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| 1 2 | Shape stabilised phase change materials based on a high melt viscosity HDPE and paraffin waxes |
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30 Abstract

Shape stabilised phase change materials (SSPCMs) based on a high density poly(ethylene)(hv-HDPE) with high (H-PW, T_m=56-58 °C) and low (L-PW, T_m=18-23 °C) melting point paraffin waxes were readily prepared using twin-screw extrusion. The thermophysical properties of these materials were assessed using a combination of techniques and their suitability for latent heat thermal energy storage (LHTES) assessed. The melt processing temperature (160 °C) of the HDPE used was well below the onset of thermal decomposition of H-PW (220 °C), but above that for L-PW (130 °C), although the decomposition process extended over a range of 120 °C and the residence time of L-PW in the extruder was < 30seconds. The SSPCMs prepared had latent heats up to 89 J/g and while the enthalpy values for H-PW in the respective blends decreased with increasing H-PW loading, as a consequence of co-crystallisation of H-PW and hv-HDPE. Static and dynamic mechanical analysis confirmed both waxes have a plasticisation effect on this HDPE. Irrespective of the mode of deformation (tension, flexural, compression) modulus and stress decreased with increased wax loading in the blend, but the H-PW blends were mechanically superior to those with L-PW.

55 **1. Introduction**

Thermal energy storage through the use of phase change materials (PCMs) in building applications has attracted much attention recently, their use having the potential to improve energy efficiency in buildings [1-3]. PCMs are substances with a high heat of fusion, which on changing phase over a certain temperature window are capable of storing and releasing large amounts of energy. The most effective method of storing thermal energy is via latent heat, which can be given by:

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$$Q = \int_{T_i}^{T_m} mC_p dT + ma_m \Delta H_m + \int_{T_m}^{T_f} mC_p dT$$
(1)

63 where, Q = the quantity of heat stored, $T_m =$ melting temperature, $T_i =$ initial temperature,

 T_f = final temperature, m = mass of storage medium, a_m = fraction of material melted, ΔH_m = 64 heat of melting per unit mass (J/kg) and C_p = specific heat capacity (J/kg/K). This process 65 creates the opportunity for utilising renewable natural energy, such as solar energy and night 66 67 ventilation by incorporating PCMs into buildings [4-7]. Many different types of PCMs have been studied, such as those based on hydrated salts, paraffin, fatty acids and polyols [8-11]. 68 Paraffin is the most attractive PCM used in buildings as it is one of the cheapest and most 69 70 readily available, being derived from petroleum and having relatively good thermo-physical properties, such as high latent heat, negligible super-cooling and a suitable transition point 71 [12]. A paraffin wax consists typically of a mixture of hydrocarbon molecules, C_nH_{2n+2} (n=1-72 100), with each specific wax having a range of about 8 to 15 carbon numbers. Latent heat is 73 stored as a consequence of the crystallisation of these hydrocarbon molecules. With a melting 74 75 point adjustable to climate specific requirements, the length of the hydrocarbon chain dictates both the melting point of the PCM and the heat of fusion. Hydrocarbon waxes have a wide 76 range of melting temperatures, from -5 °C to 61 °C [13]. This when combined with their high 77 heats of fusion, up to 266 J/g, makes them suitable for space heating applications. 78

79 However, it cannot be used in buildings directly as the phase changes of paraffin waxes are between the solid and liquid states. To overcome this, researchers have developed 80 shape stable phase change materials (SSPCMs), which use certain polymers as a supporting 81 82 matrix and paraffin wax as the functional core material. By melting and mixing polymer and wax together, the polymer can form a three dimensional network structure to envelop the 83 wax. The melting point of the polymer is always higher than that of the paraffin wax. Thus, 84 when paraffin wax changes from solid to liquid, the supporting matrix remains solid and the 85 paraffin wax will not leak, although there may be seepage with time, from the polymer 86 87 network structure [9, 14]. The composite material, therefore, can be used as laminated SSPCM wallboards with no need to incorporate them into building materials. A range of 88 polymers can be used as the structural supporting component/matrix, including high-89 90 (HDPE), low- (LDPE) and linear low-density (LLDPE) poly(ethylene), styrene-butadiene-91 styrene (SBS) tri-block copolymer and poly(propylene) (PP), although the poly(ethylene) family have been most widely studied for SSPCM application with paraffin waxes, due to 92 93 their similar chemical structures [15-19].

Inaba and Hu proposed, more than 15 years ago, the concept of HDPE/wax blends as 94 95 a new type of SSPCM by melting and mixing paraffin and HDPE for thermal energy storage applications without encapsulation and determining the thermo-physical properties of the 96 blend. The blend was composed of 26% HDPE and 74% paraffin by weight. The wax used 97 98 consisted mainly of pentacosane (C₂₅H₅₂, T_m=54.2 °C) [9]. Lee and Choi studied the durability of SSPCMs by investigating the seepage behaviour of a paraffin ($C_{24}H_{50}$) [20]. The 99 SSPCMs based on this paraffin wax with two different types of HDPE were prepared by 100 101 simple physical mixing at a paraffin content of 70 wt%. The authors reported the effect of HDPE crystalline morphology on the seepage behaviour of the paraffin and concluded that a 102 higher molecular weight HDPE was required for better sealant properties. More recently, 103

104 Chen and Wolcott identified co-continuous structures for blends of HDPE, LLDPE and LDPE with a C_{18} based paraffin wax [21]. They concluded that the co-continuous structure 105 formed was the main cause of paraffin leakage from the respective blends, and the rate of 106 leakage from HDPE was significantly slower than that from LLDPE and LDPE, for the same 107 test conditions. Blends of six types of HDPE with varying melt indices and paraffins were 108 evaluated as candidate materials for SSPCMs by Hong and Ge [14]. The HDPEs were mixed 109 110 (detail not given) with refined or semi-refined paraffin waxes of different melting points (the T_m of the waxes was not reported) at wax contents as high as 75 wt%. The authors showed a 111 112 SSPCM based on a HDPE with a MFI=11 g/10min and semi-refined paraffin which could be used in LHTES applications. Zhang et al. developed SSPCMs for building applications using 113 paraffin waxes having $T_m = 20$ °C and 60 °C as the PCM, but studied SBS as well as HDPE 114 115 as the supporting matrix [22]. The authors explored strategies to enhance the thermal conductivity of these systems by adding graphite or carbon fibre and reduce leakage of the 116 wax from the matrix by employing surface treatments, e.g. grafting or cross-linking. 117 However, the authors provided no information about the influence of different waxes, 118 polymer matrices or additives on the mechanical properties of the SSPCM blends. Kaygusuz 119 and Sari investigated the thermal properties of an SSPCM based on HDPE and four different 120 types of waxes with T_m=42-44 °C, 48-50 °C, 56-58 °C, and 63-65 °C [23, 24]. They found 121 122 that the mass fraction of paraffin wax in the SSPCM could be as high as 77% without any 123 seepage of the paraffin, for the conditions tested. The thermal conductivity of the SSPCMs, although from a low level, was improved by as much as 52% on addition of exfoliated 124 graphite at a loading of 3 wt%. Al Maadeed at el. also reported that addition of up to 15wt% 125 126 of expanded graphite (EG) to HDPE/paraffin wax blends increased both thermal stability and thermal conductivity of the blends [25]. Even the addition of small quantities of EG reduced 127 crystallisation time and thus increased the latent heat storage. Hato and Luyt studied the 128

129 influence of wax type and content on miscibility when blended with HDPE, LDPE and LLDPE [26]. The thermal behaviour of the wax is greatly influenced by the degree of 130 miscibility with the polymer matrix. All three polymers were initially melt-mixed with a hard 131 wax (H1), (T_m=59.4 °C) and an oxidised wax (A1) (T_m=55.4 °C) in a Brabender Plastograph 132 (screw speed = 30 rpm for 15 min). Interestingly, all HDPE/wax blends were completely 133 miscible at both 10 wt% and 20 wt% wax content, but only partially miscible when 30 wt% 134 135 wax was added. LDPE/hard paraffin wax blends were partially miscible at all wax loadings investigated, while only completely miscible for a low loading of 10 wt% oxidised wax. 136 137 Complete miscibility was observed for all the LLDPE/oxidised wax blends. Further work by the same group on SSPCMs consisting of HDPE, alkali-treated wood flour (WF) and either 138 M3 or H1 waxes (where M3 wax has $T_m=40-60$ °C, average $M_w=440$ gmol⁻¹; for H1, $T_m=107$ 139 °C, average $M_w=785$ g mol⁻¹) explored the effectiveness of WF in improving the mechanical 140 properties and thermal stability of the SSPCM [27, 28]. Poor filler dispersion and interfacial 141 adhesion were observed between the WF particles and HDPE matrix. Partial miscibility of 142 143 the HDPE with both M3/H1 waxes was observed, with the WF particles covered by wax. The presence of either wax (M3 or H1) reduced the thermal stability and mechanical properties of 144 all blends. With regard to the use of these SSPCMs in building applications increased M3 145 wax content resulted in a decrease in water uptake. Chen and Wolcott also studied the 146 miscibility of HDPE, LLDPE and LDPE with a C₁₈ paraffin wax and showed all three 147 148 polymers were partially miscible with this wax [29]. The miscibility between the HDPE and wax was the weakest and thus from a phase change material perspective this blend is 149 preferred for LHTES. Yan et al. prepared SSPCMs based on HDPE with four different types 150 of waxes with T_m between 21 °C and 27 °C and up to 70% mass content [30]. The SSPCMs 151 prepared had large latent heats, up to 177 J/g and were good candidates for LHTES. Co-152 crystallisation of paraffin waxes with poly(ethylene)s must also be considered when 153

154 preparing SSPCMs based on these materials. Luyt and Brüll studied the extent of cocrystallisation of SSPCMs based on an oxidised wax (average $M_w = 785$ g mol⁻¹, C/O ratio 155 18.8/1) with HDPE, LDPE and LLDPE [31]. The authors demonstrated extensive co-156 crystallisation of the wax with LLDPE, but little or no co-crystallisation with HDPE and 157 LDPE. From an applications point of view the flame retardant properties of SSPCM's are 158 very important. Recently, Wang et al. examined the effect of organo- modified 159 montmorillonite(OMMT), EG and crosslinking the polymer matrix on the burning time 160 (related to flame retardant performance) of a blend of SBS/HDPE/paraffin wax (30/10/60) 161 162 [32]. The best flame retardance was achieved when both OMMT and EG was added to the blend and the polymer matrix crosslinked by tert-butyl hydroperoxide. 163

However, there has been little research on the impact of different melting point waxes 164 165 on the thermo-physical properties of the SSPCMs which are also prepared using a continuous, scalable and industrially relevant process such as twin-screw extrusion. In this 166 paper, we describe the preparation of SSPCMs based on a high melt viscosity HDPE (hv-167 HDPE) with high (H-PW, T_m=56-58 °C) and low (L-PW, T_m=18-23 °C) melting point 168 paraffin waxes using twin-screw extrusion at loadings up to 75% content by mass. The 169 170 thermal and mechanical properties of all blends were determined. As the melting point of L-PW is close to the human comfort range, it could be used for heating and cooling in buildings 171 [33]. Moreover, the higher T_m H-PW could find application in solar water heating systems 172 173 [23, 34]. Indeed, such blends could be pulverised into powders which could be used as functional fillers for phase change coatings [35]. 174

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179 **2. Experimental**

180 2.1. Materials

The hv-HDPE (Marlex® HHM TR-144 Polyethylene) used in this study was supplied by Qatar Chemical Company Ltd in pellet form, MFI = 0.18 g/10 min (190 °C/2.16 kg, ASTM D1238) and density = 0.946 g/cm³. The H-PW was supplied in pellet form by TCS Biosciences Ltd, T_m between 56-58 °C. The hv-HDPE and H-PW were first ground to powder yielding a particle size smaller than 250 μ m. The L-PW was supplied by Rubitherm Technologies GmbH and had a T_m in the range of 18 °C - 23 °C.

187 2.2. Sample preparation

SSPCMs based on blends of hv-HDPE with H-PW loadings of 50, 65 and 75 wt% 188 and L-PW loadings of 40, 50 and 65 wt% were prepared by twin-screw extrusion. All blends 189 190 were compounded using a Dr Collin ZK25 twin-screw extruder, having an L/D of 30:1. For 191 hv-HDPE/H-PW blends, the pre-mixed hv-HDPE and H-PW were fed into a hopper and melt blended using a screw speed of 175 rpm. The temperature profile of the extruder was 120, 192 150, 170, 170, 170, 170 °C from zone 1 (feeding zone) to the die end (zone 6), respectively. 193 For hv-HDPE/L-PW blends, the temperature profile of the extruder was 150, 165, 150, 160, 194 160, 160 °C from zone 1 to the die end (zone 6), respectively. hv-HDPE was fed into hopper 195 and L-PW was fed into zone 2 via a peristaltic pump, as it is liquid at RT. The extruder screw 196 197 speed was set at 300 rpm.

All extruded strands were cooled in a water bath and pelletized. The extruded pellets obtained were further compressed into 2 mm (for tensile test) and 4 mm (for flexural and compressive test) thick sheets in a Dr. Collin P200P platen press machine by utilising two rectangular moulds $(135 \times 135 \times 2 \text{ mm} \text{ and } 120 \times 120 \times 4 \text{ mm})$ placed between the platens. Compression moulding of all the samples included four steps. The sheets were pre-heated at 170 °C for 2 minutes between the platens followed by application of a forming pressure of 70 bar for 5 minutes. The sheets were then cooled from 170 °C to 120 °C in 2 minutes and from
120 °C to 50 °C in 3 minutes, and then allowed to cool to room temperature (RT) under
ambient conditions.

207 2.3. Characterisation

Scanning Electron Microscopy (SEM) examination of all materials was carried using 208 a JEOL 6500 JSM840A scanning electron microscope using an operating voltage of 3.0 kV. 209 The specimens used were taken from 2 mm thick compression moulded samples. Fractured 210 surfaces were obtained by fracturing samples in liquid nitrogen and then immersing them in 211 xylene at room temperature to extract the paraffin wax component. This etched surface was 212 investigated by SEM. Specimens were mounted on 25 mm \times 1 mm aluminium discs using 213 Araldite rapid epoxy adhesive, allowed to cure for 24 h and subsequently sputtered with a 214 215 10nm-20nm thick coating of gold on the sample surface so as to impede charging effects and induce conductivity prior to SEM examination. 216

For Fourier Transform Infrared Spectroscopy (FTIR), thin microtomed sections (a few μ m thick) were used for H-PW and all other blends. For L-PW, as it was in the liquid state at RT (20 ± 2°C), a small sample which covered the attenuated total reflectance (ATR) crystal was used. FTIR spectra were collected using a Perkin-Elmer Spectrum 1000 microspectrometer in the spectral range 600-4000 cm⁻¹ at RT (20 ± 2°C), with 4 cm⁻¹ resolution and each spectrum averaged over 16 scans. The spectra of at least three specimens were collected for each sample.

224 X-Ray Diffraction (XRD) studies were carried out with a PANalytical X'Pert Pro 225 Multipurpose Diffractometer using Cu-K_{α} radiation with a wavelength of 1.5406 Å, a 226 scanning rate of 0.63 °C min⁻¹ (step size of 0.02 °) over a 2 θ range of 1-60°. X'Pert 227 HighScore Plus Version 2.2 software was employed to analyse XRD data. 228 Differential Scanning Calorimetry (DSC) analyses of H-PW and hv-HDPE/H-PW blends were completed using a Perkin Elmer DSC 6 instrument under flowing nitrogen (flow 229 rate 20 mL min⁻¹). The instrument was calibrated using the onset temperatures of melting of 230 indium standards, as well as the melting enthalpy of indium. Samples (5–10 mg) were sealed 231 in aluminium pans and heated from 30 °C to 160 °C at a heating rate of 10 K min⁻¹. In all 232 cases, samples were held at 160 °C for 1 min and cooled to 30 °C at 10 K min⁻¹, then 233 reheated again to 160 °C at 10 K min⁻¹. DSC analysis of L-PW and hv-HDPE/L-PW blends 234 was completed using a Perkin Elmer Diamond DSC under flowing nitrogen gas. Samples (5-235 10 mg) were sealed in aluminium pans and heated from 0 °C to 160 °C at a heating rate of 10 236 K min⁻¹. In all cases, samples were held at 160 °C for 1 min and cooled to 0 °C at 10 K min⁻¹ 237 using liquid nitrogen as a coolant, and reheated again to 160 °C at 10 K min⁻¹. Melting point 238 (T_m) and enthalpies of melting (ΔH_m) were determined from the second scan. All DSC 239 240 measurements were repeated at least three times for each sample.

Thermo-gravimetric Analysis (TGA) was carried out in a TGA Analyser TGA/SDTA 851e/LF/1600/1382 (Mettler Toledo). Specimens ranging between 5 mg and 10 mg of each sample was loaded in aluminium pans and heated from 30 °C to 600 °C at a heating rate of 10 K min⁻¹ under flowing nitrogen (flow rate 50 ml min⁻¹). The onset decomposition temperatures were determined from the weight loss curve by extrapolating the curve at 5 wt% weight loss for each blend.

247 Dynamic properties (storage modulus (E'), loss modulus (E'') and tan δ) of all samples 248 with dimensions of 10mm × 10mm × 1mm were measured using a Tritec 2000 dynamic 249 mechanical thermal analysis (DMTA) instrument. The experiments were conducted in the 250 temperature range -100 °C to 100 °C using a heating rate of 2 K min⁻¹ and a frequency of 1 251 Hz. Tests were conducted in single cantilever bending mode at 0.05 mm controlled 252 displacement.

Tensile testing of hv-HDPE, hv-HDPE/H-PW and hv-HDPE/L-PW specimens was 253 carried out using an Instron 5564 twin column tensile tester with a 5 kN load cell along with a 254 2603-080 long travel extensometer using a 25 mm gauge length according to ISO 527-255 256 1:1996. A minimum of five dumbbell samples for each blend composition was loaded to the maximum strain of 1 mm or to failure at crosshead speeds of 5 mm min⁻¹ and 50 mm min⁻¹, 257 respectively. The dumbbell samples had a total length of 75 mm, a gauge length of 24 mm, a 258 neck width of 5 mm, and a thickness of 2 mm. The thickness and width of the samples were 259 determined using a micro-meter prior to testing. All tensile properties (including Young's 260 261 modulus, yield stress and elongation at break) were extracted from stress-strain curves using Merlin software (Version 5.51). Young's modulus was estimated from the slope of initial 262 linear region of the stress-strain curves up to 2.5% strain. Analysis of variance (ANOVA) 263 264 was used to test for significant differences among the mean of the tensile property of interest 265 by quantifying the differences with the aid of Data Analysis ToolPak in Ms Excel, and the pvalue was set to 5%. 266

Flexural strength and modulus of hv-HDPE, hv-HDPE/H-PW and hv-HDPE/L-PW samples were measured in three-point bending tests using the same machine as that for tensile testing. Both flexural properties are of interest in the assessment of the blends as to whether they have sufficient mechanical strength for practical applications, e.g. in wallboards. The crosshead speed was 5 mm min⁻¹ and specimens with dimensions of 80mm ×10mm × 4mm (thickness) were cut from compression moulded plates of each blend by a band saw according to ISO 178. At least five specimens from each sample were tested.

274 Compression testing was performed on all specimens employing a strain rate of 5 mm 275 min⁻¹ using an EZ 50 testing machine from Lloyd Instruments Ltd with a 5 kN load cell. 276 According to ISO 604, samples with dimensions of $10 \text{mm} \times 10 \text{mm} \times 4 \text{ mm}$ were cut from

the centre part of moulded plates of each blend. At least 6 specimens were tested for each blend composition and all tests were performed at ambient conditions of 20 ± 2 °C.

The capillary rheological behaviour of hv-HDPE, hv-HDPE/H-PW and hv-HDPE/L-PW samples in the shear rate range 50s⁻¹ to 1500s⁻¹ was investigated using a Bohlin Rosand RH2000 Capillary Rheometer with a 0.5 mm die and utilising the Rosand Flowmaster Precision Software. The rheological data obtained was Bagley corrected, to account for the non-linear pressure drop at the die entrance, thus correcting for wall shear stress and giving the true shear stress in capillary die [36, 37].

An oscillatory melt rheology study was carried out for hv-HDPE, hv-HDPE/H-PW and hv-HDPE/L-PW samples. Dynamic rheological measurements were performed using a HAAKE MARS rotational rheometer. The measurements were carried out in an oscillatory shear mode using parallel plate geometry (Standard Aluminium plate, 25 mm diameter, 1 mm gap) at 160 °C, 170 °C and 180 °C. Frequency sweeps from 1000 rad/s to 0.1 rad/s were carried out at low stress (2Pa) which was shown to be within the linear viscoelastic limit of all the materials used in this study.

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293 **3. Results and discussion**

The surfaces of the hv-HDPE₃₅H-PW₆₅ and hv-HDPE₃₅L-PW₆₅ blends are shown in 294 Figure 1 (a) and (b), respectively (scale bar 1µm). Both images indicate that hv-HDPE forms 295 a 3D interconnected structure and the waxes are well dispersed within it. The hv-HDPE 296 provides mechanical strength to the whole compound, and so the composite material keeps its 297 shape in the solid state. Some voids on the surface of hv-HDPE₃₅L-PW₆₅ (b), (indicated with 298 arrows) were observed, perhaps as a consequence of air trapped during the manufacturing 299 300 process or the expulsion of wax. The same two surfaces are shown in Figure 1 (c) and (d) but after treatment with xylene to extract the wax component. It can be seen that there are many 301

302 voids in the etched surface of hv-HDPE₃₅H-PW₆₅ (Fig. 1 (c)), indicative of where the H-PW resided in the hv-HDPE and again showing this wax to be well dispersed and distributed 303 throughout the hv-HDPE matrix [20]. On the etched surface of hv-HDPE₃₅L-PW₆₅ (Figure 1 304 (d)), the holes are less obvious than those observed in Figure 1 (c). This may be because the 305 L-PW with smaller molecular size penetrated the hv-HDPE to a greater extent, including the 306 crystalline lamellae, than H-PW. The fractured surfaces of the hv-HDPE₃₅H-PW₆₅ and hv-307 HDPE₃₅L-PW₆₅ blends are shown in Figure 1 (e) and (f), respectively. More numerous voids 308 and deformed structure were observed in Figure 1 (e). These were formed as the paraffin was 309 310 pulled out when cryo-fracturing the sample, due to the limited wetting of the soft phase. In contrast, the voids observed in the hv-HDPE₃₅L-PW₆₅ blend are less obvious and a less rough 311 surface observed, Figure 1 (f). 312

As hv-HDPE and both waxes are non-polar, FTIR was used to confirm that blends of hv-HDPE with both waxes were physical mixes, see Figure 2 (a) and (b). The spectra obtained show four main characteristic IR bands at approximately 720 cm⁻¹, 1474 cm⁻¹, 2849 cm⁻¹ and 2912 cm⁻¹, which were assigned to CH₂ rocking, CH₂ bending, CH₂ stretching and CH₂ stretching, respectively [38]. There was no change of peak position and no new peaks generated for all samples, suggesting that there is no chemical interaction between the hv-HDPE and waxes.

The crystalline content of H-PW, hv-HDPE and all blends was determined from the XRD diffractorgrams obtained at RT (Figure 3 (a) and (b)) for the hv-HDPE/H-PW and hv-HDPE/L-PW blends), respectively. Two sharp reflection peaks at approximately $2\theta = 21.5^{\circ}$ and 23.8° appear in the diffractograms for all composites, which can be assigned to the 110 and 200 basal planes of the orthorhombic crystal form of PE [38, 39]. Both peaks are more intense in the H-PW sample, indicating that it has higher crystalline content (93%) and more regular structure than hv-HDPE (52%). In all cases the crystalline content was determined 327 from the ratio of crystalline to amorphous component in the blend with the aid of Jade 6.0 software [40, 41]. L-PW is liquid at RT and is thus non-crystalline. As the H-PW loading was 328 increased from 50 wt% to 75 wt% when blended with hv-HDPE, the crystalline content of the 329 330 blends increased up to 72%, higher than that of pure hv-HDPE. In contrast, the crystalline content of the blends decreased to a low of 33% with increasing L-PW content (up to 65 331 wt%) and all values were lower than that of pure hv-HDPE itself. This may be associated 332 with the penetration of the shorter chain L-PW into the HDPE lamellar structure during 333 cooling, inhibiting hv-HDPE crystallisation. 334

335 The crystalline behaviour and thermal properties of these blends were also studied using DSC, see Figure 4. Melting peaks associated with both hv-HDPE and the respective 336 waxes were identified in the DSC thermograms. T_m of H-PW remained fairly constant, within 337 338 experimental error, with increasing wax content for all blends. However, an increase in wax content resulted in a decrease in $T_{\rm m}$ of hv-HDPE in hv-HDPE/H-PW blends. $T_{\rm m}$ of L-PW 339 increased slightly with increasing L-PW content in the blends, but again T_m for hv-HDPE in 340 the hv-HDPE/L-PW blends deceased with increasing hv-HDPE content. This we assume is a 341 result of the plasticisation effect of both H-PW and L-PW on the hv-HDPE matrix as wax 342 that crystallised separately melted before hv-HDPE, and this molten wax acted as a plasticiser 343 [24-26]. However, the wax that co-crystallised with hv-HDPE chains melted at the same 344 temperature as the hv-HDPE, and therefore did not contribute to the plasticising effect of the 345 346 wax.

As shown in Table 1, the experimentally observed melting enthalpies (ΔH_m) of H-PW are lower than the calculated enthalpies ($\Delta H_{m\delta}$). The $\Delta H_{m\delta}$ values were determined from the melting enthalpy of the unblended pure H-PW compensating for the fraction of H-PW in the hv-HDPE/H-PW blends. The difference between the two enthalpies became insignificant with increasing wax content, indicating that some portion of H-PW partially co-crystallised 352 with hv-HDPE. The difference between the observed and the calculated enthalpies was for the hv-HDPE/L-PW blends as shown in Table 2, as there was little or no co-crystallisation 353 between hv-HDPE and L-PW [27]. The cooling curves of all samples can be seen in Figure 4 354 355 (b) and (d). The solidification point of H-PW in hv-HDPE/H-PW blends was almost constant while the crystallisation point of L-PW in hv-HDPE/L-PW blends shifted to lower 356 temperatures. The solidification point of hv-HDPE in hv-HDPE/H-PW blends shifted to 357 358 lower temperatures with increasing wax content, while the solidification point of hv-HDPE in hv-HDPE/L-PW blends remained almost constant. Again, there is less co-crystallisation of 359 360 hv-HDPE with L-PW relative to that with H-PW [26, 27]. The enthalpy of fusion (ΔH_c) of H-PW in hv-HDPE/H-PW blends was lower than the theoretical values expected, clearly 361 obvious for the 50:50 blend, see Table 3, again as a consequence of co-crystallisation of hv-362 363 HDPE and H-PW [27]. ΔH_c for L-PW in hv-HDPE/L-PW blends were lower than the theoretical values expected (Table 4). In this instance, there may be a contribution associated 364 with evaporation of some L-PW during the heating cycles in the DSC instrument. 365

TGA and DTG curves for H-PW, hv-HDPE and all hv-HDPE/H-PW blends are 366 shown in Figure 5 (a) and (b), while those for L-PW, hv-HDPE and hv-HDPE/L-PW blends 367 are shown in Figure 5 (c) and (d), respectively. For all the blends thermal stability decreased 368 with increasing wax content, as the waxes have much shorter chains and more thermally 369 labile than pure hv-HDPE [42]. Both hv-HDPE/H-PW and hv-HDPE/L-PW blends degraded 370 371 via two clearly distinguishable steps. Such degradation behaviour is typical for immiscible blends in which the components have different degradation temperatures [18]. For all the 372 blends the percentage mass loss during the first degradation step correlated well with the 373 374 amount of wax initially added to the blend. The second step was associated with hv-HDPE degradation [43]. The degradation products are mainly hydrocarbon compounds, e.g. alkanes 375 376 (methane, ethane and propane), alkenes (ethylene and propylene) and di-alkenes (butadiene)

377 [44, 45]. It can be seen from the DTG curves (Figure 5 (b)) that when the temperature reached about 220 °C, H-PW started to decompose or evaporate until none remained at 440 °C. In the 378 second period when the temperature reached 450 °C, hv-HDPE started to decompose and was 379 380 fully decomposed at 510 °C leaving no residues. From Figure 5 (d), L-PW started to decompose at around 130 °C, peaked at about 190 °C, but none remained at 250 °C. The 381 decomposition behaviour of hv-HDPE was again similar to that shown in Figure 5 (b), as 382 383 expected. Thus, we propose that mixing paraffin waxes with molten HDPE using twin screw extrusion is readily feasible as long as the wax of interest is thermally stable at the melt 384 385 processing temperatures, in this instance of HDPE (~160 °C).

The results of the dynamic mechanical thermal analysis (DMTA) of all the 386 investigated samples are shown in Figure 6. Plots of tan δ versus temperature, Figure 6 (a) 387 388 and (b), show that the hv-HDPE/H-PW blends had two relaxation maxima, one centred at 389 around -60 °C, the other at about 56 °C. The first relaxation peak around -60 °C could be assigned to the glass transition of H-PW [46]. In contrast, for unfilled hv-HDPE no obvious 390 peak in tan δ was obtained in the temperature range examined. The latter peak around 56 °C 391 could be attributed to a solid-liquid transition in H-PW [47]. Similar behaviour was observed 392 for the hv-HDPE/L-PW blends, which can be explained in a similar manner. As expected, the 393 storage modulus E', as function of temperature, decreased with increasing wax content for all 394 395 blends (Figure 6 (c) and (d)), again evidence for plasticising of hv-HDPE by the wax 396 component. Also, there are large differences in mechanical properties due to the different structures and molar masses between wax and hv-HDPE [48]. As can be seen from Figure 6 397 (c), E' instead of an immediate decrease, decreased gradually after H-PW had completely 398 399 melted in the high temperature region, similarly for all the blends, indicating that hv-HDPE forms a continuous phase in all the blends even at high wax content [48, 49]. A similar 400 401 conclusion can be made for the hv-HDPE/L-PW blends.

Plots of loss modulus (E'') versus temperature, see Figure 6 (e) and (f), show that 402 pure hv-HDPE has two relaxation maxima, one centred at around -25 °C and the other at 403 about 45 °C. The first maximum is derived from the glass transition (T_g) of the hv-HDPE 404 405 phase, although this continues to be a matter of fundamental scientific discussion. The latter peak is the α relaxation, related to the onset of molecular motion in the crystalline phase [50]. 406 However, the two peaks shifted to lower temperatures for the hv-HDPE/H-PW blends, to 407 about -60 °C and 30 °C, respectively. Again, this is strong evidence for a plasticisation effect 408 by the wax component on the hv-HDPE matrix [48]. From Figure 6 (f), the two relaxation 409 410 peaks in the hv-HDPE/L-PW blends decreased significantly, almost disappearing, as the wax content was increased. The material is becoming more viscous/less elastic due to a reduction 411 in chain dynamics (relaxation) of the hv-HDPE phase [48]. 412

413 Static tensile testing was performed at room temperature (RT) on hv-HDPE, hv-HDPE/H-PW and hv-HDPE/L-PW blends. The Young's moduli (E) of both hv-HDPE/H-PW 414 and hv-HDPE/L-PW blends were lower than that of pure hv-HDPE (see Figure 7 (a)). In both 415 416 instances, E decreased with increasing wax content up to about 40 wt%, from 700MPa for unfilled hv-HDPE down to 410MPa and 160MPa for H-PW and L-PW addition, respectively. 417 The difference in the increment between the moduli of both sets of blends is associated with 418 the higher relative crystallinity of H-PW. Further successive additions of either wax did not 419 420 result in a statistically significant change in E, as assessed by ANOVA analysis. The yield 421 stress of hv-HDPE/H-PW blends (see Figure 7 (b)) decreased with increasing H-PW content, which is as expected as the H-PW is weaker than hv-HDPE [51]. However, the yield stress of 422 hv-HDPE/L-PW blends decreased first, up to 50 wt%, but then formed a plateau when 423 424 increasing the L-PW content to 65 wt%. It can be seen that yield stress of the hv-HDPE/H-PW blends was much higher than that of hv-HDPE/L-PW blends, as L-PW is weaker and 425 426 softer than H-PW, so when added to hv-HDPE the resulting blends are more easily deformed.

This is also related to the lower crystalline content of the blends with L-PW, see Table 1. The 427 change in strain at break for hv-HDPE, hv-HDPE/H-PW and hv-HDPE/L-PW blends is 428 shown in Figure 7 (c), and as expected the strain at break for the hv-HDPE/H-PW blends is 429 430 much lower than that of hv-HDPE/L-PW blends. This behaviour can be further explained by examining the stress-strain curves for these blends, see Figure 8. Strain-hardening before 431 break was observed for pure hv-HDPE sample, while no strain-hardening was observed for 432 433 the hv-HDPE/H-PW blends (Figure 8 (a)). The strain at break of hv-HDPE is much higher than that of hv-HDPE/H-PW blends. This is because the polymer chains have the free volume 434 435 and time to orientate when the tensile force is applied. When the chains are oriented, they start to align and crystallise (strain induced crystallisation), which gives rise to an increase in 436 both strength and strain at break [52]. However, adding H-PW in such large loadings to the 437 438 polymer matrix reduces polymer chain mobility (hinders dynamics), resulting in a rapid 439 decrease in strain at break. An increase in H-PW content resulted in a decrease in strain at break for all hv-HDPE/H-PW blends (Figure 8 (a)). This can also be explained by the more 440 crystalline and numerous H-PW crystals acting as defect points for the initiation and 441 propagation of stress cracking [53]. Strain-hardening before break was observed for all hv-442 HDPE/L-PW samples, see Figure 8 (b). Strain at break for the hv-HDPE/L-PW blends is 443 much larger than that for the hv-HDPE/H-PW blends, as the smaller non-crystalline L-PW 444 molecules penetrated the hv-HDPE matrix and did not act as a barrier to 445 446 stretching/deformation. Moreover, the strain at break of all hv-HDPE/L-PW blends decreased with increasing L-PW content, probably because the average tie chain concentration in the 447 composites decreased with increasing L-PW content (reduced hv-HDPE content) [53]. 448

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The changes in flexural modulus and stress of the hv-HDPE/H-PW and hv-HDPE/L-PW blends as a function of wax content are shown in Figure 9 (a) and (b), respectively. Both properties for the hv-HDPE/H-PW blends are much higher than those of the hv-HDPE/L-PW 453 blends. We suppose that as the L-PW is weaker than H-PW and in the molten state at RT, it cannot provide limited mechanical strength when under flexural stress. The flexural modulus 454 and stress decreased with increasing wax content in all blends, not unexpected as the waxes 455 456 are much weaker than neat hv-HDPE (see Figure 9 (c) and (d)). It is worth noting that this is an important consideration should such materials find civil engineering application(s). The 457 change in compression moduli with wax content for all samples is shown in Figure 10 (a), 458 and the stress-strain data from compression testing of hv-HDPE/H-PW and hv-HDPE/L-PW 459 blends is Figure 10 (b) and (c), respectively. The compression modulus of hv-HDPE/H-PW 460 461 blends is higher than that of hv-HDPE/L-PW blends. As the crystalline content for the hv-HDPE/L-PW blends is much lower than that of hv-HDPE/H-PW blends, it was expected that 462 the compression modulus should also be lower for the blends with L-PW added. The 463 464 compression modulus decreases with increasing wax content for all blends as the waxes are 465 much softer mechanically compared to pure hv-HDPE, but to a great extent for the blends with L-PW addition. 466

467 As a further consideration if such SSPC materials are to be readily manufactured using polymer processing methods, such as with twin screw extrusion, the melt rheological 468 behaviour of these blends must be understood at high shear rates. To this end, the effect of 469 shear rate on shear viscosity of pure hv-HDPE, hv-HDPE/H-PW and hv-HDPE/L-PW blends 470 was investigated by dual capillary rheology at 160 °C, 170 °C and 180 °C in the shear rate 471 range 50 s⁻¹ - 1500 s⁻¹. This shear rate range covers the shear typically employed during 472 polymer extrusion. The data obtained from rheological measurements were Bagley corrected 473 in order to obtain true shear stress values by taking into account the pressure drop at the 474 475 entrance of the die, along its length and at its exit [36, 37, 54]. By way of example, Figure 11 (a) and (b) show the results obtained at 160 °C for both sets of blends. It is as expected, that 476 by increasing screw speed, the shear stress and the energy added to the system increased and 477

478 consequently the shear viscosity decreased making the system more favourable for wax dispersion and distribution in the hv-HDPE matrix. Furthermore, for a similar wax addition 479 the melt viscosity of the blends with L-PW were lower than those with H-PW – in the shear 480 rate range examined (50 s⁻¹ - 1500 s⁻¹). Similar behaviour was found for the measurements at 481 170 °C and 180 °C. The lower viscosity of the blends would imply that it could be more 482 easily melt processed an important consideration in the manufacturing step, if for example 483 sheets of such materials were to be used in construction applications. This is associated with 484 the lower viscosity of molten wax compared with that of hv-HDPE. By increasing the 485 486 temperature, the total energy added to the system during the mixing process increases and consequently the shear viscosity is expected to decrease. However, as it can be seen from 487 Figure 11 (c), the difference between the shear viscosity of hv-HDPE₅₀H-PW₅₀ measured at 488 489 160 °C, 170 °C and 180 °C cannot be regarded as significant. Similar results were found for 490 hv-HDPE₅₀L-PW₅₀, Figure 11 (d). This might be explained by that as each blend is consisted of a considerable large proportion of wax with a melting point far below 160 °C, the effect of 491 492 increment of temperature from 160 °C to 170 °C or from 170 °C to 180 °C on the shear viscosity for the blends is not significant. Thus, 160 °C is an adequate processing 493 temperature. This is an important consideration as the lower the temperature, the less energy 494 required to mix the blend components, but also less evaporation of wax, especially for hv-495 HDPE/L-PW blends. 496

To further investigate the interaction between and dispersion of wax in hv-HDPE, an oscillatory melt rheology study, at low shear rates, was also carried out. Polymers exhibit viscoelastic behaviour which is directly related to molecular structure. In order to evaluate the relationship between molecular structure and viscoelastic behaviour it is necessary to perform rheological experiments in the linear viscoelastic region where the viscoelastic properties observed are independent of imposed stress or strain level. An oscillatory stress sweep test

503 was performed to establish the linear viscoelastic region and determine the maximum stress for linear behaviour at 160 °C. The limit of the viscoelastic regime for each material is 504 determined by the stress value when the moduli (G' and G") start to decrease becoming non-505 506 linear. In this study, a stress value of 2Pa was selected as all the samples were in linear viscoelastic region at this value. As shown in Figure 12 (a) and (b), with increasing 507 frequency, the storage modulus G' increased for all samples, approximately by two orders of 508 magnitude. G' of hv-HDPE is higher than the two sets of the blends. With increasing wax 509 content, G' decreased. This is associated with the less viscous property of the waxes at 510 511 elevated temperatures. However, the plots of hv-HDPE₃₅H-PW₆₅ and hv-HDPE₂₅H-PW₇₅ were nearly overlapping, and lie below that for hv-HDPE₅₀H-PW₅₀, see Figure 12 (a). G' of 512 the three hv-HDPE/L-PW composites were very similar in the low frequency region and 513 514 separated at high frequencies, as shown in Figure 12 (b). Plots of log shear viscosity η' vs log frequency f are shown in Figure 12 (c) and (d). With increase f, η' decreased in all samples. 515 This is because when shear rate increased, the entanglement of the molecular of hv-HDPE 516 decreased. With increasing wax content, the viscosity of all composites decreased, again 517 associated with the less viscous properties of the waxes. However, the difference between 518 the viscosity values of hv-HDPE₃₅H-PW₆₅ and hv-HDPE₂₅H-PW₇₅ is not significant. A Cole-519 Cole plot (Log G' versus log G" plot) is a sensitive tool that can probe composite 520 miscibility/compatibility in that changing slopes of the linear relationship between both 521 522 parameters can indicate poor interaction, in this instance between hv-HDPE and wax. Curves corresponding to different wax content deviate slightly from each other and from pure hv-523 HDPE, Figure 12 (e) and (f), and indicated less interaction between hv-HDPE and wax at 524 525 higher wax loading, evidence for induced heterogeneity within the composite material [55, 5**6**]. 526

528 4 Conclusions

Both H-PW and L-PW could be mixed uniformly with hv-HDPE to form SSPCMs 529 using twin screw extrusion, and the blends formed are physical mixes with no evidence of 530 531 chemical interaction between blend components. The extrusion temperature for hv-HDPE/L-PW blends should not be > 160 °C, as the onset of the evaporation temperature of L-PW is 532 relatively low, ≤ 130 °C. However, the extent of L-PW evaporation we assume is low as the 533 residence time of L-PW in the extruder is less than 30 sec. No such consideration is required 534 for blends prepared with H-PW. The SSPCMs had latent heats up to 89 J/g (hv-HDPE₂₅H-535 PW₇₅), as determined from DSC analysis and thus these composite materials are candidates 536 for LHTES applications. The enthalpy of H-PW in SSPCM blends decreased while that of L-537 PW remained unaltered, as a consequence of co-crystallisation between H-PW and hv-HDPE. 538 539 DMTA analyses show the plasticising effect of both waxes on the hv-HDPE matrix. The mechanical properties, moduli and stress, irrespective of mode of deformation are much 540 greater for the hv-HDPE/H-PW blends compared with those of the hv-HDPE/L-PW blends at 541 RT. The tensile and flexural strength of hv-HDPE/H-PW blends were much greater than hv-542 HDPE/L-PW blends at RT. The rheological behaviour of these blends confirmed increased 543 heterogeneity with increasing wax content and that melt processing such SSPCMs with 544 conventional polymer processing techniques should be routine, at least for the wax loadings 545 used in this study. Further studies are ongoing to address some of the many limitations of 546 547 such SSPCMs [57], e.g. thermal conductivity, and will be reported shortly.

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| 711 | Table | and Figure Captions |
| 712 | Table | 1 Thermal properties of hv-HDPE/H-PW blends (melting) as determined from DSC |
| 713 | measur | rements. |
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| 719 | DSC n | neasurements. |
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| 722 | PW ₆₅ a | after xylene treatment; (e) fractured surface of $hv-HDPE_{35}H-PW_{65}$ and (f) fractured |
| 723 | surface | of $hv-HDPE_{35}H-PW_{65}$. |
| 724 | Figure | 2 FTIR spectra of (a) H-PW, hv-HDPE and hv-HDPE/H-PW blends, and (b) L-PW, |
| 725 | hv-HD | PE and hv-HDPE/L-PW blends. |

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hv-HDPE and hv-HDPE/L-PW blends.

Figure 4 DSC thermograms for (a) heating curves of H-PW, hv-HDPE and hv-HDPE/H-PW
blends; (b) cooling curves of H-PW, hv-HDPE and hv-HDPE/H-PW blends; (c) heating
curves of L-PW, hv-HDPE and hv-HDPE/L-PW blends and (d) cooling curves of L-PW, hvHDPE and hv-HDPE/L-PW blends.

Figure 5 TGA curves for (a) H-PW, hv-HDPE and hv-HDPE/H-PW blends; DTG curves for
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hv-HDPE/L-PW blends and DTG curves for (d) L-PW, hv-HDPE and hv-HDPE/L-PW
blends.

Figure 6 DMTA results of (a) Tan δ of hv-HDPE and hv-HDPE/H-PW blends; (b) Tan δ of
hv-HDPE and hv-HDPE/L-PW blends; (c) storage modulus (E') for hv-HDPE and hvHDPE/H-PW blends; (d) E' for hv-HDPE and hv-HDPE/L-PW blends; (e) loss modulus (E")
of hv-HDPE and hv-HDPE/H-PW blends; (f) E" of hv-HDPE and hv-HDPE/L-PW blends, as
a function of temperature.

Figure 7 Tensile testing results of variation in (a) Young's modulus, (b) yield stress and (c)
strain at break of hv-HDPE, hv-HDPE/H-PW and hv-HDPE/L-PW blends, as a function of
wax content.

Figure 8 Stress-strain curves of (a) hv-HDPE and hv-HDPE/H-PW blends and (b) hv-HDPE
and hv-HDPE/L-PW blends.

Figure 9 Flexural testing results of variation in (a) flexural modulus and (b) flexural stress of
hv-HDPE, hv-HDPE/H-PW and hv-HDPE/L-PW blends, as a function of wax content; stress-

strain curves for (c) hv-HDPE and hv-HDPE/H-PW blends and (d) hv-HDPE and hvHDPE/L-PW blends.

Figure 10 Compression testing results of (a) variation in compression modulus of hv-HDPE,
hv-HDPE/H-PW and hv-HDPE/L-PW blends, as a function of wax content; stress-strain
curves for (a) hv-HDPE and hv-HDPE/H-PW blends and (b) hv-HDPE and hv-HDPE/L-PW
blends.

Figure 11 Capillary rheology: plots of log shear viscosity versus log shear rate for (a) hv-HDPE and hv-HDPE/H-PW and (b) hv-HDPE and hv-HDPE/L-PW blends at 160 °C; plots of log shear viscosity versus log shear rate for (c) hv-HDPE50H-PW50 and (d) hv-HDPE50L-PW50 blends at three different temperatures.

Figure 12 Oscillatory rheology: plots of log G' versus log f for (a) hv-HDPE and hvHDPE/H-PW blends and (b) hv-HDPE and hv-HDPE/L-PW blends; plots of log η' versus log
f plot of (c) hv-HDPE and hv-HDPE/H-PW blends and (d) hv-HDPE and hv-HDPE/L-PW
blends; plots of log G' versus log G'' (Cole-Cole plots) for (e) hv-HDPE and hv-HDPE/H-PW
blends and (f) hv-HDPE and hv-HDPE/L-PW blends, at 160 °C.

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Table 1

| | - | 411 | 411 | T / | Τ/ | 4114 | 4112 | |
|----------|----------|----------------------|----------------------|------------|----------|----------|------------------|---------|
| NV-HDPE/ | I m peak | ΔHm | $\Delta H_{m\delta}$ | I m onset | I m peak | ΔH m | ΔH _{mõ} | |
| H-PW | (°°) | (J g ⁻¹) | (J g⁻¹) | (°C) | (°C) | (J g⁻¹) | (J g⁻¹) | X´c (%) |
| 100/0 | | | | 120 | 130 | 151±3 | | 51.5 |
| 50/50 | 56 | 47±1 | 60.3 | 114 | 121 | 75.2±4.2 | 75.5 | 51.3 |
| 35/65 | 56 | 74±4.5 | 78.4 | 111.5 | 118 | 56.7±2.3 | 52.9 | 55.3 |
| 25/75 | 56 | 89±3.5 | 90.4 | 110.5 | 116 | 42±3.9 | 37.8 | 57.3 |
| 0/100 | 56.8 | 121+4 | | | | | | |



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Table 2

 $T_{m peak}$, ΔH_m and $\Delta H_{m\delta}$ are the melting peak temperature, observed melting enthalpy and calculated melting enthalpy of H-PW, respectively. T'_{m peak}, Δ H'_m and Δ H'_m^{*} are the melting peak temperature, observed melting enthalpy and calculated melting enthalpy of the HDPE, respectively. X'_c is the crystallinity of the blends.

| | _ | | | | _ | | | |
|----------|---------------------|--------------|----------------------|-----------|----------|---------|---------|---------|
| hv-HDPE/ | T _{m peak} | ΔH_m | $\Delta H_{m\delta}$ | T´m onset | T´m peak | ∆H´m | ΔH´mõ | |
| L-PW | (Ô°) | (J g⁻¹) | (J g⁻¹) | (°C) | (Ô°) | (J g⁻¹) | (J g⁻¹) | X´c (%) |
| 100/0 | | | | 120 | 130 | 151±3 | | 51.5 |
| 60/40 | 26 | 43±3 | 49.2 | 112 | 120 | 80±6 | 90.6 | 47.2 |
| 50/50 | 25 | 61±2 | 61.5 | 110 | 118 | 78±8 | 75.5 | 53.2 |
| 35/65 | 25 | 70±5 | 79 | 109 | 117 | 61±5 | 54 | 595 |
| 0/100 | 24 | 122+7 | | | | | | |

786 787 788 $T_{m peak}$, ΔH_m and $\Delta H_{m\delta}$ are the melting peak temperature, observed melting enthalpy and calculated melting enthalpy of L-PW, respectively. T'm peak, Δ H'm and Δ H'm³ are the melting peak temperature, observed melting enthalpy and calculated melting enthalpy of the HDPE, respectively. X'_c is the crystallinity of the blends.

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 $\Delta H_{c\delta}$ ∆H´_{cδ} (J g⁻¹) hv-HDPE/ T´c onset ∆H´_c (J g⁻¹) T_{c peak} ΔH_{c_1} T[´]c peak H-PW (°C) (°Ċ) (J g (°C) (Jg 100/0 143±4 114.2 110.5 50/50 106.5 71.5 45 51±2.2 64 104 75±4.2 35/65 44 79±4.1 83.2 105 102 57±2.3 50 25/75 45 96 103 100.5 42±3.9 35.8 94±4.1 0/100 45 128±3.8 -----

Table 3

794 795 796 $T_{c\,peak}$, ΔH_c and $\Delta H_{c\delta}$ are the crystallisation peak temperature, observed crystallisation enthalpy and calculated crystallisation enthalpy of H-PW, respectively. $T'_{c peak}$, $\Delta H'_{c}$ and $\Delta H'_{c\delta}$ are the crystallisation peak temperature, observed crystallisation enthalpy and calculated crystallisation enthalpy of the blends, respectively.

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Table 4

| hv-HDPE/ L-PW | T _{c peak} (℃) | ∆H _c (J g ⁻¹) | ∆H _{cδ} (J g ⁻¹) | T´ _{c onset} (℃) | T´ _{c peak} (℃) | ∆H´ _c (J g ⁻¹) | ∆H´ _{cδ} (J g ⁻¹) |
|------------------|----------------------------|---|--|------------------------------|-----------------------------|--|---|
| 100/0 | | | | 114.2 | 110.5 | 143±4 | |
| 60/40 | 20 | 40±5 | 52 | 113 | 109.5 | 82±4 | 85.8 |
| 50/50 | 19.5 | 56±4 | 65 | 112.5 | 109 | 62±6 | 71.5 |
| 35/65 | 19.5 | 64±5 | 84.5 | 112 | 108.5 | 53.6±4 | 50 |
| 0/100 | 22 | 130±8 | | | | | |

 $\begin{array}{l} \textbf{R} \\ \textbf$



Figure 2











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Figure 4

(b) (a) H-PW Heat flow /mW Endo —≫ H-PW $\mathsf{HDPE}_{25}\mathsf{H}\text{-}\mathsf{PW}_{75}$ Heat flow /mW Endo $\mathsf{HDPE}_{25}\mathsf{H}\text{-}\mathsf{PW}_{75}$ HDPE₃₅H-PW₆₅ HDPE35H-PW65 HDPE₅₀H-PW₅₀ HDPE₅₀H-PW₅₀ HDPE HDPE 70 90 30 50 110 130 150 70 30 50 90 110 130 150 Temperature /°C Temperature /°C 875 (d) L-PW (c) L-PW HDPE₃₅L-PW₆₅ Heat flow /mW Endo —> Heat flow /mW Endo HDPE₃₅L-PW₆₅ HDPE₅₀L-PW₅₀ HDPE₅₀L-PW₅₀ HDPE₆₀L-PW₄₀ HDPE₆₀L-PW₄₀ hv-HDPE hv-HDPE 60 80 100 120 140 160 0 20 40 0 20 60 80 100 120 140 160 40 Temperature /°C Temperature /°C 876 877 878 879

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Figure 6









Figure 8









Figure 10 (a) hv-HDPE/H-PW Compression modulus /MPa Ŧ

hv-HDPE/L-PW

10 20 30 40 50 60 70 80

Wax content /%







Figure 11



