

This is a repository copy of *Mechanistic study of P retention by dewatered waterworks sludges*.

White Rose Research Online URL for this paper: http://eprints.whiterose.ac.uk/103147/

Version: Accepted Version

Article:

Al-Tahmazi, T and Babatunde, AO orcid.org/0000-0003-4730-9673 (2016) Mechanistic study of P retention by dewatered waterworks sludges. Environmental Technology & Innovation, 6. pp. 38-48. ISSN 2352-1864

https://doi.org/10.1016/j.eti.2016.05.002

© 2016, Elsevier. Licensed under the Creative Commons Attribution-NonCommercial-NoDerivatives 4.0 International http://creativecommons.org/licenses/by-nc-nd/4.0/

Reuse

Items deposited in White Rose Research Online are protected by copyright, with all rights reserved unless indicated otherwise. They may be downloaded and/or printed for private study, or other acts as permitted by national copyright laws. The publisher or other rights holders may allow further reproduction and re-use of the full text version. This is indicated by the licence information on the White Rose Research Online record for the item.

Takedown

If you consider content in White Rose Research Online to be in breach of UK law, please notify us by emailing eprints@whiterose.ac.uk including the URL of the record and the reason for the withdrawal request.



eprints@whiterose.ac.uk https://eprints.whiterose.ac.uk/

1	Mechanistic study of P retention by dewatered waterworks sludges
2	T. AI-Tahmazi ^{a,b} and A.O. Babatunde ^{a,*}
3	^a Hydro-environmental Research Centre, Energy and Environment Theme,
4	Cardiff University School of Engineering, Queen's Buildings, The Parade,
5	CF24 3AA, Cardiff, Wales, UK.
6	^b College of Engineering, University of Karbala, Karbala, Iraq
7	*Corresponding author: babatundea@cardiff.ac.uk
8	

9 Abstract

Eutrophication caused by excess phosphorus (P) loading poses serious environmental risk to 10 freshwater bodies around the world. Advancing our fundamental understanding towards 11 practical reduction of this risk using novel industrial by-products as P adsorbents is the focus 12 13 of this study. The study examined the combined effect of solution chemistry and the inherent properties of a novel adsorbent (dewatered waterworks sludges) on their P retention. The 14 overall aim was to contribute to a mechanistic understanding of P retention by the sludges; 15 16 and to better understand what properties regulate their P retention. Results confirm a strong 17 but variable affinity for P by the sludges. Aluminium (AI)-based sludges generally had higher 18 total specific surface areas; and tended to have higher P sorption capacities (6.09 - 26.95 mg-19 P/g) than iron (Fe) - based sludges (5.83 -23.75 mg-P/g). In most cases, adsorption data was 20 well fitted with the Freundlich model. However, data for two of the Al-based sludges was best 21 described by the Langmuir model with very minimal leaching of AI, Calcium (Ca) and sulphate (SO₄²⁻) ions observed; indicating surface complexation via P binding into the AI hydr(oxide) as 22 23 the main mechanism for these Al-based sludges.

24

Principal component and multiple linear regression analyses revealed that the metal content (AI, Fe, Al_{oxalate} and Fe_{oxalate}) and total specific surface area components had the most significant explanation for the variance of: (i) P-uptake at different initial P concentrations; (ii) the adsorption maxima; and (iii) the Freundlich constant (K_f); (p < 0.001). Total carbon (TC), organic carbon, Ca content and exchangeable Ca components explained a significant reasonable variance in P-uptake and K_{f.} This explanation was demonstrated for the role of Ca content in chemical P precipitation mechanism; and also for exchanging TC sites on the surface of the sludges with phosphate ions via ligand exchange mechanism. Overall, giving the combined effect of intrinsic sludge properties and solution chemistry; dewatered waterworks sludges with high reactive metal content (Al and Fe), Ca and SO₄²⁻ ions, and total specific surface area would be the best choice for P retention in practical applications.

36

Keywords: adsorption capacity, aluminium sludges, dewatered waterworks sludges, ferricsludges, phosphorus

39

40 **1. Introduction**

41 Eutrophication caused by excess phosphorus (P) loading poses serious environmental risk to freshwater bodies around the world. It has now become a global environmental concern 42 particularly with waters worldwide experiencing major increases in P concentrations leading to 43 additional drinking water treatment, decreased biodiversity and loss of recreational value. For 44 example, P fluxes to oceans have increased approximately 2.8-fold since the industrial 45 revolution and over 400 coastal dead zones can be found at the mouths of rivers discharging 46 P (Diaz and Rosenberg, 2008). Surveys in the United States and the European Union (EU) 47 estimates that 78% and 65% of their coastal areas, respectively, exhibit symptoms of 48 eutrophication (Mayer et al., 2013); whilst inland waters are equally at risk. According to the 49 U.S. Environmental Protection Agency, eutrophication is the biggest overall source of 50 impairment of the nation's rivers and streams, lakes and reservoirs, and estuaries; while in the 51 52 EU, approximately 50% of all lakes have total P (TP) at levels which pose a risk of 53 eutrophication (Bogestrand, 2004). In the UK, the Technical Advisory Group has advised that 65% of England's rivers fail current P limits with lakes being more sensitive to contamination 54 55 (Wood et al., 2007).

In order to prevent eutrophication of inland and coastal waters, legislation on P discharge into 56 the surrounding environment is becoming stricter worldwide and many water companies now 57 face additional treatment requirements to reduce P in their final effluent discharges. 58 Consequently, water companies are now faced with the prospect of having to implement 59 additional treatment methods in order to supplement their traditional biological, chemical and 60 physical processes for reducing P. However, finding the best application to reduce P can be 61 challenging, particularly when low consents are required, coupled with the expectation to strive 62 63 towards recovering the P.

64

In this regards, P removal via adsorption on novel materials and by-products is gaining 65 increased attention as an environmentally friendly and cost-effective means of removing and 66 reducing P in wastewater streams, and enabling its recovery. This study focuses on one of 67 such novel by-products, dewatered waterworks sludges which is a widely available by-product 68 of drinking water purification processes; and which have been shown to be effective adsorbent 69 70 for P (Babatunde et al., 2009). However, while the sludges can retain P and therefore be used 71 as an adsorbent for P removal; there is a need to further investigate the factors that influence 72 their P retention behaviour. This is because drinking water treatment plants use different water sources and different coagulants and polyelectrolytes; and therefore, they produce sludges 73 74 with variable elemental compositions and characteristics. Whilst some studies have examined 75 the influence of either solution chemistry or physicochemical characteristics of the sludges on 76 their P retention; investigation into their combined effects over a wide range of samples from various sources has been limited. This is, however, crucial for improving our mechanistic 77 understanding of their P retention behaviour and for their effective practical use for P removal. 78 Therefore, the specific objectives of this study were: (i) to evaluate the physicochemical 79 80 properties of seventeen dewatered waterworks sludges from different sources; and together 81 with the solution chemistry effects, relate these to their P retention behaviour; (ii) to probe the

- characteristics of P retention by the dewatered waterworks sludges; and (iii) to investigate and
 determine the mechanisms involved in P retention by the sludges.
- 84

85 2. Material and Methods

86 2.1 General Physicochemical characterization

Dewatered waterworks sludges were collected from seventeen drinking water treatment works 87 located in the United Kingdom. The treatment plant locations are kept anonymous on request; 88 and samples obtained were simply labelled using a sequential alphabetic code generated from 89 the location names. To determine the chemical composition, 0.1g samples of each of the 90 sludges (air dried and ground to particle size <2mm) was digested with 3 mL of HCl and 3 mL 91 of HNO₃ in a microwave and analysed using inductively coupled plasma atomic emission 92 93 spectroscopy (ICP-AES). Chloride, sulphate and exchangeable calcium ions were determined by extraction with deionized water at a 1:10 solid:liquid ratio for 4 hours, followed by filtration 94 with 0.45 µm membrane filters. The chloride and sulphate ions were measured using lon 95 Chromatography (ICS - 2000 Ion Chromatography system) while Ca concentration was 96 97 measured using ICP-AES. Total carbon (TC) and OC were determined by Total Organic Carbon Analyzer (TOC-V CSH (Shimadzu)); pH was determined following the British 98 99 Standards institution method (British Standards Institution, 1990). The total surface area was 100 measured with the sludges in a wet condition using Ethylene Glycol Monoethyl Ether (EGME) 101 method. The method determines both the internal and external surface areas where adsorption 102 and ion exchange take place (see Cerato and Lutenegger (2002) for the measuring 103 procedure). The morphological structure of the sludges was examined by X-ray diffraction 104 (XRD); the scattering angles ranged from 2° to 80° 20 with scanning speed at 0.02° 20 per 0.5 105 second. To quantify the amorphous AI and Fe oxides of the sludges, ammonium oxalate-106 extractable AI and Fe were measured according to the method described by McKeague and 107 Day (1966).

108 2.2 Adsorption isotherm study

P sorption maxima of the dewatered water sludges was determined by equilibrating 1g each 109 of the dewatered sludges samples in 200 ml acid-washed polyethylene bottles. The bottles 110 contain 100 ml solution at three pH values (4, 7 and 9); and seven initial P concentrations (5, 111 112 10, 20, 40, 80, 160 and 320 mg-P/I). Hydrochloric acid (0.01M) and potassium hydroxide 113 (0.1M) were used for pH adjustment. Potassium dihydrogen phosphate (KH₂PO₄) was used to prepare P stock solution. After 48-hours pre-determined equilibration time, samples were 114 filtered using a 0.45µm membrane filter and analysed for P using a HACH DR-3900 115 spectrophotometer. The mass of P adsorbed per mass of adsorbent (q) in mg/g was calculated 116 117 using Eq. (1).

$$118 \qquad q_e = \frac{(c_o - c_e)}{m} V \tag{1}$$

where C_o and C_e are the initial and equilibrium P concentrations, respectively in the solution (mg/l), V represents the volume of the solution (I), and m is the mass of the adsorbent (g).

The equilibrium data was fitted with Langmuir and Freundlich isotherm models; the linearized 121 forms of which 2 122 are given below, respectively in equations and 3: $\frac{C_e}{q_e} = \frac{1}{bQ_\circ} + \frac{C_e}{Q_\circ}$ 123 (2)

124
$$\log q_e = \log K_f + \frac{1}{n} \log C_e$$
 (3)
125 where b is constant of Langmuir adsorption (L/g), Q is the maximum mass of P adsorbed at

saturation conditions per mass unit of adsorbent (mg/g); K_f is the bonding energy related constant (L/g), and n is Freundlich heterogeneity constant.

128 2.3 P retention – Mechanism and linkage with inherent properties

129 2.3.1 Exchangeable ions and Precipitation tests

In order to investigate the possible mechanism of P retention by the sludges through calcium phosphate precipitation and/or adsorption to the precipitated aluminium and iron oxides, exchangeable ions and precipitation tests were carried out. For the exchangeable ions test, the leachability of Ca, AI and Fe from the sludges was determined by shaking 1 g each of the sludge samples in 100 ml of deionized water at three initial pH solutions (4, 7 and 9), and for 48 h at room temperature. The pH at time of equilibrium was determined using a pH meter, and the samples were then filtered using 0.45 µm membrane filters. The supernatants were analysed for AI, Ca, Fe, magnesium (Mg) and P using ICP-AES; and the leached concentrations determined were used as background concentration for the precipitation test before adding P.

140 Precipitation test was then conducted to determine at which pH, and Ca and P concentrations the calcium phosphate precipitation might occur. The tests were performed in conditions 141 simulating the P adsorption experiments. Aliguots of 100 ml of deionized water were placed in 142 200 ml acid washed polyethylene bottles and then agitated with different concentration of Ca 143 144 and/or Fe (the concentration of Ca and/or Fe was determined based on the result of the exchangeable test wherein some sludges leached Ca while some leached both Ca and Fe). 145 Thereafter, pH was adjusted using hydrochloric acid (0.01M) and potassium hydroxide (0.1M), 146 147 prior to adding the P stock solution. The mixtures were then agitated on a rotary shaker for 148 48h before being filtered using 0.45 µm membrane filter and then analysed for Ca, Fe and P. Any reduction in the concentrations of Ca, Fe and P after the reaction time would indicate a 149 reaction taking place. To further probe the reaction taking place and the possible mechanism, 150 samples of the sludges before and after reaction with the P stock solution were examined using 151 152 Fourier transform infrared spectroscopy (FTIR); the spectrum was scanned from 500 to 4000 cm⁻¹. 153

154 2.3.2 Linkage with inherent properties

To identify which of the measured sludge properties gives the most explanation of variance in P retention (uptake and maximum), a multiple linear regression analysis was conducted. Pearson's correlation coefficients were computed to find out if there is high correlation between the physicochemical properties of the dewatered sludges. Due to the high correlations found between the measured physicochemical properties of the seventeen dewatered sludges, rotated principal component analysis (PCA) was performed, using Varimax rotation method, to reduce the number of predictor variables which are highly correlated (multicollinearity) from eleven single variables to three uncorrelated linearly principal components. The produced component scores were then used as predictors (independent variables) in addition to initial pH of the solution in a multiple linear regression model. P uptakes at seven initial P concentrations, P adsorption maxima and Freundlich constant were chosen as the outcome (dependent) variables.

167 IBM SPSS statistic software (version 20) was used for statistical analyses. The Shapiro-Wilk's 168 test and data visualization by histograms, normal Q-Q plots and box plots were used to assess 169 the normal distribution of the experimental data. Where data was not normally distributed, a 170 transformation was performed for data to obtain a normal distribution.

171 **3. Results and discussion**

172 **3.1 General physicochemical characterization**

The dewatered waterworks sludges had highly variable physicochemical properties (see Table 1). The main constituent of the sludges, by weight was either aluminium (0.39 - 15.2) % or iron (0.59 - 29.8) %. It was evident that the AI and Fe contents of the sludges were dependent on the primary coagulant used during the water treatment process. Ten of the sludges were Fe-based, and the rest (including one sludge which contains both AI and Fe) were AI-based. The total specific surface areas (TSSA) of the sludges ranged from 97 to 468 m²/g (see Table 1).

180 TC and organic carbon (OC) of the AI- and Fe-based sludges ranged from 53.7 to 177.4 and 53.1 to 177.4 mg/g, respectively as shown in Table 1. Also, it can be seen that there is 181 negligible difference between the TC and OC content of the sludges. This implies that the 182 content of most common inorganic carbon in the sludges; i.e. calcium carbon ate and calcium 183 184 magnesium carbonate is minimal. TC has a negative impact on the P adsorption capacity of dewatered sludges by retarding P diffusion into the micropores (Makris et al., 2005). However, 185 Yang et al. (2006) found that during the adsorption process, OC exchanges with P which 186 replaces it on the surface of the sludges, thus implying that more exchangeable OC can 187 188 enhance P retention by the sludges. In our study, it was not possible to isolate the effect of TC 189 and OC on P retention; however, results of the FTIR test shows that the carboxyl group bands was changed after the sludges reacted with P, indicating the replacement of OC with the 190 191 phosphate ions on the surface of the sludge. The XRD diffraction patterns reveal sharp diffraction characteristic (peaks) for GU, BS, HO, CA, AR, HU, SF and CF sludges; and these 192 were defined as: quartz for HO, HU and CF; graphite and iron molybdenum for GU; Lithium 193 194 phosphate and calcium manganese oxide for CA; cronusite and lavendulan for AR, graphite 195 for SF and mica and nimite-1 in addition to guartz for CF (see Table 1). Interestingly, the two mineral peaks (mica and nimite-1) of CF which is a Fe-based sludge, contain iron and 196 aluminium ions. This indicates that the iron and aluminium metals alloys are in crystalline form. 197 This might impact on the adsorption behaviour of the CF sludge via reduction of the available 198 199 reactive surfaces for P retention. In addition, two crystalline peaks of graphite from carbon for 200 GU and SF which are both AI-based sludges, would suggest reduced cation and anion ions 201 leachability from these sludges, and this could restrict the adsorption process into aluminium oxide especially for the SF sludge which has a high TC content. 202

Propert	ties	GU	BS	MO	HO	CA	WD	FO	HH	AR	OS	HU	WY	WA	BU	SF	CF	BG
AI		112.81	4.59	3.89	65.35	6.80	104.22	21.16	5.16	5.87	105.34	151.88	4.84	108.78	5.80	122.29	50.05	7.71
Ca		1.16	6.83	2.65	1.90	3.33	1.80	3.17	3.06	24.87	0.88	3.21	0.89	0.93	1.47	0.63	12.56	6.67
Fe		17.00	298.10	257.80	143.29	255.46	9.75	241.69	193.85	277.72	28.73	8.25	287.34	5.94	212.09	13.91	245.79	257.99
Р		0.24	0.61	0.39	0.65	0.29	0.70	0.43	0.44	0.35	0.60	4.78	0.77	0.68	0.61	0.47	3.19	1.70
Mg		0.66	0.47	0.20	1.38	0.43	0.44	0.25	0.81	0.28	0.79	0.97	0.23	0.57	0.31	0.20	9.15	0.47
Mn		0.33	0.94	0.79	0.57	0.45	0.29	2.32	0.37	0.52	0.40	0.66	1.28	0.43	0.17	0.42	1.55	1.27
Zn		1.02	0.19	0.40	1.71	0.09	0.47	0.09	1.85	0.08	1.71	0.12	0.16	1.22	1.74	0.84	0.28	0.50
Al _{oxa}	L D	110.12	1.14	1.85	58.63	1.02	95.28	17.36	1.36	2.99	88.26	105.51	3.46	96.02	4.67	75.68	2.62	4.14
Fe _{oxa}		13.35	143.08	149.52	2 72.41	144.48	3.68	121.33	121.38	113.63	14.42	2.52	146.37	4.64	138.48	6.96	118.09	101.10
p _{oxa}		0.22	0.23	0.24	0.34	0.28	0.28	0.23	0.30	0.21	0.27	0.69	0.34	0.30	0.25	0.28	0.24	0.52
Cl		0.11	0.22	0.16	0.16	0.21	0.24	0.30	0.33	0.59	0.11	0.22	0.27	0.14	0.22	0.56	0.76	0.48
SO ₄		0.81	4.06	6.93	3.86	7.45	1.88	4.26	4.51	6.32	1.19	2.72	8.55	0.33	2.81	0.26	0.71	0.22
тс		119.6	110.8	117.4	105.2	115.9	119.6	137.	161.9	88.62	170.6	75.21	113.7	154.4	154	177.4	53.7	144.4
OC	İ	118.9	110.8	117.4	105.2	115.9	119.1	137	161.9	88.62	170.1	74.2	113.7	154	153.6	177.4	53.1	144.4
TSSA	m²/g	364.1	203.4	186.4	414.5	219.8	468	120.3	131.9	97.02	206.9	390.4	132.3	210.1	157.2	181.8	296.3	125.2
EC	µs/cm	455.5	522.8	488.3	665.7	410.7	723.1	378	375.8	1239.3	421.3	541.5	843.4	688	828	329.2	1073.1	471.1
PH		6.26	5.47	4.48	5.49	4.09	6.27	5.49	4.55	6.64	6.05	7.06	4.3	6.31	4.75	6.13	6.99	5.89
Crystal minera	line Is	Graphite, Iron Molybdenum	Lithium boride		Quartz	Lithium phosphate, Calcium manganese oxide				Cronusite, Lavendulen		Quartz				Graphite	Quartz, Mica, Nimite- 1	

203 Table 1 Physicochemical properties of the seventeen dewatered waterworks sludges

204

205 In general, XRD patterns for the sluges showed apparent poorly ordered particle distribution of AI and Fe minerals within the AI- and Fe-based sludges (with the exception of CF); this 206 207 implies that the AI and Fe sludges are in the amorphous phases. Amorphous oxide phases are assumed to be extracted with acidified ammonium oxalate and associated with non-crystalline 208 209 phase of metal oxides. Thus, the quantity of Aloxa and Feoxa in the sludges were determined using this method. Results show that the amorphous AI and Fe oxides represent 61.9 to 97.6% 210 211 of total AI for the AI-based sludges and 39.2 to 65.3% of total Fe for the Fe-based sludges (see table 1). P uptake is strongly linked to amorphous AI and Fe concentrations and the variation 212 213 in oxalate extractable AI and Fe has been shown to account for differences in P retention by 214 dewatered waterworks sludges (Dayton and Basta, 2005; Elliott et al., 2002).

215 3.2 Adsorption isotherm study

Figure 1 shows the isotherm of P uptake by the sludges. For ease of comparison, the Al- and Fe-based sludges were grouped separately. To determine if there was any significant difference in P uptake between the sludges; a one-way ANOVA was used. The results revealed significant differences in P uptake between the sludges (p= 0.002). These findings are consistent with those of Makris et al. (2005) who studied the P sorption/desorption characteristics and kinetics for seven dewatered waterworks sludges and found that the Albased sludges had higher adsorption capacity than the Fe-based sludges.

223

224



225

Figure 1 Isotherms of P uptake by the seventeen dewatered water sludges (at initial pHs of 4, 7 and 9; t=48 hours; plots to the left and right refer to, respectively, aluminium- and iron-based sludges).

Further data analysis show that the P adsorption data was well fitted with the Freundlich model;
and that the adsorption density value for all the sludges was > 1 and ranged from 1.40 to 2.79.
For most sludges, the bonding energy related constant decreased as the adsorption density

increased, in accordance with preferential adsorption occupying surface sites in order fromstrongest to weakest binding strength (Apak, 2013).

234 P adsorption capacities obtained from the fitting of the Langmuir model (see figure 2) shows generally that sludges had variable adsorption capacities which increased with decrease initial 235 236 pH solution. This suggests that P adsorption by the sludges is favourable at acidic conditions. It should be noted that the adsorption capacities reported herein relate to the equilibrium 237 238 concentration of P in solution. Therefore, using the adsorbents at very low P concentration 239 means the process would be operating under the most unfavourable condition. To compare 240 the P adsorption capacity (as determined by the Langmuir model for those sludges with good 241 fitting); one-way ANOVA analysis was used. The results of the test showed that there was significant difference in adsorption capacities between the AI- and Fe-based sludges (P< 242 0.001). This is in agreement with Makris et al. (2005) which showed higher P adsorption 243 capacity for AI-based sludge than Fe-based sludges. Elliott et al. (2002) also reported similar 244 findings in P adsorption between AI- and Fe-based sludges. In addition, the adsorption capacity 245 is related with SSA which in turn depends on the metal oxide. Makris et al. (2004) found that 246 Al-based sludges have higher SSA than Fe-based sludges, resulting in the differences in their 247 248 adsorption capacities. In our study, higher TSSA and P adsorption capacity were found for Al-249 based sludges with the exception of SF sludge. The SF sludge has the highest carbon content (crystalline – graphite) which restricts the contact surfaces available for P retention. 250



251

Figure 2 P adsorption capacities of AI- and Fe-based sludges calculated from fitting Langmuirmodel at three initial pH solution values.

254 3.3 P retention – Mechanisms

Table 2 presents results of the exchangeable ions test. Results show that the cations 255 256 concentrations decreased as the initial solution pH increased. The pH at equilibrium was either 257 increased or decreased relative to the initial pH. This could be explained by the fact that during 258 the agitation, the hydroxyl groups on the surface of the sludge and also cations and anions (as 259 Ca, Mg, Cl-, SO₄², TOC) released into the solution influence the increase or decrease of the 260 pH from its initial value. The P released from the sludges was low across the three initial pHs. 261 This P originates from the raw water and becomes part of the structure of the dewatered sludges; and it is minimally released over time (Makris, 2004). The concentration of Ca 262 released across the three initial pHs was generally higher than that observed for the other 263 cations and ranged from 3.0 mg/l to 34.5 mg/l at initial pH 4. The amount of exchangeable Ca 264 was proportional with Ca content of the sludges with the exception of GU and SF, both of which 265 contain carbon as graphite (crystalline), resulting in low exchangeable ions. In addition, 266 significant Fe concentrations were observed for BS, CA, HH and WY sludges with 1.38; 3.73; 267 2.36 and 1.54 mg/l of Fe respectively at initial pH 4. The pHs were acidic for most of the sludges 268 269 except for AR, HU and CF which all had approximately neutral equilibrium pH. The neutral pH

- of the three sludges resulted from the combination of the initial pH and pH at equilibrium,
- 271 combined with increased Ca concentration which might then encourage calcium phosphate
- 272 precipitation (Del Bubba et al., 2003).

	pH [*] 4							pH [*] 7						рН [*] 9					
sludge	pH**	Al mg/l	Ca mg/l	Fe mg/l	Mg mg/l	P mg/l	PH**	Al mg/l	Ca mg/l	Fe mg/l	Mg mg/l	P mg/l	PH **	Al mg/l	Ca mg/l	Fe mg/l	Mg mg/l	P mg/l	
GU	5.93	0.027	4.345	0.003	0.447	0.549	6.07	0.018	3.228	0.001	0.428	0.441	6.08	0.016	2.939	0.001	0.411	0.402	
BS	5.15	0.024	13.17	1.381	1.251	0.413	5.23	0.038	11.95	1.31	1.179	0.407	5.25	0.028	11.3	1.167	1.127	0.381	
MO	4.28	0.346	6.679	0.909	0.709	0.384	4.35	0.259	6.141	0.892	0.701	0.378	4.38	0.235	6.072	0.889	0.714	0.373	
НО	5.36	0.121	11.94	0.146	0.928	0.391	5.49	0.095	11.21	0.095	0.875	0.375	5.47	0.075	10.11	0.064	0.888	0.357	
CA	4.25	0.554	12.28	3.734	1.068	0.355	4.28	0.442	11.58	3.526	1.035	0.354	4.29	0.43	11.73	3.567	1.03	0.334	
WD	5.76	0.045	7.778	0.0012	0.919	0.377	5.98	0.015	6.929	0.0011	0.92	0.353	6.11	0.017	7.299	0.001	0.911	0.352	
FO	5.35	0.032	8.923	0.035	0.724	0.402	5.52	0.031	7.541	0.068	0.72	0.395	5.53	0.029	6.494	0.086	0.593	0.379	
НН	4.93	0.319	4.596	2.363	0.594	0.382	5.05	0.222	3.138	2.161	0.425	0.376	5.06	0.291	3.707	2.619	0.488	0.366	
AR	7.33	0.033	34.50	1.081	0.524	0.388	7.41	0.021	33.88	0.959	0.504	0.379	7.42	0.007	33.21	0.612	0.5	0.375	
OS	5.37	0.072	3.955	0.009	0.704	0.38	5.74	0.028	2.709	0.008	0.601	0.371	5.75	0.027	2.822	0.0075	0.597	0.326	
HU	7.08	0.011	12.06	0.001	0.944	0.4	7.10	0.01	11.43	0.001	0.981	0.398	7.15	0.01	10.9	0.001	0.981	0.392	
WY	3.85	0.669	6.495	1.541	0.581	0.392	3.96	0.657	6.028	1.497	0.561	0.342	3.96	0.542	5.823	1.357	0.521	0.334	
WA	4.75	1.58	5.257	0.006	0.489	0.346	4.81	0.932	5.049	0.005	0.497	0.344	4.81	0.916	4.736	0.003	0.463	0.299	
BU	4.15	0.635	5.841	0.400	0.718	0.351	4.25	0.425	5.459	0.33	0.706	0.347	4.29	0.349	5.444	0.303	0.699	0.312	
SF	4.87	0.051	2.964	0.003	0.938	0.621	5.89	0.042	2.404	0.002	0.227	0.548	5.99	0.04	2.213	0.001	0.215	0.401	
CF	7.46	0.045	13.64	0.195	0.938	0.396	7.58	0.032	10.14	0.065	0.761	0.395	7.59	0.026	9.388	0.051	0.692	0.371	
BG	6.50	0.04	3.431	0.098	0.423	0.378	6.64	0.032	2.361	0.094	0.332	0.378	6.66	0.029	2.325	0.047	0.327	0.356	

Table 2 Equilibrium pH and the released concentrations of aluminium, iron, calcium, magnesium and phosphorus after agitating one gram of each sludge in 100 ml of deionized water with three initial pH values for 48 h (n=2)

^{*} initial pH solution, ^{**} pH at equilibrium time (after 48 hrs agitation)

275

Furthermore, precipitation test was conducted to determine the conditions of pH, Ca, Fe and 276 P concentrations which might cause phosphate precipitation. To decide which equilibrium pH, 277 278 and Ca and Fe concentrations across the three initial pHs should be used in the precipitation 279 test; a one-way ANOVA analysis was performed to find out if there is any significant differences 280 in these values across the initial pHs. The results showed that there was no significant 281 differences in the variation of the pH at equilibrium and the Ca and Fe concentrations (p > 0.05). 282 Thus, different samples with different pH values and Ca and Fe concentrations were used depending on the exchangeable ions test; while the P concentration values used were based 283 on the change in P uptake over the range of initial P concentrations. Results obtained (not 284 shown) indicate that no significant changes between initial and final concentration of both Ca 285 and P to precipitate calcium phosphate minerals occurred at pH less than 7.3. Whereas at pH 286 > 7.3, preliminary phosphate retention via precipitation mechanism was found at high initial P 287 concentrations. Based on the molar ratio of Ca to P (0.5), it can be proposed that monocalcium 288 289 phosphate was the precipitated metal. The formation of monocalcium phosphate metal is 290 dependent on the availability of phosphoric acid (H₃PO₄), which is one of the orthophosphate species; in addition to calcium at alkaline condition. The amount of H₃PO₄ is minimal at neutral 291 292 to alkaline pH solution, thus the calcium phosphate precipitation in this study can be considered 293 to be minimal. The P precipitation retention mechanism as calcium phosphate minerals will 294 spontaneously occur and is the dominant mechanism at pH > 8 (Khelifi et al., 2002; Søvik and Kløve, 2005). In this study, high equilibrium pH (> 7.3) was observed for AR and CF sludges, 295 both of which also have the highest Ca content (table 1) and exchangeable Ca (table 2). In 296 these conditions, P retention by calcium phosphate precipitation is minimal and P adsorption 297 298 by AI and Fe oxides are the main possible mechanisms for the AR and CF sludges.

For samples that contained Fe ions, prior to reaction with the phosphate ions; the initial Fe precipitated as iron oxides when the dissolved Fe had reacted with sodium hydroxide ions which had been added for pH adjustment. Thus the final Fe concentrations were minimal and below the limit of detection. After adding the P stock solution, the iron precipitates have the ability to adsorb phosphate ions via surface complexation mechanism through the formation ofinner sphere and/or outer sphere complexes with the iron precipitates.

The P retention mechanism was further investigated by analysing the FTIR spectra of the 305 sludges before and after reaction with the phosphate ions (see figure 3). Results reveal that 306 307 without phosphate adsorption, the FTIR spectra of the sludges had a strong hydroxyl stretching (e.g. 3200 cm⁻¹ for BS and HU) and bending (1558 cm⁻¹ for BS and HU) vibrations, which are 308 309 due to physically adsorbed water molecules; while the band at 1413 and 1386 cm⁻¹ could be 310 assigned to stretching vibration of C-O and deformation vibration of C-H for carboxyl functional groups (Izquierdo et al., 2012). Additionally, deformation vibrations of multi-centred hydroxyl 311 312 groups of iron and aluminium oxides (Fe-OH, AI-OH) of the sludges were observed at 1028 cm⁻¹ bands for the Fe-based sludge and two bands of 1066 and 977 cm⁻¹ for the Al-based 313 sludges (Zhang et al., 2007). After reaction with phosphate ions, the FTIR spectrums of the 314 sludges showed clear changes. The peaks of physically adsorbed water and stretching and 315 deformation of carboxyl groups became broad and intensive which is attributed to replacement 316 of H₂O, C-O and C-H during the phosphate adsorption. Moreover, the peaks of bending 317 vibration of multi-centred hydroxyl groups for Fe-OH and AI-OH completely disappeared, while 318 319 a new broad and intensive peak appeared at 1018 and 1004 cm-1 for Fe and Al oxides respectively. This peak could be attributed to the formation of inner sphere surface 320 complexation between phosphate ions and oxides (Persson et al., 1996); and outer sphere 321 322 surface by exchanging phosphate ions with hydroxyl group on the surface of dewatered sludge. 323 The FTIR results indicate that the surface complexation of inner and outer sphere played a key 324 role in the adsorption mechanism.



325

Figure 3 FTIR spectra of (a) Fe-based sludge and (b) Al-based sludge; before and after adsorption test with 10 mg/l initial P concentration at pH 4 and 7.

328 **3.4 P retention – Linkage with inherent properties**

The results of the principal component analysis are presented in Table 3. The properties which 329 combine in the same principal component (PC) could be identified as; PC1- metal content and 330 TSSA - related component (high loadings for AI, Fe, Aloxa, Feoxa and TSSA, total variance = 331 332 42.75%); PC2- Ca content, exchangeable Ca (Caex), TC, total organic carbon (TOC) related component (total variance = 34.56%); and PC3 - SO₄²⁻ content and sludge pH related 333 component (total variance = 16.48%). Combined, the three PCs could explain 93.8% of the 334 total variance in the physicochemical characteristics. The scores of the three PCs and initial 335 pH of the incubation solution were then used as predictors in multiple regression analysis, 336 where the outcome variable was the amount of P removed at different initial P concentrations. 337

The largest and most significant explanation in variability of P removal was found at initial P 338 concentration of 80 mg/l. When PC1 was entered first, it accounted for 52.9% of variance in P-339 uptake (p < 0.001). When PC2 was entered next into the model, an additional 4.5% significant 340 341 P removal was recorded (p < 0.05); and when PC3 and the initial pH of incubation solution 342 were entered, a 2.9% and 4.4% explanation, respectively of significant variability in P-uptake 343 (p< 0.05) was obtained. Thus the total significant variance in P-uptake in the linear regression 344 model that could be explained by these characteristics of the sludges and initial pH solution was 64.6% (p < 0.001). In the case of 160 mg/l and 320mg/l initial P concentrations, the multiple 345 linear regression analysis exhibited similar pattern, but the total explainable variance in P-346 uptake became less by excluding the effect of sulphate content and pH related component 347 (PC3). By following the same procedure for the lower initial P concentration, the total 348 explainable variance in P-uptakes by the three predictors (initial pH solution was excluded) 349 increased with increasing initial P concentration except for the P-uptake at 5 mg/l initial P 350 concentration. At 5 mg/l, PC3 and initial pH solution were not significantly linked to the P-351 352 uptake and the metal content related factor; and the Ca, Caex, TC and TOC related factor 353 combined together, explained 55.9% in the variance in P-uptake. The metal content related component (PC1) was the most significant predictor in explaining the variance in P-uptakes 354 355 across the initial P concentration.

356 The same procedure above was used to determine the physicochemical characteristics of the sludges which had the most effect on the maximum P adsorption capacity as calculated by the 357 Langmuir model. The scores of the three PCs and the initial solution pH were used as 358 predictors in multiple linear regression analysis, where the calculated P adsorption capacity 359 360 was used as the outcome variable. Combined together, PC1 and initial solution pH accounted for 44.8% significant variability of calculated P adsorption maxima, while PC2 and PC3 were 361 not significantly correlated with the P adsorption maxima. As discussed previously, the best fit 362 for adsorption data for all the sludges at the three pHs was given by Freundlich model. 363 364 Therefore, to identify which of the physicochemical properties of the sludges had the most 365 effect on the Freundlich bonding energy related parameter (K_f), the same procedure above

366	was used. The significant variances in P-uptakes and adsorption parameters explained by the
367	physicochemical properties of the sludges and initial pH solution are presented in the Table 3.
368	The metal content and TSSA related component (PC1); Ca content, exchangeable Ca, TC and
369	OC related component (PC2), and initial solution pH were significantly related to K_f Freundlich
370	parameter. A total 78.4% of variability in K_f (p < 0.001) was explained by these predictors at
371	significant levels < 0.001, < 0.01, and < 0.01 respectively.
372	
373	
374	
375	
376	
377	
378	
379	
380	
381	
382	
383	

Table 3 Principal component analysis of the physicochemical characteristics of the seventeen dewatered waterworks sludges; and linear regression analysis between the three principal components scores and initial pH solution as predictors, and amount of P-uptake at different initial P concentration, P adsorption capacity maxima and Freundlich P bonding energy related constant as outcomes variables.

Principal component	PC1	PC2	PC3	Independent	PC1	PC2	PC3	рН	TV%			
Eigenvalue	5.626	3.668	1.023	variable	Percentage of explainable variance							
Proportion of variance (%)	42.745	34.563	16.477	q ₁ ^a	45.3***	6.1 [*]	NOT Sig.	NOT Sig.	55.9***			
Cumulative proportion of variance (%)	72.745	77.308	93.785	q ₂ ^a	28.9***	9.3**	NOT Sig.	NOT Sig.	38.2***			
Rotated fac	ctor loading			Q ₃ ^a	30.8***	10.1**	6.1 [*]	NOT Sig.	46.9***			
Variable	PC1	PC2	PC3	q ₄ ^a	36.9***	8.1**	8.2**	NOT Sig.	53.2***			
AI	0.925	-0.044	0.33	q_5^{a}	52.9***	4.5 [*]	2.9*	4.4*	64.6***			
Fe	-0.918	0.255	-0.256	q ₆ ^a	46.4***	6.5**	NOT Sig.	6.9*	59.8***			
Al _{oxa}	0.953	-0.083	0.259	q ₇ ^a	42.3***	4*	NOT Sig.	9.5**	55.8***			
Fe _{oxa}	-0.881	0.168	-0.402	Q _° ^b	34.4***	NOT Sig.	NOT Sig.	10.4*	44.8***			
Ca	-0.596	0.691	0.337	K _f c	66.4***	6.2**	NOT Sig.	5.8**	78.4***			
Ca _{ex}	-0.154	0.915	-0.081	* explainable vari	ance is sign	ificant at the	0.05 level					
SO ₄ ² -	-0.419	0.271	-0.801	*** explainable var	riance is sig	nificant at the	e 0.001 level					
ТС	0.019	-0.969	0.012	^a P-uptakes rang	ed q1, q2,	q3, q4, q5, c	q6, and q7 a	t initial P con	centrations			
ТОС	0.013	-0.969	0.009	ranged 5, 10, 20, 40, 80, 160 and 320 mg/l; ^b calculated P adsorption maxima determined from fitting the linearized Langmuir model: ^c bonding energy related								
TSA	0.756	0.563	0.027	constant calculate	constant calculated from fitting the linearized Freundlich model; For the principal							
рН	0.438	0.343	0.805	component table, variable with high component loading are shown in bold								

388 **4. Conclusion**

This study aimed at contributing to practical reduction of eutrophication caused by excess 389 390 phosphorus (P) loading to the environment. Specifically, it was focused on advancing our fundamental understanding of P reduction by novel industrial by-products, using dewatered 391 drinking water treatment sludge as P adsorbent. Findings have shown that aluminium (AI) and 392 iron (Fe) based dewatered waterworks sludges have considerable variability in their 393 physicochemical properties; and the difference in their P retention behaviour can be explained 394 395 by the amount of reactive AI and Fe available, the total specific surface area, and in some 396 cases, the presence of crystalline phases of total carbon and other minerals. Al-based sludges tended to have higher total specific surface areas and thus, higher adsorption capacity. P 397 retention was shown to be generally through surface complexation, ligand exchange and/or 398 precipitation. In particular, FTIR results indicate that surface complexation of inner and outer 399 sphere played a key role in the adsorption mechanism. In almost all cases, adsorption data 400 was well described by the Freundlich model indicating the heterogeneity of P adsorption on 401 402 the surface of the sludges. However, adsorption data for two of the sludges which were Al based were best fitted with the Langmuir model, with minimal leaching of AI, Calcium and 403 sulphate ions observed. This implies that P adsorption by surface complexation is the only 404 possible mechanism for the two sludges. 405

406 Acknowledgements

407 Authors gratefully acknowledge the support of the technical staff at the Cardiff University 408 School of Engineering, in particular Mr. Jeff Rowlands. The first author would like to thank the 409 Iraqi Ministry of Higher Education and Scientific Research for financial support.

410 **References**

- Apak, R., 2013. Adsorption of heavy metal ions on soil surfaces and similar substances:
 theoretical aspects. ChemInform 44.
- Babatunde, a O., Zhao, Y.Q., Burke, a M., Morris, M. a, Hanrahan, J.P., 2009.
- 414 Characterization of aluminium-based water treatment residual for potential phosphorus 415 removal in engineered wetlands. Environ. Pollut. 157, 2830–6.

- 416 doi:10.1016/j.envpol.2009.04.016
- British Standards Institution, 1990. Methods of test for soils for civil engineering purposes
 (BS 1377). Part 2 Classif. tests.
- 419 Cerato, A.B., Lutenegger, A.J., 2002. Determination of surface area of fine-grained soils by
 420 the ethylene glycol monoethyl ether (EGME) method. Geotech. Test. J. 25, 315–321.
 421 doi:10.1520/GTJ11087J
- 422 Dayton, E. a, Basta, N.T., 2005. A Method for Determining the Phosphorus Sorption Capacity
 423 and Amorphous Aluminum of Aluminum-Based Drinking Water Treatment Residuals. J.
 424 Environ. Qual. 34, 1112. doi:10.2134/jeq2004.0230
- Del Bubba, M., Arias, C. a, Brix, H., 2003. Phosphorus adsorption maximum of sands for use
 as media in subsurface flow constructed reed beds as measured by the Langmuir
 isotherm. Water Res. 37, 3390–400. doi:10.1016/S0043-1354(03)00231-8
- Elliott, H. a, O'Connor, G. a, Lu, P., Brinton, S., 2002. Influence of water treatment residuals
 on phosphorus solubility and leaching. J. Environ. Qual. 31, 1362–1369.
 doi:10.2134/jeq2002.1362
- Goldberg, S., Johnston, C.T., 2001. Mechanisms of Arsenic Adsorption on Amorphous
 Oxides Evaluated Using Macroscopic Measurements, Vibrational Spectroscopy, and
 Surface Complexation Modeling. J. Colloid Interface Sci. 234, 204–216.
 doi:10.1006/jcis.2000.7295
- Ippolito, J. a, Barbarick, K. a, Elliott, H. a, 2011. Drinking water treatment residuals: a review
 of recent uses. J. Environ. Qual. 40, 1–12. doi:10.2134/jeq2010.0242
- Izquierdo, M., Marzal, P., Gabaldón, C., Silvetti, M., Castaldi, P., 2012. Study of the
 Interaction Mechanism in the Biosorption of Copper(II) Ions onto Posidonia oceanica
 and Peat. CLEAN Soil, Air, Water 40, 428–437. doi:10.1002/clen.201100303
- Johansson, L., Gustafsson, J.P., 2000. Phosphate removal using blast furnace slags and
 opoka-mechanisms. Water Res. 34, 259–265. doi:10.1016/S0043-1354(99)00135-9
- Khelifi, O., Kozuki, Y., Murakami, H., Kurata, K., Nishioka, M., 2002. Nutrients adsorption
 from seawater by new porous carrier made from zeolitized fly ash and slag. Mar. Pollut.
 Bull. 45, 311–315. doi:10.1016/S0025-326X(02)00107-8
- Makris, K.C., 2004. Long-Term Stability of Sorbed Phosphorus By Drinking-Water Treatment
 Residuals: Mechanisms and Implications 198p.
- Makris, K.C., El-Shall, H., Harris, W.G., O'Connor, G. a., Obreza, T. a., 2004. Intraparticle
 phosphorus diffusion in a drinking water treatment residual at room temperature. J.
 Colloid Interface Sci. 277, 417–423. doi:10.1016/j.jcis.2004.05.001
- Makris, K.C., Harris, W.G., O'Connor, G. a., Obreza, T. a., Elliott, H. a., 2005.
 Physicochemical properties related to long-term phosphorus retention by drinking-water treatment residuals. Environ. Sci. Technol. 39, 4280–4289. doi:10.1021/es0480769
- McKeague, J. a., Day, J.H., 1966. DITHIONITE- AND OXALATE-EXTRACTABLE Fe AND AI
 AS AIDS IN DIFFERENTIATING VARIOUS CLASSES OF SOILS. Can. J. Soil Sci. 46,
 13–22. doi:10.4141/cjss66-003
- 456 Persson, P., Persson, P., Nilsson, N., Nilsson, N., Sjöberg, S., Sjöberg, S., 1996. Structure

- 457 and Bonding of Orthophosphate Ions at the Iron Oxide-Aqueous Interface. J. Colloid
 458 Interface Sci. 177, 263–275. doi:10.1006/jcis.1996.0030
- 459 Søvik, a. K., Kløve, B., 2005. Phosphorus retention processes in shell sand filter systems
 460 treating municipal wastewater. Ecol. Eng. 25, 168–182.
 461 doi:10.1016/j.ecoleng.2005.04.007
- Yang, Y., Zhao, Y., Babatunde, a, Wang, L., Ren, Y., Han, Y., 2006. Characteristics and
 mechanisms of phosphate adsorption on dewatered alum sludge. Sep. Purif. Technol.
 51, 193–200. doi:10.1016/j.seppur.2006.01.013
- Zhang, G.-S., Qu, J.-H., Liu, H.-J., Liu, R.-P., Li, G.-T., 2007. Removal Mechanism of As(III)
 by a Novel Fe–Mn Binary Oxide Adsorbent: Oxidation and Sorption. Environ. Sci.
 Technol. 41, 4613–4619. doi:10.1021/es063010u

468