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Tailoring wood waste biochar as a reusable microwave absorbent for pollutant removal: Structure-property-performance relationship and iron-carbon interaction

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Abstract

This study innovated the concept in designing an efficient and reusable microwave (MW) absorbent through concurrent exploitation of carbon graphitization, oxygen functionalization, and carbothermal iron reduction underpinned by an endothermic co-pyrolysis of wood waste and low-dosage iron. A powerful MW assimilation was accomplished from nanoscale amorphous magnetic particles as well as graphitized microporous carbon-iron skeleton in the biochar composites. Relative to a weak magnetic loss derived from the iron phase, the graphitic carbon architecture with abundant surface functionalities (*i.e.*, C–O and C=O) exhibited a strong dielectric loss, which was thus prioritized as major active sites during MW reuse. The MW-absorbing biochar demonstrated a fast, robust, and durable removal of a refractory herbicide (2,4-dichlorophenoxy acetic acid) under mild MW irradiation with zero chemical input, low electricity consumption, and negligible Fe dissolution. Overall, this study will foster carbon-neutral industrial wastewater treatment and wood waste valorization.

Keywords: microwave absorption, engineered biochar, iron-biochar composite, sustainable wastewater treatment, wood waste recycling/management.

1. Introduction

There is an increasing deterioration and scarcity of water resources, caused partly by the ubiquitous distribution of toxic and resistant synthetic organic contaminants (Palansooriya et al., 2020). Future

wastewater treatment should be consistent with the global consensus on low-carbon, sustainable technology featuring energy saving and resource circulation (Kamali et al., 2021). Microwave-assisted wastewater treatment is attractive with a reduced reactor size, short reaction time, limited chemical addition, and low energy consumption (Wei et al., 2020). These advantages are primarily dependent on the design of eco-friendly microwave absorbent. The ideal microwave absorber can effectively convert electromagnetic wave radiation into thermal or other types of energy, to induce thermal activation and generation of oxidative radicals from water molecules for organics degradation (Xia et al., 2022).

Carbonaceous materials with adjustable dielectric properties and iron-based materials with strong magnetic responses are commonly used microwave absorbents (Wang et al., 2018). However, they usually display poor performance due to inferior porous architectures, high density, and easy oxidation/corrosion (Shukla, 2019). Recently, iron-carbon composites derived from high-temperature ($> 800\text{ }^{\circ}\text{C}$) calcination of iron-containing metal-organic frameworks (MOFs) have attracted intensive research interest as effective microwave absorbents (Liu et al., 2021a, 2021b). However, a plethora of fossil fuel-derived energy and chemicals were exhausted during the complicated synthesis procedures (Zhao et al., 2019). In contrast, an iron-biochar composite produced from negative-emission, economical-feasible, scalable, and renewable one-pot pyrolysis of waste forestry biomass, would be a highly advantageous substitute (Kim et al., 2020). This material can benefit from the complementary nature of the carbon and iron compositions for synchronous dielectric loss and magnetic loss to promote microwave absorption capacity.

Recent research studies have demonstrated the promising performance of iron-biochar composites as a microwave-active catalyst for organics removal from wastewater. Lv et al. (2019) produced a sludge-derived biochar by means of 650°C pyrolysis and ~20 wt.% Fe precipitation. With additional hydrogen peroxide (H₂O₂, 0.3 M), this magnetic biochar composite achieved fast degradation of bisphenol S *via* a Fenton-like reaction and maintained a stable efficiency for three cycles. Cai et al. (2020) prepared an Fe/Fe₃C@C powder through calcinating a mixture of Fe³⁺ and citric acid (molar ratio of 1:2) at 700°C. This catalyst exhibited super-fast removal of methyl orange without extra oxidant. Nevertheless, the composites were synthesized without scientific hypothesis to unravel the structure-property-performance relationships. In particular, the over-loaded Fe content (*e.g.*, > 20%) and use of citric acid dissipates valuable resource/energy and results in low reusability as well as secondary environmental contamination due to substantial Fe leaching. Overall, the available literature is limited in these critical aspects, which would restrict the practical application of microwave-assisted wastewater treatment.

This study aims to shed light on the essential microwave-absorbing properties and iron-carbon interactions in producing a tailored biochar composite as an efficient, reusable, and environmentally friendly microwave absorber that can accomplish the rapid removal of a representative refractory organic contaminants with low energy and chemical consumption. The following hypotheses were thus proposed: (i) At different pyrolysis conditions, both biochar and loaded Fe species can evolve from microwave-transparent materials to a microwave-absorbent; the composite characteristics including graphitic carbon, reduced Fe-based magnetic

particles, oxygen functional groups, defective structure, and hierarchically porous carbon-iron interfaces, would be closely related to its microwave absorption capacity. (ii) A low dosage of Fe impregnation can catalyze reformation of carbon structure during co-pyrolysis, while a high dosage of Fe would block the porous structure and detach from the biochar matrix.

By virtue of multiple advanced spectroscopic analyses, this study disseminated that sufficient MW-assisted organic removal, energy efficiency, and reusability of the composites required high MW absorption ability corresponding to dielectric and magnetic loss, which could be maximized by the formation of nano-sized amorphous magnetic particles, rich defective sites, and abundant surface functionalities on the graphitized microporous carbon-iron skeleton. These composite features were pivotal for the beneficial Fe-catalytic effects on both the carbothermal reduction of Fe speciation and carbon structure evolution during the endothermic reactions. Overall, this study could provide valuable insights into application-oriented design of biochar composites for microwave-assisted wastewater treatment.

2. Materials and Methods

2.1 Chemicals

All the chemicals used in this study were of analytical grade and solvents were of high-performance liquid chromatography (HPLC) grade. Detailed information can be found in the previous study (Sun et al., 2020).

2.2 Tailored preparation of biochar composites

A lignocellulosic waste biomass, namely oak tree sawdust with intrinsic porous structure, high lignin content, and low impurity (Jing et al., 2022), was collected from a furniture manufacturer in Wuxi (Jiangsu Province, China) and used as a precursor material without acid washing. The wood biomass was cut and crushed to pass through a 30-mesh sieve (particle size < 0.6 mm), and then oven-dried at 60 °C overnight before use. An aliquot of the wood powder (10 g) was mixed uniformly with a certain amount of $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$, giving Fe to biochar mass ratios of approximate 1, 5, and 10% (according to the biochar yield at the selected pyrolytic temperature), respectively, in 600 mL deionized water (DIW) in a ceramic container by a magnetic stirring apparatus at room temperature for 24 h. The liquid-solid mixture was then evaporated in a 105°C oven overnight. To rationally tune the porosity, graphitization level, surface functionality, and Fe speciation of the iron-biochar composites, the solid residue was ground for homogeneity and pyrolyzed in a tube furnace that was heated to four different temperatures (*i.e.*, 500, 700, 800, and 900 °C) at a ramping rate of 10 °C min⁻¹, and held for 2 h at the target temperature with continuous N₂ purging at a flowrate of 200 mL min⁻¹ (Xu et al., 2021). After cooling to ambient temperature inside the furnace through a 30-min slow air-N₂ exchange, the stabilized samples were taken out and stored in air-tight containers for further use. The obtained samples were denoted as FeXBCY, where X (X = 1, 5, and 10) and Y (Y = 500, 700, 800, and 900) represented the Fe loading ratio (%) and pyrolytic temperature (°C), respectively. The pristine biochars (denoted as BC500, BC700, BC800, and BC900) were also prepared following the same protocols above.

Detailed information about the microwave absorption ability of biochar composites was comprehensively

characterized. The analyses included vector network analyzer (Agilent, HP8722ES, USA), transmission electron microscopy coupled with energy dispersive X-ray spectroscopy (TEM-EDX) (Thermo Fisher Scientific, FEI Talos F200X, USA), X-ray diffraction (XRD) (Rigaku SmartLab, Japan), N₂ isothermal adsorption-desorption analyzer (Micromeritics, ASAP2460, USA), Micro-Raman spectroscopy (Renishaw, UK), X-ray photoelectron spectroscopy (XPS) (Thermo Fisher Nexsa, USA), Fe K-Edge X-ray absorption near-edge structure (XANES) and extended X-ray adsorption fine structure (EXAFS) spectroscopy coupled with linear combination fitting (LCF) and wavelet transformation (WT) analyses, and thermogravimetry-derivative thermogravimetry-differential scanning calorimetry (TG-DTG/DSC) (Netzsch, STA 449F3, Germany). Analytical conditions and detailed procedures can be found in the previous studies (Feng et al., 2020; Lin et al., 2007; Sun et al., 2019, 2020).

2.3 Microwave-assisted removal of organic contaminant

As one of the most widely used herbicides and possible human carcinogens, the ubiquitously detected and easily mobilized organic contaminant, 2,4-dichlorophenoxy acetic acid (2,4-D), with a high water solubility (900 mg L⁻¹), recalcitrant chemical structure, low biodegradability, and moderate toxicity, was selected as a target refractory organic contaminant (Zuanazzi et al., 2020). To initiate the reaction, 20 mg (1 g L⁻¹) of the BC or FeBC composites were transferred into 100 mL Teflon reaction vessels containing 20 mL solution of 2,4-D at an initial concentration of 100 mg L⁻¹ (a typical concentration reported in 2,4-D manufacturing wastewaters) without pH adjustment (Sun et al., 2020). The vessels were heated in a microwave (MW) reactor

(Milestone Ethos Up, Italy, 2450 MHz, maximum power of 1500 W). The reactor temperature was ramped from ambient to 90 °C within 2 min, held for 1min, and gradually cooled down to 60 °C by mechanical ventilation in the MW reactor. Constant magnetic stirring was only deployed during the temperature-holding stage, where 2,4-D was in full contact with biochar. The adopted BC/FeBC loading, reaction temperature, and duration, were comparable to previous studies on MW-assisted organic removal (Cai et al., 2020; Lv et al., 2019). After reaction, the liquid phase was filtered using a 0.45-μm mixed cellulose ester (MCE) membrane filter before measurement of 2,4-D concentration and Fe leaching. A control experiment with only MW and no BC or FeBC was also conducted. The 2,4-D adsorption by BC and FeBC was investigated at room temperature (RT) with end-over-end rotation at 50 rpm. After reaction under both MW and RT conditions, the spent samples were collected after vacuum filtration, DIW rinsing, and 60°C oven-dry overnight, and then tested for 2,4-D affinity (by solvent extraction) and reusability. The scavenger tests were implemented under both MW and RT conditions to determine *in-situ* formation of oxidative radicals. All experimental procedures were conducted at least in triplicate, and data were presented as mean values ± standard errors. Detailed information on experimental procedures and analytical parameters is available in the previous study (Sun et al., 2020).

3. Results and Discussion

3.1 Fast 2,4-D removal by the energy-efficient FeBC/MW system

The 2,4-D removal was found to depend on both the pyrolytic temperature and Fe impregnation ratio as depicted in **Fig. 1a** (and **see Supplementary Material**). The 900°C-composites displayed clearly greater 2,4-D adsorption capacities (47.6–49.3% 2,4-D removal in 1 min) than those prepared at lower temperatures (*i.e.*, 500, 700, and 800 °C), except for a comparably low efficacy (12.0%) of the Fe10BC900. This divergence might be attributed to their larger external surface area, higher graphitization level, and more oxygen-containing functional groups for improved 2,4-D removal *via* pore filling, π - π interactions, and chemisorption (Wu et al., 2021). MW irradiation notably promoted the performances (increase of 11.9–28.2% and 25.3–37.7%, respectively) of the high-temperature (*i.e.*, 800 and 900 °C) composites. In contrast, the MW-stemmed improvement was indiscernible for the other composites (**see Supplementary Material**). The low Fe dosages (*i.e.*, 1 and 5 wt.%) endowed an upward momentum, albeit with a small rise below 18.0%, in the composite performance under the MW condition. However, the highest Fe loading (*i.e.*, 10 wt.%) elicited an opposite impact on those composites. The Fe10BC800 was superior (59.9% *vs.* 16.5–34.5%) whereas the Fe10BC900 was inferior (27.7% *vs.* 74.6–85.4%) than their counterparts, respectively. The critical structure-property-performance relationships of these composites will be comprehensively scrutinized in the following sections.

After reaction under the MW condition, even an intensive solvent extraction by methanol was incapable and accomplished less than 33.1% desorption of 2,4-D from the composites (**Fig. 1b**). The particularly high 2,4-D affinity (*i.e.*, only 1.8–7.5% 2,4-D desorption) in the Fe10BC800, Fe1BC900, and Fe5BC900 might

rely on their abundant microporous structure, graphitized carbon domain, and rich O-functionality (Ordúz et al., 2021). This strong bonding unfortunately allowed no procurement of possible degradation intermediates in this study. Nevertheless, the significantly curbed MW-assisted 2,4-D removal (see Supplementary Material) by the composites in the presence of various organic scavengers (TBA, FFA, and AA), contrasting the almost unaffected performance under room temperature condition (data not shown), provided a corollary to the *in-situ* formation of oxidative radicals ($\bullet\text{OH}$, $^1\text{O}_2$, and $\text{O}_2^{\bullet-}$) under MW irradiation for 2,4-D degradation. A more comprehensive experimental-computational design (*e.g.*, full identification of 2,4-D intermediates by mass spectrometry, detection of released Cl^- in the solution, and comparison of different organic contaminants displaying variable interactions with engineered biochar) will further validate and quantify the organics degradation in the MW/Fe-biochar system in future studies.

Good energy efficiencies of the prepared FeBC composites (Fig. 1c and see Supplementary Material) further demonstrated their versatility in developing the MW-assisted wastewater treatment. Notably, the MW reactors containing the BC900, Fe1BC900, and Fe5BC900 showed multifaceted performance ameliorations in 2,4-D removal (74.6–85.4%) as well as electricity consumption (0.014–0.018 kWh/mg 2,4-D). Meanwhile, with an appreciable increase of the reactor temperature (0.4–0.7 °C), these composites intrigued a more efficient MW-to-thermal energy transformation outperforming the conventional thermal activation (Qu et al., 2022). The previous study carried out a comparative study under oil-bath heating with the same experimental setup, which showed that biochar entrapped less 2,4-D even with a much longer (1 min vs. 30 min) reaction

time, probably owing to a non-thermal (*i.e.*, “hot-spot”) effect on the biochar surface (Sun et al., 2020).

These results unequivocally indicated that this chemical-free and energy-saving FeBC/MW system would be more feasible and sustainable for treating wastewater contaminated with refractory organic herbicides than other types of advanced oxidation processes (AOPs). For instance, the previous reports included photocatalysis (*e.g.*, 92.9% removal of 1.73 mg L⁻¹ chlorotoluron in 10 min with 0.060 kWh/mg using ultraviolet radiation and 0.0253 g L⁻¹ persulfate as oxidant) (Lai et al., 2022), electrolysis (*e.g.*, 100% removal of 40 mg L⁻¹ diuron in 75 min with 0.0962 kWh/mg using the three-dimensional carbon felt/ β -PbO₂ anode and 6.1 g L⁻¹ Na₂SO₄ as electrolyte) (Rahmani et al., 2021), and ozonation (*e.g.*, 51% removal of 200 μ g L⁻¹ atrazine in 30 min with 0.160 kWh/mg by purging an ozone/oxygen gas mixture) (Liu et al., 2021c). Moreover, the variable MW performances of the composites strongly depend on their MW absorption capacities, which will be further elaborated in the following sections.

3.2 Roles of the iron and carbon phases in achieving high MW absorption

The 2D projection of MW reflection loss (RL, **Fig. 2a**) illustrated that each composite possessed an optimized MW absorption value (RL_{min}) over the frequency (f_m) range of 2–18 GHz and the thickness (d_m) range of 1–6 mm. The frequency range with an RL value below -10 dB is commonly defined as the effective absorption bandwidth (EAB) where more than 90% of electromagnetic waves can be absorbed (Cao et al., 2019). The Fe5BC900 displayed the smallest RL_{min} (-50.6 vs. -27.1–-46.8 dB) and a wide EAB (2.40 vs.

1.76–3.68 GHz) at $f_m = 11.20$ GHz with a thin d_m (2.8 vs. 2.7–5.5 mm) compared with the other composites (Fig. 2b). Thus, the Fe5BC900 (with only 4.64 wt.% Fe) had the strongest microwave absorption capacity, which could even be comparable with the magnetic nano-porous carbon nanorods prepared from the high-temperature calcination of the Fe-based MOF (40 wt.% Fe, $RL_{min} = -52.9$ dB, EAB = 4.56 GHz, $d_m = 3.5$ mm) (Wu et al., 2019). In this study, the MW absorption capacity of the biochar composites demonstrated a decreasing trend, as follows: Fe5BC900 > Fe1BC900 > BC900 > Fe10BC800 > Fe10BC900 > Fe1BC800 > Fe5BC800 > BC800. This trend is similar to the variations in their MW-assisted 2,4-D removal, energy efficiency, and reactor temperature.

The integral MW absorption capacity of the composite was closely related to the dielectric loss and magnetic loss ($\tan \delta_E$ and $\tan \delta_M$, Fig. 2c) derived from the carbon and iron compositions, respectively. For the FeBC900s, the f_m values matching their RL_{min} were shifted to a higher range (8.64–11.20 GHz, where $\tan \delta_M > \tan \delta_E$) than the BC900 (5.76 GHz, where $\tan \delta_M < \tan \delta_E$), implying that the Fe phase was the major MW absorbent. In contrast, the carbon phase largely contributed to MW absorption for the BC800, Fe1BC800, and Fe5BC800, displaying similar f_m values (5.04–5.36 GHz, where $\tan \delta_M < \tan \delta_E$). Interestingly, the Fe10BC800 demonstrated approximately equal values (0.17 and 0.24) of $\tan \delta_M$ and $\tan \delta_E$ (at $f_m = 7.12$ GHz), suggesting both the Fe and carbon phases played essential roles in its MW absorption capacity.

In general, dielectric loss depends on conduction loss and polarization loss (Liu et al., 2021a), while magnetic loss is mainly determined by natural ferromagnetic resonance (Zeng et al., 2020). The following

conjectures were raised: (i) graphitic carbon and nanoscale reduced magnetic particles facilitate electron transport to induce conduction loss; (ii) oxygen-functionality and defective structure combined with the graphitic carbon framework accumulate bound charges to produce dipolar polarization; and (iii) hierarchically porous carbon-iron interfaces with uneven charge distribution promote interfacial polarization. These assumptions were then further verified through detailed characterization of the biochar composites.

3.3 Iron induces contrasting catalytic effects on pyrolytic carbon evolution

After the designed fabrication for testing our hypothesis, FeBC composites with distinguishable surface morphologies yet similar Fe compositions were obtained according to the TEM images with EDX mapping and XRD patterns (**see Supplementary Material**). The FeBC800s presented a large amount of nano-sized (32.9–154 nm) iron-oxide particles with high crystallinity (light spots in the SAED patterns) (Nadejde et al., 2015) on the amorphous carbon domain. In contrast, the FeBC composites prepared at 900 °C illustrated that relatively sparse nanoscale (35.4–166 nm) iron-based particles in amorphous form (ring structure without light spots in the SAED patterns) (Nadejde et al., 2015) were encapsulated in the graphitized carbon (crystalline spacing $d \approx 0.250$ nm) matrix (Wan et al., 2020). The Fe speciation in all the composites consisted predominantly of magnetite (Fe_3O_4 , PDF 89-0688), as indicated by the representative peaks in the XRD patterns and calculated d (~ 0.279 nm) (Fei et al., 1999) in the HRTEM images. The high Fe loading ratio (*i.e.*, 10 wt.%) resulted in severe particle aggregation, as evidenced by the largest average crystal size (determined

by Scherrer Equation) identified in the Fe10BC800 and Fe10BC900.

Obvious variations in the composite surface area and porosity were manifested in **Fig. 3a**. In contrast to the gradually collapsed porous structure in the pristine biochars prepared over 700 °C, more micropores (S_{micro} and V_{micro} increased by 2.56–5.34 and 1.69–3.28 times, respectively) were formed after co-pyrolysis with lower dosages (1 and 5 wt.%) of Fe at 900 °C. In comparison, more macro/meso-pores (S_{ext} and V_{total} amplified by 59.4–83.0 and 24.3–30.7%, respectively) were generated under 800 °C. These observations were consistent with the previous findings that metal chlorides (*e.g.*, CuCl_2) acted as a pore-forming agent of biochar during high-temperature pyrolysis (Wan et al., 2019). By contrast, thermal treatment at lower temperatures (500 and 700 °C) or with over-loaded (10 wt.%) Fe led to blockage of the porous structure in the biochars. The underdeveloped porosity might be a cardinal prejudicial factor in the undifferentiated and mediocre 2,4-D adsorption by these above-mentioned composites (**Fig. 1 and see Supplementary Material**).

The different pyrolytic conditions exerted cynosural influences on the graphitization level and interfacial chemical behaviour of the FeBC composites, based on quantitative deconvolution of the Raman (**Fig. 3b**) and XPS (**Fig. 3c and see Supplementary Material**) spectra. With temperature increasing from 800 to 900 °C, no obvious changes in the carbon structure were observed for the pristine biochars (*i.e.*, BC800 and BC900). However, co-pyrolysis with Fe promoted beneficial carbon evolution within this temperature range. The aromatic oxygen-functionality (S) and methylene semicircle ring structures (V_L) in the FeBC800s transformed into defective large aromatic carbon structures (D) and highly ordered sp^2 -hybridized graphitic

crystallites (G) (Sun et al., 2020; Wan et al., 2019) in the FeBC900s (**Fig. 3b**). Compared with the 800°C-composites ($A_D/A_G = 0.43\text{--}0.87$, $A_D/A_{(V_R+V_L)} = 0.33\text{--}0.42$), the FeBC900s displayed higher levels of defect ($A_D/A_G = 1.00\text{--}1.09$) and graphitization ($A_D/A_{(V_R+V_L)} = 1.13\text{--}1.23$) (Wan et al., 2020).

Surprisingly, Fe loading results in deterioration of the carbon structure during the 800°C-pyrolysis. With low-dosage (1 and 5 wt.%) of Fe, about 50% D band and 30% G band in the BC800 were decomposed into V_L and S bands (**Fig. 3b and see Supplementary Material**). The resultant FeBC composites (*i.e.*, Fe1BC800 and Fe5BC800) are inferior in terms of defect level ($A_D/A_G = 0.85\text{--}0.87$ vs. 1.12) and graphitization degree ($A_D/A_{(V_R+V_L)} = 0.37\text{--}0.42$ vs. 1.21, $\pi\text{--}\pi$ transition ratios of 3.32–5.13% vs. 11.1%) than the BC800. A similar disrupted carbon structure was observed in the FeBC700s relative to the FeBC500s. A further increased Fe loading (*i.e.*, 10 wt.%) completely eradicated the V_L band, and newly formed amorphous carbon structures (V_R) and G band in the Fe10BC800, with a slightly more graphitized carbon domain detected in the HRTEM purview.

Moreover, after pyrolysis at 800 and 900 °C, Fe impregnation contributed to more abundant oxygen-functionalities in the composite surfaces (**Fig. 3c and see Supplementary Material**). The ratios of C–O and C=O increased by 5.60% and 7.80% in the Fe1BC900 and Fe10BC900, respectively, in comparison with the BC900. The FeBC800s were also more enriched (11.5–18.4% vs. 8.27%) with C=O functional groups than the BC800. Contrastingly, Fe addition at lower temperatures (*i.e.*, 500 and 700 °C) largely consumed the C–O and HO–C=O bonds in the biochars. Thus, this study underscored the importance of catalytic Fe co-pyrolysis

in reinforcing oxygen-containing groups (*i.e.*, C=O and C–O) on the biochar surface at high temperatures, which was overlooked in other relevant recurrences (Sun et al., 2019; Xu et al., 2022).

It is important to note that Fe impregnation induced intensive carbon evolution but imposed opposite catalytic effects during co-pyrolysis at high temperatures of 800 and 900 °C, respectively. In contrast to the pristine biochars, the Fe1BC900 and Fe5BC900 exhibited a hierarchically microporous skeleton, abundant nano-sized amorphous magnetic particles, a promoted defect level, an enhanced graphitization degree, and a rich O-functionality. These merits were essential for their associated MW-assisted 2,4-D removal due to the synchronously strong 2,4-D adsorption and MW absorption. However, the Fe1BC800 and Fe5BC800 demonstrated inferior performances, possibly ascribed to the annihilated carbon structure. In particular, the lowest defect as well as graphitization level ($A_D/A_G=0.85$, $A_D/A_{(VR+VL)}=0.37$, [see Supplementary Material](#)) of the Fe5BC800 were pertinent to its relatively weak MW absorption and poor 2,4-D removal (**Fig. 1**). The excessive Fe (*i.e.*, 10 wt.%) alleviated the thermal impact at 800 or 900 °C, probably due to reforming the primeval disordered carbon matrix or blocking the original graphitic porous carbon architecture, respectively. The distinctive physicochemical properties, surface morphology, porous structure, and interfacial chemical interactions were attributed to the iron-carbon interactions during the pyrolytic process.

3.4 Concurrent exploitation of carbothermal reduction of iron and catalytic reformation of carbon

LCF/WT analyses of the XANES and EXAFS spectra (**Fig. 4 and [see Supplementary Material](#)**) were

further conducted to scrutinize the Fe atoms in the FeBC composites. The LCF results (**Fig. 4a&c**) revealed that magnetite (Fe_3O_4 , PDF 89-0688) was the major (50.9–68.0%) Fe component. The WT analysis (**Fig. 4b**) showed similar first and second shell contributions for all the FeBC composites, where the weak/strong back-scattering signals appeared in the energy range of 4–6 and 5–8 \AA^{-1} , respectively, in accordance with the Fe–O and Fe–Fe scattering of magnetite (Giannetta et al., 2020; Karlsson et al., 2008). The bond distances (**Fig. 4d**) found in the first Fe–O shell (2.00–2.09 \AA) and second Fe–Fe shell (2.94–3.10/3.43–3.51 \AA) of the samples were in fair agreement with the Fe–O and Fe–Fe bond length reported for magnetite (Changela et al., 2012). Moreover, much lower fractions (19.2–26.7 and 12.8–22.4%) of wustite (FeO , PDF 74-1886) and metallic Fe (Fe^0 , PDF 88-2324) were also observed in the composites, consistent with the small representative peaks in the XRD patterns and the calculated crystalline spacing (~ 0.433 nm of FeO) (Jette and Foote, 1933) in the HRTEM images (**see Supplementary Material**).

It was evident that the 800°C-pyrolysis caused the reductive transformation of the Fe species, as the contents of Fe^0 (from 12.8 to 22.4%) and FeO (from 19.2 to 26.7%) were increased with the higher Fe loading ratios (1–10 wt.%) in the FeBC800s (**Fig. 4c**). In contrast, the FeBC900s maintained relatively constant Fe composition (*i.e.*, 17.9–19.3% Fe^0 , 22.9–24.0% FeO , and 56.7–59.2% Fe_3O_4) irrespective of the Fe dosages. Furthermore, the smallest bond distance (2.94 vs. 3.02–3.20 \AA) for the short Fe–Fe path in the Fe10BC800 implied a major aggregation of iron oxide particles on the biochar composites, which was consistent with the analyses of average crystal size (**see Supplementary Material**) and surface area (**Fig. 3a**). Compared with

the Fe1BC900, the Fe10BC900 exhibited a more extended Fe–Fe path (3.49/3.51 vs. 3.04/3.43 Å) but a more compact Fe–O path (2.02 vs. 2.09 Å), which indicated that the Fe atoms were inserted into the carbon framework, probably *via* Fe–O–C bonding (Sun et al., 2019).

The above discussion is further substantiated by evaluating the variations in weight loss and heat flow direction associated with thermal pyrolysis of the Fe-oak mixtures based on the TG/DTG/DSC analyses (**Fig. 5**). For the oak biomass without the co-existing Fe, char was formed at ~360 °C (line 4 in **Fig. 5b**). The exothermic (*i.e.*, decomposition) or endothermic (*i.e.*, carbonization) reaction occurred below or above this temperature (line 4 in **Fig. 5c**) (Li et al., 2021), respectively. The Fe-induced catalytic effect obviously lowered the required temperature for char formation (Beliy and Udoratina, 2014) to approximately 350, 320, and 270 °C (lines 1–3 in **Fig. 5b**) with increasing Fe doses of 1, 5, and 10 wt.%, respectively. At lower Fe dosages of 1 and 5 wt.%, a tangible mass decay with an upward peak similar with the pristine biomass (lines 5 & 6 in **Fig. 5b&c**) appeared at approximate 631 and 596 °C. This phenomenon might refer to the catalytic char cracking due to depolymerization and fragmentation (Rangabhashiyam and Balasubramanian, 2019), which coincided with the disrupted carbon structure in the FeBC700s rather than FeBC500s. Meanwhile, similar DSC peaks (lines 8 & 10 in **Fig. 5c**) with no detectable mass decay was noted at ~781 and ~745 °C at the Fe contents of 5 and 10 wt.%, respectively. These conditions possibly induced secondary char formation *via* repolymerization and graphitization (He et al., 2021), in agreement with the intensive carbon evolution that took place at over 800 °C. In comparison, with the same amount of Fe impregnation, downward DSC peaks

(lines 7 & 9 in **Fig. 5b&c**) with obvious mass decays emerged at ~707 and ~747 °C, implying the transformation of Fe speciation, which was also evidenced by the LCF/WT analyses (**see Supplementary Material**).

Overall, in this study, these distinctions in the Fe configuration and thermal transformation suggested that 800 °C was a critical temperature to initiate the carbothermal reduction of crystalline Fe oxides by the labile carbon. The exothermic decomposition reactions at low temperatures (illustrated as a downtrend of the DSC curves in **Fig. 5c**) involved in preparation of the Fe1BC800 and Fe5BC800 resulted in deterioration of the C structure in the biochar composites. Nevertheless, after forming the stable amorphous Fe compounds, the impregnated Fe primarily contributed to catalytic reformation of the carbon structure at high temperatures. The endothermic carbonization reactions (depicted as an uptrend of the DSC curves in **Fig. 5c**) produced the Fe5BC900 and Fe10BC900 with improved graphitization and defective level. Meanwhile, the DSC curves (**Fig. 5c**) corresponding to the Fe1BC900 (after a decline) and Fe10BC800 (before an ascendance) reached a relatively plateau phase, which possibly offered improvement in their surface functionality and graphitization level, respectively.

3.5 Composite reusability depends on preferable active sites

The reusability of the composite is critical for determining its commercial practicability. It is noteworthy that the Fe1BC900 maintained 73.2% and 64.1% of the original efficacy after 3rd and 5th use (**Fig. 6a**),

respectively, exhibiting the best reusability for 2,4-D adsorption. Under MW irradiation, the BC900 gave the most resilient performance (*i.e.*, 67.3% of the primary capacity after 3rd use, **Fig. 6b&c**). These carbonaceous materials can be regenerated through a low-temperature (at ~200 °C) thermal annealing treatment. The previous research gave evidence that this process remediated 70% of the initial efficiency in a wood waste biochar after 3rd run for 4-CH removal (Wan et al., 2021).

At ambient temperature, the FeBC composites and pristine biochars primarily consumed their graphitic C–C/C=C structure after reaction with 2,4-D *via* π - π interactions (**see Supplementary Material**). Thus, the intriguingly higher/lower 2,4-D adsorption by the Fe10BC800/Fe10BC900 aligned with the revitalized/blocked graphitized carbon domain relative to their counterparts. In addition, the Fe1BC900 preferably utilized its high-level C–O/C=O groups as active sites for chemisorption (**Fig. 6d**). Meanwhile, for the MW-assisted 2,4-D removal, the pristine biochars generally relied on the C–O functionality (**Fig. 6d**), whereas the FeBC composites preferentially expended the C–C/C=C and C=O bonds.

After reaction with the Fe1BC900 or Fe5BC900 under MW conditions for three times, a negligible fraction (< 0.3%) of Fe was leached or detached from the biochar composite. Their deconvoluted Raman spectra demonstrated a transformation from D, G, and V_R bands to S and G_R bands, accompanied with decreased values of A_D/A_G and A_D/A_(V_R+V_L+G_R) (**Fig. 6e and see Supplementary Material**). However, the XPS analysis of C1s binding state displayed a conspicuous change from C–C/C=C to C–O/C=O bonds, and this MW-triggered variation was ~3 times that under ambient condition (**Fig. 6d**). Thus, the carbon structure in the

365 Fe1BC900 and Fe5BC900 became more disordered and oxidized after MW reuse. Similar effects were
366 observed with the pristine biochars (*i.e.*, BC800 and BC900). In contrast, Fe dissolution (**Fig. 6b&c**) was
367 detected in the MW reactors when using the Fe1BC800 (1.1%), Fe5BC800 (0.4%), and Fe10BC900 (5.1%).
368 Their carbon skeleton showed no significant changes after MW reaction compared with ambient temperature
369 (**Fig. 6d&e**). Unlike all the other composites, after the first MW use, the Fe10BC800 presented a medium-
370 level Fe leaching (0.6%), a more disordered carbon matrix (V_R and G bands converted into G_R and D bands,
371 respectively), and a significant loss (17.1%) of C=O groups. Meanwhile, similar changes with the ambient
372 condition (*i.e.*, ~20% decrease in C–C/C=C) were shown after the third use.

373 Accordingly, the iron and carbon phases in the FeBC composites showed different priorities for MW
374 reaction. At the MW working frequency (*i.e.*, 2.45 GHz), owing to the prominently larger values of $\tan \delta_E$
375 than $\tan \delta_M$ for all the composites (**Fig. 2c**), the electromagnetic waves were capable of penetrating the Fe
376 layer and directly irradiating the carbon phase. The highly graphitized and hierarchically porous carbon
377 architecture of the Fe1BC900 and Fe5BC900, with a substantial MW absorption ability ($\tan \delta_E = 0.548$ and
378 0.675), which was even higher than the activated carbon (Garcia-Costa et al., 2017), would serve predominant
379 active sites. Nevertheless, the unstable and surplus Fe particles inevitably interfered microwave propagation,
380 which resulted in a lower MW performance of the Fe10BC900 with obvious Fe leaching. In comparison, for
381 the crystalline Fe_3O_4 particles, a half-metallic material where electron hopping arises between the Fe^{2+} and
382 Fe^{3+} (Shukla, 2019), might act as the chief active spots of the Fe1BC800 and Fe5BC800, because the MW

energy was marginally absorbed by their carbon domain and reflected to the Fe layer. Contrastingly, both the carbon and Fe fractions were MW-sensitive in the Fe10BC800 deploying promoted MW capture. Its slightly graphitized carbon matrix incompletely assimilated the MW irradiation, and the residual energy was taken up by the Fe components.

4. Conclusions

This study demonstrates a high-efficacy, chemical-free, and energy-saving MW-assisted removal of a prevalent herbicide by environmentally benign and reusable wood waste-derived MW absorbent. The design of high-performance biochar lies in the science-informed customization of the pyrolytic conditions (*e.g.*, Fe loading ratio and temperature). Both reductive transformation of Fe speciation and catalytic evolution of carbon matrix should be simultaneously tailored and exploited during the endothermic reactions. Overall, this application-oriented synthesis of the MW-reactive and environmentally friendly iron-biochar composites will facilitate multifaceted improvement towards sustainable wastewater treatment as well as value-added wood waste recycling.

Supplementary Material

E-supplementary data for this work can be found in the online version of the paper.

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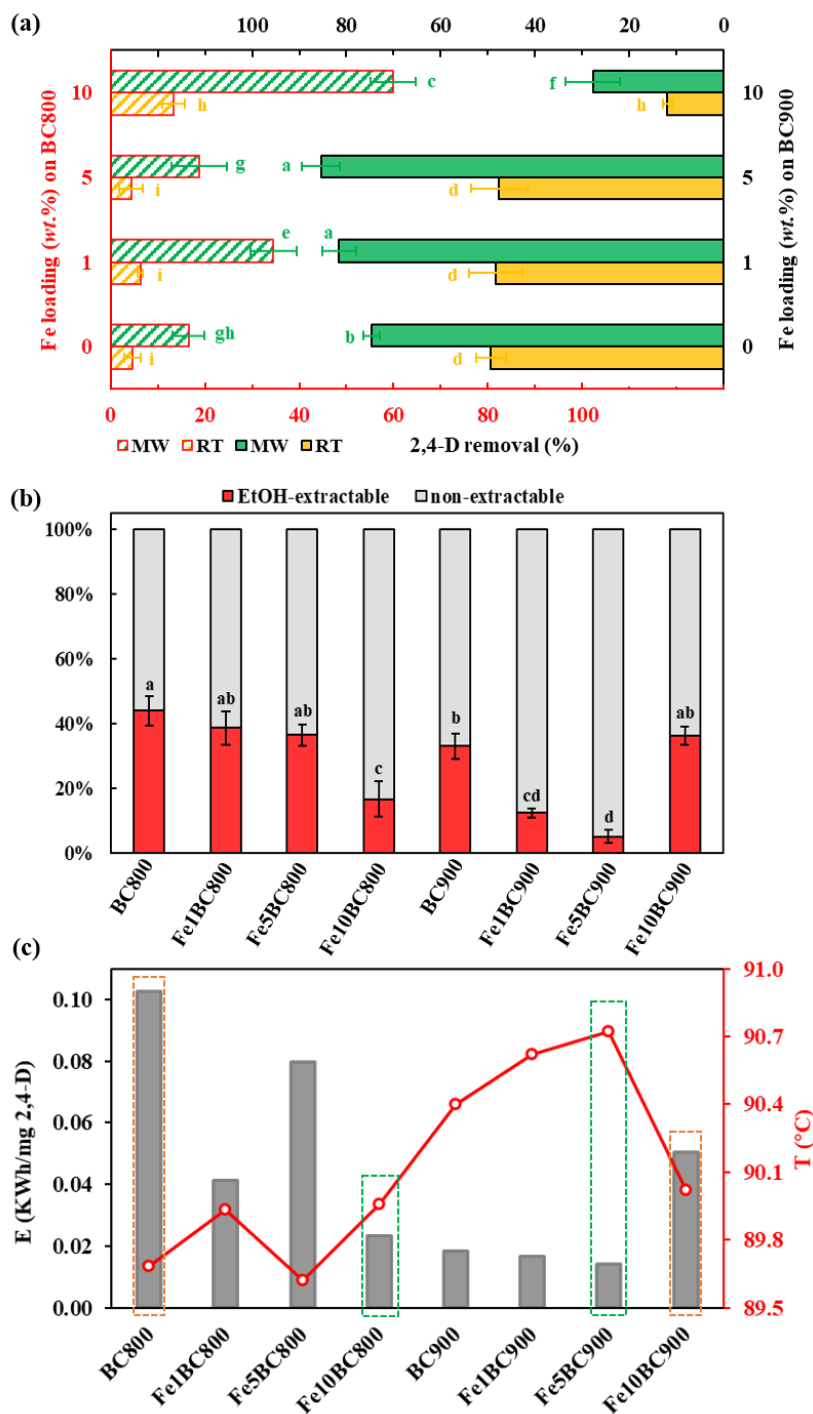


Fig. 1. Comparison of 2,4-D removal performance under room temperature (RT) and microwave (MW) conditions (a); 2,4-D affinity (based on the ethanol (EtOH) extractability after reaction) under MW condition (b); and MW energy efficiency (according to the electricity consumption and reactor temperature during 2,4-D removal) (c) of the FeBC composites (lower-case letters indicate the significance levels ($p < 0.05$) of differences).

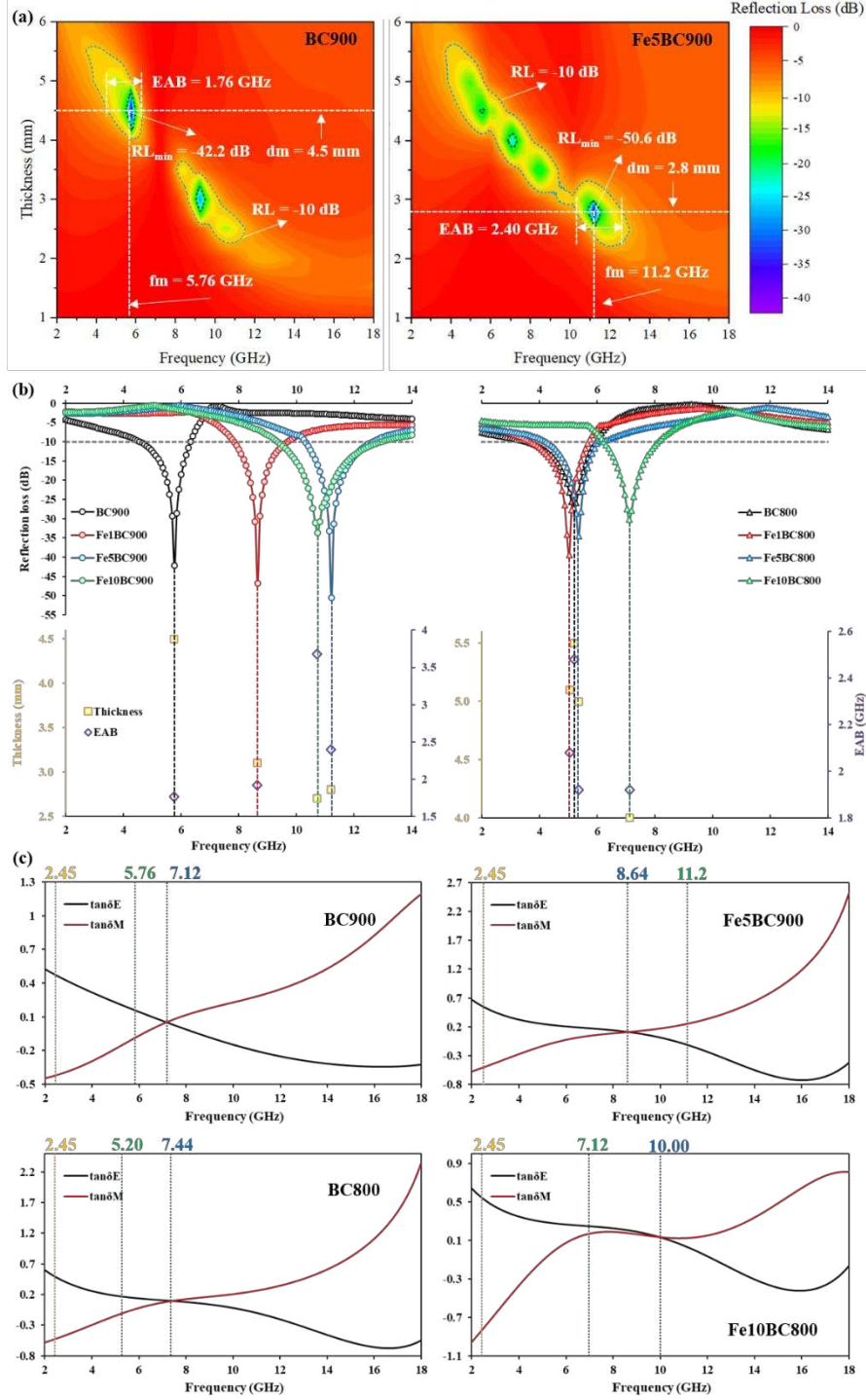


Fig. 2. Comparison of microwave (MW) absorption ability of the FeBC composites with frequency (2–18 GHz): (a) 2D projection of reflection loss (RL) values ($RL = -10$ dB, 90% MW absorption); (b) minimum reflection loss (RL_{min}) values with corresponding frequency (f_m), composite thickness (d_m), and effective absorption bandwidth (EAB); and (c) tangent magnetic loss ($\tan\delta_M$) and dielectric loss ($\tan\delta_E$) values (yellow line: working frequency of the MW reactor; green line: f_m).

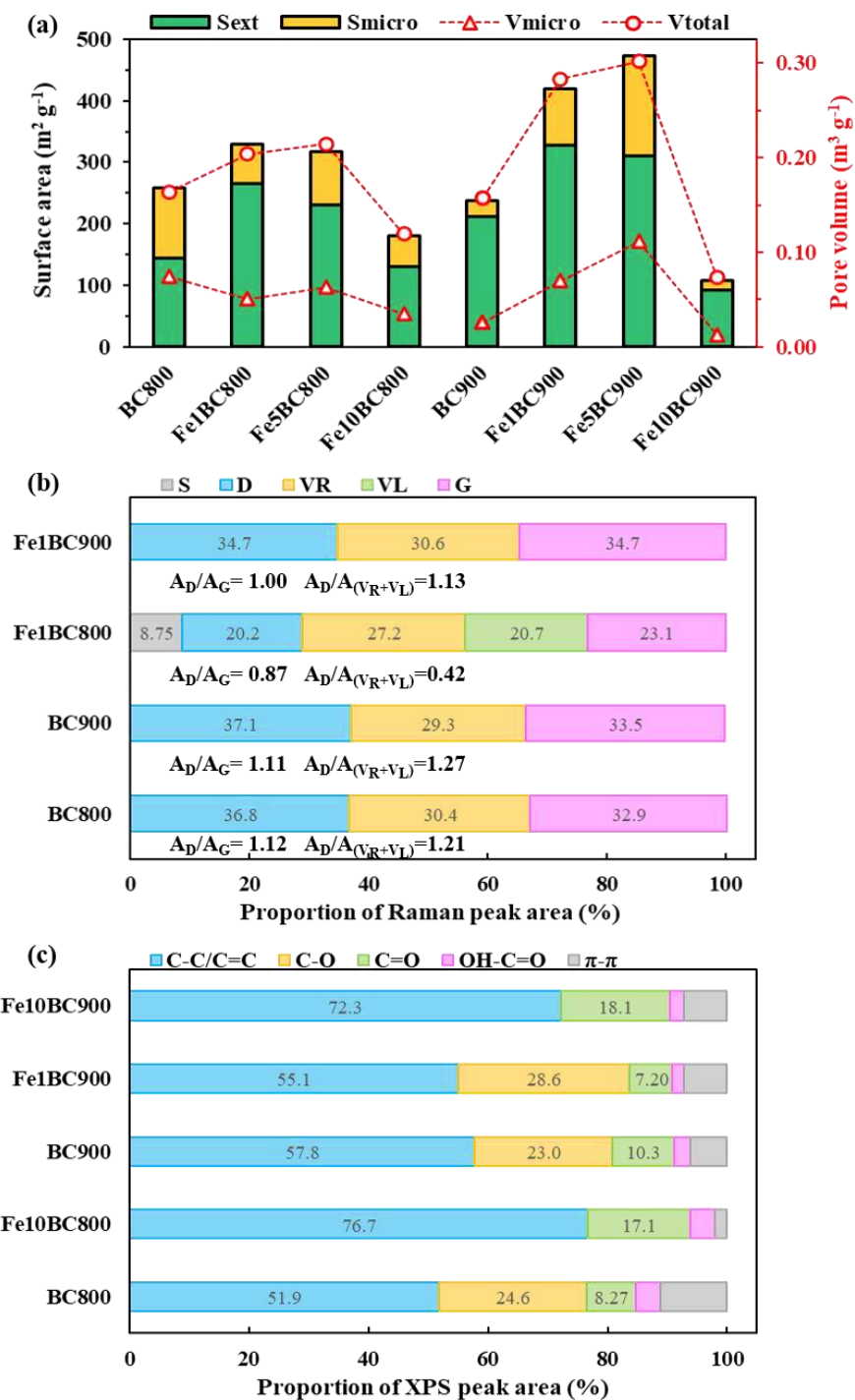


Fig. 3. Surface area and porosity (a); Raman analyses (b); and XPS results (c) for the selected FeBC composites.

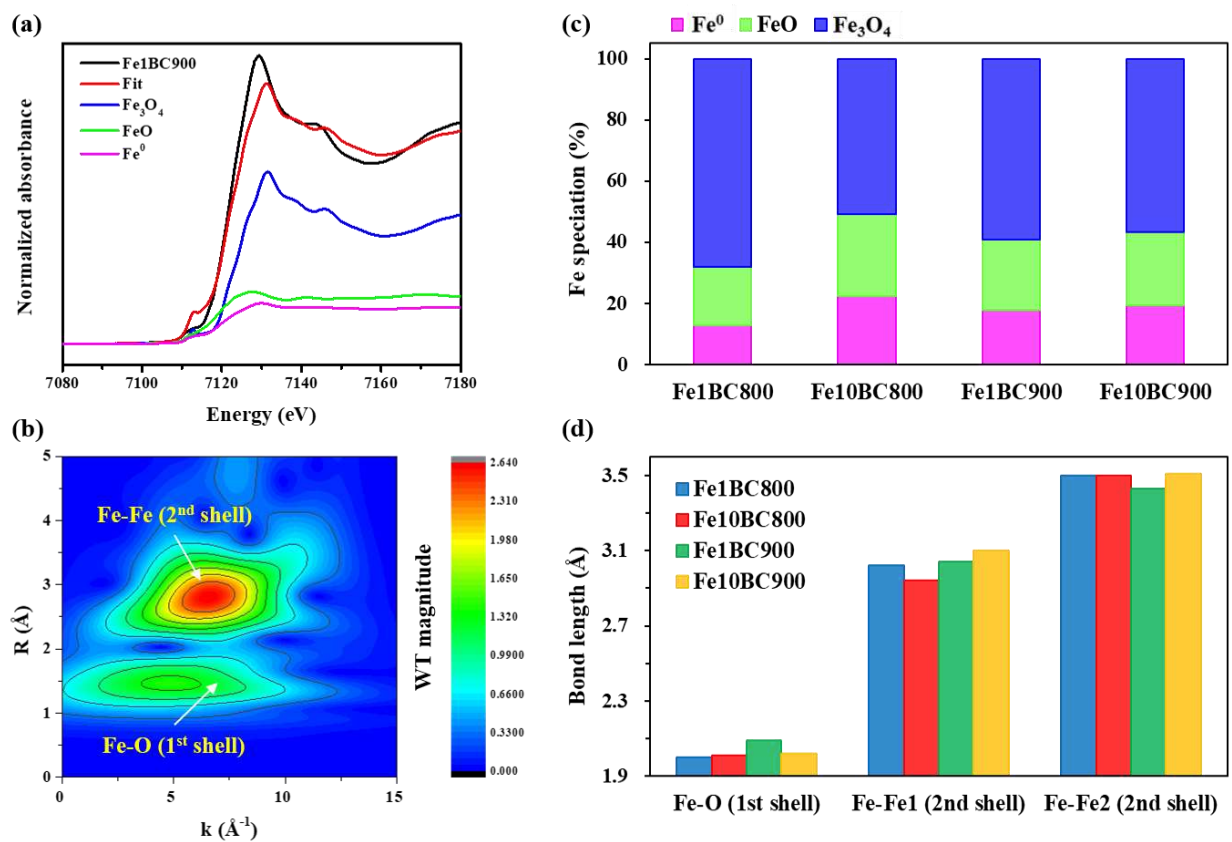


Fig. 4. Edge-step normalized Fe *K*-edge XAFS spectra (a) and high-resolution WT plot displaying the first and second coordination shells (b) of the Fe1BC900. Fe speciation (c) calculated from XANES-LCF and bond length (d) modelled from EXAFS analyses of the selected FeBC composites.

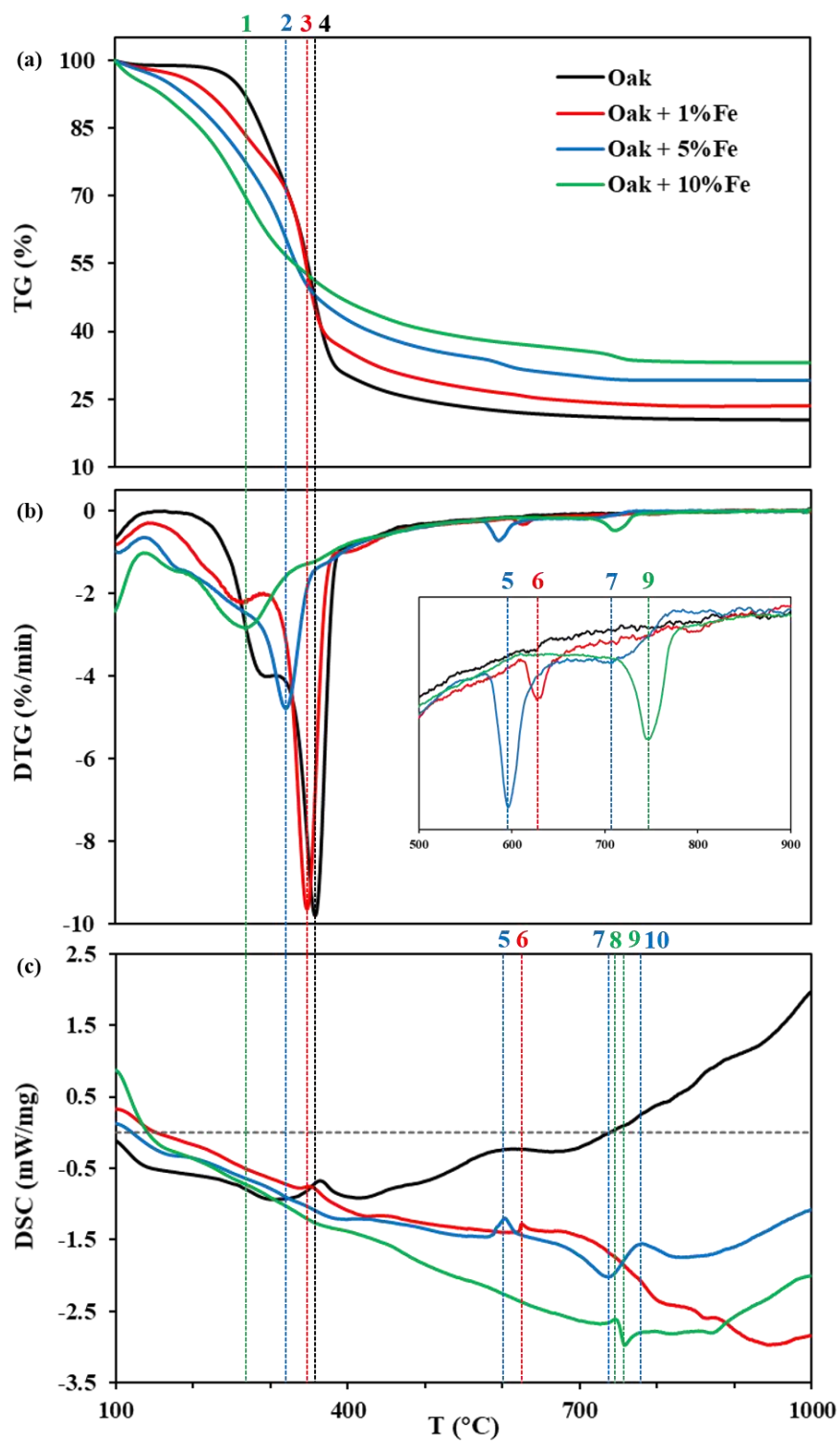


Fig. 5. TG (a); DTG (b); and DSC (c) analyses of the Fe-oak mixtures (1–4: char formation; 5 & 6: char cracking; 7 & 9: transformation of Fe speciation; 8 & 10: secondary char formation).

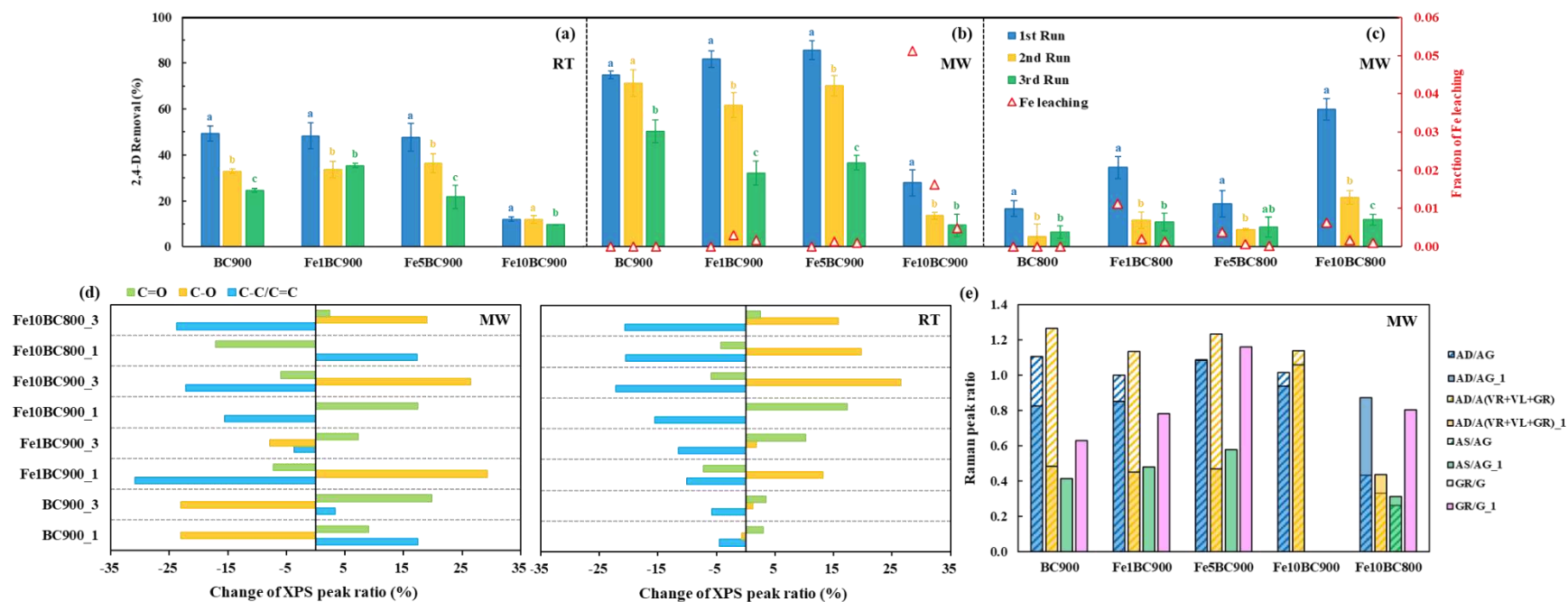


Fig. 6. Reusability of the FeBC composites under room temperature (RT) (a) and microwave (MW) (b&c) conditions. Characterization of the FeBC composites after reuse by XPS C1s (d) and Raman (e) analyses (1: after 1st use; 3: after 3rd use; the change of XPS peak ratio was relative to the previously used composite).