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Modelling ruptures of buried high-pressure dense-phase CO₂ pipelines in carbon capture and storage applications - Part II. A full-scale rupture

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Abstract

Carbon capture and storage (CCS) presents a short-term option for significantly reducing the amount of carbon dioxide (CO₂) released into the atmosphere. National Grid initiated the COOLTRANS research programme to consider the CCS pipeline transportation of high-pressure dense-phase CO₂, including the development and application of a mathematical model for predicting the sonic near-field dispersion of pure CO₂ following pipeline venting or failure. In Part I (Wareing et al. IJGGC 2015 doi:10.1016/j.ijggc.2015.01.020) validation of this numerical model against experimental data was considered, with reasonably good agreement quantitatively and qualitatively demonstrated for a rupture of a 0.15 m external diameter pipeline. In this second part, the model is applied to the rupture of a 96 km pipeline with a nominal 0.61 m external diameter, the same as that proposed in the Don Valley CCS

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Project. In the base-case, six snapshots of the flow dispersing into dry air are numerically simulated. Integrated mass and momentum fluxes exiting the crater are calculated, with the intention that they can be directly employed as source conditions for far-field dispersion simulations. The amount of solid CO₂ deposited in the crater is estimated through particle tracking techniques and six sensitivity studies vary crater properties.



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1. Introduction

Carbon capture and storage (CCS) refers to a set of technologies designed to reduce carbon dioxide (CO₂) emissions from large industrial point sources of emission, such as coal-fired power stations, in order to mitigate greenhouse gas production. The technology involves capturing CO₂ and then storing it in a reservoir, instead of allowing its release to the atmosphere, where it contributes to climate change. Once captured, the CO₂ is transported and stored, typically underground, or used for processes such as enhanced oil recovery.

National Grid initiated the TRANSPORTation of Liquid CO₂ research programme (COOLTRANS) (Cooper, 2012) in order to address knowledge gaps relating to the safe design and operation of onshore pipelines for transporting dense-phase CO₂ from industrial emitters in the UK to storage sites offshore. This includes developing the capability for modelling the low-probability, high-impact worst case - an accidental release from a buried pipeline that contains CO₂ in the dense-phase. Learning from these studies can subsequently be combined with a range of other information to develop an ap-

18 appropriate quantified risk assessment (QRA) for a dense-phase CO₂ pipeline.
19 With regard to modelling the worst case, the programme includes theoret-
20 ical studies by University College London (UCL), the University of Leeds
21 and the University of Warwick, carried out in parallel to provide “state of
22 the art” numerical models for the pipeline outflow (UCL), near-field dis-
23 persion behaviour (University of Leeds) and far-field dispersion (University
24 of Warwick) behaviour associated with below-ground CO₂ pipelines that are
25 ruptured or punctured. Experimental work and studies using currently avail-
26 able practical models for risk assessment are being carried out by DNV GL
27 (Allason et al., 2012).

28 The University of Leeds mathematical model (Wareing et al., 2013a) has
29 been previously validated for free releases into air (Woolley et al., 2013;
30 Wareing et al., 2014a), small-scale laboratory releases and dry ice particle
31 behaviour (Wareing et al., 2013b, 2015b) and punctures of buried pipelines
32 (Wareing et al., 2014b). In Wareing et al. (2015a) (hereafter referred to as
33 Part I), the model was applied to a rupture experiment involving a 0.15 m ex-
34 ternal diameter pipeline - nominally 1/4 of the scale of the ‘full-scale’ 0.61 m
35 external diameter pipeline proposed in the Don Valley CCS Project (Cooper,
36 2012; Cooper and Barnett, 2014). Numerical simulations were compared to
37 experimental data, specifically measurements of temperature on a plane 1 m
38 above the crater into which the release flowed. The comparison demonstrated
39 reasonably good quantitative and qualitative agreement regarding tempera-
40 tures and structures in the dispersion flow. Inconsistencies were interpreted
41 as effects of differences between the ideal numerical initial condition and the
42 real conditions in the experiment, only revealed through post-experiment

43 investigations. Specifically the data-blind simulation assumed the two flows
44 into the symmetric crater were identical. Investigations revealed this was not
45 the case. Full details can be found in Part I. Here, in Part II, we consider the
46 near-field flow in a full bore rupture of a buried full-scale pipeline. We define
47 the near-field in this scenario as the region of the flow containing the sonic
48 multi-phase shock-containing expansion regions around any pipeline rupture
49 locations and interactions of flows in any crater formed by the rupture. The
50 aim of this work is to produce validated flows at the termination of the near-
51 field region, ideally at the top of the crater (ground-level), that can act as a
52 thermodynamically accurate source condition for far-field modelling, defined
53 as the regions of the flow outside and downstream of the near-field. The
54 objective of this paper is to present these validated flows for far-field use.
55 Previous modelling of the near- and far-field, discussed in detail in Part I,
56 has lacked such sonic flow and thermodynamic accuracy. Consequent far-field
57 dispersion in the COOLTRANS project has been modelled by the University
58 of Warwick and is not in the scope of this paper.

59 The rupture is modelled as a break at the mid-point along a 96 kilometre
60 (km) length of below-ground transportation pipeline. The rupture break is
61 modelled as if an entire 12 m section of the pipeline has unzipped along the
62 pipeline direction, then unrolled across the pipeline direction and separated
63 from the rest of the pipeline, forming the base of crater and leaving two
64 clean guillotine breaks in the pipeline at the locations where this section pre-
65 viously joined to the rest of the pipeline. This creates two identically-shaped
66 inlets into the crater, each a cross-section of the pipeline. One is on the
67 upstream side of the rupture, henceforth referred to as the upstream inlet,

68 and one is on the downstream side of the rupture, henceforth referred to as
69 the downstream inlet. This is commonly known as a ‘double-ended guillotine
70 break’ in a pipeline. UCL have numerically modelled the pipe flow assum-
71 ing instant removal of the section described above and provided a two-hour
72 outflow prediction detailing the upstream and downstream inlet conditions.
73 We use this prediction to define conditions at the upstream and downstream
74 pipe inlets into the crater. Since it has not been computationally possible to
75 simulate the entire outflow in sufficient detail to accurately capture the near-
76 field thermodynamics, a method of simulating a number of instants in time,
77 or snapshots of the sequence of steady-states that the flow passes through,
78 with sufficient resolution has been used to investigate the rupture flow. Inte-
79 grated mass and momentum flux through a horizontal plane at or above the
80 crater (depending on the near-field flow structure) has been calculated for
81 each snapshot. The size and shape of the crater remains constant, based on
82 craters observed in experimental studies, the details of which were provided
83 from DNV GL through the COOLTRANS research programme. To test the
84 effect of different crater sizes and shapes on the dispersion flow through the
85 crater, a number of sensitivity studies are performed.

86 We reviewed relevant CO₂ dispersion work previously and refer the reader
87 to our recent publications in this area, specifically to Part I, to Wareing
88 et al. (2014a) and to Wareing et al. (2014b). The work herein represents
89 the first application of an accurate near-field model to an accidental rupture
90 scenario involving a time-dependent decompression from a full-scale buried
91 CCS pipeline. Other recent work in this area has been limited to above-
92 ground free venting releases, or has used a similar near-field model to that

93 described herein, but considered a constant crater source condition for the
 94 far-field modelling (Woolley et al., 2014).

95 In the next Section we review our mathematical model and numerical
 96 method. In Section 3 we present our methodology, including numerical tech-
 97 niques, initial conditions, sensitivity studies and particle tracking methods.
 98 The base-case numerical predictions are presented in Section 4 with the re-
 99 sults of the sensitivity study presented in Section 5. Finally, the limits of
 100 applicability of these simulations are discussed in Section 6, followed by the
 101 conclusions and possibilities for future developments and improvements in
 102 Section 7.

103 2. Mathematical model and numerical method

104 The numerical approach is essentially the same as that adopted and val-
 105 idated in our earlier papers, discussed in detail in Part I. We reproduce the
 106 necessary details below.

107 2.1. Reynolds-averaged Navier-Stokes model

108 The Reynolds-averaged Navier-Stokes (RANS) equations, closed with a
 109 compressibility-corrected k- ϵ turbulence model, employed in this work are:

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0 \quad (1)$$

$$\frac{\partial \rho C}{\partial t} + \nabla \cdot (\rho C \mathbf{u}) - \nabla \cdot (\mu_T \nabla C) = 0 \quad (2)$$

$$\frac{\partial \rho \mathbf{u}}{\partial t} + \nabla \cdot (\rho \mathbf{u} \mathbf{u}) + \nabla P - \nabla \cdot \tau = 0 \quad (3)$$

$$\frac{\partial E}{\partial t} + \nabla \cdot [(E + P) \mathbf{u} - \mathbf{u} \cdot \tau] - \nabla \cdot (\mu_T T \nabla S) = 0 \quad (4)$$

113

$$\frac{\partial \rho k}{\partial t} + \nabla \cdot (\rho k \mathbf{u}) - \nabla \cdot (\mu_T \nabla k) = s_k \quad (5)$$

114

$$\frac{\partial \rho \epsilon}{\partial t} + \nabla \cdot (\rho \epsilon \mathbf{u}) - \nabla \cdot (\mu_\epsilon \nabla \epsilon) = s_\epsilon \quad (6)$$

115 where the variables have their usual meanings and are defined in the Notation
 116 section, noting that the vector velocity is expressed in bold as \mathbf{u} and S is the
 117 entropy per unit mass. The turbulent diffusion coefficients are

$$\mu_T = \rho C_\mu \frac{k^2}{\epsilon}, \quad (7)$$

118 and

$$\mu_\epsilon = \frac{\mu_T}{1.3}, \quad (8)$$

119 with $C_\mu = 0.09$. The turbulence production term is

$$P_t = \mu_T \left[\frac{\partial u_i}{\partial x_j} \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \right] - \frac{2}{3} \nabla \cdot \mathbf{u} (\rho k + \mu_T \nabla \cdot \mathbf{u}), \quad (9)$$

120 where the summation convention has been assumed. The k source term is

$$s_k = P_t - \rho \epsilon \quad (10)$$

121 whilst the ϵ source term is

$$s_\epsilon = \frac{\epsilon}{k} (C_1 P_t - C_2 \rho \epsilon) \quad (11)$$

122 with $C_1 = 1.4$ and $C_2 = 1.94$. The turbulent stress tensor, τ , is

$$\tau_{ij} = \mu_T \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) - \frac{2}{3} \delta_{ij} (\mu_T \nabla \cdot \mathbf{u} + \rho k). \quad (12)$$

123 The k - ϵ turbulence model described here is coupled to a compressibility
 124 dissipation rate correction proposed by Sarkar et al. (1991). Comparisons of

125 model predictions with this correction and experimental data have shown sig-
126 nificant improvements over results derived using the standard $k-\epsilon$ approach
127 for moderately and highly under-expanded jets of the type under considera-
128 tion here (Cumber et al., 1994, 1995).

129 *2.2. Equation of state*

130 For CO_2 , the composite equation of state described in Wareing et al.
131 (2013a) is employed. This composite method predicts the thermophysical
132 properties of the three phases of CO_2 for the range of temperatures of rele-
133 vance to CO_2 dispersion from releases at sonic velocities, of interest to the
134 CCS industry. This equation of state has been developed in such a way that
135 is convenient for computational fluid dynamic applications; the gas phase is
136 computed from the Peng-Robinson equation of state (Peng and Robinson,
137 1976), and the liquid and condensed phases from tabulated data generated
138 with the Span & Wagner equation of state (Span and Wagner, 1996) and the
139 DIPPR[®] Project 801 database (<http://www.aiche.org/dippr/>), academic ac-
140 cess to which can be gained through the Knovel library (<http://why.knovel.com>).
141 Pressure, gas and condensed phase densities, sound speed and internal energy
142 have all been tabulated against temperature on the saturation line between
143 100K and the critical temperature, providing the basis for a fully functional
144 form for differentiation, interpolation and extrapolation in numerical simu-
145 lations. Air is modelled via an ideal gas equation of state with $\gamma_a = 7/5$.

146 *2.3. Homogeneous equilibrium model*

147 In previous work considering dense-phase CO_2 releases from small nozzles
148 and punctures (Wareing et al., 2014a,b), particles of solid CO_2 do not reach

149 equilibrium with the CO₂ gas flow in the initial expansion due to the short
150 distance between release point and Mach shock when compared to particle
151 thermal and dynamic relaxation times and velocities (Wareing et al., 2013b).
152 There a relaxation model was applied to the movement of the condensed
153 phase. In this work, where the distance between the release point and Mach
154 shock is an order of magnitude or more times greater than the relaxation
155 distances (dictated by the particle velocities and thermal and dynamic relax-
156 ation times (Wareing et al., 2013b, 2015b)) we assume that the condensed
157 phase is in equilibrium with the vapour phase and no relaxation model is
158 used.

159 *2.4. Implementation*

160 The composite equation of state is implemented within this homogeneous
161 equilibrium model into MG, an adaptive mesh refinement (AMR) RANS hy-
162 drodynamic code (Falle, 1991). The code employs an upwind, conservative
163 shock-capturing scheme and is able to employ multiple processors through
164 parallelisation with the message passing interface (MPI) library. Integration
165 in time proceeds according to a second-order accurate Godunov method (Go-
166 dunov, 1959). In this case, a Harten Lax van-Leer (van Leer, 1977; Harten
167 et al., 1983) (HLL) Riemann solver was employed to aid the implementation
168 of complex equations of state. The disadvantage of the HLL solver is that it
169 is more diffusive for contact discontinuities; this is not important here since
170 the contact discontinuities are in any case diffused by the artificial viscos-
171 ity. The artificial viscosity is required to ensure shocks travel at the correct
172 speed in all directions and is at a very low level, decreasing proportionally
173 with increasing resolution.

174 *2.5. Adaptive meshing strategy*

175 The AMR method (Falle, 2005) employs an unstructured grid approach,
176 requiring an order of magnitude less memory and giving an order of magni-
177 tude shorter computation times than structured grid AMR. The two coarsest
178 levels (0 and 1) cover the whole computational domain; finer grids need not
179 do so. Refinement or derefinement depends on a given tolerance. Where
180 there are steep gradients of variable magnitudes such as at flow boundaries
181 or discontinuities such as at the Mach disc, this automated meshing strategy
182 allows the mesh to be more refined than in areas of the free stream in the
183 surrounding fluid. Each layer is generated from its predecessor by doubling
184 the number of computational cells in each spatial direction. This technique
185 enables the generation of fine grids in regions of high spatial and temporal
186 variation, and conversely, relatively coarse grids where the flow field is numer-
187 ically smooth. Defragmentation of the AMR grid in hardware memory was
188 performed at every time-step, gaining further speed improvements for neg-
189 ligible cost through reallocation of cells into consecutive memory locations.
190 The simulations presented below employed 5 levels of AMR and hence a low
191 level of artificial viscosity. A grid resolution control has been imposed in the
192 AMR, allowing for the full resolution of the sonic decompression and Mach
193 shock near the inlet pipes and also the larger scale of the crater, extending
194 a few metres above and to the sides of the crater, in order to establish the
195 flow out of the crater on a plane above the near-field of the release. This was
196 required to achieve reasonable computational execution times (on average
197 100,000 CPU hours per run, more for higher resolution convergence tests).

198 **3. Methodology**

199 *3.1. Quasi-steady-state flows*

200 Quasi-steady-state flows were achieved by integrating the simulations un-
201 til the flow out of the top of the crater did not change and the integrated
202 mass-flux leaving the crater through a horizontal plane at or above ground-
203 level matched the integrated mass-flux into the crater from the combined
204 pipe inlets. These are henceforth referred to as ‘steady-state’ flows. Steady-
205 state flows were typically achieved in a physical time of less than 1 second.
206 They are convergent, tests with higher resolutions, a single symmetry and no
207 symmetry boundaries having shown that the flow structure is qualitatively
208 and quantitatively closely similar to the results presented here. It should also
209 be noted that small variations in pressure, temperature and velocity at the
210 inlets do not greatly affect the steady-state flow structure, shifting only the
211 position and width of the Mach shock very slightly, with little to no effect
212 on the post-shock flow conditions, although if these variations unbalance the
213 inlet conditions between upstream and downstream pipes, large effects can
214 be observed, moving the flow out of the crater away from the centre of the
215 crater as shown later in this work.

216 *3.2. Pipeline inlet conditions*

217 The full-scale rupture modelled is a double ended guillotine break at the
218 mid-point along a 96 km length of below-ground transportation pipeline, with
219 external diameter (d) of 0.61 m and pipeline wall thickness of 19.4 mm. It
220 is henceforth referred to as the ‘base-case’. A single 12 m section of pipeline
221 has ruptured, in effect unzipping, flattening and dropping to form the base

222 of the crater as previously described. The pipeline has a 1.2 m depth of
223 soil cover. Valves are located 8 km upstream and 8 km downstream of this
224 break. Valve closure begins after 900 s and the valve closure time is 30 s.
225 At the time of the break, the pipeline is assumed to be filled with stationary
226 dense-phase CO₂ at an initial pressure at the upstream end of the pipeline of
227 150 barg and temperature of 303 K. We employ predictions of the pipeline
228 outflow calculated by UCL and provided through the COOLTRANS research
229 programme. This model has recently been applied to the modelling of CO₂
230 discharge following full-bore rupture of pipelines (Brown et al., 2013) where
231 it was shown to produce reasonable agreement in comparison with available
232 experimental data.

233 The inlet pressure at each pipe end predicted by UCL is shown in Figure
234 1. As can be seen from this figure, the variation of inlet pressure with time is
235 slow compared to the thermal and dynamical relaxation times in this decom-
236 pression, which are fractions of a second (Wareing et al., 2013b, 2015b). The
237 variation of the other inlet conditions is also slow i.e. temperature, velocity,
238 mass-flow and condensed phase fraction. The velocities in the near-field are
239 high (greater than 50 m s⁻¹) with flow times across the crater and into the
240 plume consequently short (less than 0.5 s). The decompression flow there-
241 fore passes through a sequence of steady states, as the steady-state flow out
242 of the crater is achieved in typically less than a second, considerably faster
243 than the variation of inlet conditions affects the near-field. Hence, as it not
244 computationally possible to simulate the entirety of the decompression (due
245 to hardware and time constraints), it is entirely reasonable to simulate a
246 number of representative steady states, or ‘snapshots’, at specific times that

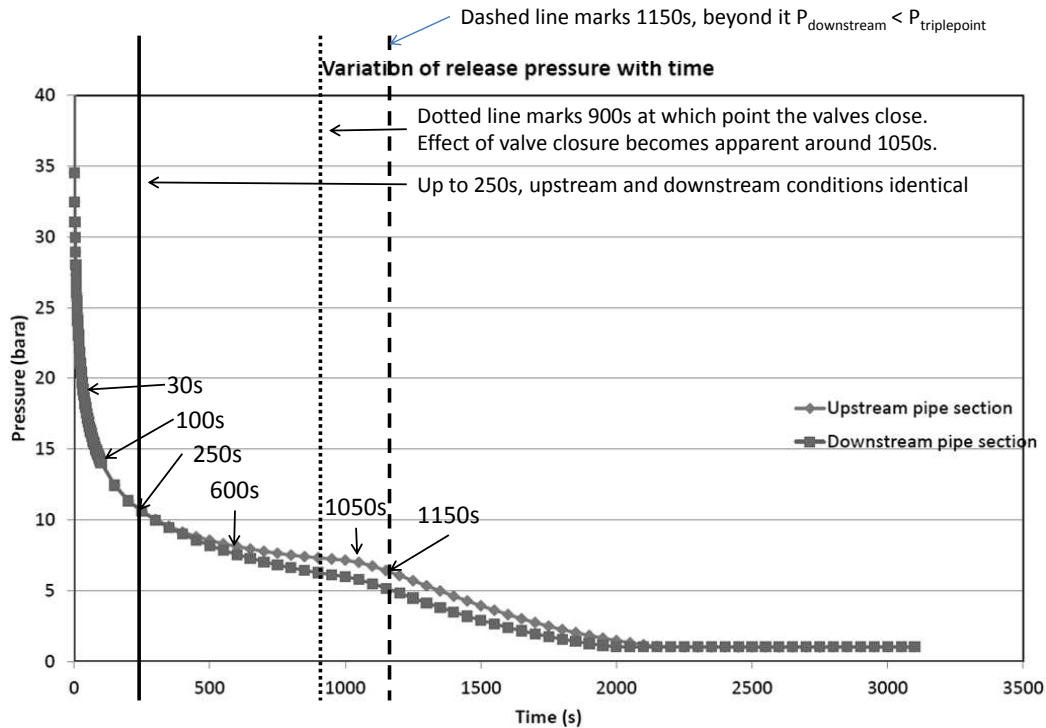


Figure 1: Prediction of the variation of the inflow pressure with time in the base case (Mahgerefteh, private communication) and the points chosen for snapshot simulations.

247 represent or bracket points of interest in the decompression, as is frequently
 248 done in performing such pipeline risk assessments. Further, enough snapshots
 249 had to be modelled such that a reconstructed extrapolated flux for the entire
 250 duration would represent the smooth variation of the flow, to be presented in
 251 a future publication. In discussion with DNV GL through the COOLTRANS
 252 research programme, these snapshots were specified at $t = 30$ s, 100 s, 250 s,
 253 600 s, 1000 s and 1150 s for the base case. Complete prescriptions of the inlet
 254 boundary conditions at these times at the upstream and downstream pipe in-
 255 lets into the crater are shown in Table 1. The snapshots at 30, 100 and 250 s

256 cover the duration of the decompression where the upstream and downstream
257 pipeline inlet conditions are identical - they are ‘balanced’. Given the range
258 of pressures (and hence saturated temperatures), these three snapshots were
259 chosen to cover the initial high pressure, high mass-flow period. Although
260 the pressures were higher earlier than 30 s, it was concluded that the first
261 seconds of the rupture may be heavily affected by the clearance of overlying
262 soil and the formation of the crater, so no earlier snapshots were computed.
263 The snapshots at 1000s and 1150s were chosen in order to bracket the time
264 at which the valve closure has an effect on the flow into the crater, shown
265 in Figure 1. A final snapshot at 600 s was chosen in order to characterise
266 the period of unbalanced flow (where the upstream and downstream inlet
267 conditions differ) before the effect of the valve closure became apparent on
268 the inlet conditions. Beyond 1150s, the downstream pipe inflow rate drops
269 below the triple point. Given that the flow rates have decreased considerably
270 compared to their initial values in the first 10 s of the rupture and questions
271 arise over the multiphase flow behaviour below the triple point, we do not
272 to model any snapshots beyond 1150 s at this time. The impact of these
273 assumptions is discussed in Section 6.

274 *3.3. Crater geometry*

275 The geometry of the crater is illustrated in Figure 2. It is assumed that
276 the crater is shaped like a ‘bath tub’, with a horizontal rectangular section
277 at its base of length L and width W . The length of the flat section is
278 assumed to be equal to the fracture length of a complete single section and its
279 width is assumed to be equal to the circumference of the pipeline, centered
280 on the original position of the pipeline, as if a section of the pipeline has

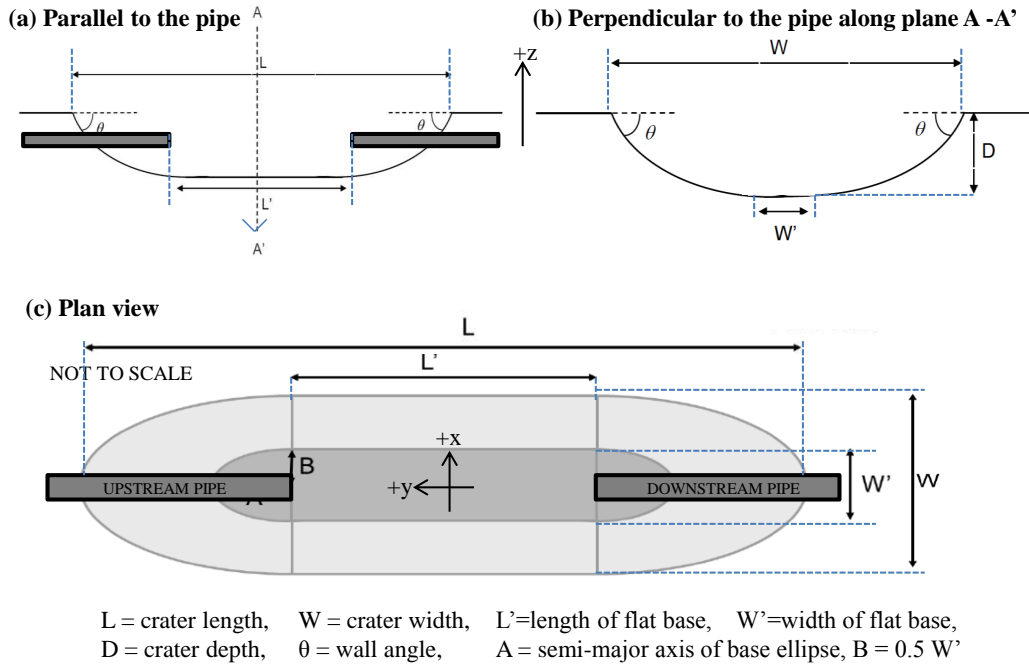


Figure 2: Details of the crater used in the full-scale rupture simulations (Cleverly, private communication).

281 unzipped and then unrolled, leaving the neighbouring sections in tact. The
 282 flat base is at the maximum crater depth, D . The dimensions of the crater
 283 have been estimated using the DNV GL COOLTRANS crater formation
 284 predictive model, based on real craters generated in incidents. The values
 285 that have been obtained are given in Table 2 for the base-case rupture As
 286 a first order modelling scenario, this represents the worst case failure of a
 287 pipeline reasonably well. Other failure scenarios will result in lower, less
 288 collimated, flow rates.

289 *3.4. Numerical mesh and initial domain conditions*

290 In computationally simulating this crater release, a three-dimensional
291 Cartesian coordinate grid mesh has been employed. The inlet conditions
292 at the upstream and downstream inlet pipes in the crater, as shown in Table
293 1, are enforced on every timestep of the simulation. The initial state of the
294 fluid in the rest of the domain consists entirely of stationary air at atmo-
295 spheric pressure and a temperature of 283 K. The surface of the crater has
296 been defined using ellipses. The two ends of the flat base are flat ellipses.
297 The method for joining the flat section of the crater to the crater rim in a
298 smooth manner is based on ellipses calculated from the dimensions and wall
299 angle of the crater, ensuring a smooth change of depth and a constant crater
300 wall angle perpendicular to the pipeline at all positions along the rim. Below
301 this ‘surface’, in the ground, no numerical integration is carried out and the
302 ground is considered solid.

303 Symmetry boundaries were used where possible in these simulations.
304 Specifically, as the inlet pipe flows are balanced for the 30 s, 100 s and 250
305 s snapshots as indicated by the overlapping upstream and downstream pre-
306 dictions in Figure 1, two symmetry boundaries were used in order to reduce
307 the computational effort and achieve steady state with minimum execution
308 time. The symmetry boundaries were imposed vertically at $x = 0$ m, parallel
309 to the pipeline through the centre of the pipeline, and vertically at $y = 0$
310 m, perpendicular to the pipeline through the centre of the crater. A quarter
311 crater was hence simulated on the domain (x, y, z) (0, 0, -3.5) m to (15, 10,
312 11.5) m. The single pipeline inlet is semi-circular in this domain and located
313 on the x - z plane at $y = 6$ m, with the centre located at (0, 6, -1.2), with a

314 radius of 0.3 m. A solid pipeline was modelled for $y > 6$ m. For the 600 s,
315 1000 s and 1150 s snapshots, where the upstream and downstream predic-
316 tions do not overlap in Figure 1, only a single symmetry boundary was used
317 as the inlet pipe flows are unbalanced, specifically at the $x = 0$ m bound-
318 ary parallel to the pipeline and through its centre. A half crater was hence
319 simulated on the domain (x, y, z) (0, -10, -3.5) m to (15, 10, 11.5) m. The
320 upstream and downstream pipeline inlets are semi-circular in this domain
321 and located on x - z planes at constant y . The upstream inlet is at $y = 6$ m
322 with the centre of circle located at (0, 6, -1.2), and a radius in x - z plane of
323 0.3 m. The downstream inlet is at $y = -6$ m with the centre located at (0,
324 -6, -1.2), and a radius in x - z plane of 0.3 m. Solid pipelines were modelled
325 for $y > 6$ m and $y < -6$ m. The remaining boundaries were set to free-flow,
326 only allowing the in-flow of air with the initial atmospheric condition when
327 in-flow was detected e.g. air dragged in from behind the pipe inlets. In all
328 cases, the coarsest grid cell size (on AMR level 0) was $0.5 \times 0.5 \times 0.5$ m. The
329 finest grid cell size (on the AMR level 4) was 3.125×10^{-2} m on a side. This
330 is equivalent to a fixed grid resolution of $480 \times 480 \times 320$ cells for the quarter
331 crater simulations and equivalent to a fixed grid resolution of $480 \times 480 \times 640$
332 cells for the half crater simulations.

333 As symmetry axes were used, cross-winds were not modelled in the cases
334 presented here. Four test simulations were performed to establish the validity
335 of this approach, considering a quarter-crater (with two symmetry axes), a
336 half-crater (with one symmetry axis along the pipeline), a full crater (with
337 no symmetries) but with still air and finally a full crater with a cross-wind
338 of 2 m s^{-1} . A comparison of the results showed that at the crater rim or

339 just above it, the flow out of the crater is fast enough (on the order of 100
340 m s^{-1}) not to be affected by the cross-wind and hence it has been ignored
341 in these near-field simulations. Further, the possibility of reentrainment of
342 a cooled CO_2 and air mixture, rather than just ambient air, has not been
343 considered, as to do this accurately would require a coupled near and far-
344 field computation, beyond the immediate capability of this model. These
345 assumptions and limitations are discussed in the penultimate section of this
346 article, Section 6.

347 *3.5. Sensitivity studies*

348 The sensitivity studies consider variations of crater size and shape only,
349 keeping the pipe inlet conditions the same as in the base-case rupture. De-
350 tails of the sensitivity study variations are specified in Table 2. Numerical
351 domains were extended by increasing numbers of cells as necessitated by the
352 variation of crater size, but the base resolution as above was kept constant. A
353 single snapshot (at $t = 250$ s) is simulated for each study, unless unexpected
354 behaviour or features become apparent, or there is specific industrial interest
355 in the case, detailed later.

356 *3.6. Integrated fluxes*

357 During establishment of a steady-state flow in the near-field, fluxes are
358 monitored through a horizontal plane in the simulation, either at or just
359 above ground level depending on how far the shock expansion zone protrudes
360 out of the crater above ground level. The CO_2 mass flow, or flux, into
361 the simulation domain from the upstream and downstream pipeline inlets
362 is defined in the initial condition and it is to this total input CO_2 mass

363 flux that the CO₂ mass flux through the plane is compared. The mass flux
364 is calculated by integration of the mass flowing through this plane, for the
365 total mass, CO₂ mass and solid CO₂ mass. Momentum flux is calculated
366 by a similar integration for the total momentum, CO₂ momentum and solid
367 CO₂ momentum. Simple velocities are inferred by dividing the integrated
368 momentum by the integrated mass.

369 *3.7. Particle deposition*

370 In order to estimate particle deposition in the crater, a Lagrangian par-
371 ticle tracking method has been one-way coupled to the fluid-flow model and
372 used to inject and track the movement of particles through the crater. This
373 method has been proved successful in modelling particle behaviour in below-
374 ground pipeline puncture modelling (Wareing et al., 2014b) and also in small-
375 scale laboratory releases (Wareing et al., 2013b, 2015b). As this previous
376 work has shown that the CO₂ particles are in equilibrium with the flow for
377 large-scale releases they are injected in the inlet region with the same ini-
378 tial velocity vector magnitude and direction as the CO₂ fluid. They have
379 a radius of 2×10^{-6} m and are given a density appropriate to solid phase
380 CO₂ at the sublimation temperature, based on properties measured in our
381 recent laboratory scale experiments (Wareing et al., 2013b). The movement
382 of the particles is then computed, including drag effects, through a one-way
383 coupling where the fluid influences the particles and not vice versa, until the
384 particles begin to leave the simulation domain. Any particles that have hit
385 the crater walls and stuck there are assumed to have been deposited in the
386 crater and counted. This number is converted to a percentage of the original
387 number of particles inserted into the flow and then scaled to the solid mass

388 flux into the crater post Mach shock in order to obtain a rate of solid CO₂
389 mass deposition into the crater.

390 4. Numerical results for the base-case rupture

391 In this section, Figures 3 to 9 are either shown on vertical or horizontal
392 planes through the numerical domain. Specifically, the vertical y - z plane
393 is always through the centre of the crater at the midpoint of the pipeline
394 rupture, parallel to the initial velocity vectors and the $x = 0$ m boundary.
395 The position of the horizontal x - y plane varies in z from $z = 0$ m (ground-
396 level) to $z = 2$ m. Each figure shows (a) temperature, (b) CO₂ fraction, (c)
397 solid CO₂ fraction, (d) velocity and (e) density.

398 4.1. Simulated flow 30 seconds after rupture

399 Figure 3 shows the predicted steady state flow on the vertical plane at
400 $t = 30$ s. The expansion zone as the CO₂ exits the pipeline is clearly visible
401 in temperature, velocity and density. In this region, the lowest temperatures
402 are reached, passing below the triple point and freezing the remaining liquid
403 CO₂ into the solid phase. Just before the Mach shock at the termination of
404 this zone, the highest velocities and lowest pressures are reached. Beyond the
405 Mach shock, the temperature is at the sublimation temperature as both solid
406 and gas phase CO₂ are present, enforced by the homogeneous equilibrium
407 model for pure CO₂. The overall fluid (CO₂ and air) temperature drops
408 slowly as air is mixed into the jet and the plume exits the crater. The solid
409 fraction just beyond the Mach shock is around 0.35 and this only begins to
410 drop outside the crater, indicating sublimation only begins to occur as the
411 jet leaves the crater. The core and sheath nature of the sonic jet is clear

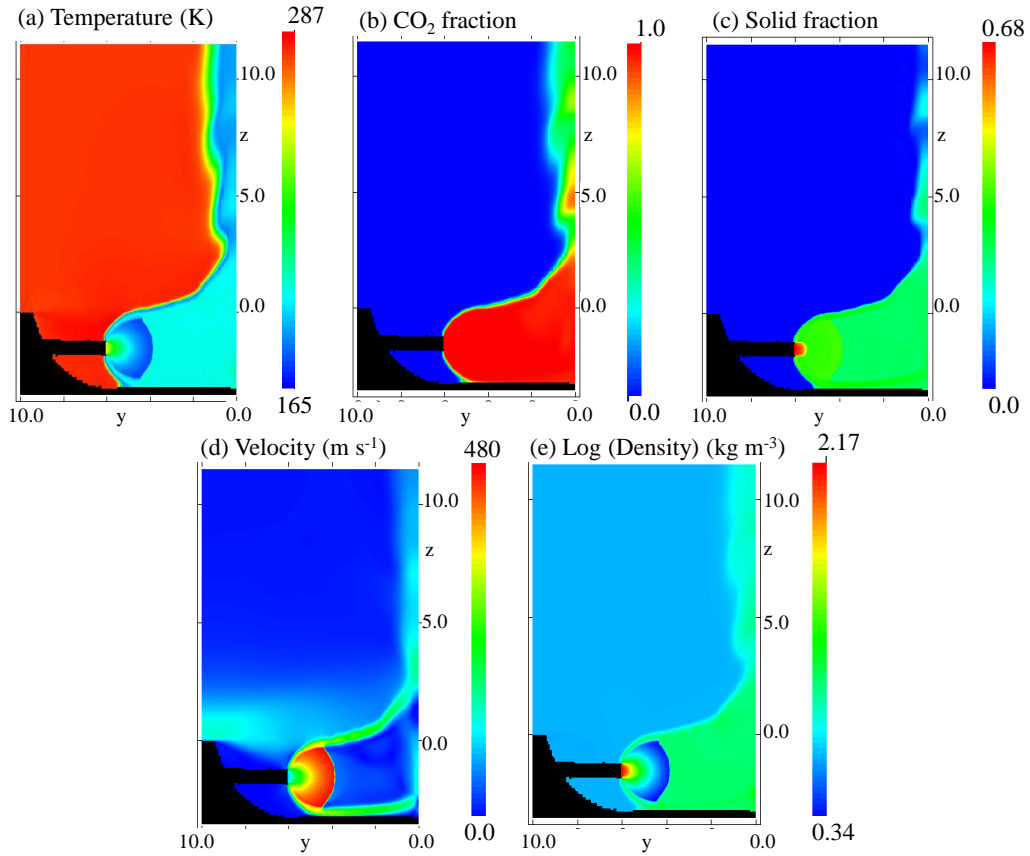


Figure 3: Vertical plane through the crater at $t=30$ s.

412 in the plot of velocity, where the vertical slice shows the slow moving core
 413 surrounded by the fast moving sheath. On interaction with the oncoming
 414 jet at the $y = 0$ m symmetry boundary, the flow is diverted upwards, but
 415 also spreads out perpendicular to the pipeline axis. This spreading lateral
 416 flow then runs up the crater walls and leaves the crater inclined at the crater
 417 wall angle. The velocity plot shows that as expected air is entrained into the
 418 crater from behind the pipeline inlets at a rate of a few tens of metres per
 419 second.

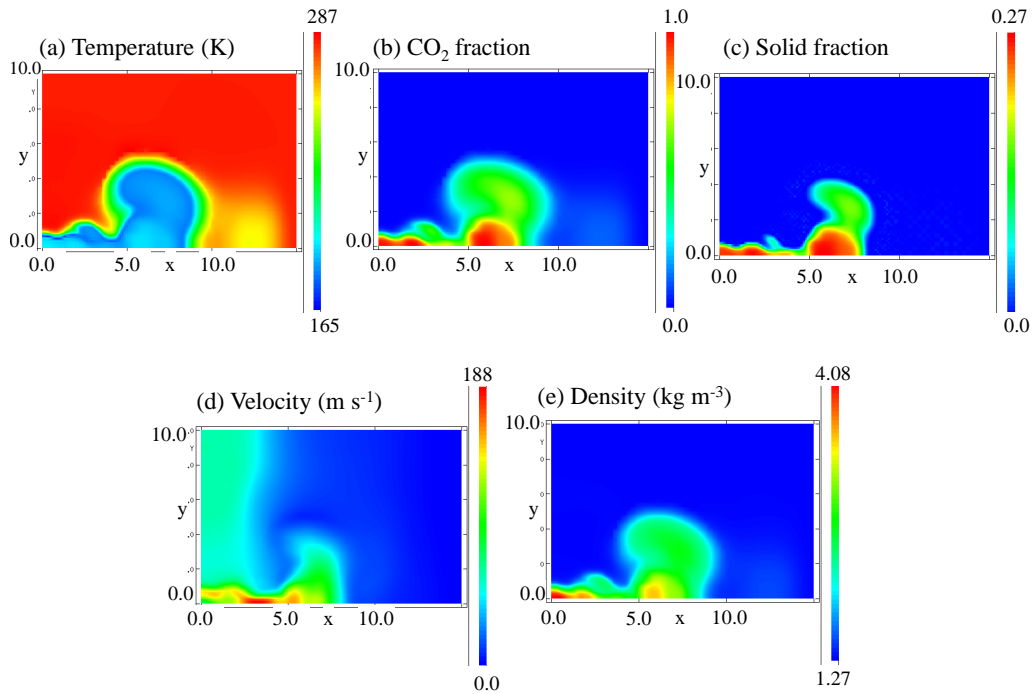


Figure 4: Horizontal plane 2 m above the crater at $t=30$ s.

420 Figure 4 shows the flow on the horizontal plane 2m above the crater.
 421 This is the lowest height at which the horizontal plane does not intersect the
 422 near-field expansion zone terminated by the Mach shock and the associated
 423 high-velocity jet structure and hence is the lowest plane at which data can
 424 be passed to a far-field simulation. The highest densities and CO_2 fractions
 425 are in a jet directed upwards in the centre of the crater (at the origin (0,0)
 426 of the numerical grid) and in the lateral spread of the flow turned upwards
 427 by interaction with the crater at $x = 5$ m to $x = 7$ m on the x axis. The
 428 peak velocities are between these two regions, but this region is less dense
 429 and hence carries less momentum. The jet still contains up to approximately
 430 25% solid CO_2 at this height and hence the temperature in this equilibrium

431 model is below the sublimation temperature in CO₂ and air mixture. Whilst
 432 the peak velocity is up to 188 m s⁻¹, the average velocity is less than half
 433 this. Integrated mass and momentum fluxes on this plane are shown in Table
 434 3.

435 *4.2. Simulated flow 100 seconds after rupture*

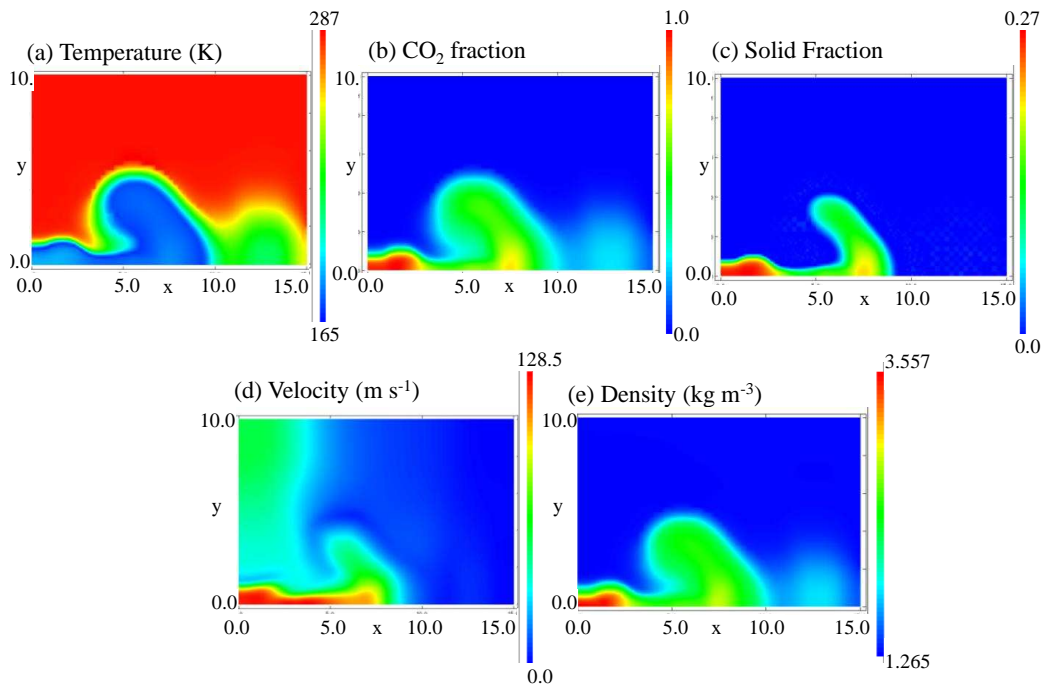


Figure 5: Horizontal plane 2 m above the crater at t=100 s.

436 In this case, the expansion zone is smaller (as the pressure at the pipe
 437 inlet is lower). Compared to the steady-state flow at $t = 30$ s, the structure is
 438 somewhat smoother and more collimated into a fan shape out of the centre
 439 of the crater perpendicular to the pipeline. Figure 5 shows the flow on a
 440 horizontal plane 2m above the crater. Even though the inlet pressure is lower,

441 this is still the lowest height at which the horizontal plane does not intersect
442 the near-field expansion zone terminated by the Mach shock and associated
443 high-velocity jet structure, and hence is the lowest plane at which data can
444 be passed to a far-field simulation. The highest densities, CO₂ fractions
445 and highest velocities are in the fan perpendicular to the pipeline directed
446 upwards in the centre of the crater (at the origin (0,0,0) of the numerical
447 grid), laterally spreading along the x axis. The cloud expanding towards
448 positive y away from the x -axis in Figure 5 at around $x = 7.5$ is a result
449 of the flow from the interacting jets in the centre of the crater running up
450 the crater wall below this plane and then spreading upwards and backwards
451 toward the pipeline. The integrated upwards mass and momentum fluxes on
452 this plane are shown in Table 3.

453 *4.3. Simulated flow 250 seconds after rupture*

454 The expansion zone is smaller than at $t = 100$ s due to the lower inlet
455 pressure. Compared to the flow at $t = 100$ s, the width of the jet in the
456 crater and the resulting upwards plume are smaller and carrying less CO₂,
457 although the solid fraction is still the same. The velocities in the jet are on
458 an identical range to those noted in the earlier base-case rupture snapshots.
459 The expansion zone at the end of the pipe is now almost entirely below the
460 ground level. The structure of the flow on a plane 1m above the crater, as
461 this is now the lowest plane that can be considered without interference from
462 the near-field expansion zone, is quantitatively and qualitatively similar to
463 that at $t = 100$ s. The highest densities and CO₂ fractions are now in an oval
464 cold plume moving directly upwards (toward positive z) from the centre of
465 the crater at around at 80 to 100 m s⁻¹. The integrated upwards mass and

466 momentum fluxes on this plane are shown in Table 3.

467 *4.4. Simulated flow 600 seconds after rupture*

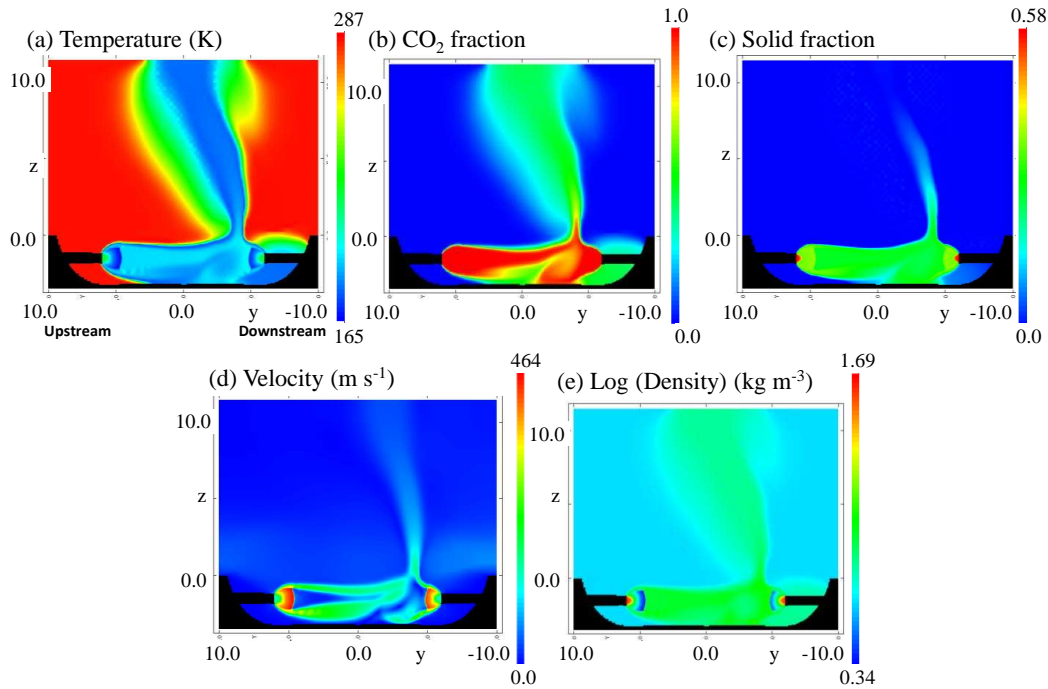


Figure 6: Vertical plane through the crater at $t=600$ s.

468 Figure 6 shows the predicted steady state flow at $t = 600$ s on the vertical
469 slice described previously. The flows out of the pipes into the crater are now
470 unbalanced i.e. the upstream and downstream inlet conditions are different
471 and the predictions no longer overlap in Figure 1. The higher pressure of the
472 upstream inlet flow has pushed the exit plume over toward the lower pressure
473 downstream inflow. Compared to previous snapshots, as expected with lower
474 inlet pressures, the expansion zones are now smaller. The fraction of CO_2 in
475 the solid phase is still the same at the crater rim.

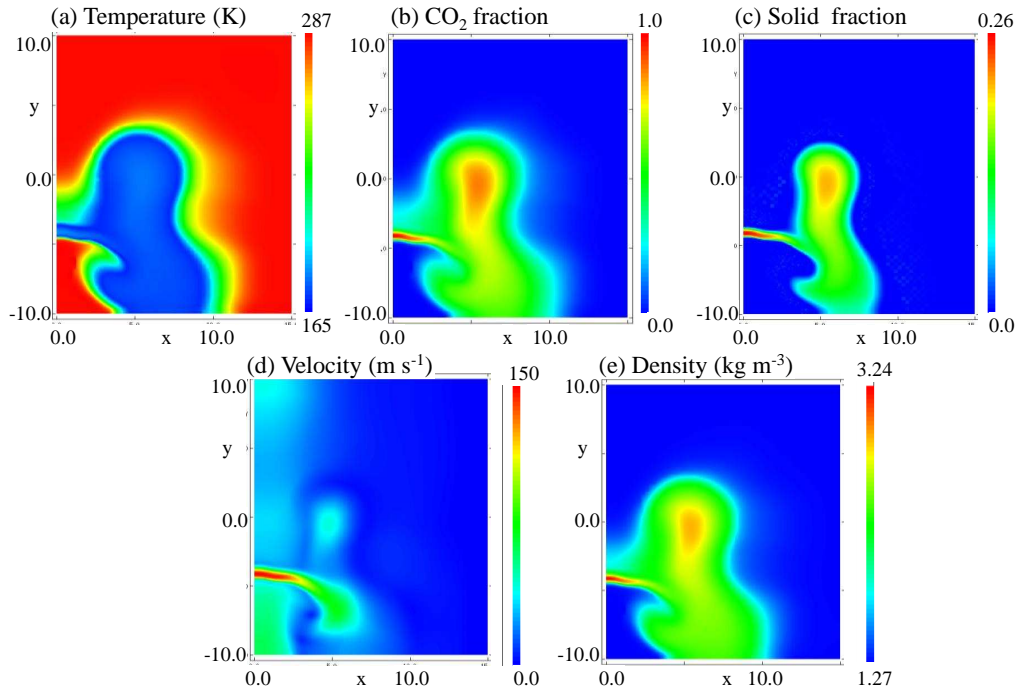


Figure 7: Horizontal plane 1 m above the crater at $t=600$ s.

476 Figure 7 shows the flow on a horizontal plane 1m above the crater. This is
 477 the lowest height at which the horizontal plane does not intersect the near-
 478 field expansion zone terminated by the Mach shock and associated high-
 479 velocity jet structure and hence is the lowest plane at which data can be
 480 passed to a far-field simulation. The flow out of the crater is in the form of a
 481 thin fan directed upwards from the interaction region, which in this steady-
 482 state snapshot is moved from the centre of the crater toward the downstream
 483 pipe. Compared to previous snapshots with balanced inlets, the flow out of
 484 the crater is still narrow in the centre of the crater above the pipeline axis,
 485 but widened by the crater walls and unbalanced inlets toward positive x . It
 486 should be noted that this simulation, with only one plane of symmetry at

487 $x = 0$ m, shows the same fan jet structure emerging from the crater as the
 488 previous three snapshots, albeit shifted toward the downstream pipe. The
 489 integrated upwards mass and momentum fluxes on this plane are shown in
 490 Table 3.

491 *4.5. Simulated flow 1000 seconds after rupture*

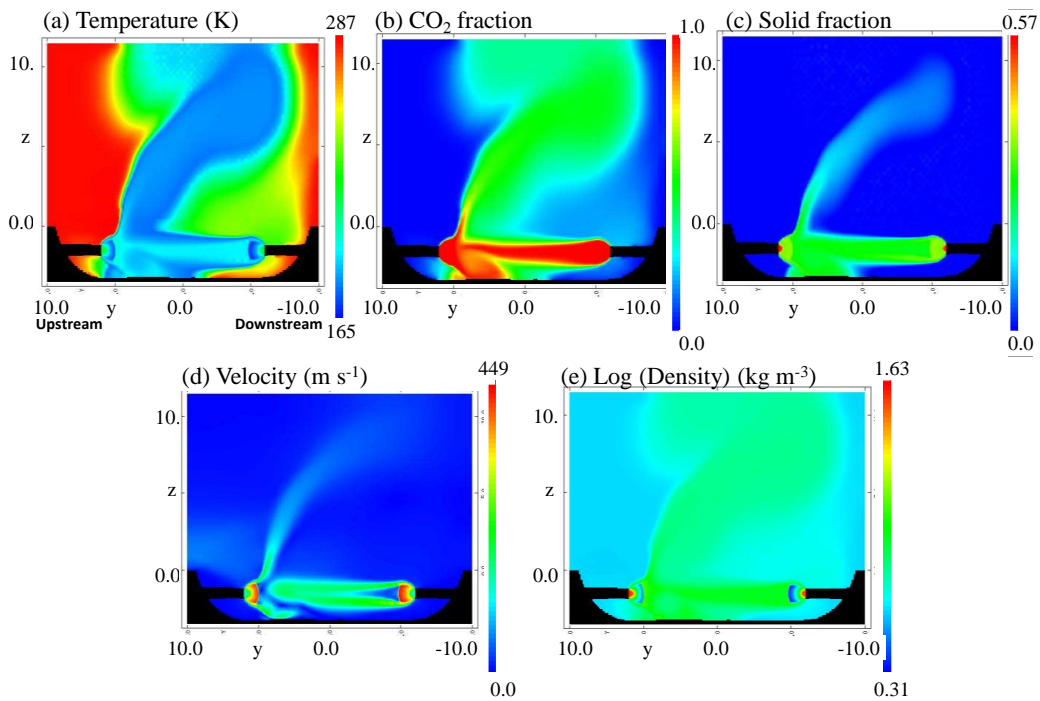


Figure 8: Vertical plane through the crater at $t=1000$ s.

492 Figure 8 shows the predicted steady state flow at $t = 1000$ s. The up-
 493 stream and downstream pipe flows into the crater are unbalanced and the
 494 fan jet leaving the crater is now close to the upstream Mach shock. The
 495 velocity plot shows the downstream jet remains fairly collimated across the
 496 whole crater. The lower pressure at the downstream pipe inlet results in a

497 smaller diameter Mach shock and a smaller jet diameter post-Mach-shock.
498 It is apparent that the jet from the downstream inlet has been able to split
499 the upstream jet. Whilst it is possible that this result is a numerical issue,
500 this is unlikely given the behaviour observed in the sensitivity studies and at
501 other times, where stable jets form and the location of the stagnation point is
502 stable. It is also possible to speculate whether this effect should have shown
503 up at earlier simulation times but for the use of symmetry planes. The cross-
504 wind tests using quarter, half and full craters have shown no movement of
505 the stagnation point. The simulation has also been advanced in time to ex-
506 amine whether the near-field has not yet reached structural steady-state. No
507 shift away from the current position was observed. The CO₂ fraction is lower
508 in the plume, rapidly dropping to 50% by a few metres above the crater,
509 although the fraction of CO₂ in the solid phase is on the same order as all
510 previous snapshots.

511 Figure 9 shows the flow on a horizontal plane 1m above the crater. This
512 is the lowest height at which the horizontal plane does not intersect the
513 near-field expansion zone terminated by the Mach shock and associated high-
514 velocity jet structure and hence is the lowest plane at which data could be
515 passed to a far-field simulation. The flow out of the crater is in the form of a
516 thin fan directed upwards from the interaction region, which in this snapshot
517 is moved toward the upstream pipe and bent toward the downstream pipe as
518 a result of the air inflow into the crater behind that pipe which is forcing the
519 upwards plume fan to bend over toward the downstream pipe. It is worth
520 noting that the upwards flow is still vertical and unaffected by the air inflow
521 for the first few metres. As the air is flowing into the crater at velocities

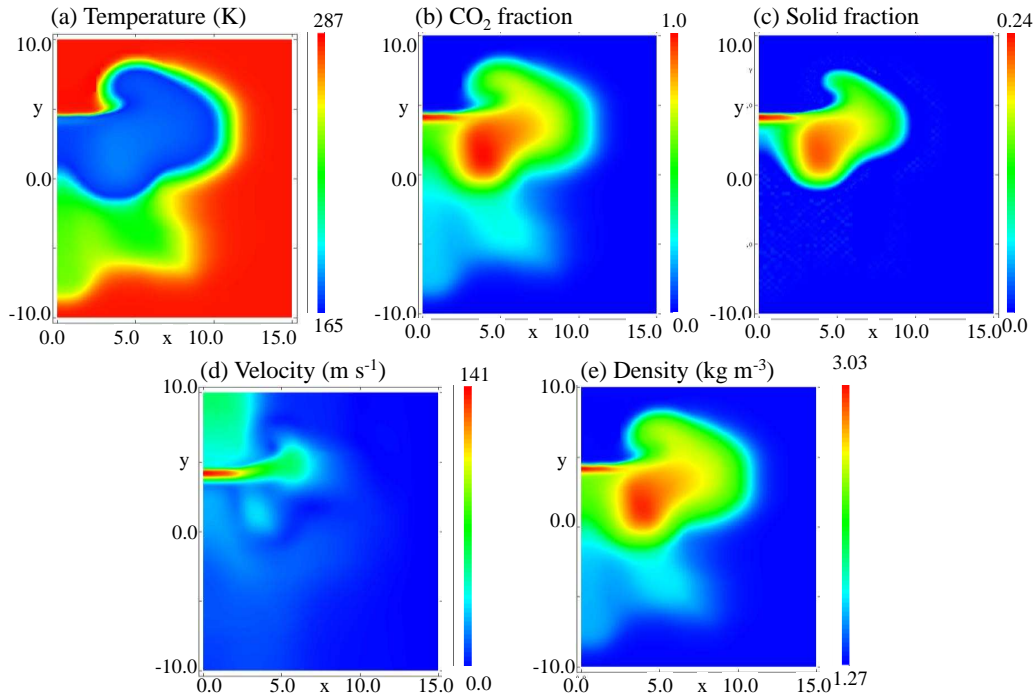


Figure 9: Horizontal plane 1 m above the crater at $t=1000$ s.

522 on the order of tens of metres per second, this further supports the previous
 523 tests that show cross-winds of a few metres per second do not affect the
 524 initial vertical flow out of the crater, and hence the use of symmetry planes
 525 is justified. The integrated mass and momentum fluxes on this plane are
 526 shown in Table 3.

527 4.6. Simulated flow 1150 seconds after rupture

528 The upstream and downstream inlet conditions remain unbalanced. As
 529 in the previous snapshot at $t = 1000$ s, the downstream jet has pushed the
 530 interaction region back to the Mach shock of the upstream crater inlet, with
 531 the upwards plume close to the upstream Mach shock. The balance is still
 532 towards the momentum of the downstream jet with a smaller cross-sectional

533 area. The flow on a plane above the crater is very similar to that predicted
534 at $t = 1000$ s, in the form of a thin fan directed upwards from the interaction
535 region in the crater, with lateral spreading from material flowing up the crater
536 wall. The integrated mass and momentum fluxes on this plane are shown in
537 Table 3.

538 *4.7. Particle deposition*

539 Figure 10 shows the particle locations after the particles have been allowed
540 to evolve through the flow until one or more have left the computational
541 domain. In the first three snapshots (panels (a), (b) and (c)), at times when
542 the flow from the upstream and downstream pipelines is balanced, we find no
543 particles embed into the crater walls and hence no solid is deposited into the
544 crater. At $t = 600$ s, 1.5% of the particles introduced have been deposited
545 into the crater walls, primarily through the flow coming from downstream
546 inlet pipe flow split by the upstream flow. At $t = 1000$ s, 1% of the particles
547 introduced have been deflected into the base of the crater, this time near the
548 upstream pipe rupture; the same occurs at $t = 1150$ s.

549 An important question in the quantified risk assessment of this rupture
550 scenario is how much solid is deposited in the crater. We now consider two
551 particle deposition scenarios. First, the more extreme case, where we average
552 across the entire duration of the release and estimate that approximately 1%
553 of particles released during a full-scale pipeline rupture end up embedded
554 in the base of the crater. Based on this, a total of 14,000 kg of solid CO₂
555 could be deposited over the 1150s before the pressure at the downstream
556 rupture reaches the triple point. This is equivalent to 10 cubic metres of
557 solid CO₂ spread around the base of the crater. covering the base to a

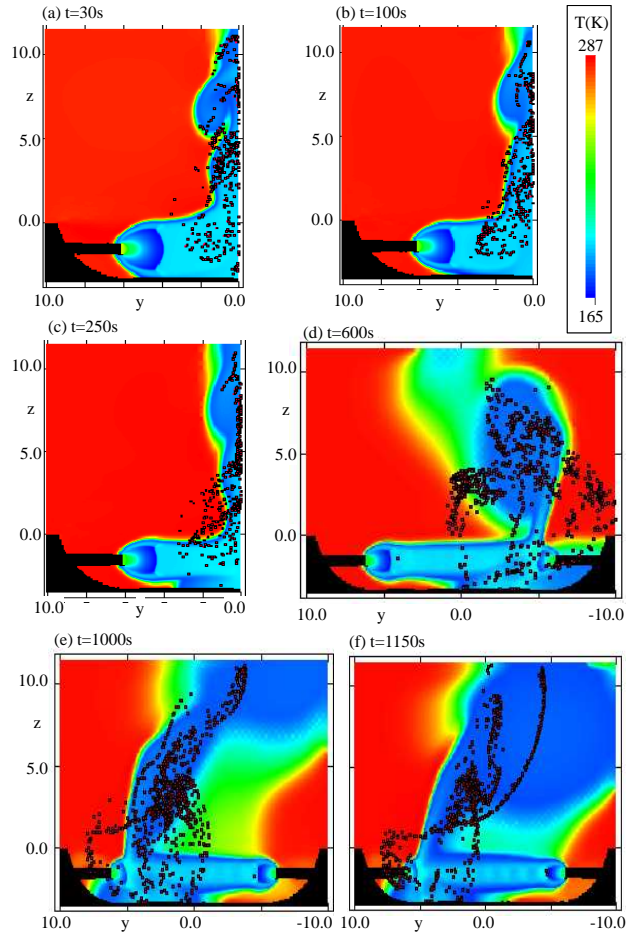


Figure 10: Vertical planes through each of the base-case snapshots with particles. Panels (a), (b) and (c) only show half the slice through the crater as they were quarter crater simulations. Onto each plane are collapsed all the locations of the particles in the entire three-dimensional simulation, marked by red squares. Particles considered to be deposited in the walls are shown as the red squares inside the black solid walls.

558 depth of approximately 0.4m. Secondly, we assume that whilst the pipeflows
 559 are balanced up to 250 s, there is no particle deposition in the crater. An
 560 integration from 250 s to 1150 s reveals that approximately 8500 kg of solid

561 CO₂ could be deposited in that time - 40% less than in the first scenario.

562 **5. Sensitivity studies**

563 For reference, details of the sensitivity studies are summarised in Table 2.
564 Unless specifically detailed, the initial conditions were identical to the base
565 case.

566 *5.1. Sensitivity study 1 - a longer fracture*

567 In the first sensitivity study (S1), the pipeline fracture length is doubled
568 to 24m and the crater size changed according to Table 2. The motivation for
569 this study is to examine the consequences of constructing the pipeline from 24
570 m sections, rather than 12 m in the base case. All six equivalent snapshots of
571 the flow have been simulated in this case. The integrated upwards mass and
572 momentum fluxes are presented in Table 4. The effect of changing fracture
573 length appears to smooth and balance the flow from the centre of the crater,
574 and leading to lower CO₂ and solid CO₂ fractions in the plume out of the
575 crater. The effect on the flow out of the crater compared to the base case
576 is due to the greater distance between the upstream and downstream pipes,
577 which gives a greater distance before the two jets interact, which in turn
578 results in a more collimated flow out of the crater.

579 As a result, the plume out of the crater has a very similar shape and
580 position in the centre of the crater at all six times considered. The flow on
581 a horizontal plane above the crater is shown in Figure 11(b). The upwards
582 flow is very symmetric with a thin fan perpendicular to the pipeline in the
583 centre of the crater at all times, with lateral spreading of the cloud caused by
584 interaction with the crater wall as the flow moves outward from the pipeline

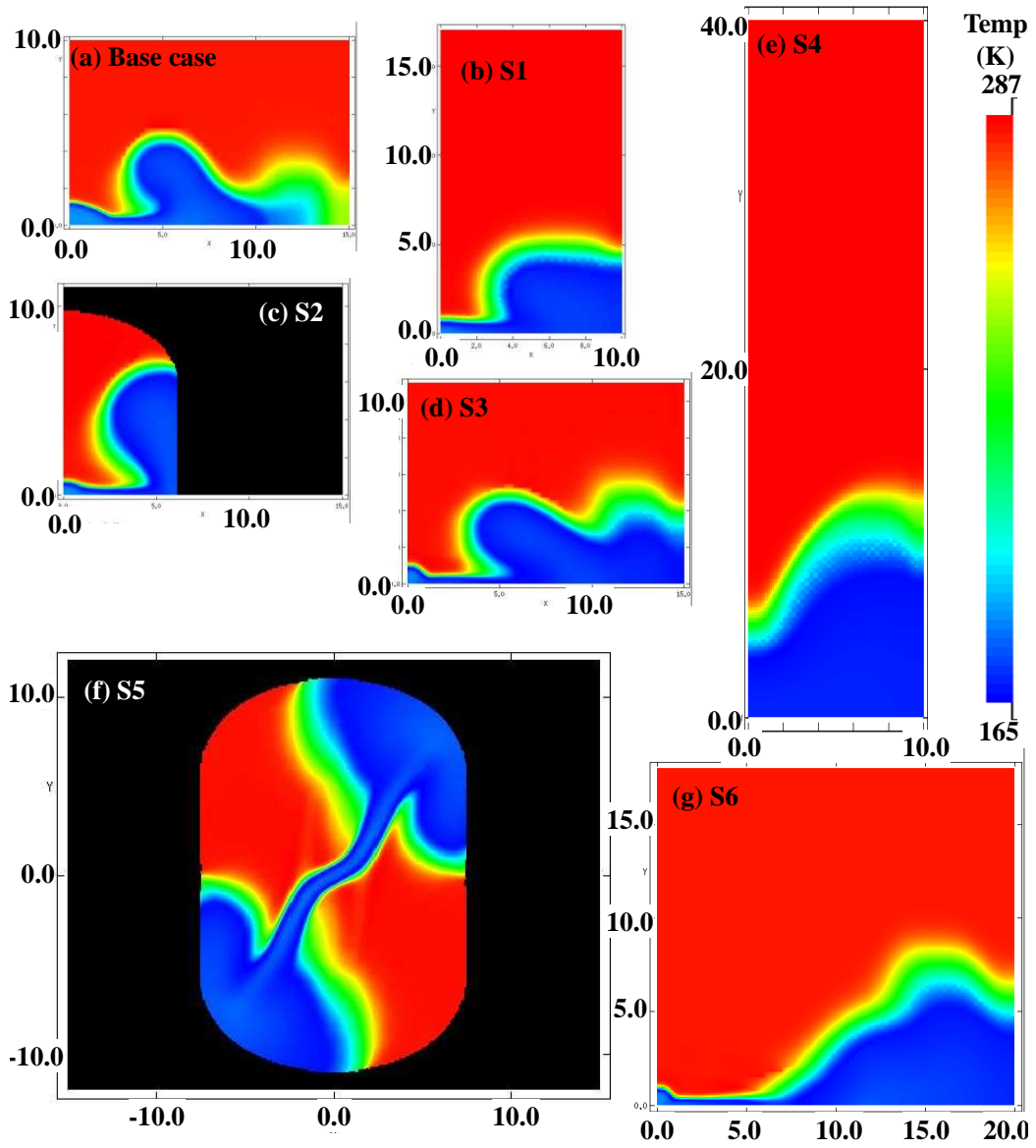


Figure 11: Steady-state flow on horizontal planes above the crater comparing the base case (a) and the six sensitivity studies (b-g) at 250 s after the rupture.

585 axis at the centre of the crater. At later time the flow was not shifted
586 toward either upstream or downstream inlet pipe. The integrated fluxes are
587 presented in Table 4. At early times, the integrated flow is very similar to
588 that of the equivalent time base case snapshots. At later times, CO₂ fraction
589 and solid fraction linearly decrease, rather than remain constant as in the
590 base case.

591 *5.2. Sensitivity study 2 - a deeper pipeline*

592 In this second sensitivity study (S2), the depth of cover of the pipe is
593 increased from having 1.2 m of soil cover to 2 m of soil cover and the crater
594 depth changed according to Table 2. The motivation for this study is to
595 examine the consequences of a deeper amount of soil cover, as the level of
596 cover is expected to vary along a pipeline as it encounters local geography.
597 A single snapshot at $t = 250$ s was considered for comparison to the base
598 case. The integrated flux on a plane above the crater is presented in Table
599 5. The effect on the flow out of the crater is minimal. The flow is smooth
600 and has the same structure as the base case snapshot at 250 s, as shown in
601 Figure 11.

602 *5.3. Sensitivity study 3 - a shallower crater*

603 In the third sensitivity study (S3), reducing the crater wall angle is con-
604 sidered - generating a shallower walled crater as detailed in Table 2. The
605 motivation for this study is to examine possible consequences of different soil
606 cover varieties. A single snapshot at $t = 250$ s was simulated for comparison
607 to the base case. The crater wall angle θ was decreased from 75° to 64°. The
608 effect of changing crater wall angle appears only to increase the width of the

609 cloud, allowing for more lateral spreading, as shown in Figure 11, but this is
610 not where the majority of the mass-flux and momentum is located and hence
611 the effect on the plume is minimal. The integrated fluxes are presented in
612 Table 5. The CO₂ fraction and solid fraction are slightly less than the $t = 250$
613 s results for the base case. Velocity and temperature are very similar to the
614 base case.

615 *5.4. Sensitivity study 4 - a 72 m fracture*

616 In the fourth sensitivity study (S4), modelling of a large crater is per-
617 formed, detailed in Table 2. The motivation for this study is to examine the
618 consequences of an unarrested pipeline crack creating a 72 m fracture length
619 (L') and associated elongated crater. As this is a considerably different sce-
620 nario to the base case, all six snapshots of the flow have been simulated in
621 this case. The flow is considerably different, as shown in Figure 11 and in
622 order to establish integrated profiles, slices are higher above the crater than
623 for the base case. The effect is to reduce the CO₂ fraction going upwards
624 in the plume and considerably reduce the solid fraction. Velocities are also
625 lower, as detailed in Table 6. The effect of the extended fracture length is
626 to allow the flow out of each pipe to have a considerable distance to expand
627 and to deflect off the crater base (approximately 36m, rather than 6m in the
628 base case) before meeting in the interaction region in the centre of the crater.
629 Hence much more air is mixed in and CO₂ levels are lower with less solid
630 present. In order to find a plane above the crater that is above this interac-
631 tion region, it has to be considerably higher than in the base case. On this
632 plane, the plume out of the crater is moving predominantly straight upwards.
633 As the time increases, the CO₂ fraction decreases, the solid fraction decreases

634 and the velocity drops on this plane, as shown in the integrated mass and
635 momentum fluxes in Table 6. The net result is a slower, less concentrated,
636 wider but more collimated flow compared to the base case, as shown in Figure
637 11.

638 5.5. Sensitivity study 5 - misaligned pipes

639 In this sensitivity study (S5), modelling the effect of upstream and down-
640 stream pipe inlet misalignment on the flow out of the crater is considered.
641 The misalignment considered, 10° outwards in the horizontal plane, with the
642 ‘anchor’ point for the pipeline coincident with the crater edge, is an *extreme*
643 case in order to bracket potential real world scenarios. These simulations re-
644 vealed considerable effects on the flow and all six snapshots of the flow have
645 been simulated in this case. The pipes were misaligned as above, the crater
646 length L was increased to 22 m and the width W to 14.9 m. The structure
647 of the flow is considerably different to the base case and the integrated pro-
648 files show larger fractions of CO_2 and larger solid fractions, but comparable
649 velocities and temperatures. Given the nature of the flow, an upwards flow
650 through a plane is of questionable validity here in representing this extreme
651 case. The general crater shape is not changed, although in reality the crater
652 shape will almost certainly be distorted away from the symmetric ‘bath-tub’
653 used throughout in this work. The interaction region between the two jets
654 is still in the centre of the crater, although it is now twisted and leads to
655 a upwards flow of CO_2 out of the crater as before, as well as a new flow
656 which consists of the jets from each pipe end partially deflecting off one an-
657 other, into the opposing crater wall, up the wall and then out of the crater.
658 The shape of the crater strongly affects these new deflected flows. With this

659 crater shape, the flow is deflected upwards out of the crater at the crater wall
660 angle, whilst also carrying momentum in the horizontal plane, resulting in a
661 ‘fountain’ over opposite edges of the crater, as well as the plume in the middle
662 of the crater, as shown in Figure 11. At early stages, the jets from each pipe
663 and the interaction region dominate, forming a complex plume, but moving
664 predominantly upwards with comparable CO₂ fractions and solid fractions
665 to previous sensitivity studies (as shown in Table 7). The jets do not de-
666 flect and there is minimal sideways flow perpendicular and away from the
667 pipeline. By $t = 250$ s into the release, the jets are narrow enough that
668 the major interaction consists of a deflection as the jets pass each other and
669 hence the flow out of the crater is dominated by the crater shape opposite
670 the pipe rupture as the jets hit the opposite walls (see Figure 11. As these
671 flows are complex, the integrated fluxes have been calculated at the crater
672 rim and are shown in Table 7.

673 *5.6. Sensitivity study 6 - sandy soil crater*

674 In this final sensitivity study (S6), the motivation is to study variation
675 in the type of soil cover. Instead of clay, this case considers sandy soil and
676 hence a much wider and longer crater with a shallower wall angle. A single
677 snapshot at $t = 250$ s is presented for comparison to the base case in Figure
678 11. The crater length L was increased to 33.9 m, the width W to 26.8 m and
679 the crater wall angle θ decreased to 40°, as detailed in Table 2. The effect
680 on the upwards plume in the centre of the crater is minimal, although the
681 lateral spreading of the plume at ground level is considerably widened by the
682 larger crater and shallower wall angle, as shown in Figure 11. As the depth
683 and fracture length remain the same, there is minimal effect of soil type on

684 the plume going upwards from the centre of the crater. This is the region of
685 the flow carrying the greatest amount of material at the highest velocities.
686 The key effect is as a result of the widening of the crater. The lateral spread
687 of the cloud from the central interaction region is less focussed around the
688 crater as the crater wall angle is considerably far less than previously which
689 means the flow more easily runs up and over the lip of the crater heading
690 perpendicularly away from the pipeline. The velocities in this lateral cloud
691 are very low though. The integrated fluxes presented in Table 5 show that
692 the CO₂ fraction and solid fraction are slightly less than those in the $t = 250$
693 s snapshot for the base case. Velocity and temperature are very similar to
694 the base case $t = 250$ s snapshot.

695 **6. Discussion**

696 The validation of the pipeline rupture model presented in Part I, and
697 comparisons to experimental data published elsewhere (Woolley et al., 2013;
698 Wareing et al., 2013b, 2014a,b), have shown that in general, this dispersion
699 model can predict the characteristics of high pressure releases of CO₂ from
700 reservoir conditions similar to those under consideration in the CCS industry,
701 including releases directly to air (as in venting operations), punctures and
702 ruptures of below-ground pipelines.

703 These predictions have required a complex equation of state which ac-
704 counts not only for accurate behaviour in the gas phase, but also, because of
705 the temperature range from the release point into the far-field, for accurate
706 behaviour in the liquid and solid phases and the transition to the solid phase.

707 The method used here has modelled steady-state snapshots at a number

708 of points in the decompression of the pipeline. Based on short dynamic and
709 thermal relaxation times, the short flow-crossing time of the near-field and
710 the slow variation of the ruptured pipe inlet conditions, the pipeline goes
711 through a sequence of steady-states during the decompression. The choice
712 of only examining a number of these, limited by the high computational ex-
713 penses of accurately modelling the near-field thermodynamics and ensuring
714 resolution of the near-field shock structures is therefore justified. However,
715 it should be noted that by taking such snapshots of the flow at instants in
716 time, the precludes any effect on the steady state snapshot in question of the
717 earlier evolution of the flow, theoretically minimal as it may be. Future soft-
718 ware and hardware developments may allow the investigation of a complete
719 depressurisation of a full-scale pipeline, with the necessary accuracy and re-
720 solve any questions over the transient nature of the dispersion flow and the
721 assumption that it has no ‘memory’.

722 Water vapour in the atmosphere will also affect the flow, but have limited
723 bearing on the true near-field. Predictions indicate that a free jet is entirely
724 CO₂ until approximately 40 release diameters downstream from the release
725 point. Any water vapour in the air cannot affect the core whilst it is 100%
726 CO₂, so it is unlikely to have an effect on the true near-field around the Mach
727 shock as that is always within 10 diameters of the release point. Given the
728 likely size of craters formed in pipeline ruptures, it is unlikely to strongly
729 affect the flow *in the crater* of a full-scale rupture. Once air does begin to
730 mix into the core, water ice will form in the low temperature environment
731 and since water has a latent heat of fusion greater than that of CO₂, it will
732 be an energy sink and the CO₂ jet itself will not be as cold as a consequence.

733 Also, the jet formed will be more buoyant. Water droplets condensed by the
734 cold jet will also define the visual extent of the jet. This is true throughout
735 the jet, but requires air to mix into the jet, which initially in the near-field
736 happens at very low levels. Following the interaction region in the crater,
737 water vapour condensing when the temperature drops below the dew point
738 will visually define the outer extent of the jet.

739 Re-entrainment of CO₂ back into a crater has been considered in two
740 ways. Taking far-field predictions, a mixture containing 15% CO₂ and 85%
741 air by mass was allowed to flow into the simulation domain in previous punc-
742 ture studies (Wareing et al., 2014b), at ambient temperatures and pressures
743 as predicted by the far-field simulation. This appeared to have no effect on
744 the crater outflow. In the second examination, a simplified two dimensional
745 simulation of a stalling plume was considered, as the full simulation is not
746 possible with a near-field model alone. The results have shown that plume
747 height is affected - it drops by one third as the cold cloud is re-entrained into
748 the flow. Further full far-field simulations modelling the crater and employ-
749 ing near-field predictions, just past the Mach shock but before the interaction
750 region in the crater, as input could be used to explore this issue further. It
751 is possible to conclude from the tests conducted that in these scenarios, re-
752 entrainment of ambient temperature, low concentration dispersing CO₂ into
753 the crater has little effect on a crater outflow, but re-entrainment of a stalling
754 plume, containing high concentration, cold CO₂ does have an effect on the
755 plume, leading to a lower stalling height and different dispersion properties.

756 A homogeneous equilibrium model has also been used throughout the
757 simulations presented here. In the case of ruptures, this is entirely applicable,

758 as discussed in detail elsewhere (Wareing et al., 2013b), since the particles
759 will be in equilibrium with the flow and follow the flow streamlines.

760 The choice of turbulence model has a bearing on the predictions. These
761 simulations have employed the $k - \epsilon$ turbulence model with a compressibil-
762 ity correction required by the decompression of the highly-underexpanded
763 pipeline flow. We have shown previously that this model is capable of mod-
764 elling free releases into air (Wareing et al., 2014a). To ensure compatibility
765 within the COOLTRANS research programme, we continued to employ this
766 model for the below-ground releases, with good results for punctures com-
767 pared to experimental data (Wareing et al., 2014b). However, a Reynolds-
768 stress turbulence model would be more appropriate for these situations. Even
769 with such a second-moment turbulence closure, it is not possible to capture
770 the true transient turbulent nature of these releases with a RANS model, as
771 the model is *time-averaged* predicting a time-averaged structure. Large eddy
772 simulation could be advantageously employed, but questions then have to be
773 answered as to how this would link with pipe-flow and near-field models and
774 feed into the RANS methods common in industry.

775 Further simulations of complex particle interactions will provide more
776 clarity, especially when considered in combination with far-field dispersion
777 calculations to estimate rain-out of solid CO₂, as the heaviest agglomerates
778 are probably formed in the interaction region in the middle of the crater.
779 Given the assumptions above about where particles deposit, these should
780 be considered upper limit estimates based on the method and analysis ap-
781 plied. However, it is difficult to apply these general assumptions. Given the
782 behaviour in the case of releases from pipeline punctures (Wareing et al.,

783 2014b), the simulations indicate that deposition could alter the profile of the
784 crater in such a way as to provide a ‘smooth’ flow path and inhibit further
785 deposition. It would be fair to say then that the 1% estimate is a ‘peak’ rate
786 of deposition and that once significant accumulation of solid occurs in the
787 crater, the flow may adapt to reduce this rate, thereby reducing the estimates
788 of total deposition made above considerably further.

789 In previous work (Wareing et al., 2014b), we have estimated particle de-
790 position rates for punctures of buried pipelines. Predicted particle behaviour
791 and deposition was seen in the experiments. There exists no evidence to
792 support or contradict the level of particle deposition estimated here - hor-
793 izontal venting experiments in CO2PIPETRANS have shown piles of solid
794 CO₂ under impact plates and deposition has been seen in both the puncture
795 experiments mentioned above and in the quarter scale rupture experiment
796 used for validation of this method in Part I, so we have reasonable confidence
797 in saying there will certainly be some particle deposition. Scaling up punc-
798 ture and quarter scale rupture experiments indicate it may be a considerable
799 amount, not entirely different to the amounts calculated above. Particle
800 collision and agglomeration, not included, may also be significant in these
801 rupture flows.

802 Whatever the amount of CO₂ in or around the crater, it should be sepa-
803 rately considered for further risk analysis as a secondary source of a dispersing
804 gas cloud after a rupture event, separate to the dispersion of the gas cloud
805 as a result of the rupture itself. It should also be noted that these are very
806 simple estimates that can be changed considerably by small changes in as-
807 sumptions, e.g. assuming 0.5% deposition and the quantity deposited drops

808 by a factor two. Without further refinement, and possibly testing of different
809 ways of introducing particles and capturing their behaviour, they should be
810 used with extreme caution in any future work. Further experimental data is
811 required to refine these predictions.

812 The sensitivity study of the base case has shown how different crater
813 parameters affect the flow out of the crater. It is reasonable to say that
814 the greatest effect comes from mis-aligning the pipes in Sensitivity study 5,
815 although the case considered is an extreme one and further studies would
816 be required to investigate the impact of, and corresponding changes to, the
817 crater geometry as a results of jet impingement on the crater walls. Other-
818 wise, a much increased fracture length (on the order of 72m) also has a large
819 effect on the flow structure, but not that much of an effect on the integrated
820 profiles. Changing the pipe depth, pipe section length, crater wall angle or
821 soil type have effects on the flow structure that can be understood in terms of
822 the parameter change, but are relatively minimal, especially when consider-
823 ing the integrated fluxes. It should be safe to assume that in all cases, except
824 the pipe mis-alignment case, a maximum of 1% of the particles released end
825 up in the base of the crater. The above results could also be interpreted to
826 mean that during balanced flow, all particles flow out of the crater, but this
827 would seem to be the other extreme of the scale and would ignore any possi-
828 bility of particle collisions in the interaction region that would drive particles
829 into the crater base. In the case of mis-aligned pipe inlets, considerably more
830 solid CO₂ may stay in the crater as the flows are deflected into the crater
831 walls, where particles will embed. However, the bath-tub crater shape used
832 is in fact unlikely to be the shape of the crater in such a mis-aligned release

833 and hence this result should again be used with caution. Further numerical
834 and experimental testing is required to elucidate this issue.

835 **7. Conclusions**

836 This article has presented the application of a novel method for simulat-
837 ing sonic high pressure releases of dense-phase CO₂ to the realistic scenario
838 of a rupture of a buried pipeline. The pipeline rupture proceeds through
839 a sequence of steady-states, or snapshots. Due to computational time con-
840 straints, only a number of these snapshots have been modelled. Integrated
841 fluxes have been produced for the flow out of the crater, providing signifi-
842 cantly novel initial conditions beyond the shock-containing thermodynamically-
843 complex near-field. Future far-field dispersion simulations can now employ
844 these integrated fluxes as source conditions and avoid the need to accurately
845 model the near-field conditions.

846 A set of six sensitivity studies has also been presented, examining the
847 effect of varying crater parameters on the flow out of the crater. Integrated
848 fluxes are also presented for each of these sensitivity studies. All these near-
849 field predictions have required a three-phase accurate equation of state, that
850 also accounts for the latent heat of fusion.

851 Extrapolations of the integrated fluxes to the full transient decompression
852 will now also be considered. Further experimental data at both laboratory-
853 scale and larger scales is required to further validate the model and shed
854 light on the behaviour of solid CO₂ in and around the crater, although we
855 have used Lagrangian particle tracking methods and appropriate conditions
856 derived from laboratory-scale experiments to estimate particle deposition

857 rates into the crater in this work.

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946 **Notation**

Roman letters:

a	model parameter
b	model parameter
c	adiabatic sound speed
C	specific heat
d	non-dimensional nozzle diameter
e	total energy per unit volume
F	Helmholtz free energy
k	turbulence kinetic energy
m	mass
p	pressure
r	non-dimensional radial location
R	universal gas constant
t	time
S	entropy
T	temperature
u	magnitude of velocity
U	internal energy per unit mass
v	molar volume
w	molecular weight
z	non-dimensional axial location

Greek letters:

α	condensed phase fraction
β	total mass fraction of CO ₂
δ	Peng-Robinson equation of state parameter
ϵ	dissipation rate of k
γ	ratio of specific heats
μ	molecular viscosity
ρ	density
τ	relaxation time
ω	acentric factor of the species

Subscripts:

0	reference state
a	air
c	condensed phase
crit	critical point
g	gas
i	initial
mix	mixture
s	saturation
trip	triple point
v	vapour

Table 1: Initial upstream and downstream pipe outflow conditions for the rupture cases (Mahgerefteh, private communication).

Time s	Stream direction	Pressure 10^6 Pa	Temp. K	CO ₂ %	Liquid %	Velocity m s^{-1}	Mass-flow kg s^{-1}
30	Up	1.971	253.3	100.0	69.0	98.19	3773
30	Down	1.971	253.3	100.0	69.0	98.19	3773
100	Up	1.403	242.8	100.0	64.0	108.5	2661
100	Down	1.403	242.8	100.0	64.0	108.5	2661
250	Up	1.060	234.8	100.0	61.0	114.0	1992
250	Down	1.060	234.8	100.0	61.0	114.0	1992
600	Up	8.12	227.7	100.0	58.0	119.4	1506
600	Down	7.55	225.8	100.0	58.0	120.1	1402
1000	Up	7.14	224.4	100.0	57.0	121.5	1334
1000	Down	5.98	220.1	100.0	56.0	123.3	1118
1150	Up	6.42	221.8	100.0	57.0	122.2	1205
1150	Down	5.16	216.6	100.0	55.0	124.2	971.0

Table 2: Crater parameters for the base rupture case and the range of sensitivity studies considered.

Case #	Fracture Length L'(m)	Crater Description	Length L(m)	Width W(m)	Depth D(m)	Wall angle θ°
Base	12	Clay soil, 1.2m depth	18.5	11.4	3.2	75
S1	24	Longer pipeline fracture	30.5	11.4	3.2	75
S2	12	Pipe top at 2m depth	19.4	12.3	4.0	75
S3	12	Shallower wall angle	18.5	11.4	3.2	64
S4	72	Longer fracture	78.5	11.4	3.2	75
S5	12	Pipes misaligned by 10°	22.0	14.9	3.2	75
S6	12	Sandy soil crater	33.9	26.8	3.2	40

Table 3: Snapshot integrated fluxes above the crater in the base rupture case.

Time (s)	30	100	250	600	1000	1150
Plane at:	2m	2m	1m	1m	1m	1m
Mass-flow	(kg s ⁻¹)					
Total up	12700	9830	6990	5290	4330	4080
Total down	1030	1710	1960	1190	1150	1360
CO ₂ up	7550	5810	4320	2990	2600	2370
CO ₂ down	15.8	43.8	48.9	134	200	145
Solid up	1440	1010	801	455	443	502
Solid down	0.020	0.064	0.006	0.197	1.54	0.404
Momentum	(kg m s ⁻²)					
Total up	914000	637000	415000	233000	171000	155000
Total down	4388	11900	18500	19500	9350	8740
CO ₂ up	600000	444000	290000	142000	107000	94400
CO ₂ down	82.4	239	243	1460	1210	972
Solid up	126000	93200	62000	25600	20000	21200
Solid down	0.111	0.307	0.004	2.190	8.018	2.386
Velocity	(m s ⁻¹)					
Up	72.1	64.9	59.3	44.1	39.5	37.9
CO ₂ up	79.5	76.4	67.1	47.7	41.3	39.8
Solid up	87.1	91.9	77.4	56.3	45.2	42.3
Peak	188	129	164	150	141	134
Temp.	192 K	188 K	189 K	186 K	188 K	187 K

Table 4: Snapshot integrated fluxes above the crater for Sensitivity Study 1.

Time (s)	30	100	250	600	1000	1150
Plane height:	2m	2m	2m	1m	1m	1m
Mass-flow	(kg s ⁻¹)					
Total up	11900	9230	7350	5890	5510	5050
Total down	3440	3080	2870	2820	2840	2610
CO ₂ up	7540	5280	3840	2960	2520	2340
CO ₂ down	78.8	49.3	35.1	53.4	33.5	57.9
Solid up	1440	859	518	386	292	323
Solid down	9.37	2.80	0.870	1.09	0.133	0.208
Momentum	(kg m s ⁻²)					
Total up	873000	651000	457000	333000	286000	226000
Total down	34600	28900	24700	26700	32300	25600
CO ₂ up	597000	410000	268000	192000	154000	117000
CO ₂ down	290	228	183	291	201	597
Solid up	125000	76900	44600	31300	22700	20000
Solid down	16.3	2.52	0.585	1.32	0.226	0.725
Velocity	(m s ⁻¹)					
Upwards	73.6	70.6	62.2	56.6	52.0	44.7
CO ₂ up	79.2	77.7	69.7	64.8	60.9	50.2
Solid up	86.5	89.5	86.1	81.3	77.7	61.9
Peak	169	156	149	155	153	142
Temp. (K)	188	188	188	188	191	188

Table 5: Integrated fluxes for the snapshots at $t = 250$ s Sensitivity Studies 2, 3 and 6.

Sensitivity study	S2	S3	S3
Plane height (m)	0	2	1
<hr/>			
Mass-flow (kg s^{-1})			
Total up	6530	7170	7090
Total down	2500	2080	3090
CO ₂ up	4020	3910	3830
CO ₂ down	144	231	78.7
Solid up	735	578	584
Solid down	0.380	6.76	6.38
<hr/>			
Momentum (kg m s^{-2})			
Total up	482000	373000	362000
Total down	9320	18800	18100
CO ₂ up	324000	241000	240000
CO ₂ down	1470	1580	108
Solid up	66500	45700	48600
Solid down	2.13	53.6	10.7
<hr/>			
Velocity (m s^{-1})			
Inferred up	73.8	52.1	51.0
Inferred CO ₂ up	80.7	61.5	62.7
Inferred solid up	90.5	79.1	83.3
<hr/>			
Flow-weighted temp. (K)	188	188	190

Table 6: Snapshot integrated fluxes above the crater for Sensitivity Study 4.

Time (s)	30	100	250	600	1000	1150
Plane height:	6m	5.5m	6m	6m	5m	6m
Mass-flow	(kg s ⁻¹)					
Total up	14800	11700	9540	7700	6850	6500
Total down	4150	4180	3550	2830	2860	2680
CO ₂ up	7540	5320	3980	2910	2440	2180
CO ₂ down	3.79	5.52	1.11	1.06	5.09	0.85
Solid up	934	461	238	81.9	30.1	113
Solid down	0.0	0.0	0.0	0.0	0.0	0.0
Momentum	(kg m s ⁻²)					
Total up	391000	267000	164000	93800	72700	61700
Total down	26200	26400	18600	12600	12800	11800
CO ₂ up	209000	128000	70800	36000	26200	20800
CO ₂ down	16.3	20.8	3.0	2.6	14.6	2.2
Solid up	7070	12400	4600	1010	307	1060
Solid down	0.0	0.0	0.0	0.0	0.0	0.0
Velocity	(m s ⁻¹)					
Inferred up	26.3	22.9	17.2	12.2	10.6	9.5
Inferred CO ₂ up	27.7	24.0	17.8	12.4	10.7	9.6
Inferred solid up	7.6	26.9	19.3	12.3	10.2	9.4
Peak	50.6	42.0	29.8	23.9	26.6	21.6
Temp. (K)	186	186	186	188	190	187

Table 7: Snapshot integrated fluxes above the crater for Sensitivity Study 5.

Time (s)	30	100	250	600	1000	1150
Plane height:	0m	0m	0m	0m	0m	0m
Mass-flow	(kg s ⁻¹)					
Total up	11000	7820	6360	4970	4290	3580
Total down	4230	2490	2350	1870	1650	1480
CO ₂ up	7720	5400	4030	2980	2510	2120
CO ₂ down	570	53.2	150	125	152	166
Solid up	1730	1160	755	510	408	418
Solid down	1.73	0.06	0.22	0.39	0.86	8.88
Momentum	(kg m s ⁻²)					
Total up	496000	369000	276000	162000	119000	85100
Total down	134000	30200	30700	19000	16400	12600
CO ₂ up	378000	273000	185000	102000	72800	53400
CO ₂ down	17800	433	2030	1270	1860	1670
Solid up	89600	62200	38000	18900	12800	11200
Solid down	28.3	0.41	2.19	1.76	5.20	76.7
Velocity	(m s ⁻¹)					
Upwards	45.2	47.2	43.4	32.6	27.6	23.7
CO ₂ up	49.0	50.6	45.9	34.2	29.0	25.2
Solid up	51.9	53.7	50.3	37.1	31.3	26.7
Peak	245	207	162	140	109	83.6
Temp. (K)	191	190	188	187	186	186