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| 1 | Thermodynamic modelling of alkali-activated slag |
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| 2 | cements |
| 3 | |
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| 14 | 114 222 5490, fax +44 114 222 5493 |
| 15 | |
| 16 | Keywords |
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| 18 | Thermodynamic modelling; alkali-activated slag cement; C-A-S-H; phase diagram; layered double |
| 19 | hydroxide; zeolite |
| 20 | |
| 21 | Abstract |
| 22 | |
| 23 | This paper presents a thermodynamic modelling analysis of alkali-activated slag-based cements, |
| 24 | which are high performance and potentially low-CO ₂ binders relative to Portland cement. The |

25 thermodynamic database used here contains a calcium (alkali) aluminosilicate hydrate ideal solid 26 solution model (CNASH ss), alkali carbonate and zeolite phases, and an ideal solid solution model for a hydrotalcite-like Mg-Al layered double hydroxide phase. Simulated phase diagrams for NaOH-27 and Na₂SiO₃-activated slag-based cements demonstrate the high stability of zeolites and other solid 28 29 phases in these materials. Thermodynamic modelling provides a good description of the chemical compositions and types of phases formed in Na₂SiO₃-activated slag cements over the most relevant 30 bulk chemical composition range for these cements, and the simulated volumetric properties of the 31 cement paste are consistent with previously measured and estimated values. Experimentally 32 determined and simulated solid phase assemblages for Na₂CO₃-activated slag cements were also 33 found to be in good agreement. These results can be used to design the chemistry of alkali-activated 34 35 slag-based cements, to further promote the uptake of this technology and valorisation of metallurgical 36 slags.

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39 **1. Introduction**

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41 Development of high performance and low CO_2 cement-based materials is needed to reduce the CO_2 footprint of the construction industry. Alkali-activated cements are formed through the reaction of a 42 soluble alkali source (the 'activator'), water and aluminosilicate precursors, which are often sourced 43 44 as industrial by-products (Provis, 2014). Blast furnace slag is one such material, and forms an 45 important component of many modern cements, including use as the main raw material in production of alkali-activated slag (AAS) cements (Provis and Bernal, 2014). The reactive component of blast 46 furnace slag is a calcium-magnesium aluminosilicate glass that dissolves under the high pH conditions 47 provided by the activator to form a hydrated phase assemblage that consolidates into a hardened 48 49 binder. AAS-based cements are attractive solutions for waste valorisation and utilisation of industrial by-products, e.g. in immobilisation matrices for radioactive wastes (Bai et al., 2011), and can provide 50 substantial CO₂ savings relative to Portland cement (PC)-based materials (McLellan et al., 2011). 51

52 Understanding the durability of alkali-activated cements is a key scientific challenge facing their 53 commercial uptake and utilisation (van Deventer et al., 2012). Durability is intimately linked to the 54 chemistry and microstructure of these cements, and thus depends on physicochemical factors 55 including chemical shrinkage and the solid phase assemblage formed.

56

The main component of hardened AAS-based materials is a calcium (alkali) aluminosilicate hydrate 57 (C-(N-)A-S-H) gel¹ that is poorer in Ca (molar Ca/Si ratio ≈ 1 (Shi et al., 2006)) and richer in Al 58 59 (molar Al/Si ratio > 0.1 (Le Saoût et al., 2011; Myers et al., 2013; Richardson et al., 1994)) than the calcium (alumino)silicate hydrate (C-(A-)S-H) gel formed in hydrated PC (Taylor et al., 2010). The 60 solid phase assemblage in AAS cements contains phases other than C-(N-)A-S-H gel, typically 61 including Mg-Al layered double hydroxide (LDH) phases (Richardson et al., 1994; Wang and 62 63 Scrivener, 1995) and aluminoferrite-mono (AFm) type phases including strätlingite (C_2ASH_8) (Ben Haha et al., 2012; Richardson et al., 1994; Wang and Scrivener, 1995), and calcium 64 65 monocarboaluminate hydrate ($C_4A\underline{c}H_{11}$) in Na₂CO₃ (N<u>c</u>)-activated slag (N<u>c</u>-AS) cement (Shi et al., 66 2006). Katoite (C_3AH_6) (Bonk et al., 2003), zeolites including gismondine and heulandite (Bernal et 67 al., 2015; Bernal et al., 2011), and the third aluminate hydrate (TAH) (Myers et al., 2015a), which is 68 described as a poorly ordered Al(OH)₃ phase (Taylor et al., 2010), may additionally form in AAS 69 cements. Recently, evidence for the formation of alkali aluminosilicate (hydrate) (N-A-S(-H)) gels in 70 AAS cement has been presented (Myers et al., 2015a; Myers et al., 2013); this phase is considered to 71 be similar to the 'geopolymer' gels formed through alkali-activation of low-Ca raw materials (Provis 72 et al., 2005).

73

Thermodynamic modelling can be used to predict the chemistry of hydrated/alkali-activated cements,
assuming equilibrium between the solid reaction products and pore solution (Atkins et al., 1992;
Lothenbach, 2010; Savage et al., 2011), which is critically important in understanding their long-term
behaviour, e.g. in radioactive waste disposal applications (Glasser and Atkins, 1994). This approach

¹ The various alkalis that may be incorporated into C-(N-)A-S-H gel are all represented by Na here because the alkali source in an alkali-activated cement is typically Na-based. Cement chemistry notation is used throughout the text: C = CaO; $S = SiO_2$; $A = Al_2O_3$; $N = Na_2O$; $H = H_2O$; M = MgO; $c = CO_2$; and $s = SO_3$.

78 has been applied to AAS cements in the past (Lothenbach and Gruskovnjak, 2007), however the 79 calcium silicate hydrate (C-S-H) thermodynamic model (Kulik and Kersten, 2001) used in that study does not explicitly define the uptake of Al and Na which is needed to fully describe C-(N-)A-S-H gel. 80 Chemically complete definitions of Al chemistry in the thermodynamic models used to simulate the 81 82 phases formed in AAS-based cements are important in enabling accurate prediction of the chemistry of these cements. The inclusion of alkalis as a key component in thermodynamic models for C-(N-)A-83 S-H gel is also important to enable correct description of the solubility relationships of this phase 84 85 under the high pH conditions (>12) and alkali concentrations (tens to hundreds of mmol/L) relevant to the majority of cementitious materials (Myers et al., 2014). 86

87

88 The CNASH ss thermodynamic model used in the current paper was recently developed (Myers et 89 al., 2014) to formally account for Na and tetrahedral Al incorporated in Ca/Si < 1.3 C-(N-)A-S-H gel. 90 Here, this thermodynamic model is used to simulate the chemistry of AAS cements activated by 91 aqueous solutions of NaOH ((NH)_{0.5}), Na₂SiO₃ (NS), Na₂Si₂O₅ (NS₂) and N_{\underline{c}}. This thermodynamic model can describe a large set of solubility data for the CaO-(Na₂O,Al₂O₃)-SiO₂-H₂O and AAS 92 93 cement systems, and closely matches the published chemical compositions of calcium aluminosilicate 94 hydrate (C-A-S-H) gel, and the volumetric properties of C-(N-)A-S-H gel measured in a sodium 95 silicate-activated slag cement (Myers et al., 2014). The CNASH_ss thermodynamic model is assessed 96 here in terms of the prediction of solid phase assemblages and the Al content of C-(N-)A-S-H gel over 97 the bulk slag chemical composition range which is most relevant to AAS cement-based materials. 98 These simulations are performed using the Gibbs energy minimisation software GEM-Selektor v.3 99 (http://gems.web.psi.ch/) (Kulik et al., 2013; Wagner et al., 2012) and an expanded thermodynamic 100 database for cements, based on the CEMDATA07 database (Babushkin et al., 1985; Hummel et al., 2002; Lothenbach et al., 2008; Lothenbach and Winnefeld, 2006; Matschei et al., 2007; Möschner et 101 al., 2008; Möschner et al., 2009; Schmidt et al., 2008; Thoenen and Kulik, 2003) with the addition of 102 an updated definition of Mg-Al LDH intercalated with OH⁻ (MA-OH-LDH), and including some 103 zeolites and alkali carbonates. The results are discussed in terms of implications for the design of high 104 105 performance AAS-based cements.

106

107 **2. Methods**

108 2.1 Thermodynamic model for C-(N-)A-S-H gel

The CNASH_ss thermodynamic model (Myers et al., 2014) is formulated as an ideal solid solution 109 110 with mixing on six of eight sublattice sites to give three C-S-H gel end-members, one calcium (alkali) silicate hydrate (C-(N-)S-H) gel end-member, two C-A-S-H gel end-members and two C-(N-)A-S-H 111 gel end-members (Table 1). End-member chemical compositions are defined in this model by 112 extension of the 'Substituted General Model' (Richardson and Groves, 1993) for consistency with 113 114 tobermorite-like nanostructures containing no 'interstratified Ca(OH)₂' (Richardson, 2004), which limits the applicability of the CNASH_ss thermodynamic model to Ca/Si ratios <1.3 in the C-(N-)A-115 116 S-H gel. Pentahedral Al (Al[5]) and octahedral Al (Al[6]) are not explicitly considered in the endmember structures described by CNASH ss. 117

118

119 C-(N-)A-S-H gel is formally described in terms of non-cross-linked chain structures in the 120 CNASH ss thermodynamic model, but without precluding representation of cross-linked tobermoritelike chain structures, because these structural types cannot be differentiated by bulk chemical 121 composition alone. Thermodynamic calculations using the CNASH_ss thermodynamic model are 122 therefore also consistent with cross-linked C-(N-)A-S-H gel structural models such as those described 123 by the 'Cross-linked Substituted Tobermorite Model' (CSTM) (Myers et al., 2013). Full details of the 124 development and implementation of the CNASH_ss thermodynamic model are given in (Myers et al., 125 126 2014).

127

128 2.2 Thermodynamic model for MA-OH-LDH

Thermodynamic data for MA-OH-LDH were reformulated into an ideal solid solution thermodynamic
model (MA-OH-LDH_ss) containing three end-members with Mg/Al ratios of 2, 3 and 4 (Table 1) to

131 match the known chemical composition range of this solid solution $(Mg_{(1-x)}Al_x(OH)_{(2+x)} \cdot mH_2O, 0.2 \le x)$

132 ≤ 0.33 (Richardson, 2013)).

133

Recalculation of recently published solubility data for Mg/Al = 2 MA-OH-LDH (M_4AH_{10}) (Gao and Li, 2012) and existing solubility data for this phase (Bennett et al., 1992) was performed in GEM-Selektor v.3 (http://gems.web.psi.ch/) (Kulik et al., 2013; Wagner et al., 2012) using the dissolution reaction eq.(1):

138

139
$$Mg_4Al_2(OH)_{14} \cdot 3H_2O = \frac{K_s}{4Mg^{2+}} + 2AlO_2^- + 6(OH)^- + 7H_2O$$
 (1)

140

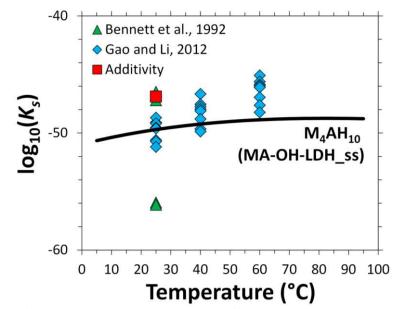
where K_s is the solubility product. Solubility data for this phase were also calculated using the additivity method (Anderson and Crerar, 1993) with brucite (Mg(OH)_{2 (s)}), magnesite (MgCO_{3 (s)}) (Table 1), and hydrotalcite (Mg_{0.74}Al_{0.26}(OH)₂(CO₃)_{0.13} \cdot 0.39H₂O_(s)) (Allada et al., 2005) constituents.

144

145 The recalculation results indicate that the solubility product used previously by Lothenbach and Winnefeld (2006) to describe this phase $(\log_{10}(K_s) = -56.02 \text{ at } 25^{\circ}\text{C} \text{ and } 1 \text{ bar})$, taken from the low 146 147 solubility data reported by Bennett et al. (1992), is not consistent with the solubility data reported by Gao and Li (Gao and Li, 2012) (Figure 1). Here, a solubility product of $\log_{10}(K_s) = -49.70$ at 25°C and 148 149 1 bar is selected for improved consistency with the solubility data reported by Gao and Li (Gao and Li, 2012). The standard heat capacity and entropy of this phase are adapted from the thermodynamic 150 data reported by Allada et al. (Allada et al., 2005) for Mg_{0.74}Al_{0.26}(OH)₂(CO₃)_{0.13}.0.39H₂O using the 151 additivity method with Mg(OH)_{2 (s)} and MgCO_{3 (s)} constituents, i.e. the standard heat capacity for 152 153 M_4AH_{10} is calculated via eq.(2):

154

155
$$Cp^{\circ}_{M_{4}AH_{10}} = 2\left(\frac{1}{0.26}Cp^{\circ}_{Mg_{0.74}AI_{0.26}(OH)_{2}(CO_{3})_{0.13}\cdot 0.39H_{2}O} - 0.5Cp^{\circ}_{MgCO_{3}} - 0.346Cp^{\circ}_{Mg(OH)_{2}}\right)$$
(2)



157

Figure 1. Comparison between the recalculated solubility data (Bennett et al., 1992; Gao and Li, 2012), results using the additivity method, and calculated solubility of the M_4AH_{10} end-member of the MA-OH-LDH_ss thermodynamic model used in this work (thick black line) (P = 1 bar). The green triangles at $log_{10}(K_s) = -56.02$ (25°C and 1 bar), represents the solubility product used previously to describe this phase in the cement chemistry literature.

163

164 Standard entropies and heat capacities for Mg/Al = 3 MA-OH-LDH (M_6AH_{12}) and Mg/Al = 4 MA-OH-LDH (M₈AH₁₄) were determined in the same manner (using solid constituents and a reaction 165 analogous to eq.(2)), using the thermodynamic data reported by Allada et al. (Allada et al., 2005). A 166 difference of -22.32 \log_{10} units was specified between the solubility products of M₄AH₁₀ ($\log_{10}(K_s) = -$ 167 168 49.70) and M_6AH_{12} (log₁₀(K_s) = -72.02), and between those of M_6AH_{12} and M_8AH_{14} (log₁₀(K_s) = -94.34) at 25°C and 1 bar, which is the difference between the solubility products of these phases when 169 determined using the additivity method described here. A similar difference is found between reported 170 thermodynamic data for MA-c-LDH (Mg₄Al₂(OH)₁₂(CO₃).4H₂O, $\log_{10}(K_8) = -44.19$ (Rozov et al., 171 172 2011) and Mg₆Al₂(OH)₁₆(CO₃).5H₂O, $\log_{10}(K_s) = -66.58$ (Rozov, 2010)), which suggests that the 173 additivity approach is appropriate for these structurally-similar Mg-Al LDH phases. The three MA-OH-LDH phases M4AH10, M6AH12 and M8AH14 were specified as end-members of the ideal solid 174 175 solution 'MA-OH-LDH_ss'. This is justified because it has been shown that the assumption of 176 mechanical (ideal) mixing is appropriate for modelling the total solubility of the structurally-similar hydrotalcite-pyroaurite solid solution series (Rozov et al., 2011). This MA-OH-LDH solid solution 177 178 model is used in the thermodynamic modelling performed in this work.

179

180 **2.3 Occurrence of Mg, Fe and S-bearing phases**

Thermodynamic modelling of AAS cements requires consideration of additional constituent elements 181 outside the CaO-Na₂O-Al₂O₃-SiO₂-H₂O system, most notably Mg, Fe and S, as well as carbonates. 182 183 While the precipitation of Mg in AAS cement is generally well explained by its incorporation into 184 Mg-Al LDH phases (Ben Haha et al., 2011b; Richardson et al., 1994; Wang and Scrivener, 1995), there is less consensus regarding the precipitation of Fe and S. Fe was excluded from this work, 185 consistent with the passivated state of this element in GBFS (Bernal et al., 2014a), and S released by 186 the slag was represented as S^{2-} with its oxidation limited by using a simulated $N_{2(g)}$ atmosphere in the 187 thermodynamic modelling calculations. 188

189

190 **2.4 Other solid phases**

191 Thermodynamic data for cement-related solid phases other than C-(N-)A-S-H gel and MA-OH-LDH 192 were taken from the PSI/Nagra 12/07 thermodynamic database (Thoenen et al., 2013) and the 193 CEMDATA07 thermodynamic database, which was updated to include recently published data for 194 Al(OH)₃ and hydrogarnet phases (Dilnesa et al., 2014; Lothenbach et al., 2012) (Table 1).

195

| Phases ^a | V° (cm ³ mol ⁻¹) | ΔH_{f}° (kJ mol ⁻¹) | $\Delta G_{f}^{\circ} (kJ mol^{-1})$ | S° (J mol ⁻¹ K ⁻ 1) | Cp° (J mol ⁻¹ K ⁻ ¹) | Reference |
|---|--|--|--------------------------------------|---|--|---|
| ¹ / ₂ AH ₃ (microcrystalline) | 32.0 | -1265 | -1148 | 140 | 93.1 | (Lothenbach e al., 2012) (Robie and |
| Portlandite, CH | 33.1 | -985 | -897 | 83.4 | 87.5 | Hemingway, 1995) |
| SiO ₂ (amorphous) | 29.0 | -903 | -849 | 41.3 | 44.5 | (Helgeson et a 1978; Kulik ar Kersten, 2001 |
| C ₂ AH ₈ | 90.1 | -5278 | -4696 | 450 | 521 | (Lothenbach e al., 2012) |
| Katoite, (C ₃ AH ₆) | 150 | -5537 | -5008 | 422 | 446 | (Lothenbach al., 2012) |
| C_4AH_{19} | 382 | -1002 | -8750 | 1120 | 1382 | (Lothenbach) al., 2012) (Lothenbach) |
| CAH_{10} | 194 | -5288 | -4623 | 610 | 668 | al., 2012) (Matschei et a |
| Strätlingite, C ₂ ASH ₈ | 216 | -6360 | -5705 | 546 | 603 | 2007) |
| Calcium monocarboaluminate hydrate, $C_4A\underline{c}H_{11}$ | 262 | -8250 | -7337 | 657 | 881 | (Matschei et a 2007) |
| Calcium hemicarboaluminate hydrate, $C_4A\underline{c}_{0.5}H_{12}$ | 285 | -8270 | -7336 | 713 | 906 | (Matschei et a 2007) |
| Calcium tricarboaluminate hydrate, $C_6A\underline{c}_3H_{32}$ | 650 | -16792 | -14566 | 1858 | 2121 | (Matschei et a 2007) (Lothenbach |
| Ettringite, $C_6A\underline{s}_3H_{32}$ | 707 | -17535 | -15206 | 1900 | 2174 | al., 2008) (Hummel et a |
| Gypsum, C <u>s</u> H ₂ | 74.7 | -2023 | -1798 | 194 | 186 | 2002; Thoene et al., 2013) (Hummel et a |
| Anhydrite, C <u>s</u> | 45.9 | -1435 | -1322 | 107 | 99.6 | 2002; Thoene et al., 2013) |
| Lime, C | 16.8 | -635 | -604 | 39.7 | 42.8 | (Helgeson et a 1978) (Helgeson et a |
| Brucite, MH | 24.6 | -923 | -832 | 63.1 | 77.3 | 1978; Humm et al., 2002; Thoenen et al 2013) |
| MA- <u>c</u> -LDH, M ₄ A <u>c</u> H ₉ | 220 | -7374 | -6580 | 551 | 647 | (Lothenbach al., 2008) |
| C-(N-)A-S-H gel ideal | solid solutio | n end-mem | bers, 'CNAS | H_ss' (Myer | s et al., 2014 | 4) |
| 5CA, C _{1.25} A _{0.125} S ₁ H _{1.625} | 57.3 | -2491 | -2293 | 163 | 177 | (Myers et al. 2014) |
| INFCA, C ₁ A _{0.15625} S _{1.1875} H _{1.65625} | 59.3 | -2551 | -2343 | 154 | 181 | (Myers et al. 2014) |
| 5CNA, $C_{1.25}N_{0.25}A_{0.125}S_1H_{1.375}$ | 64.5 | -2569 | -2382 | 195 | 176 | (Myers et al. 2014) (Myers et al. |
| INFCNA, C ₁ N _{0.34375} A _{0.15625} S _{1.1875} H _{1.3125} | 69.3 | -2667 | -2474 | 198 | 180 | (Myers et al. 2014) (Myers et al. |
| INFCN, C ₁ N _{0.3125} S _{1.5} H _{1.1875} T2C*, C _{1.5} S ₁ H _{2.5} ^b | 71.1 | -2642 | -2452 2465 | 186 | 184 | 2014) (Myers et al. |
| | 80.6 | -2721 | -2465 | 167 | 237 | 2014) |

| | | | | | | 2014) |
|---|---------------|--------------|----------------|----------------|-----------|--|
| TobH*, $C_1S_{1.5}H_{2.5}$ b | 85.0 | -2831 | -2560 | 153 | 231 | (Myers et al., 2014) |
| Calcium monosulfoaluminate- | hydroxoalun | ninate hydra | te non-ideal s | solid solution | (Matschei | et al., 2007) |
| $\label{eq:calcium monosulfoaluminate hydrate,} C_4 A\underline{s} H_{12}$ | 309 | -8750 | -7779 | 821 | 942 | (Matschei et al., 2007) |
| C_4AH_{13} | 274 | -8300 | -7324 | 700 | 930 | (Lothenbach et al., 2012) |
| MA-OH-LD | H ideal solid | solution end | -members, 'N | MA-OH-LDI | H_ss' | |
| | | | | | | (Allada et al., |
| M_4AH_{10} | 219 | -7160 | -6358 | 549 | 648 | 2005; Richardson, 2013) |
| M_6AH_{12} | 305 | -9007 | -8023 | 675 | 803 | This study ^c |
| M_8AH_{14} | 392 | -10853 | -9687 | 801 | 958 | This study ^c |
| | | Carbonat | es | | | |
| Aragonite, C <u>c</u> | 34.2 | -1207 | -1128 | 90.2 | 81.3 | (Hummel et al., 2002; Thoenen et al., 2013) (Hummel et al., |
| Calcite, C <u>c</u> | 36.9 | -1207 | -1129 | 92.7 | 81.9 | 2002; Thoenen et al., 2013) |
| Dolomite (disordered), CM _{C2} | 64.4 | -2317 | -2157 | 167 | 158 | (Hummel et al., 2002; Thoenen et al., 2013) |
| Natron, N <u>c</u> H ₁₀ | 197 | -4079 | -3428 | 563 | 550 | (Königsberger et al., 1999; Taga, 1969) |
| Gaylussite, NC <u>c</u> 2H5 | 149 | -3834 | -3372 | 387 | _ d | (Dickens and Brown, 1969; Königsberger et al., 1999) |
| Pirssonite, NC <u>c</u> ₂ H ₂ | 104 | -2956 | -2658 | 239 | 329 | (Dickens and Brown, 1969; Königsberger et al., 1999) |
| Magnesite, M <u>c</u> | 28.0 | -1113 | -1029 | 65.7 | 75.8 | (Hummel et al., 2002; Thoenen et al., 2013) (Graf and |
| Huntite, CM ₃ <u>c</u> ₄ | 123 | -4533 | -4206 | 300 | 310 | Bradley, 1962; Hemingway and Robie, 1972; Königsberger et al., 1999) |
| Artinite, M ₂ <u>c</u> H ₄ | 96.2 | -2921 | -2568 | 233 | 248 | (de Wolff, 1952; Hemingway and Robie, 1972; Königsberger et al., 1999) |
| Lansfordite, McH ₅ | 103 | -2574 | -2198 | 250 | 386 | (Hill et al., 1982; Königsberger et al., 1999) |
| | | Zeolites | | | | |
| Na-analcime, Na _{0.32} .[Al _{0.32} Si _{0.68} O ₂].0.333H ₂ O | 32.5 ° | -1099 | -1026 | 75.6 | 70.5 | (Johnson et al., 1982) |
| | | | | | | |

| Natrolite, Na _{0.4} .[Al _{0.4} Si _{0.6} O ₂].0.4H ₂ O | 33.8 ° | -1144 | -1063 | 71.9 | 60.4 | (Johnson et al., 1983) |
|---|-------------------|-------|-------|-------------------|-------------------|---------------------------|
| Ca-heulandite, Ca _{0.111} .[Al _{0.222} Si _{0.778} O ₂].0.667H ₂ O | 35.2 ° | -1179 | -1090 | 87.1 | 82.9 | (Kiseleva et al., 2001) |
| (Ca,Na)-heulandite, Ca _{0.111} Na _{0.028} .[Al _{0.25} Si _{0.75} O ₂].0.667H ₂ O | 35.2 ° | -1185 | -1094 | 84.0 | 82.9 | (Kiseleva et al., 2001) |
| Basic sodalite, Na _{0.65} (OH) _{0.15} .[Al _{0.5} Si _{0.5} O ₂].0.27H ₂ O | 35.0 ^e | -1190 | -1106 | 67.8 ^f | $66.7 \ ^{\rm f}$ | (Moloy et al., 2006) |

198^a Cement chemistry notation is used: C = CaO; $S = SiO_2$; $A = Al_2O_3$; $H = H_2O$; $N = Na_2O$; M = MgO;199 $\underline{c} = CO_2$; $\underline{s} = SO_3$.200^b The asterisks for the T2C*, T5C* and TobH* end-members indicate that these components have201slightly modified thermodynamic properties but the same chemical composition relative to the T2C,

T5C and TobH end-members of the downscaled CSH3T thermodynamic model (Kulik, 2011).

^c Thermodynamic properties based on the thermochemical data in (Allada et al., 2005) and solubility
 data in (Bennett et al., 1992; Gao and Li, 2012), section 2.2, with molar volumes calculated from
 (Richardson, 2013).

206 ^d Not available

^e Molar volumes calculated from framework densities, lattice types and lattice cell parameters for each
 zeolite framework type (Baerlocher et al., 2007).

^f Standard entropy and heat capacity estimated using the additivity method (Anderson and Crerar, 1993) based on H₂O (1) (Table 2), gibbsite (Helgeson et al., 1978; Hummel et al., 2002), NaOH (s)

211 (Robie and Hemingway, 1995) and amorphous SiO₂ (Table 1).

212

Thermodynamic data for some zeolites and alkali carbonate minerals were used to provide a preliminary assessment of the stability of these phases in AAS cements (Table 1) and should be treated as provisional only, because the thermodynamic data were not recompiled for full internal consistency with the Nagra-PSI and CEMDATA07 thermodynamic databases. Reliable thermodynamic data for other Na-carbonates which can form in AAS cements (i.e. natrite, thermonatrite, nahcolite and trona) were not available (Königsberger et al., 1999; Monnin and Schott, 1984), and so were not included in the simulations.

220

221 The formation of siliceous hydrogarnet was suppressed in the simulations because this phase does not

tend to form at ambient temperature and pressure, possibly for kinetic reasons (Lothenbach et al.,

223 2008). No additional restrictions related to the formation of any other solid phases shown in Table 1

were specified.

2.5 Approach 226

Thermodynamic modelling was performed using the Gibbs energy minimisation software GEM-227 Selektor v.3 (http://gems.web.psi.ch/) (Kulik et al., 2013; Wagner et al., 2012), with thermodynamic 228 data for the solid phases shown in Table 1 and thermodynamic data for aqueous species/complexes 229 and gases shown in Tables 2 and 3, respectively. The Truesdell-Jones form of the extended Debye-230 Hückel equation (eq.(3)) (Helgeson et al., 1981) and the ideal gas equation of state were used for the 231 aqueous and gaseous phase models, respectively, with the average ion size (\dot{a}, \dot{A}) and the parameter 232 for common short-range interactions of charged species (b_v, kg mol⁻¹) specified to represent NaOH-233 dominated solutions (3.31 Å and 0.098 kg mol⁻¹, respectively (Helgeson et al., 1981)). 234

235

236
$$\log_{10} \gamma_{j} = \frac{-A_{\gamma} z_{j}^{2} \sqrt{I}}{1 + \dot{a} B_{\gamma} \sqrt{I}} + b_{\gamma} I + \log_{10} \frac{X_{jw}}{X_{w}}$$
(3)

237

The parameters γ_j and z_j in eq.(3) are the activity coefficient and charge of the j^{th} aqueous species, 238 respectively, A_y (kg^{0.5} mol^{-0.5}) and B_y (kg^{0.5} mol^{-0.5} cm⁻¹) are T,P-dependent electrostatic parameters, I 239 is the ionic strength of the aqueous electrolyte phase (mol kg⁻¹), x_{jw} (mol) is the molar quantity of 240 water and X_w (mol) is the total molar amount of the aqueous phase. The activity of water is calculated 241 from the osmotic coefficient (Helgeson et al., 1981) and unity activity coefficients for neutral 242 243 dissolved species are used.

244

Table 2. Thermodynamic properties of the aqueous species used in the thermodynamic modelling 245 simulations

|) | | | simulations. | | | | |
|---|--|--|--|--|--|---|-------------------------|
| | Species/complex ^a | V° (cm ³ mol ⁻¹) | ΔH _f ° (kJ mol ⁻¹) | ΔG _f ° (kJ mol ⁻¹) | S° (J mol ⁻ ¹ K ⁻¹) | Cp° (J mol ⁻¹ K ⁻¹) | Reference |
| _ | Al ³⁺ | -45.2 | -530.6 | -483.7 | -325.1 | -128.7 | (Shock et al., 1997) |
| | $AlO^+ (+ H_2O = Al(OH)_2^+)$ | 0.3 | -713.6 | -660.4 | -113 | -125.1 | (Shock et al., 1997) |
| | $AlO_{2}^{-} (+ 2H_{2}O = Al(OH)_{4}^{-})$ | 9.5 | -925.6 | -827.5 | -30.2 | -49 | (Shock et al., 1997) |
| | $A1OOH^{\circ} (+ 2H_2O = A1(OH)_3^{\circ})$ | 13 | -947.1 | -864.3 | 20.9 | -209.2 | (Shock et al., 1997) |
| | AlOH ²⁺ | -2.7 | -767.3 | -692.6 | -184.9 | 56 | (Shock et al., |

| | | | | | | 1007) |
|---|-------|--------|--------|--------|--------|---|
| $AlHSiO_{3}^{2+} (+ H_{2}O = AlSiO(OH)_{3}^{2+})$ | -40.7 | -1718 | -1541 | -304.2 | -215.9 | 1997) (Matschei et al., 2007) |
| $AlSiO_4^- (+ 3H_2O = AlSiO(OH)_6^-)$ | 25.5 | -1834 | -1681 | 11.1 | -4.6 | (Matschei et al., 2007) |
| AlSO_4^+ | -6.0 | -1423 | -1250 | -172.4 | -204.0 | (Matschei et al., 2007) |
| $Al(SO_4)_2^-$ | 31.1 | -2338 | -2006 | -135.5 | -268.4 | (Matschei et al., 2007) |
| Ca ²⁺ | -18.4 | -543.1 | -552.8 | -56.5 | -30.9 | (Shock et al., 1997) |
| CaOH ⁺ | 5.8 | -751.6 | -717 | 28 | 6 | (Shock et al., 1997) |
| $CaHSiO_{3}^{+} (+ H_2O = CaSiO(OH)_{3}^{+})$ | -6.7 | -1687 | -1574 | -8.3 | 137.8 | (Sverjensky et al., 1997) |
| $\begin{array}{l} \text{CaSiO}_{3^{\text{o}}} (+ \text{H}_2\text{O} = \\ \text{CaSiO}_2(\text{OH})_{2^{\text{o}}}) \end{array}$ | 15.7 | -1668 | -1518 | -136.7 | 88.9 | (Matschei et al., 2007) |
| CaSO ₄ ° | 4.7 | -1448 | -1310 | 20.9 | -104.6 | (Sverjensky et al., 1997) |
| CaCO ₃ ° | -1.6 | -1202 | -1099 | 10.5 | -123.9 | (Sverjensky et al., 1997) |
| $CaHCO_{3^{+}}$ | 13.3 | -1232 | -1146 | 66.9 | 233.7 | (Hummel et al., 2002; Thoenen |
| \mathbf{K}^+ | 9.0 | -252.1 | -282.5 | 101 | 8.4 | et al., 2013) (Shock et al., 1997) |
| KOH° | 15 | -474.1 | -437.1 | 108.4 | -85 | (Shock et al., 1997) |
| KSO_4^- | 27.5 | -1159 | -1032 | 146.4 | -45.1 | (Sverjensky et al., 1997) |
| Na^+ | -1.2 | -240.3 | -261.9 | 58.4 | 38.1 | (Shock et al., 1997) |
| NaOH ^o | 3.5 | -470.1 | -418.1 | 44.8 | -13.4 | (Shock et al., 1997) |
| $NaSO_4^-$ | 18.6 | -1147 | -1010 | 101.8 | -30.1 | (Matschei et al., 2007) |
| NaCO ₃ - | -0.4 | -938.6 | -797.1 | -44.3 | -51.3 | (Hummel et al., 2002; Thoenen et al., 2013) |
| NaHCO ₃ ° | 32.3 | -929.5 | -847.4 | 154.7 | 200.3 | (Hummel et al., 2002; Thoenen et al., 2013) |
| $HSiO_{3}^{-}(+H_{2}O = SiO(OH)_{3}^{-})$ | 4.5 | -1145 | -1014 | 20.9 | -87.2 | (Sverjensky et al., 1997) (Kulik and |
| $SiO_{2^{o}} (+ 2H_{2}O = Si(OH)_{4^{o}})$ | 16.1 | -887.9 | -833.4 | 41.3 | 44.5 | Kersten, 2001; Shock et al., 1989) |
| SiO_3^{2-} (+ H ₂ O = SiO ₂ (OH) ₂ ²⁻) | 34.1 | -1099 | -938.5 | -80.2 | 119.8 | (Matschei et al., 2007) |
| $S_2O_3^{2-}$ | 27.6 | -649.9 | -520.0 | 66.9 | -238.5 | (Shock et al., 1997) |
| HSO ₃ - | 33.0 | -627.7 | -529.1 | 139.7 | -5.4 | (Shock et al., 1997) |
| SO ₃ ²⁻ | -4.1 | -636.9 | -487.9 | -29.3 | -281.0 | (Shock et al., |

| | | | | | | 1997) (Shaaly et al |
|--|-------|---------|--------|--------|--------|---|
| HSO_4^- | 34.8 | -889.2 | -755.8 | 125.5 | 22.7 | (Shock et al., 1997) |
| SO4 ²⁻ | 12.9 | -909.7 | -744.5 | 18.8 | -266.1 | (Shock et al., 1997) |
| H_2S^o | 35.0 | -39.0 | -27.9 | 125.5 | 179.2 | (Shock et al., 1997) |
| HS | 20.2 | -16.2 | 12.0 | 68.2 | -93.9 | (Shock et al., 1997) |
| S ²⁻ | 20.2 | 92.2 | 120.4 | 68.2 | -93.9 | (Shock et al., 1997) |
| Mg^{2+} | -22.0 | -465.9 | -454.0 | -138.1 | -21.7 | (Shock et al., 1997) |
| MgOH ⁺ | 1.6 | -690.0 | -625.9 | -79.9 | 129.2 | (Shock et al., 1997) |
| $MgHSiO_{3}^{+} (+ H_{2}O = MgSiO(OH)_{3}^{+})$ | -10.9 | -1614 | -1477 | -99.5 | 158.6 | (Shock et al., 1997) |
| ${ m MgSO_4}^{ m o}$ | 1.8 | -1369 | -1212 | -50.9 | -90.3 | (Hummel et al., 2002; Shock et al., 1997; Thoenen et al., 2013) |
| $MgSiO_{3}^{\circ} (+ H_{2}O = MgSiO_{2}(OH)_{2}^{\circ})$ | 12.1 | -1597 | -1425 | -218.3 | 98.2 | (Hummel et al., 2002; Thoenen et al., 2013) (Hummel et al., |
| MgCO ₃ ° | -16.7 | -1132 | -999.0 | -100.4 | -116.5 | 2002; Sverjensky et al., 1997; Thoenen et al., |
| MgHCO ₃ + | 9.3 | -1154.0 | -1047 | -12.6 | 254.4 | 2013) (Hummel et al., 2002; Thoenen et al., 2013) (Hummel et al., |
| $\rm CO_2^o$ | 32.8 | -413.8 | -386.0 | 117.6 | 243.1 | 2002; Shock et al., 1989; Thoenen et al., 2013) |
| CO ₃ ²⁻ | -6.1 | -675.3 | -528.0 | -50.0 | -289.3 | (Shock et al., 1997) |
| HCO ₃ - | 24.2 | -690.0 | -586.9 | 98.5 | -34.8 | (Shock et al., 1997) |
| $ m CH_4^o$ | 37.4 | -87.8 | -34.4 | 87.8 | 277.3 | (Hummel et al., 2002; Shock and Helgeson, 1990; Thoenen et al., 2013) |
| OH- | -4.7 | -230 | -157.3 | -10.7 | -136.3 | (Shock et al., 1997) |
| H^{+} | 0 | 0 | 0 | 0 | 0 | (Shock et al., 1997) |
| H_2O^o | 18.1 | -285.9 | -237.2 | 69.9 | 75.4 | (Johnson et al., 1992) |
| ${\rm H_2}^{\rm o}$ | 25.3 | -4.0 | 17.7 | 57.7 | 166.9 | (Hummel et al., |
| | | | | | | |

| | | | | | | 2002; Shock et al., 1989; Thoenen et al., 2013) |
|--------------|------|-------|------|------|-------|--|
| $N_2^{ m o}$ | 33.4 | -10.4 | 18.2 | 95.8 | 234.2 | (Shock et al., 1989) |
| O_2^{o} | 30.5 | -12.2 | 16.4 | 109 | 234.1 | (Shock et al., 1989) |

^a The hydration reactions shown in parentheses indicate hydrated species/complexes represented by

the simulated aqueous species/complexes.

249

250 Table 3. Thermodynamic properties of the gases used in the thermodynamic modelling simulations.

| Gases | V° (cm ³ mol ⁻¹) | ΔH _f ° (kJ mol ⁻ ¹) | $\Delta G_{f}^{\circ} (kJ mol^{-1})$ | S° (J mol ⁻¹ K ⁻¹) | Cp° (J mol ⁻¹ K ⁻¹) | Reference |
|--------|--|---|--------------------------------------|--|---|-----------------------|
| N_2 | 24790 | 0 | 0 | 191.6 | 29.1 | (Wagman et al., 1982) |
| O_2 | 24790 | 0 | 0 | 205.1 | 29.3 | (Wagman et al., 1982) |
| H_2 | 24790 | 0 | 0 | 130.7 | 28.8 | (Wagman et al., 1982) |
| CO_2 | 24790 | -393.5 | -394.4 | 213.7 | 37.1 | (Wagman et al., 1982) |
| CH_4 | 24790 | -74.8 | -50.7 | 186.2 | 35.7 | (Wagman et al., 1982) |
| H_2S | 24790 | -20.6 | -33.8 | 205.8 | 34.2 | (Wagman et al., 1982) |

251

252

253 Chemical equilibrium between the solid, aqueous and gaseous phases was assumed, and the simulated 254 slag was specified to dissolve congruently at each particular bulk slag chemical composition. The 255 assumption of congruent dissolution is valid for calcium aluminosilicate glasses of similar bulk 256 chemical compositions to GBFS in highly under-saturated conditions at pH = 13 (Snellings, 2013). 257 This condition is likely to be approximated in AAS cements when the solution pH is sufficiently high 258 (Bernal et al., 2015), although it is clear that this assumption will need to be revisited in some 259 systems, particularly for AAS cements cured for long times or synthesised with less basic activators 260 such as Nc (Bernal et al., 2015).

261

Simulations of AAS cements were performed using 100 g slag, additions of H₂O, NaOH or Na₂O, SiO₂ and Na₂CO₃ to achieve fixed water to binder (w/b, where binder = slag + anhydrous activator

- component) ratios of 0.4 and activator concentrations of 4 g Na₂O equivalent/100 g slag (the
- activators used are NaOH, Na₂SiO₃, Na₂Si₂O₅ and Na₂CO₃), a nitrogen atmosphere (10 mol N_{2 (g)} per
- 266 100 g slag), and temperature/pressure conditions of 298.15 K and 1 bar. This simulation setup directly
- represents the AAS cements studied in (Bernal et al., 2015; Bernal et al., 2014b; Myers et al., 2015a;
- 268 Myers et al., 2013), and is also similar to the AAS cement formulations reported in (Ben Haha et al.,
- 269 2011b, 2012; Le Saoût et al., 2011) (which had ~3 mass% Na₂O equivalent and w/b = 0.4). With the
- 270 exception of the phase diagram simulations (section 3.4), the simulated slag compositions are based
- on the GBFS composition shown in Table 4.
- 272
- Table 4. Bulk chemical composition of the GBFS (from (Myers et al., 2015a)) used to specify the
 chemical compositions of the simulated slag in the thermodynamic modelling simulations.

| Component | Chemical composition (mass%) |
|------------------------------|------------------------------|
| SiO ₂ | 33.8 |
| CaO | 42.6 |
| MgO | 5.3 |
| Al_2O_3 | 13.7 |
| Na ₂ O | 0.1 |
| K_2O | 0.4 |
| SO ₃ ^a | 0.8 |
| Other | 1.5 |
| LOI ^b | 1.8 |
| Total | 100 |

^a S is represented in oxide form in standard XRF analysis, but S is treated as S²⁻ here (see section 2.2).
 ^b LOI is loss on ignition at 1000°C.

277

278 In section 3.1, the utility of the thermodynamic database (Tables 1-3) is assessed by using the slag composition given in Table 4 in terms of SiO₂, CaO, MgO, Al₂O₃, Na₂O, K₂O, and H₂S 279 (corresponding to the "SO₃" content of the slag in Table 4) only, except for a variable oxide 280 component (Al₂O₃, MgO or CaO), which was specified according to the simulation conducted. A 281 282 simulated slag reaction extent of 60% was employed, which represents a typical degree of reaction quantified for GBFS in sodium silicate-activated slag cements (~48% at 180 days in (Ben Haha et al., 283 2011a), 54 ±3% at 100 days in (Le Saoût et al., 2011), 58-61% at 180 days in (Bernal et al., 2014b) 284 and >70% after 1 month in (Myers et al., 2015a)). A density of 2.8 g/cm³ was selected for the 285 286 unreacted slag component (Bernal et al., 2015).

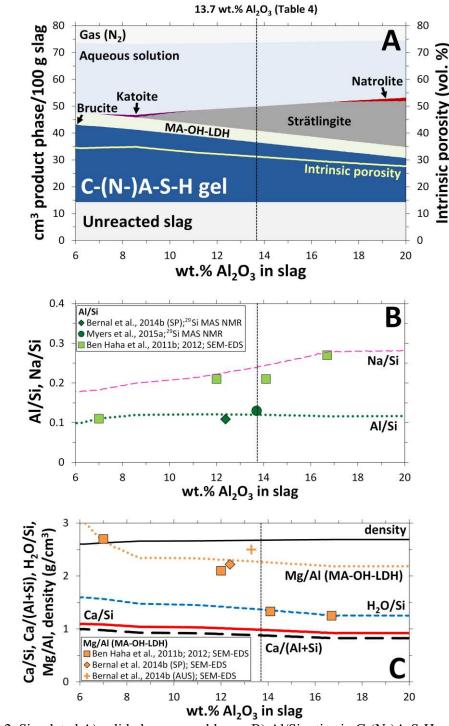
Specific details pertaining to the descriptions of the slags simulated here, for each other aspect of thestudy, are shown near the beginning of each of sections 3.2-3.4.

290

3. Results and discussion

3.1 Utility of the CNASH_ss and MA-OH-LDH_ss thermodynamic models

Figure 2A shows that the calculated phase assemblage in NS-activated slag (NS-AS) cement changes 293 as a function of Al₂O₃ content in the slag. The phase assemblage is dominated by C-(N-)A-S-H gel, in 294 addition to MA-OH-LDH at all Al₂O₃ contents, and strätlingite, which also forms between 9 and 20 295 296 mass% Al₂O₃. Mg-Al LDH phases are commonly identified in sodium silicate-activated slag cements derived from slags with \geq 5 mass% MgO (Bernal et al., 2014b), in good agreement with these results; 297 298 LDH formation is reassessed in detail below. The simulated volume of the MA-OH-LDH phase does 299 not change greatly here because its formation is limited by the amount of Mg supplied by the slag, 300 which is constant at a fixed slag reaction extent. Small amounts of katoite are predicted for slags with 301 7-11 mass% Al₂O₃, which is relatively consistent with the observation of small amounts of this phase 302 in sodium silicate-activated slag cements produced from slags with ~ 13 mass% Al₂O₃ (Bernal et al., 2014b; Schneider et al., 2001). Natrolite is predicted between 17 and 20 mass% slag Al₂O₃ content 303 and very small quantities of brucite are predicted for slags with <7 mass% Al₂O₃. 304



306

308 Figure 2. Simulated A) solid phase assemblages, B) Al/Si ratios in C-(N-)A-S-H gel, and C) Mg/Al 309 ratios in MA-OH-LDH in NS-AS cements with bulk slag chemical compositions rescaled from Table 310 4 except for the Al₂O₃ content, which is varied here. Changes in B) Na/Si, C) H₂O/Si, Ca/Si and 311 Ca/(Al+Si) ratios in C-(N-)A-S-H gel, and C) C-(N-)A-S-H gel density (g/cm³) are shown for visual 312 313 reference. The symbols in B) and C) are experimental results for sodium silicate-activated slag cements cured for 180 days and derived from slag precursors with similar MgO and equivalent or 314 slightly lower CaO content (5.2 < mass% MgO < 7.7, 35 < mass% CaO \leq 42.6) to the slag 315 represented by Table 4. 316 317

318 The Mg/Al ratio of the simulated MA-OH-LDH phase is between 2 and 3 over the full range of 319 simulated slag Al₂O₃ compositions (Figure 2C), in excellent agreement with experimentally determined Mg/Al ratios for this phase by scanning electron microscopy (SEM) with energy-320 dispersive X-ray spectroscopy (EDS) analysis in sodium silicate-activated slag cements for slags 321 containing $7 \le \text{mass}\%$ Al₂O₃ ≤ 13.3 (Ben Haha et al., 2012; Bernal et al., 2014b). However, the 322 experimental SEM-EDS data suggest a systematic reduction in the Mg/Al ratio of this phase to below 323 2 as a function of increasing slag Al_2O_3 content (Ben Haha et al., 2012; Bernal et al., 2014b), that was 324 not captured by the modelling performed here, as the MA-OH-LDH_ss thermodynamic model only 325 describes solid solutions in the range $2 \le Mg/Al \le 4$. Regions with Mg/Al ratios < 2 identified in 326 transmission electron microscopy (TEM)-EDS analysis of hydrated PC/GBFS cements (Taylor et al., 327 2010) are discussed in terms of intimate mixtures of Mg-Al LDH and Al(OH)₃-type phases because 328 329 the chemical composition of Mg-Al LDH is theoretically limited to the range modelled here, 2 < 1Mg/Al \leq 4 (Richardson, 2013). The experimental Mg/Al ratios < 2 shown in Figure 2C can thus be 330 described similarly, which would explain the difference between the modelled and experimentally 331 332 measured data. This analysis suggests a need for additional thermodynamic data describing Al-rich and Mg-poor solid phases that are not currently included in the thermodynamic database (e.g. TAH 333 334 (Andersen et al., 2006)) rather than a deficiency in the MA-OH-LDH_ss thermodynamic model as 335 such.

The amount of C-(N-)A-S-H gel formed in the simulated NS-AS cements decreases with increasing 337 338 Al₂O₃ content of the slag (Figure 2A) at the expense of strätlingite precipitation. An Al/Si ratio ≈ 0.12 is calculated for C-(N-)A-S-H gel in NS-AS cements derived from slags with >8 mass% Al₂O₃ 339 (Figure 2B), which corresponds closely to the Al/Si ratios determined for this phase by analysis of 340 deconvoluted ²⁹Si magic angle spinning nuclear magnetic resonance (MAS NMR) spectra for these 341 materials at 180 days of age (Bernal et al., 2014b; Myers et al., 2015a) using the CSTM (Myers et al., 342 2013). The CSTM is a structural model that represents C-(N-)A-S-H gel in terms of mixed cross-343 linked/non-cross-linked components that enables chemical compositions and structural parameters to 344 345 be determined from deconvolution analysis of ²⁹Si MAS NMR spectra for materials containing this

phase. However, the experimental Al/Si ratios determined from ²⁹Si MAS NMR shown here exclude 346 347 the potential uptake of Al[5] (Andersen et al., 2006) and Al[6] (Sun et al., 2006) in C-(N-)A-S-H gel, so are expected to be slightly lower than the 'true' Al/Si ratio in this phase. This discrepancy is 348 discussed further in section 3.2. However, the much higher Al/Si ratios shown by the other SEM-EDS 349 350 data, with Mg/Al < 2, could indicate mixtures of C-(N-)A-S-H gel with Mg-free and Al-containing phases in the interaction volumes analysed by SEM-EDS. This description is similar to the analysis 351 above for Mg-Al LDH, so the thermodynamic modelling results are not necessarily inconsistent with 352 these experimental SEM-EDS data. 353

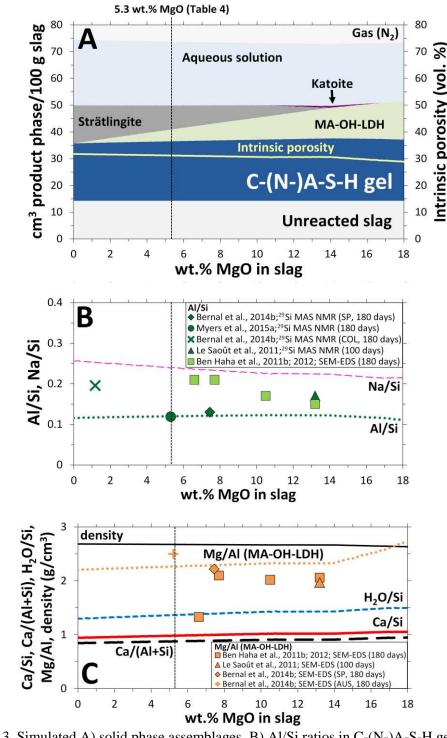
354

The total binder volume (solid + aqueous phases) is calculated to be approximately constant over the 355 full range of slag Al₂O₃ compositions studied (Figure 2A), suggesting that the bulk Al content of the 356 357 slag in NS-AS cements should not greatly affect the chemical shrinkage properties of these materials. The results indicate a 20% change in intrinsic porosity (defined as the ratio of aqueous phase volume 358 to total binder volume, where water chemically bound in, or adsorbed to, the solid phases described in 359 360 Table 1 is considered to be a component of the solid) for slag compositions between ~8 and 20 mass% 361 Al₂O₃. This interpretation corresponds to the simulated C-(N-)A-S-H gel density of 2.5-2.7 g/cm³ and 362 H₂O/Si ratios between 1.3 and 1.7 (in agreement with C-(N-)A-S-H gel at RH \approx 25% (Muller et al., 2013)), as shown in Figure 2C. Therefore, this phase is conceptually equivalent to C-(N-)A-S-H gel 363 with interlayer and some adsorbed water but no 'gel' or 'free' water (Jennings, 2008). However, the 364 reduced intrinsic porosity found here at higher bulk slag Al_2O_3 content does not explain the weak 365 366 dependency of sodium silicate-activated slag cement compressive strengths on bulk slag Al₂O₃ content (Ben Haha et al., 2012), because an increase in compressive strength would be expected at 367 lower porosity. This discrepancy is attributed to the higher amount of strätlingite simulated here 368 compared to the amount of this phase which is identified in AAS cements; this issue is revisited in 369 section 3.2. 370

371

372 Simulations of NS-AS cements derived from slags with 0-18 mass% MgO (Figure 3) show little373 change in intrinsic porosity and total binder volume as a function of MgO content. This result differs

- 374 from previous thermodynamic modelling that showed a significant increase in total solid volume over
- this same MgO composition range (Ben Haha et al., 2011b). This difference is partly founded in the
- 376 high amounts of strätlingite predicted, but also relates to the use of the CNASH ss thermodynamic
- 377 model here, rather than the less complex thermodynamic model used to describe C-(N-)A-S-H gel by
- Ben Haha et al. (2011b) (density $\approx 2.2-2.4$ g/cm³ (Lothenbach et al., 2008)), as the current work
- 379 formally defines the uptake of Al in C-(N-)A-S-H gel and much more closely describes the volumetric
- properties of this phase in sodium silicate-activated slag cement (density = 2.6-2.7 g/cm³ in Figure
- 381 3C, compared to 2.73 ± 0.02 g/cm³ reported by Thomas et al. (2012)).
- 382
- 383



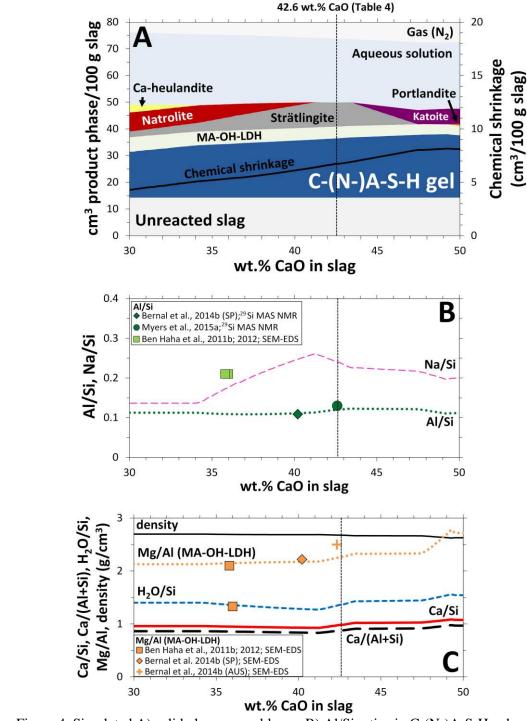
387 Figure 3. Simulated A) solid phase assemblages, B) Al/Si ratios in C-(N-)A-S-H gel, and C) Mg/Al ratios in MA-OH-LDH in NS-AS cements with bulk slag chemical compositions rescaled from Table 388 4 except for the Mg content, which is varied here. Changes in B) Na/Si, C) H₂O/Si, Ca/Si and 389 390 Ca/(Al+Si) ratios in C-(N-)A-S-H gel, and C) C-(N-)A-S-H gel density (g/cm³) are shown for visual reference. The symbols in B) and C) represent experimentally measured data for sodium silicate-391 activated slag cements (curing times are indicated in parentheses) derived from slag precursors with 392 similar Al₂O₃ and equivalent or slightly lower CaO content (11.3 < mass % Al₂O₃ < 14.1, 33.4 <393 mass% CaO \leq 42.6) to the slag represented by Table 4. 394 395

385

396 The solid phase assemblage changes markedly as a function of the MgO content of the slag (Figure 397 3A), but little change in C-(N-)A-S-H gel volume is simulated between 0 and 18 mass% MgO. The only Mg-bearing solid phase predicted is MA-OH-LDH, the amount of which increases as a function 398 of the slag MgO content. The simulated and experimentally measured Mg/Al ratios of this phase in 399 400 sodium silicate-activated slag cements are consistent to ± 0.3 units (simulated Mg/Al ≈ 2.3 , Figure 3C) 401 (Ben Haha et al., 2011b; Bernal et al., 2014b; Le Saoût et al., 2011), with the exception of the samples containing significant intermixing of additional products (with Mg/Al \ll 2). This result further 402 supports the thermodynamic description of MA-OH-LDH used here. The only predicted minor phase 403 is katoite at 11-17 mass% MgO. Brucite is not predicted here, in good agreement with its absence 404 from experimentally observed solid phase assemblages in AAS cements (Ben Haha et al., 2011b; 405 Myers et al., 2015a; Richardson et al., 1994; Schneider et al., 2001; Wang and Scrivener, 1995). 406

407

408 The Al/Si ratio of the simulated C-(N-)A-S-H gel (Al/Si ≈ 0.12) is similar to the experimentally determined Al content of this phase in sodium silicate-activated slag cements derived from slags with 409 13.2 ≥ mass% MgO (Bernal et al., 2014b; Le Saoût et al., 2011) (Figure 3B), except for the SEM-410 EDS datum at ~7.8 mass% MgO (Ben Haha et al., 2012) and the ²⁹Si MAS NMR datum at 1.2 mass% 411 MgO (Al/Si ≈ 0.2) (Bernal et al., 2014b). This discrepancy can be partly attributed to the incomplete 412 description of solid phases in the thermodynamic database, which would be particularly relevant for 413 414 the datum at 1.2 mass% MgO, as gismondine and/or N-A-S(-H) gel (which is thought to be a poorlyordered zeolite-type phase (Provis et al., 2005)) were identified as reaction products in the cement 415 416 studied by Bernal et al. (2014b). Simulations of NS-AS cements show that Ca-heulandite and natrolite are predicted for slags with \leq 41 mass% CaO (Figure 4), in good agreement with this analysis and the 417 identification of zeolites in these materials (Bernal et al., 2011; Bernal et al., 2014b). The bulk CaO 418 concentration is therefore a key parameter controlling the formation of zeolite-type phases in AAS-419 based cements. However, it is important to note that Ca-rich zeolites such as gismondine, which are 420 expected to have relatively high stability in AAS-based cements, are not described in the 421 thermodynamic database used here because reliable thermodynamic data for these phases are not 422 423 always available (Wolery et al., 2007).



424

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Figure 4. Simulated A) solid phase assemblages, B) Al/Si ratios in C-(N-)A-S-H gel, and C) Mg/Al 427 428 ratios in MA-OH-LDH in NS-AS cements with bulk slag chemical compositions rescaled from Table 429 4 except for the Ca content, which is varied here (traces). Changes in B) Na/Si, C) H₂O/Si, Ca/Si and Ca/(Al+Si) ratios in C-(N-)A-S-H gel, and C) C-(N-)A-S-H gel density (g/cm³) are shown for visual 430 431 reference. The symbols in B) and C) represent experimentally measured data for sodium silicate-432 activated slag cements derived from slag precursors with similar Al_2O_3 and MgO content (12 < 433 mass% $Al_2O_3 < 14.1$, 5.2 < mass% MgO < 7.7) to the slag represented by Table 4. The difference in intrinsic porosity within the full range of modelled CaO compositions is 3%. 434 435

436 It is also notable that the total binder (solid + aqueous phase) volume changes markedly as a function 437 of the CaO content in the slag, which suggests that the bulk CaO concentration is also a key parameter influencing the chemical shrinkage properties of these materials; a difference of $3.8 \text{ cm}^3/100 \text{ g slag}$ 438 (Δ chemical shrinkage = 47%) is identified over the range $30 \leq CaO \leq 49$ mass%, with more chemical 439 440 shrinkage predicted at higher slag CaO content (Figure 4A). Therefore, it is expected that chemical shrinkage in NS-AS cements can be reduced through the use of raw materials with lower CaO 441 content. Simulated Mg/Al ratios of the MA-OH-LDH phase and Al/Si ratios of C-(N-)A-S-H gel are 442 in close agreement with the experimental data, with the exception of the SEM-EDS data at a slag CaO 443 content of ~36 mass% which likely contains some intermixed low-Mg high-Al phases (Taylor et al., 444 2010). 445

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The modelling results presented here provide a satisfactory account of the experimental data and so give confidence in using the CNASH_ss and MgAl-OH_LDH_ss thermodynamic models to describe NS-AS cements over the most common ranges of slag compositions and activator doses used in AAS cements ($7 \le mass\% Al_2O_3 \le 13.7$, Figure 2, $5.2 \le mass\% MgO \le 13.2$, Figure 3, and $35.8 \le mass\%$ CaO ≤ 42.3 , Figure 4). Within this range, the model predictions are within ~0.04 units in the Al/Si ratios of the C-(N-)A-S-H gel and ~0.3 units in the Mg/Al ratios of the MA-OH-LDH phase.

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3.2 Simulated reaction of a Na₂SiO₃-activated slag cement

Additional thermodynamic modelling analysis of NS-AS cements was performed by varying the slag reaction extent from 0-100%, in the presence of Na_2SiO_3 (8 g $Na_2SiO_3/100$ g slag), while holding the slag chemical composition constant (Table 4).

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The predicted solid phase assemblage consists of C-(N-)A-S-H gel as the dominant reaction product, and additionally MA-OH-LDH (Mg/Al \approx 2), strätlingite, Ca-heulandite, brucite, natrolite and katoite (Figure 5A). Zeolites are only predicted for slag reaction extents <40% (i.e. effectively at low bulk CaO concentrations, consistent with Figure 4), which is less than the experimentally-determined slag

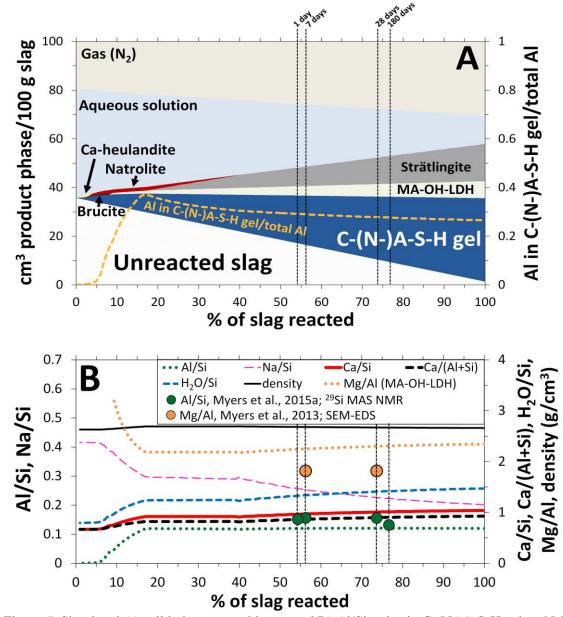
reaction extent for AAS cement after 1 day of curing (Myers et al., 2015a), and is relatively consistent
with the experimental observation of only minor amounts of these phases in AAS cements (Bernal et al., 2011; Bernal et al., 2014b).

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467 The prediction of MA-OH-LDH and strätlingite is in relatively good agreement with experimentallydetermined solid phase assemblages in NS-AS cements (Ben Haha et al., 2012; Brough and Atkinson, 468 2002; Burciaga-Díaz and Escalante-García, 2013; Myers et al., 2015a; Wang and Scrivener, 1995), 469 where Mg-Al LDH phases are often identified and the formation of AFm-type phases are likely, 470 although the calculations here do markedly over-predict the amount of strätlingite formed compared 471 to the experimental observations. Approximately constant proportions of the main hydrate phases 472 (strätlingite, MA-OH-LDH and C-(N-)A-S-H gel) are predicted relative to the total reaction product 473 474 volume at slag reaction extents exceeding 40%. The influence of the additional Si supplied by the activator is diluted as more slag reacts, as the activator is assumed to be fully dissolved in the mix 475 water prior to contact with the slag, and so contributes more significantly to the chemistry of the 476 477 reaction products when the degree of reaction of the slag is low. This means that the slag chemical 478 composition, rather than the activator, controls the stable product phase assemblage at higher extents 479 of reaction.

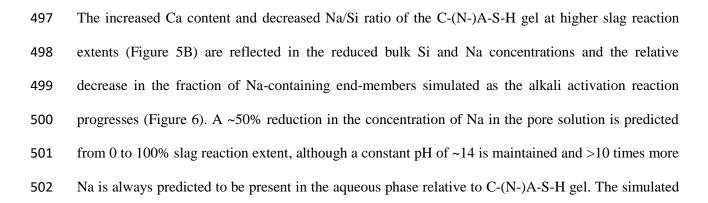
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The chemical shrinkage in this system is predicted to be $11 \text{ cm}^3/100 \text{ g}$ slag at complete reaction of the slag (an overall volume reduction of 15%, Figure 5A), which matches the chemical shrinkage quantified experimentally by Thomas et al. (2012) for a sodium silicate-activated slag cement (12.2 ± 1.5 cm³/100 g slag) and is close to the values modelled by Chen and Brouwers (2007) (11.5-13.9 cm³/100 g slag) at 100% degree of reaction of the slag. Therefore, thermodynamic modelling predicts significantly larger chemical shrinkage in NS-AS cements than measured in hydrated PC (~6 cm³/100 g cement reacted (Jensen and Hansen, 2001; Tazawa et al., 1995)).



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Figure 5. Simulated A) solid phase assemblages, and B) Al/Si ratios in C-(N-)A-S-H gel and Mg/Al
ratios in MA-OH-LDH in an NS-AS cement using the slag chemical composition in Table 4. Changes
in B) Na/Si, H₂O/Si, Ca/Si and Ca/(Al+Si) ratios in C-(N-)A-S-H gel, and B) C-(N-)A-S-H gel
density (g/cm³) are shown for visual reference. The dashed vertical lines correspond to slag reaction
extents determined experimentally at each time of curing (Myers et al., 2015a).



503 amounts of H₂O and Ca in C-(N-)A-S-H gel are directly linked via the end-member chemical 504 compositions defined in the CNASH_ss thermodynamic model (Myers et al., 2014): the Ca-rich T2C* end-member (Ca/Si = 1.5) has a higher H₂O/Si ratio (= 2.5) compared to the Al and Na-containing 505 end-members ($H_2O/Si < 2$, Table 1), and relatively more of this end-member is simulated at higher 506 507 bulk slag reaction extents (Figure 6B). The simulated trends in pore solution element concentrations at >40% slag reaction extent (Figure 6A) are within ± 1 order of magnitude to those reported for NS-AS 508 cement cured for 1-180 days (Gruskovnjak et al., 2006). More solubility data for NS-AS cement are 509 needed to further assess the simulated pore solution compositions. 510



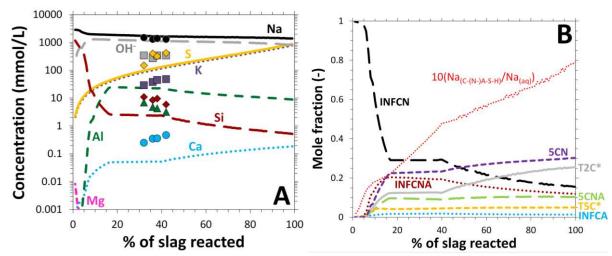
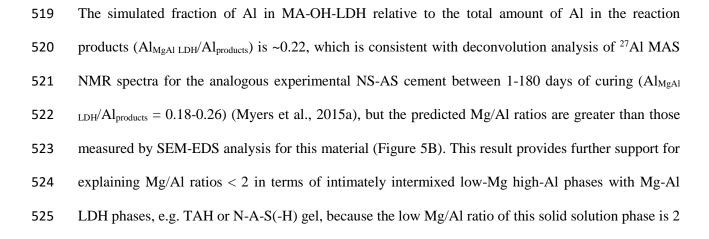


Figure 6. Simulated A) pore solution chemical compositions and B) end-member mole fractions and
ratio of Na in C-(N-)A-S-H gel relative to Na in the aqueous phase (aq) for the NS-AS cement
described by Figure 5. The mole fraction of the TobH* end-member is close to 0 over the full range of
simulated slag reaction extents (not shown in B)). The symbols in A) represent sodium silicateactivated slag pore solution data reported by Gruskovnjak et al. (2006).



526 (Richardson, 2013). However, the simulations predict that the fraction of Al in C-(N-)A-S-H gel 527 (Al_{CNASH}) relative to the total amount of Al in the reaction products (Al_{CNASH}/Al_{products}) is ~0.28 for slag reaction extents >50% (Figure 5A), which is much less than the relative amount of four-528 coordinated Al (Al[4]) assigned to the reaction products (Al[4]/Al_{products}) in ²⁷Al MAS NMR spectral 529 deconvolution analysis of this NS-AS cement (Al[4]/Alproducts = 0.60-0.75) (Myers et al., 2015a). 530 These ratios, Al_{CNASH}/Al_{products} and Al[4]/Al_{products}, would be comparable if C-(N-)A-S-H gel were the 531 only major Al[4]-bearing solid phase present in AAS cements (i.e. $Al_{CNASH}/Al[4] \approx 1$), but that is not 532 the case here. Recent solubility results for C-(N-)A-S-H gel (Myers et al., 2015b) do not support any 533 further increase in the stability of the Al-containing end-members in the CNASH ss thermodynamic 534 model, meaning that this discrepancy in the distribution of Al[4] is probably due to other factors. 535 These factors may include incomplete description of other Al[4]-containing phases in the 536 537 thermodynamic database used here, or that the discrepancy is founded in the experimental ²⁹Si and ²⁷Al MAS NMR analysis. Both options are now discussed. 538

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The amount of strätlingite predicted by the thermodynamic modelling (Figures 2-5) was likely 540 541 overestimated because this phase is not clearly distinguished in X-ray diffractograms of sodium 542 silicate-activated slag cements cured for up to 3 years (Ben Haha et al., 2012; Burciaga-Díaz and Escalante-García, 2013; Wang and Scrivener, 1995), or in NS-AS/4 mass% PC blends cured for 3 543 years (Bernal et al., 2012). The solubility product used to describe this phase (Table 1) has an 544 estimated uncertainty interval of ± 1 log unit derived directly from the scatter in the available 545 546 solubility data for this phase (see Matschei et al. (2007) and references therein), and so an error in this value is unlikely to contribute significantly to the over-prediction of this phase. Therefore, it is likely 547 that additional solid phase(s) are missing from the thermodynamic database used here (Table 1), 548 which would be predicted to form in preference to strätlingite if they were present in the simulation. 549 These may be zeolites such as gismondine and thomsonite (Bernal et al., 2011; Bernal et al., 2014b), 550 or poorly ordered Q⁴-type N-A-S(-H) ('geopolymer') gels (Myers et al., 2013), each of which will 551 accommodate Al in tetrahedral form and could account for the difference between the high tetrahedral 552 553 fraction determined experimentally, and the notably lower tetrahedral fraction predicted in the current

554 simulations. Thermodynamic data are available for a large number of zeolites (see the compilation by 555 Arthur et al. (2011) for example), but the large variety of possible chemical compositions and the 556 availability of only a few data for each zeolite framework type (often only one datum), mean that 557 more thermochemical or solubility data are needed to better define these phases in thermodynamic 558 databases.

559

The maximum possible amount of Al[4] attributable to zeolites or N-A-S(-H) gel is, however, limited 560 by the intensity of the ²⁷Al MAS NMR spectra of this NS-AS cement (Myers et al., 2015a) at ~60 561 ppm (relative to Al($H_2O_{63^{+}}$), which is the typical observed chemical shift at which Al[4] resonates in 562 these phases (Davidovits, 1991; Duxson et al., 2007; Fyfe et al., 1982). Consequently, it is unlikely 563 that zeolites and N-A-S(-H) gel can account for the large discrepancy between the modelled amount 564 565 of Al[4] in C-(N-)A-S-H gel (Al_{CNASH}/Al_{products} ≈ 0.28 , Figure 5A) and the experimentally observed amount of Al[4] assigned to reaction products (Al[4]/Al_{products} = 0.60-0.75 (Myers et al., 2015a)). 566 Further explanation for this discrepancy can be found in the assumption of congruent slag dissolution 567 applied in the analysis of ²⁹Si and ²⁷Al MAS NMR spectra used as experimental data here (Bernal et 568 569 al., 2014b; Myers et al., 2015a), which may not be fully attained in slag-based cements, and could 570 significantly alter the deconvolution analysis presented due to the different lineshapes of partially 571 reacted and unreacted slag (Dyson et al., 2007). Development of this understanding will be essential to further enhance the accuracy of the characterisation and simulation of the complex phase 572 573 assemblages which are formed in AAS-based cements.

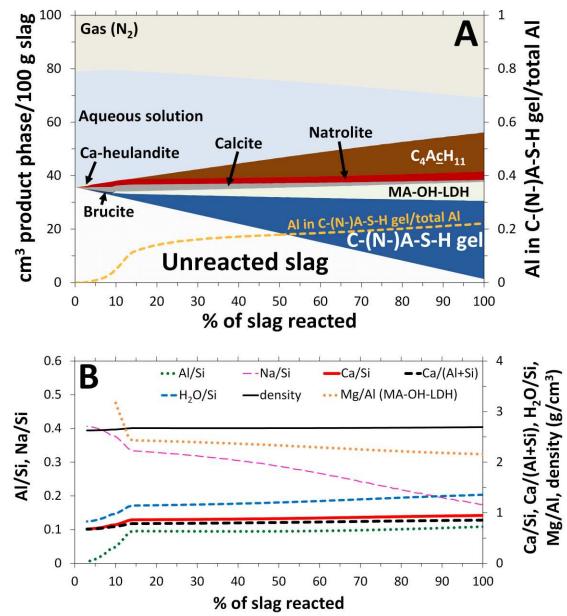
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3.3 Simulated reaction of a Na₂CO₃-activated slag cement

The reaction of a N<u>c</u>-AS cement is simulated via the same procedure used in the simulation of NS-AS cement discussed in section 3.2, except for the change in activator. The simulated solid phase assemblage contains C-(N-)A-S-H gel as the primary reaction product (Figure 7A). The additional products are C₄A<u>c</u>H₁₁, MA-OH-LDH, calcite and natrolite. The prediction of calcite is consistent with the observation of CaCO₃ polymorphs in N<u>c</u>-AS cements cured for 20 months (Sakulich et al., 2010)

and 180 days (Bernal et al., 2015). Simulation of natrolite and Ca-heulandite is also in good 581 582 agreement with the identification of heulandite and zeolite-A in Nc-AS cement (Bernal et al., 2015). The modelling results presented here and in section 3.3 are consistent with the identification of more 583 prominent peaks for zeolites in X-ray diffraction patterns for Nc-activated (Bernal et al., 2015), 584 compared to NS-activated, slag cements (Bernal et al., 2014b). C₄A<u>c</u>H₁₁ has been identified in X-ray 585 diffractograms of Nc-AS pastes cured for 1 day and for 540 days (Shi et al., 2006), although this 586 phase is not always observable (Bernal et al., 2015; Sakulich et al., 2010) due to its tendency to be 587 present as intermixed (Richardson et al., 1994) and/or poorly crystalline structures (Wang and 588 Scrivener, 1995). The simulated chemical shrinkage extents for Nc-AS (Figure 7) and NS-AS cements 589

590 (Figure 5) at 100% slag reaction extent are comparable, at $11 \text{ cm}^3/100 \text{ g slag}$.



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Figure 7. Simulated A) solid phase assemblages and B) C-(N-)A-S-H gel chemical compositions and densities (g/cm³), and Mg/Al ratios in MA-OH-LDH in an N<u>c</u>-AS cement using the slag chemical composition in Table 4.

Mg-Al LDH phases are experimentally observed in N<u>c</u>-AS cements after 180 days (Bernal et al., 2015) and 55 days (Sakulich et al., 2009) of curing, in good agreement with the predicted phase assemblage (Figure 7A). Here, MA-<u>c</u>-LDH is not predicted despite the high availability of CO₂, demonstrating the very high stability of MA-OH-LDH under the pH \geq 13 conditions in a hardened N<u>c</u>-AS cement. Further clarification of this result is needed because recent ²⁷Al MAS NMR results for superficially carbonated NS-AS cements (Myers et al., 2015a), and carbonation depth analysis of

604 these materials after exposure to air for 16 months (Bernal et al., 2014b) can be interpreted in support 605 of the formation of Mg-Al LDH phases intercalated with CO₃²⁻. Detailed assessment of solubility and thermochemical data for Mg-Al LDH phases intercalated with OH^{-} and CO_{3}^{2-} (Bennett et al., 1992; 606 Gao and Li, 2012; Johnson and Glasser, 2003; Morimoto et al., 2012; Rozov et al., 2011) indicates 607 608 that the solubility product used to describe the Mg/Al = 2 MA-OH-LDH end-member of the MA-OH-LDH ss thermodynamic model here may be in error by as much as several log units (Figure 1) and 609 demonstrates the need for further studies of the thermodynamic properties of Mg-Al LDH phases. 610 611 Gaylussite has been observed in Nc-AS cement at early age (Bernal et al., 2015) but is not present in 612 the solid phase assemblage simulated here (Figure 7); this phase is slightly undersaturated at low slag 613 reaction extents at ~25°C (Bury and Redd, 1933; Königsberger et al., 1999). This difference indicates 614

and this is consistent with its observed consumption as the reaction proceeds (Bernal et al., 2015).

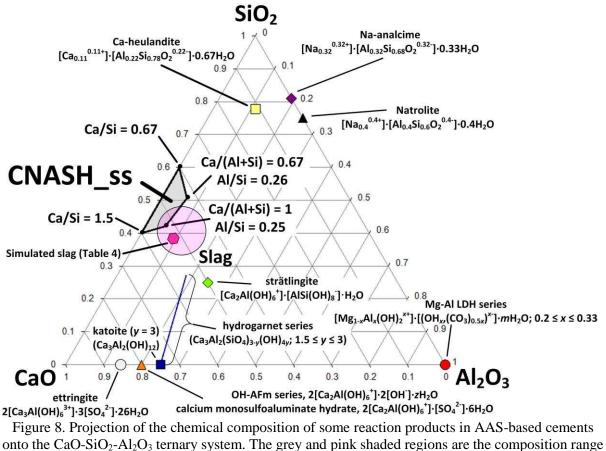
that kinetic factors enable the formation of gaylussite in Nc-AS cement cured at room temperature,

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618 **3.4 Phase diagrams for alkali-activated slag-based cements**

The prediction of several reaction products in the simulated AAS cements is consistent with the bulk chemical composition of the mixes, which generally lie outside the composition envelope of phasepure C-(N-)A-S-H gel (Figure 8).



onto the CaO-SiO₂-Al₂O₃ ternary system. The grey and pink shaded regions are the composition range
 described by the CNASH_ss thermodynamic model for C-(N-)A-S-H gel (Myers et al., 2014), and the
 typical bulk chemical composition range of slag, respectively. The simulated slag described in Table 4
 is represented by the pink hexagon.

Further analysis of AAS cement chemistry is performed by simulating phase diagrams at a fixed slag 630 631 reaction extent of 60%, a constant amount of H_2S (equivalent in S content to a slag composition of 2 632 mass% SO₃, which is taken as a representative value of S content in slags studied in the literature (Ben Haha et al., 2011a; Bernal et al., 2014b; Gruskovnjak et al., 2006; Puertas et al., 2011; 633 Richardson et al., 1994; Shi et al., 2006)) and slag compositions of either 30 or 40 mass% SiO₂, with 634 the remaining chemical composition specified in terms of CaO, Al_2O_3 and MgO only. The CaO-635 636 Al₂O₃-MgO composition range selected here was chosen to represent the bulk chemical composition range relevant to AAS-based cements. 637

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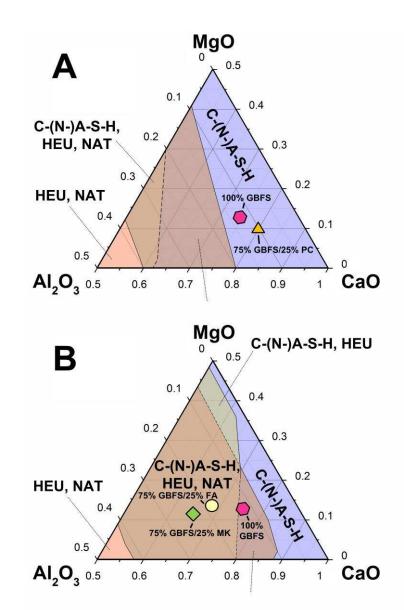
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Zeolites are predicted in every phase diagram for the AAS cements simulated (shown for NS-AS
cements only in Figure 9), and are more prominent at higher Si (i.e. lower Ca) and Al concentrations,
but only Ca-heulandite and natrolite are predicted among the zeolites included in the thermodynamic

642 database (Table 1). The CaO-Al₂O₃-MgO composition region where C-(N-)A-S-H gel and zeolites are 643 both simulated indicates where C-(N-)A-S-H and N-A-S(-H) gels are likely to coexist in AAS cements, due to the fundamental similarities of zeolites and N-A-S(-H) ('geopolymer') gels (Provis et 644 al., 2005). Inclusion of reliable thermodynamic data for N-A-S(-H) gel and zeolites will be necessary 645 646 to clarify the chemical compositional envelope in which these gels can coexist. The prediction of zeolites here, in both the higher pH ((NH)_{0.5}-AS) and lower pH systems (Nc-AS), Figures 7 and 9, 647 indicates that increasing pH does not destabilise these phases and the corresponding N-A-S(-H) gel in 648 favour of C-(N-)A-S-H gel in the pH and chemical composition range relevant to cements, as was 649 proposed previously by García-Lodeiro et al. (2011). The increased stability of zeolites at lower CaO 650 content (Figure 4), or alternatively higher Si and Al concentrations (Figure 9) - i.e. decreasing 651 CaO/(Al₂O₃ + SiO₂) - demonstrates that control of Ca-Al-Si compositions is needed to form alkali-652 653 activated cements with mixed C-(N-)A-S-H and N-A-S(-H) gels (Ismail et al., 2014). Figure 9 shows that mixtures of C-(N-)A-S-H gel and zeolites are expected to be stable in Na₂SiO₃-activated 75 654 mass% GBFS/25 mass% fly ash (FA) (overall precursor SiO_2 content = 41 mass% based on the FA 655 chemical composition from (Bernal et al., 2013)) or metakaolin (MK) cements (overall precursor SiO₂ 656 657 content = 38 mass% based on the MK chemical composition from (Bernal et al., 2011)), but not in a hybrid system of Na2SiO3-activated 75 mass% GBFS/25 mass% PC (based on a PC chemical 658 composition of 19.7 mass% SiO₂, 63.2 mass% CaO, 1.85 mass% MgO, 4.7 mass% Al₂O₃, 3.35 659 660 mass% SO₃ (Lothenbach and Winnefeld, 2006)). Figure 9 also shows that the stability of zeolites, and 661 therefore of N-A-S(-H) gels, in NS-AS cement depends greatly on the slag SiO₂ content.

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| 667 | Figure 9. Phase diagrams for NS-AS-based cement systems with overall precursor chemical |
| 668 | compositions of 2 mass% SO ₃ equivalent and A) 30 mass% SiO ₂ and B) 40 mass% SiO ₂ , with only |
| 669 | the regions of stability for C-(N-)A-S-H gel and zeolites shown (Mg-containing phases are also |
| 670 | typical reaction products: MA-OH-LDH at moderate and high Al ₂ O ₃ content |
| 671 | $(Al_2O_3/(CaO+Al_2O_3+MgO) > 0.1)$; and brucite at moderate and low Al_2O_3 concentrations |
| 672 | (Al ₂ O ₃ /(CaO+Al ₂ O ₃ +MgO) < 0.25)). See text for the GBFS, FA, MK and PC chemical compositions |
| 673 | used. The w/b ratio is 0.4, the overall precursor reaction extent is 60% and the units are in mole |
| 674 | fraction. |
| 675 | |
| | |

676 Simulated phase diagrams for $(NH)_{0.5}$ -AS-based cements are shown in Figure 10. The dominant solids 677 in the simulated phase diagrams for $(NH)_{0.5}$ -AS-based cements (Figure 10) are C-(N-)A-S-H gel and 678 MA-OH-LDH. C-(N-)A-S-H gel is simulated over the full range of modelled CaO-Al₂O₃-MgO 679 compositions, and MA-OH-LDH is predicted everywhere in this composition range except at very 680 low Al₂O₃ content (Al₂O₃/(CaO+Al₂O₃+MgO) < 0.05).

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Symbol

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| Phase assemblage | 0.4 |
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| 1, 2, 5, 6, 10 | |
| 1, 2, 5, 6 | 0.4 m k 1 0.1 |
| 1, 2, 4, 5, 6 | b |
| 1, 2, 4, 5, 6, 10 | 0.5 |
| 1, 2, 3, 4, 5, 6, 10 | |
| 1, 2, 3, 4, 5, 6 | Al ₂ O ₃ 0.5 0.6 0.7 0.8 0.9 1 CaO |
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| 1, 2, 3, 5, 6, 7 | |
| South Company of the Southern State of the Company of | n. MaO |
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| 1, 2, 5, 9, 10 1, 5, 6, 10 1, 5, 10 1, 2, 5, 6, 8, 10 | |
| 1, 2, 5, 9, 10 1, 5, 6, 10 1, 5, 10 | B q 0.1 u 0.5 a 0.4 c |
| 1, 2, 5, 9, 10 1, 5, 6, 10 1, 5, 10 1, 2, 5, 6, 8, 10 1, 2, 5, 8, 10 | $\mathbf{B} \qquad \mathbf{q} \qquad 0 \qquad $ |
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| 1, 2, 5, 9, 10 1, 5, 6, 10 1, 5, 10 1, 2, 5, 6, 8, 10 1, 2, 5, 8, 10 1, 2, 5, 8 1, 2, 3, 5, 8 1, 2, 3, 5, 8, 10 1, 2, 3, 5, 7, 8, 10 | $B = \begin{pmatrix} d & 0 & 0.5 \\ 0.1 & 0.4 & c \\ 0.2 & v & 0.3 \\ 0.3 & v & c \end{pmatrix}$ |
| 1, 2, 5, 9, 10 1, 5, 6, 10 1, 5, 10 1, 2, 5, 6, 8, 10 1, 2, 5, 8, 10 1, 2, 5, 8 1, 2, 3, 5, 8 1, 2, 3, 5, 8, 10 1, 2, 3, 5, 7, 8, 10 1, 2, 3, 5, 7, 8 | B q 0.1 0.4 0.4 0.4 0.4 0.3 c |
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| 1, 2, 5, 9, 10 1, 5, 6, 10 1, 5, 10 1, 2, 5, 6, 8, 10 1, 2, 5, 8, 10 1, 2, 5, 8 1, 2, 3, 5, 8 1, 2, 3, 5, 8, 10 1, 2, 3, 5, 7, 8, 10 1, 2, 3, 5, 7, 8 1, 2, 9, 10 | B q 0.1 0.2 0.4 v 0.4 c 0.3 c 0.3 c 0.1 d 0.4 c 0.3 c 0.1 d 0.4 c 0.3 c 0.1 d 0.4 c 0.3 c 0.2 0.4 c 0.3 c 0.3 c 0.4 c 0.3 c 0.3 c 0.4 c 0.4 c 0.3 c 0.4 c 0.4 c 0.3 c 0.4 c c 0.4 c 0.4 c c c c c c c c c c c c c |

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Figure 10. Phase diagrams in the relevant bulk CaO-Al₂O₃-MgO composition range for (NH)_{0.5}-AS-685 based cements with A) 30 and B) 40 mass% slag SiO₂ content, and 2 mass% SO₃ equivalent. The 686 phases are: 1, C-(N-)A-S-H gel; 2, MA-OH-LDH; 3, strätlingite; 4, katoite; 5, ettringite; 6, calcium 687 monosulfoaluminate hydrate; 7, natrolite; 8, Ca-heulandite; 9, portlandite; and 10, brucite. The w/b 688 ratio is 0.4, the slag reaction extent is 60% and the units are in mole fraction. 689 690

691 Ettringite is predicted over a much larger range of CaO-Al₂O₃-MgO compositions than calcium monosulfoaluminate hydrate. These phases are predicted to form here for slag with 2 mass% SO₃ 692 equivalent but not for slag containing 0.8 mass% equivalent SO_3 (Table 4). Katoite is only present in 693 the phase diagrams for slags with 30 mass% SiO₂ in the (NH)_{0.5}-AS system. Portlandite is more 694 prominent in the 30 mass% SiO₂ (NH)_{0.5}-AS system (Figure 10A), but is only formed at relatively low 695

696 Al₂O₃ content (Al₂O₃/(CaO+Al₂O₃+MgO) \leq 0.12). Brucite is predicted in both phase diagrams, but 697 not at high Al_2O_3 concentrations ($Al_2O_3/(CaO+Al_2O_3+MgO) > 0.2$). Natrolite and Ca-heulandite are the only zeolites simulated in the phase diagrams. Ca-heulandite has a larger stability region than 698 699 natrolite in the 40 mass% SiO₂ system, but is not predicted at a SiO₂ content of 30 mass%, where only 700 natrolite is simulated. However, the overall CaO-Al₂O₃-MgO composition region where zeolites are 701 stable in $(NH)_{0.5}$ -AS-based cements increases as a function of increasing slag SiO₂ content, which is consistent with the trends in zeolite stability described above for NS-AS-based cements (Figures 4 702 and 9). Similarly, the CaO-Al₂O₃-MgO composition range where strätlingite is stable is larger in the 703 40 mass% SiO₂ (NH)_{0.5}-AS cement system. These phases, strätlingite, natrolite and Ca-heulandite are 704 only simulated for $Al_2O_3/(CaO+Al_2O_3+MgO)$ ratios > 0.1, showing that intermediate to high Al 705 706 concentrations are needed to stabilise these phases in (NH)_{0.5}-AS-based cements.

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The phase diagrams presented here provide a framework for predicting solid phase assemblages in 708 AAS cements, which can be improved with more relevant data, e.g. development of the 709 thermodynamic database used (Tables 1-3). This work improves the way in which high-performance 710 711 AAS-based cements can be designed, by linking the volumetric properties and solid phases formed in these cements to the raw materials used in their production. This framework also represents an 712 important step towards predicting the durability of AAS-based cements, although further work is 713 needed to link the key degradation mechanisms, e.g. carbonation, with the volumetric properties 714 715 (Provis et al., 2012) and phase assemblages (Bernal et al., 2014b) in these cements.

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- 717

718 **4. Conclusions**

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720 This paper has presented a thermodynamic modelling analysis of AAS-based cements. The 721 thermodynamic database used contains a CNASH_ss thermodynamic model for C-(N-)A-S-H gel, 722 which explicitly describes Na and tetrahedral Al incorporated into this phase, a MA-OH-LDH_ss

723 ideal solid solution thermodynamic model for MA-OH-LDH, and thermodynamic data for some alkali 724 carbonate and zeolite phases. The thermodynamic database presented here extends the utility of 725 thermodynamic modelling in predicting the long-term chemistry of AAS-based cements, which is 726 important for application of these materials, e.g. in the design of high performance cements for 727 construction and in nuclear waste disposal applications, and further promotes the valorisation of 728 metallurgical slags.

729

Thermodynamic modelling of NS-AS cements generally showed that the CNASH_ss thermodynamic 730 model described the Al/Si ratios of the C-(N-)A-S-H gels formed in the most relevant composition 731 range/alkali content for the majority of AAS cements. The Mg/Al ratios of the simulated MA-OH-732 LDH phase was generally in good agreement with experimental results for this phase in AAS 733 734 cements, although additional thermodynamic data for MA-OH-LDH are needed to clarify the stability of this phase in carbonated and Nc-activated cement. Additional thermodynamic data for other 735 736 reaction products such as TAH, zeolites and N-A-S(-H) gels are also needed for better consistency 737 with the experimental Al/Si ratios in C-(N-)A-S-H gel and Mg/Al ratios in Mg-Al LDH. Simulated 738 solid phase assemblages for NS-AS cements compared closely to the solid phases identified experimentally in these materials, and the simulations accurately predicted the experimentally 739 740 measured chemical shrinkage in a NS-AS cement.

741

Phase diagrams for (NH)_{0.5}-AS- and NS-AS-based cements were simulated, which showed that C-(N-742 743)A-S-H gel and MA-OH-LDH are formed over the majority of chemical compositions relevant to these cements. Natrolite and Ca-heulandite featured more prominently in the phase diagrams at lower 744 CaO concentration, and higher SiO₂ and Al₂O₃ content, indicating that the bulk CaO/(SiO₂ + Al₂O₃) 745 ratio plays a significant role in stabilising zeolites, and therefore N-A-S(-H) gels, in AAS-based 746 cements. Zeolites were predicted to be stable in NS-activated 75 mass% GBFS/25 mass% FA and MK 747 cements but not in hybrid NS-activated 75 mass% GBFS/25 mass% PC. Therefore, these phase 748 diagrams can be used as a reference tool for the development of high-performance AAS-based 749

cements, by enabling solid phase assemblages for these cements to be predicted from the bulkcompositions of the raw materials used.

752

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- 756

757 **6. References**

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