



## Full Length Article

# Soot particles generated by *n*-heptane and *n*-heptane/OME<sub>3</sub> in an inverse diffusion flame: A comparative analysis of physical properties and oxidative reactivity

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## ABSTRACT

The widespread adoption of E-fuel, oxymethylene ether-3 (OME<sub>3</sub>), is a promising solution to accelerate the decarbonisation of the transport sector. However, the application of OME<sub>3</sub> inevitably alters the combustion characteristics, affecting the soot generation process and consequently changing the physical properties of these soot particles. These alterations, in turn, influence not only associated health and climate concerns but also the control strategies of diesel particulate filter (DPF) regeneration. Here, high-resolution transmission electron microscopy (HRTEM) and thermogravimetric analysis (TGA) were employed to explore the effects of blending OME<sub>3</sub> on soot primary particle size, fractal dimension, nanostructure, and oxidative characteristics. The results show that the addition of OME<sub>3</sub> form smaller soot precursors and accelerates the oxidation of soot particles, which subsequently reduces the size of primary particles. The smaller size of soot particles favours oxidation, but they are likely to pose more severe health risks. The smaller primary particles exhibit more pronounced Brownian motion and weaker van der Waals forces, leading to the formation of a looser agglomerate structure and smaller fractal dimensions (*D<sub>p</sub>*). Furthermore, the addition of OME<sub>3</sub> results in a reduction of long-range order in C atoms network and an increase of odd-number carbon rings during the generation of soot particles, which in turn leads to a reduction in fringe length (*L<sub>f</sub>*) and an increase in fringe tortuosity (*T<sub>f</sub>*) and separation distance (*S<sub>f</sub>*) of soot particles. These nanostructural changes induced by OME<sub>3</sub> enhance the oxidative reactivity of soot particles, as evidenced by the lower oxidative characteristic temperatures and reduced activation energy.

## 1. Introduction

Traffic-related CO<sub>2</sub> emissions accounted for 24 % of the global total CO<sub>2</sub> emissions from fuel combustion in 2019, with road transport contributing approximately 74 % of this share [1]. Despite ongoing efforts to improve thermal efficiency and fuel economy, the increasing number of internal combustion engine vehicles (ICEVs) still leads to a continuously grow in CO<sub>2</sub> emissions each year. [2]. Given the

carbon-neutral nature of E-fuels driven from CO<sub>2</sub>-captured techniques, their application in ICEVs could significantly contribute to achieving carbon neutrality. Among the various E-fuels, oxymethylene ethers (OME<sub>x</sub>) have demonstrated exceptional potential. First, OME<sub>x</sub> can be synthesized by recycling CO<sub>2</sub> through electrochemical methods powered by clean energies, thus achieving a carbon balance [3]. Second, the OME<sub>x</sub> blends easily with diesel without requiring modifications to the ICEVs [4]. Third, the high oxygen content and reduced C–C bonds in

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oxygenated OME<sub>x</sub> fuels facilitate the suppression of soot precursor formation, thereby reducing soot particle emissions [5].

Among the OME<sub>x</sub> ( $x = 1-5$ ) fuels, OME<sub>3</sub> demonstrates superior potential in real-world application, with a suitable cetane number of 78, melting point of  $-41^{\circ}\text{C}$ , and boiling point of  $156^{\circ}\text{C}$  [6]. The physical properties of OME<sub>3</sub> confer it with better storage capacity compared to OME<sub>1</sub>, higher safety over OME<sub>2</sub>, and superior low-temperature fluidity relative to OME<sub>x</sub> (where  $x > 4$ ) [7,8]. Therefore, the application of OME<sub>3</sub> in diesel additives has attracted significant attention [5,9,10]. However, it is important to note that OME<sub>3</sub> is not a carbon-free fuel; both pure OME<sub>3</sub> or diesel/OME<sub>3</sub> blend fuels inevitably generate particulate matter (PM). Previous research has demonstrated the advantages of OME<sub>n</sub> fuels in reducing PM emissions. For instance, Arias et al. [11] investigated the impact of substituting diesel with OME<sub>3</sub> in an Euro 6 engine. They found that a 20 % OME<sub>3</sub> blend could reduce 61 % particle number emissions for the WLTC condition. Similarly, García-Oliver et al. [12] pointed out that adding over 30 % OME<sub>3</sub> to diesel changes combustion characteristics and significantly reduces soot particle emissions. Schmitz et al. [13] observed that the addition of OME<sub>3</sub> in premixed flames significantly reduces the emissions of larger soot particles. Existing studies mainly focus on the potential of OME<sub>3</sub> blends to reduce soot particle emissions. However, research on how OME<sub>3</sub> blends influence the soot physical properties remains limited.

The soot physical properties influence not only the environment and human health but also the efficiency of DPF regeneration. For instance, soot particle size and fractal dimension affect atmospheric residence time and transport, while soot nanostructure influences oxidative reactivity and the oxidative rate during DPF regeneration [14–16]. Soot particles with a more disordered nanostructure tend to oxidise more readily, enhancing DPF regeneration efficiency [17]. Conversely, highly ordered soot structures may resist oxidation, impeding regeneration processes [18]. Consequently, an in-depth understanding of the mechanisms by which OME<sub>3</sub> addition influences the physical properties of soot particles is crucial for mitigating adverse health effects and optimising control strategies of DPF regeneration.

Given these identified research gaps mentioned above, this research systematically examined the effects of OME<sub>3</sub> addition on the soot physical properties. In terms of ICEVs, isolating specific parameters is challenging because of the extremely complex thermal and dynamic processes involved. To achieve more controlled experimental conditions, an inverse diffusion flame was therefore employed in this research, as it enables more precise control over combustion parameters, allowing for a deeper understanding of the effects of OME<sub>3</sub> addition on the soot physical properties. In the tests, soot particles were collected at three varying heights above the burner (HAB), representing the phases of soot formation, growth, and oxidation. High-resolution transmission electron microscopy (HRTEM) and thermogravimetric analysis (TGA) were employed to characterise the physical properties and oxidative reactivity of soot particles, involving soot particle size, fractal dimension, fringe length, tortuosity, separation distance, oxidative characteristic temperatures and activation energy. The findings from this study are expected to provide a theoretical basis for the practical application of OME<sub>3</sub>, contributing valuable insights into the broader adoption of e-fuels for sustainable transport solutions.

## 2. Experimental

### 2.1. Burner setup

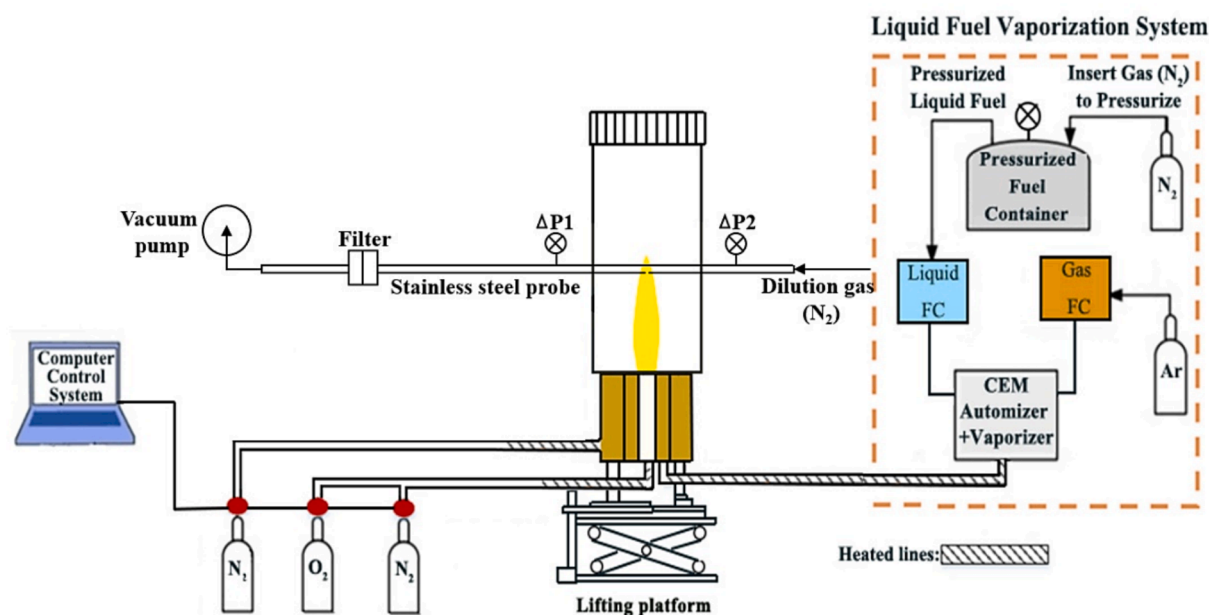
To better understand soot properties in diesel engine combustion, the diffusion flame was used in this study as it exhibits similar characteristics to the primary combustion mode in diesel engines. Both involve a mixing-controlled combustion process, where fuel and air react at the flame front rather than being pre-mixed, making diffusion flames an effective platform for investigating soot formation, growth, and oxidation mechanisms under conditions relevant to diesel combustion.

However, differences exist, such as pressure and turbulence levels, as diesel engines operate at high pressure with transient flow conditions, while the test burner operates at ambient pressure in a steady-state environment. Despite these differences, diffusion flames provide a controlled and reproducible setting, allowing for a detailed analysis of how fuel composition influences soot characteristics, which has been widely used in research [19,20]. As shown Fig. 1, the burner structure consists of three key components: 1) a 12.7 mm central tube designed for the oxygen and nitrogen gases, 2) a 30 mm intermediate annular porous plug for fuel delivery, and 3) a 75 mm outer porous plug used to serve as a shield to avoid secondary flames forming with ambient air. The burner was mounted on a vertical translation platform with a precision of  $\pm 0.005$  mm, allowing for accurate control of the soot sampling position. The experiments were conducted at ambient pressure and a room temperature of  $20^{\circ}\text{C}$ . The gas flow rates of O<sub>2</sub>, N<sub>2</sub>, and shielding N<sub>2</sub> were set to 0.52 L/min, 0.6 L/min, and 55 L/min, respectively. Additionally, a commercial fuel delivery system (Bronkhorst) was employed to continuously provide vaporised fuel with Ar (99.999 %) carrier to the burner through heated tubes maintained at  $200^{\circ}\text{C}$ . The flow rates of both fuel and Ar were regulated using digital flow controllers (Bronkhorst), with precisions of 0.02 % and 0.2 %, respectively.

Considering OME<sub>3</sub>'s fast combustion speed, high cetane number, and tendency to increase NO<sub>x</sub> emissions, its typical blending ratio in diesel engines without major modifications is usually kept below 30 % to maintain engine performance and emission compliance [21,22]. Given several studies investigated 10 % and 20 % OME<sub>3</sub> blending ratios [23,24]. Using the same blending ratios in this study contributes to a more comprehensive understanding of OME<sub>3</sub>'s impact by integrating findings from different perspectives, leading to a broader evaluation of its combustion and emission characteristics. Therefore, here, 10 % and 20 % OME<sub>3</sub> blending ratios (by substituting 10 % and 20 % of the total carbon content of *n*-heptane) were selected to explore the effects of OME<sub>3</sub> addition on soot particles, which designated as OME-10 and OME-20. After adding the OME<sub>3</sub>, the overall vaporised fuel flow rate of carbon remains nearly constant. Table 1 provides the specific flow rates used in this study. The same approach was widely utilised for the analysis of other alternative fuels [25,26].

### 2.2. Soot sampling

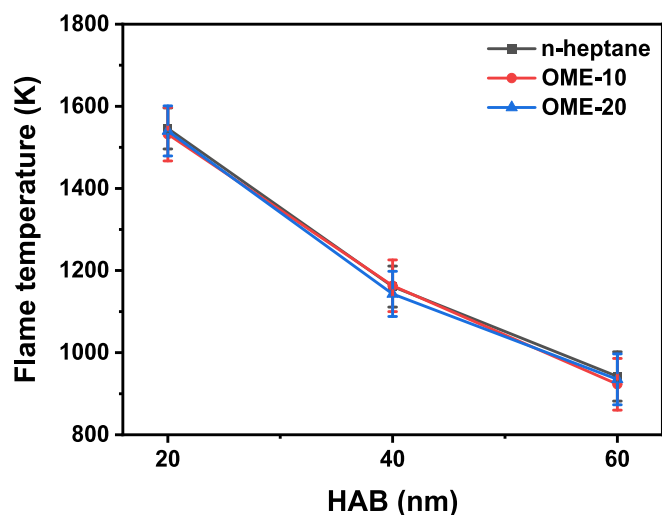
As shown in Fig. 1, the stainless-steel probe sampler with a 0.15 mm sampling orifice downward to the flame was positioned horizontally directly above the flame. The sampling positions were the central axis of the flame with different HABs of 20, 40, and 60 mm, a Teflon filter was used to collect the samples used for TGA. To stopping subsequent chemical reactions during sampling, a cold nitrogen gas with 26.8 L/min flow rate was employed to cool and dilute the extracted gases. Further details on the probe sampling technique can be found in our previous studies [27–29]. After sampling sufficient soot particles, the samples were carefully gathered from the filter. Furthermore, the thermophoretic sampling method was employed to collect soot particles for the high-resolution transmission electron microscopy (HRTEM) analysis. This system was equipped with a linear electric cylinder (FESTO) with an acceleration above  $100\text{ m/s}^2$  and a top speed of 3 m/s, and the sampling time of soot particle was within 30 ms. The rapid sampling time can more accurately reflect the morphology of soot particles in the flame. In addition, the flame temperatures at different HABs were measured by an R-type thermocouple along the flame central axis. The recorded temperatures were corrected for radiative heat loss following the method outlined by Mcenally et al. [30]. Fig. 2 displays the measured temperatures at the three sampling locations. It can be seen that the difference in flame temperature was minimal after adding OME<sub>3</sub>, indicating that the influence of OME<sub>3</sub> addition on combustion temperature is negligible.



**Fig. 1.** Schematic diagram of experiment system.

**Table 1**  
Parameters settings in the test.

| Fuel  | <i>n</i> -heptane | OME-10 | OME-20 |
|---|-------------------|--------|--------|
| Flow rate of N <sub>2</sub> (L/min)         | 0.31              | 0.31   | 0.31   |
| Mass flow rate of <i>n</i> -heptane (g/min) | 1.17              | 1.05   | 0.93   |
| Mass flow rate of OME <sub>3</sub> (g/min)  | 0                 | 0.22   | 0.44   |
| Carbon flow rate (g/min)                    | 0.98              | 0.98   | 0.98   |
| Flame height (mm)                           | 70                | 68     | 65     |



**Fig. 2.** Flame temperatures of different sampling positions.

### 2.3. Soot characterization

### 2.3.1. High-resolution transmission electron microscopy (HRTEM)

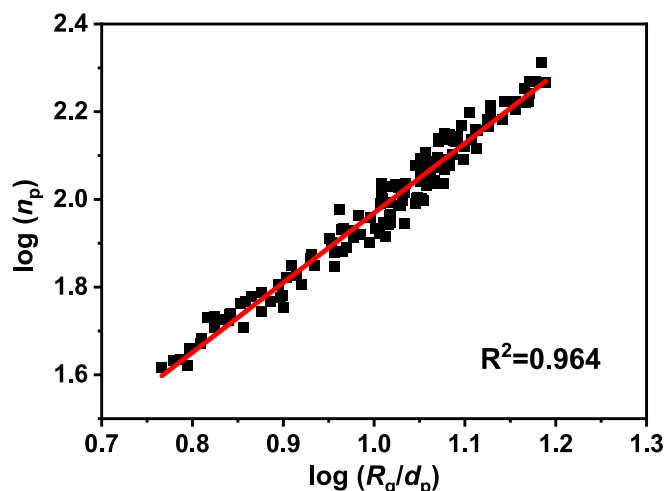
To explore soot morphology and nanostructure, HRTEM (EM-2010F) with magnification of 40,000 $\times$  and 400,000 $\times$  was employed. The TEM were used to determine the morphology parameters, including the number of primary particles ( $n_p$ ), mean radius of gyration ( $R_g$ ), and primary particle size ( $D_p$ ), to calculate the fractal dimension ( $D_f$ ). Taking the *n*-heptane soot at HAB = 20 mm as an example, the  $D_f$  was obtained

from the slope of the scatter plot generated with  $\log(R_g/D_p)$  on the x-axis and  $\log(n_p)$  on the y-axis, as shown in Fig. 3. For each sampling HAB, more than 100 soot aggregates were selected to ensure statistical significance.

HRTEM images were employed to analyse nanostructure parameters, including fringe length ( $L_f$ ), fringe tortuosity ( $T_f$ ) and separation distance ( $S_f$ ) using an automated fringe image processing system (FIPS). This FIPS involves image normalisation, selection of the region of interest, segmentation, enhancement, application of a Gaussian low-pass filter, binary conversion, skeletonisation, and calculation of the nanostructure parameters. Details of the image program are described in [31]. As shown in Fig. 4, the  $L_f$  was determined by converting the pixel count of each fringe to length based on a pixel size. The  $T_f$  was calculated as the ratio between the  $L_f$  and the distance connecting two endpoints. The  $S_f$  was determined by averaging the separation distances between the nearest points of each fringe pair.

### 2.3.2. Thermogravimetric analysis (TGA)

The oxidative reactivity of soot particles was evaluated using oxidative characteristic temperatures and activation energy ( $E_a$ )



**Fig. 3.** Plot  $\log(n_p)$  vs.  $\log(r_g/d_p)$  of *n*-heptane soot sample.

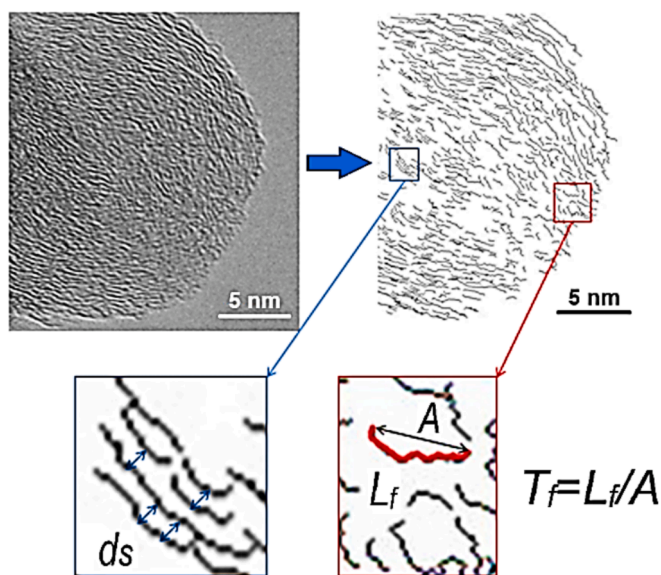


Fig. 4. Definition of soot nanostructure parameters.

through a thermogravimetric analyzer (TGA, Mettler-Toledo DSC1). The  $T_p$  is defined as the temperature when soot reaches its maximum oxidation rate during the temperature-programmed oxidation process at atmospheric pressure, and  $T_b$  is the temperature that 90 % soot mass is lost. The  $E_a$  reflects the minimum energy required for the reactants to transition from a stable state to an activated state, and the detailed process for calculating the  $E_a$  was reported in our previous work [32,33]. Before the experiment, the soot sample was heated to 773 K and maintained at this temperature for 60 min under a nitrogen atmosphere with a flow rate of 60 ml/min. After the temperature lowered to 473 K, soot sample was subjected to heating with a heating rate of 5 K/min to 1073 K in an air environment, maintained at a flow rate of 60 ml/min. In this study, the test of each sampling point was repeated three times to reduce experimental error.

### 3. Results and discussion

#### 3.1. Size of primary particles

Fig. 5 shows the  $D_p$  under different HABs and OME<sub>3</sub> substituting proportions. It is evident that when HAB < 40 mm, the  $D_p$  for all soot samples exhibits an upward trend as the HAB increases. Conversely, when HAB > 40 mm, the  $D_p$  decreases with further increases in HAB.

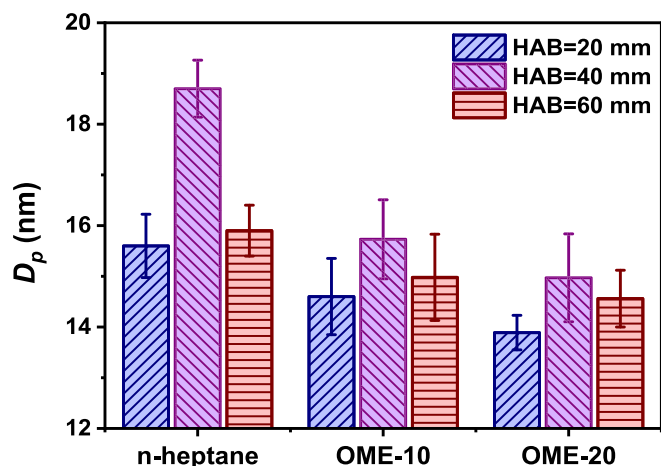


Fig. 5. Mean size of primary particles ( $D_p$ ) from soot samples.

This phenomenon can be explained by the development stages of primary soot particles, which transition from a soot growth-dominant phase and an oxidation-dominant phase. The final diameter of the primary soot particles is the result of a competition between soot growth and oxidation [34]. During the soot growth-dominant phase, the growth rate of soot exceeds the oxidation rate, leading to an increase in the primary particle diameter. Conversely, during the oxidation-dominant phase, the oxidation rate surpasses the growth rate, causing a gradual reduction in the primary soot particle diameter. Therefore, based on the variation in particle size at different HABs, it can be inferred that soot growth is the dominant process when HAB increases from 20 mm to 40 mm. However, as the HAB further elevates from 40 mm to 60 mm, longer residence time of soot in flame makes oxidation becomes the prevailing process.

In addition, with the increase of OME<sub>3</sub> substituting proportion, the  $D_p$  of samples at the same HAB gradually decrease. The  $D_p$  range decreases from 15.6–18.7 nm to 13.9–15.0 nm when OME<sub>3</sub> substituting proportion increases from 0 to 20 %. This phenomenon indicates that the addition of OME<sub>3</sub> could distinctly reduce the size of primary soot particles. This variation may be mainly attributed to differences in soot formation and oxidation caused by the addition of OME<sub>3</sub>. On the one hand, the higher oxygen content in OME<sub>3</sub> increases the air/fuel stoichiometric ratio for combustion, promoting more complete combustion and the formation of smaller soot precursors, such as acetylene or polycyclic aromatic hydrocarbons (PAHs), which subsequently inhibit the growth of soot particles [35]. On the other hand, the addition of OME<sub>3</sub> facilitates the formation of more oxygenated functional groups on soot surfaces, which accelerates the oxidation of soot particles and reduces the size of primary particles [36,37]. The primary soot particle with smaller  $D_p$  has a relatively large specific surface area which provides more active sites, thereby contributing to improving the oxidative reactivity [38]. Furthermore, the reduction in  $D_p$  increases the probability of the carbon layer collapsing into shorter fringes, which become intertwined with amorphous carbon, ultimately facilitating exfoliation, layer delamination, or internal combustion, contributing to the oxidation of soot particles [39]. Therefore, the small primary soot particles generated by OME<sub>3</sub>-containing fuels would have higher oxidative reactivity.

Although the smaller size of soot particles is more susceptible to oxidation, it is worth noting that these smaller soot particles may also exhibit increased toxicity and pose serious harm to human health. This is primarily attributed to the enhanced capacity of smaller soot particles to promote the formation of reactive oxygen species (ROS) in both acellular and cellular environments, subsequently leading to oxidative stress [40]. Gren et al. [41] found that primary soot particles with a diameter less than 16 nm exhibit approximately 10 times the ROS formation potential compared to particles with a diameter above 20 nm. This significant difference is because smaller particles correspond to larger surface area, promoting the generation of free radicals, thus inducing oxidation stress, inflammation and enhancing genotoxicity [42,43]. Moreover, smaller soot particles can deposit more into the alveoli and further spread and penetrate distal organs through the bloodstream [44]. In addition, due to their reduced size, these particles are less likely to be effectively targeted and cleared by alveolar macrophages, leading to prolonged retention in the lungs and higher localised concentrations [45]. Consequently, the smaller soot particles caused by the addition of OME<sub>3</sub> may pose more significant risks compared to soot particles from pure petroleum fuels.

#### 3.2. Fractal dimension

The  $D_f$  is typically used to quantify the compactness of soot aggregates. A higher  $D_f$  value indicates a more compact structure of soot aggregate, while a lower  $D_f$  value suggests a looser structure [32,40]. The  $D_f$  of soot samples with different HABs and OME<sub>3</sub> substituting proportions are displayed in Fig. 6. It can be seen that the  $D_f$  of soot



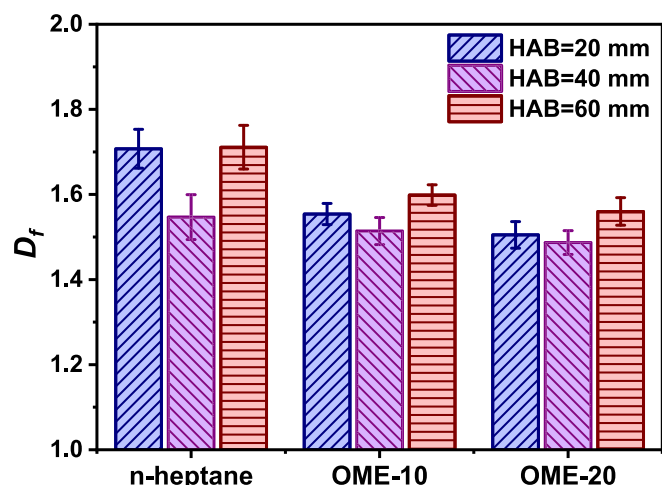


Fig. 6. Fractal dimension ( $D_f$ ) of soot samples.

particles from all soot samples decreases initially and then increases with increasing HAB. This interesting phenomenon suggests that the degree of soot aggregation undergoes a decreasing and then increasing change as the HAB increases. This phenomenon can be attributable to the fact that, at lower HABs, the shorter residence time of soot within the flame is not conducive to the formation of chain-like structures [46]. As the HAB elevates to 40 mm, the continued coagulation of primary soot particles promotes the formation of more long-chain soot agglomerates. Furthermore, the decrease in flame temperature with increasing HAB further suppresses the agglomeration of soot particles, causing a decrease in  $D_f$  [47]. When the HAB is elevated to 60 mm, despite the further reduction in flame temperature, the soot aggregates undergo a longer residence time in the flame, allowing for a higher degree of agglomeration among the soot particles [48].

In addition, it can be seen from Fig. 6 that the  $D_f$  of soot aggregate from *n*-heptane varies within the range of 1.547 to 1.711 as the HAB changed, while the range of OME-20 only is 1.487 to 1.560. The gradual decrease in  $D_f$  with the addition of OME<sub>3</sub> indicates that the soot aggregates formed from OME<sub>3</sub>-containing fuel have a looser structure. The reduction in  $D_f$  caused by the introduction of OME<sub>3</sub> can be explained by the following aspects. First, the soot particles generated from blending OME<sub>3</sub> have relatively smaller  $D_p$ . According to the diffusion-limited agglomeration mechanism, the soot particles with small sizes exhibit more pronounced Brownian motion. This increases the random motion of soot particles during the diffusion process prevents them from stacking in a tightly packed manner, leading to the formation of a looser agglomerate structure [49]. Moreover, smaller particles tend to be subjected to weaker van der Waals forces, making them more tend to form loose structures upon collision [50]. As looser aggregate structures typically exhibit larger specific surface area and more active sites, the soot aggregates generated by OME<sub>3</sub>-containing fuel have higher oxidative reactivity [51,52].

It is worth noting that, soot also acts as an efficient absorbing medium, with its absorption–emission heat exchange capacity closely related to the  $D_f$  [53,54]. Liu et al. [55] found that as soot aggregates  $D_f$  decreases, their scattering cross-section significantly reduces. This reduction is caused by the looser chain-like structure of the aggregates, which weakens scattering interaction among soot particles. As a result, the smaller scattering cross section of soot implies a reduced capacity to reflect solar radiation, leading to more heat reach the earth's surface [56]. Thus, soot particles generated from OME<sub>3</sub>-containing fuels, with the smaller  $D_f$ , may have weaker scattering capacity, potentially increasing solar radiation and contributing to climate warning.

### 3.3. Soot nanostructure

HRTEM analysis was conducted to illuminate the effects of OME<sub>3</sub> on soot nanostructure. Fig. 7 presents representative morphology images of *n*-heptane and *n*-heptane/OME<sub>3</sub> soot samples. As far as HRTEM images are concerned, the fringe are actually projections of graphene layers, and thus the fringe characteristics reflect the properties of graphene layers [57].

To quantify the changes of soot nanostructure following the addition of OME<sub>3</sub>, the  $L_f$ ,  $T_f$ , and  $S_f$  were calculated through lattice fringe analysis [33]. Fig. 8 shows the mean values of  $L_f$ ,  $T_f$ , and  $S_f$  for different soot samples. From Fig. 8a, the  $L_f$  of *n*-heptane soot increases from 0.711 nm to 1.131 nm with an increase in HAB from 20 mm to 60 mm. However, the range of  $L_f$  reduces to 0.581–0.829 when the OME<sub>3</sub> substituting proportion achieved 20 %, indicating the blending of OME<sub>3</sub> would suppress the growth of the fringe length. This phenomenon is likely attributed to the changes in  $sp^3$  and  $sp^2$  orbital hybridisation development within the internal structure of soot particles. Ferraro et al. [58] and our previous research [59] found that the incorporation of OME<sub>3</sub> increases the proportion of  $sp^3$  hybridisation within soot particles. The  $sp^3$ -hybridised C atoms represent defect sites that can disrupt the  $sp^2$ -hybridised network, leading to a reduction in long-range order, which in turn results in a decrease in fringe length [37,60]. The graphene layers are composed of carbon atoms situated at basal plane and edge positions. The edge carbon atoms exhibit significantly higher reactivity than those in basal plane [61]. Generally, shorter fringes which means smaller graphene layers have a higher proportion of edge-positioned carbon atoms, resulting in the high oxidative reactivity. Furthermore, it was found that the  $L_f$  of all soot samples increased as the HAB elevated from 20 mm to 60 mm. The gradually growth of fringe length with elevating HAB are likely due to the longer residence time in flame and relatively lower flame temperatures at higher HAB [62]. A longer residence time promotes the hydrogen abstraction carbon addition reaction on soot surface, resulting in the growth of fringe length [63]. At the same time, a lower flame temperature slows down soot oxidation, leading to an increase in the  $L_f$  of all soot samples [62].

Fig. 8b depicts the  $T_f$  of soot samples. It can be seen that the  $T_f$  of *n*-heptane soot samples at different HABs is in the range of 1.366–1.291. As the OME<sub>3</sub> content increases to 20 %, the  $T_f$  range of soot particles increases to 1.445–1.345. This phenomenon may be attributed to the effects of OME<sub>3</sub> on forms of carbon atom in soot particles. In ideal graphite microcrystalline layers, the carbon atoms are in the form of a six-membered ring lamellar structure [64]. However, in practice, due to differences in the generation environments, gas phase components, and reaction pathways, a certain amount of odd-number carbon rings would form during the generation of soot particles, which lead to a certain curving of the microcrystalline layer [65,66]. The curved fringes facilitate the overlapping of electronic orbitals, increasing the C–C bond strain and weakening electronic resonance stabilisation, thereby making the C atoms more vulnerable to oxygen [67]. That is, the increase in fringe tortuosity of soot particles generally leads to higher oxidative reactivity. Furthermore, as illustrated in Fig. 8b, with the increase in HAB, the  $T_f$  of all soot samples shows a decreasing trend. According to the analysis presented in Section 3.1, this trend can be attributed to the progressive dominance of oxidation at higher HABs. Fringes with higher tortuosity exhibit reduced electronic resonance stabilisation, which renders them more susceptible to consumption during the oxidation phase [31,68]. Consequently, as the oxidation process dominates, the overall fringes gradually become a flatter with increasing HAB, thereby contributing to a reduction in  $T_f$ .

Fig. 8c displays the  $S_f$  variations of different soot samples with various OME<sub>3</sub> substituting proportions and HABs. The  $S_f$  range increases from 0.423–0.373 nm for *n*-heptane to 0.531–0.472 nm for OME-20 soot, suggesting that the soot transforms toward a more disordered structure after adding OME<sub>3</sub>. This phenomenon is likely related to the reduction in  $L_f$  following the addition of OME<sub>3</sub>. The  $L_f$  in HRTEM images reflects the

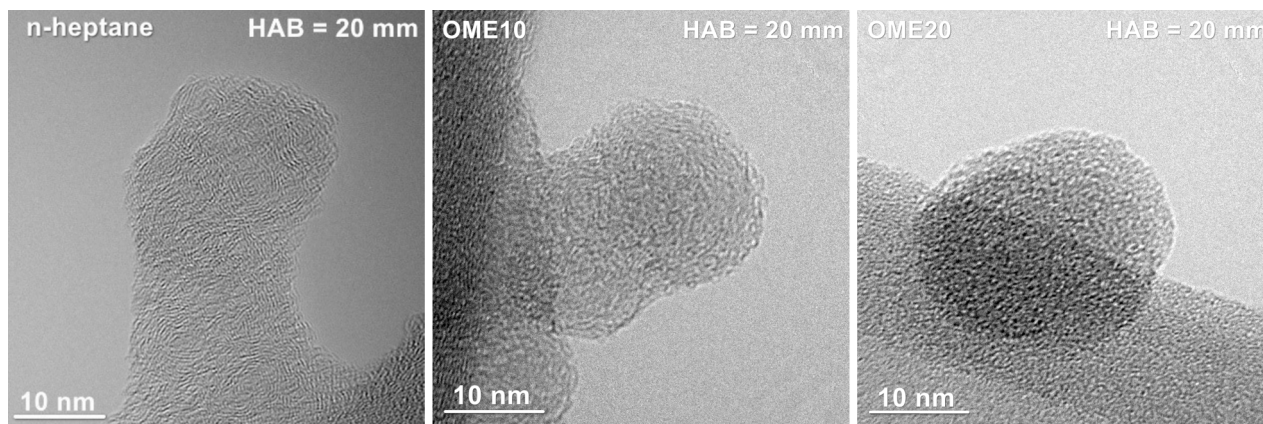


Fig. 7. Representative HRTEM images of *n*-heptane and *n*-heptane/OME<sub>3</sub> soot samples.

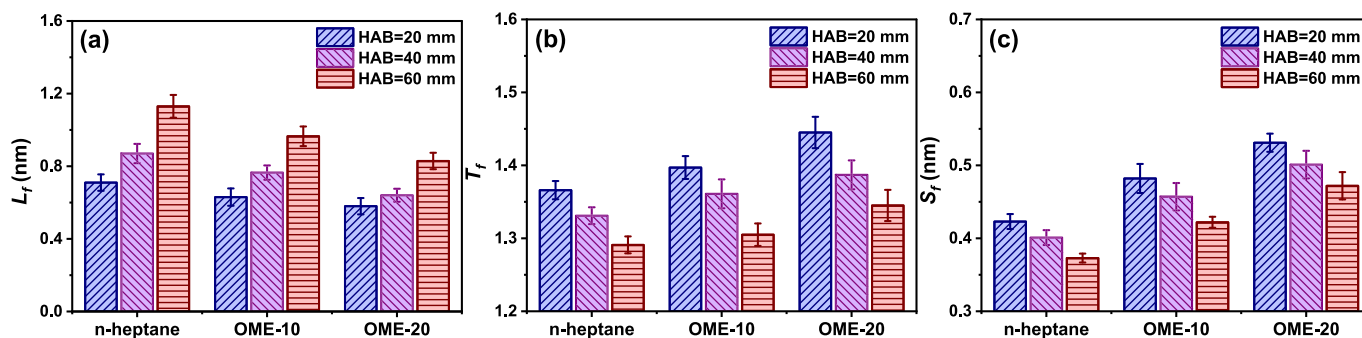


Fig. 8. Mean fringe length ( $L_f$ ), fringe tortuosity ( $T_f$ ) and separation distance ( $S_f$ ) of soot samples.

size of the microcrystalline layer, with shorter  $L_f$  indicating smaller microcrystalline layer size in soot samples. The addition of OME<sub>3</sub> decreases the  $L_f$ , and the resulting smaller size of microcrystalline layers weakens the Van der Waals forces between layer planes, resulting in the increase of separation distance [69]. During the oxidation process of soot particles, gases diffuse through the continuous domains between microcrystalline layers. The larger interlayer spacing between these microcrystalline layers would reduce the resistance to gas diffusion and facilitate the diffusion of O<sub>2</sub> to the active sites, thereby the increased  $S_f$  caused by adding OME<sub>3</sub> favors the oxidation of soot particles [61,70]. In addition, when the HAB increased from 20 to 60 mm, the  $S_f$  of all soot samples presents a similar decreasing trend. This phenomenon suggests that the soot samples transform towards a more ordered structure with increasing residence time of soot in flame. This is likely because, with prolonged residence time, the  $L_f$  continues to increase, enhancing the interlayer forces between layers and bringing them closer together.

To comprehensively compare the nanostructural characteristics, the histograms and Gaussian fitting curves of the distributions of  $L_f$ ,  $T_f$  and  $S_f$  were also analysed for soot samples at HAB = 20 mm. Fig. 9 shows the distribution characteristics of nanostructural parameters for *n*-heptane and *n*-heptane/OME<sub>3</sub> soot samples, where the bin widths are 0.1 nm for the  $L_f$  distribution, 0.05 for the  $T_f$  distribution and 0.0125 nm for the  $S_f$  distribution. Overall, the trend of peak variations for  $L_f$ ,  $T_f$  and  $S_f$  distribution are similar to that of their mean values. Specifically, the  $L_f$  distribution of all soot particles is in the range of 0–2 nm, with approximately 75 % of the  $L_f$  in *n*-heptane soot particles being less than 0.8 nm. As the OME<sub>3</sub> blending ratio increases, the  $L_f$  distribution shifts toward shorter sizes, and about 75 % of the crystalline lengths are smaller than 0.7 nm for OME-20 soot particles. The  $T_f$  distribution is in the range of 0.8–2 for all soot particles. As the OME<sub>3</sub> blending ratio increases, the peak of the  $T_f$  distribution shows an increasing trend. The  $S_f$  distribution of soot particles shows significantly change with adding

OME<sub>3</sub>. The  $S_f$  distribution of *n*-heptane soot particles concentrated in the range of 0.35–0.55 nm, while that of OME-20 soot particles is concentrated in the range of 0.45–0.6 nm.

### 3.4. Oxidative reactivity

The results obtained from HRTEM analysis demonstrated that the blending of OME<sub>3</sub> resulted in a reduction in  $D_p$ ,  $D_f$  and  $L_f$  and an increase in  $T_f$  and  $S_f$ . These changes in physical properties are likely to enhance the oxidative reactivity of soot particles [63,65,66]. To further validate the influence of changes in soot physical properties on oxidative reactivity, the  $T_p$ ,  $T_b$ , and  $E_a$  obtained from TGA analysis were employed to evaluate the oxidative characteristics of soot samples.

Fig. 10 illustrates the  $T_p$  and  $T_b$  values for soot samples. Both  $T_p$  and  $T_b$  decrease with increasing OME<sub>3</sub> substituting proportion. The maximum reductions of the  $T_p$  and  $T_b$  reach 28.6 °C and 36.4 °C, respectively, at HAB = 60 mm following the addition of OME<sub>3</sub>. The lower  $T_p$  and  $T_b$  values suggest that the blending of OME<sub>3</sub> increases the soot oxidative reactivity, and lowers the difficulty of achieving soot oxidative removal, both of which are beneficial to the regeneration of deposited soot in DPF. Consequently, the addition of OME<sub>3</sub> can reduce the fuel required for active DPF regeneration and improve fuel economy.

In parallel, a decrease in the  $E_a$  as depicted in Fig. 11, clearly demonstrates the effect of OME<sub>3</sub> on enhancing oxidative reactivity of soot particles. Specifically, at HAB = 20 mm, the  $E_a$  reduction after 20 % addition of OME<sub>3</sub> reaches 7.7 %. The maximum reduction is observed at HAB = 60 mm, with  $E_a$  decreasing by 14.6 %. These results further confirm that the physical properties variations of soot particles, such as  $D_p$ ,  $D_f$ ,  $L_f$ ,  $T_f$  and  $S_f$ , induced by the introduction of OME<sub>3</sub>, contribute to the enhancement in oxidative reactivity. In addition, the enhanced soot reactivity and oxidation behaviour difference have direct implications for diesel particulate filter (DPF) performance. The increased reactivity

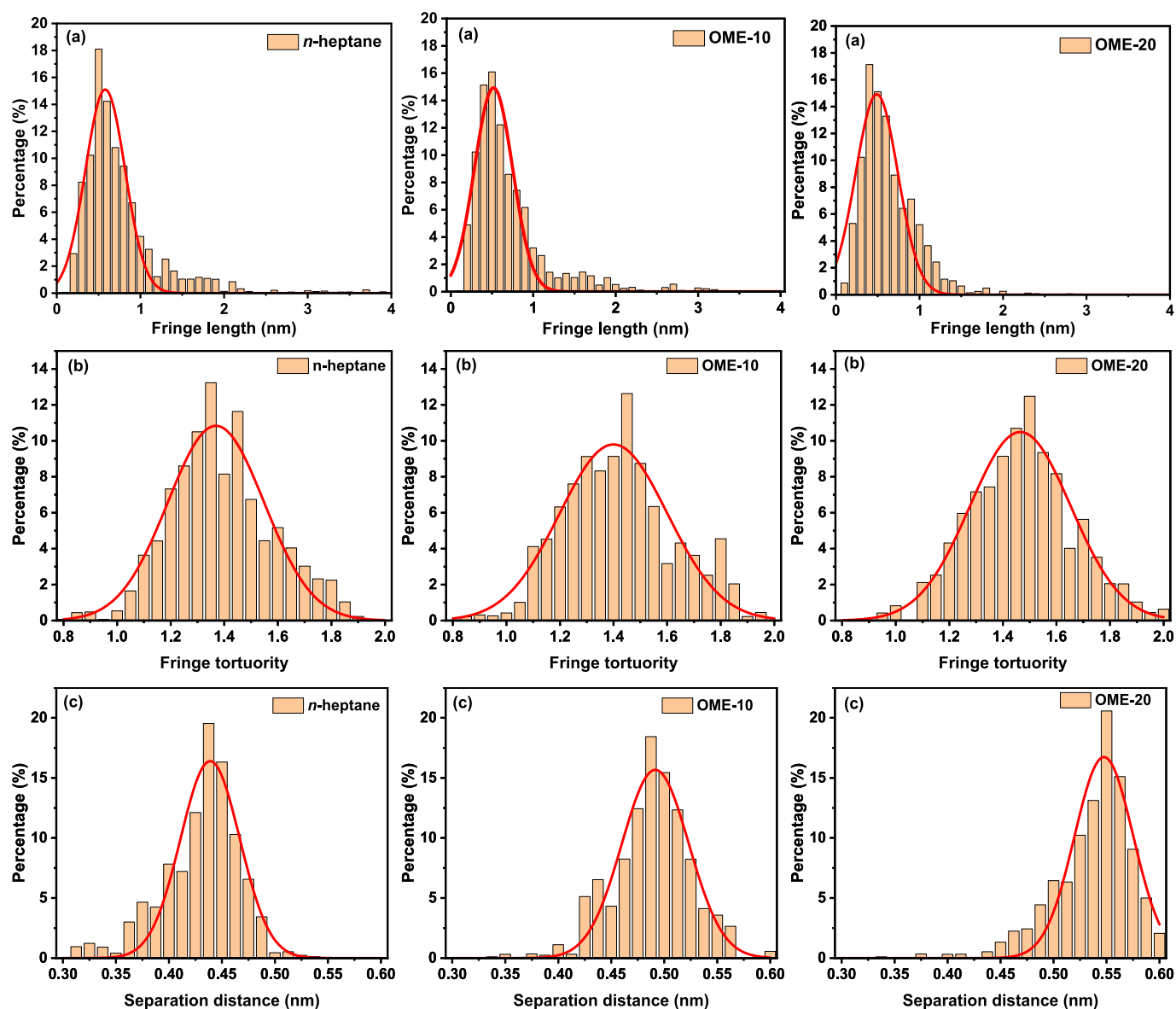


Fig. 9. Histograms of fringe length ( $L_f$ ), fringe tortuosity ( $T_f$ ) and separation distance ( $S_f$ ) of soot samples at HAB = 20 mm.

suggests that soot from OME<sub>3</sub>-containing fuels may oxidise more readily, potentially improving DPF regeneration efficiency. This could enable better regeneration temperatures or shorter regeneration cycles, leading to reduced fuel consumption and extended DPF lifespan.

#### 4. Conclusions

To clarify the effects of OME<sub>3</sub> addition on the physical properties and oxidative reactivity of soot particles, high-resolution transmission electron microscopy (HRTEM) and thermogravimetric analysis were used to explore the primary particle size, fractal dimension ( $D_f$ ), fringe length ( $L_f$ ), tortuosity ( $T_f$ ), separation distance ( $S_f$ ), and oxidative characteristics of *n*-heptane and *n*-heptane/OME<sub>3</sub> soot particles. The main conclusions of this study can be summarised as follows:

- The addition of OME<sub>3</sub> distinctly reduces the size of primary soot particles. Although the smaller size of soot particles promotes oxidation, they increase the likelihood of prolonged retention in the lungs, promoting oxidative stress, and thereby posing greater health risks.

- Soot aggregates from OME<sub>3</sub>-containing fuels exhibit a smaller  $D_f$  than compared to those from *n*-heptane, which reduces the scattering capacity of soot particles, allowing more solar radiation to penetrate and potentially contributing to climate warming.
- The addition of OME<sub>3</sub> results in a reduction in  $L_f$  and an increase in  $T_f$  and  $S_f$ . These variations in soot nanostructure enhance oxidative reactivity, as indicated by lower oxidative characteristic temperatures and reduced activation energy. This indicates that adding OME<sub>3</sub> can facilitate more efficient regeneration of diesel particulate filters (DPF).

#### CRediT authorship contribution statement

**Ye Liu:** Writing – original draft, Visualization, Project administration, Methodology, Investigation, Formal analysis, Data curation, Conceptualization. **Ran Zhang:** Writing – review & editing, Resources. **Chenxi Wang:** Writing – review & editing, Visualization, Methodology, Investigation, Data curation, Conceptualization. **Haibo Chen:** Project administration, Funding acquisition. **Gang Lyu:** Writing – review & editing, Project administration. **Jun Wang:** Writing – review & editing. **Huayu Tian:** Data curation. **He Yang:** Data curation. **Yajun Wang:**

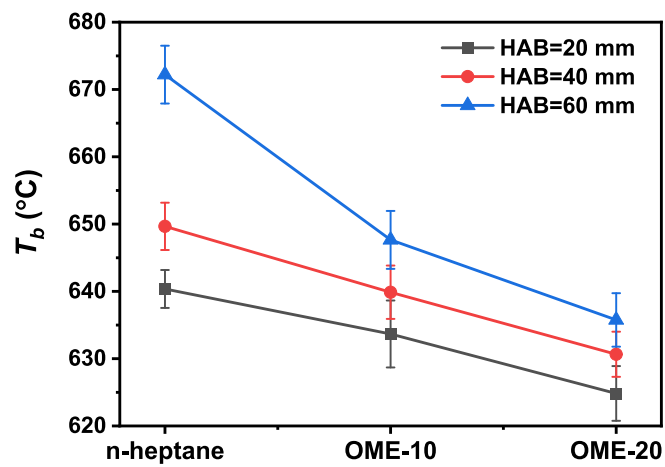
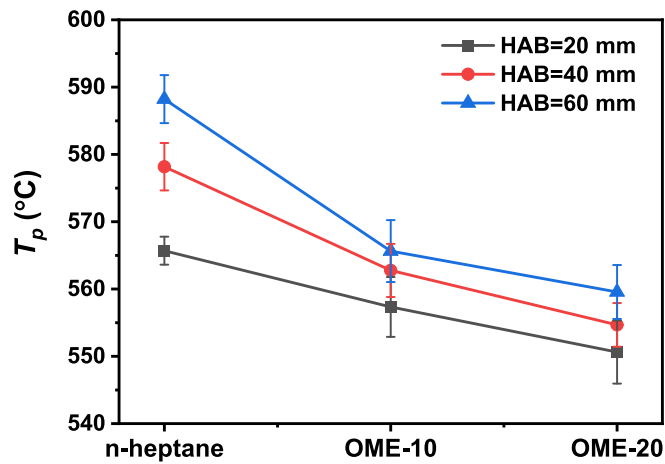


Fig. 10. Peak and burnout temperatures of soot samples.

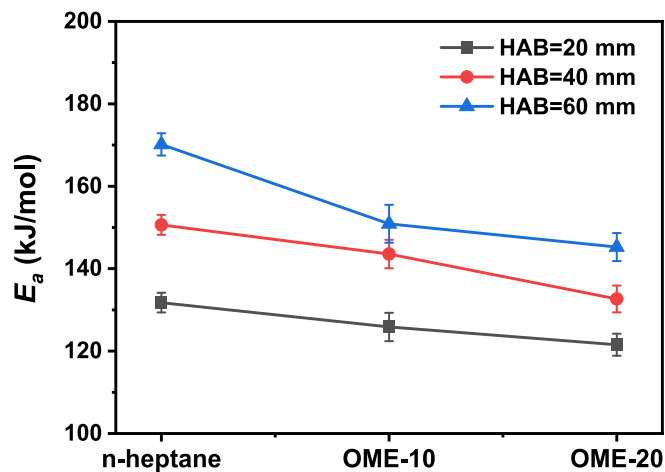


Fig. 11. Activation energy ( $E_a$ ) of soot samples.

Writing – review & editing. **Chenyang Fan**: Writing – review & editing. **Bin Xu**: Writing – review & editing. **Xiaowei Wang**: Visualization, Investigation. **Hongyuan Wei**: Visualization, Investigation. **Dimitris Margaritis**: Writing – review & editing.

## Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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## Data availability

The authors do not have permission to share data.

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