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1                   **Flame impingement to facilitate the stability of NH<sub>3</sub>-**  
2                   **CH<sub>4</sub> laminar diffusion flames: High-speed imaging and**  
3                   **schlieren visualization**

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21 **Abstract**

22 As a hydrogen-rich and carbon-free fuel with high energy density, ammonia is  
23 regarded as a promising substitute for fossil fuels. In this study, flame characteristic and  
24 flow field were investigated to explore the maximum substitution ratio of ammonia  
25 (critical substitution ratio, i.e.) in NH<sub>3</sub>-CH<sub>4</sub> by high-speed direct imaging and schlieren  
26 method. To follow up the realistic scenario of flames in enclosed combustion systems,  
27 the stability of impinging flame was also investigated under the effect of water-cooled  
28 cooper wall. The results showed that the critical ammonia substitution ratio for free  
29 laminar flames was less than 63% for the tested cases. Meanwhile, the free flames  
30 exhibited periodic expansion and separation, with significant fluctuations in lift-off  
31 height and flame stretch rate, accompanying with the periodic motion of the shear layer  
32 between the flame and air. After the introduction of the impinging wall, the critical  
33 ammonia substitution ratio of the flame increased from 63% to over 80% (up to 94%)  
34 in dependent upon the height of impinging wall. At low ammonia substitution ratio  
35 (40%), reducing the impinging height enhanced the stability of the flow field by  
36 suppressing the development of shear layers and vortex around the flame. When the  
37 ammonia substitution ratio gradually increased to 63% and the critical substitution ratio,  
38 the flame anchored on the wall at different impingement heights, and no obvious vortex  
39 development was observed in the flow field. Higher ammonia substitution ratios can  
40 weaken the influence of impingement height on the flame flow field.

41 **Keywords:** Ammonia combustion; Impinging flame; Flame stability; Schlieren  
42 technique; Vortex

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**Nomenclature**

$Re$	Reynolds number
$Le$	Lewis number
$D$	Inner diameter of burner nozzle (mm)
$H_b$	Length from nozzle exit to root of lift-off flame (mm)
$R_r$	Radius of flame root (mm)
$R_t$	Radius of flame tip (mm)
$\kappa$	Flame stretch rate ( $s^{-1}$ )
$A_f$	Projected area of flame yellow luminescent region ( $mm^2$ )
$\alpha$	Ammonia substitution ratio
$\alpha_{cr}$	Critical ammonia substitution ratio
$Q_f$	Fuel flow rate (SLPM)
$H_I$	Distance between nozzle and impinging wall (mm)
$\beta$	Ratio of the $H_b$ to the $D$
$H_v$	Length between vortex position and nozzle exit (mm)
$V_x$	Axial motion velocity of vortex (m/s)
$H_r$	Distance between flame root and impinging wall (mm)

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46        **1. Introduction**

47        With the rising demand for clean energy, ammonia ( $\text{NH}_3$ ) has attracted attention  
48        as a sustainable fuel [1-3]. As an excellent hydrogen carrier,  $\text{NH}_3$  is a carbon-free and  
49        high energy density fuel which can be stored and transported safely with advanced  
50        facilities [4, 5]. Thus,  $\text{NH}_3$  is regarded as a non-hydrocarbon based fuel that may be  
51        applied in combustion systems such as gas turbines [6], internal combustion engines  
52        and industrial furnaces [7-9]. However, studies have shown that  $\text{NH}_3$  has inferior  
53        combustion characteristics, including low laminar burning velocity and high minimum  
54        ignition energy requirement [10, 11]. These characteristics limit the practical  
55        application of  $\text{NH}_3$ . Co-combustion of  $\text{NH}_3$ - $\text{CH}_4$  mixed fuel with  $\text{CH}_4$  accounting for  
56        70% has a burning velocity 2.14 times higher than that of pure  $\text{NH}_3$  flames, and thus is  
57        widely used in various combustion devices for practical applications [10, 12].

58        Flame stability constitutes a critical issue for industrial applications and remains a  
59        subject of extensive studies. Lin et al. [13] reported that in ammonia-methane laminar  
60        diffusion flames, increasing ammonia fraction from 30% to 50% reduced flame  
61        flickering frequency and shifted vortex formation downstream. Colson et al. [14]  
62        similarly observed this phenomenon, attributing it to reduced mixture reactivity with  
63        ammonia addition, which stabilized flames farther downstream where local velocities  
64        were lower. In the study of Zheng et al. [15] about instability for ammonia-methane  
65        non-premixed flames, they found that as the ammonia content increased to 40%, the  
66        flame would transition from turbulent to laminar lifted flame and be directly  
67        extinguished from laminar lifted flames. The study of Colson et al. [16] on the stability

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68 of non-premixed methane jet flames found that the flame can't be stabilized when the  
69 ammonia ratio exceeds 0.3. Thus, to better utilize ammonia, increasing the ammonia  
70 substitution ratio in ammonia-methane blended fuels and enhancing flame stability  
71 under high ammonia substitution ratios are imperative.

72 Numerous studies have indicated that the flame instability or extinction behavior  
73 is primarily influenced by three factors: chemical reactions [17], thermal instability [18],  
74 and flow instability [19]. Won et al. [20] studied the chemical kinetics of hydrocarbon  
75 fuel (n-alkanes and iso-octane) diffusion flames. They found that hydroxyl (OH)  
76 radicals are key reactive intermediates in the oxidation reactions of hydrocarbon fuels  
77 and the concentration of OH radicals affect the rate of chain reactions related to alkane  
78 pyrolysis. Insufficient supply of OH radicals leads to a decrease in decomposition rate,  
79 making combustion unsustainable. Furthermore, there is a positive feedback  
80 relationship between the generation and consumption rate of OH radicals and the heat  
81 release rate in the flame, thereby affecting flame extinction. Chu et al. [21] found that  
82 the addition of NH<sub>3</sub> lessened the production of OH radicals in the methane flame,  
83 thereby making the flame easier to extinguish. In the study of Chen et al. [17] on  
84 ammonia-methane counterflow diffusion flames, increasing the initial pressure and  
85 temperature could compensate the negative effect of ammonia addition on flame  
86 instability, thereby increasing the ammonia substitution ratio. They attributed this  
87 phenomenon to the fact that elevated initial pressure and temperature could accelerate  
88 chemical reaction efficiency and increase heat release. Increasing the initial pressure  
89 and temperature during combustion may be one of the methods to improve the ammonia

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90 substitution ratio.

91 For practical applications on combustion systems (engine chambers, *etc.*),  
92 impinging flames have received considerable attention [22]. In despite of the thorough  
93 investigation on the stability characteristics of NH<sub>3</sub>-CH<sub>4</sub> jet flames, the NH<sub>3</sub>-CH<sub>4</sub>  
94 impinging flames may have distinctly different structures and dynamics and requires  
95 further understanding on the stability characteristics. Several studies investigated the  
96 influence of impinging wall on the combustion characteristics of hydrocarbon or  
97 ammonia-blended flames. Study on methane impinging flames have shown that the  
98 wall distance significantly affects the flame structure and near wall chemical reaction  
99 rate, potentially leading to local extinction [23]. In terms of flow field structure, vortex  
100 structures generated at the junctions of the primary jet region, wall jet region, and  
101 stagnation flow region disrupt the continuity of the flame front, triggering oscillations  
102 and reducing stability [24]. When ammonia is blended into the fuel, these effects  
103 become more pronounced. Research indicates that the addition of ammonia decreases  
104 the peak flame temperature and makes non-premixed impinging flames more prone to  
105 local extinction in the wall jet region [25]. On the other hand, for premixed flames, wall  
106 impingement can enhance stability by reducing the flow velocity around the flame,  
107 thereby enabling a higher ammonia blending ratio [26].

108 The previous studies investigated the effects of adding ammonia and impinging  
109 wall on flame stability, especially in chemical reactions. However, the maximum  
110 ammonia substitution ratio in ammonia-methane flames and the dominant factors  
111 related to the flame stability near the critical ammonia substitution ratio need further

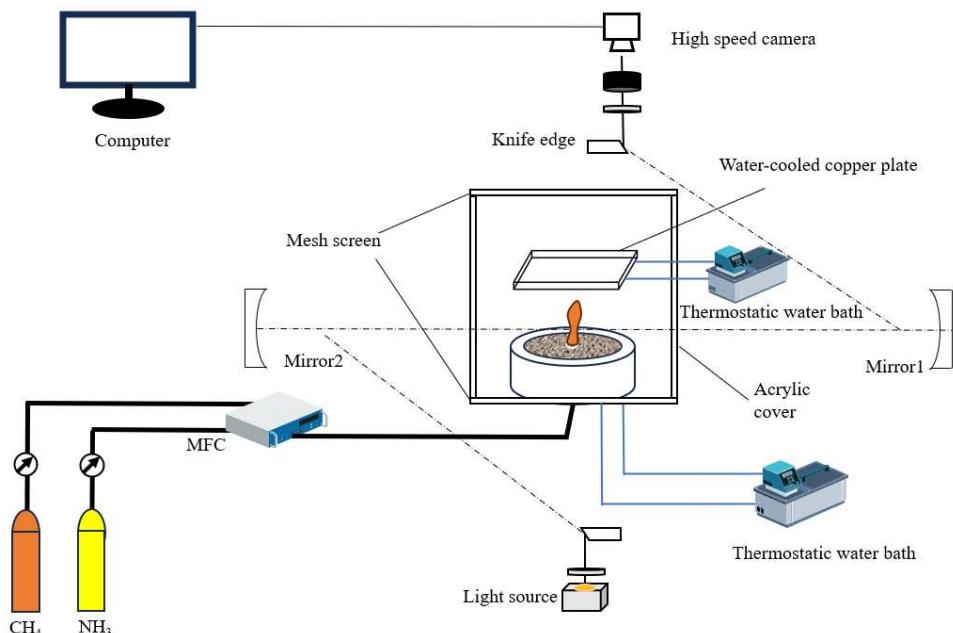
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112 investigation under the coupling effect of ammonia and impinging wall. In this study, a  
113 combination of high-speed direct imaging and schlieren method was utilized to analyze  
114 the flame structure and dynamic characteristics. The promoting effect of the impinging  
115 wall on the critical ammonia substitution ratio was obtained by comparing the  
116 differences in flame structure and stability between NH<sub>3</sub>-CH<sub>4</sub> free flames and  
117 impinging flames. The critical ammonia substitution ratios under different impinging  
118 heights were obtained. Additionally, the evolution of the flame flow field was  
119 investigated to shed light on its effect on flame stability. The present work may enrich  
120 the understanding of NH<sub>3</sub>-CH<sub>4</sub> impinging flames and facilitate the application of  
121 ammonia fuel on combustion systems.

122 **2. Experimental description**

123 The set-up of experimental apparatus is shown in Fig.1, consisting of a McKenna  
124 flat-flame burner, mass flow meters and a water-cooled copper plate. Acrylic cover was  
125 enclosed on the laminar diffusion flame to mitigate environmental interference. The  
126 burner with a fuel nozzle inner diameter ( $D$ ) of 8 mm, surrounded by a 60 mm diameter  
127 coaxial air annulus, contains an Archimedes spiral cooling circuit for water flow to  
128 minimize radial temperature gradient. CH<sub>4</sub> and NH<sub>3</sub> with purity of 99.99% were  
129 supplied to the burner at given mass flow rates. A water-cooled copper plate with a size  
130 of 150 mm × 100 mm and a thickness of 10 mm was positioned directly above the  
131 burner to study the flame impingement process. Six water channels were built in to fix  
132 the plate temperature to 313±2 K through circulating water connected to thermostatic  
133 water bath (THS-10, Tianheng, China).

134 The optical measurement system includes a high-speed camera and the Z-type  
135 schlieren imaging system. A high-speed camera (Memrecam GX-8, NAC) was used to  
136 capture the configuration and structure of flame. All flame images ( $1024 \times 1024$  pixels)  
137 were recorded at a frame rate of 50 fps. A Z-type schlieren imaging system (HGD-  
138 SD200) is mainly composed of a 300 W tungsten halogen lamp and two concave  
139 mirrors. The Halogen Tungsten lamp was employed due to its continuous spectrum in  
140 the visible range, providing stable and broad light output. Each mirror has an effective  
141 diameter of 200 mm and a focal length of 2000 mm. It was used to investigate the  
142 density gradient of flame flow field and obtain the flame stretch ratio. Schlieren  
143 imaging was performed using a direct visualization technique, with all image sequences  
144 acquired at identical frame rates (500 fps) and shutter speeds to ensure temporal  
145 consistency across experimental conditions.

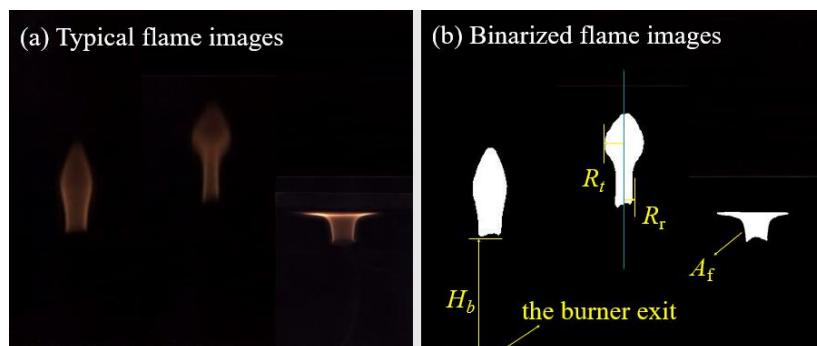


146  
147 Fig.1 Experimental set-up.  
148 Each flame image is converted into a binary image based on OTSU algorithm [27].  
149 The algorithm distinguishes the flame boundary by assigning binary values (1 for flame

150 and 0 for background). Then, the binarized images are further scrutinized to extract the  
 151 flame dimensional parameters in terms of the height of lift-off ( $H_b$ ), the radius of flame  
 152 root ( $R_r$ ), and the radius of flame tip ( $R_t$ ), as depicted in Fig. 2(b). The  $H_b$  defined as the  
 153 length from the nozzle exit to the root of lift-off flame. To characterize the flame stretch  
 154 rate ( $\kappa$ ) of impinging flames, the projected area of the flame yellow luminescent region  
 155 ( $A_f$ ) in the binarized images are measured. The  $\kappa$  is obtained according to the method of  
 156 Chung et al. [28]:

$$157 \quad \kappa = \frac{1}{A} \cdot \frac{dA}{d\tau} \quad (1)$$

158 where  $A$  represents the area of the flame surface,  $\tau$  denotes the time scale, and  
 159  $dA/d\tau$  is the rate of change of the flame area with respect to time. In terms of boundary  
 160 processing, for the first and last frames of the flame images, the forward difference [29]  
 161 and backward difference [30] methods were adopted for calculation, respectively. For  
 162 the flame images in the middle, the central difference method was used [31].



163  
 164 Fig. 2 (a) Typica images of free and impinging flame and (b) definitions of flame dimensional  
 165 parameters.

166 In this study, the effects of different ammonia substitution ratios ( $\alpha$ ) in the fuel  
 167 mixture and cold-flow Reynolds numbers ( $Re$ ) on flame stability were investigated.  
 168 These parameters are defined by Eq. (2) and Eq. (3), respectively. The flow rate of  $\text{CH}_4$   
 169 and  $\text{NH}_3$  were controlled by mass flow meters (AB-11, AiroBoost) with an accuracy of

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170 1% of full scale. The ammonia substitution ratio exhibited a  $\pm 1\%$  experimental  
171 uncertainty due to pressure fluctuation of fuel flow and systematic calibration  
172 deviations of the mass flow meters. Each test condition was conducted with more than  
173 three repeated experimental trials. The results derived from the flame images were  
174 averaged, with error bars representing the deviations from multiple repeated  
175 experiments.

176

$$\alpha = \frac{Q_{NH_3}}{Q_{NH_3} + Q_{CH_4}} \quad (2)$$

177

$$Re = \frac{\rho_{mix} V_{mix} D}{\mu_{mix}} \quad (3)$$

178 Where  $Q$  represents the volumetric flow rate of gases, and  $\rho_{mix}$ ,  $V_{mix}$ , and  $\mu_{mix}$   
179 represent the density, velocity, and viscosity coefficient of the fuel mixture, respectively.  
180 Additionally,  $D$  is the inner diameter of the nozzle.

181 In this study, critical ammonia substitution ratio ( $\alpha_{cr}$ ) in  $NH_3$ - $CH_4$  diffusion flames  
182 under different experimental conditions were investigated experimentally. For free  
183 flame without impinging wall, three fuel flow rates (0.7 slpm, 0.8 slpm, 0.9 slpm) were  
184 set as shown in Tab. 1, and  $\alpha$  was continuously increased to obtain the threshold of  
185 ammonia proportion of  $NH_3$ - $CH_4$  free flame. In the experiment, the threshold of  
186 ammonia proportion beyond which the flame turned to an unstable nature was recorded  
187 as the  $\alpha_{cr}$ . The unstable nature refers to the phenomenon that the flame boundary  
188 continuously fluctuates until eventual blow-out. Subsequently, a water-cooled copper  
189 plate was introduced to establish an impinging flame. The flame behavior patterns were  
190 found to be consistent across all three flow rates in free flames. Therefore, the

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191 impinging flame experiments were conducted with the representative flow rate of 0.8  
192 slpm. Various impinging height ( $H_I$ ), defined as the vertical distance between the exit  
193 of burner nozzle and the water-cooled copper plate, corresponding to 3, 6, 9 and 12  
194 times the nozzle inner diameter were adopted for the impinging flame experiments. To  
195 eliminate the interference of wall temperature on the experiment, the plate temperature  
196 was retained at  $313 \pm 2$  K through a thermostatic water bath.

197 Tab.1 Test conditions.

Case	Fuel flow (SLPM)	$H_I$ (mm)	Critical ammonia substitution ratio ( $\alpha_{cr}$ )	Cold flow Reynolds number under $\alpha_{cr}$ ( $Re$ )
F1	0.7	/	63%	118.09
F2	0.8	/	63%	134.96
F3	0.9	/	63%	151.83
I1	0.8	24	84%	137.43
I2	0.8	48	87%	137.79
I3	0.8	72	94%	138.62
I4	0.8	96	91%	138.14

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198 **3. Results and discussion**

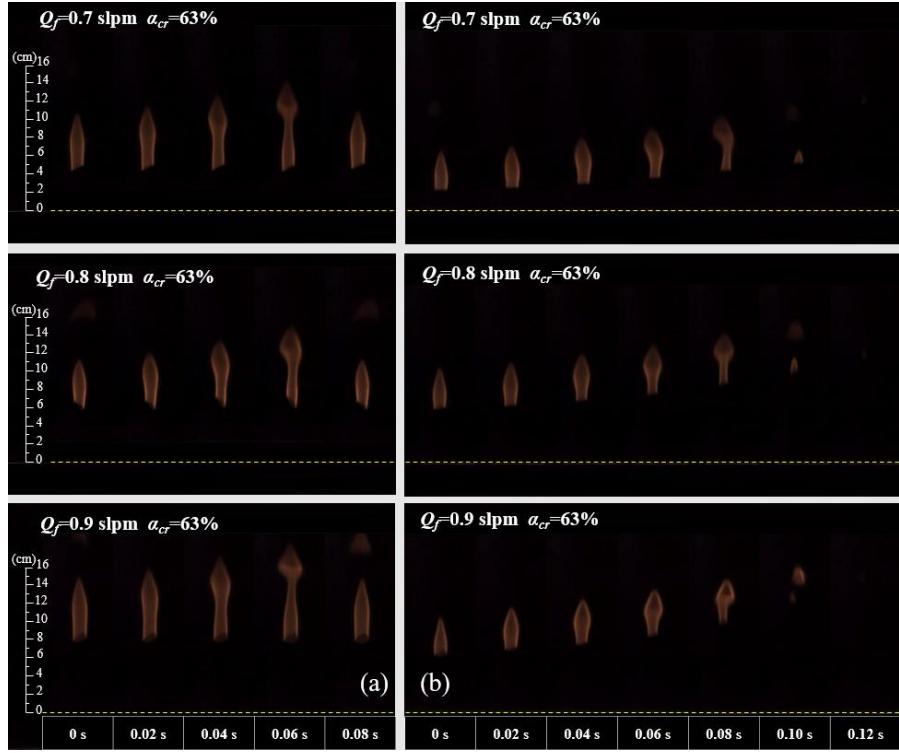
199 *3.1 Threshold of ammonia substitution ratio for flame extinction*

200 *3.1.1 Free diffusion flame*

201 In our previous work [13], flame instability in  $\text{NH}_3\text{-CH}_4$  laminar free diffusion  
202 flames was investigated at up to 50% substituted ratio of  $\text{NH}_3$ . It was found that upon  
203 ammonia addition, flames exhibit recurrent periodic oscillations similar to pure  
204 methane flames. In this study, the  $\alpha$  is further elevated to explore the mechanism for

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205 why the flame instability occurs. After further increasing the  $\alpha$  ( $\geq 60\%$ ), the flame  
206 possesses a more pronounced lift-off height and appears a blow-out as  $\alpha_{cr}$  is achieved.  
207 As the ammonia substitution ratio reached the threshold, high-speed camera was  
208 triggered simultaneously with flame ignition to capture the blow-out process. The flame  
209 exhibited periodic contraction oscillations, followed by a marked decrease in lift-off  
210 height. Fig. 3(a) shows the flame periodic oscillation process under various  $Q_f$  at  $\alpha_{cr}$ .  
211 The periodic oscillation of flame arises from the following mechanisms: differences in  
212 velocity and density between the fuel and air form the shear layer, within which  
213 oxidation reactions of the fuel release heat that induces thermal expansion [32].  
214 Thermal expansion exacerbates the density difference, and together with gravity,  
215 generates buoyancy. Driven by thermal expansion and buoyancy, the shear layer  
216 increases in diameter and forms vortex. The pushing or pulling effects of vortex on the  
217 flame surface cause local extinction and flame separation [33]. The shear layer repeats  
218 the developmental process, ultimately resulting in the periodic oscillation of the flame.  
219 Subsequently, the flame root undergoes a progressive elevation, contraction and  
220 expansion, ultimately leading to necking phenomena that detach the protruding region  
221 of the flame as time evolves, and eventually flame extinguishes as shown in Fig. 3(b).  
222 Necking originates from vortex generated by the shear layer between the jet and the  
223 ambient air, producing critical flame stretch rates that peak within the constricted region  
224 [34]. Enhanced flame stretch induced by flame surface curvature can trigger local  
225 extinction and necking [28]. Subsequently, the flame extinguished in both upward and  
226 downward directions.



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Fig. 3 The extinction process of  $\text{NH}_3\text{-CH}_4$  free diffusion flame: (a) first sequence after ignition; (b) last sequence preceding flame extinction. (The yellow dashed lines represent the burner nozzle exit.)

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To clearly observe flame evolution from ignition to extinction, the minimum and

maximum of  $H_b$  within each oscillation cycle were obtained, as well as the maximum

values of  $R_t$  and minimum values of  $R_r$ . As shown in Fig. 4(a) and (b), both  $H_b_{\min}$  and

$H_b_{\max}$  undergoes a reduction-then-increase trend as the time evolves under the various

$Q_f$ . Furthermore, when the  $Q_f$  increases from 0.7 to 0.8 slpm,  $H_b_{\min}$  and  $H_b_{\max}$

correspondingly raise. However, upon further increase to 0.9 slpm, a higher magnitude

of reduction is observed and the minimum values of  $H_b_{\min}$  and  $H_b_{\max}$  are even lower

than that for 0.8 slpm. According to the study of Lin et al. [13], when shear layer

vortices reach a critical threshold, they trigger global flame lift-off, and ammonia

addition enhances this phenomenon. Concerning lift-off conditions, Takahashi et.al [35]

proposed that a lift-off occurs when the local flow velocity at the flame base exceeds

flame laminar burning velocity. Due to the relatively small laminar burning velocity of

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243 ammonia, as  $\alpha$  increases, the flame laminar burning velocity will significantly decrease  
244 [36, 37], facilitating the lift-off flame phenomenon. Similar phenomena were also  
245 observed in the study of Zheng et al. [15] on the unstable characteristics of NH<sub>3</sub>-CH<sub>4</sub>  
246 non-premixed jet flames. They found that for the fixed ammonia substitution ratio,  
247 increasing the fuel injection speed would cause the flame to transition from an attached  
248 flame to a lift-off flame and further increasing the fuel injection speed would result in  
249 an increase in  $H_b$ . Similarly, Fig. 4(c) and (d) reveal that  $R_{t_{\max}}$  and  $R_{r_{\min}}$  exhibit an  
250 overall trend of initially irregular fluctuations across various  $Q_f$ , followed by a steep  
251 decline during the final 3~6 oscillation cycles preceding extinction. Quantitatively,  
252  $R_{t_{\max}}$  and  $R_{r_{\min}}$  increase correspondingly with higher  $Q_f$  across the tested range. The  
253 aforementioned dynamics phenomenon is a comparison of three cases under free  
254 diffusion flame. Given their consistent behavioral pattern as a whole, a representative  
255 flow rate of 0.8 slpm was selected as the  $Q_f$  for subsequent impinging flame experiment.

256 The non-monotonic structure variation and eventual blow-out of the NH<sub>3</sub>-CH<sub>4</sub> free  
257 flame at  $\alpha_{cr}$  indicate that a high ammonia substitution ratio leads to a significant  
258 decrease in laminar burning velocity, thereby intensifying the global extinction  
259 phenomenon induced by shear layer vortex [38]. For the flame impingement condition,  
260 the axial velocity of the unburned gas flow in the stagnation zone will be significantly  
261 reduced due to impingement on the wall, while the flow in the near wall jet region will  
262 be significantly affected by the boundary layer [26]. Therefore, the impingement  
263 process can establish a flow field with a lower velocity than that in the free flame, which  
264 is ultimately conducive to establishing a more stable flame shape and a complete flame

front. In this case, further investigation on the effect of the impinging wall is conducted and explore whether and how the impinging wall can further extend the threshold of ammonia substitution ratio.

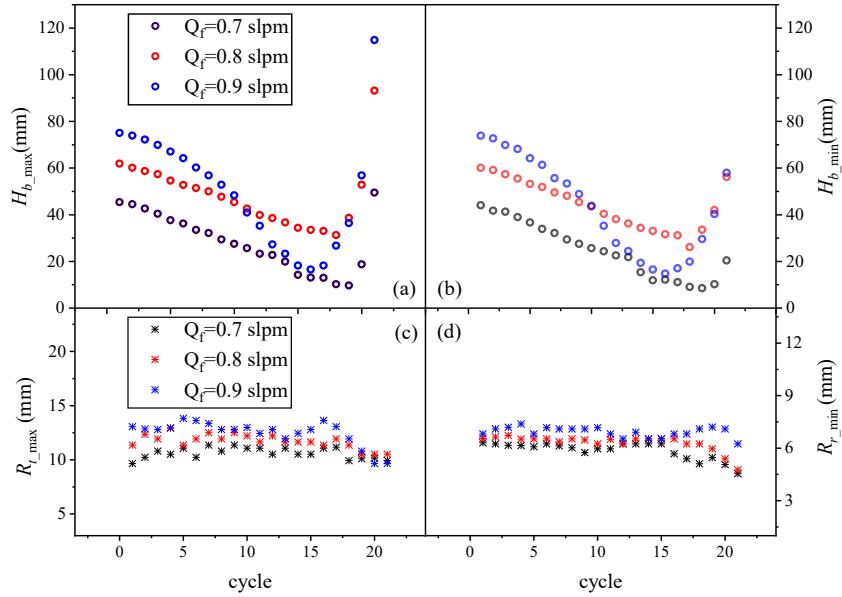


Fig. 4 Variation of flame size parameters over cycle: (a) the maximum height of lift-off ( $H_b_{\max}$ ) with various fuel flow rate ( $Q_f$ ); (b) the minimum height of lift-off ( $H_b_{\min}$ ) with various  $Q_f$ ; (c) the maximum radius of the flame tip ( $R_t_{\max}$ ) with various  $Q_f$ ; (d) the minimum radius of flame root ( $R_r_{\min}$ ) with various  $Q_f$ .

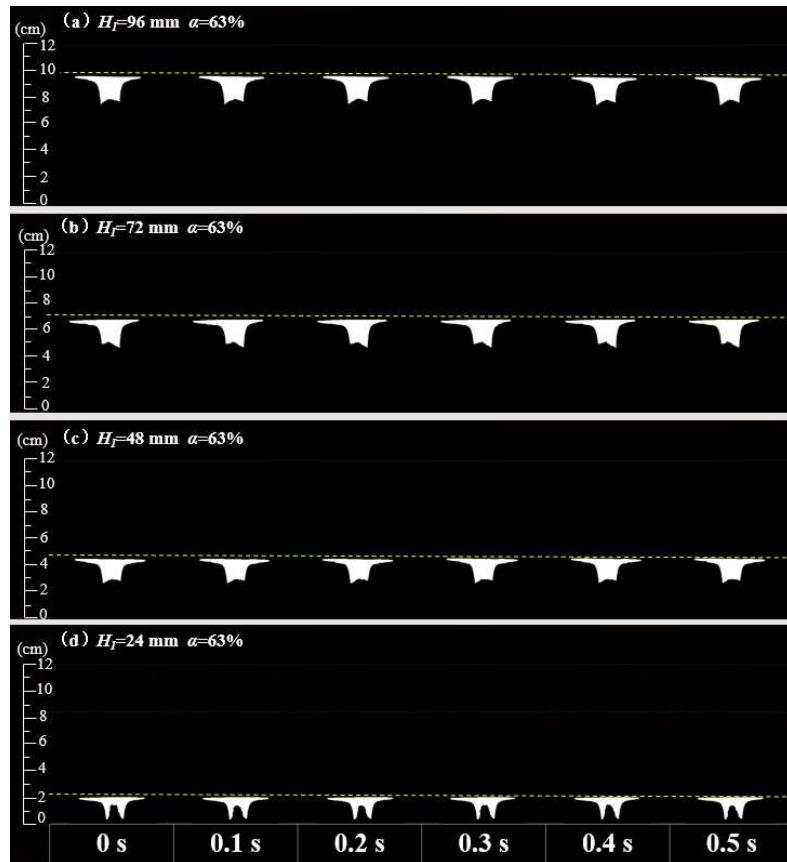
### 3.1.2 Impinging flame

To evaluate the effect of the impinging wall on laminar diffusion flames, experiments on  $\text{NH}_3\text{-CH}_4$  diffusion impinging flames with different  $\alpha$  are conducted at a constant  $Q_f$  of 0.8 slpm by varying the  $H_l$ . At the same  $\alpha$ , the appearances of  $\text{NH}_3\text{-CH}_4$  impinging flames differ from that of free flames, as shown in Fig. 5. Under this condition, the necking and separation characteristic of free flames are not appeared by the impinging flame that instead exhibit a stable lift-off flame attached to the impinging wall. A further analysis of Fig. 5 reveals that  $H_b$  increases with the increase in  $H_l$ . A dimensionless parameter  $\beta$ , defined as the ratio of the lift-off height ( $H_b$ ) to the nozzle

282 inner diameter ( $D$ ) is used to reveal the effect of  $H_I$

283

$$\beta = H_b / D \quad (2)$$

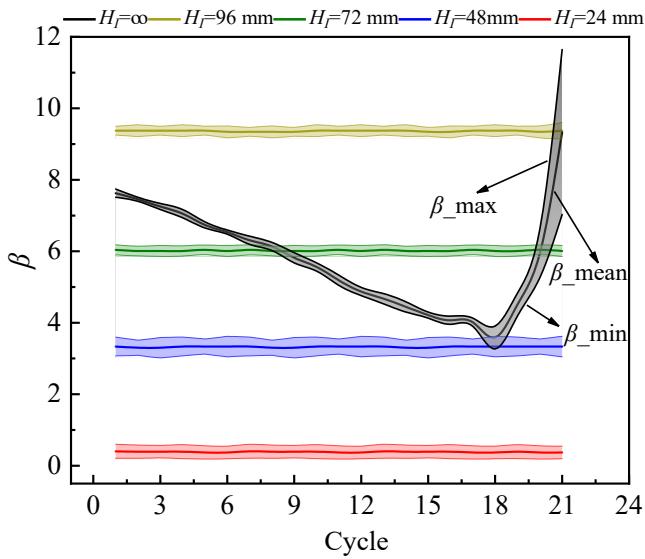


284

285 Fig. 5 Sequence diagrams of binarized images of impinging flame at different impinging heights  
286 ( $H_I$ ) under the fuel flow rate ( $Q_f$ ) of 0.8 slpm and the ammonia substitution ratio ( $\alpha$ ) of 63%, with  
287 the yellow dashed line denoting the position of the water-cooled copper plate.

288 For comparison with free flames at  $\alpha$  of 63%, the cycle experienced by the free  
289 flame from ignition to extinction is defined as the period of interest. Given that the  
290 impinging flame does not extinguish, flame images captured at equal time intervals are  
291 used to quantify the corresponding parameter. The results in Figs. 6-8 are the mean  
292 values obtained for each cycle. Fig.6 shows the variation of  $\beta$  for free flames during the  
293 extinction process and that for imping flame under different  $H_I$ . It is observed that for  
294 the impinging flame  $\beta$  increases with the rise in impinging height. Besides, it is noted  
295 that adjusting  $H_I$  improves the flame stability. When  $H_I$  decreases from 48 mm to 24

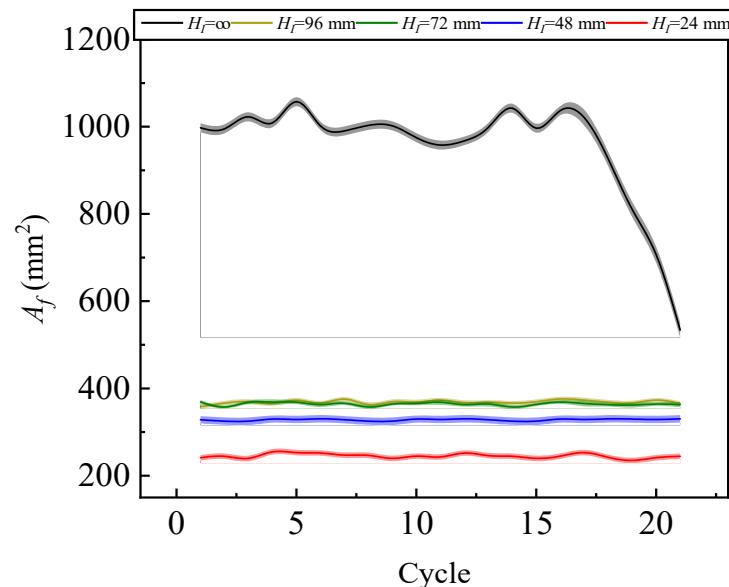
296 mm,  $\beta$  drops to around 0.4, indicating that reducing  $H_l$  facilitates the transition of the  
 297 flame from lifted to attached state. Furthermore, the  $\beta$  of the impinging flame exhibits  
 298 marginal fluctuations over the whole period, which indicates a stable combustion. In  
 299 contrast,  $\beta$  for the free flame shows significant fluctuations. This phenomenon is related  
 300 to the above-mentioned necking and separation occurring in the free flame. Vortex  
 301 beneath the bulge of the free flame tip pushes the flame surface outward, while vortex  
 302 above the bulge pulls the surface inward, thereby enhancing fuel and air mixing at  
 303 specific moments [39]. As a result, the local burning velocity and stretch rate increase,  
 304 leading to fluctuations at the flame boundary.



305  
 306 Fig. 6 Variation of the ratio of the lift-off height to the nozzle inner diameter ( $\beta$ ) for different  
 307 impinging heights ( $H_l$ ) at the fuel flow rate ( $Q_f$ ) of 0.8 slpm and the ammonia substitution ratio ( $\alpha$ )  
 308 of 63% with cycle (where the impinging height of  $\infty$  corresponds to the free flames).

309  $A_f$  for flames under different  $H_l$  are derived from the binarized images, as shown  
 310 in Fig. 7.  $A_f$  for the free flames exhibit a significant fluctuation amplitude over cycle,  
 311 particularly during the latest cycles of the flame extinction process. This behavior  
 312 corresponds to the aforementioned changes in  $\beta$ . After the introduction of the impinging  
 313 wall, the variation amplitude of  $A_f$  decreases, further verifying the improvement in

314 flame stability. In addition,  $A_f$  shows a significant reduction with the introduction of  
 315 impinging wall, and gradually increases with the increasing  $H_l$ . However, when the  $H_l$   
 316 increases from 72 mm to 96 mm,  $A_f$  shows no significant increase and sustains a  
 317 comparable level. Similar phenomenon was also found by Zhen et al. [40]. In the  
 318 presence of an impinging wall, the conical shape of the flame front is truncated by the  
 319 wall, causing radial stretch of flame and restricting the axial development, finally  
 320 resulting in the flame taking on ‘V’ and ‘M’ shapes. For impinging flames, Li et al. [23]  
 321 found that as the impinging height increases, the flame shape changes from a horn-like  
 322 form to a complete shape. They explained that the space for flame development  
 323 expanded with an increase in impinging height, permitting more ambient air entrained  
 324 into the combustion zone, resulting in more thorough combustion and an enlarged flame  
 325 area.

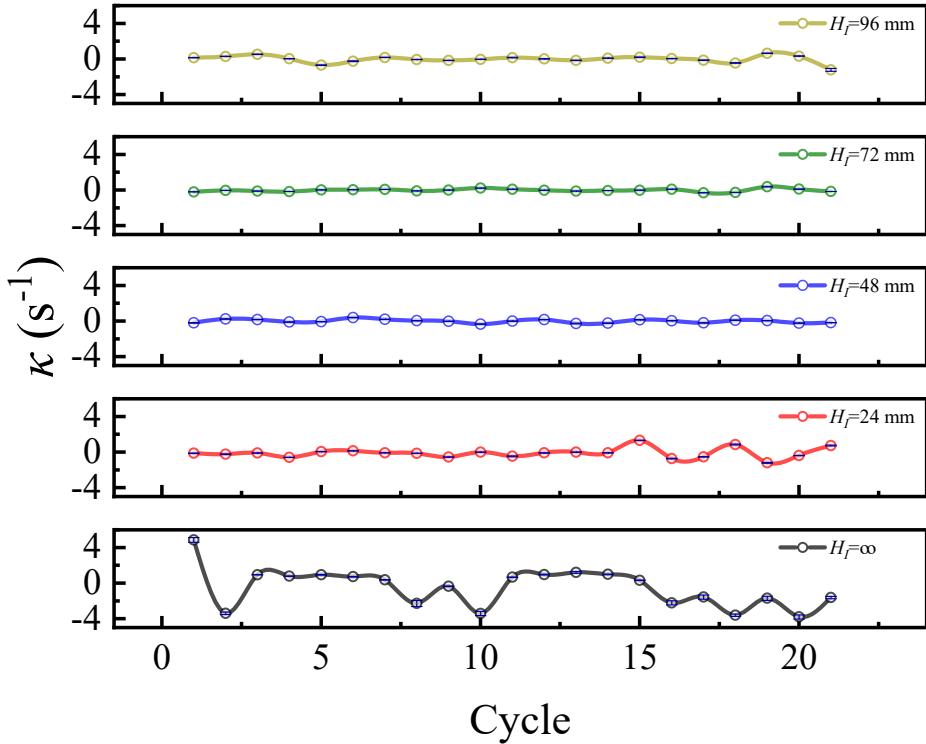


326  
 327 Fig. 7 Variation of projected area of the flame yellow luminescent region ( $A_f$ ) for different  
 328 impinging heights ( $H_l$ ) at the fuel flow rate ( $Q_f$ ) of 0.8 slpm and the ammonia substitution ratio ( $\alpha$ )  
 329 of 63% with cycle.

330 Flame stretch rate ( $\kappa$ ) is also employed to quantify the improvement of flame

---

331 stability by wall impingement. As shown in Fig. 8,  $\kappa$  for the impinging flames are nearly  
332 zero, indicating that the flame area varies slightly and tends to a stability. For  $H_l \geq 48$   
333 mm,  $\kappa$  shows moderate fluctuate and exhibit no significant affinity with the variation in  
334  $H_l$ . Surprisingly, for  $H_l$  of 24 mm,  $\kappa$  shows marginal fluctuation in the early cycle, but  
335 present a large amplitude fluctuation in the later cycle. In contrast, the free flames  
336 exhibit higher level and fluctuation amplitude (-4~5) in  $\kappa$ , suggesting severe changes in  
337  $A_f$ . According to Jung et al. [41], larger flame stretch rate reduces the flame heat release  
338 rate, inhibiting heat release in the reaction zone, and ultimately leads to flame extinction.  
339 In the last 7 cycles before the extinction of the free flame,  $\kappa$  remained negative,  
340 suggesting a continuous decrease in  $A_f$  until extinction. This phenomenon may be  
341 related to the rates of mass diffusion and thermal diffusion in the flame, i.e. the Lewis  
342 number ( $Le$ ) of the fuel.  $Le$  for  $\text{NH}_3$  is significantly higher than that for  $\text{CH}_4$  [42-44]. In  
343 the study by Zhang et al. [45], it was found that in the tip region of ammonia-methane  
344 flames, the preferential diffusion effect induced by the high Lewis number leads to  
345 insufficient local fuel mass diffusion and contraction of the flame area, which further  
346 causes flame contraction and eventually results in extinction.



347

348 Fig. 8 Variation of flame stretch rates ( $\kappa$ ) of flames for different impinging heights ( $H_I$ ) at the fuel  
 349 flow rate ( $Q_f$ ) of 0.8 slpm and the ammonia substitution ratio ( $\alpha$ ) of 63% with cycle.

350 The  $\alpha$  is further expanded to explore the maximum level of ammonia application

351 in NH<sub>3</sub>-CH<sub>4</sub> fuels. Compared with the free flame,  $\alpha_{cr}$  for the impinging flame increases

352 significantly, rising from 63% to over 80%, as shown in Fig. S1 of the supplementary

353 material. This phenomenon indicates that the impinging wall enhances the stability of

354 flames and  $\alpha_{cr}$  is greatly improved. In laminar diffusion flames, the flame burning

355 velocity and the flow velocity of the unburned gas are the key factors determining flame

356 stability. The impinging wall may form a lower-velocity flow field matching the

357 reduced laminar flame velocity for higher ammonia content, and facilitate the flame

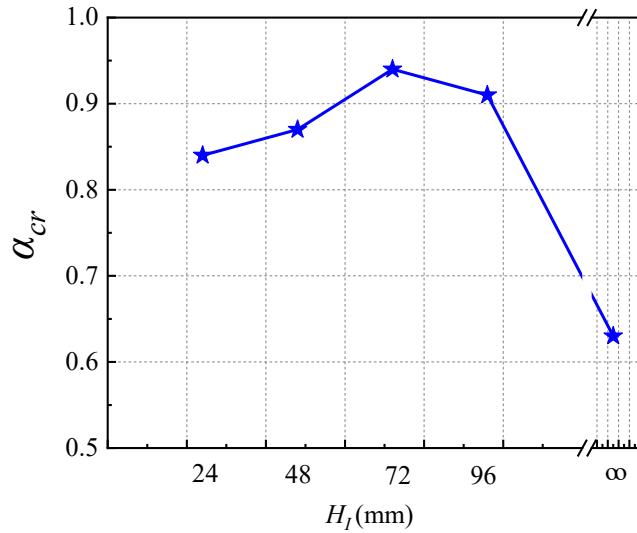
358 stability [26].  $H_I$  is a crucial factor influencing the combustion characteristics of

359 impinging flames [46]. As  $H_I$  increases from 24 to 72 mm,  $\alpha_{cr}$  shows a monotonical

360 increase and achieves the peak value of 94% at  $H_I$  of 72 mm. The impinging wall creates

361 a stagnation flow field with a low velocity zone [24], reducing local stretch rate, as

362 shown in Fig. 8. A lower  $\kappa$  can lead to a more stable flame anchoring, permitting a  
 363 higher proportion of  $\text{NH}_3$  to be substituted in the fuel mixture before reaching the  
 364 critical condition. When  $H_l$  is further increased to 96 mm, the  $\alpha_{cr}$  decreases to 91%. As  
 365  $H_l$  continues to increase, the flow becomes more complex with large fluctuations in the  
 366 fuel-air mixture ratio and flow velocity. The non-homogeneous fuel mixture  
 367 distribution and rapid changes in flow conditions make it difficult for  $\text{NH}_3$  to burn  
 368 efficiently. As a result, the flame stability deteriorates and  $\alpha_{cr}$  decreases. At each  $H_l$ , the  
 369 process from flame ignition to extinction under  $\alpha_{cr}$  is recorded and digitalized with a  
 370 time scale of 0.1 ms to derive the variations of  $\beta$ ,  $A_f$  and  $\kappa$  over time.

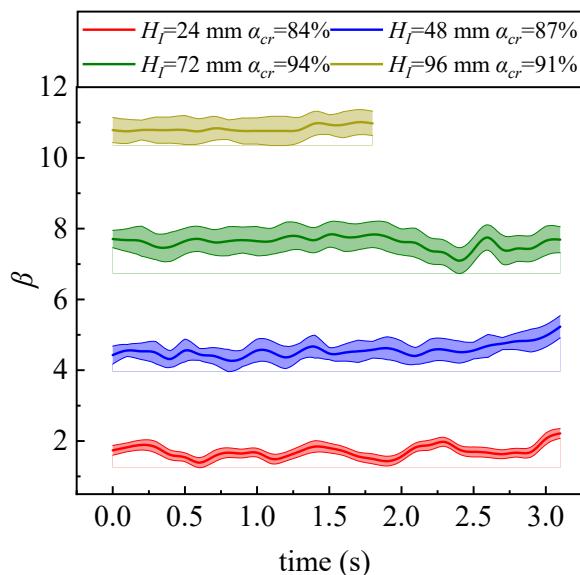


371  
 372 Fig. 9 Critical ammonia substitution ratio ( $\alpha_{cr}$ ) for different impinging heights ( $H_l$ ) at the fuel  
 373 flow rate ( $Q_f$ ) of 0.8 slpm (where the impinging height of  $\infty$  corresponds to the free flames).

374 As shown in Fig. 10, for the same  $H_l$ ,  $\beta$  increases significantly with the increase in  
 375  $\alpha$ , indicating that the flame base moves toward the upstream of flame. At the flame lift-  
 376 off conditions [35], the local flow velocity equals to the flame burning velocity. As  $\alpha$   
 377 further increases, the  $\text{NH}_3$  addition further reduce the fuel burning velocity [36], and  
 378 thus the flame root moves to downstream (with a lower flow velocity) to re-establish

---

379 equilibrium. Meanwhile, the fluctuation amplitude of  $\beta$  increases as  $\alpha$  further increases.  
 380 At the initial  $\alpha$  of 63% for the impinging flame,  $\beta$  shows nearly no temporal fluctuation.  
 381 Conversely, at  $\alpha_{cr}$ ,  $\beta$  exhibits distinct fluctuations across different  $H_l$ , suggesting a  
 382 deterioration in flame stability. The results of Colson et al. [47] indicated that the  
 383 counterflow non-premixed ammonia-methane flames cannot be stabilized at higher  
 384 ammonia constituted ratio ( $>70\%$ ) due to the flame weakness and strong buoyancy  
 385 effect. At that condition, the flame resides in a regime proximate to the extinction limit,  
 386 thereby exhibiting heightened susceptibility to perturbation, and  $\beta$  fluctuation increases.  
 387 Additionally, further increasing  $\alpha$  will also lead to an increase in  $Le$  of the fuel [43].  
 388 Wang et al. [48] found that on ammonia-methane laminar expanding flames, an increase  
 389 in the  $Le$  leads to a more uneven distribution of flame surface curvature, exacerbating  
 390 the geometric distortion of the flame surface. Owing to the high  $Le$  of  $\text{NH}_3$ , it is more  
 391 sensitive to the interaction of vortex structure in the lifted state, resulting in the  
 392 intensification of  $\beta$  oscillation under the lift-off condition.



393  
 394 Fig. 10 Variation of the ratio of the lift-off height to the nozzle inner diameter ( $\beta$ ) for different  
 395 impinging heights ( $H_l$ ) at the fuel flow rate ( $Q_f$ ) of 0.8 slpm and the acritical ammonia substitution

396 ratio ( $\alpha_{cr}$ ) with time.

397 Under  $\alpha_{cr}$ ,  $A_f$  at different  $H_l$  all exhibit distinct fluctuations over time, as shown in

398 Fig. 11. Meanwhile, as  $\alpha$  increases from 63% to  $\alpha_{cr}$ ,  $A_f$  under different  $H_l$  decrease. The

399 lower flame propagation speed, corresponding to a higher ammonia content, are prone

400 to slow down the expansion rate of the combustion reaction zone and affect the mixing

401 process of fuel and oxidizer [49], resulting in reduction in  $A_f$ . As  $H_l$  increased to 72 mm

402 at which the largest  $\alpha_{cr}$  is achieved,  $A_f$  is significantly larger than that at other  $H_l$ . The

403 lower  $A_f$  at  $H_l$  of 24 mm and 48 mm may come from the strong cooling effect from the

404 impinging wall on the flame front of the laminar flame [50]. When  $H_l$  further increases

405 to 96 mm,  $A_f$  decreases significantly, and the combustion duration also reduces

406 obviously. For this case, the cooling effect of the impinging wall on the combustion

407 process may be diminished, while the entrainment of ambient air provides more

408 oxidizer, exerting a significant cooling effect on flame combustion and leading to a

409 reduction in  $A_f$  [51]. Similar to the free flame,  $A_f$  of the impinging flame gradually

410 decreases until it extinguishes.

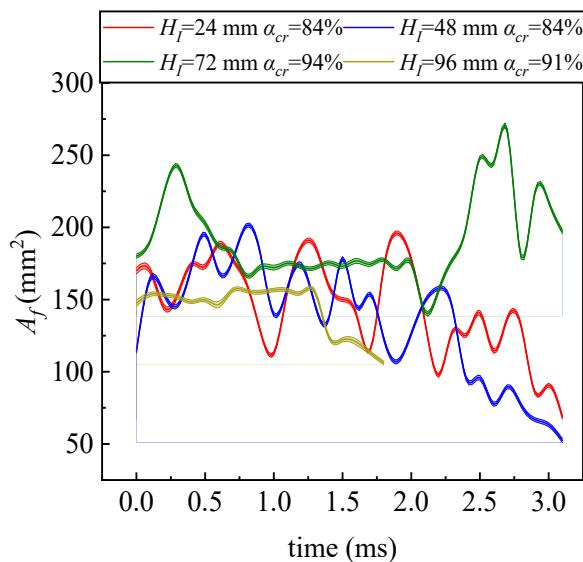
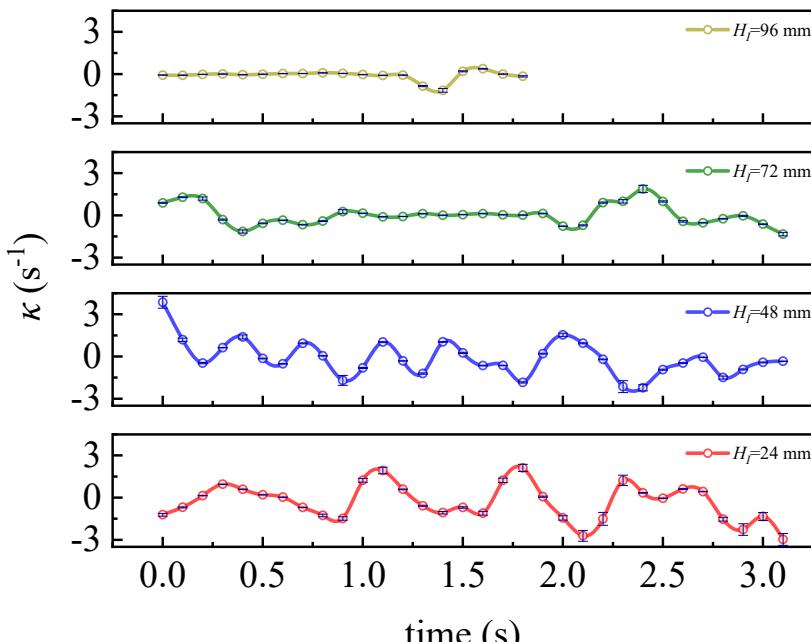


Fig. 11 Variation of projected area of the flame yellow luminescent region ( $A_d$ ) for different

413 impinging heights ( $H_I$ ) at the fuel flow rate ( $Q_f$ ) of 0.8 slpm and the critical ammonia substitution  
414 ratio ( $\alpha_{cr}$ ) with time.

415 Fig. 12 shows the variation of  $\kappa$  with time at different  $H_I$ . At all impingement  
416 heights,  $\kappa$  possess periodical fluctuation over time. At  $H_I$  less than 48mm, the  
417 fluctuation amplitude of  $\kappa$  is relatively large (-3 to 4  $s^{-1}$ ). The flame is significantly  
418 affected by the wall, leading to the stretching and compression of the flame front at low  
419  $H_I$ . As  $H_I$  increased from 48 mm to 72 mm, the fluctuation amplitude of  $\kappa$  decreases (-  
420 1 to 1.5  $s^{-1}$ ). At this time, the impinging flow field is stable, and the fuel and air may be  
421 mixed uniformly. When  $H_I$  increases to 96 mm,  $\kappa$  is relatively low in the early stage,  
422 but the fluctuation intensifies (-1.5 to 0.5  $s^{-1}$ ) in the later stage. At higher  $H_I$ , the fuel  
423 jet develops sufficiently, and the oxidizer is sufficient, but the turbulence intensity  
424 increases, which intensifies the local deformation of the flame front, resulting in larger  
425 fluctuations of  $\kappa$  in the later stage of combustion [52].



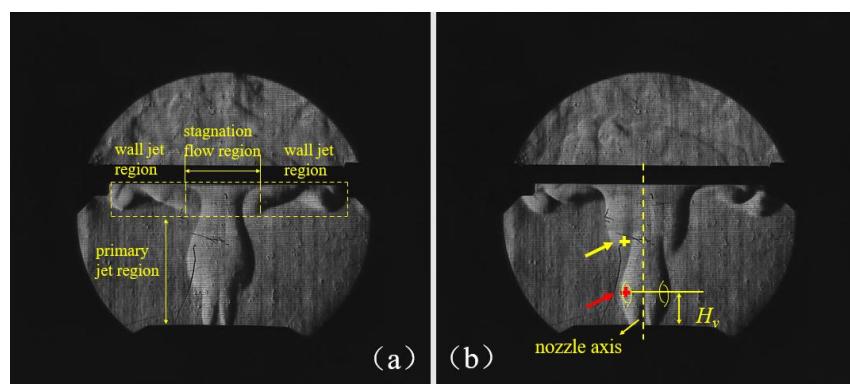
426  
427 Fig. 12 Variation of flame stretch rate ( $\kappa$ ) of flames for different impinging heights ( $H_I$ ) at the fuel  
428 flow rate ( $Q_f$ ) of 0.8 slpm and the critical ammonia substitution ratio ( $\alpha_{cr}$ ) with time.

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429 3.2 *Schlieren image analysis*

430 Schlieren visualization is used to study the generation and distribution of vortex  
431 around flames and their interaction with flames [53, 54].

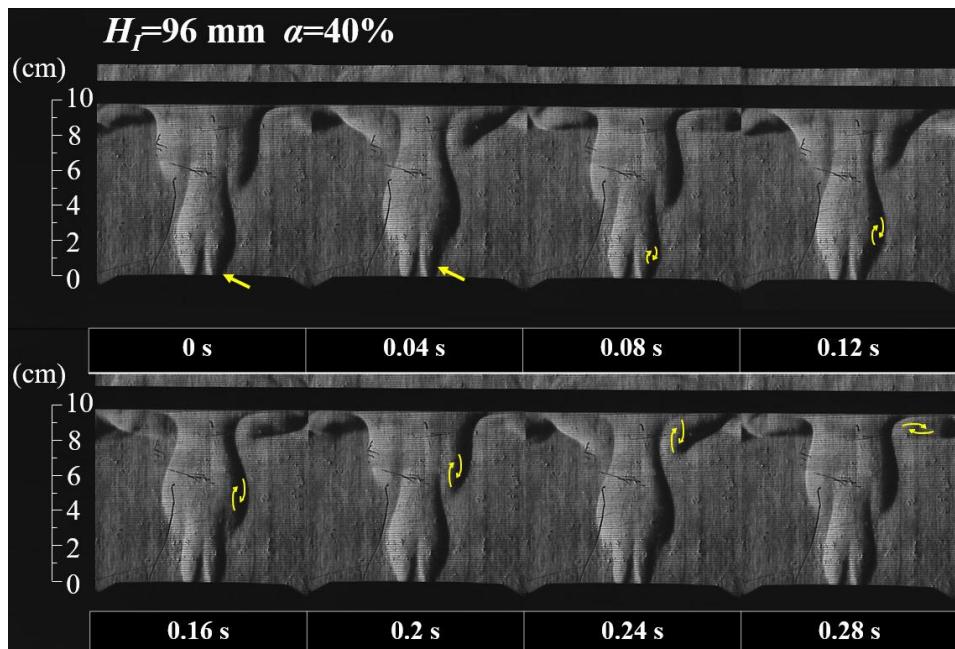
432 By changing  $H_l$  (24, 48, 72, 96 mm) and  $\alpha$  ( $\geq 40\%$ ), the effect of impinging wall  
433 and ammonia substitution ratio on the stability of  $\text{NH}_3\text{-CH}_4$  flame is obtained. Fig. 13(a)  
434 presents the schlieren image of typical impinging flame. There are three characteristic  
435 regions in the flow field: the primary jet region, the stagnation flow region and the wall  
436 jet region, which are consistent with the previous study of [55]. In the primary jet region,  
437 the impinging wall has no significant influence on the flow and the shear layer at the  
438 interface of flame and surrounding air presents a spindle shape, similar to the free  $\text{NH}_3\text{-}$   
439  $\text{CH}_4$  laminar diffusion flame studied by Lin et al. [13]. In the stagnation flow region,  
440 the axial flow strongly decelerates and the radial flow accelerates, resulting in an  
441 increase in pressure and ultimately leading to the wall jet region. The wall jet region  
442 begins where the velocity is basically parallel to the impinging wall. In the wall jet  
443 region, the flame spreads along the wall surface.



444  
445 Fig. 13 (a) Schlieren diagram of the typical impinging flame; (b) schematic diagram of parameter  
446 definition.

447 A typical sequence of schlieren images depicting the development of flame vortex

448 and their position in the flow field at  $H_I$  of 96mm and  $\alpha$  of 40% is presented in Fig.14.  
 449 In the primary jet region, the spindle-shaped shear layer at the flame and air interface  
 450 undergoes periodic motion due to thermal expansion [56]. As shown in Fig. 14 , the  
 451 flame vortex evolves sequentially: initial slight inward concavity (roll-up vortex) on the  
 452 shear layer develops into an internal vortex with increasing shear layer diameter [57]  
 453 Upon impingement, the axial development of the shear layer is constrained and  
 454 gradually moving radially. At this time, the shear stresses near the wall generate an  
 455 annular vortex in the near wall region [58, 59]. The vortex positions refer to the study  
 456 by He et al. [59]. As the impingement distance increases, more vortex structures can be  
 457 observed.



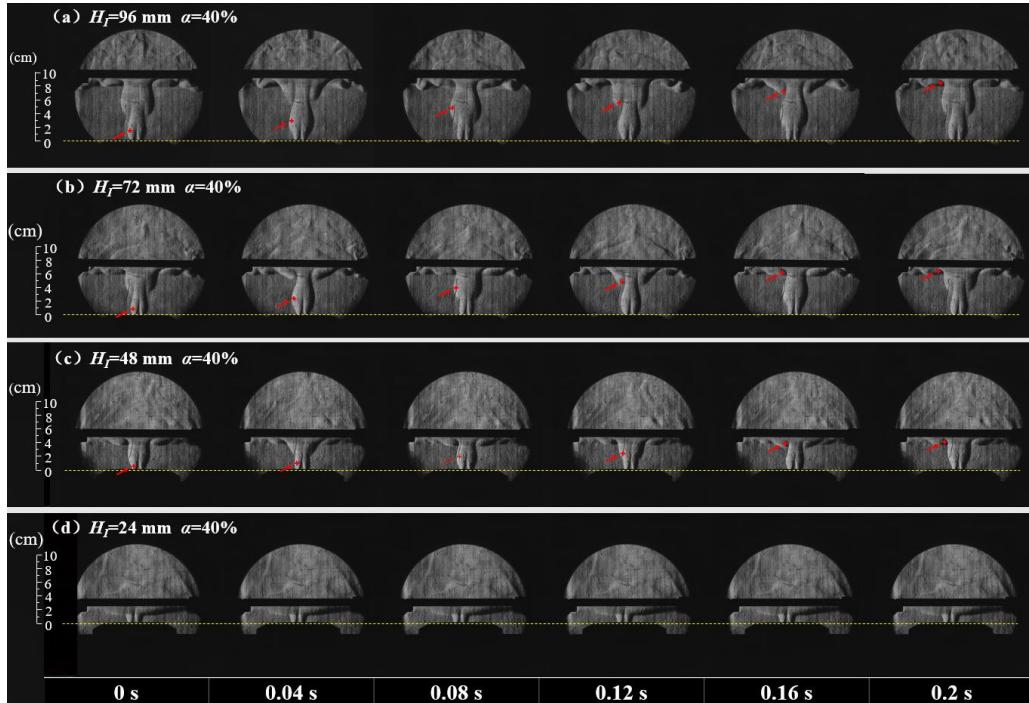
458  
 459 Fig. 14 Whole schlieren image sequence of flame vortex evolution at an impingement height  
 460 ( $H_I$ ) of 96 mm and an ammonia substitution ratio ( $\alpha$ ) of 40% (the yellow markers indicate the  
 461 vortex positions)

462 Fig. 15 presents the complete sequence of schlieren images depicting the flames  
 463 at  $\alpha=40\%$  for various  $H_I$ . At  $H_I \geq 48$  mm, the spindle shaped shear layer undergoes  
 464 periodic motion due to thermal expansion [13, 56]. Firstly, the shear layer expands

---

465 gradually until the flame front impinges on the wall. Subsequently, the shear layer  
466 develops along the wall into a vortex - like shape. In contrast, with the lower  $H_I$  of 24  
467 mm, the flame remains in a stable state in which the flame boundary exhibits negligible  
468 fluctuations, with no coherent vortical structures developing within the wall jet region.  
469 At lower impingement heights, the development of the fuel jet is constrained, leading  
470 to rapid dissipation of axial momentum [60]. The main jet region is compressed, which  
471 suppresses the development of flame vortex and alters the temperature distribution [59].  
472 Consequently, a flow field distinct from that observed at other heights is formed.  
473 According to the study by Hsu et al. [57] on jet impinging on a flat plate, there are two  
474 axisymmetric vortices within each spindle-shaped shear layer, with the vortex center  
475 located at the maximum diameter of the shear layer, as shown by the red arrow in Fig.  
476 13(b). After the flame impinges on the wall, the shear layer begins to stretch radially  
477 under the combined action of the wall and the original thermal expansion force, causing  
478 the alteration of the vortex center. The vertex center is the local extremum of the  
479 vorticity, therefore the new vortex center after flame impingement is obtained [24, 61],  
480 as depicted by the yellow arrow in Fig. 13(b). Therefore, to compare the influence of  
481  $H_I$  on vortex development, the evolution of vortex center is studied. Red crosses track  
482 the development trajectory of the vortex, as shown in Fig. 15 (a-c). Initially, the spindle-  
483 shaped shear layer bends inward and forms roll-up vortex, depicted by the red arrows  
484 in the images. As time evolves, the elevation of vortex position with the development  
485 of the shear layer. After impinging on the wall, the flame front takes a V-shape and  
486 propagates radially along the wall. The difference in flame stability with the same  $\alpha$  at

487 different  $H_l$  indicates that reducing the  $H_l$  can mitigate the influence of vortex on flames  
 488 by suppressing the development of flame shear layer, making it easier to achieve stable  
 489 processes. In addition, the lower  $H_l$  allows more heat and active free radicals to be fed  
 490 back to the unburned gas near the nozzle, which also helps stabilize the flame [62].

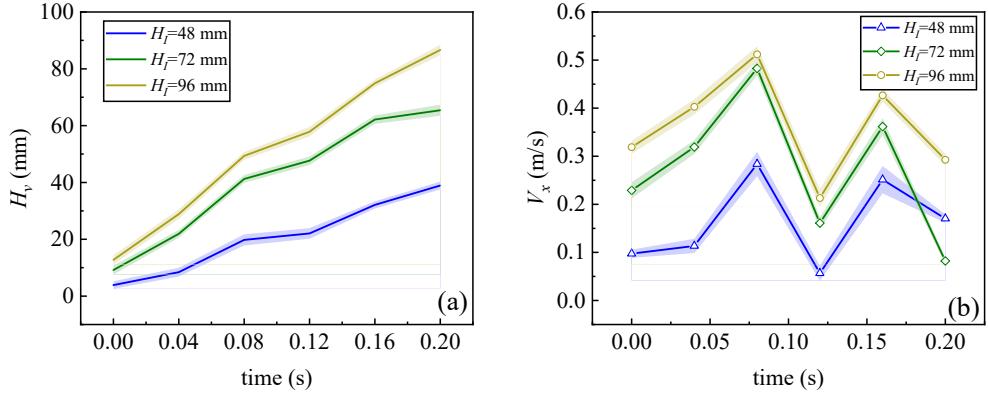


491  
 492 Fig. 15 Whole sequence of schlieren images for different impinging heights ( $H_l$ ) at the fuel flow  
 493 rate ( $Q_f$ ) of 0.8 slpm and the ammonia substitution ratio ( $\alpha$ ) of 40%, with yellow dashed line  
 494 represents the nozzle exit position.

495 The yellow horizontal line shown in Fig. 13 (b) represents the height of the vortex  
 496 position ( $H_v$ ), defined as the length between the vortex center and nozzle exit, which is  
 497 used to calculate the axial motion velocity of vortex ( $V_x$ ). Take the differential of  $H_v$   
 498 within the 0.04 s time interval to obtain  $V_x$ . The changes in  $H_v$  and  $V_x$  can be qualitatively  
 499 used to describe the intensity of the vortex [63]. Fig. 16(a) shows the variation of  $H_v$   
 500 with time under different  $H_l$ . At all  $H_l$ ,  $H_v$  gradually increases over time and eventually  
 501 reaches a constant value. The reason is the low density hot gas enters the high density  
 502 ambient air, causing the flame shear layer to expand continuously, and the vortex rises

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503 as the shear layer expands [64]. At 0.16 s, the vortex enters the wall jet region, the flame  
504 develops radially under the influence of the impinging wall, and  $H_v$  reaches a constant  
505 value. The  $V_x$  at different times is shown in Fig. 16(b). At each  $H_l$ ,  $V_x$  shows the same  
506 variation law. At 0~0.08 s, the vortex is located in the primary jet region with little  
507 constraint by the wall and the vortex axial motion driven by thermal expansion force  
508 and jet momentum. The thermal expansion force causes a decrease in gas density near  
509 the flame front, forming an axial pressure gradient that accelerates the unburned gas  
510 and increases the flame burning velocity [65], resulting in an increase in  $V_x$ . At 0.08 s,  
511 the flame schlieren image shows that the flame tip collides with the impinging wall,  
512 causing the shear layer to be radially stretched and change of the vortex center.  
513 Subsequently, the wall stagnation effect gradually intensifies and exerts a reverse force  
514 on the flame through momentum exchange [66], leading to a significant decrease in  $V_x$ .  
515 At 0.12~0.16 s, the shear layer develops under the combined action of wall confinement  
516 and thermal expansion force, further increasing  $V_x$ . However,  $V_x$  in this case remains  
517 lower level than that before the impingement. After the vortex enters the wall jet region,  
518 it develops radially along the wall. As the radial distance increases, the vortex gradually  
519 dissipates and  $V_x$  decreases due to the influence of wall viscous resistance and shear  
520 stress [25]. Reduced  $H_l$  relocates vortex downstream, leading to reduction in  $V_x$ . The  
521 reduction of  $H_l$  shortens the primary jet region and may enhance the wall-induced  
522 stagnation effects, thereby weakening the axial acceleration driven by thermal  
523 expansion force. Consequently, shear layer and vortex development are suppressed,  
524 establishing a stable flow field as depicted in Fig. 15(d).



525

526 Fig. 16 Parameters of the vortex over time for different impinging heights ( $H_I$ ) at the fuel flow rate  
 527 ( $Q_f$ ) of 0.8 slpm and the ammonia substitution ratio ( $\alpha$ ) of 40%: (a) the length between the vortex  
 528 center and nozzle exit ( $H_v$ ); (b) the axial motion velocity of vortex ( $V_x$ ).

529

To further understand the influence of  $\alpha$ , the flame schlieren images for higher  $\alpha$  (63% and  $\alpha_{cr}$ ) at different  $H_I$  are shown in Fig. 17. At higher  $\alpha$ , the flow field exhibits similar stable state at each  $H_I$  to that for  $H_I=24$  mm of  $\alpha=40\%$ . Notably, for  $\alpha=63\%$ , as  $H_I$  elevates to higher value of  $\geq 48$  mm, the periodic development of shear layer and vortex vanishes and the flow field undergoes towards the stable state. He et al. [24] observed a similar phenomenon, in the near-wall region, the area of vortex significantly decreases with an increase in the  $\text{NH}_3$  blending ratio. When further increases  $\alpha$  from 63% to  $\alpha_{cr}$ , the flow field stability remains unaltered under different  $H_I$ . However, the flame in the primary jet region moves downstream, and the motion of the flame flow field is mainly concentrated in the stagnation flow region and the wall jet region. That is, increasing  $\alpha$  probably weaken the influence of  $H_I$  on the flame flow field, enabling the flame to stably attach to the wall for combustion.

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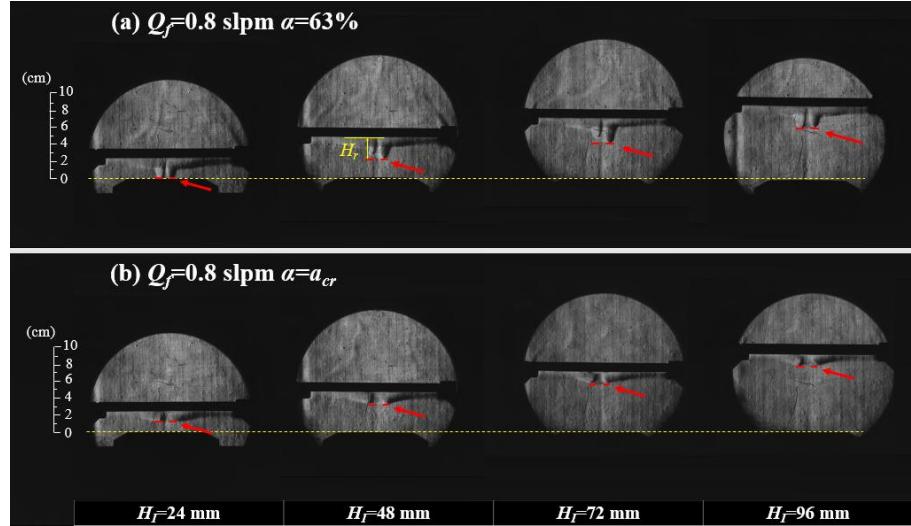
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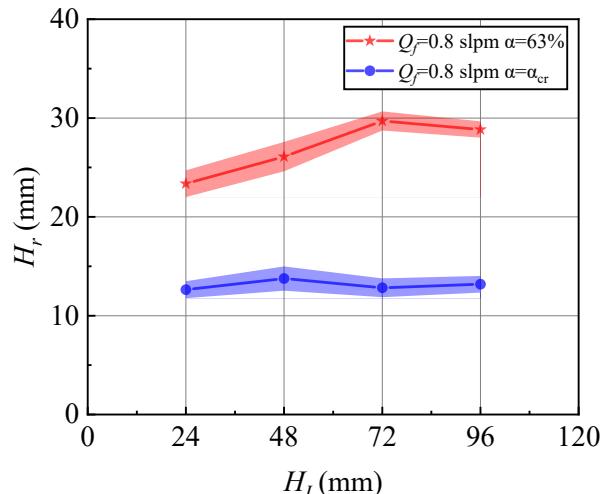
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Fig. 17 Schlieren images for different impingement heights ( $H_I$ ) and ammonia substitution ratios ( $\alpha$ ) at the fuel flow rate ( $Q_f$ ) of 0.8 slpm, with yellow dashed line represents the nozzle exit position.

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The distance between the flame root and the impinging wall, termed as  $H_r$ , is used to further depict the flow structure. The definition of  $H_r$  is demonstrated in Fig. 17. As shown in Fig. 18, for  $\alpha=63\%$ , with increasing  $H_I$ ,  $H_r$  gradually rises and reaches the peak at  $H_I=72$  mm, then decreases slightly as  $H_I$  further increases to 96 mm. When further increasing to  $\alpha_{cr}$ ,  $H_r$  exhibits no consistent trend and scatters within a range of 12.5 mm to 13.5 mm, meaning that  $H_r$  may be insensitive to the variation in  $H_I$ . This phenomenon indicates that the increase of  $\alpha$  may anchor the flame root in the near wall region, suppressing the effect of  $H_I$  on flow field. According to the study of Takahashi et al. [35],  $H_r$  is controlled by flame burning velocity and local fuel flow velocity. Higher ammonia content in flames reduces flame burning velocity, driving the flame root downstream and transitioning from attached flame to lifted flame configuration [36]. At  $H_I \geq 48$  mm, the lifted flame shortens  $H_r$ , which may result in a flow field similar to that at  $H_I = 24$  mm. Therefore, the impinging wall suppress vortex development and enhance flow field stability, thereby the lifted flame anchoring.

559 Conversely, at higher ammonia substitution ( $\alpha=63\%$ ), the free flame undergoes necking  
560 as the shear layer develops, leading to flame instability and ultimately triggering blow-  
561 out probably.



562 Fig. 18 The value of  $H_r$  under different impingement heights ( $H_I$ ) at the fuel flow rate of 0.8 slpm.  
563  
564 In relevant studies, the extinction of  $\text{NH}_3\text{-CH}_4$  flame has been extensively  
565 scrutinized and attributed to various factors such as fluid dynamics [19], chemical  
566 reactions [17] and thermal effects [18]. Under the critical substitution ratio of ammonia  
567 in hydrocarbon fuels, the development of flame vortex is suppressed and the flow  
568 instability within the flow field is weakened with the effect of the impinging wall. Thus,  
569 chemical reactions and thermal instability may be the main factors leading to flame  
570 extinction under the condition. This assertion is supported in the study of [59] on  
571 characteristics of methane non-premixed impinging flame. The high-temperature  
572 region was concentrated in the stagnation region, and the temperature gradually  
573 decreased as the wall-attached flame propagated. They attributed this phenomenon to  
574 the decrease in flame temperature caused by heat and momentum dissipation during the  
575 propagation of the wall-attached flame in the near wall region, which leads to weakened

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576 flame stability and extinction behavior. According to the study of Chu et al. [21], a  
577 decrease in flame temperature due to the addition of ammonia to methane non-premixed  
578 flames reduces the reaction rate and decreases the production of OH radicals, thereby  
579 resulting in a lower extinction limit of the flame. With the introduction of impinging  
580 wall, the flame flow field becomes jointly controlled by both impinging height and  
581 ammonia substitution ratio. The impinging wall likely enhances the critical ammonia  
582 substitution ratio primarily by altering vortex distribution and evolution within the flow  
583 field. Under the present experimental conditions, when ammonia substitution ratio  
584 reaches a certain level, it may weaken the effects of impinging height, causing flow  
585 fields to converge toward identical characteristics.

586 **4. Conclusion**

587 The effect of impinging wall on the stability of ammonia-methane laminar  
588 diffusion flame was investigated by the high-speed camera system and schlieren  
589 method in this work. The main findings are summarized as follows:

590 In the absence of the impinging wall, the free flame exhibits periodic expansion  
591 and separation at the critical ammonia substitution ratio, displaying pronounced  
592 fluctuations dominated by flow instability. With introduction of the impinging wall, the  
593 critical ammonia substitution ratio of the flame increases from 63% to over 80%. At a  
594 low ammonia substitution ratio (40%), reducing the impinging height promote the  
595 stability of flow field by suppressing the development of shear layer and vortex around  
596 the flames. When the ammonia substitution ratio is gradually increased to 63% and the  
597 critical substitution ratio, the flames are anchored on the wall at different impinging

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598 heights, with no significant vortex development in the flow field. Therefore, a higher  
599 ammonia substitution ratio can weaken the influence of impinging height on the flame  
600 flow field, and chemical and thermal instability may be the main factors leading to  
601 flame extinction under this condition. In addition to flow instability caused by flow  
602 field fluctuations, chemical kinetics and thermal instability in the flame are also key  
603 factors affecting flame stability. Therefore, the chemical kinetics and temperature  
604 effects of ammonia-methane flames under impinging wall conditions will be further  
605 investigated in our subsequent studies.

606 **CRediT authorship contribution statement**

607 **Yidu Tong:** Conceptualization, Investigation, Data curation, Visualization,  
608 Writing-original draft. **Chenyang Fan:** Investigation, Methodology, Funding  
609 acquisition, Supervision, Project administration, Writing-review and editing. **Zheng Fu:**  
610 Investigation, Resources, Validation. **Ye Liu:** Investigation, Validation. **Huiyong Du:**  
611 Methodology, Resources. **Bin Xu:** Methodology, Resources. **Guorong Lin:**  
612 Conceptualization, Visualization. **Shuo Jin:** Investigation, Data curation, Validation.  
613 **Shuainan Yang:** Investigation, Data curation, Validation. **Mingliang Wei:** Resources,  
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