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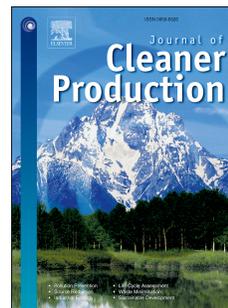
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# Accepted Manuscript

Valorization of spruce needle waste via supercritical extraction of waxes and facile isolation of nonacosan-10-ol

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Nonacosan-10-ol

Waste  
needles

Hydrophobic  
coatings

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2

3 **Valorization of spruce needle waste via supercritical**  
4 **extraction of waxes and facile isolation of nonacosan-10-ol**

5

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8

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14

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16 Biorefinery

17 **Abstract**

18

19 Supercritical carbon dioxide was utilized as a sustainable alternative to solvent  
20 extraction of waxes from the waste needles of two spruce species, namely Norwegian  
21 and Sitka spruce. These extracts were rich in nonacosan-10-ol, an organic compound  
22 with hydrophobic properties that lends its use in the preparation of superhydrophobic  
23 coatings. The highest crude yields were 1.7% w/w of needles obtained at 400 bar and

24 60 °C , while nonacosan-10-ol was selectively extracted at 200 bar and 60 °C (8070  
25  $\pm 91.1$   $\mu\text{g/g}$  of needles). Purification of nonacosan-10-ol from the wax extracts was  
26 conducted using a simple rapid green recrystallization technique. This yielded a  
27 recovery of 44.6%  $\pm 2\%$  and 48.4%  $\pm 2\%$  of the total nonacosan-10-ol from the original  
28 crude Sitka (3600  $\mu\text{g/g}$  of needles) and Norwegian wax (1920  $\mu\text{g/g}$  of needles)  
29 respectively. Application of nonacosan-10-ol to a filter paper led to the formation of  
30 highly hydrophobic surfaces, with preliminary contact angles of up to 149°. This  
31 sustainable production method may develop opportunities to valorize forestry waste  
32 within a holistic biorefinery.

33

## 34 1. Introduction

35

36 Wood is a valuable resource that has been utilized for centuries in a wide variety of  
37 applications including construction, paper and as a source of chemicals (Arshadi et al.,  
38 2012 & 2013; Attard et al., 2016a). Wood based biorefineries currently exist in parts of  
39 Scandinavia and North America. However, a greater utilization of waste residues is  
40 necessary to make a biorefinery truly holistic (Arshadi et al., 2016; Attard et al., 2015a,  
41 2016a,b; Budarin et al., 2011). Therefore, research must be carried out to systematically  
42 tailor and select 'green sustainable' processes to isolate, extract and analyze different  
43 chemicals from low-value tree waste fractions with considerable content of extractives  
44 (Backlund et al., 2014; Miranda et al., 2012). Needles from forestry wastes are one of  
45 the examples that currently constitute a waste resource as they are not utilized by the  
46 forestry industry.

47

48 Although exploitation of forest residues would lead to a reduction in waste and  
49 utilization of renewable resources, there has been very little attention given to valorize  
50 this potential feedstock. This has led to significant accumulation of overproduced  
51 biomass from neglected forests that have little or no use, which is not only a waste but  
52 could also pose as a major fire risk.

53

54 The extractives found in the needles have a host of bio-derived chemicals that could  
55 potentially be utilized in a number of industrial applications including hydrophobic  
56 coatings (Attard et al., 2015a; Backlund et al., 2014). There has been considerable  
57 interest in studying the superhydrophobicity of plant surfaces due to their potential wide  
58 applications in self-cleaning, drag reduction, anti-sticking, anti-icing and so on  
59 (Bhushan and Jung, 2011; Chen et al., 2012). The definition for superhydrophobicity is  
60 when a drop on a surface has a contact angle above  $150^\circ$  (Guo and Liu, 2007). The  
61 major property of superhydrophobic surfaces is their ability to repel water. An  
62 important factor to superhydrophobicity is the chemical composition of the epicuticular  
63 waxes covering the aerial tissues of the plant coupled with the micro-/nano-hierarchical  
64 structure of the cuticle (Bhushan et al., 2009; Wang et al., 2014). In lotus leaves, the  
65 strong water repellency is due to wax tubules composed of the secondary alcohols  
66 nonacosan-10-ol and nonacosanediols (Ensikat et al., 2011). Nonacosan-10-ol is present  
67 in many natural superhydrophobic surfaces including lotus leaves and conifer needles,  
68 and it has significant potential for its use in coatings for porous materials. However, this  
69 molecule is currently not commercially exploited. Since nonacosan-10-ol comprises up  
70 to 60% of the total wax found in the needles of conifer species (Matas et al., 2003), it  
71 could be used as an alternative to the currently utilized non-renewable coatings, such as

72 plastic coatings on porous materials. Extraction of nonacosan-10-ol from spruce offers  
73 several distinct advantages. Firstly, nonacosan-10-ol is the most abundant wax found  
74 in spruce needles (Simmleit and Schulten, 1989). Secondly, the growth rate of spruce  
75 trees is very fast (Macmillan, 1991), with a yield class (mean cubic meters growth) for  
76 Sitka spruce of 14 (i.e. 14 cubic meters per hectare per year according to Forestry  
77 Commission (Forestry Commission, 2017)). In terms of maximum timber potential,  
78 Sitka spruce requires only 40 – 60 years, whereas oak trees require 150 years (Forestry  
79 Commission, 2017). Spruce comprises 29% of all UK commercial forestry, which  
80 covers over 1,000,000 hectares (Mason and Perks, 2011; Moore, 2011), resulting in a  
81 high turnover and large quantities of needles. Thirdly, as previously stated, spruce  
82 needles currently constitute a waste stream and have no commercial value.

83

84 The extraction of epicuticular waxes from agricultural wastes (Attard et al., 2015a,b &  
85 2016b), as well as nonacosan-10-ol from Ephedra herbs (Choi et al., 1996), have  
86 already been shown to be effective utilizing supercritical carbon dioxide (scCO<sub>2</sub>) as a  
87 renewable solvent . ScCO<sub>2</sub> offers numerous advantages over conventional solvent  
88 extraction in that the selectivity towards target molecules could be achieved by fine-  
89 tuning the solvent power (McHugh and Krukonis, 1994; Özcan and Özcan, 2004). This  
90 is carried out simply by changing the temperature and pressure of the solvent (Lang and  
91 Wai, 2001; Vilegas et al., 1997; Zougagh et al., 2004). ScCO<sub>2</sub> leaves no solvent  
92 residues and is regarded as a non-toxic solvent (Hunt et al., 2010). Furthermore, scCO<sub>2</sub>  
93 has been shown to be effective in improving the downstream processing of biomass in a  
94 biorefinery, whereby increased sugar yields have been reported for various biomass  
95 types, as well as significantly improved off-gassing from wood pellets (Attard et al.,

96 2015b, 2016a, b). This recent work indicates that scCO<sub>2</sub> can be used effectively for  
97 valorizing forestry waste, generating bio-derived chemicals as well as improving  
98 downstream processing. Optimization studies on wax extraction from spruce species  
99 have not been previously conducted. To date, reported purification of nonacosan-10-ol  
100 involved time and material intensive chromatographic techniques, which utilize toxic  
101 solvents, in particular CHCl<sub>3</sub> and benzene (Jetter and Riederer, 1994; Matas et al., 2003;  
102 Yao et al., 2007).

103 Herein, this work focuses on the supercritical extraction of waste spruce needles that are  
104 rich in the secondary alcohol nonacosan-10-ol. The extraction, optimization and  
105 characterization of waxes from two species of spruce namely Sitka Spruce and  
106 Norwegian Spruce have been carried out for the first time using scCO<sub>2</sub> as a green  
107 alternative solvent. More importantly, a facile green recrystallization technique was  
108 conducted in order to isolate the nonacosan-10-ol from the complex mixture of  
109 lipophilic molecules utilizing a highly scalable method. To the authors' best knowledge,  
110 combination of supercritical extraction followed by the use of a facile recrystallization  
111 technique for the recovery of nonacosan-10-ol has not yet been reported.

112

## 113 **2. Materials and Method**

### 114 2.1 Biomass and sample preparation

115

116 With the kind support of the Forestry Commission, Sitka Spruce was collected from  
117 Dalby Forest at North Yorkshire in the United Kingdom, while the Norwegian Spruce  
118 was collected from Umeå, Sweden. The biomass constituted the needle-rich small  
119 branches from numerous trees that had been recently felled for lumber. Samples of the

120 biomass were then separated, through air drying until a constant weight was observed  
121 (*circa* three weeks) and a small portion refrigerated at 5 °C. A small sample of the dry  
122 biomass and all of the refrigerated wet biomass were then milled as a whole, while the  
123 needles of the remaining dry feedstock were easily separated by shaking from the  
124 branch. All milling was carried out using a Glen-Creston mill, with a 2 mm mesh.

## 125 2.2 ScCO<sub>2</sub> extraction of spruce needle wax

126

127 A Thar SCF500 CO<sub>2</sub> extractor was used to carry out the extractions. The dried, milled  
128 biomass (50 g) was placed into the extraction cylinder and extracted for 2 hours with  
129 CO<sub>2</sub> at various pressures (200, 300 and 400 bar) and temperatures (40, 50 and 60 °C),  
130 with a flow rate of 40 g min<sup>-1</sup>. The extract was depressurized to atmospheric conditions  
131 into the first extraction vessel and the wax removed using dichloromethane (2 x 50 mL  
132 washes). The solvent was evaporated to yield the product.

133

## 134 2.3 Purification of nonacosan-10-ol from scCO<sub>2</sub> extracted spruce needles (150 g)

135

136 Methanol (50 ml) was added to the spruce needle extract (3.22 g). The solution was  
137 stirred at 50 °C for 10 minutes and left to cool to room temperature. The solution was  
138 filtered and washed with cold methanol (2 x 10 ml) to obtain the crude product. The  
139 crude product was then dissolved in hot methanol (30 ml) yielding a light green solution  
140 and a dark green wax/dense oil. The solute (light green solution) was decanted and left  
141 to cool yielding a light green precipitate. The dark green wax/dense oil was washed  
142 with hot methanol (10 ml) to yield a brittle wax. The light green precipitate was  
143 recrystallized a second time in hot methanol (30 ml), decanted, left to cool, filtered,

144 washed with cold methanol (2 x 10 ml) and dried to yield a white precipitate,  
145 nonacosan-10-ol. Unrecovered nonacosan-10-ol could be recovered from the  
146 recrystallization media by evaporation of the methanol solvent, allowing this crude  
147 mixture to potentially be recycled within the recrystallization process.

148

149 [Scheme 1 here]

150

151 2.4 Contact angle method

152 Basic contact angle measurements were obtained by dissolving a known amount of pure  
153 nonacosan-10-ol in hot methanol to give a 1% or 20% by weight solids content. A solid  
154 support (glass or filter paper) was then dipped in the solution, removed and left to dry  
155 under atmospheric conditions. Once dry, a drop of distilled water was applied to the  
156 surface using a pasture pipette with a minimum drop height without the pipette coming  
157 into contact with the surface material. Photos of the droplet were then taken and the  
158 contact angle was determined.

159

160 2.5 Derivitization prior to High Temperature-Gas Chromatography (HT-GC) analysis

161 Derivitization was achieved by the addition of 200  $\mu$ l N,O-*bis*-(trimethylsilyl)-trifluoro-  
162 acetamide with 1% trimethylchlorosilane to 30 mg of the crude extract dissolved in 1 ml  
163 toluene. The solution was placed in an oven and heated at 75 °C for 45 minutes.

164

165 2.6 HT-GC procedure for analysis of wax

166 High temperature Gas Chromatography was conducted using an Agilent Technologies  
167 6890N Network GC System. This was fitted with a ZB-5HT capillary column

168 (dimensions: 30 m x 250  $\mu\text{m}$  x 0.25  $\mu\text{m}$  nominal) at constant pressure (22.35 psi). A  
169 temperature of 300  $^{\circ}\text{C}$  was selected as the injector temperature and flame ionization  
170 detector temperature while the carrier gas utilized was helium. A split ratio of 5:1 was  
171 applied. Injection of the sample (1  $\mu\text{l}$  injection volume) was carried out by automated  
172 injection. The oven temperature was set as follows: (i) Initial temperature of 60  $^{\circ}\text{C}$ , held  
173 for 1 minute ii) The temperature was increased to 360  $^{\circ}\text{C}$  at a ramp rate of 8  $^{\circ}\text{C min}^{-1}$   
174 iii) The temperature was held at 360  $^{\circ}\text{C}$  for 30 minutes.

175 2.7 HT-GC-MS (High Temperature-Gas chromatography Mass Spectrometry)

176 procedure for wax analysis

177 A Perkin Elmer Clarus 500 GC coupled with a CLarus 500 quadrupole mass  
178 spectrometer was used to perform the high temperature-gas chromatography mass  
179 spectrometry. A DB5HT capillary column was fitted (dimensions: 30 m x 250  $\mu\text{m}$  x  
180 0.25  $\mu\text{m}$  nominal) at constant pressure (22.35 psi). A temperature of 300  $^{\circ}\text{C}$  was  
181 selected as the injector temperature and helium was selected as the carrier gas. The flow  
182 rate was 1.2  $\text{ml min}^{-1}$ . The temperature profile for the oven was as follows: (i) Initial  
183 temperature of 60  $^{\circ}\text{C}$ , held for 1 minute ii) The temperature was increased to 360  $^{\circ}\text{C}$  at  
184 a ramp rate of 8  $^{\circ}\text{C min}^{-1}$  iii) The temperature was held at 360  $^{\circ}\text{C}$  for 30 minutes. The  
185 electron ionization mode (EI) at 70 eV was selected for the Clarus 500 quadrupole mass  
186 spectrometer with a source temperature of 300  $^{\circ}\text{C}$ . A scan range of 30 – 1200 amu per  
187 second was applied.

### 188 3. Results and Discussion

189 3.1 Optimization of the supercritical extraction of waxes from Spruce needles

190

191 An attempt was made to optimize the % yield of wax extracted from the spruce needles  
192 using scCO<sub>2</sub> extraction by applying the factorial experimental design, whereby  
193 temperature and pressure (independent variables) were varied in order to study the  
194 effect this has on the extraction yield (dependent variable). The experiments required 2<sup>f</sup>  
195 runs (f = factors), where each factor was at two levels, those of the minimum and  
196 maximum extraction limits.

197

198 A variety of temperatures and pressures were utilized in an experimental 2x2 plot  
199 (supplementary Figure S1) in order to investigate two parameters at the same time. A  
200 pressure range of 200 to 400 bar was applied (since previous studies have shown that  
201 very low pressures give low yields of extract) while a temperature range of 40 to 60 °C  
202 was applied. Four experimental points were selected at maximum and minimum  
203 temperatures and pressures (A, B, C and D – Figure S1). A center point was also  
204 introduced in order to ensure there was no risk of missing a non-linear relationship  
205 within the experimental range.

206

207 The impact of pressure and temperature was modelled by means of a dimensionless  
208 factor coordinate system, whereby “-1” was assigned for the low level and “+1” was  
209 given to the high level for each parameter. The center point was assigned a coordinate  
210 value of “0” (coincides with the origin of the system) as shown in Tables 1 and 2 below.

211

212 [Table 1 here]

213 [Table 2 here]

214

215 Therefore, five experiments were conducted for the optimization study and multiple  
 216 linear regression (MLR) was used in order to deduce the relationship between crude  
 217 yield and temperature and pressure. The first order polynomial function utilized for the  
 218 MLR is shown below in Equation 1:

$$Y = b_0 + b_1x_1 + b_2x_2 + b_{12}x_1x_2$$

219  
 220

Equation 1: First order polynomial function

221 Where Y is the % crude yield,  $b_1$  and  $b_2$  correspond to the major effects of the  
 222 coordinates  $x_1$  (temperature) and  $x_2$  (pressure),  $b_0$  represents the center point yield (E –  
 223 the response at “0” level) and  $b_{12}$  is the second order interaction term. Two-hour  
 224 extraction times were allotted for each set of experiments and a flow rate of  $40 \text{ g min}^{-1}$   
 225 was applied. Table 3 summarizes the % yield of wax obtained at different temperatures  
 226 and pressures.

227

228 **[Table 3 here]**

229 **[Figure 1 here]**

230

231 From the % yields shown in Table 3, MLR was conducted as shown in Equations 2-5  
 232 below in order to obtain a first order polynomial function to model the  $\text{scCO}_2$  extraction  
 233 of waxes from Sitka spruce needles.

$$b_0 = \frac{1}{4}(y_1 + y_2 + y_3 + y_4)$$

$$b_1 = \frac{1}{4}(-y_1 + y_2 - y_3 + y_4)$$

$$b_2 = \frac{1}{4}(-y_1 - y_2 + y_3 + y_4)$$

234

$$b_{12} = \frac{1}{4}(y_1 - y_2 - y_3 + y_4)$$

235 Equations 2, 3, 4 and 5: coefficient calculations for the first order polynomial function

236

$$237 \quad Y = 1.32 + 0.24x_1 + 0.16x_2 - 0.015x_1x_2$$

238 Equation 6 First order polynomial function for the scCO<sub>2</sub> extraction of waxes from  
239 needles.

240

241 The coefficients of pressure, temperature and the second order interaction term are  
242 shown in equation 6, and can be used to help understand the effect of temperature and  
243 pressure (as well as the combined effect of the two parameters) on the extraction  
244 process. The theoretical % yield for the center point value E (1.32%) was found to be in  
245 good correlation with the experimental value (1.41%) (a 0.09% difference with a 6.8%  
246 error) indicating the model behaves well for this extraction. It can be seen that in this  
247 instance the value of  $x_1$  for temperature is higher than that of  $x_2$  (pressure) which  
248 indicates that temperature has a higher influence on the extraction yield than pressure  
249 and density (since an increase in pressure at constant temperature leads to an increase in  
250 density).

251 Figure 1 demonstrates a 2-D plot highlighting the variation in % crude yield of wax  
252 with varying temperature and pressure (the different % crude yields may also be viewed  
253 in Figure S2). As shown in Table 1, the % yield of wax extracted from the Spruce  
254 needles under the different conditions applied varied from 0.91 to 1.70%.

255 The dielectric constant and density of CO<sub>2</sub> are dictated by temperature and pressure  
256 (Hunt et al., 2010). In the extraction of wax the density of CO<sub>2</sub> is an important factor.  
257 Higher yields were obtained at 400 bar 40 °C than at 200 bar 40 °C, indicating that the  
258 increase in density led to a greater yield, this is consistent with other wax extraction

259 studies (Attard et al., 2015b; Sin et al., 2014). However, the highest yields (1.70%) were  
260 achieved using a pressure of 400 bar and temperature of 60 °C, where the density is  
261 lower than that at 400 bar and 40 °C. This demonstrates that even though density has an  
262 important role, there are other factors such as temperature that dictate the solubility of  
263 compounds in CO<sub>2</sub>. These results are consistent with the findings of the first order  
264 polynomial function. Studies have highlighted that higher yields can be obtained when  
265 the temperature is close to or above the waxes melting point (Sin et al., 2014). Since  
266 wax is in semi-crystalline form, higher temperatures enable the melting of the wax and  
267 therefore aiding in extraction. Furthermore, an increase in temperature at constant  
268 pressure results in vapor pressure increase leading to an increase in solute solubility in  
269 scCO<sub>2</sub>.

270  
271 The results show that a significant increase in yield was observed at elevated  
272 temperatures, where the extraction yields at 200 bar and 40 °C were 0.91% rose to  
273 1.41% when increased by 20 °C. Furthermore, at high pressure conditions a significant  
274 increase in yield was obtained at higher temperatures (i.e. 1.70% at 400 bar and 60 °C –  
275 ), as compared to lower temperatures (i.e. 1.26%, at 400 bar and 40 °C –). This data  
276 correlates to the first order polynomial function obtained, whereby temperature is the  
277 most influential factor on the % yield (though pressure also has a positive influence).

278  
279 3.2 Characterization and quantification of lipophilic compounds in the needle extracts  
280 from Sitka Spruce.

281

282 GC and GC-MS analyses were used to characterize the underivatized and silylated  
283 extracts using a high temperature capillary column and methods which allowed for the  
284 elution and determination of high-molecular weight compounds such as sterols and  
285 unsaturated long-chain ketones.

286 Results from Table 4 and Figure 2 showed that the major compounds identified were  
287 found to be nonacosan-10-ol, free saturated (ranging from C<sub>12</sub> to C<sub>20</sub> in chain length)  
288 and unsaturated fatty acids (C<sub>18</sub> chain length), unsaturated ketones (C<sub>28</sub> and C<sub>30</sub> chain  
289 length), sterols, hydroxyacids, benzoic acid and phytol. For all conditions examined, it  
290 was found that nonacosan-10-ol was the predominant compound in the wax extracts.

291 Although conditions of 400 bar and 60 °C gave the highest % crude extract yield, it was  
292 found that the conditions which led to the highest yields of nonacosan-10-ol were 200  
293 bar and 60 °C, with approximately 8,070 ± 91.1 µg/g needles extracted. This is also  
294 consistent with the observation that a high % crude yield of wax was extracted using  
295 these conditions. The lowest quantities of nonacosan-10-ol were extracted when using  
296 conditions of 200 bar and 40 °C, with approximately 2,870 ± 266.6 µg/g of needles  
297 extracted. When using the conditions of 200 bar and 60 °C, the highest yields of β-  
298 sitosterol and benzoic acid were also obtained, with an estimated 398 ± 6.6 and 100 ±  
299 16.6 µg/g of needles extracted respectively. Conditions of 300 bar and 50 °C led to the  
300 highest yields of ketones, with approximately 978 ± 81.3 µg/g of needles extracted. The  
301 same conditions led to the highest extraction of fatty acids and hydroxyacids. Therefore,  
302 it can be concluded that, although conditions of 400 bar and 60 °C led to the highest %  
303 crude yield of wax extract, the largest quantities of nonacosan-10-ol were achieved with  
304 200 bar and 60 °C. Thus, the conditions needed for the extraction vary according to the  
305 desired product, i.e. the extract as a whole or nonacosan-10-ol or unsaturated ketones.

306

307 [Table 4 here]

308 [Figure 2 here]

309

310 Furthermore, nonacosan-10-ol is the major compound, constituting around 60% of the  
311 total extract at 200 bar and 60 °C. For all other extracts, nonacosan-10-ol constitutes  
312 considerably low proportion of the composition (i.e. 22 – 42%).

313

314 3.3 Characterization and quantification of lipophilic compounds in the needle extracts  
315 from Norwegian Spruce.

316

317 Since conditions of 200 bar and 60 °C led to the highest quantities of nonacosan-10-ol  
318 from Sitka Spruce, these conditions were also applied to the extraction of wax from  
319 Norwegian spruce needles in order to make a direct comparison of the nonacosan-10-ol  
320 content between the two species. When compared to the Sitka, Norwegian spruce  
321 exhibited a more complex mixture of lipophilic chemicals (as seen in Figure S3). There  
322 is a wider variety of fatty acids, steroids and also a number of terpenoid compounds,  
323 which are absent or below the level of detection in the Sitka spruce.

324

325

326 Figure 3 compares the major compounds found in the waxes extracted from the Sitka  
327 spruce and Norwegian spruce. Nonacosan-10-ol concentrations in Sitka spruce needles  
328 are approximately double the amount present in the Norwegian spruce needles, 8070  
329  $\pm 91.1$   $\mu\text{g/g}$  of needles and 3966.6  $\pm 114.3$   $\mu\text{g/g}$  of needles respectively. On the other

330 hand, significantly larger amounts of saturated and unsaturated fatty acids are present in  
331 the Norwegian spruce needles ( $2122.4 \pm 20 \mu\text{g/g}$  of needles and  $3669.3 \pm 19.1 \mu\text{g/g}$  of  
332 needles respectively) compared to the Sitka spruce needles ( $551.8 \pm 37 \mu\text{g/g}$  of needles  
333 and  $181.42 \pm 20.3 \mu\text{g/g}$  of needles respectively). Sitosterol is the only steroidal  
334 compound found in the Sitka spruce, while three other steroidal compounds are found in  
335 the Norwegian spruce (9,19-cyclolanostan-3-ol, 24 methylene - ( $3\beta$ -)-, 24-  
336 Methylene-cycloartan-3-one and Stigmastan-3,5-diene) which accounts for the greater  
337 concentration of these compounds in the Norwegian spruce extracts ( $2122.4 \pm 43.6 \mu\text{g/g}$   
338 of needles). Unsaturated ketones are present in the needle extracts of both species;  
339 however, a higher abundance is found in the Sitka spruce ( $885.1 \pm 20.1 \mu\text{g/g}$  of needles)  
340 when compared to the Norwegian spruce ( $159.6 \pm 0.9 \mu\text{g/g}$  of needles) (Table 5).

341

342 [Table 5 here]

343 [Figure 3 here]

344

345 3.4 Simple isolation and purification of Nonacosan-10-ol from spruce

346

347 The development of new separation technologies for biorefineries is of significant  
348 importance for their long-term development and commercial success. Due to the  
349 complex and highly functionalized nature of bio-derived molecules, traditional  
350 techniques such as distillation are not always suitable for retaining functionality.  
351 Therefore, new or greener methods that preserve the complexity of the bio-derived  
352 molecules are of vital importance. Furthermore, standard chromatographic separation  
353 techniques such as HPLC and continuous liquid chromatography are energy intensive

354 and use large quantities of solvents leading to cumulative solvent waste which is often  
355 problematic to dispose(Yao et al., 2007). Therefore, a simple and efficient isolation and  
356 purification methodology for nonacosan-10-ol was developed. The placing of the crude  
357 product obtained by extraction in a polar solvent causes most lipophilic compounds to  
358 crash out. The initial polar solvents screened were methanol, ethanol and iso-propanol.  
359 These polar solvents were selected as they are labelled as 'Recommended' on the recent  
360 Chem 21 solvent selection guide and Sanofi selection guide; whereas these had only  
361 some issues on the GSK solvent selection guide (associated with health, flammability  
362 and explosion) (Henderson et al., 2011; Prat et al., 2013&2015).

363

364 The purest product was obtained using methanol as solvent for purification, where the  
365 ratio of methanol to crude extract used was much smaller (12:1), resulting in the  
366 formation of a green precipitate (Figure S14). Methanol has the advantages of being  
367 relatively inexpensive, potentially bioderived, easily biodegradable and has low  
368 resistivity (Prat et al., 2013). However, the drawbacks of methanol are flammable and  
369 volatile (Prat et al., 2013). After filtration, this green precipitate could, in turn, be  
370 solvated in hot methanol to produce a light green solution and dark green black wax.  
371 The hot solute was then carefully decanted into separate glassware and left to cool,  
372 where a light green precipitate formed upon cooling. This was recrystallized a second  
373 time to yield a white precipitate. GC-MS analysis (shown in Figure S4 and S5) of the  
374 white precipitate confirmed it to be nonacosan-10-ol, however minor impurities are still  
375 present. The purity of the nonacosan-10-ol obtained was found to be 90% (Figure S6).  
376 Proton and carbon NMR of the product matched literature values, although other signals  
377 are also present, again indicating the presence of minor impurities (as shown in Figures

378 S7 and S8). Evaporation of methanol could also be utilized to recover additional  
379 nonacosan-10-ol.

380

381 In addition to the nonacosan-10-ol, a brittle dark green wax was also obtained. GC-FID  
382 analysis of this brittle wax reveals that the sample contains nonacosan-10-ol, two trace  
383 fatty acids and predominantly two compounds. As shown in Figures S9 and S10, the  
384 GC-MS EI fragmentation patterns suggest these two compounds to be  $C_{28}$  and  $C_{30}$   
385 unsaturated aldehydes, giving molecular ions of 406 and 434 respectively, with no other  
386 fragments observed, relating to compounds with molecular formulas of  $C_{28}H_{54}O$  and  
387  $C_{30}H_{58}O$ . Figure S11 shows the proton NMR of the compound, with evidence of  
388 unsaturation visible in the spectrum. However, the distinctive signal of the aldehyde  
389 proton is missing, which shows that these compounds are more likely to be unsaturated  
390 ketones. Additional unrecovered nonacosan-10-ol in this sample could be recovered  
391 through recycling of this crude mixture within the recrystallization process.

392

393 In order to ensure repeatability as well as broad application, the same purification  
394 technique was conducted on the more complex Norwegian spruce wax extract  
395 (Figure 4). Once again three fractions were obtained, each differing in composition. The  
396 methanol-soluble layer was found to be rich in terpenes, fatty acids, phenolic  
397 compounds and sterols. These molecules are completely absent or found in minute  
398 quantities in the other fractions showing the selective extraction of these molecules in  
399 methanol. A dark green/black wax was also obtained with the Norwegian spruce  
400 extract, which consists mainly of unsaturated ketones, saturated aldehydes and wax  
401 esters. Importantly, the same result was obtained with the Norwegian spruce extract as

402 with the Sitka spruce extract, i.e. a white precipitate was collected following the  
403 purification method which was confirmed to be nonacosan-10-ol by GC-FID. This  
404 indicates that, although Norwegian spruce had a more diverse and complex range of  
405 lipophilic molecules, the purification method still led to the selective isolation of  
406 nonacosan-10-ol of reasonably high purity. This shows that the purification method is  
407 not limited to just one type of biomass extract but can be applied to different wax  
408 extracts containing high amounts of nonacosan-10-ol.

409

410

411 Mass balances were calculated for each wax extract and it was found that approximately  
412 44.6% and 48.4%  $\pm$  2% of the total nonacosan-10-ol were recovered from the original  
413 crude Sitka and Norwegian wax respectively. As shown in Figure 4, some of the  
414 nonacosan-10-ol was lost during the first step due to its limited solubility in methanol  
415 (as shown in Figure 4.) while some of it was also found present in the ketone layer.  
416 Nevertheless, substantial amounts of nonacosan-10-ol were isolated using this simple  
417 technique, equating to approximately 3,600  $\mu$ g/g needles for the Sitka spruce and 1,920  
418  $\mu$ g/g needles for the Norwegian spruce. Recycling of the methanol and recycling the  
419 dark green brittle wax to undertake additional recrystallizations could yield yet more  
420 nonacosan-10-ol (Figure S14).

421

422 **[Figure 4 here]**

423

424 Therefore, it has been shown that a simple single solvent purification technique could  
425 be used to obtain nonacosan-10-ol of relatively high purity. This would reduce

426 considerably the volumes of solvent used and the time of separation when compared to  
427 standard chromatographic techniques. Furthermore, since only one solvent is used, it  
428 can be recycled without risk of contamination.

429

### 430 3.5 Scanning Electron Microscopy (SEM)

431 The surface of the original biomass and supercritically extracted biomass, along with  
432 nonacosan-10-ol and wax residue were investigated by scanning electron microscope  
433 (Figure 5). Figure 5A and 5B show the nanotubules formed by nonacosan-10-ol and  
434 observed on the needles. Figure 5C and 5D shows that these self-assembled nano  
435 structures have partially survived the milling process and are present in the biomass  
436 feedstock prior to extraction. . Figure 5E and 5F demonstrate the purified nonacosan-  
437 10-ol compound and despite the rapid recrystallisation process complex spherical  
438 structures, which indicates self-assembly phenomenon was observed. Additionally SEM  
439 images of the biomass post extraction showed no remaining wax indicating all surface  
440 wax had been successfully removed (figure S12).

441 **[Figure 5 here]**

442

### 443 3.6 Simple application of the nonacosan-10-ol extract

444 Initial testing of nonacosan-10-ol to demonstrate its use in potential barrier property  
445 applications was achieved by its coating onto a porous material. To this end, a 1%  
446 nonacosan-10-ol solution in methanol was applied to a glass slide. Nonacosan-10-ol  
447 solution in methanol (1% and 20%) were applied to porous materials, namely filter  
448 paper. As shown in Figure 6, droplets formed on the glass and filter paper. The contact  
449 angles were measured and are reported in Table 6.

450

451 [Figure 6 here]

452 [Table 6 here]

453

454 A droplet of water was then applied to the coated surface and the contact angle was  
455 measured (Figure 6). In the case of the glass (Figure 6C), i.e. the presence of a 1%  
456 nonacosan-10-ol increases the contact angle from  $37^\circ$  (control – untreated slide) to  $128^\circ$   
457 for the coated slide (Figure 6D), indicating markedly increased water barrier properties.  
458 For the filter paper, it can be observed that a 1% nonacosan-10-ol solution increased the  
459 contact angle from  $0^\circ$  to  $132^\circ$  while a 20% nonacosan-10-ol solution resulted in a  
460 contact angle of  $149^\circ$ , indicating a hydrophobic surface which borders on being  
461 superhydrophobic. Optical Microscopy imaging and SEM show the nonacosanol  
462 assembling on glass slide (Figure S13 and Figure 6F respectively). These preliminary  
463 tests demonstrate significant promise and future work will optimize the process to  
464 obtain superhydrophobic coatings for utilization in various applications.

465

#### 466 4. Conclusions

467

468 Therefore, it has been shown that a natural hydrophobic molecule, with potential  
469 industrial applications in coatings, could be selectively extracted from forestry waste  
470 using clean technology (scCO<sub>2</sub>) and purified using a simple single solvent technique  
471 resulting in significant reductions in solvent usage, considerably lower volumes of  
472 solvent waste and hence a more efficient process.

473 Extraction of Spruce using scCO<sub>2</sub> extraction yielded 1.70% of wax at 400 bar and  
474 60 °C, nonacosan-10-ol was the major component at 200 bar and 60 ° C. Purification of  
475 nonacosan-10-ol from the wax was conducted using a simple, green recrystallization  
476 technique with a purity of 90%. Preliminary results on contact angle measurements  
477 show coating of paper with 20% nonacosan-10-ol solution resulted in a highly  
478 hydrophobic surface with contact angle of 149°. This method may develop new  
479 opportunities to selectively extract and purify nonacosan-10-ol using green technologies  
480 and solvents from a forestry waste to generate additional value as part of a holistic  
481 biorefinery. Finally, valorization of the forest waste would reduce the problem of  
482 significant accumulation of overproduced biomass residues from neglected forests.

483

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485

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490

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- 599

## List of Figures



Scheme 1. Flow diagram illustrating the purification of Nonacosan-10-ol from Spruce.

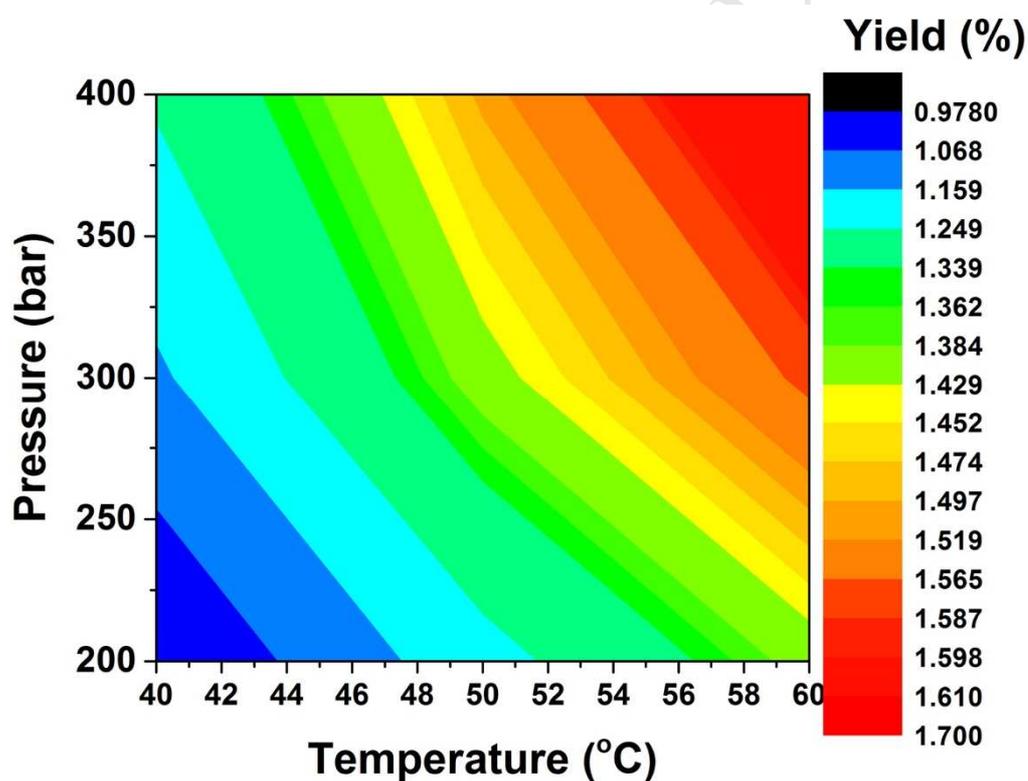
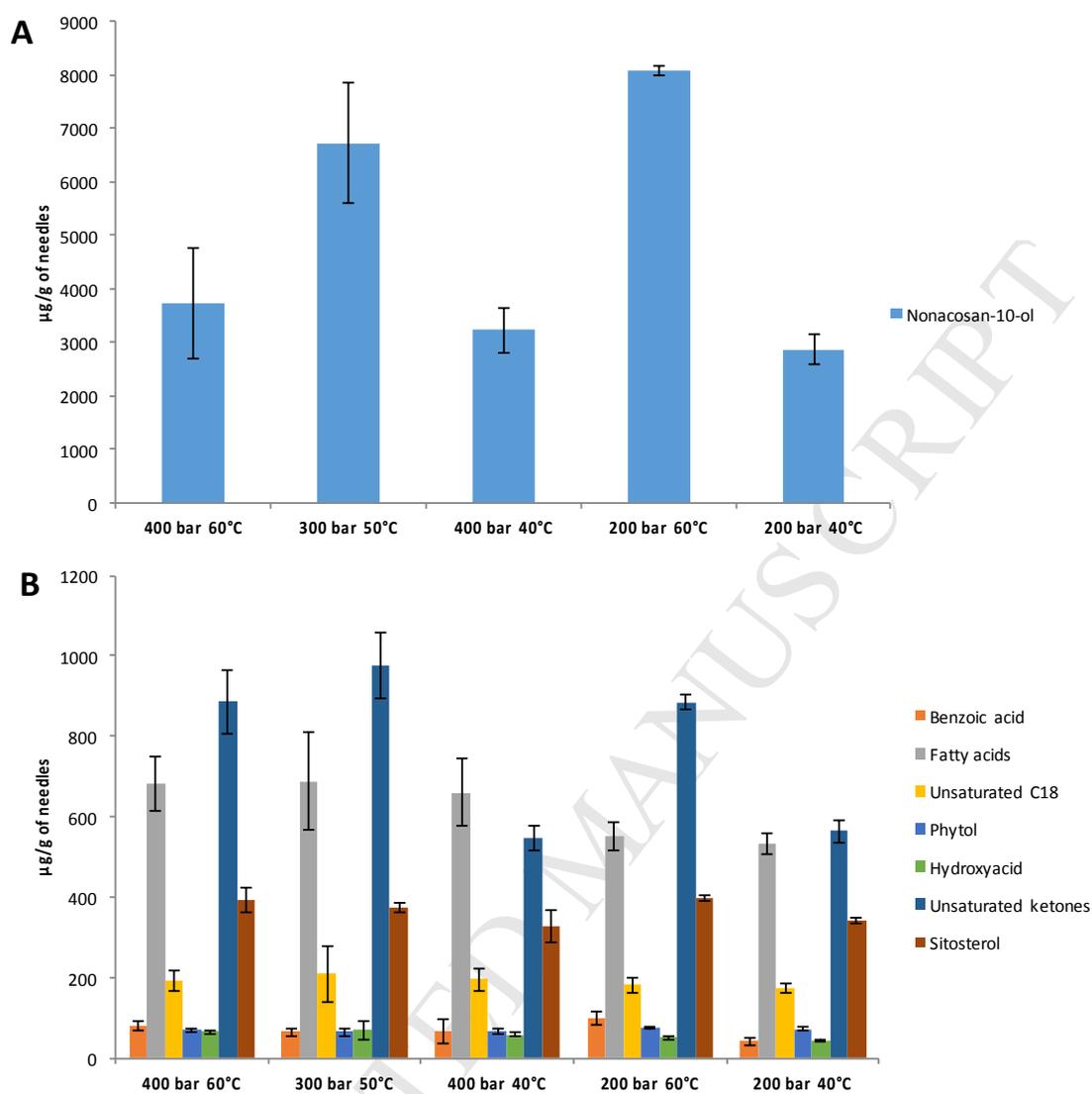
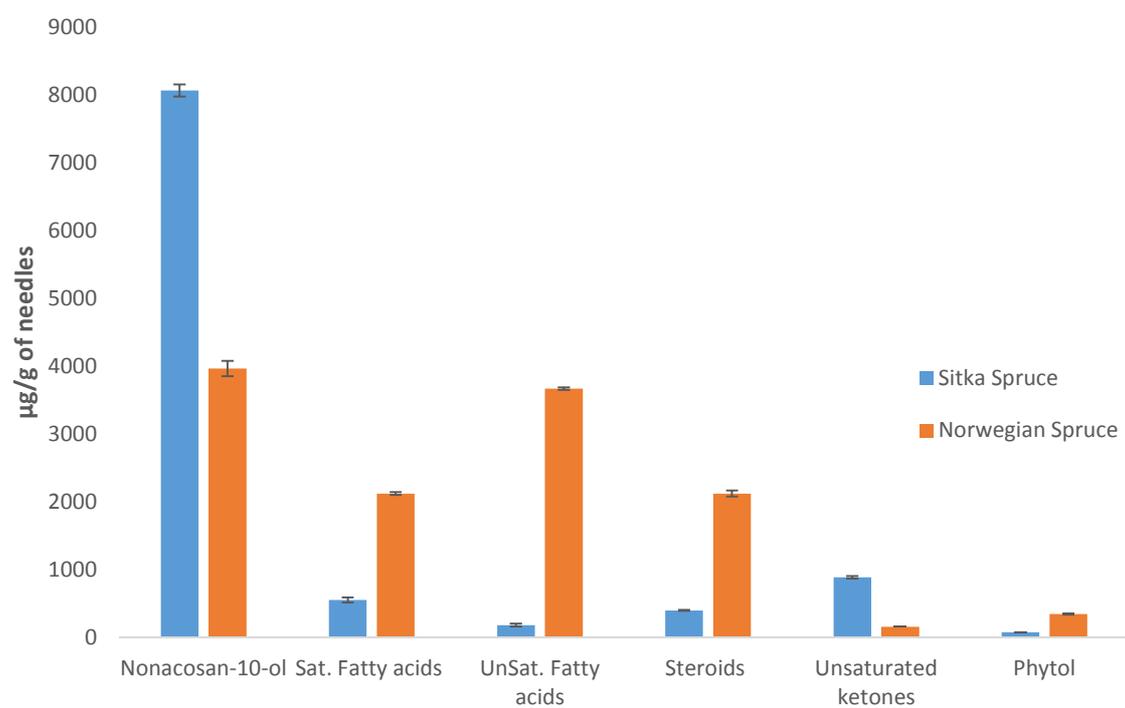


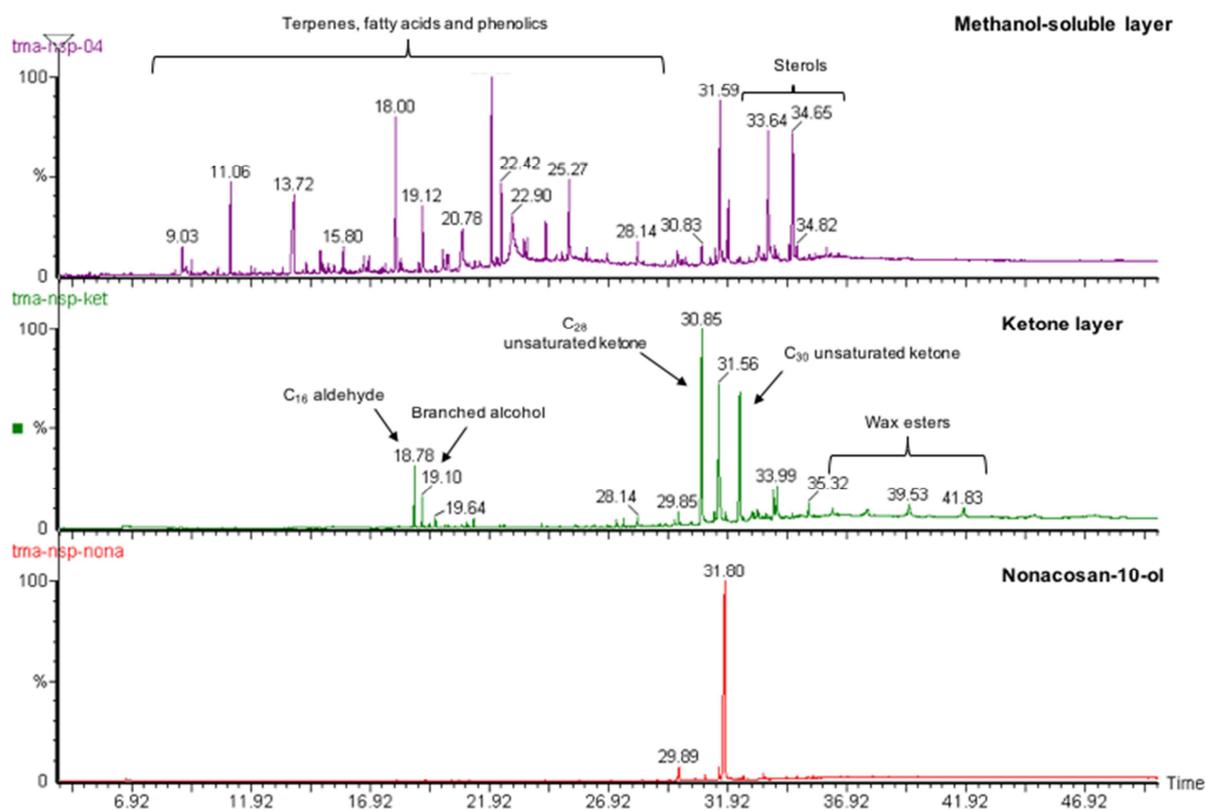
Figure 1. 2-D plot showing the effect of varying pressure and temperature on the % crude wax yield from Sitka Spruce.



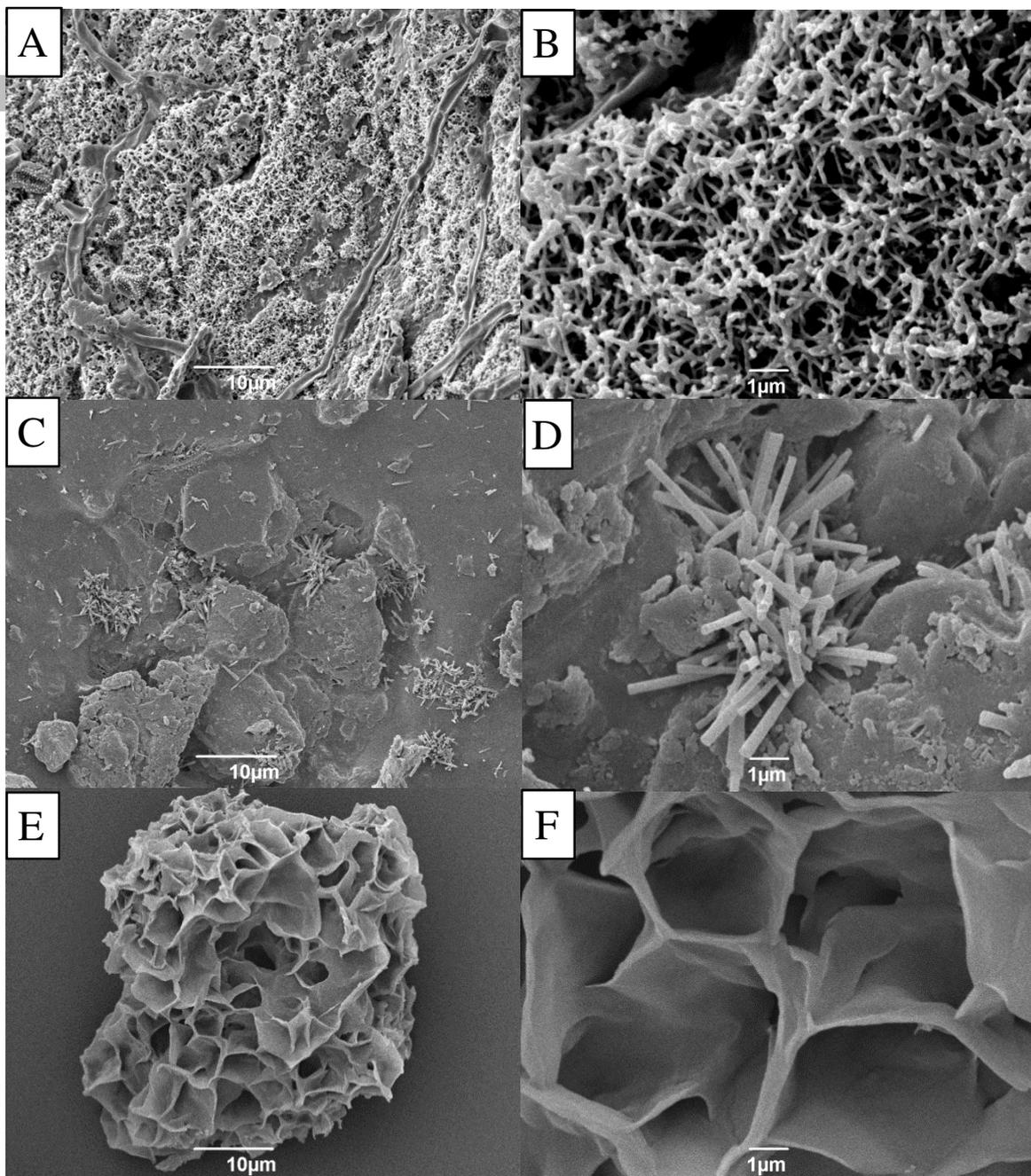
**Figure 2. Composition of organic compounds at various temperature and pressure: A) Nonacosan-10-ol B) Benzoic acid, Fatty acids, Unsaturated C18 acids, Phytol, Hydroxyacid, Unsaturated ketones and Sitosterol.**



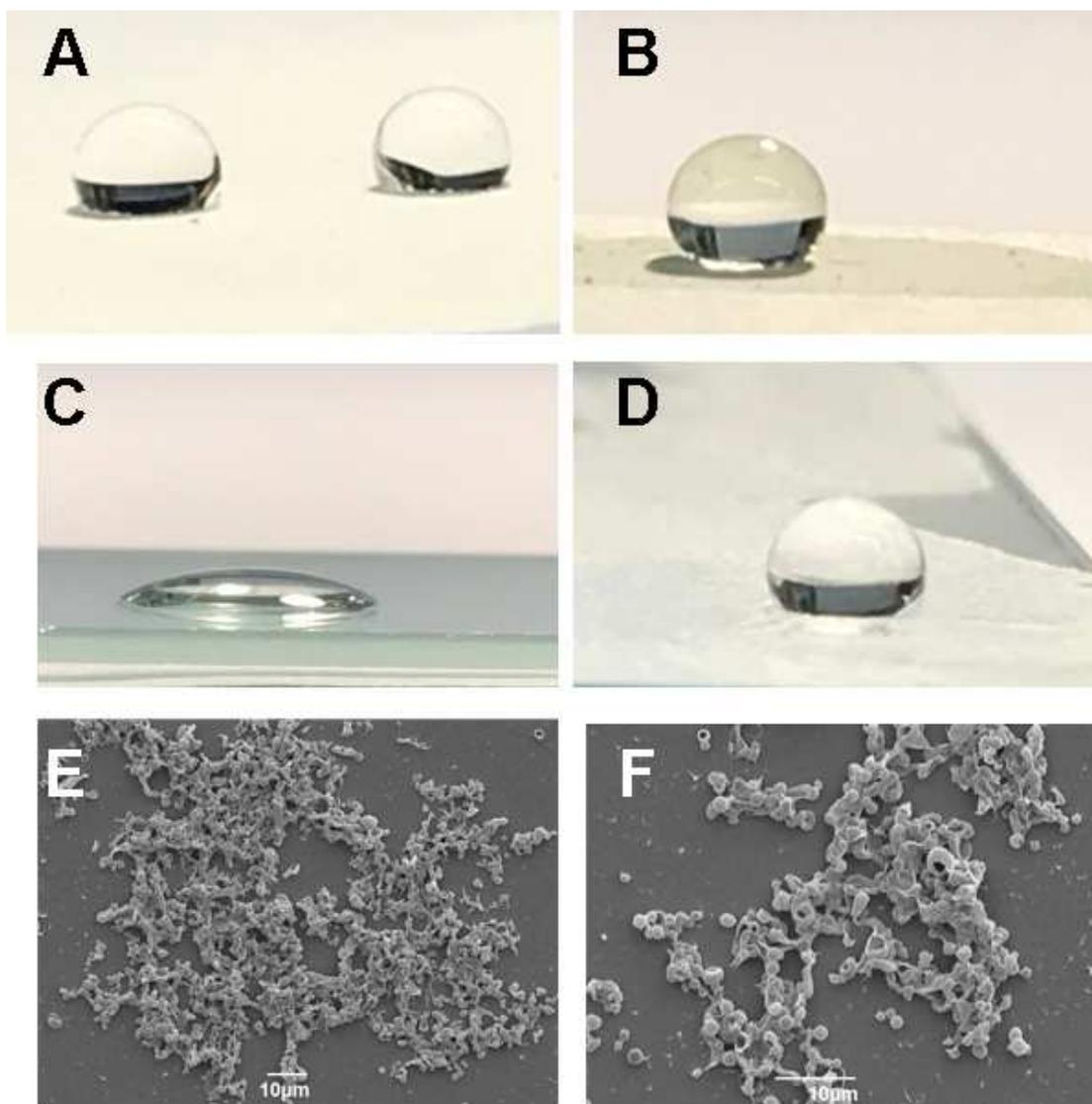
**Figure 3. Comparison of major compounds found in waxes from Sitka spruce and Norwegian spruce.**



**Figure 4. GC-MS chromatograms of a) Methanol-soluble layer b) Ketone layer and c) Nonacosan-10-ol.**



**Figure 5. SEM images of spruce and spruce extracts. A and B = Nanotubules formed by nonacosan-10-ol on the biomass (spruce needles), C and D = Nanotubules still present on needles following milling, E and F = complex, spherical structures of purified nonacosan-10-ol.**



**Figure 6 A) Droplets formed on filter paper with a 1% nonacosan-10-ol solution B) Droplet formed on paper with a 20% nonacosan-10-ol solution C) Control: droplet on a glass slide and D) Droplet on glass covered with a 1% nonacosan-10-ol solution. E) SEM of nonacosanol assembling on glass slide ( $\times 500$ ) F) SEM of nonacosanol assembling on glass slide ( $\times 1,000$ ).**

## List of Tables

**Table 1** The experimental design with the normalized values for temperature and pressure.

Factor	Variable	Normalized values		
		-1	0	1
X1	Temperature (°C)	40	50	60
X2	Pressure (bar)	200	300	400

**Table 2.** Experimental design with the different conditions and the assigned normalized values.

Experiment Point	Coordinate values		Experimental conditions	
	X1	X2	Temp. (°C)	Pressure (bar)
A	-1	+1	40	400
B	+1	+1	60	400
C	-1	-1	40	200
D	+1	-1	60	200
E	0	0	50	300

**Table 3.** Extraction yields obtained at different temperatures and pressures for Sitka spruce needles.

Experiment	Temperature (°C)	Pressure (Bar)	Extraction Yield (%)
1	40	200	0.91
2	60	200	1.45
3	60	200	1.36
4	40	400	1.26
5	50	300	1.41
6	60	400	1.70

**Table 4. Quantification data of the most abundant compounds found in the wax extracts from spruce under various conditions.**

Compounds	scCO <sub>2</sub> extraction conditions (°C/bar)				
	40/200 (µg/g of needles)	60/200 (µg/g of needles)	50/300 (µg/g of needles)	40/400 (µg/g of needles)	60/400 (µg/g of needles)
<b>Fatty acid</b>					
C12:0	89.6 ±4.2	95.9 ±4.3	109.8 ±25.4	116 ±12.5	104.2 ±5
C14:0	157 ±5.6	157.3 ±8.2	198 ±41.5	210.9 ±24.6	203.8 ±9.9
C16:0	244.6 ±8.8	259.1 ±18.2	294.9 ±74.8	290.1 ±32	284.6 ±25.2
C18 unsat. fatty acids	175.1±11.7	181.4 ±20.3	210.3 ±68.6	196.3 ±27.7	195 ±25.4
C18:0	29.1 ±4.2	27.7 ±4.6	33.2 ±15.2	32.1 ±10.5	33.8 ±9.3
C20:0	13.8 ±1.9	11.9 ±1.7	53.7 ±36.4	11.7 ±3.9	79.9 ±20
Total Fatty acids	709.3 ±36.4	733.2 ±57.3	899.7 ±261.9	857.1 ±111.2	877.5 ±94.8
<b>Fatty alcohols</b>					
Nonacosan-10-ol	2869.8 ±249.1	8070 ±91.1	6718.6 ±1117	3225.3 ±415.8	3719.8 ±1039.2
<b>Unsaturated ketones</b>					
C <sub>28</sub> + C <sub>30</sub> Unsat. ketones	563.7 ±27	885.1 ±20.1	978.4 ±81.3	548 ±31.4	885.7 ±79.4
<b>Sterols</b>					
Beta-sitosterol	341.6 ±7.8	397.9 ±6.6	374.5 ±13	329.1 ±39.7	393 ±28.6
<b>Other compounds</b>					
Benzoic acid	42.5 ±8.3	100.2 ±16.6	65.1 ±8.5	67.1 ±28.7	80.9 ±10.3
Hydroxyacid	43.8 ±2.6	51.3 ±5.3	69.5 ±23.6	59.5 ±4.7	65.1 ±8.5
Phytol	74 ±3.1	75.3 ±2.7	65 ±7.2	67.5 ±8.4	70.3 ±3.2

**Table 5 Quantification data of the most abundant compounds found in the wax extracts from Norwegian spruce under various conditions.**

Compounds	µg/g of needles
<b>Fatty acid</b>	
C12:0	19.3 ±2.6
C14:0	222.4 ±0.8
C16:0	1377.9 ±7.8
C18 unsaturated fatty acids	3669.3 ±19.1
C18:0	156.3 ±7.9
C20:0	122.6 ±0.4
C22:0	223.8 ±0.4
Total Fatty acids	5791.3 ±39.1
<b>Fatty alcohols</b>	
Nonacosan-10-ol	3966.6 ±114.3
<b>Unsaturated ketones</b>	
C28 & C30 Unsaturated ketones	159.6 ±0.8
<b>Sterols</b>	
Beta-sitosterol	1111 ±21.1
9,19-cyclolanostan-3-ol, 24 methylene - (3β)-	703.5 ±9.4
24-Methylenecycloartan-3-one	59.6 ±1.1
Stigmastan-3,5-diene	248.3 ±12
Total steroid compounds	2122.4 ±43.6
<b>Other compounds</b>	
Borneol	97.7 ±3.5
Bornyl acetate	220 ±27.6
4-hydroxyacetophenone	419.8 ±6.3
Phytol	343.7 ±9.5
Total other compounds	

**Table 6. Contact angle measurements for the nonacosan-10-ol coatings on different materials.**

Type		Paper CA	Glass CA
Control		0°	37°
1% solution	Nonacosan-10-ol	132°	128°
20% solution	Nonacosan-10-ol	149°	-

- Supercritical extraction was employed to valorise waste spruce needles
- Nonacosan-10-ol accounted for  $8070 \pm 91.1$   $\mu\text{g/g}$  of needles
- A facile and green recrystallization process isolated 90% pure nonacosanol
- Nonacosanol demonstrated promise as a coating for porous materials
- Highly hydrophobic nonacosanol surfaces exhibited contact angles of  $149^\circ$

ACCEPTED MANUSCRIPT