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# 1 Mechanisms and Mitigation of Agglomeration during Fluidized Bed

## 2 Combustion of Biomass: A Review

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### 11 Abstract

12 A key issue associated with Fluidized Bed Combustion of biomass is agglomeration. The presence of  
13 high quantities of alkali species in biomass ash leads to the formation of sticky alkali-silicate liquid  
14 phases during combustion, and consequently the adhesion and agglomeration of bed material. This  
15 review principally examines probable mechanisms of agglomeration and the effects of operational  
16 variables in reducing its severity. Additionally, an overview of monitoring and prediction of  
17 agglomerate formation is given. Two key mechanisms of agglomeration are apparent in literature,  
18 and both may occur concurrently dependent on fuel composition. Coating-induced agglomeration is  
19 defined by the interaction of alkali metals in fuel ash with the bed material, commonly silica sand, to  
20 form an alkali-silicate melt. Melt-induced agglomeration is defined by the presence of sufficient  
21 amounts of both alkali compounds and silica liquid phases sourced from the fuel ash to form a  
22 eutectic mixture. Physical mechanisms, such as tumble agglomeration and sintering, may further  
23 enhance either of the coating-induced or melt-induced mechanisms. Of the operational variables

24 examined in this review, temperature, fluidizing gas velocity, fuel, bed material and additives have  
25 been shown to have the greatest effect on agglomeration severity. Prediction of agglomeration  
26 propensity may be attempted with mathematical correlations or lab-scale fuel testing before use in  
27 the boiler, “pre-combustion” methods, or in-situ methods, which are focused on temperature or  
28 pressure analysis. The review of the literature has highlighted the need for further research in some  
29 areas, including: mechanisms when using alternate bed materials, use of dual-fuel biomass blends,  
30 technical and economic optimisation of alternative bed material, the use of additives or improvers  
31 and further modelling of coating growth behaviours.

## 32 **Keywords**

33 Fluidized bed; Combustion; Biomass; Agglomeration; Review

## 34 **Nomenclature**

35	AFBC		Atmospheric fluidized bed combustion
36	BFB		Bubbling fluidised bed
37	CFB		Circulating fluidised bed
38	$d_{bed}$	m	Bed diameter
39	DDGS		Distillers dried grain using wheat and solubles
40	FBC		Fluidized bed combustion
41	$h_{bed}$	m	Static bed height
42	IDT		Initial deformation temperature
43	PF		Pulverized fuel
44	PFBC		Pressurized fluidized bed combustion

45	$T_{\text{aggl}}$	°C	Agglomeration temperature
46	$t_{\text{def}}$	mins	Defluidization time
47	$U$	m/s	Superficial gas velocity
48	$U/U_{\text{mf}}$	-	Fluidization number
49	$U_{\text{mf}}$	m/s	Minimum fluidization velocity
50	XRD		X-Ray Diffraction

## 51 **1. Introduction**

52 In recent decades, there has been an increased importance placed on fuels and power generation  
53 methods that emit reduced amounts of carbon dioxide (CO<sub>2</sub>), a key contributor to anthropogenic  
54 changes to the atmosphere. [1, pp. 12-19]. One fuel type that has the potential to address this issue  
55 is biomass, due to its potential to approach carbon neutrality [2], and has thus been the subject of  
56 research into technical issues that may negatively affects its use in the power generation industry,  
57 and policy driven regulation to incentivize its deployment.

58 Biomass is a direct, low carbon alternative to fossil fuels for power and heat generation, and is  
59 abundant in many areas of the world [3, 2]. In the UK it can offer competitively priced power  
60 generation versus options such as nuclear and offshore wind [4]. The combustion of biomass comes  
61 with several technological challenges for traditional burner technologies such as those adopted in  
62 pulverized fuel (PF) power stations [5]; i.e. : low energy density after initial harvesting, variable  
63 volumes of non-combustible contaminants, high moisture contents and, in most applications,  
64 requires a large amounts of pre-processing/pre-treatment with specialised transportation. Due to  
65 these challenges, technologies such as fluidized bed combustion (FBC) boilers have been employed.  
66 FBC offers a number of advantages, such as combustion of different fuel types, blends, and ranges of  
67 qualities, features commonly referred to under the umbrella term of “fuel flexibility” [5]. Hundreds

68 of full-scale bubbling fluidized bed (BFB) [6, p. 7] and circulating fluidized bed (CFB) [6, p. 8] boilers  
69 have been deployed around the world [7, 8] for power generation and/or steam sales to industrial or  
70 chemical plant sites. However, each FBC plant development has to overcome slagging, fouling,  
71 corrosion and, most significantly, agglomeration issues resulting from the composition and  
72 behaviour of the biomass fuel stock [9].

73 Analytical studies of wide ranges of fuel types have typically shown biomass to be high in volatiles  
74 and moisture, with mineral matter content rich in alkali and alkali earth metals such as potassium  
75 and calcium [10, 11, 12, 13]. There is also a high complexity and variation in biomass ash  
76 compositions. Saidur, et al. [12] placed biomass fuels into one of three different categories based  
77 upon their fuel ash composition:

- 78 • Ca- & K-rich, Si-lean. Typically woody biomass.
- 79 • Si- & Ca-rich, K-lean. Typically herbaceous or agricultural.
- 80 • Ca-, K-, & P-rich, e.g. sunflower stalk ash or rapeseed expeller ash.

81 The above components in biomass ash, together with sodium and chlorine, have been identified as  
82 being responsible for agglomeration, slagging, fouling, and corrosion in Fluidized Bed boilers [10, 14,  
83 pp. 471-491].

84 Agglomeration occurs within the bed itself, and is where bed particles begin to group together into  
85 larger particles [14, pp. 471-491] (Figure 1). In the case of biomass combustion on a silica sand bed,  
86 this is due to the formation of sticky, low melting temperature, alkali-silicate complexes. These  
87 agglomerates may be further strengthened by sintering, in which high localised temperatures leads  
88 to the melting of particles and thus fusing agglomerated materials into large hardened structures.  
89 This method of agglomeration, in which fuel ash interacts with bed material, is typically termed  
90 coating-induced agglomeration. When fuel ash contains quantities of both silica and alkali melts  
91 sufficient to create melts, the term melt-induced agglomeration is commonly used. The

92 accumulation of agglomerates eventually leads to defluidization of the bed. This is the point at which  
93 the bed particles no longer move and behave as a fluid in response to the fluidizing gas, as the mean  
94 bed particle size will have increased and the minimum fluidization velocity,  $U_{mf}$ , is no longer achieved  
95 [15].

96 In an industrial installation, operators may control agglomeration by varying fuel feeds, using  
97 alternative bed materials and/or additives, moderating combustion temperatures and combustion  
98 distribution, altering and moderating airflows, or varying rates of bottom ash removal and bed  
99 replenishment [16, 17]. A full bed defluidization event would necessitate a plant shutdown, as the  
100 bed is cooled, replenished, and started up again [18, pp. 2-110]. The financial cost associated with  
101 plant outage can mean that the profitability of the plant may be at risk. Moreover, frequent start-up  
102 and shutdown cycles may reduce the working lifespan of plant equipment [19, pp. 38-42]. As such,  
103 considerable efforts have been made towards methods to predict or prevent agglomeration [20].

104 Considering the upper sections of the boiler, slagging on the membrane walls, fouling on  
105 superheater tubes [21, pp. 406-412, 22, 23], as well as corrosion on superheater tubes [22, 24, 25,  
106 26] are driven by reactions with the same chemical components as agglomeration, namely, alkali  
107 and alkali earth metals, and silicon, with chlorine aiding alkali transport [27] (see Figure 2).

108 Therefore, it is important to consider the whole boiler system and the secondary or consequential  
109 negative impacts when evaluating a potential mitigation or solution for any of the aforementioned  
110 phenomena.

111 This review sets out to bring together the literature on the mechanisms of agglomeration, means of  
112 mitigating it through varying operational conditions, and the relationships between both areas.

113 Literature from lab-scale work through to investigations on full-scale industrial boilers has been  
114 selected, so that this review may be of use to both researchers and plant operators. In doing so, this  
115 review has also highlighted numerous areas in which further work would be beneficial to both  
116 broaden and deepen the knowledgebase.

## 117 **1.1 Review Scope**

118 This review focuses on the issue of agglomeration during FBC of biomass, and is divided into three  
119 sections:

- 120 • A review of the mechanisms of agglomeration found within the literature
- 121 • A review of the effects of process variables on agglomeration severity
- 122 • A brief overview of the current methods to predict the occurrence of agglomeration, with  
123 signposting to the other available articles and reviews on this subject

124 Summaries are provided after each section. These act to highlight key findings from the literature  
125 evaluated, note the important critiques, and discuss key areas for further work noted within the  
126 review. The end conclusion highlights the main areas where further work is needed.

## 127 **2. Mechanisms of Agglomeration**

128 As noted in the introduction, the fundamental chemistry driving agglomeration is the formation of  
129 alkali silicate eutectics. This is from the interaction of SiO<sub>2</sub> in the bed material or ash together with  
130 an alkali metal oxides in the fuel ash, such as K<sub>2</sub>O or Na<sub>2</sub>O. For example [28]:



132 The value of 'n' may range from 1-4. In the case of potassium silicates, higher values of 'n' generally  
133 reduce the eutectic melting point: with K<sub>2</sub>O-SiO<sub>2</sub> this is 976°C, whilst for K<sub>2</sub>O·4SiO<sub>2</sub> the melting point  
134 is 764°C [28]. These low melting points allows for the formation of a melt through the typical FBC  
135 operational temperature range of 800-900°C [29], which can then cause adhesion of the bed  
136 particles and agglomeration.

137 Early works into agglomeration with biomass fuels identified these eutectic melts as key drivers of  
138 agglomeration [30, 31, 32]. Sintering had been identified as a key driver as agglomeration in coal  
139 research [33]. Skrifvars, et al. [34] looked at this phenomena when combusting biomass, and found  
140 that the presence of >15% molten phase in ash would lead to elevated amounts of sintering.

141 Skrifvars, et al. [35] then applied standardised ash testing methods to predict sintering and  
142 agglomeration temperatures in biomass, to see if such methods could accurately predict  
143 troublesome fuels at typical industrial operational conditions. However, there was limited success  
144 with both of these methods.

145 Subsequent work on the behaviours of biomass ashes has led to the definition to two different  
146 agglomeration mechanisms: coating-induced agglomeration and melt-induced agglomeration.

## 147 **2.1 Coating-induced Agglomeration**

148 In the work of Öhman & Nordin [36], combustion experiments for several different biomass fuels  
149 were performed at lab-scale, using the “Controlled Fluidized Bed Agglomeration” methodology put  
150 forth in their earlier work [37]. Here, controlled incremental heating is applied to the bed until  
151 agglomeration is detected by Principal Component Analysis of temperature and pressure  
152 fluctuations within the bed. This was followed by SEM/EDS analysis of the resulting agglomerates,  
153 which focused on the “neck” between two joined particles.

154 The most abundant non-silica components in the agglomerates were alkali or alkaline earth metals –  
155 primarily either potassium or calcium – which accounted for between 20-70wt% across the different  
156 fuels. For some fuels, aluminium and iron featured amounts of up to 20wt%. Öhman & Nordin [36]  
157 then proposed the following mechanism for agglomeration:

- 158 1. Ash is deposited on bed particles creating a coating, through a mixture of small particles  
159 attaching to bed material, gaseous alkali molecules condensing, and reactions involving  
160 gaseous alkali molecules on the surface of the bed material.
- 161 2. Sintering occurs on this bed particle coating, homogenizing and strengthening it.
- 162 3. Melting of this silicate coating layer controls adhesive forces, which influence the severity of  
163 the agglomeration process. This is temperature-driven.



164 The work of Silvennoinen [38] also describes a coating mechanism similar to that of Öhman & Nordin  
165 [36] and state that whilst potassium silicates are the primary chemical basis for coating layers, in  
166 some cases sodium silicates are instead present. This highlights that other alkali-silicates can be the  
167 basis of coating layers.

168 The works of Nuutinen, et al. [39], Visser [40], Brus, et al. [41], and Öhman, et al. [42] are closely  
169 related, in that they further investigated bed particle coatings, all finding compositional and  
170 structural differences through the layers, indicating the presence of multiple layers. These works  
171 took samples from woody fuels, typically using quartz sand beds, at scales from lab-scale FBC units  
172 to full-scale installations.

173 The presence of multiple layers appears to be a factor of the potassium content of the fuel, with an  
174 example from the work of Visser [40] shown diagrammatically in Figure 3. Fuels that are lean in  
175 potassium produce two layers: an “inner” homogenous layer with significant calcium content, and  
176 an outer heterogeneous layer more similar in composition to that of the fuel ash. Fuel that are rich  
177 in potassium produce an additional “inner-inner” layer with notable amounts of potassium. The  
178 relative compositions of the inner and outer layers remain similar regardless of if the fuel is  
179 potassium-rich or lean.

180 Some different observations can be seen between the works of Nuutinen, et al. [39], Visser [40],  
181 Brus, et al. [41], and Öhman, et al. [42].

182 Nuutinen, et al. [39] noted that for the combustion of peat “inner” layer was absent, leaving only the  
183 outer ash layer. This could perhaps be a result of the operational time, conditions, or behaviour  
184 unique to peat as a fuel. Nuutinen, et al. [39] also trialled a proprietary magnesium based bed  
185 particle named “GR Granule”, which had two coating layers present: an inner layer of ~60% calcium  
186 and 15-20% silicon, and outer layer with notable amounts of magnesium, possibly from abrasion of  
187 the bed material.

188 Visser [40] proposed a coating mechanism similar to that of Öhman & Nordin [36], albeit without  
189 mention of interactions with gaseous alkali compounds. It was described as a build-up of small ash  
190 particles on bed material or larger ash particles to create a coating, followed by neck formation  
191 between two coated particles, which can be followed agglomeration and/or sintering. If this  
192 agglomeration leads to localised defluidization, an increase in localised bed temperatures may occur,  
193 triggering melt-induced agglomeration (see section 2.2).

194 Brus, et al. [41] examined agglomerate samples produced from plant-scale CFB and BFB boilers  
195 ranging from 30-122MW<sub>th</sub>, and those from a lab-scale BFB rig. “Inward chemical attack” by  
196 potassium or calcium silicates on the original quartz sand bed particle was observed. This conclusion  
197 was drawn through using quartz sand of a homogenous particle size distribution of 106-125µm,  
198 taking 200 SEM images of particles before and after experimentation had occurred, and then  
199 comparing the mean cross-sectional area of the sand particles before and after experimentation.  
200 This is an adequate method, given the alternative of tracking and comparing a specific particle and  
201 the challenges which that would entail. SEM/EDS imaging of sand particles that had been in boilers  
202 for upwards of 33 days showed the diffusion of potassium into cracks in the sand particle and the  
203 formation of potassium silicate veins within the sand particle. This adds additional support to the  
204 conclusion of inward chemical attack occurring. Brus, et al. [41] also noted that the calcium-silicate  
205 dominated “inner” coating layer is replaced by potassium- or other alkali-silicates in locations where  
206 calcium is not as available, such as cracks in sand particles, or when the fuel ash contains less  
207 calcium.

208 Brus, et al. [41] presented three mechanisms of agglomeration:

- 209 • Coating-induced agglomeration, with inward chemical attack by potassium/calcium silicates.
- 210 • Direct-attack by gaseous potassium compounds, forming low melting point potassium  
211 silicates and resulting in viscous-flow sintering.

212 • Direct adhesion through partially melted ash derived potassium silicate particles (melt-  
213 induced agglomeration, section 2.2).

214 Öhman, et al. [42] examined coating distribution across the particles examined with SEM/EDS, as  
215 summarised in Table 1. To obtain their SEM/EDS data, Öhman, et al. [42] selected 3-5 particles per  
216 fuel. All the fuels tested led to bed agglomeration, yet, as per Table 1, the quantity of coated  
217 particles to cause agglomeration varied in from being <10% of particles examined to the “majority”,  
218 which can be assumed as at least > 50%. This raises questions around the methods by which  
219 agglomeration occurred: for example, whether these differences are down to sampling methods or  
220 are the result of other mechanisms. Therefore, it would be worth investigating the differences  
221 coating composition and frequency of coated particles across the whole bed. This may indicate if  
222 certain zones are more susceptible to agglomeration and help provide a better understanding of  
223 bed-scale agglomeration and defluidization mechanisms.

224 Zevenhoven-Onderwater, et al. [43] investigated the ash compositions of five different woody fuels:  
225 bark, two forest residues, construction residue wood, and sawdust. From analysis of bed material  
226 and fuel ash compositions, the coating layer thickness observed, and the weight of the bed before  
227 and after experimentation, the source of coating elements was determined. Roughly 50wt% of  
228 potassium from the fuel remained in the bed, along with 8-30wt% of the calcium and 30-65wt% of  
229 fuel derived silicon, all of which could contribute to agglomeration. Coating layers were  
230 homogenous, with a formation method suggested: potassium-silicates begin forming a “first layer”  
231 on bed particles at around 750°C, which then captures other ash components, leading to the  
232 formation of a sticky layer of melting point <800°C.

233 Grimm, et al. [44] investigated agglomeration behaviour when using Olivine as a bed material.  
234 Experiments were performed for willow, logging residue, wheat straw, and distillers dried grain  
235 using wheat and solubles (DDGS) fuels, on both Olivine and quartz sand beds, with a 5kW BFB

236 reactor. An Olivine bed resulted in reduced agglomeration tendency for willow and logging residue,  
237 with no change noticed for wheat straw or DDGS.

238 The outer coating layer with Olivine was similar in composition to the fuel ash, as it was with quartz  
239 sand. A key difference versus quartz sand though was the composition of the homogenous inner  
240 coating layer for willow and logging residue, which comprised of Mg, Si and Ca as opposed to K, Si  
241 and Ca. This may have been due to the methodology used: fuels were combusted at around 800°C  
242 for 8 hours before the temperature was incrementally increased until agglomeration occurred or the  
243 maximum of 1060°C was reached. Temperatures in excess of 1000°C, as were reached with willow  
244 and logging residue, may have allowed some fraction of the magnesium in Olivine to partake in melt  
245 formation. Such temperatures would not be reached in typical FBC operation, therefore this result  
246 may not be wholly representative of a full-scale facility. Wheat straw and DDGS did not reach such  
247 high temperatures, and did not exhibit differences in coating composition when using Olivine  
248 compared to quartz sand.

249 He, et al. [45] analysed the effect of the operational time on quartz sand bed particles for a lab-scale  
250 5kW<sub>th</sub> BFB, 30MW<sub>th</sub> BFB, and 122MW<sub>th</sub> CFB. Samples were taken after the addition of a fresh bed,  
251 and at intervals of several hours for the lab-scale unit or every few days for the full-scale plants. The  
252 bed material was replenished at the standard operational rate for the two full-scale units: <3wt% of  
253 the bed per day for the 30MW<sub>th</sub> BFB unit, and 50wt% of the bed per day for the 122MW<sub>th</sub> CFB unit.  
254 He, et al. [45] noted similar layer composition findings to others [39, 40], though there was a time  
255 dependency for their formation.

256 In the case of the 5kW<sub>th</sub> BFB, a single coating layer was found on bed particles. For the 30MW<sub>th</sub> BFB,  
257 a single layer was found on 1 day old particles, whereas older particles displayed an inner  
258 homogenous layer and outer non-homogenous layer. For the 122MW<sub>th</sub> CFB, 3 day old samples  
259 displayed two coating layers, equivalent in composition to the “inner-inner” and “inner” layers  
260 observed by others [39, 40]. An outer layer was found only on 4 and 6 day old particles.

261 Only the 122MW<sub>th</sub> CFB presented an “inner-inner” Si-K-Ca layer. The fuel used in the CFB had higher  
262 ash content than the 30MW<sub>th</sub> BFB (3.1wt% dry, versus 1.8wt% dry) and higher potassium content  
263 (0.18wt% dry, versus 0.11wt% dry). This adds further support to the theory that an inner-inner layer  
264 of Si-K-Ca is only present with sufficient availability of potassium in the fuel [39, 40].

265 Layer growth was tracked over time by He, et al. [45], the results of which are reproduced in Figure  
266 4. XRD analysis on 30MW<sub>th</sub> BFB samples from 3-23 days old revealed that initially K-based  
267 compounds formed the majority of the mass of the layer. This then progressed to the layers  
268 primarily comprising of calcium based compounds such as Ca<sub>3</sub>Mg(SiO<sub>4</sub>)<sub>2</sub>, Ca<sub>2</sub>SiO<sub>4</sub> and Ca<sub>3</sub>SiO<sub>5</sub>.

269 He et al. [45] then gave the following theory for agglomerate formation: Potassium species first react  
270 with the bed particle to form low-melting point potassium-silicates. Layer growth proceeds with the  
271 addition of calcium to this melt, causing precipitation of stable calcium-silicates with high melting  
272 points. The increase in calcium concentration within the layer, and loss of potassium, results in a  
273 weaker driving force for calcium diffusion and reaction, thus a reduced layer growth rate over time.  
274 A higher amount of melt in this inner layer would influence diffusion and reaction of calcium into the  
275 layer, thus influence layer growth rate.

276 Gatternig & Karl [46] have further explored coating-induced mechanisms. Experiments were first  
277 performed with a progressively heated bed, and multiple coating layers were observed aligning with  
278 the findings of others [39, 40].

279 Building on the inward coating growth theory suggested by Brus, et al. [41], Gatternig and Karl [46]  
280 suggested that collisions between two coated particles allows for capillary action to draw coating  
281 melts inwards into the particle. Additionally, from SEM/EDS imaging, visible remains of the  
282 heterogeneous outer coating shell were seen in agglomerate necks/joins. Gatternig & Karl [46]  
283 concluded that the outer coating layer is dry and powdery, a feature observed by others [42], and  
284 that it increases in melt fraction towards the centre. On collision, this shell fractures, allowing for the  
285 inner melt to form a liquid bridge, with remnants of the outer shell being present within it. Such a

286 theory diverges from previous suggestions that bridges between coated particles form during the  
287 initial melt layer phase.

288 Gatternig & Karl [46] also performed experiments with a fluidized bed of sand above a fixed bed into  
289 which fuel was added, to detect the effects of gaseous phase alkali compounds on agglomeration.  
290 No coating layer formation was found, indicating that gaseous or aerosol alkali metals do not  
291 contribute to coating formation. Others have speculated this to be the case, such as Scala & Chirone  
292 [47]. However, the methodology employed by Gatternig & Karl [46] does not allow for other bed  
293 phenomena to proceed, such as localised defluidization and/or bed hotspots, as there is no direct  
294 contact with the fuel. However, such phenomena may provide a temperature gradient over which an  
295 evaporation-condensation cycle could occur.

296 Recently, He, et al. [48] have expanded upon their previous work [45] by means of chemical  
297 equilibria modelling for ash reactions and the development of a diffusion model, using the FactSage  
298 software package. The data used in the model, and for validation, was that of their previous work  
299 [45].

300 Temperature had a large effect on layer growth rate for operation at 850°C. The model predicted  
301 layer thicknesses of 10µm at 5 days of operation and 15µm at 16 days, whilst at 900°C, a thickness of  
302 about 20µm was predicted at 5 days, and 40µm at 16 days. It was suggested that the additional  
303 temperature allowed for increased diffusion of Ca<sup>2+</sup> into the inner melt layer, hence greater layer  
304 growth.

305 The decrease in inner layer growth rate over time is suggested as being due to changes in inner layer  
306 composition. Ca<sup>2+</sup> diffusivity was higher in Ca<sub>2</sub>SiO<sub>4</sub> than in Ca<sub>3</sub>SiO<sub>5</sub>, but it is the latter which increases  
307 in concentration within the inner layer over time. Furthermore, the physical growth of the layer  
308 would increase the diffusion distance, further impacting calcium diffusion.

309 The agglomerate coating layer growth mechanism thus suggested by He, et al. [48] is reproduced in  
310 Table 2.

311 When He, et al. [48] validated the model against experimental data, the model was found to provide  
312 a good indication of starting and ending coating layer thickness, though did not match the variations  
313 in layer growth rate that happened on smaller timescales. This highlights an area for further work:  
314 accurately modelling layer growth rate over the entirety of coating layer growth periods. This would  
315 be of particular use for full-scale FBC units, as bed material is removed and replenished during  
316 operation [17, 49]. The ability to accurately model and predict coating layer thicknesses across the  
317 bed at any point in time could allow for optimisation of bed replenishments frequencies.

## 318 **2.2 Melt-induced Agglomeration**

319 Olofsson, et al. [28] proposed an agglomeration formation mechanism, “heterogeneous  
320 agglomeration”, and stated that this arises due to localised “hot-spots” of over 1000°C, versus given  
321 operational temperatures of ~670-870°C, allowing the creation of a melt phase of alkali-silicate  
322 derived from both fuel ash and bed material. The largest agglomerates had glass-like appearance,  
323 indicating prolonged exposure to high temperatures, and were 50-60mm in size, and frequently  
324 caused defluidization. Olofsson, et al. [28] speculated that the causation of “hot-spots” in the bed  
325 was a combination of small fuel feed fluctuations and temporary gas channelling through the bed  
326 leading to localized fluidization disturbances.

327 The later work of Lin, et al. [50] presented an alternative melt-induced agglomeration mechanism,  
328 from combustion of wheat straw on a quartz sand bed. After two minutes of combustion at a bed  
329 temperature of 720°C, weak agglomerates were present in the form of a charred fuel pellet with  
330 sand particles weakly attached. After two minutes of combustion at 920°C, the agglomerates were  
331 stronger and there was far less of a char core present. After ten minutes of combustion, the char  
332 core had fully combusted leaving hollow sand agglomerates in the shape of the fuel pellet.

333 Lin, et al. [50] proposed a mechanism as follows: Burning char particles had been observed as being  
334 at higher temperatures than bed particles, and go from partially to almost completely molten  
335 between 750-900°C. When bed particles collide with these molten char particles, they may adhere  
336 to them, and become coated with the molten char melt. As the char particle burns away, the sand  
337 particles would remain stuck together. Such a conclusion is supported by their results: two minutes  
338 of combustion at 920°C versus 720°C resulted in a stronger agglomerate, therefore there could be  
339 more of a molten char melt hence a stronger agglomerate forms. Additionally, at this temperature  
340 sintering may have strengthened the agglomerate.

341 Visser [40] put forth a melt-induced agglomeration formation mechanism from a comparison  
342 between a lab-scale FBC unit and an 80MW<sub>th</sub> FBC plant, and described it as the result of collisions  
343 between bed particles or larger ash particles, which adhere to one another due to molten ash  
344 particles that function as a viscous glue. It is notable that whilst similar in nature to the method of  
345 Lin, et al. [50], it does not suggest that larger molten char particles may act as a platform from which  
346 agglomerates can grow.

347 Chirone, et al. [51] examined agglomeration behaviour when combusting pine seed shells, using lab-  
348 scale and pilot-scale equipment. Chirone, et al. [51] proposed that bed particles stick to melting char  
349 particles which then burn away, leaving behind hollow agglomerates in the shape of fuel particles.  
350 Chirone, et al. [51] further suggested that combusting char particles act as a localised temperature  
351 “hot-spot”. This causes more severe melting and thus more severe agglomeration than coating-  
352 induced agglomerates typically display.

353 Scala & Chirone [47] studied mechanisms of agglomeration with a lab-scale unit using olive husk  
354 fuel. A prior examination of the literature revealed that temperature had negligible effects on alkali  
355 deposition rate, and experimentation with variable air flow rates to control temperature gave little  
356 change in amounts of bed ash. Scala & Chirone [47] concluded that vaporisation and condensation  
357 pathways for alkali deposition likely had a negligible effect on agglomeration. Scala & Chirone [47]



358 proposed a mechanism for agglomeration: Ash is transferred to bed particles via collisions with small  
359 fine ash or large coarse char particles. Alkali species then physically diffuse through the ash and  
360 interact with silica to form a eutectic. From the observations of others [50, 51], Scala and Chirone  
361 [47] then stated that the transfer of alkali species by collision and their melting behaviour was likely  
362 promoted by high temperature char particles. With sufficient temperature and alkali content in the  
363 bed, defluidization will occur. If the bed temperature is not high enough to melt the eutectics,  
364 burning char particles may provide a “hot-spot” that can drive melt formation and the accumulation  
365 of smaller agglomerates, which can defluidize the bed.

366 Liu, et al. [52] looked at melt-induced phenomena, when combusting rice straw, and suggested that  
367 the presence of K and Na components on the exterior of fuel fragments would allow them to form  
368 adhesive alkali-silicates with relative ease. Large ash fragments ( $>10\mu\text{m}$ ) may then bind together bed  
369 material, as was evidenced by agglomerates being conjoined by necks of similar composition to that  
370 of the fuel ash.

371 Gatternig & Karl [46] provided further evidence in support of the melt-induced agglomeration  
372 behaviour seen by Lin et al. [50] and Chirone, et al. [51]. Gatternig & Karl [46] first observed that  
373 denser fuel particles, such as wood pellets, were fully submerged in the bed during combustion thus  
374 had similar temperatures to the bed itself. When testing less dense hay pellets, the pellet “floated”  
375 on top of the bed and reached temperatures up to  $400^{\circ}\text{C}$  higher than the bed. This would be  
376 sufficient to produce molten ash fuel pellets to drive the melt-induced agglomeration mechanisms  
377 proposed by Lin, et al. [50], and may offer one explanation for temperature “hot-spots”. Gatternig &  
378 Karl [46] state that lower density fuels, typically herbaceous ones, will likely undergo this behaviour.  
379 This aligns with the experiences of Lin, et al. [50], whom used low density wheat straw, Chirone, et  
380 al. [51] whom used pine seed shells, and Olofsson, et al. [28], whom recorded the occurrence of  
381 “hot-spots” and more severe agglomeration when lower density fuels were used (sawdust, straw,  
382 and meat and bone meal).

383 An aspect not explored within the literature is the relative presence of silica and alkaline metals  
384 within the ash to drive melt-induced agglomerate formation. The fundamental difference seen  
385 between coating-induced and melt-induced agglomeration, present throughout the literature, is that  
386 the former involves the interaction of alkaline metals with silica in the bed material, whilst the latter  
387 relies on the presence of both silica and alkali metals in the ash to form an alkali-silicate ash melt  
388 [40, 53]. The fuels used in the majority of the works above where severe melt-induced  
389 agglomeration occurred were generally herbaceous with high silica content in the ash [46, 47, 28,  
390 50, 52]. Therefore, there may be a point at which the melt-induced mechanism takes precedence  
391 over coating-induced agglomeration as the dominant mechanism for agglomeration, due to the  
392 relative availability of silica in the ash.

### 393 **2.3 Physical Agglomeration Mechanisms**

394 There are several larger, bed-scale mechanisms, which may assist or propagate agglomeration.  
395 These mechanisms have been explored and exploited in other industries, with comprehensive works  
396 available, such as those of Pietsch [54, 55].

397 The first of these mechanisms is sintering, a mechanism frequently referenced in the literature [33,  
398 36, 40, 41]. This is the process by which bridges between particles are formed or strengthened by  
399 the diffusion of surface matter across particle boundaries, resulting in particles being fused together.  
400 Sintering can be pressure or temperature driven, though in the context of atmospheric FBC of  
401 biomass is temperature driven.

402 Tumble or growth agglomeration is a result the of sum of all forces acting to adhere the particles  
403 being greater than the sum of those acting against the adhesion. The ash melts or coating layers that  
404 form on or between bed particles provide an additional adhesive force between the particles, thus  
405 making it easier for agglomerates to form.

406 A “molecular cramming” mechanism was first suggested by Anthony et al. [56]. It was proposed that  
407 the increase in molar volume when converting calcium oxide in deposits to calcium carbonate and

408 then to calcium sulphate led to it filling any available pores or inter-particle space and produced  
409 denser deposits. It was further suggested that higher quantities of materials such as iron-,  
410 aluminium, and silicon-oxides in fuel ash may create small discontinuities in deposits that are  
411 enhanced by molecular cramming and allow them to fracture more easily. There has been some  
412 further supporting evidence for this theory [57, 58], though it appears there has been no conclusive  
413 proof at the full-scale, or in the context of biomass fuels.

414 A final mechanism is pressure agglomeration [54, p. 504] whereby bonding and densification occur  
415 through the application of an external force. In the context of atmospheric FBC of biomass, this may  
416 occur around changes in bed geometry whereby particle can be pressed together, such as around  
417 baffles or in-bed heat exchange tubes. Pressure agglomeration may also compliment tumble  
418 agglomeration, as the larger agglomerates cause by the latter obstruct particle motion and cause  
419 variances in pressure, allowing for pressure agglomeration to occur.

420 As can be imagined, both sintering and tumble agglomeration would enhance coating-induced and  
421 melt-induced agglomeration. The larger, stronger agglomerates that result would also allow for  
422 further localised temperature variation, which may allow for “hot spots” that could drive the  
423 formation of larger melt fractions, further worsening agglomeration.

## 424 **2.4 Summary of Agglomeration Mechanisms**

425 The current knowledge of agglomeration mechanisms can be summarised as follows (shown  
426 diagrammatically in Figure 7 and Figure 8):

### 427 **Coating-induced agglomeration (Figure 7)**

428 There is broad agreement that this mechanism is initiated via the formation of a molten adhesive  
429 alkali-silicate melt upon the surface of bed particles, usually potassium-silicate, though in some cases  
430 sodium-silicates if sufficient quantities are present in the fuel [38]. This layer forms via the  
431 accumulation of K-compounds from fuel ash on silicate-rich bed particles, under temperatures in

432 excess of 750°C. Initial layer formation may be influenced through condensation of gaseous K-  
433 species from fuel ash onto bed particles [36, 40, 43].

434 This K-silicate layer then grows inwards via reaction with silicate species in the bed material [41].  
435 There may be the effects of capillary action from cracks in the bed particle drawing K-compounds  
436 further inwards after collisions with other coated particles [46]. Any silica within the fuel ash may  
437 also react together with potassium species on the bed material surface to generate more of a melt.  
438 Calcium species from the outer ash layer begin diffusing into the molten K-silicate inner layer and  
439 react to form stable species with silicate with melting points in excess of 1000°C, such as  $\text{Ca}_2\text{SiO}_4$  and  
440  $\text{Ca}_3\text{SiO}_5$  [45].

441 At the end of this process, bed particles typically possess two- or three-layer coatings. In the case of  
442 a two-layer coating, there is an inner homogenous layer rich in Ca-silicate compounds, and an outer  
443 heterogeneous layer whose composition is broadly in line with that of the fuel ash [44, 45, 46]. In  
444 the case of three layer coating systems, there is an additional “inner-inner” homogenous layer, rich  
445 in silicate, K, and Ca [40, 45]. The causation of this inner-inner layer has been speculated as the  
446 presence of high amounts of K in the fuel [40], or perhaps the lack of diffusive driving force for Ca to  
447 diffuse and react all the way to the bed particle-coating layer boundary [45, 48]. The outer ash layer  
448 appears to prevent formation of further K-silicate melts, by denying K-compounds access to the  
449 silicate of the bed material with which it would otherwise form a melt. In particular, magnesium in  
450 the outer ash layer has been identified as preventing alkali-silicate melt formation [39].

451 Agglomeration appears to proceed at any point during layer formation. Bed particles collide, in some  
452 cases breaking the outer ash layer [46], and enable that formation of a K- or Ca-silicate neck  
453 conjoining bed particles [36, 40, 51]. Temperature-induced sintering may occur on the agglomerate,  
454 strengthening it [36, 40, 41, 42] and with sufficient accumulation of agglomerates defluidization  
455 occurs.

456 **Melt-induced agglomeration (Figure 8)**

457 The central idea of melt-induced agglomeration is the collision of larger molten ash particles with  
458 bed particles, where the molten ash particles act as a viscous glue [40, 47, 51]. Scala & Chirone [47]  
459 suggest that burning char particles create a localised hotspot that further enhances the adhesive  
460 potential of this “viscous glue”. The resultant agglomerates are characterized by displaying a more  
461 severe melting and agglomeration than traditional coating-induced agglomerates [51].

462 A notable variant to melt-induced agglomeration is when molten char particles act as a platform for  
463 agglomerates to grow, as was first described by Lin, et al. [50]. Combusting char fragments have  
464 elevated temperatures in comparison to the bed average, and become almost completely molten at  
465 around 900°C. In collisions with bed particles, the bed particles adhere to the char fragment and the  
466 viscous alkali-silicate melt on its surface. This coats the bed particles, and propagates further  
467 adhesion of bed particles. Eventually, the char fragment fully combusts, typically leaving an  
468 agglomerate with a hollow centre in the shape of the initial fuel fragment. The agglomerate  
469 retaining the shape of the fuel particle is likely due to the ash skeleton of the fuel particle that  
470 remains after combustion of the fuel pellet, a topic discussed in the work of Chirone, et al. [59]  
471 (further discussed in section 3.6).

472 The elevated temperature during char combustion would allow for sintering of the agglomerate,  
473 strengthening it. Gatternig & Karl [46] extended this theory, stating that less dense fuels, e.g. straws,  
474 were observed to “float” on top of the fluidized bed whilst combusting, as opposed to being  
475 submerged within the bed, and were exposed to higher temperatures. Moreover, Olofsson, et al.  
476 [28] observed temperature hot-spots whilst utilizing less dense fuels, perhaps also due to this  
477 “floating” behaviour.

#### 478 **Recommendations for further work**

479 Agglomeration mechanisms when using non-SiO<sub>2</sub> based bed materials have not received a great deal  
480 of work. Both Nuutinen, et al. [39] and Grimm, et al. [44] used Mg-based materials (the former a  
481 proprietary material, the latter Olivine). Clearly, potassium will not react with silica in the bed

482 material to generate a K-silicate melt, yet layer formation still occurred. This is perhaps indicative of  
483 a melt-induced type mechanism, though further work is needed to clarify the exact mechanisms  
484 under which layer growth is occurring for non-SiO<sub>2</sub> based bed materials.

485 Use of chemical equilibria modelling software such as FactSage has received increased attention in  
486 recent years due to improvements in the accuracy and quality of databases. The work of He, et al.  
487 [48] resulted in a relatively accurate model of coating layer growth in a silica sand and wood fuel  
488 scenario. However, intermediate variances and fluctuations in growth rates weren't fully captured  
489 by the model, presenting an opportunity for future improvement. A more comprehensive model of  
490 coating growth rate would allow for optimisation of bed replenishment in industrial facilities, and  
491 allow for minimisation of agglomeration risk through prediction of the coating distribution across the  
492 bed inventory. Beyond this, similar coating growth and ash melt models would be of use for  
493 different fuels and alternative bed materials, again with the intention of informing agglomeration  
494 risk at the industrial scale.

495 Related to this would be investigation into bed scale variances in coating composition and the  
496 relative frequency and distribution of coated bed particles across the bed. If certain zones are found  
497 to be particularly problematic with regards to enabling agglomeration, targeted control and  
498 prevention methods may be possible.

499 Melt-induced agglomeration proceeds with sufficient silica and alkali metal content in the fuel ash.  
500 However, it appears there has been no work to find a point at which the more severe melt-induced  
501 agglomeration becomes the dominant form of agglomeration within the bed, due to fuel ash  
502 composition. Such a value would help further inform fuel selection and fuel blending trials. Related is  
503 a more general, secondary area for work, on transition points and relationships between melt-  
504 induced and coating-induced agglomeration occurrence.

### 505 **3. Effect of Operational Variables on Agglomeration**

#### 506 **3.1 Temperature**

507 The effects of temperature on agglomeration have been extensively researched within the  
508 literature. The general trend exhibited is that with increases in temperature, there is an increase in  
509 the severity of agglomeration because of the increased presence of liquid and gas phases.

510 Ultimately, this leads to a reduction in the defluidization time,  $t_{def}$  [50, 43, 60]. The elevated  
511 temperatures increase the melt fraction within the ash, and decrease the viscosity of the melt [50].  
512 This results in a more abundant and more mobile melt, leading to more severe agglomeration. The  
513 temperatures at which FBC operate at (750-900°C) are within the range at which alkaline metal  
514 complexes melt. Furthermore, the modelling efforts of He, et al. [48] highlighted that increases in  
515 temperature of 50°C may lead to a 2-3x increase in coating layer growth rate. This elevated growth  
516 rate would make it easier for neck formation between coated particles during collisions, due to the  
517 availability of a larger melt layer, thus worsening agglomeration.

518 Conversely, lower bed temperatures delay the onset of agglomeration defluidization. For example,  
519 Yu, et al. [61] found that  $t_{def}$  more than quadrupled from 60 minutes to 270 minutes by reducing the  
520 operating temperature for burning straw from 800°C to 650°C. However, it is important to consider  
521 that at plant scale, the end goal of combusting biomass is often to raise steam. Lowering combustion  
522 temperatures will limit the conditions of the steam that can be raised, having large impacts  
523 downstream of the boiler, such as on turbine efficiency [17]. Therefore, bed temperatures are likely  
524 to be constrained by steam requirements.

#### 525 **3.2 Pressure**

526 Most literature on agglomeration when using biomass utilises Atmospheric FBC (AFBC) units.  
527 However, PFBC units have been seen to experience similar agglomeration phenomena to AFBC units.  
528 The work of Olofsson, et al. [28] utilised a PFBC unit, showing similar phenomena to later work by

529 others who used AFBC equipment. Recent work by Zhou, et al. [62] looked at agglomeration during  
530 Pressurised Fluidized Bed Gasification of biomass, which appeared to exhibit similar coating  
531 phenomena to what would be experienced during AFBC of biomass. However, caution should be  
532 taken when drawing comparisons between AFBC and PFBC agglomeration mechanisms, as whilst the  
533 end result may be the same, the pathway there may differ.

### 534 **3.3 Fluidizing Gas Velocity**

535 The fluidizing gas velocity,  $U$ , has an important role to play in determining the fluidization regime in  
536 any FBC system [15, 63]. Over the years, numerous researchers have looked at the effect of varying  
537  $U$ , or the ratio  $U/U_{mf}$ , known as the fluidization number, on agglomeration and defluidization.

538 Lin, et al. [50] doubled  $U$  whilst maintaining the same combustion conditions through use of  $N_2$ . This  
539 increased  $t_{def}$  by 30%. Chaivatamaset, et al. [64] found that increases to  $U$  of 28% and 60%, led to  
540 average increases of  $t_{def}$  for two different fuels of 56% and 95% respectively. Lin, et al. [65] recorded  
541 increases in  $t_{def}$  with successive increments in  $U$ , across four types of particle size distribution  
542 (narrow, Gaussian, binary flat). Yu, et al. [61] observed reduced agglomeration by increasing  $U/U_{mf}$   
543 by a factor of 1.6, noting that agglomerates no longer presented themselves as larger clumps, but as  
544 a few bed particles attached to an ash fragment.

545 It is clear then that increases in  $U$  or  $U/U_{mf}$  will cause an increase in  $t_{def}$ . With increases in  $U$ , bed  
546 particles gain momentum thus are more likely to overcome adhesive forces during collisions with  
547 coated bed particles and molten ash particles [50, 65]. Furthermore, higher  $U$  values would lead to  
548 more vigorous bed mixing. This in turn would reduce the chance of certain areas experiencing poor  
549 fluidization; a behaviour suspected to propagate agglomeration.

### 550 **3.4 Gas Distribution Uniformity**

551 An aspect that has received little direct investigation is that of the fluidizing gas distribution  
552 uniformity on agglomeration. Bubbles will form at the bottom of the fluidized bed as gas is released



553 from the gas distribution plate. These bubbles will coalesce into larger ones as they rise through the  
554 bed [15]. This bubble movement drives fluidisation and heat transfer within the bed, as well as how  
555 well mixed it is [66], thus if impaired may have significant effects on operation.

556 Oka [67] suggests that with damaged bubble cap, thermal diffusivity across the bed would be  
557 reduced and the bed hydrodynamics would be altered. This would create regions of high and low  
558 turbulence, and lead to temperature gradients across the bed that may assist or accelerate the  
559 formation of agglomerates. Kuo, et al. [68] trialled a fixed grate furnace with wood fuel, and gave a  
560 comparison between sidewall air injection and under-grate air injection. They noted that changing  
561 the air distributor configuration had significant effects on flame coverage, and led to higher and  
562 lower temperature regions within the furnace. This behaviour could increase the rate of  
563 agglomerate formation. Lin, et al. [65] found that a temporary burst of high velocity air was  
564 sufficient to break apart in-situ agglomerates and postpone a defluidization event. This could imply  
565 that a region of higher turbulence in the bed may be beneficial for minimising agglomerate  
566 formation.

567 The work of Chilton [69, pp. 225-291] aimed to test the effects of non-uniform air distribution when  
568 using five different biomasses in a 200kW<sub>th</sub> FBC unit. A uniform air distributor with 30 evenly spaced  
569 bubble caps was compared against with one that had 18 slightly larger bubble caps plus an ash chute  
570 occupying one corner of the distributor. The ash chute had an air gap around it, allowing for air  
571 leakage and further non-uniformity. Use of the non-uniform plate created greater variations in  
572 temperatures across the bed and freeboard, and in emissions. Data on defluidization times was less  
573 conclusive. Peanuts and straw experienced reductions in defluidization time of 10% and 40%  
574 respectively with the non-uniform air distribution plate, whilst oats experienced an increase of 181%  
575 and miscanthus an increase of 73%. Whilst this does not provide a conclusive result on the effects of  
576 gas distribution uniformity on agglomeration, it does indicate that differences in distribution plate

577 design, and the effects of bubble cap failures or leaks, can be significant on defluidization times. It  
578 also shows that it is an area where future work may be useful, albeit challenging to execute.

### 579 **3.5 Static Bed Height**

580 Lin & Wey [53] examined the effects of static bed height on  $t_{def}$  during FBC of waste. Increases in the  
581 Bed Height to Diameter ratio ( $h_{bed}/d_{bed}$ ), produced a non-linear decline in  $t_{def}$  (Figure 9). The  
582 explanation cited was reduced vertical mixing with increasing bed height, allowing for agglomeration  
583 to proceed more easily upon release of alkali-metals from ash. However, a reasoning was not  
584 proposed for the rate of this decline, in particular from  $2.0h_{bed}/d_{bed}$  and  $2.3h_{bed}/d_{bed}$ . This is perhaps  
585 indicative of some larger change in the bed dynamics when moving between these two bed heights,  
586 thus allowing for defluidization to occur much sooner. However, this was not explored further.  
587 Moreover, the timescales of  $t_{def}$  are all below 15 minutes, meaning that smaller irregularities e.g. in  
588 fuel feeding, may have a large proportional impact on the results.

589 Chaivatamaset, et al. [64] examined the effect of static bed height on  $t_{def}$ , and observed behaviours  
590 that were opposite to those noted by Lin & Wey [53]. Doubling  $h_{bed}$  whilst maintaining the same  
591 fluidizing gas velocity, temperature and bed particle size resulted in increases in  $t_{def}$  of between 5-  
592 55%, dependent upon the fuel and fluidizing velocity. Corncob typically showed greater percentage  
593 increases than Palm Shell in response to increases in static bed height. No further comparison was  
594 performed between agglomerates from the two different static bed heights examined.

595 It may be of interest to further examine the effects of static bed height on agglomeration,  $t_{def}$ , and  
596 determining any relationships that may exist. A larger static bed height is known to allow the  
597 coalescence of bubbles to larger sizes, and causes increased turbulence at the top of the bed [70].  
598 This behaviour may also influence that seen through the observations of Gatternig & Karl [46],  
599 whom noted that low density fuel pellets floating on the bed surface caused severe melt-induced  
600 agglomeration. Therefore, the effects on agglomeration of bubble size and behaviour at the bed  
601 surface may be worthy of investigation.

602 **3.6 Fuel**

603 **Fuel Type**

604 The effects of different fuels on agglomeration have been extensively researched. As noted in the  
605 introduction, fuel and ash composition can vary massively across different biomass fuels [10, 11]. As  
606 illustrated in section 2, the presence of alkali and alkali earth metals within fuel ash is a key  
607 contributing factor to agglomeration severity.

608 Works such as those by Skrifvars, et al. [34], Öhman, et al. [36], and Brus, et al. [41], have looked at  
609 fuels across a variety of different biomass categories. Fuels with high amounts of alkali metals within  
610 their ash agglomerate more quickly, and at lower temperatures. For example, fuels such as straws  
611 are particularly bad due to their high potassium contents, as discussed by Yu, et al. [61]. As a general  
612 comment, fuels with a combination of high silica content and high alkali content, such as straws,  
613 seem predisposed to agglomerating via melt-induced agglomeration, as the fuel ash itself has the  
614 necessary material to create an alkali silicate melt. In industrial and plant-scale settings, woody fuels  
615 have emerged as the preferred fuel type for FBC of biomass, due to their less severe agglomeration  
616 tendencies [17].

617 **Co-firing**

618 Co-firing of biomass fuel blends may be performed due to economic and operational needs, for  
619 example balancing usage of a better quality, more expensive fuel with a poorer, cheaper one [71, 72,  
620 17]. Whilst there is a sizable body of research available on co-firing of coal-biomass blends, there are  
621 fewer systematic studies available on biomass fuel blends and the effects of altering blend ratios.  
622 Hupa [71] notes that there was an increasing number of FBC boilers employing co-firing in the 2001-  
623 2002 period, some of which using biomass-only fuel blends, and this amount would likely have only  
624 increased with time as there are more FBC units online thus greater competition for biomass fuels. A  
625 recent review on biomass combustion and ash behaviours by Hupa [73] again notes the lack of  
626 knowledge surrounding co-firing of biomass blends.

627 Salour, et al. [74] blended rice straw with wood, in order to control the severe agglomeration  
628 ordinarily caused by rice straw. When combusted at a bed temperature at or below 800°C, blends of  
629 up to 50% rice straw were acceptable. Beyond this,  $t_{\text{def}}$  decreased with increasing rice straw fraction.  
630 Salour, et al. [74] also measured key ash fusion temperatures such as the initial deformation  
631 temperature (IDT). These were found to be non-linear in behaviour, Figure 10 providing an example.  
632 Non-linear behaviours such as these add difficulty in predicting the behaviour of fuel blends, and  
633 highlight the need further systematic studies of behaviour with blend variations.

634 Davidsson, et al. [75] examined the effects of biomass co-firing in a 12MW<sub>th</sub> CFB with a mixture of  
635 86% wood and 14% straw pellets on an energy basis. This produced a high level of alkali deposits  
636 compared to their coal based tests, a result of alkali metal content in the straw. Concentrations of  
637 KCl in the flue gas rose from around 3-4ppm with wood pellets to 20ppm with the 14% straw blend.

638 Thy, et al. [76] investigated agglomeration behaviour of a blend of wood with between 2.6-25.0wt%  
639 rice straw. They found a strong positive correlation between increasing amount of straw and  
640 severity of agglomeration, with blends of 2.6wt% rice straw producing mild agglomeration whilst  
641 those of 9.6% and above resulted in defluidization and large plugs of agglomerates being extracted.  
642 A visual estimation of the proportion of the bed that suffered from agglomeration produced an  
643 exponential relationship between percentage agglomerated and percentage rice straw content.

644 Elled, et al. [77] explored usage of a wood-straw fuel blend. A two layer coating was formed on bed  
645 particles, the inner layer dominated by potassium silicates, whilst the outer layer comprised  
646 primarily of calcium silicates. Whilst these results broadly align with what is typically seen in a single  
647 fuel system, a closer comparison was not drawn.

648 Silvennoinen & Hedman [78] examined the effects of co-firing wood biomass with up to 30wt%  
649 sunflower seed hull pellets or oat seeds, in a 75MW<sub>th</sub> commercial BFB. During their experimentation,  
650 no agglomeration was detected, a result of an intentional reduction of temperature to 750°C which  
651 would bring the system to just above the melting point of potassium-silicate eutectics (742°C).

652 Becidan, et al. [79] modelled the effects of a binary system consisting of straw with either peat or  
653 sewage sludge on alkali chloride formation; a key driver of corrosion [25, 26]. Non-linear  
654 relationships were exhibited with increasing weight percentages of peat or sewage sludge, and the  
655 mechanisms and elements affecting formation and decomposition of alkali chlorides changed with  
656 fuel blend ratios. This further highlights the complexities of using biomass fuel blends.

657 The works of Suheri & Kuprianov [80] and Sirisomboon & Kuprianov [81] looked at varying blend  
658 ratios of binary biomass mixtures, as well as combustion excess air ratios, on emissions and  
659 combustion efficiency. Emissions behaviours here seemed to scale more proportionately between  
660 varying secondary fuel percentages.

#### 661 **Fuel Particle Size**

662 Lin, et al. [50] performed an experimental run with smashed straw pellets of particle size <1mm, to  
663 compare against straw pellets of sizes 1-10mm, but did not find a notable change in  $t_{def}$ . The work of  
664 Yu, et al. [61] looked at the effect of straw fuel size, with a comparison of small straw bales against  
665 milled straw powder, in a lab-scale BFB. Use of the powder allowed for a total fuel feeding of 281g,  
666 as opposed to 110g for the bales. However, the low density of straw powder may allow for it to be  
667 easily entrained within the flue gas. An analysis of the amount of unburnt carbon within the fly ash  
668 in not provided, nor an analysis of the potassium retained within the bed at the end of the run.

669 Therefore, it cannot be stated if this elevated level of fuel feeding before defluidization is simply due  
670 to fuel becoming entrained within the flue gas.

671 Burton & Wei [82] looked at the effect of fuel particle size in the context of Fluidised Bed Pyrolysis. A  
672 relation between biomass fuel particle size and 'Sand Loading' was drawn; this latter term being  
673 defined as the mass of bed sand adhered to fuel particles normalised against the total mass of fuel  
674 fed. Sand Loading increased with fuel particle size up to 430 $\mu$ m, and then decreased until reaching a  
675 plateau at around 1500 $\mu$ m. This was suggested as being due to transfer of the sticky alkali coating

676 within the fuel particle being convection controlled to a particle size of 430 $\mu$ m, and diffusion  
677 controlled at larger sizes.

678 Also related are the combustion profiles of a fuel. Chirone, et al. [59] performed a comprehensive  
679 investigation into combustion profiles and characteristics of three pelletized fuels: wood, straw, and  
680 sludge. Fuels underwent several repetitions of a combustion-quenching process, in order to examine  
681 the condition and structure of fuel pellets at successive times. With sludge a “shrinking core” pattern  
682 was seen, where the initial size of the pellet was preserved with an ash skeleton that remained after  
683 burn-off of the carbon. Wood followed a “shrinking particle” pattern, whereby the pellet slowly  
684 shrank and fragmented over time. Straw took a pathway almost between these two. Shrinkage of  
685 the pellet was observed, but an ash skeleton did remain, and said skeleton had bed sand adhered to  
686 it. This ash skeleton supports the melt-induced agglomeration observations of Lin, et al. [50] and  
687 Chirone, et al. [51] whereby an agglomerate is formed in the shaped of a fuel particle (section 2.2).

#### 688 **Fuel Moisture**

689 Fuel moisture has not been investigated in relation to agglomeration behaviour in the literature. This  
690 may be of interest due to the high relatively moisture content of biomass fuels, e.g. wood has been  
691 reported as having a moisture content of 40-70% [27]. This moisture content affects parameters  
692 such as the fuel heating value, bed temperatures, and flue gas composition during combustion [10,  
693 27]. Higher moisture content negatively affects the overall boiler efficiency, as additional heat  
694 energy is used on the fuel drying phase of combustion, and larger variations in moisture content will  
695 affect combustion control [83]. However, it is known that water will leach out soluble fractions alkali  
696 and alkali earth metals responsible agglomeration problems [11], thus there is some benefit in the  
697 fuel initially being exposed to a higher moisture content.

#### 698 **Fuel Feeding Rate**

699 Fuel feeding rate has not been directly investigated as a factor, largely because a higher fuel feeding  
700 rate for a FBC unit would imply a higher thermal rating. Therefore, higher temperatures will naturally  
701 result, the effects of which are described in section 3.1. Moreover, it will of course provide more fuel  
702 ash to drive agglomeration.

### 703 **3.7 Bed Material**

704 As is evident throughout section 2, the common denominator for agglomeration is the presence of  
705 large quantities of silica within the bed material. Thus, research has been ongoing for alternative bed  
706 materials. A selection of these results have been summarised in Table 3.

707 Substituting SiO<sub>2</sub>-based sands for materials dominant in Mg, Al or Ca has a proven positive effect on  
708 reducing agglomeration, as doing so reduces or eliminates the availability of silicon for  
709 agglomeration. The exception is for fuels that contain sufficient amounts of Si to drive the formation  
710 of alkali-silicate melts themselves, such as straw, as seen in several works [44, 75, 61]. Use of  
711 different bed materials does still have some positive effect on lengthening  $t_{def}$  in these cases though.  
712 More recently, Knutsson, et al. [84] investigated the potential of mixing bed materials to balance  
713 performance and economic aspects, an idea little explored in the literature. Varying mixtures of one  
714 to all of silica sand, bauxite (Al<sub>2</sub>O<sub>3</sub>), K<sub>2</sub>CO<sub>3</sub>, and CaCO<sub>3</sub>, were thermodynamically modelled and tested  
715 experimentally. The presence of bauxite with silica sand or K<sub>2</sub>CO<sub>3</sub> weakened agglomeration tendency  
716 over silica sand alone, as did blends with CaCO<sub>3</sub>, which had a stronger effect on reducing  
717 agglomeration tendency. Knutsson, et al. [84] state that calcium forms a barrier preventing further  
718 diffusion of potassium into silicate melts. This appears to be an exploitation of the protective  
719 capabilities of calcium described by He, et al. [45], by forming a calcium-silicate protective layer  
720 faster than one would otherwise arise during the natural progression of coating-induced  
721 agglomeration.

722 Corcoran, et al. [85] trialled a blend of quartz sand with up to 40wt% Ilmenite (FeTiO<sub>3</sub>) when  
723 combusting wood. It was found that a very thin layer of potassium from fuel ash would initially form

724 on the Ilmenite, and this would disappear as the potassium diffused into the bed particle, thus  
725 removing its availability for driving agglomeration and corrosion. Iron was found to migrate  
726 outwards to the surface of the Ilmenite bed particle, and calcium from fuel as was observed to form  
727 a layer on the surface of the Ilmenite particle. This may have prevented further diffusion of  
728 potassium inwards, similar to the calcium observations of Knutsson, et al. [84] and He, et al. [45].  
729 Recently, energy supplier E.ON has begun using an Ilmenite-based bed material named “Improbed”  
730 in several of their FBC units [86].

### 731 **3.8 Bed Material Particle Size**

732 Figure 11 provides graphs of the effect of changing average bed particle size on  $t_{def}$  from four  
733 separate works. The trend exhibited is that with an increase in bed particle size, there is a reduction  
734 in  $t_{def}$ . Some notes on these graphs are as follows:

- 735 • Lin, et al. [50] maintained a constant temperature and superficial gas velocity,  $U$ , between  
736 the two  $d_p$  values. They suggested that poorer mixing due to the smaller  $U/U_{mf}$  ratio for the  
737 larger particles led to a lower  $t_{def}$ .
- 738 • Chaivatamaset, et al. [64] also maintained a constant fluidizing gas velocity across the bed  
739 particle sizes. Tests for all fuels at 900°C also showed decreases in  $t_{def}$  with increases in  $d_p$ .
- 740 • Yu, et al. [61] used a near constant  $U/U_{mf}$  value for all three particle sizes, as opposed to  
741 maintaining a constant  $U$  value as Lin, et al. [50] and Chaivatamaset, et al. [64] did. However,  
742 Yu, et al. [61] also hand fed bundles of straw every 20 seconds as fuel. This non-continuous  
743 fuel feeding method have affected results somewhat.
- 744 • Lin & Wey [53] combusted Municipal Solid Waste (MSW) within a Fluidized Bed, a fuel with  
745 similar agglomeration characterisations to biomass due to its high Na content. They note  
746 that sand particles up to 770 $\mu$ m acted as a Geldart Group B powder, whilst the 920 $\mu$ m sand



747 acted as a Group D powder. This change in Geldart classification is accompanied by a sharp  
748 decline in  $t_{def}$ .

749 The distinction between the Geldart particle classifications by Lin & Wey [53] is perhaps an  
750 important one: particles in Group B favour bubbling behaviour at  $U_{mf}$ , whilst Group D will spout as  
751 they more readily form large bubbles [87, 15]. This raises the question of the potential impact of  
752 different Geldart powder classifications on agglomeration during FBC of biomass, and if a wider  
753 study may reveal relationships between particle size, Geldart particle classification, and  
754 agglomeration. For example, perhaps the bubbling behaviour of Group B acts to minimize the  
755 formation of potential agglomerates by improved bed mixing, whereas Group D materials may allow  
756 for bed material to end up grouped together, promoting temperature non-uniformities and  
757 agglomerate formation.

758 Scala & Chirone [60] reported a different trend for increases in  $d_p$  (Table 4). Increases in  $d_p$  by a  
759 factor of 2-3 led to an approximate doubling of  $t_{def}$  for all fuels and scenarios. In the Pine Seed Shells  
760 data fuel feed rate was reduced to increase amounts of excess air which may explain increases in  
761  $t_{def}$ . However, this was not the case for the virgin olive husk fuel, which exhibited the same trend.  
762 The reasoning for this put forth by Scala & Chirone [60] was that large particles will participate in  
763 more energetic collisions, making it harder for adhesive forces to mitigate these and cause adhesion  
764 between the particles.

765 Lin, et al. [65] performed a comprehensive study on the effects of different  $d_p$  distributions of sand  
766 on  $t_{def}$ , albeit for MSW as opposed to biomass. Four  $d_p$  distributions were selected:

- 767 • A narrow distribution of  $d_p$  between 590-840 $\mu\text{m}$
- 768 • A Gaussian distribution where  $d_p$  ranged between 350-1190 $\mu\text{m}$
- 769 • A Binary distribution where 59% of bed mass was 840-1000 $\mu\text{m}$ , whilst the remainder was  
770 500-590 $\mu\text{m}$

- 771 • A flat distribution, ranging between 350-1190 $\mu\text{m}$

772 Increases in fluidizing gas velocity resulted in larger values of  $t_{\text{def}}$  across the board. The narrow  
773 distribution showed a noticeably longer  $t_{\text{def}}$ , sometimes up to 20% longer than the other  
774 distributions at 700°C and 800°C. The Gaussian distribution also showed slightly longer  $t_{\text{def}}$  compared  
775 to the other two distributions. At 900°C however, there was almost no difference in  $t_{\text{def}}$  between the  
776 distributions, perhaps indicating severe ash melting due to the temperature. With increasing Na  
777 concentration in the bed,  $t_{\text{def}}$  declined as would be expected, but the narrow distribution frequently  
778 produced the largest values of  $t_{\text{def}}$ , with the Gaussian distribution also showing slightly higher values  
779 of  $t_{\text{def}}$ . At the highest Na concentration, there was little difference between the four distributions.

780 The work of Lin, et al. [65] indicates the potential importance of particle size distribution. The  
781 narrow distribution displayed some sizable increases in  $t_{\text{def}}$  over the other distributions at moderate  
782 temperatures and sodium contents, a behaviour displayed to a lesser extent by the Gaussian  
783 distribution. However, different distributions of smaller particles were not examined here, and these  
784 were seen to produce longer  $t_{\text{def}}$  times in the work of others [50, 64, 61]. Therefore, further work  
785 into finding the optimal particle size distribution for typical bed materials may be worthy of  
786 investigation.

### 787 **3.9 Additives**

788 The use of additives to minimize or eliminate agglomeration has been a key area of research. The  
789 work of Steenari & Lindqvist [88] identified Kaolin and Dolomite as increasing the ash melting  
790 temperature for straw ash, with the former having a greater effect. Öhman & Nordin [89] trialled  
791 Kaolin, comprising primarily of Kaolinite ( $\text{Al}_2\text{Si}_2\text{O}_5(\text{OH})_4$ ) with some Halloysite ( $\text{Al}_2\text{Si}_2\text{O}_5(\text{OH})_4(\text{H}_2\text{O})_2$ ).  
792 An amount of 10wt% of a quartz bed sand bed was used, with bark and wheat straw as fuel. For  
793 wheat straw the agglomeration temperature,  $T_{\text{aggl}}$ , increased from 739°C to 886°C, whilst for bark it  
794 increased from 988°C to 1000°C. The Kaolin used had transformed into meta-kaolinite and absorbed  
795 potassium, thus denying potassium for agglomeration.

796 Olofsson, et al. [28] experimented with the addition of mullite, calcite, clay, and a clay-calcite  
797 mixture, each 10wt% of the bed, for different bed materials and fuels. Mullite was found to largely  
798 mitigate agglomeration, clay worsened agglomeration due to its potassium content of 1.28wt%,  
799 whilst calcite was present in agglomerates but had a somewhat positive effect on reducing  
800 agglomeration severity.

801 Davidsson, et al. [72] trialled several additives in a 12MW CFB for the combustion of a blend of wood  
802 pellets and straw pellets on a quartz sand bed. When using Kaolin as an additive,  $T_{\text{aggl}}$  of cyclone ash  
803 samples were over 100°C above those of samples where Kaolin wasn't used. A molar ratio of Kaolin  
804 to alkali of 0.85 was sufficient to maintain a  $T_{\text{aggl}} > 1100^{\circ}\text{C}$ . The effects of ammonium sulphate and  
805 sulphur were also monitored. These additives are typically used for corrosion control [25, 26]. In  
806 theory, these would convert gaseous KCl into K-sulphates, and favour the release of potassium into  
807 the gaseous form. Ammonium sulphate gave a small increase in  $T_{\text{aggl}}$  of around 50°C to 919°C, whilst  
808 sulphur had no such effect.

809 Vamvuka, et al. [90] tested Kaolinite ( $\text{Al}_2\text{Si}_2\text{O}_5(\text{OH})_4$ ), Clinoclone ( $(\text{Mg,Al,Fe})_6[(\text{Si,Al})_4\text{O}_{10}](\text{OH})_8$ ) and  
810 Ankerite ( $\text{Ca}(\text{Mg,Fe,Mn})(\text{CO}_3)_2$ ) for the combustion of olive kernel and olive tree wood on a Na-  
811 feldspar bed. The authors state that this bed material was selected itself to reduce agglomeration,  
812 thus will affect the apparent effectiveness of these additives. All three additives prevented  
813 agglomeration during the tests, retaining alkali species within the bottom ash.

814 Zabetta, et al. [17] discuss the commercial experiences of Foster Wheeler with additives. They too  
815 note that Kaolin has been found to be the most effective, but also list some alternatives used with  
816 their boilers such as bauxite, emalthisite, sillimanite, and diatomaceous earth. These materials are  
817 noted to contain one or more of silicon-, aluminium-, or iron-oxide which react with  $\text{H}_2\text{O}$  to form HCl,  
818 transferring the alkali to the mineral used and preventing the formation of KCl.

819 Lin, et al. [91] investigated the addition of calcium and magnesium for incineration of waste. Both  
820 reduced agglomeration tendency and increased  $t_{\text{def}}$ , when the molar ratio of Na, which drove

821 agglomeration in waste incineration, to Mg or Ca was below 2. Above this ratio there was no  
822 inhibiting effect.

823 To summarise, additives that are rich in Mg, Ca, or Al have a positive effect in reducing  
824 agglomeration tendency, similar to use of alternative bed materials (section 3.7); Kaolin in particular  
825 has been successful. Moreover, additives generally retain alkali species within the bottom ash, thus  
826 preventing it from contributing to fouling, slagging or corrosion. Agglomeration may still proceed for  
827 fuels that produce melt-induced agglomeration, though additives still have a positive effect. It would  
828 perhaps be of some interest to investigate the effects of varying additive dosage, relative to the  
829 molar amount needed for the fuel feed rate. This could help determine the relative technical  
830 benefits of under and overdosing additives on both bed agglomeration and other downstream issues  
831 such as slagging, fouling and corrosion.

### 832 **3.10 Effect of Additives and Alternative Bed Materials on Chlorine Emissions**

833 As discussed in sections 3.7 and 3.9, additives and alternative bed materials will alter or prevent the  
834 reactions that would otherwise occur between bed material and fuel ash. The behaviour of Chlorine  
835 may be of particular interest, as it acts as an alkali carrier gas driving fouling, slagging, and corrosion  
836 [21, 22, 23, 24, 25, 26].

837 Coda, et al. [92] trialled use of Kaolin, Bauxite, and Limestone as additives with wood and waste  
838 fuels. Kaolin doses of 25% mass of fuel ash had little effect on Cl in flue gas, whilst moving Kaolin  
839 dosage to 50% mass of fuel ash almost doubled the Cl content in flue gas, a value that remained near  
840 constant when further increasing Kaolin dosage to 79% mass of fuel ash. Bauxite had a similar effect,  
841 whereby a dosage of 40% mass of fuel ash gave a 100% increase in Cl in the flue gas. This emphasises  
842 the large effect that additive dosing can have on emissions.

843 Davidsson, et al. [72] attained some emissions data when using Kaolin as an additive or Olivine as a  
844 bed material in a 12MW<sub>th</sub> CFB combusting a blend of wood and straw. Three different Kaolin doses  
845 were trialled, leading to increases of up to 50% in HCl concentration prior to the convective pass,

846 over reference values of 55-60ppm. Sharp declines in alkali chloride concentrations were observed,  
847 as would be expected, due to the reaction of the Kaolin with alkali metals in fuel ash. At the stack  
848 HCl concentrations were doubled with high Kaolin doses compared to those without Kaolin. These  
849 increases in HCl concentration, particularly at the stack, should be noted in regards to what the  
850 allowable metal losses due to HCl corrosion are.

851 Use of Olivine instead of quartz sand as a bed material caused alkali chloride concentrations in the  
852 convective pass to almost double. HCl concentrations here were also higher by around 30%.

853 Downstream at the stack, HCl concentrations were approximately 30% lower with Olivine. The  
854 Olivine does not contain significant quantities of silica thus would not react with the alkali metal  
855 content of the fuel, hence allowing it to form alkali chlorides instead. Once again, these elevated  
856 quantities of HCl and alkali chlorides would be of concern when considering the acceptable metal  
857 losses due to corrosion.

858 These findings reinforce the idea that the boiler system must be considered as a whole, since  
859 solutions to one issue may free up additional material to drive another. It also highlights that there  
860 would be value in a comprehensive study that evaluates the effects on the whole boiler system  
861 when using additives or alternative bed materials. For example, ammonium sulphate is a common  
862 additive used to convert alkali chlorides into alkali sulphates [26], though if used in a system with an  
863 Olivine bed there would be significantly more alkali chlorides available, thus the potential for  
864 elevated HCl concentrations given sufficient amounts of ammonium sulphate.

### 865 **3.11 Coating Thickness**

866 The idea of a “Critical Coating Thickness” and the effects of liquid layering on particles in a fluidised  
867 bed is one that been discussed in the literature for many years. For example, Seville & Clift [93]  
868 noted that the continuous addition of liquid layers to fluidised particles of Geldart Group B would  
869 cause them to transition to Geldart Groups A and C, as inter-particle forces are enhanced. A “Critical  
870 Coating Thickness” would be the point at which neck formation between coated particles occurs and

871 bed agglomeration proceeds. Brus, et al. [94] performed an analysis of coating thickness over time,  
872 taking samples from industrial scale FBC plants, and stated that the critical coating thickness is less  
873 than 10 $\mu$ m. The recent work of He, et al. [45] provides a systematic investigation into coating  
874 thickness over time for a lab-scale BFB, 30MW<sub>th</sub> BFB, and 122MW<sub>th</sub> CFB. An initial rapid growth of  
875 coating layers occurred over the first several days in the full-scale units. This growth rate declined as  
876 diffusion of calcium into the melt began and higher melting point calcium compounds formed.  
877 However, there was no further discussion of a critical coating thickness. Others in the literature have  
878 also mentioned the idea of a critical coating thickness with little other discussion [39, 43, 47, 95].

### 879 **3.12 Size & Scale of Fluidized Bed**

880 For generating solutions to industrial problems at the lab- or pilot-scale, it is important to  
881 understand the applicability of results and findings to full-scale FBC plants. Many researchers have  
882 investigated agglomeration in full-scale plants, and performed direct comparisons to samples  
883 produced by lab- or pilot-scale facilities. Visser [40] looked at agglomerates from both the lab-scale  
884 and the 80MW<sub>th</sub> Cuijk FBC unit in the Netherlands. The two operational differences between these  
885 setups were that the lab-scale unit had fuel fed directly into the bed, whilst for Cuijk it was above-  
886 bed, and that there was a constant bed renewal and replenishment cycle in effect at Cuijk. This  
887 bottom ash removal and bed replenishment ability is a common agglomeration control strategy  
888 within industry [17, 49]. However, it is also one not available to most lab- and pilot-scale facilities. It  
889 is of note that variations to replenishment rate to determine the effect on agglomeration is not  
890 something that appears to have been examined in the literature, but equally would require a  
891 suitable lab- or pilot-scale facility.

892 Visser [40] concluded that lab-scale agglomeration testing provided a representative view of the  
893 initial stages of plant-scale agglomeration. The constant replenishment of sand at the Cuijk bio-  
894 energy plant was believed to be the cause of some of the differences in the chemistry of outer  
895 coating layers, due to providing fresh material for chemical reactions. Furthermore, samples at Cuijk

896 had thicker coatings due to a longer average residence time in the bed compared to the lab-scale  
897 agglomerate samples.

898 Others have also observed consistent results between lab- and full-scale facilities, be it for topics  
899 such as agglomeration mechanisms, additives, or fuels, albeit with the same shortcomings such as  
900 those seen by Visser [40], e.g. thinner coatings due to shorter residence times [38, 39, 45, 72, 78].

901 One difference suggested by Chirone, et al. [51] is that a pilot-scale fluidized bed provided a longer  
902  $t_{\text{def}}$  time compared to a lab-scale setup due to higher inertial forces in the bed. A comparison  
903 between a pilot- and lab-scale unit resulted in a  $t_{\text{def}}$  that was 3.6 times longer at pilot-scale, and had  
904 a higher ash content within the bed at time of defluidization (4wt% versus 2wt%). Chirone, et al. [51]  
905 suggested an increase in inertial forces inside the bed when moving up in scale would counteract the  
906 formation of weaker agglomerates that might otherwise cause a quicker onset of defluidization.  
907 Therefore, at plant-scale higher inertial forces may also assist in lengthening  $t_{\text{def}}$ .

### 908 **3.13 Summary of Effects of Operational Variables**

909 Table 5 summarises the effect of operational variables on agglomeration.

910 Increases in combustion temperature have a sizable effect on agglomeration, by increasing the  
911 amount of alkali-silicate melt that is generated and making it less viscous. Therefore a lower  
912 temperature is desirable, insofar as it does not have too great of an impact on the conditions of  
913 raised steam at full scale.

914 From the limited literature available on agglomeration in PFBC units, the final agglomerates formed  
915 in PFBC units seem of similar composition and type to those that would form in an AFBC.

916 Increases in the fluidizing gas velocity,  $U$ , have consistently produced longer values of  $t_{\text{def}}$  in the  
917 literature. This appears to be a result of two factors:

- 918 • Better in-bed mixing preventing the formation of localized temperature hot spots or bed  
919 dead-zones.

920       • Higher kinetic forces of bed particles that may overcome adhesive coating or melt forces.

921 There is little research on the effects of static bed height, and what is available is not conclusive.

922 Work using a constant  $U$  value across several bed heights has produced an increase and decrease in

923  $t_{\text{def}}$  with increasing bed height, indicating perhaps the involvement of other factors. Additionally,

924 increases in bed height allow for coalescence of bubbles to larger sizes. Therefore, will be increased

925 turbulence at the bed surface where the bubbles exit, which in turn may affect combustion

926 behaviour of the fuel particles and agglomeration behaviour.

927 Investigations into bed material particle size have generally shown that increasing  $d_p$ , even whilst

928 maintaining a constant  $U/U_{\text{mf}}$ , leads to a reduction in  $t_{\text{def}}$  thus worsened agglomeration. Variations of

929 bed particle size distribution for larger bed particles have shown that Gaussian and narrow

930 distributions provide longer  $t_{\text{def}}$  values.

931 Alternative bed materials that comprise primarily of aluminium-, calcium-, or magnesium-oxides, as

932 opposed to the  $\text{SiO}_2$ , have been shown to reduce or eliminate agglomeration. A change of the bed

933 material can increase the ash fusion temperature of complexes forming, and in doing so reduce melt

934 phases. The exception is where a fuel is rich in both alkali metals and  $\text{SiO}_2$ , such as straw, which will

935 form a melt-induced agglomerates with just its fuel ash contents.

936 Similar to bed materials, aluminous-, calcium-, or magnesium-based additives have been shown to

937 be effective. Kaolin in particular has shown itself to be successful in reducing or eliminating

938 agglomeration several times within the literature. Both additives and bed materials have been noted

939 to have a large effect on emissions, particularly Chlorine, which can drive corrosion mechanisms.

940 Fuel has a large influence on agglomeration. Fuels with increasing amounts of alkali metals such as

941 potassium exhibit more severe agglomeration, typically melt-induced agglomeration, and lower

942 values of  $t_{\text{def}}$ . Co-firing of fuels is something primarily explored in the context of coal-biomass or

943 wood-straw mixtures within the literature. A common trend for biomass blends is that relationships



944 between blend ratios and agglomeration factors such as melt temperatures are non-linear. Fuel  
945 particle size has receive some attention, with smaller particle sizes giving better combustion  
946 efficiencies and longer values of  $t_{def}$ . This is perhaps due to combustion taking place at higher regions  
947 of, or just above, the bed.

948 Coating thickness and critical values for triggering agglomeration are of general interest. Growth  
949 rates are typically quicker at the start and then trail off due to diffusion of Ca into the K-silicate melt,  
950 forming a Ca-silicate melt of higher melting point. Neck formation between coated particles can  
951 occur at coating thicknesses less than 10 $\mu$ m.

952 The applicability of lab- and pilot-scale results to full-scale facilities has been explored within the  
953 literature. Mechanisms and behaviours generally map well to full-scale facilities for the initial  
954 triggering of agglomeration. Over time, there is a divergence due to replenishment of bed material  
955 in full-scale facilities, plus longer residence times, leading to thicker coatings on bed particles.

#### 956 **Recommendations for further work**

- 957 • Large bed heights allow for further coalescence of bubbles, leading to greater turbulence at  
958 the surface of the bed, as well as enhanced combustion efficiencies [6, 70]. Gatternig, et al.  
959 [46] observed that less dense fuel particles “floated” on the surface of the bed, reaching  
960 higher temperatures, and exacerbating agglomeration issues, thus there may be interest in  
961 the effects of bed height on agglomeration severity.
- 962 • Smaller particle sizes have generally been shown to lengthen  $t_{def}$ , and certain particle size  
963 distributions (Gaussian, narrow) have been shown to lengthen  $t_{def}$  albeit with larger average  
964 particle sizes. Therefore, it would be of interest to trial different size distributions of a  
965 smaller mean particle size, to see if similar findings are apparent, and if there may be an  
966 optimum size range and size distribution.
- 967 • Several alternative bed materials and additives have been shown to mitigate or prevent  
968 agglomeration in numerous studies, with some such as Olivine (bed material) and Kaolin

969 (additive) being used in industrial installations. Investigatory work into new bed material and  
970 additives would always be welcomed, but also more comprehensive studies into the effects  
971 of alternative bed materials and additives on other phenomena driven by the alkali metal  
972 content of biomass fuels, such as slagging, fouling and corrosion. Some alternatives bed  
973 materials and additives have been observed to have large effects on alkali chlorides and HCl,  
974 which drive corrosion within the boiler.

- 975 • There may be some interest in blending of bed materials, perhaps to balance performance  
976 with cost, and investigating impact on the whole boiler system.
- 977 • There may also be some interest in trialling different dosage rates of additives from under to  
978 overdosing relative to the molar amount needed for the given fuel, and investigating the  
979 cost and performance impact on the whole boiler system.
- 980 • Co-firing of biomass-biomass blends and the effect on agglomeration is something that has  
981 received little work outside of wood-straw mixtures. From current works, biomass ashes  
982 have exhibited complex, non-linear relationships for properties such as initial ash  
983 deformation temperature. Work in this area could aid in assessing the viability of such  
984 blends for larger scale FBC units.
- 985 • Studies into optimising bed replenishment rates may be of interest, as no work on this area  
986 seems apparent in literature. However, this may be challenging from the perspective of  
987 finding a suitable and available test facility or full-scale unit on which a study could be  
988 conducted.

#### 989 **4. Agglomeration Monitoring and Prediction**

990 This section provides a brief overview and introduction to agglomeration monitoring and prediction  
991 methods. A more extensive and comprehensive review of this broad field is available with the work  
992 of Bartels, et al. [20].

993 These methods can fall under one of two general categories:

- 994 1. “Pre-combustion” prediction – methods applied before use of the fuel in a full scale boiler,  
995 e.g. empirical correlations, lab-scale testing.
- 996 2. “In-situ” monitoring and prediction – methods that may be applied within a full-scale boiler  
997 to monitor agglomeration during standard operation.

#### 998 **4.1 Pre-combustion Prediction of Agglomeration**

##### 999 **Experimental Methods**

1000 Several research groups have attempted to utilise standardised fuel ash testing methods to predict  
1001 agglomeration temperatures. For example, the ASTM ash fusion test was performed on several  
1002 biomass fuels by Skrifvars, et al. [35], though it was found to be unreliable, as it predicted  
1003 problematic temperatures for ashes well in excess of the temperatures where they are known to be  
1004 problematic in a fluidised bed. A sintering test was more accurate, but typically under-predicted  
1005 temperatures at which ashes would be problematic by 20-50°C. At present, the most reliable  
1006 experimental method for determining agglomeration difficulties associated with a new fuel may be  
1007 is through lab- and pilot-scale trials.

##### 1008 **Theoretical Methods**

1009 Use of the thermochemical software package FactSage has gained popularity in recent years as a  
1010 tool to predict slagging and melting phase temperatures for fuels, as the available databases have  
1011 improved in breadth and accuracy [77, 96]. The work of Fryda, et al. [97], whilst using older  
1012 databases, is an example of FactSage being used to predict melt formation fractions across typical  
1013 FBC operating temperatures. A point of note here is that there was a prediction of 25-45% less melt  
1014 formed when the silica in bed material did not react with fuel ash elements. Fryda, et al. [97] note  
1015 that this was more realistic for their fuels, as from their SEM/EDS observations there was not  
1016 significant interactions between bed material and fuel ash. As Fryda, et al. [97] state, this highlights  
1017 some general shortfalls of FactSage modelling, in that it considers all silica equally reactive, and does  
1018 not have any allowance for bed material porosity or size, leading to the suggestion that only a

1019 fraction of silica in the bed material should be considered within the FactSage model. More  
1020 generally, this reinforces the necessity of having a good understanding of the real phenomena in  
1021 order to create an accurate model.

1022 The more recent work of Rizvi, et al. [96] examined slag formation quantities and compositions using  
1023 FactSage, for pine wood, peanut shells, sunflower stalks, and miscanthus. All fuels were predicted to  
1024 have some liquid slag formation at 700°C, however each fuel had different responses to increases in  
1025 temperature. For example, both peanut ash and pine wood maintained relatively constant liquid slag  
1026 fractions through typical FBC operating temperatures of 800-900°C. Miscanthus on the other hand  
1027 exhibited a 10-15% increase. It should be noted though that this work does not consider the fuel in  
1028 the presence of the bed material, only the fuel alone, and doing so would likely encounter many of  
1029 the similar challenges highlighted by Fryda, et al. [97].

### 1030 **Indices**

1031 Numerous empirical agglomeration indices have been proposed over the years by researchers.  
1032 Gatternig [98, p. 56] provided a summary of common agglomeration indices and relationships for  
1033 both coal and biomass. The coal indices tested on biomass, as well as those proposed for biomass,  
1034 have been reproduced and further added to in Table 6.

1035 These indices have varying levels of usefulness. The Alkali Index has been examined by several  
1036 researchers, and provides a generally good indication of the likelihood of fouling, slagging, or  
1037 agglomeration, but its effectiveness decreases when other factors are at play such as alternate bed  
1038 materials and/or additives [90, 99, 100]. The alkaline earth oxides to alkaline oxides ratio examined  
1039 by Fernández Llorente & Carrasco García [101] was found to provide a poor indication of the  
1040 likelihood and severity of ash sintering. Therefore, it is important to consider the combustion  
1041 conditions under which the fuel will be used when applying an agglomeration indicator, as these  
1042 indicators have been empirically derived and may not be directly applicable.

## 1043 **4.2 In-situ Monitoring and Prediction of Agglomeration**

### 1044 **Pressure Drop**

1045 Pressure drop across the bed is a common reading taken on FBC units, with it giving operators real-  
1046 time information on bed hydrodynamics and fluidisation behaviour, as well as density and height  
1047 [20, 102]. However, bed pressure drop only gives a view of the bed as a singular entity, with the  
1048 potential for smaller scale disturbances going unnoticed. Moreover, probe blockages may cause  
1049 measurement inaccuracies.

1050 Nonetheless, researchers have tried to apply algorithms or statistical analyses to detect when  
1051 agglomeration or a defluidization event may be beginning [20]. For example, Chirone, et al. [51]  
1052 looked at pressure drop variance, and noted a 60% decline in pressure drop variance had occurred at  
1053 the point of defluidization, with similar observations noted in a subsequent work [47].

### 1054 **Temperature**

1055 Temperatures are routinely measured on FBC units, often in several locations within the bed.

1056 Moreover, as has been seen in sections 2 and 3, operating temperature has a large impact on melt  
1057 formation and the likelihood of other phenomena such as sintering to worsen agglomeration. An  
1058 issue with this approach is successfully determining a localised spike due to agglomerate formation  
1059 versus one that is the result of normal variances during combustion. Furthermore, full coverage of  
1060 the bed with thermocouples is not possible, as there is always the possibility of missing small,  
1061 localised variations of importance [103]. Some authors have evaluated the potential for  
1062 temperature-based detection of hot-spots and agglomerate formation. For example, Khan and  
1063 Turton [104] used thermocouple data and empirically derived heat transfer coefficients to analyse  
1064 temperature variations within the bed, whilst Basu [105] applied a statistical analysis to highlight  
1065 abnormal temperature variances within the bed. Lau & Whalley [106] trialled radially mounted  
1066 differential thermocouples to detect hotspots when combusting caking coals with some success,  
1067 though this was in the context of a lab-scale wall-heated FBC unit.

1068 **Other Methods**

1069 Several novel methods for agglomeration detection have been trialled over the years. One example  
1070 is the use of fibre optic sensors to measure bed hydrodynamic data, though this has been restricted  
1071 to lab-scale units [107, 108, 109, 110].

1072 The work of Wang, et al. [102] trialled analysis of acoustic emissions, resultant from inter-particle  
1073 and particle-wall collisions. It was shown that there was potential with this methodology, given  
1074 sufficient data and a competent interpretive model. Others have since expanded upon acoustic  
1075 emissions monitoring methods and the associated mathematical analyses to the point where specific  
1076 agglomerates can be identified, though further development is needed to improve reliability and  
1077 scale them up for full-scale FBC units [111, 112, 113].

1078 **Combined Approaches**

1079 Some researchers have attempted to combine monitoring approaches to see if the result is more  
1080 accurate for detecting agglomeration and defluidization. An example is the recent work of  
1081 Shabanian, et al. [114] where bed pressure drop and temperatures were considered together.  
1082 Shabanian, et al. [114] took reference values for the temperature difference between an upper and  
1083 lower point in the bed, as well as pressure difference between an upper lower point in the bed, and  
1084 then compared a moving average of real temperature and pressure differences against these  
1085 reference values. From this, they were able to derive settings that could be used as “high” and “high-  
1086 high” alarm points, warning of defluidization. In some cases, their method gave indication of  
1087 defluidization upwards of 3 hours in advance. This highlights that there may be some considerable  
1088 promise in combined approaches to agglomeration monitoring, though still leaves open the question  
1089 of mitigation and prevention.

### 1090 **4.3 Summary of Agglomeration Monitoring and Prediction Methods**

1091 Monitoring and prediction of agglomeration is an area where much work is still needed to create  
1092 accurate, robust, reliable, and cost effective solutions. Empirical indices appear to require further  
1093 refining across a variety of fuels, conditions, and scales to be of more use, and to do so would likely  
1094 take large collaborative efforts to collect, compile and analyse the necessary data. Lab-scale  
1095 combustion trials of fuels are perhaps the best way to assess its issues prior to use at the full scale,  
1096 but numerous tests may be needed to represent the range of fuel qualities that a facility may use,  
1097 and this would increase the cost and time requirements of such studies. For in-situ monitoring,  
1098 pressure drop and temperature based methods are preferred as such measurements are readily  
1099 available on industrial units, however there are still challenges in drawing accurate and reliable  
1100 correlations for the prediction of agglomeration and defluidization. Combined approaches such as  
1101 that of Shabanian, et al. [114] have been shown to have some promise, and developments along  
1102 similar lines may be worthwhile.

## 1103 **5. Conclusion**

1104 Sections 2.4, 3.13, 4.3 provide more detailed summaries and suggestions for further work for each  
1105 area examined within this review. The main findings from this review are as follows:

- 1106 • There is a wealth of mechanism research when combusting biomass on SiO<sub>2</sub>-based bed  
1107 materials, with agglomeration mechanisms being of the coating- or melt-induced variety. For  
1108 coating agglomeration in the case of SiO<sub>2</sub>-based bed materials, there is the common  
1109 occurrence of two or three distinct particle layers, with a higher presence of potassium  
1110 within the fuel causing the “inner-inner” third layer. Sufficient growth of the calcium-based  
1111 “inner” layer appears to prevent further formation of K-silicate melts with the bed particle,  
1112 and as the layer changes in composition further diffusion of calcium is limited. Melt-induced  
1113 agglomeration is the result of sufficient silica and alkali metal content in the fuel forming an  
1114 ash melt. In some cases, the ash skeleton shape of the particle appears to allow the

1115 formation of agglomerates similar in shape to that of the fuel particle. Further work is  
1116 particularly needed into mechanisms when using alternate bed materials and additives, with  
1117 consideration given to the effects on the whole boiler system.

- 1118 • Of the operating variables, fuel, bed material, additives, fluidizing gas velocity and  
1119 temperature have the greatest effect on agglomeration severity. An overall ranking of  
1120 parameters examined is given in Table 5. Most other variables have received some degree of  
1121 attention, though may benefit from some deeper studies. Co-firing of dual-biomass blends  
1122 stands out as one area that may benefit from additional work, given that work so far has  
1123 focused on coal-biomass or wood-straw mixes, together with further work into alternative  
1124 bed materials and additives.
- 1125 • A brief overview of agglomeration monitoring and prediction methods has been given,  
1126 showing that whilst there are numerous potential methods available, accuracy is a key  
1127 concern. Monitoring and prediction is in general an area that would benefit from further  
1128 work into accurate, reliable, robust and cost-effective monitoring and prediction methods  
1129 for full-scale installations. Recent work on combined approaches using temperature and  
1130 pressure drop measurements has shown some promise in this field, where defluidization  
1131 was successfully predicted up to 3 hours in advance.

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1135 **6. References**

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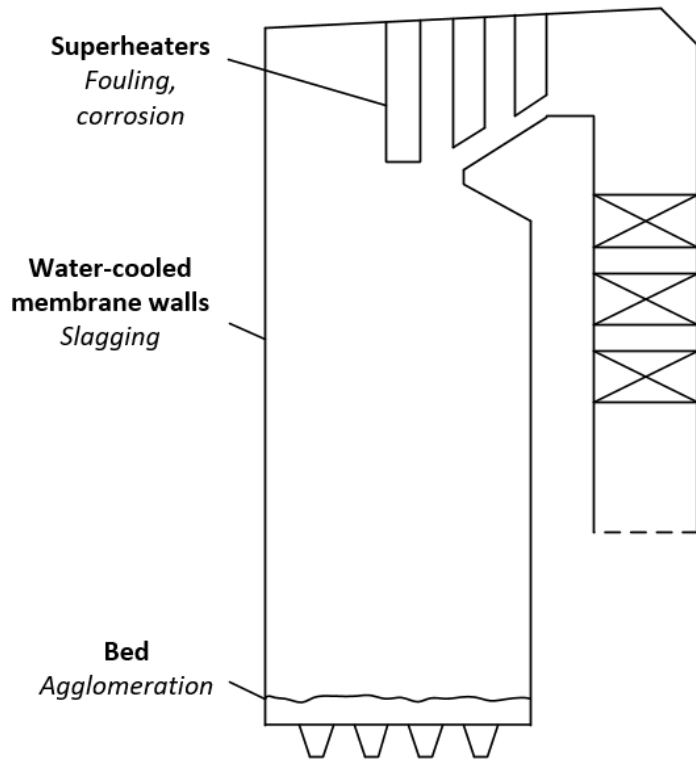
1138

1139 **7. Figures**



1140

1141 **Figure 1: Image of several agglomerate samples collected from 50kW<sub>th</sub> Fluidized Bed combusting**  
1142 **wheat straw pellets.**



1143

1144 **Figure 2: Simplified diagram of a BFB boiler highlighting areas where biomass ash contents - alkali**  
 1145 **and alkali earth metal, silica and chlorine - cause issues. Adapted from the diagram of Hupa, et al.**  
 1146 **[73].**



Three-layer coating: K-rich system

Two-layer coating: K-lean system



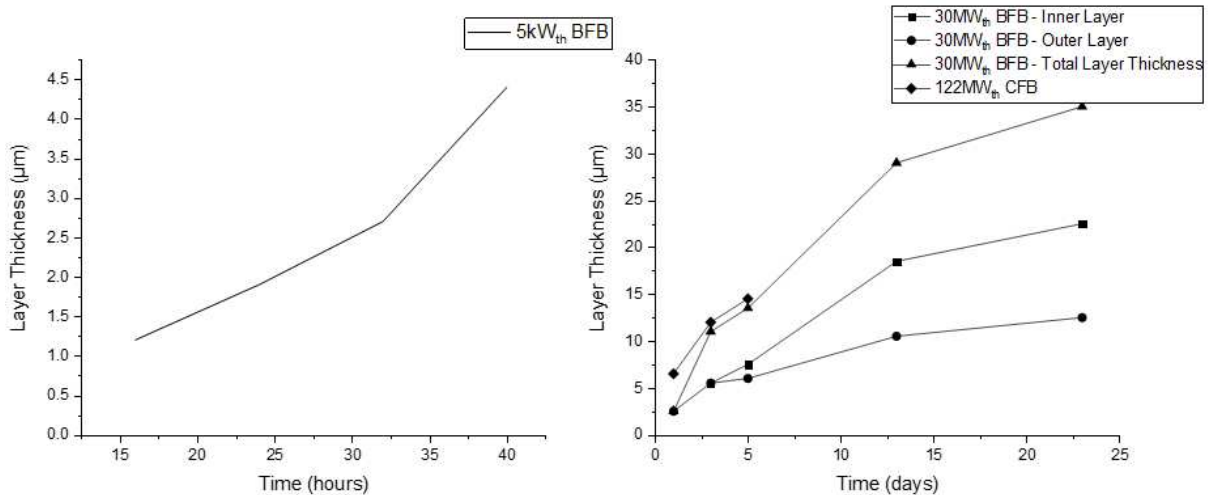
	Outer Layer	Inner Layer	Inner-Inner Layer
Element	wt%	wt%	wt%
Si	3	14-18	34
P	6	-	-
S	4	-	-
K	7	-	10
Ca	29	44	4-5

	Outer Layer	Inner Layer
Element	wt%	wt%
Si	3	14
P	5	-
S	4	-
K	7	-
Ca	28	41

1148

1149 **Figure 3: Diagram showing the compositional differences between two- and three-layer coating**

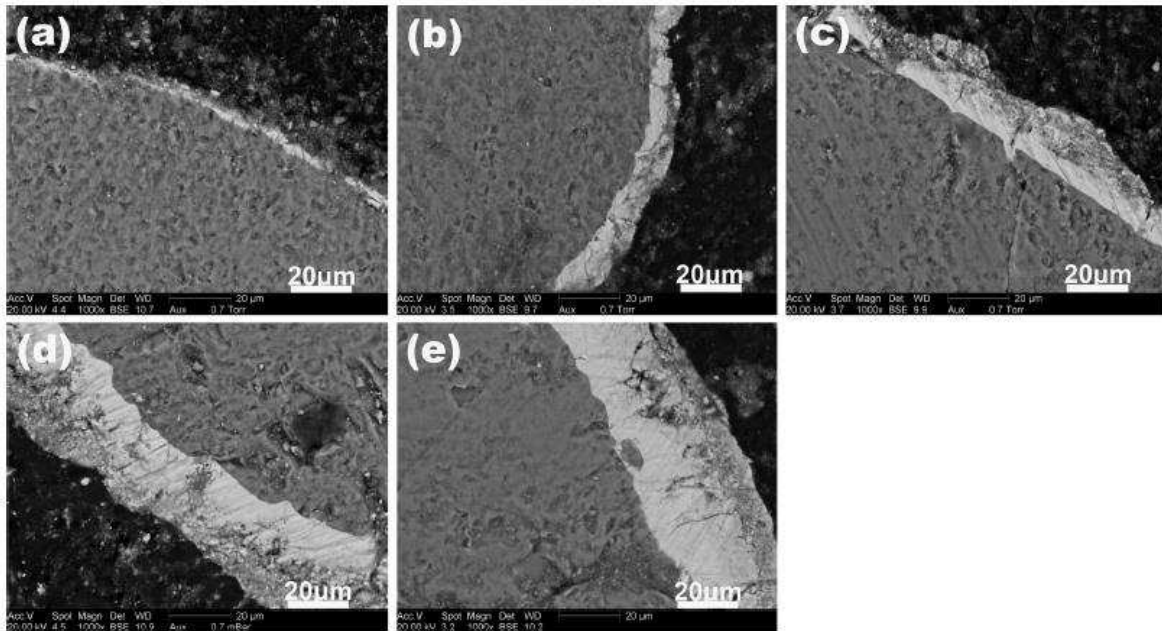
1150 **systems, as described by Visser [40]. Based on the diagram of Visser [40].**



1151

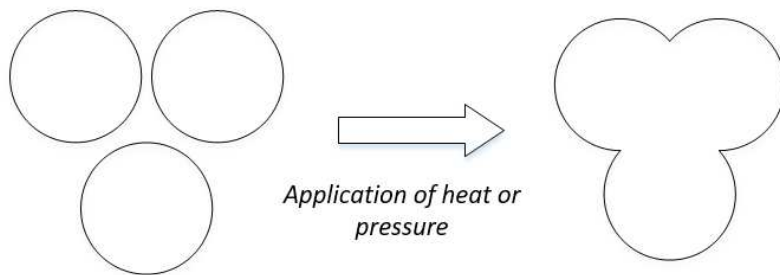
1152 **Figure 4: Coating layer growth over time for lab-scale BFB and full-scale BFB and CFB units. Based**

1153 **on the data of He, et al. [45].**



1154

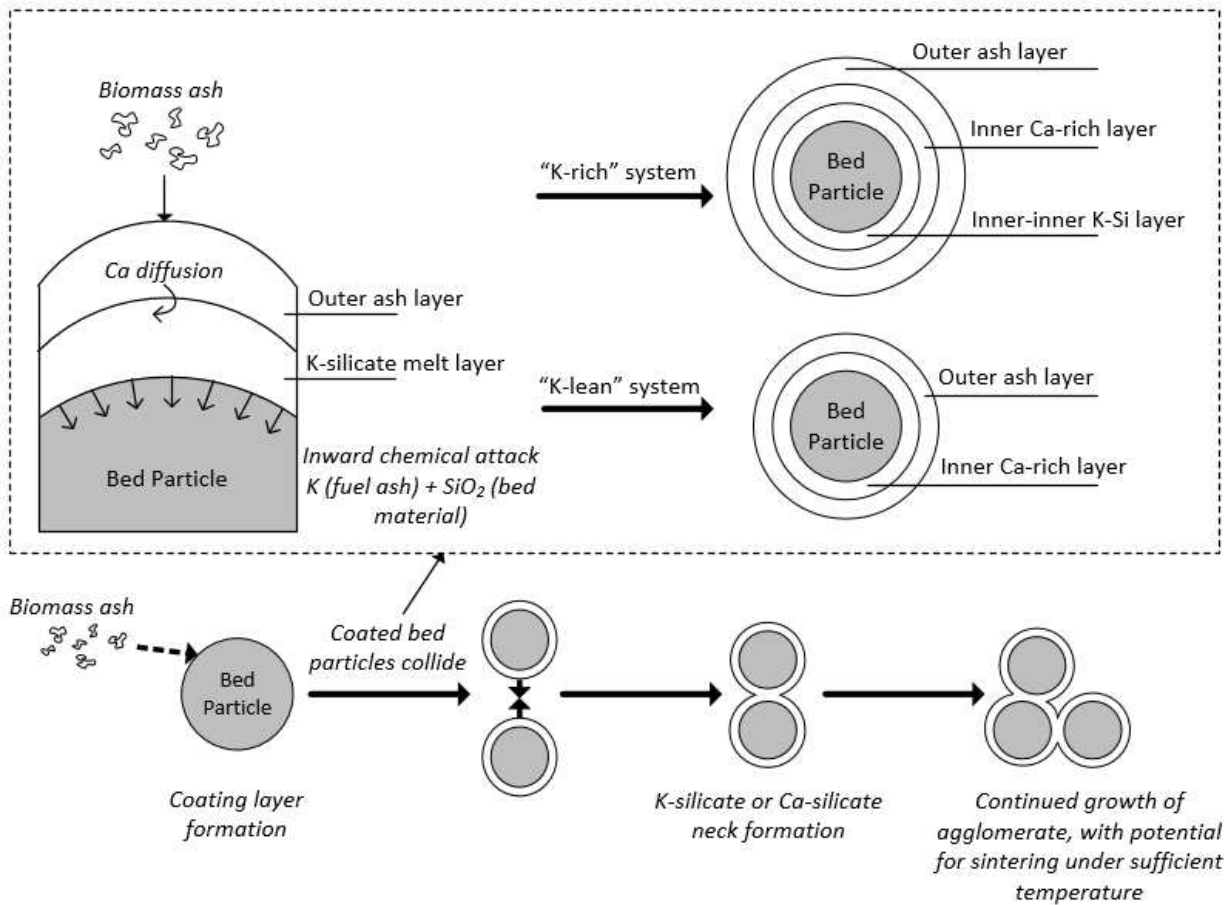
1155 **Figure 5: Example SEM images of coating layers (lighter grey) resulting from the combustion of**  
 1156 **wood on a sand bed in a 30MW<sub>th</sub> Bubbling FBC unit. Images ‘a’ through ‘e’ are of particles 1, 3, 5,**  
 1157 **13, and 23 days after initial bed start-up. Differences in layer homogeneity moving outward can be**  
 1158 **clearly seen in images ‘c’ through ‘e’. Images reproduced with permission from the work of He, et**  
 1159 **al. [45].**



1160

1161 **Figure 6: Generalised diagram showing the progression of sintering. Within an atmospheric**  
 1162 **fluidised bed, particles may be fused together under high temperatures. Diagram adapted from**  
 1163 **Hosford [115, p. 144].**

## Coating-induced Agglomeration Mechanism - SiO<sub>2</sub>-based Bed Material



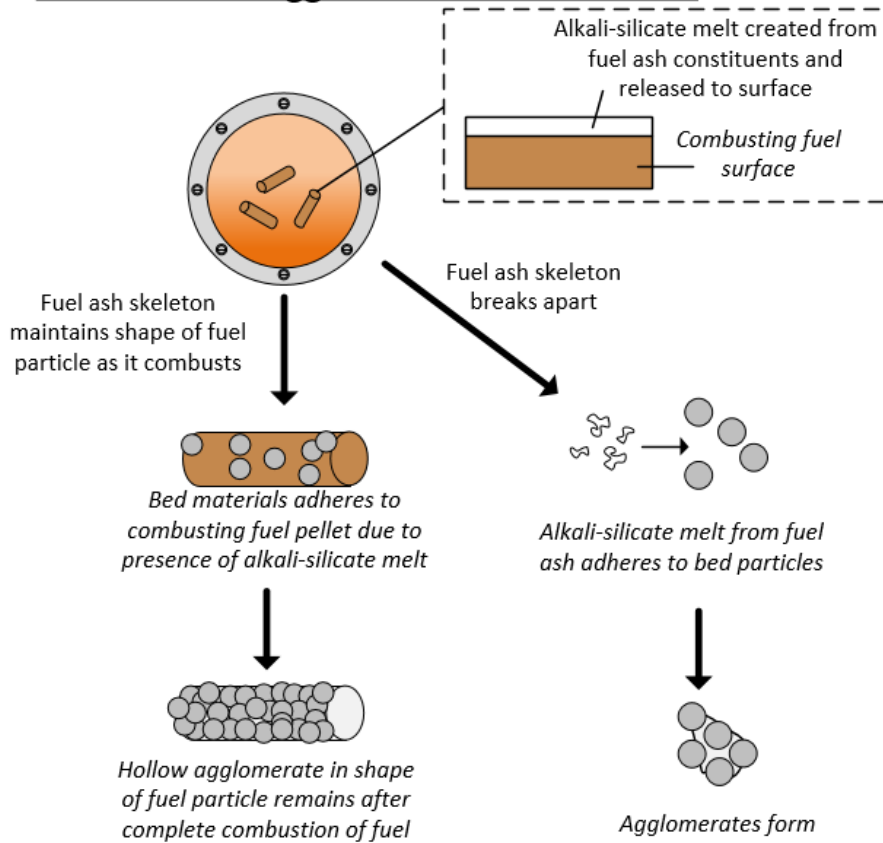
1164

1165 **Figure 7: Coating-induced agglomeration mechanism in a system with an SiO<sub>2</sub>-based bed material,**

1166 **whereby agglomeration proceeds due to potassium presence within the fuel ash. Described within**

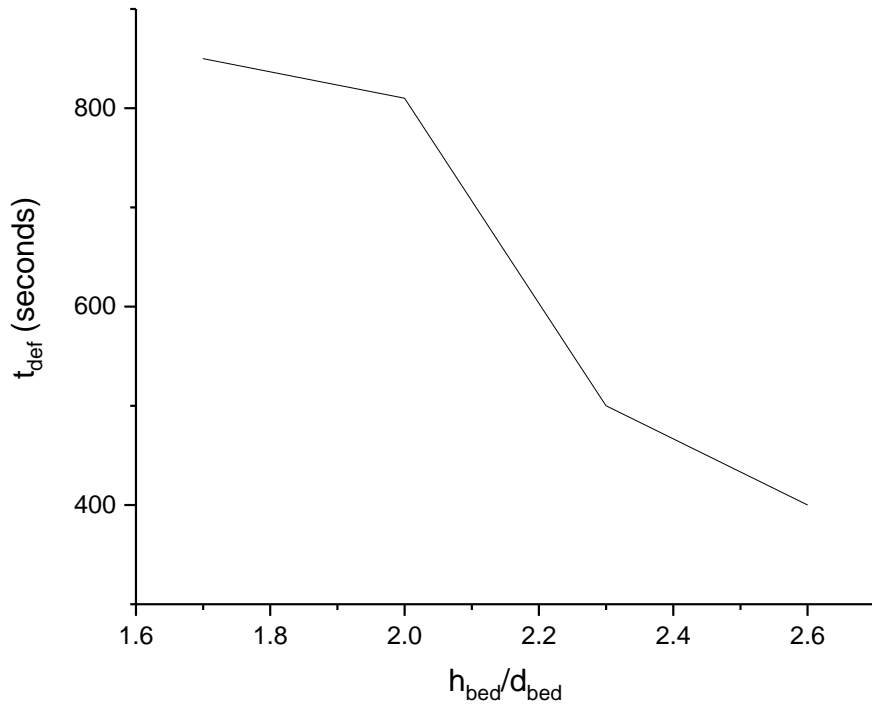
1167 **the text of section 2.4.**

## Melt-induced Agglomeration Mechanism



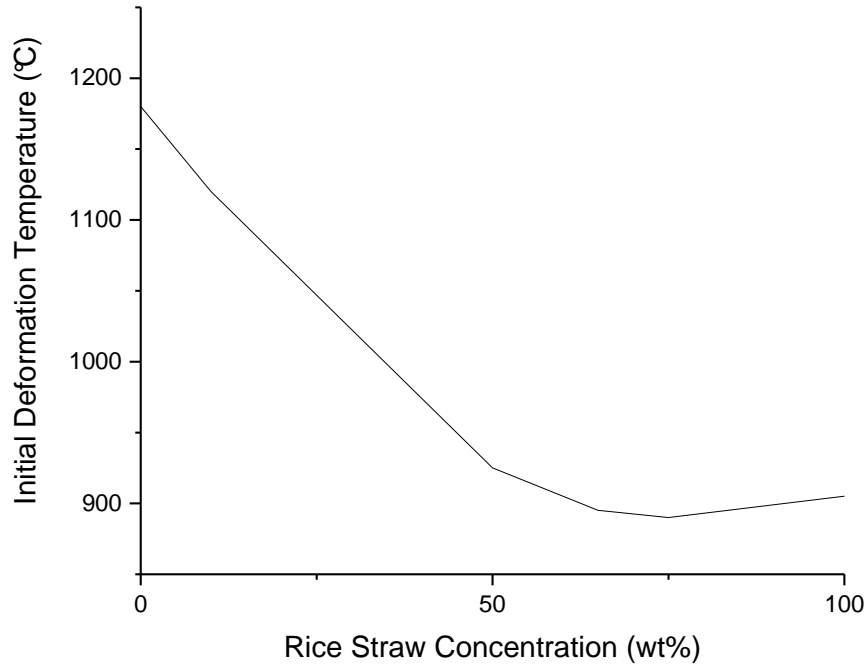
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1169 **Figure 8: Melt-induced agglomeration mechanism, as described within the text of section 2.4.**



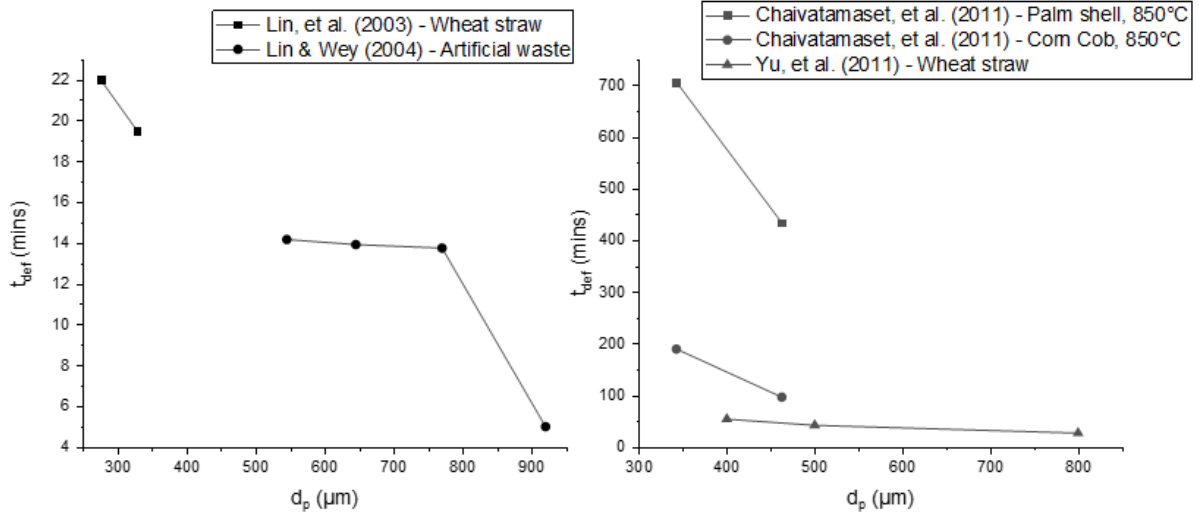
1170

1171 **Figure 9: Graph showing the effect of changing the bed height-to-diameter ratio,  $h_{bed}/d_{bed}$ , on the**  
 1172 **defluidization time,  $t_{def}$ . Based on the work of Lin & Wey [53].**



1173

1174 **Figure 10: Variations in initial deformation temperature (IDT) for Rice Straw/Wood fuel blend.**  
 1175 **Reproduced from the work of Salour, et al. [74].**



1176

1177 **Figure 11: Graphs showing the effect of changing average bed particle size on defluidization time,**  
 1178  **$t_{def}$ . Based on the works of Lin, et al. [50], Lin & Wey [53], Chaivatamaset, et al. [64], and Yu, et al.**  
 1179 **[61].**

1180

1181 **8. Tables**

1182 **Table 1: Table summarising fuel and relative presence of coating on the particles examined with**  
 1183 **SEM/EDS [42]. Note that this percentage presence of coating was found to be identical for both**  
 1184 **combustion and gasification environments.**

<b>Fuel</b>	<b>Amount of particles examined where coating was present</b>
Bark	“Majority”
Reed canary grass	10%
Lucerne	10%
Olive flesh	“Majority”
Cane trash	10-30%
Bagasse	<10%

1185

1186 **Table 2: Coating-induced agglomeration layer growth mechanisms proposed by He, et al. [48].**

1187 **Table reproduced from He, et al. [48].**

<b>Phase</b>	<b>Controlled Process</b>	<b>Main Crystalline Phases</b>	<b>Layer Growth Rate</b>
1 (<1 day)	Reaction	Only K-rich silicate melt	Fast in the presence of enough available calcium
2 (from 1 day to ~2 weeks)	Diffusion	CaSiO <sub>3</sub> , Ca <sub>2</sub> SiO <sub>4</sub>	Medium
3 (from ~>2 weeks)	Diffusion	Ca <sub>2</sub> SiO <sub>4</sub> , Ca <sub>3</sub> SiO <sub>5</sub>	Quite low

1188

1189

1190 **Table 3: Table summarising the effect of varying bed material on agglomeration. Results taken from the literature as noted.**

Reference	Bed Material	Composition	Fuel(s)	Effect on Agglomeration
Olofsson, et al. [28]	Bone ash	44.2wt% CaO, 28.8wt% P <sub>2</sub> O <sub>3</sub>	Straw	Reduced agglomeration tendency compared to quartz sand
Olofsson, et al. [28]	Mullite	75.2wt% Al <sub>2</sub> O <sub>3</sub> , 24.5wt% SiO <sub>2</sub>	Straw	Reduced agglomeration tendency compared to quartz sand and better than Bone ash or Magnesite. Noted as being due to high melting point of alumina silicates.
Olofsson, et al. [28]	Magnesite	84.4wt% MgO, 7.55wt% CaO, 3.93wt% SiO <sub>2</sub>	Straw	Reduced agglomeration tendency compared to quartz sand
Nuutinen, et al. [39]	GR Granule (commercial/proprietary)	Proprietary (Mg-based, SiO <sub>2</sub> -free)	Various: woody, wastes, industrial residues	Prevented agglomeration in cases where quartz sand otherwise did
Fernández Llorente, et al. [116]	Limestone	CaCO <sub>3</sub>	Brassica, Thistle, Almond shells	Prevented agglomeration in cases where quartz sand otherwise did
De Geyter, et al. [117]	Potassium feldspar	66.2wt% SiO <sub>2</sub> , 19.3wt% Al <sub>2</sub> O <sub>3</sub> , 8.2wt% K <sub>2</sub> O	Bark, olive residue, wheat straw	Increased agglomeration risk with bark and olive residues, no effect on wheat straw (agglomeration still occurred).  Note that K-feldspar may be a constituent of natural sand.
De Geyter, et al. [117]	Plagioclase	54wt% SiO <sub>2</sub> , 27wt% Al <sub>2</sub> O <sub>3</sub> , 11wt% CaO	Bark, olive residue, wheat straw	Increased T <sub>aggl</sub> for olive residue, no effect on bark, no effect on wheat straw (agglomeration still occurred).  Note that Plagioclase may be a constituent of natural sand.
De Geyter, et al. [117]	Olivine	49.5wt% MgO 45.0wt% SiO <sub>2</sub>	Bark, olive residue, wheat straw	Increased t <sub>def</sub> for olive residue, no effect with bark, no effect on wheat straw (agglomeration still occurred)



Reference	Bed Material	Composition	Fuel(s)	Effect on Agglomeration
Liu, et al. [118]	Aluminous bed material	75.93wt% Al <sub>2</sub> O <sub>3</sub> , 19.92wt% SiO <sub>2</sub>	Cotton stalk	Agglomeration issues after 38h of operation, as opposed to 8h for silica sand, when using 200kW <sub>th</sub> CFB.
Davidsson, et al. [75]	Olivine	(Mg, Fe) <sub>2</sub> SiO <sub>4</sub>	80% woody + 20% straw blend (energy basis)	Higher T <sub>aggl</sub> compared to sand. No reaction between melt-layers and Olivine. Agglomerates formed over time due to presence of straw & melt-induced agglomeration.
Davidsson, et al. [75]	Blast furnace slag	Ca/Mg/Al silicates	80% woody + 20% straw blend (energy basis)	Higher T <sub>aggl</sub> compared to sand and Olivine. No reaction between melt-layers and blast furnace slag. Agglomerates formed over time due to presence of straw leading to melt-induced agglomeration.
Yu, et al. [61]	Aluminous bed material	Al <sub>2</sub> O <sub>3</sub>	Rice straw	Increase in t <sub>def</sub> though melt-induced agglomeration still occurred due to fuel.
Corcoran, et al. [85]	Quartz sand + Ilmenite (up to 40wt%)	FeTiO <sub>3</sub>	Wood chips	Reduction in agglomeration tendency – potassium diffused into the centre of the bed particle thus was less available to form alkali-silicate melts.
Grimm, et al. [44]	Olivine	49.0wt% MgO, 41.0wt% SiO <sub>2</sub> , 8.4wt% Fe <sub>2</sub> O <sub>3</sub>	Willow, wood residues, wheat straw, wheat distiller's dried grain with solubles (DDGS)	Fewer agglomerates with willow & wood residues compared to quartz sand bed, plus different coating layer composition (Mg/Si/Ca vs. Si/K/Ca).  No reduction in agglomeration tendency with wheat straw or DDGS.

1192 **Table 4: Summary of the effects Bed Particle Diameter variations from the work of Scala & Chirone**  
 1193 **[60], using a quartz sand bed.**

<b>Fuel</b>	<b>Temperature (°C)</b>	<b>Fluidizing Gas Velocity (m/s)</b>	<b>Excess Air (%)</b>	<b>d<sub>p</sub> (μm)</b>	<b>t<sub>def</sub> (mins)</b>
Virgin Olive Husk	850	0.61	77	212-400	197
Virgin Olive Husk	850	0.61	76	600-850	348
Pine Seed Shells	850	0.55	35	212-400	320
Pine Seed Shells	850	0.50	75	212-400	388
Pine Seed Shells	850	0.54	58	600-850	702

1194

1195

1196 **Table 5: Table summarising the effect of various operational variables on reducing agglomeration severity.**

Effect on REDUCING Agglomeration Severity			
Conflicting or Unknown	No Effect	Minor	Major
Increase/Decrease Bed Height	Increase/Decrease Pressure	Decrease mean $d_p$	Decrease temperature
		Different Particle Size Distribution (Gaussian, Narrow)	Increase $U/U_{mf}$ ratio
		Decrease fuel particle size	Decrease fuel feed rate
			Decrease Alkali Metal/Alkali Metal + Si content of fuel
			Use of Al/Mg/Ca-based additives
			Decrease bed material $SiO_2$ content (use of Al/Mg/Ca-based bed material)

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1198

1199 **Table 6: Summary of common agglomeration indices and relationships. Adapted and expanded upon from the work of Gatternig [98, p. 56]**

Index	Definition	Limit(s) for safe operation	Reference
Alkali Index	$AI = (K_2O + Na_2O)kg/GJ$	0.17 < AI < 0.34 Agglomeration possible AI > 0.34 Agglomeration near certain	[90, 99, 100]
Bed Agglomeration Index	$BAI = \frac{Fe_2O_3}{K_2O + Na_2O}$	Agglomeration when BAI < 0.15	[90, 119]
Base-to-acid ratio	$R_{b/a} = \frac{\%(Fe_2O_3 + CaO + MgO + K_2O + Na_2O)}{\%(SiO_2 + TiO_2 + Al_2O_3)}$	Lower $R_{b/a}$ implies lower ash melt temperatures, see [74]	[10, 74]
Agglomeration Index I1	$I1 = \frac{Na + K}{2S + Cl}$	High agglomeration potential when I1 > 1	[40]
Agglomeration Index I2	$I2 = \frac{Na + K + Si}{Ca + P + Mg}$	I2 > 1 <i>Noted as being arbitrary/requiring further confirmation</i>	[40]
Alkaline earth oxides to alkaline oxides	$I = \frac{(CaO + MgO)}{(K_2O + Na_2O)}$	No effective correlation found	[101]

1200