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# Micro-scale graded electrodes for improved dynamic and cycling performance of Li-ion batteries

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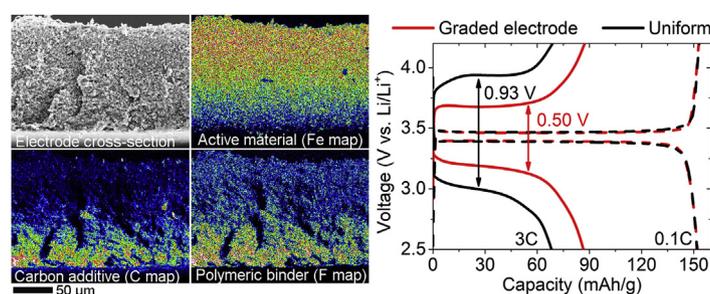
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## HIGHLIGHTS

- Composition graded cathodes are fabricated by a layer-by-layer spray printing method.
- Micron-resolution distribution of electrode components across thickness is realized.
- C-rate performance and degradation are improved due to gradient material distribution.
- Graded cathodes have lower charge transfer resistance and polarization than uniform.
- This technique is feasible for large area, fast production.

## GRAPHICAL ABSTRACT



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## ABSTRACT

Li-ion battery cathodes based on LiFePO<sub>4</sub> are fabricated by a layer-by-layer spray printing method with a continuous through thickness gradient of active material, conductive carbon, and binder. Compared with cathodes with the more usual homogeneous distribution, but with the same average composition, both C-rate and capacity degradation performance of the graded electrodes are significantly improved. For example at 2C, graded cathodes with an optimized material distribution have 15% and 31% higher discharge capacities than sprayed uniform or conventional slurry cast uniform cathodes, and capacity degradation rates are 40–50% slower than uniform cathodes at 2C. The improved performance of graded electrodes is shown to derive from a lower charge transfer resistance and reduced polarization at high C-rates, which suggests a more spatially homogeneous distribution of over-potential that leads to a thinner solid electrolyte interphase formation during cycling and sustains improved C-rate and long-term cycling performance.

## 1. Introduction

Improvements in the power, energy density, and lifetime of lithium ion batteries are critical for their greater penetration of electric vehicle markets [1]. While much effort continues to be made in searching for new materials, or the chemical modification/decoration of existing materials [2,3], less attention has been paid to radical approaches to

electrode engineering that includes more careful control of the electrode structure [4]. Research into these structured electrodes has however strengthened in recent years, including detailed optimization of the fraction of each electrode constituent, layered electrodes, and optimized and/or directional porosity distributions [5–7]. This growing interest is driven by the desire to overcome the conventional constraints placed on electrode microstructural design when manufacture is

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restricted to slurry casting only [5,8], and which include: increasing the fraction of conductive additive to reduce electrode impedance by which sacrifices gravimetric energy density [9]; increasing electrode porosity to facilitate lithium ion transfer by which sacrifices volumetric energy density [10,11]; and using thinner electrodes to improve sluggish ion transfer kinetics by which reduces the overall energy density because it increases the current collector weight fraction [12,13]. When alternative manufacturing routes are available that allow for control over pore channel direction through the thickness of the electrodes, for example by magnetic guided templating [6], or magnetic particle alignment [4], ion transport and electrode kinetics can be significantly improved due to the reduced tortuosity of lithium ion pathways [4,6,14,15]. Similar aligned pore channels in electrodes have also been realized by ice-templating [16–18] or co-extrusion followed by sintering [14]. However, these improvements rely on relatively sophisticated manufacturing techniques that may be, in some cases, limited to the laboratory scale, or too expensive for industrialization.

Graded electrodes with a continuous or layered distribution of microstructure and functionality through the electrode thickness may circumvent conventional microstructural design restrictions, but have been explored primarily only through modelling and simulation due to the lack of corresponding practical manufacture techniques [19–21]. Some predictions have been discouraging for graded porosity electrodes, with only marginal forecast improvements in energy density when compared with constant porosity electrodes [20], or only a marginal decrease in electrode resistance [19]. However, simulations have also predicted more uniform overpotential distributions through the electrode thickness [19], and a reduction of ohmic heat generation of up to 14% [21]. If realized in practice, both effects may mitigate battery degradation during long-term cycling. Recent work on two-layer graded porosity cathodes also showed reduced capacity fade of approximately 8% in full-cells and 5% in half-cell configuration over 50 cycles [22].

Graded electrode designs need not be restricted to spatial variations in porosity only. Composition variations may also provide improvements in some aspects of electrode and cell performance but are largely unexplored, especially by experiment.

In this paper we use a large area, layer-by-layer spray printing approach [7,23–26] to fabricate compositionally graded lithium-ion battery cathodes based on  $\text{LiFePO}_4$  that have a micro-scale continuous gradation through the electrode thickness of active material, carbon electron conductive additive, and polymer binder fraction. C-rate performance and capacity degradation is compared with equivalent homogeneous electrodes made by spray printing and by industry-standard slurry casting. Critically, all electrodes are fabricated with an identical average composition ratio of active material:carbon:binder of 80:10:10 (wt.%), and had similar thickness, overall porosity, and active material loading per area in order to isolate the effect of material distribution only on electrode performance.

## 2. Experimental

### 2.1. Spray printing apparatus

The layer-by-layer spray printing equipment has been developed over several years [7,23–26] and is shown schematically in Fig. 1. An industrial spray nozzle was attached to a stiff x-y-z linear manipulator gantry in which the position and speed of the nozzle was precisely controlled by computer. A mixture of the electrode materials suspended/dissolved in a liquid (suspension A) was pumped into the nozzle at a controlled volumetric flow rate by a peristaltic pump. The suspension was continuously atomized by compressed air (e.g. 0.4 bar) and the resulting spray of suspension droplets deposited as a well-focused spray cone onto a metallic foil current collector placed on a constant temperature heated vacuum chuck at typically 140 °C so that the liquid fraction of the spray evaporated almost instantaneously. The

electrode formed incrementally layer-by-layer with each pass, or cycle, of the spray nozzle.

### 2.2. Suspension preparation

The gradient distribution of materials within the electrode was realized by continuously changing the composition of suspension A, by mixing it with suspension B as deposition proceeded. Table 1 shows the experimental conditions for seven different types of  $\text{LiFePO}_4$ -based cathodes with different material distributions, where  $\text{LiFePO}_4$  and Super-P carbon black were obtained from MTI (USA); PVDF (polyvinylidene fluoride, Mw ~ 534,000) binder, NMP (1-Methyl-2-pyrrolidinone,  $\geq 99.0\%$ ), and IPA (2-propanol, 99.5%) were obtained from Sigma-Aldrich (UK).  $\text{LiFePO}_4$  was chosen as a widely available exemplar or “model” material with generic insights on the effects of grading translatable to any similar cathode or anode material.

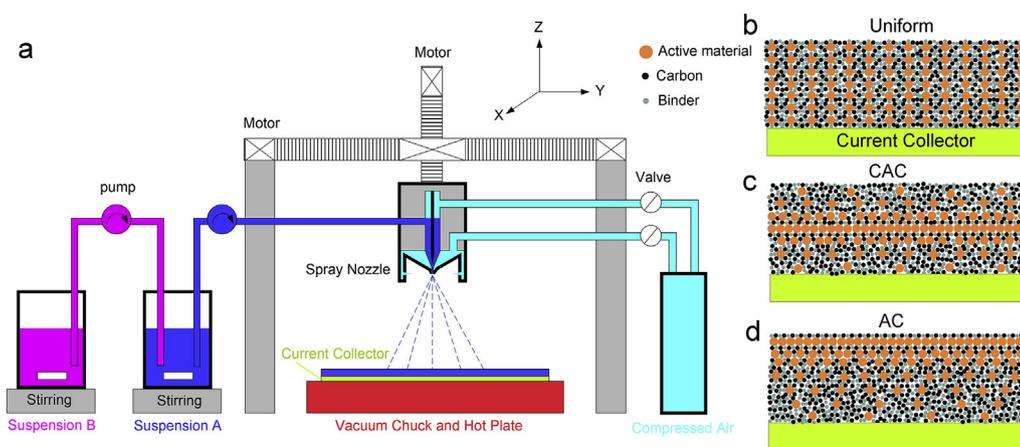
PVDF was first dissolved in NMP with magnetic stirring; in parallel,  $\text{LiFePO}_4$  and Super-P were mixed with IPA by ball milling at 300 rpm for 1 h, and then the two liquids mixed together with stirring. If the suspension did not contain PVDF, only ball milling of the solid material in a mixture of NMP and IPA was conducted. The suspensions were further dispersed by high energy ultrasonication at 20 Hz and 750 W for 2 h (Vibra-cell, Sonics Inc., USA) and then vigorously stirred by magnetic stirring at ~ 800 rpm overnight.

### 2.3. Cathode preparation

For each type of spray printed cathode listed in Table 1 the total weight of solid material within the suspension (suspension A + suspension B) was fixed at 3 g, and the overall weight ratios were kept constant at  $\text{LiFePO}_4$  (AM):Super-P (Carbon):PVDF (Binder) = 80:10:10. The spray nozzle moved in a zig-zag trajectory over the current collector and the active material ( $\text{LiFePO}_4$ ) loading for different electrodes was approximately constant at  $11.4 \pm 1.8 \text{ mg cm}^{-2}$ , measured by a balance (accuracy 0.1 mg, Sartorius, Germany).

For example with reference to Table 1, to fabricate the CAC electrode, which has an active-material-rich region sandwiched by two carbon-rich regions, suspension A in spray step 1 was pumped into the spray nozzle; at the same time, suspension B, in spray step 1, was pumped into suspension A. Due to the difference in weight ratios of the two suspensions, the active material loading in suspension A gradually increased from zero towards 100 wt % as time increased and the fraction of suspension B in A increased, while both the carbon and binder loading decreased from 50 wt% towards zero. Because the overall composition of each sprayed layer related to the instantaneous composition of suspension A, a CA-type graded electrode was realized. Then, suspensions A and B were switched in spray step 2 (see Table 1) so that an AC-type graded electrode formed progressively on top of the CA type electrode, resulting in final CAC-type electrode. As an example, energy-dispersive X-ray spectroscopy (EDX) element mapping of an as-sprayed AC-type electrode was shown in Fig. S1, which confirmed the gradient materials distribution through the thickness of the electrode.

A MATLAB® code was developed (see Supplementary Data) to predict the change of composition ratios through the thickness of electrode by using the data in Table 1 as input, and the calculated ideal composition distributions are plotted in Figs. 2a, 4a and 4b. The final cathode formulation given in Table 1 was fabricated by conventional slurry casting with a doctor blade on the same current collector (Al foil), where the slurry was prepared by ball milling at 300 rpm for 45 min (dry milling for 15 min and wet milling in NMP for 30 min). The height of the doctor blade was adjusted to keep a similar active material loading as the spray printed electrodes. All the cathodes were dried at 60 °C overnight in air before calendaring to a similar thicknesses ( $100 \pm 19 \mu\text{m}$ , measured by a micrometer) with similar porosities of  $51.2 \pm 9.7\%$  and electrode densities of  $1.45 \pm 0.29 \text{ g cm}^{-3}$ , based on measurement of 60 different cathodes used in the coin cell tests.



**Fig. 1.** Illustration of an experimental setup for the fabrication of graded composition electrodes. (a) Experimental arrangement based on a layer-by-layer spray printing approach, featuring the use of two suspensions simultaneously in series with independently controlled pumps to produce fine-scale control of the graded profile. (b–d) Schematic illustration of three types of sprayed electrodes with uniform, CAC gradation and AC gradation, respectively, through the thickness of the electrodes from bottom (next to the current collector) to top (next to the separator), where A denotes the active material-rich region and C denotes carbon black-rich region.

**Table 1**

Experimental conditions for electrodes with different material distributions. Active material (AM) is  $\text{LiFePO}_4$ , carbon refers to Super-P conductivity enhancer, binder is PVDF, NPM is 1-Methyl-2-pyrrolidinone, and IPA is 2-propanol.

Cathode type	Spray step	Suspension A (pumping into spray nozzle)						Suspension B (pumping into suspension A)					
		AM (g)	Carbon (g)	Binder (g)	NMP (mL)	IPA (mL)	Pump rate (mL min <sup>-1</sup> )	AM (g)	Carbon (g)	Binder (g)	NMP (mL)	IPA (mL)	Pump rate (mL min <sup>-1</sup> )
CAC	1	0	0.150	0.150	5	95	9.0	1.200	0	0	5	95	4.5
	2	1.200	0	0	5	95	9.0	0	0.150	0.150	5	95	4.5
CAC@	1	0.240	0.120	0.075	5	95	9.0	0.960	0.030	0.075	5	95	4.5
	2	0.960	0.03	0.075	5	95	9.0	0.240	0.120	0.075	5	95	4.5
AC	1	0	0.300	0.300	10	190	9.0	2.400	0	0	10	190	4.5
AC@	1	0.480	0.240	0.150	10	190	9.0	1.920	0.060	0.150	10	190	4.5
CA	1	1.920	0.060	0.150	10	190	9.0	0.480	0.240	0.150	10	190	4.5
Uniform	1	2.4	0.3	0.3	10	190	9.0						
Slurry		2.4	0.3	0.3	4								

Slurry is prepared by ball milling at 300 rpm for 15 min (dry milling) plus 30 min (wet milling in NMP), and casted on Al foil with a doctor's blade.

#### 2.4. Microscopy characterization

The cross-section of electrodes was observed in a Carl Zeiss Merlin high resolution field emission scanning electron microscope (FE-SEM) combined with an Oxford Instruments Xmax 150 EDX detector. EDX line scan were performed across cross-sections in order to obtain an indication of key element distributions through the thickness. After cycling, cathodes were recovered by disassembling the half-cells in a glove box, washed in DMC (dimethyl carbonate) and then dried in glove box. Transmission electron microscopy (TEM) samples were prepared by re-dispersing the cycled cathode material in NMP by ultrasonication to dissolve the PVDF binder, and the filtered solid was then dispersed in ethanol. A TEM grid covered with a holey carbon film was dipped into this suspension, dried in glove box, and then sealed in a glass tube. The coated TEM grid was transferred to a TEM sample holder in air within minutes and the cathode particulate examined in a JEOL JEM-2100 TEM. Similarly, X-ray Photoelectron Spectroscopy (XPS) was performed on the cycled cathode particulate in a K-Alpha XPS system (Thermo Scientific). XPS samples were prepared by fixing the recovered cathodes on a sample holder in a glove box, sealed into a vacuum lock, and then transferred to the XPS system without air contamination. Quantitative analysis of XPS data was performed by CasaXPS (Casa Software, Ltd).

#### 2.5. Cell preparation and testing

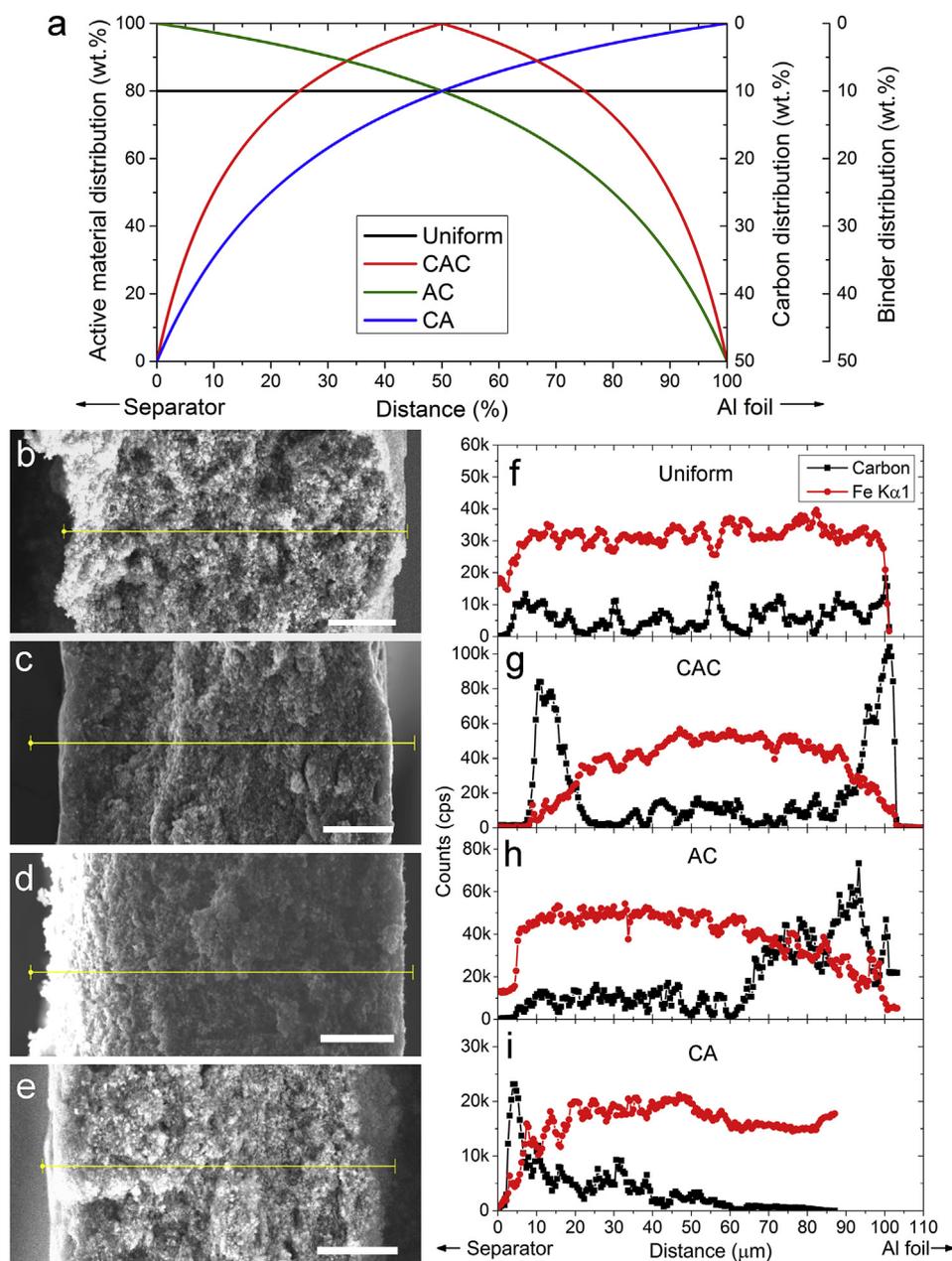
CR2032 half-cells were assembled with the cathode working against Li foil with glass fibre as a separator, soaked in 1M  $\text{LiPF}_6$  in ethylene carbonate and dimethyl carbonate (EC/DMC = 50/50 v/v, Sigma-Aldrich, UK) electrolyte. Before assembling, all cell components were stored in a vacuum oven at 60 °C in a Ar filled glove box for more than 5 h to reduce residual moisture and then assembled within the same

glove box. As-assembled battery cells were aged for 6–12 h before testing. Coin cells were investigated using an Arbin battery cycler (Arbin Instruments, USA, Models: BT-G-25 and IBT21084LC) in the potential range 2.5–4.2 V vs.  $\text{Li/Li}^+$  at room temperature at various C-rates from 0.1 to 7C. For long-term cycling, pristine cells were first cycled at 0.1C for 5 and 3 cycles before repeated cycling at 0.2 and 2C, respectively. Here, 0.1C corresponded to 17 mA g<sup>-1</sup> of active material. Within each cycle, charging and discharging were performed at the same C-rate. Electrochemical impedance spectroscopy (EIS) was performed at open circuit voltage after discharging to 2.5 V and aging of approximately 12 h, with a 10 mV sine wave perturbation in the frequency range 1 MHz down to 0.01 Hz. All measured EIS data were fitted with an equivalent circuit in order to estimate charge transfer resistance and other parameters [27–29].

### 3. Results and discussion

A MATLAB® code was developed to mimic the spraying process and to predict the weight ratio of active material:carbon:binder through the thickness of electrodes by using values in Table 1 as input (see Supplementary Data). The program is suitable for any composition ratio in the suspensions, pumping rates, volumes, and etc., and was used to ensure the overall ratio of constituents remained constant.

Fig. 2a shows the ideal, calculated material distribution of four typical gradient electrodes: uniform, CAC, AC, and CA, where C and A indicates carbon-rich and active materials-rich regions, and the sequence of C and A indicates the “stacking” order towards the current collector. For instance, the CAC electrode means the active material-rich region was sandwiched by two carbon-rich regions, which gave a convex parabola distribution of active materials and a concave parabola distribution of carbon and binder across the thickness (Fig. 2a, red line).



**Fig. 2.** Idealized and realized gradient material distribution through the thickness of electrodes. (a) Idealized, nominal distribution of  $\text{LiFePO}_4$  (left) and carbon & binder (right) in  $\text{LiFePO}_4$ -based cathodes fabricated by layer-by-layer spray printing using the suspensions listed in Table 1 (b–e) Scanning electron microscopy (SEM) cross-section views of uniform, CAC, AC, and CA cathodes (scale bar =  $20\mu\text{m}$ ). (f–i) Energy-dispersive X-ray spectroscopy (EDX) line scan through the electrode thickness (yellow lines as indicated in (b–e)), where the carbon and the Fe EDX signals denote the presence of Super-P and  $\text{LiFePO}_4$ , respectively. The average composition ratio of each electrode was the same at  $\text{LiFePO}_4$ : Super-P: PVDF = 80:10:10 (wt.%). (For interpretation of the references to colour in this figure legend, the reader is referred to the Web version of this article.)

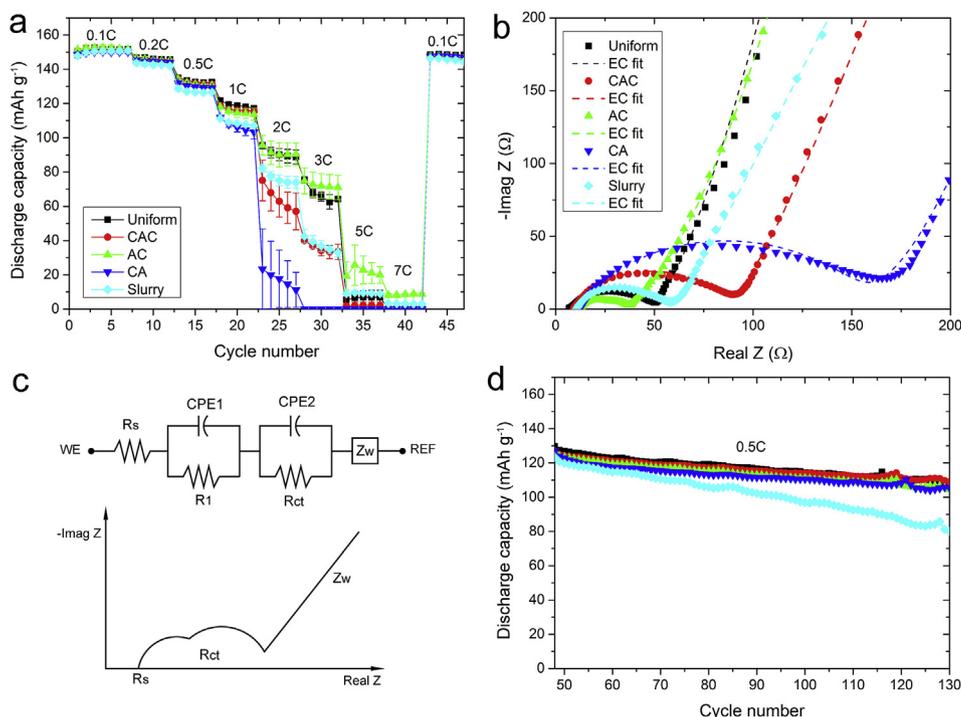
AC indicates that the weight ratio of active material decreases continuously from 100% at the electrode/separator interface to 0% at the electrode/Al interface; while the carbon (the same as for the binder) increases from 0% to 50% (Fig. 2a, green line). The CA electrode had the inverse of the material distribution of the AC electrode.

Fig. 2b–e shows SEM cross-section views of the four spray printed electrodes corresponding to the ideal profiles in Fig. 2a. Fig. 2f–i shows the corresponding carbon and active material ( $\text{LiFePO}_4$ , indicated by the Fe EDX signal) distribution across the electrodes along the yellow lines. Here, the variation of binder fraction followed that of the carbon due to the identical weight loading in the suspensions (see Table 1). By comparing Fig. 2f–i with Fig. 2a, the spray printed electrodes showed good qualitative agreement of actual with intended composition variation, noting that quantitative weight ratio measurement, especially for carbon, was judged insufficiently accurate by EDX. The cross-section and EDX line scans confirmed that the electrodes were  $\sim 100\mu\text{m}$  thick after calendaring and consistent with measurement by micrometer. The thickness of CA electrode was slightly lower because it partially spalled from the current collector during SEM sample preparation with a small

part of the electrode remaining attached to the current collector. A fuller view of the cracked CA electrode is given in Fig. S2, and is discussed later.

Using conventional electrode fabrication methods, such as widely used slurry casting, the continuous micro-scale variations in local composition, shown in Fig. 2, are impossible. So far, only two-layer (porosity graded) electrodes have been fabricated by multi-steps of slurry casting/drying/calendaring/2nd slurry casting/drying/calendaring [22], with different porosities in each layer but the same composition ratio. The complexity of this type of iterative casting method increases with the number of discrete layers, as will the number of distinct interfaces between layers, which may lead to cracking during long term cycling; there is also a minimum thickness of each later that can be reproducibly slurry cast, typically  $> 10\mu\text{m}$ , whereas the layer thickness in spray printing is determined only by the active particle size, allowing relatively fine-scale composition variations.

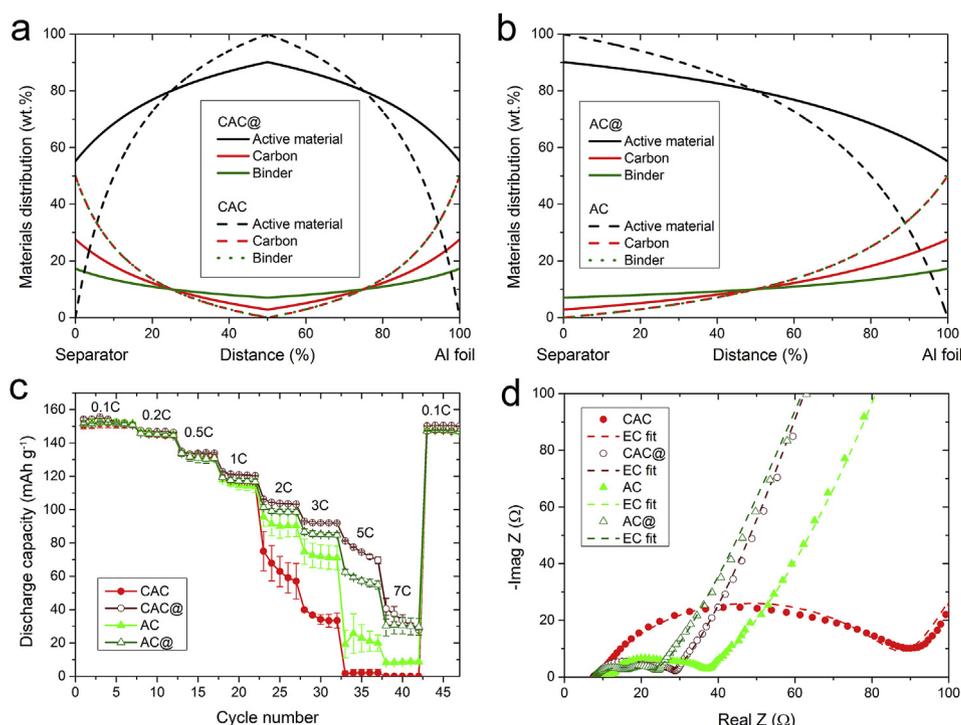
The C-rate performance of five types of pristine  $\text{LiFePO}_4$ -based cathode is shown in Fig. 3. The cells were first subject to 7 charging/discharging cycles at 0.1C and current  $17\text{mA g}^{-1}$ , and then



**Fig. 3.** Electrochemical characterization of graded electrodes. (a) C-rate performance of pristine LiFePO<sub>4</sub>-based half-cells with gradient and uniform material distribution corresponding to Fig. 2. (b) Electrochemical impedance spectroscopy (EIS) for one group of cells after the C-rate testing shown in (a). Solid symbols were experimental measurements and dash lines were fitted with equivalent circuit (EC fit) in (c) with fitting parameters given in Table S1. (d) The other group of cells were continuously cycled at 0.5C after testing in (a).

experienced 5 cycles at each of the subsequent C-rates. All had similar discharge capacities of approximately 150 mAh g<sup>-1</sup> at a low C-rate of 0.1C, which was reasonable since they contained the same amount of active material and capacity should be controlled only by the intrinsic capacity of LiFePO<sub>4</sub> at low rate [30], and not by the electrode structure. However, as the C-rate increased, the electrode structure began to influence the deliverable capacity [31], including a growing influence of charge transfer resistance for redox reactions and impedance to ion transport. For example, at 3C, the highest-to-lowest ranking of electrode capacity was: AC (72.4 mAh g<sup>-1</sup>) > uniform (67.1 mAh g<sup>-1</sup>) > slurry (40.5 mAh g<sup>-1</sup>) > CAC (35.5 mAh g<sup>-1</sup>) > CA (0 mAh g<sup>-1</sup>), which was consistent with the lowest-to-highest charge transfer resistance (R<sub>ct</sub>) measured after C-rate testing: AC (25.5 Ω) < uniform (41.5 Ω) < slurry (45.4 Ω) < CAC (77.3 Ω) < CA (143.2 Ω). Here, R<sub>ct</sub> was obtained by fitting the equivalent circuit (EC) shown in Fig. 3c to the impedance data, with the best-fit curves shown as dash lines in Fig. 3b and fitting parameters given in Table S1. Other equivalent circuits were considered, such as assuming the Warburg impedance (Z<sub>w</sub>) was arranged in parallel with constant phase element (CPE2) and in series with charge transfer resistance R<sub>ct</sub> [32]; however, the fit was not improved, and the physical interpretation of more complex equivalent circuits more uncertain.

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**Fig. 4.** C-rate performance of optimized graded electrodes. Calculated target material distribution in gradient cathodes (a) CAC@ (second iteration) and CAC (first iteration); (b) AC@ and AC. (c) C-rate performance of pristine half-cells of second iteration CAC@ and AC@ cathodes in comparison with first iteration CAC and AC cathodes. Two cells were tested for each type of cathode. (d) Electrochemical impedance spectroscopy data for half-cells after C-rate testing in (c).

The two semi-circles illustrated in Fig. 3c correspond to the two time constants ( $\tau = RC$ ) that represent the time required to charge the capacitor having the effective capacity of the constant phase element CPE. The first semi-circle is usually attributed to the impedance at the active particle surface and the second semi-circle usually attributed to the charge transfer of redox reactions [27–29,33]. Often in experiment, as here, the two semi-circles overlap to some extent and EC fitting is necessary in order to extract an estimate of  $R_{ct}$ .

Compared with the slurry cast electrodes, the spray printed electrodes had a lower rate of capacity degradation during long term cycling. As shown in Fig. 3d at 0.5C, the four sprayed electrodes had a relatively stable degradation of 0.25 mAh g<sup>-1</sup> per cycle and similar discharging capacities (2–3% difference) while the slurry cast electrode had a capacity degradation of 0.56 mAh g<sup>-1</sup> per cycle i.e. approximately twice that of spray printed electrodes. This increased stability was in part attributed to the improved mixing of the constituent materials within each sprayed micro-layer, consistent with in our previous work on non-graded spray printed electrodes [7,24]. For example, the liquid fraction in a slurry cast suspension is normally less than 50 wt% in order to give the optimum viscosity for coating and to promote a high peeling strength [34]; in contrast, spray printing used more dilute formulations (see Table 1) that allow stable atomization but also facilitate suspension homogenization by high-energy ultrasonication. In addition, the suspension atomization and droplet deposition steps also impart significant shear strain that may help to break up any agglomerates.

Fig. 3 provides proof-of-concept that grading may offer some benefits to electrode performance, and was used a starting point for a subsequent iteration of grading optimization based on the trend data. First, Fig. 3a and b suggested that a carbon-rich region at the current collector, rather than an active material-rich region, reduced the charge transfer resistance [24], with was also inversely proportional to capacity retention at high C-rates ( $\geq 1C$ ) e.g.  $R_{ct}$  of electrode AC was  $\sim 20\%$  that of electrode CA (Fig. 3b) and C-rate performance was dramatically better. Second, each of the gradient electrodes in Fig. 3 had a region of ultra-high fraction of active material, close to or equal to 100 wt%, which was unlikely to be optimum due to a lack of electrical conductivity. Therefore, accounting for these two effects, two other types of gradient electrodes with smooth variations of constituent materials were then designed, both with a carbon-rich region close to the current collector and maximum local fraction of active material of 90%, termed CAC@ and AC@ in Table 1. The target, nominal composition variations for these electrodes are shown in Fig. 4a and b, with the previous CAC and AC electrodes also shown for comparison. Once again, the overall relative fraction of all materials was constant across all electrodes.

The C-rate performance of pristine CAC@ and AC@ half-cells is shown in Fig. 4c. Compared with the previous graded electrodes (CAC and AC) there were significant capacity improvements at C-rates  $\geq 2C$ . For example, at 5C, the discharge capacity of CAC@ was 75 mAh g<sup>-1</sup> while CAC had no discharge capacity; the discharge capacity of AC@ was 58 mAh g<sup>-1</sup> while AC had a discharge capacity of only 22 mAh g<sup>-1</sup>. Compared with AC@/AC, CAC@/CAC showed the stronger improvement, which was mainly due to the initially sluggish performance of the CAC arrangement.

As previously mentioned, the CAC electrode easily split into two layers during SEM sample preparation because the middle region had no binder ( $\sim 100$  wt% active material); in contrast, the middle region of CAC@ had 7 wt% binder (Fig. 4a) that was sufficient to maintain electrode integrity. As shown in Fig. 4d, the trend of increasing C-rate performance was again consistent with a reduction in charge transfer resistance:  $R_{ct}$  of CAC@ (19.7  $\Omega$ ) was smaller than CAC (72.8  $\Omega$ ); similarly,  $R_{ct}$  of AC@ (16.2  $\Omega$ ) was smaller than AC (25.5  $\Omega$ ).

Fig. 5a summarizes the C-rate performance of the various electrodes. At high C-rates ( $\geq 2C$ ), much higher capacity retention was realized in CAC@ and AC@ compared with uniform and slurry cast cathodes while at low C-rates ( $\leq 0.5C$ ), graded electrode discharge

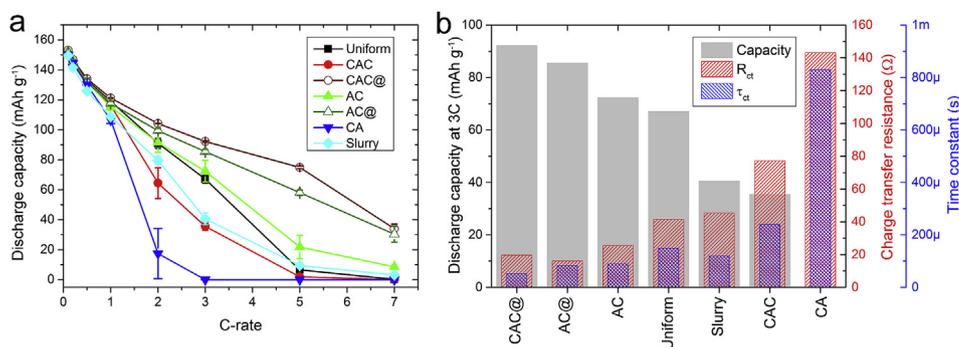
capacities were almost the same as uniform electrodes, i.e. the gradient material distribution did not sacrifice energy density to achieve higher power density. Specifically, the discharge capacities of the CAC@ cathode increased 15% and 31% at 2C, and 38% and 128% at 3C compared with spray printed uniform and slurry cast equivalent respectively. Similarly, the discharge capacity of the AC@ cathode increased 9% and 25% at 2C, and 27% and 110% compared with spray printed uniform and slurry cast uniform cathodes respectively. The discharge capacity at 3C was inversely proportional to the charge transfer resistance  $R_{ct}$  (Fig. 5b, red curve). The time constant  $\tau_{ct} = R_{ct}C_{eff}$  (Fig. 5b blue) that expresses the time required for charge transfer during redox reactions, was also inversely proportional to the discharge capacity at 3C.

Overall, Fig. 5 demonstrates how charge transfer related C-rate performance can be tuned by arranging the materials distribution in different ways at the micro-scale across the thickness of electrode. Surprisingly, simply by arranging identical materials in gradient fashion, capacity can be increased by nearly 100% over a homogeneous, random mixture. Note that in the manufacture of the slurry cast electrodes, the ball milling time and mixing sequence [9,35], were probably not fully optimised and more time spent in this respect may narrow the performance gap with the spray printed uniform electrodes. However, by the same token, the gradient electrodes provides many degrees of freedom for microstructural optimization not yet fully explored, which may increase their performance even further.

Fig. 6a shows that the charge-discharge curves for both graded and uniform cathodes were almost the same at 0.1C. When the C-rate increased to 3C, the mean charge voltage increased and the mean discharge voltage decreased for all cathodes (polarization increased); however, while the polarization of the uniform cathode increased to 0.93 V the polarization of both the graded cathodes increased to only 0.50 V (Fig. 6b). Polarization here refers to the difference between charge and discharge voltages [36,37]. The larger polarization for uniform cathodes most likely indicated that a higher activation overpotential was required for Li<sup>+</sup> intercalation/deintercalation reactions, which in turn can increase the rate of side reactions, such as increasing the thickness of solid electrolyte interphase (SEI) [22]. This would be consistent with the measured increase in charge transfer resistance and capacity fading at high C-rates (Fig. 5b at 3C). Thus it is suggested that certain graded material distributions may contribute to a more uniform distribution of overpotential across the thickness of the electrode, and it is this overpotential homogenization that underpins the observed improved charge storage properties. This interpretation is consistent with recent simulation studies of the optimization of overpotential distribution in multi-layered graded electrodes [19].

For 90 repeating cycles at 0.2C, Fig. 7a shows that the CAC@ graded cathode had the slowest average capacity degradation rate of 0.22 mAh g<sup>-1</sup> per cycle, while AC@, CAC, uniform spray printed, and slurry cast cathodes showed similar degradation rates of 0.26–0.29 mAh g<sup>-1</sup> per cycle. The degradation rate was increased slightly to 0.33 and 0.36 mAh g<sup>-1</sup> for CA and AC graded cathodes. When the charging/discharging rate increased ten times to 2C, Fig. 7b shows that both CAC@ and AC@ graded cathodes had the slowest capacity degradation rate of 0.24–0.25 mAh g<sup>-1</sup> per cycle, compared with the uniform spray printed cathode of 0.41 mAh g<sup>-1</sup> per cycle, and slurry cast cathode of 0.48 mAh g<sup>-1</sup> per cycle. The AC, CAC, and CA graded cathodes had average degradation rates of 0.51, 0.58, and 1.0 mAh g<sup>-1</sup> per cycle at 2C, respectively. From slow to fast charging/discharging rates (0.2C–2C), CAC@ and AC@ cathodes maintained similar capacity degradation rates below 0.3 mAh g<sup>-1</sup> per cycle for 90 cycles, and were the best performing.

Thus, compared with either uniform spray printed or uniform slurry cast cathodes, the advantage of the best graded cathodes was not only higher capacity retention with increasing C-rate (Fig. 5a) but also slower and more stable capacity degradation (Fig. 7a and b). The graded electrodes offered no increase in capacity at low C-rates



**Fig. 5.** Comparison of various cathodes with the same average weight ratio (active material: carbon: binder = 80: 10: 10 wt%). (a) C-rate performance. (b) Discharge capacities at 3C (left), the charge transfer resistance  $R_{ct}$  of the corresponding cells measured after C-rate testing (right, red), and time constant ( $\tau_{ct} = R_{ct}C_{eff}$ ) for charge transfer (right, blue), where  $C_{eff}$  is the effective capacity of the constant phase element, CPE2, in the equivalent circuit (Fig. 3c). (For interpretation of the references to colour in this figure legend, the reader is referred to the Web version of this article.)

(< 0.5C) which was determined only by the theoretical capacity and fraction of the active material. However, considering practical applications, such as electric vehicles that require frequent charging/discharging in short time (i.e. at high C-rates), the advantage of gradient electrodes became significant e.g. less than half the rate of capacity degradation (Figs. 7b) and 31% higher capacity (Fig. 5a) compared with slurry cast electrodes at 2C.

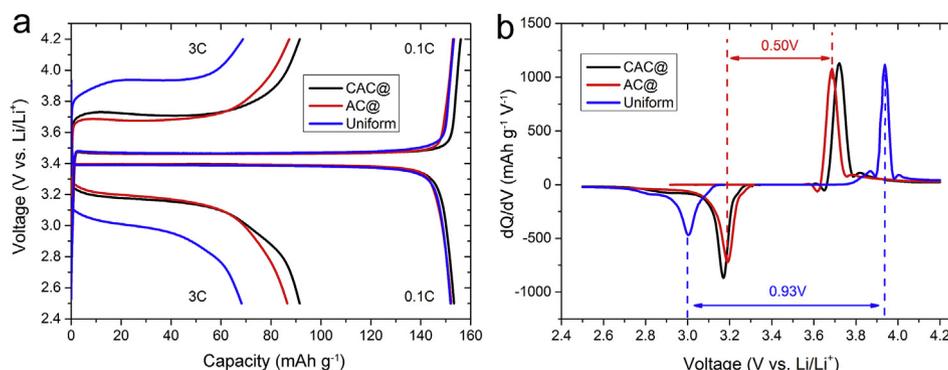
According to Figs. 5–7, the optimized graded electrodes (e.g. AC@) have a superior C-rate, polarization, and cycling performance to the uniform electrodes. According to simulation, porosity-graded electrodes may have a more homogeneous over-potential distribution across the electrode thickness [19], which can restrict or slow down side reactions at the electrolyte/active material interface, leading to a thinner solid electrolyte interphase (SEI) formation and supporting improved electrochemical performance [22]. Although these simulations focused on porosity-graded electrodes, which is different from the composition-graded electrodes presented here, the idea of a more homogeneous over-potential distribution supporting improved performance may be common for both graded cases.

To explore this hypothesis, transmission electron microscopy (TEM) images of the cycled  $\text{LiFePO}_4$  particles collected from uniform and AC@ graded cathodes after the cycling regime shown in Fig. 7a are shown in Fig. 8a and b, respectively. The average SEI layer thickness on active particles from the uniform electrode was  $11.5 \pm 1.8$  nm and  $6.7 \pm 2.8$  nm for particles from the AC@ graded electrode.

Although the SEI thicknesses differences support the hypothesis, the differences were small and it was not possible to be sure from which part of the cathode the particulates came from, and the SEI layer thickness through the electrode thickness may be different [39]. Therefore, X-ray photoelectron spectra (XPS) were also obtained from the surface only (nearest the separator) of the same cycled uniform and AC@ graded cathodes, which are shown in Fig. 8c and d. Because XPS has only a restricted depth penetration [41], the detection region was approximately the same for both electrodes. The P 2p XPS spectra in Fig. 8c shows that the pristine uniform cathode contained only  $2p_{3/2}$

(133.4 eV) and  $2p_{1/2}$  (134.3 eV) doublets that were attributed to phosphate (i.e.  $\text{LiFePO}_4$  active material). After cycling, an additional strong peak appeared in both uniform and AC@ cathodes at a binding energy  $\sim 136.9$  eV, which was assigned to fluorophosphates ( $\text{Li}_x\text{PO}_y\text{F}_z$ ) resulting from the degradation of the  $\text{LiPF}_6$  electrolyte and SEI formation [40]. Using peak deconvolution, the ratio of  $\text{Li}_x\text{PO}_y\text{F}_z$ :  $\text{LiFePO}_4$  peak area was 3.2 for the cycled uniform cathode and 1.7 for the cycled AC@ cathode. This difference indicated a thicker SEI layer on  $\text{LiFePO}_4$  in the uniform cathode. Similarly in Fig. 8d, the C 1s XPS spectra shows that both cycled uniform and AC@ graded cathodes produced  $\text{Li}_2\text{CO}_3$  and semi-organic carbonates with a characteristic O–C=O bond at  $\sim 289.6$  eV i.e. typical components of a SEI layer [39]. Using peak deconvolution and integration and using the C–C chemical bond as a reference ( $\sim 284$  eV), the O=C–O:C–C peak area ratios were 1.0 and 0.8 for cycled uniform and AC@ cathodes respectively. In Fig. 8e, the O 1s XPS spectra confirmed that both uniform and graded cathodes produced  $\text{Li}_x\text{PO}_y\text{F}_z$  and  $\text{Li}_2\text{CO}_3$  after cycling (both the F–P–O bond in  $\text{Li}_x\text{PO}_y\text{F}_z$  and the O=C–O bond in  $\text{Li}_2\text{CO}_3$  contributed to the peak at  $\sim 533.8$  eV, although organic carbonates may be also included [39]). From Fig. 8e, 13 at.% of all the O in the spectrum contributed to this peak in the uniform cathode, compared with 9 at.% for the AC@ graded cathode. In summary, P, C and O spectra all inferred SEI formation after cycling and all suggested a thicker SEI layer on the uniform cathode, consistent with the TEM observations shown in Fig. 8a and b.

While recognizing the TEM and XPS data provide support rather than conclusive evidence, when synthesised with the prior modelling and simulation work and the impedance data shown previously, the improved performance of the graded electrode can be understood as follows. The graded material distribution gives rise to a more homogenized over-potential distribution through the electrode thickness, which leads to less pronounced side-reactions at the active material/electrolyte interface and leads to thinner SEI layer formation. The relatively thin SEI layer supports and sustains throughout cycling a comparatively high electrode electric and ionic conductivity that reduces the electrode overall charge transfer resistance, particularly



**Fig. 6.** Polarization difference between graded and uniform electrodes. (a) Galvanostatic charge-discharge curves of graded (CAC@, AC@) and uniform sprayed  $\text{LiFePO}_4$ -based cathodes at 0.1C and 3C, respectively. (b) 1st derivative of capacity (Q) to voltage (V),  $dQ/dV$ , corresponding to charge-discharge curves at 3C in (a).

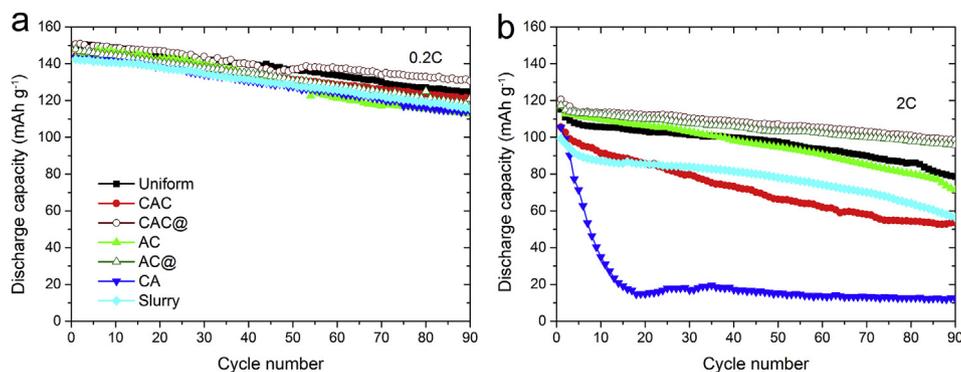


Fig. 7. Cycling performance of various types of LiFePO<sub>4</sub>-based cathodes at (a) 0.2C and (b) 2C, respectively.

improving the charge/discharge kinetics.

#### 4. Conclusions

Graded composition cathodes based on LiFePO<sub>4</sub> that had a

continuous micro-scale variation in the weight ratios of active material:carbon:binder across the electrode thickness were fabricated using a layer-by-layer spray printing technique. By arranging the materials distribution while keeping the average material loading the same as uniform cathodes, both C-rate performance and capacity degradation

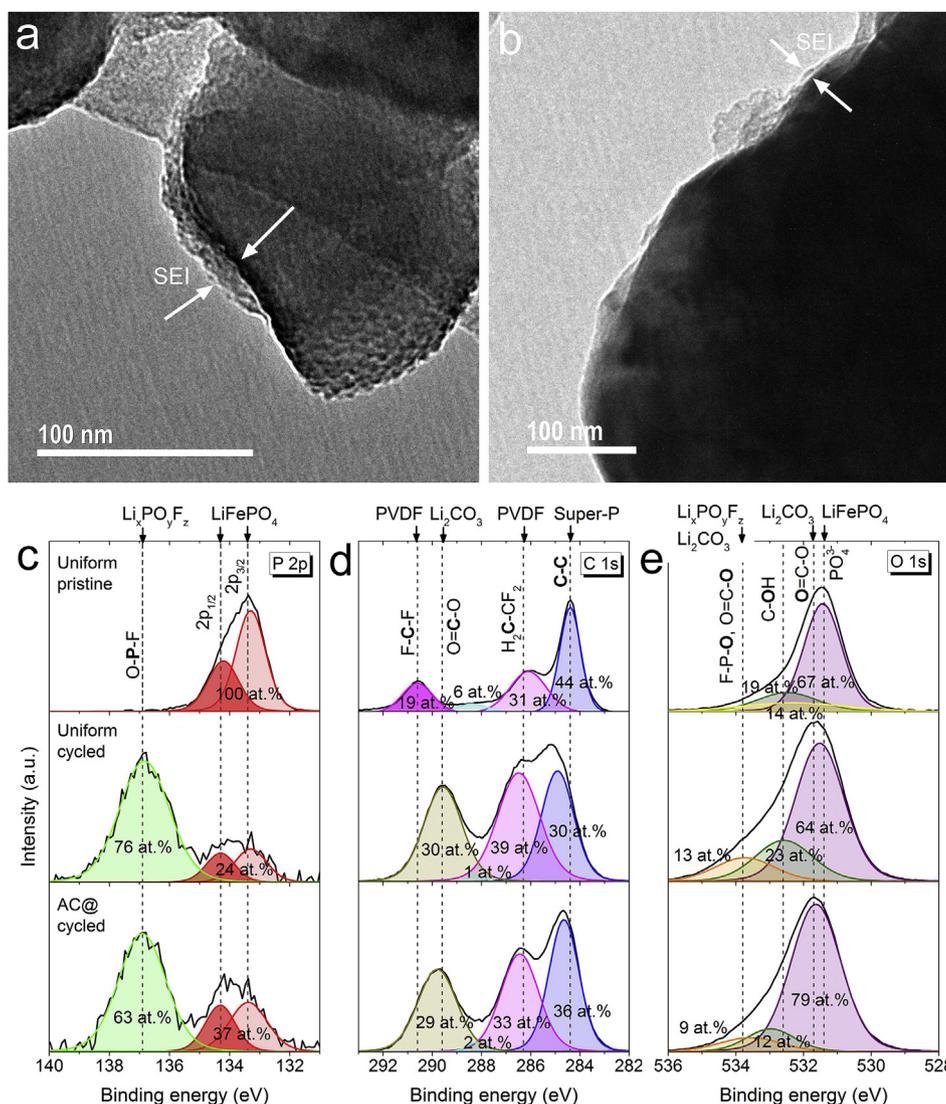


Fig. 8. Transmission electron microscopy (TEM) images of LiFePO<sub>4</sub> particles collected from (a) uniform and (b) AC@ graded cathodes after the cycles shown in Fig. 7a. Corresponding X-ray photoelectron spectra (XPS) of the uniform and AC@ graded cathodes after the cycles shown in Fig. 7a. The pristine uniform cathode without cycling is also given for comparison. (c) P 2p XPS spectra, (d) C 1s XPS spectra, and (e) O 1s XPS spectra. The vertical dash lines indicate the labelled reference chemical bonds taken from the literature [38–40]. The atomic percentage refers to the elemental P, C and O of each species within the spectrum.

during long term cycling were improved in this model LiFePO<sub>4</sub>-based cathode system. In terms of C-rate performance, the discharge capacities of CAC@ graded cathodes increased 15% and 38% at 2C and 3C compared with spray printed uniform cathodes. Similarly, the discharge capacities of AC@ gradient cathodes increased 9% and 27% at 2C and 3C compared with spray printed uniform cathodes. These differences were even larger when compared with conventional slurry cast cathodes. The improvement in C-rate performance was due to much reduced (~50%) charge transfer resistance in graded electrodes. In terms of capacity degradation during cycling, CAC@ and AC@ graded cathodes had similar low capacity degradation rates (0.22–0.28 mAh g<sup>-1</sup> per cycle) at both 0.2C and 2C, which were slightly reduced compared with uniform cathodes at 0.2C, but significantly smaller (40–50%) than uniform cathodes at 2C (0.41–0.48 mAh g<sup>-1</sup> per cycle). Consistent with modelling studies in the literature and our TEM and XPS investigations, the performance improvements were suggested to derive from (i) reduced interfacial resistance at the cathode/current collector interface due to a local carbon-rich region, and (ii) a reduction in polarization and an improved spatial homogenization of overpotential that leads to a thinner SEI layer formation during cycling and sustains improved C-rate and long-term cycling performance. These findings should be applicable to other types of cathode or anode active materials. To demonstrate the feasibility for large area faster deposition more attuned to the needs of industry, we have established a capability for multi-spray deposition in controlled atmosphere (Fig. S3).

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## Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.jpowsour.2018.12.021>.

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