000 Torr, with the detection cell at 347 a pressure of 0.8 Torr, for sampling distances of a) 5 mm and b) 200 mm for reactions of OH with CH<sub>3</sub>OCH<sub>3</sub> 348 (dimethyl ether, DME). Best fit lines are shown in blue; (k =  $(2.6 \pm 0.2) \times 10^{-12}$  cm<sup>3</sup> s<sup>-1</sup> when probing at 5 349 mm from the sampling point (panel a, analysed using a single exponential decay);  $k = (1.2 \pm 0.2) \times 10^{-12} \text{ cm}^3$ 350 s<sup>-1</sup> when probing at 200 mm from the sampling point (panel b, analysed using a biexponential decay)). The 351 data points shown by the open symbols correspond to the kinetic traces shown in Figure 2. Literature 352 recommendations shown in red (k =  $2.8 \times 10^{-12}$  cm<sup>3</sup> s<sup>-1</sup>) (45). Note that at longer probe distances (200 mm in 353 panel b) and low reactant concentrations, the observed OH kinetics are similar to those expected from 354 literature values, with higher reactant concentrations leading to deviation from expected kinetics. Additional 355 kinetic results obtained for  $OH + CH_4$  at probe distances of < 5 mm and 50 mm, and for  $OH + C_5H_8$  at a 356 probe distance < 5 mm, are shown in the supplementary information. 357

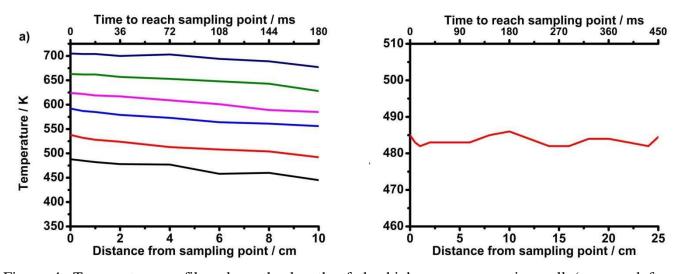


Figure 4: Temperature profiles along the length of the high pressure reaction cell (measured from the 359 sampling point, such that the pinhole nozzle is at 0 cm). Temperatures were measured in the centre of the gas 360 flow for flow rates of ~5 slm, corresponding to a residence time of ~ 18 ms in each 1 cm length of the 361 reaction cell (times taken to reach the sampling point from the corresponding distance at a flow rate of 5 slm 362 are shown in the upper x-axes). Pressures in the reaction cell were maintained at 1000 Torr. Panel (a) shows 363 the temperature profiles obtained using the single heating coil only (18 cm in total length, of which only the 364 section with stable temperature profile is shown); panel (b) shows an example temperature profile obtained 365 using the ceramic pre-heater in addition to the coil heater. 366

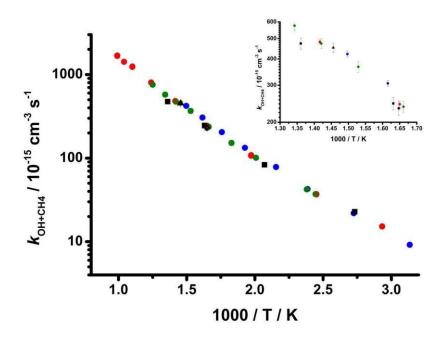
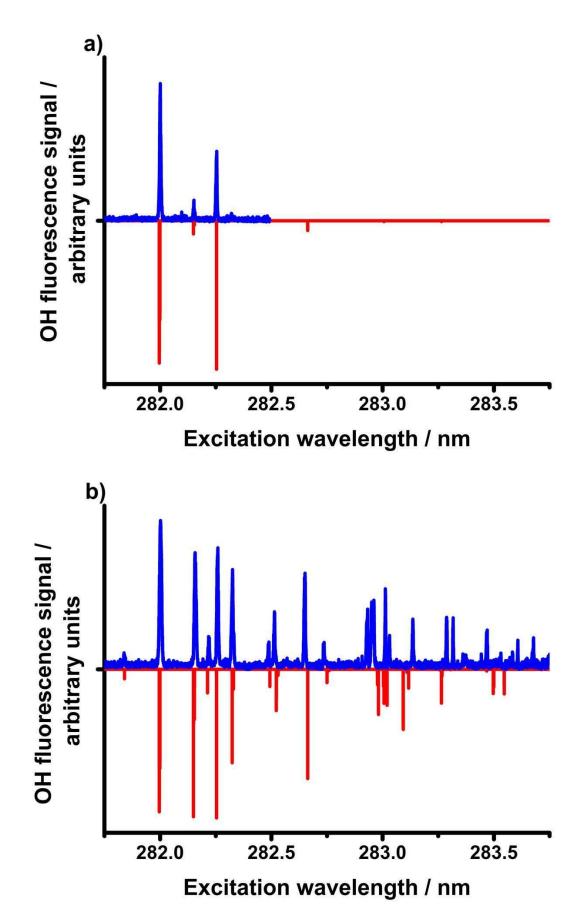
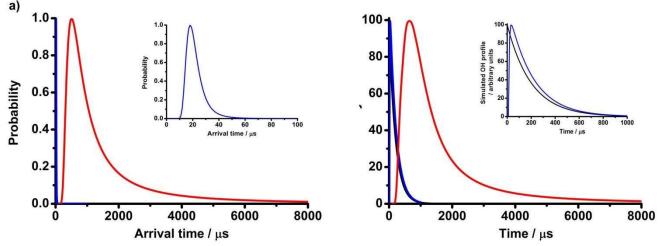


Figure 5: Bimolecular rate coefficients obtained for the reaction of OH with CH<sub>4</sub> as a function of temperature. Data obtained in this work are shown in the black points (squares represent data in 2 atm of N<sub>2</sub>; diamonds represent data in 2 atm of Ar; triangles represent data in 1 atm of N<sub>2</sub>). Previous measurements are shown for Bonard et al. (48) (blue circles), Bryukov et al. (49) (red circles) and Dunlop and Tully (50) (green circles). Errors are  $2\sigma$  (although masked by the data points on the scale). The inset shows an expanded region to that the data can be seen in greater detail.



### Figure

6: LIF excitation spectra for OH at sampling distances of a) 5 mm and b) 200 mm. Observed spectra are shown in blue (positive values), with LIFBASE simulations shown in red (negative values) for rotational temperatures of a) 40 K and b) 200 K. There is a sharp change in the observed spectrum at the expected location of the Mach disk (~ 12 mm in these experiments).



379 380 Figure 7: Simulations showing impacts of velocity distributions at probe regions of 5 mm (blue; shown more 381 clearly in the inset plots) and 200 mm (red) on a) the normalised probabilities of arrival times at the probe region (i.e. for species leaving the sampling point at t = 0) and b) the apparent OH signal at the probe region 382 for identical pseudo-first-order reaction conditions ( $k^{-}$  = 5000 s<sup>-1</sup>, shown by the black line for a simulation not 383 including any transport). Note that Creasey et al. (53), using a combination of experimental data and 384 385 computational fluid dynamics calculations, demonstrated that the mean bulk gas velocity in the plug flow region was ~ 65 m s<sup>-1</sup>. The impact of this slow mean bulk gas flow in our experiments is apparent from the 386 difference in the arrival times simulated here to those observed experimentally (Figure 2b), but has not been 387 included in these simulations since it is not possible to determine the mean bulk velocity in the plug flow 388 region for our experimental configuration a priori with any certainty. 389

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