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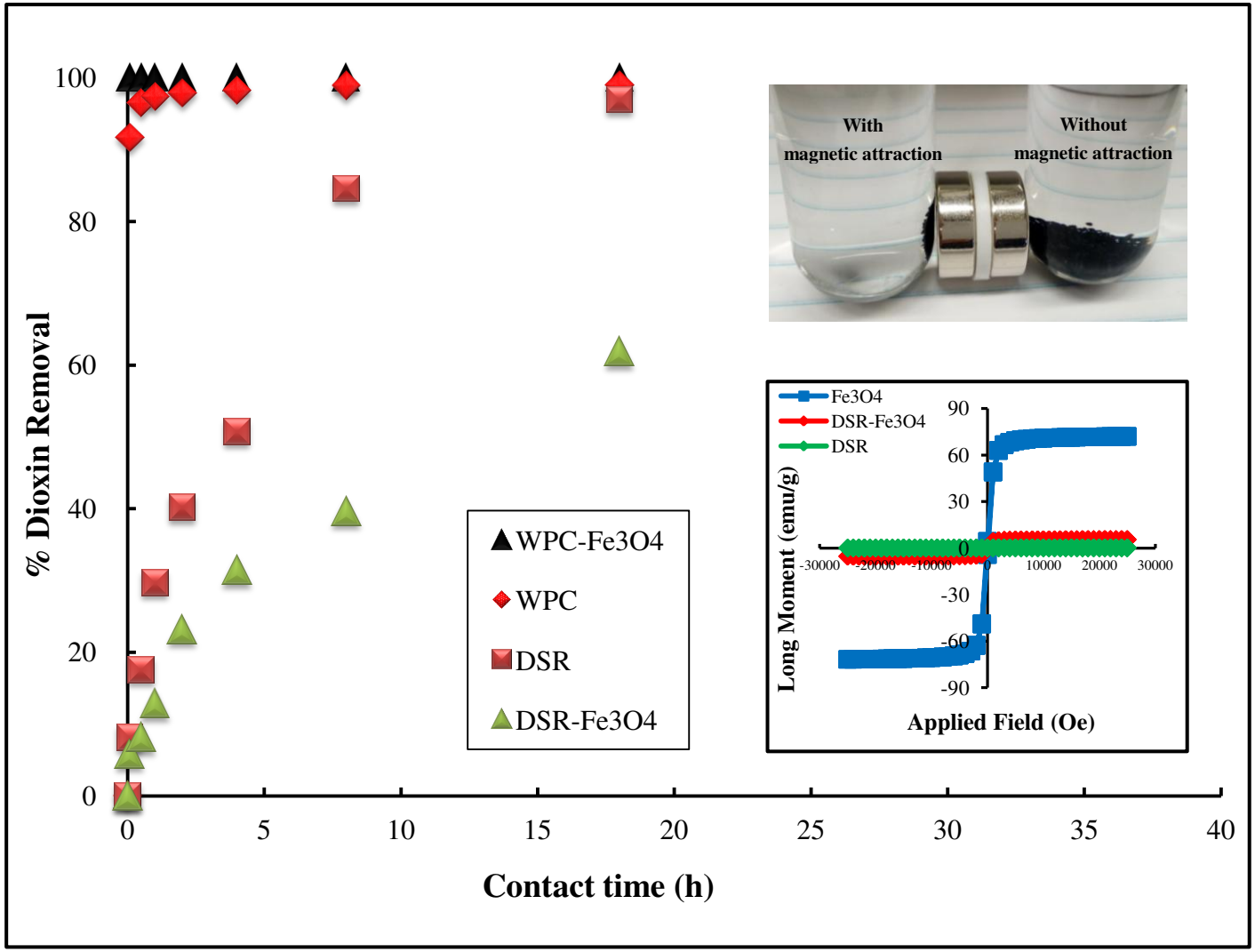
Graphical Abstract



*Title Page

Synthesis and evaluation of Fe_3O_4-impregnated activated carbon for dioxin removal

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Abstract

Polychlorinated dibenzo-p-dioxins and -furans (PCDD/PCDFs) are highly toxic organic pollutants in soils and sediments which persist over timescales that extend from decades to centuries. There is a growing need to develop effective technologies for remediating PCDD/Fs-contaminated soils and sediments to protect human and ecosystem health. The use of sorbent amendments to sequester PCDD/Fs has emerged as one promising technology. A synthesis method is described here to create a magnetic activated carbon composite (AC-Fe_3O_4) for dioxin removal and sampling that could be recovered from soils using magnetic separation. Six AC-Fe_3O_4 composites were evaluated (five granular ACs (GACs) and one fine-textured powder AC(PAC)) for their magnetization and ability to sequester dibenzo-p-dioxin (DD). Both GAC/PAC and GAC/PAC-Fe_3O_4 composites effectively removed DD from aqueous solution. The sorption affinity of DD for GAC-Fe_3O_4 was slightly reduced compared to GAC alone, which is attributed to the blocking of sorption sites. The magnetization of a GAC-Fe_3O_4 composite reached 5.38 emu/g based on SQUID results, allowing the adsorbent to be easily separated from aqueous solution using an external magnetic field. Similarly, a fine-textured PAC-Fe_3O_4 composite was synthesized with a magnetization of 9.3 emu/g.

Keywords: dibenzo-p-dioxin, granular activated carbon, Fe_3O_4, magnetic separation,

activated carbon-Fe_3O_4 composite

1. Introduction

Polychlorinated dibenzo-p-dioxins (PCDDs) are prototypical persistent organic pollutants (POPs) that are commonly found in soils and sediments. Due to their exceptionally low water solubilities, these highly toxic lipophilic substances are highly bio-accumulative (Guruge et al., 2005; Maier et al., 2016; Champoux et al., 2017). Exposure to PCDDs, even at trace concentrations (Denison et al., 1989; Eljarrat et al., 2002), can result in measurable toxic and carcinogenic effects in mammals (Huwe, 2002; McKay, 2002; Charnley and Doull, 2005). PCDDs occur both naturally and from anthropogenic activities which include forest fires, coal combustion, iron ore sintering, chlorine bleaching of pulp and paper, waste incineration, and as by-products of pesticide manufacturing and the chlor-alkali process (Fiedler, 1996; Everaert and Baeyens, 2002; Kulkarni et al., 2008; Zheng et al., 2008; Zhou et al., 2016; Prisciandaroa et al., 2017; Zhao et al., 2017). Owing to their lipophilicity, PCDD/Fs accumulate in surface soils, sediments and biota, including the fatty tissues of fish (WHO, 2010). In natural environments, they occur predominantly in the sorbed state associated with pyrogenic carbonaceous matter (PCM), amorphous organic matter, and clays (Ferrario et al., 2000; Fabietti et al., 2010). In fact, the significant role of PCM as a sorption domain has been well established (Cornelissen et al., 2005). As a group, PCDD/Fs are characterized by low aqueous solubilities and high octanol-water coefficients K_{ow} (Shiu et al., 1988; Kim et al.,

58 2002; Li et al., 2009). Consequently, their concentrations in natural waters are extremely low
59 with concentration ranges of pg/L to fg/L (Charlestra et al., 2008; Cornelissen et al., 2008b;
60 Louchouarn et al., 2018). PCDD/F-contaminated soils are found in ecosystems worldwide
61 (Masunaga et al., 2001; Moon et al., 2008; Zheng et al., 2008), and have proven difficult and
62 expensive to remediate. For example, the estimated cleanup cost of a *single* Superfund site
63 along the Passaic River which is contaminated by PCDD/Fs has exceeded one billion US
64 dollars.

65 Traditional site remediation has relied on removal of the contaminants via excavation or
66 dredging followed by disposal in a hazardous waste landfill. Recently, sorbent amendments
67 have gained attention as a means to lower or even eliminate bioavailability of soil/sediment-
68 bound contaminants (Ghosh et al., 2011; Cornelissen et al., 2012; Hale et al., 2012;
69 Cornelissen et al., 2016; Cho et al., 2017), and this has formed the basis of a new direction in
70 management of sites contaminated with PCDD/Fs (Ghosh et al., 2011). Activated carbon
71 (AC) materials (including granular activated carbon (GAC) and powdered activated carbon
72 (PAC), has emerged as an effective sorbent amendment for this purpose (Cornelissen et al.,
73 2012; Denyes et al., 2013; Gomez-Eyles et al., 2013; Balasubramani and Rifai, 2018).

74 The retrieval of the amendment with its sorbed contaminants after deployment has
75 become a priority for a number of reasons. First, complete removal of contaminants, rather
76 than just immobilization, is preferred by many environmental regulatory agencies (e.g.,

77 USEPA, 1997). Second, recovery of the sorbent amendment after its use as a passive sampler

78 can help determine mass transfer kinetics (Cornelissen et al., 2008a; Oen et al., 2011).

79 Adsorbent magnetization is an emerging remediation area where magnetic separation

80 simplifies isolation and regeneration (Mohan et al., 2014). Numerous studies have

81 demonstrated that activated carbon/Fe_3O_4 composites can be synthesized that maintain high

82 surface area and high sorption affinities for a growing list of contaminants that includes

83 organic dyes (Do et al., 2011), arsenic (Zhang et al., 2007, Zhang et al., 2010), heavy metals

84 (Han et al., 2015), pesticides and PAHs (Mohan et al., 2014). Our previous work showed

85 that magnetic Fe_3O_4 can be easily fabricated from the hydrothermal ferrite process and has

86 the potential to remove/recover toxic/precious elements from aqueous solutions (Tu et al.,

87 2012; Tu et al., 2013; Tu et al., 2015). To date, adsorbent magnetization has not been applied

88 to applications involving PCDD/Fs.

89 In our prior work, we provided the first evidence that bioavailability of TCDD sorbed to

90 two contrasting GACs and one PAC was eliminated in the mammalian (mouse) model. This

91 conclusion was based upon the use of two highly sensitive bioassays, hepatic induction of

92 cyp1A1 mRNA, an indirect measure of TCDD exposure, and immunoglobulin M antibody-

93 forming cell response, a direct measure of immune response (Boyd et al., 2017; Sallach et al.,

94 2019). Prior to this, reductions in bioavailability had only been established based on simpler

95 model organisms (e.g., worms) or passive samplers (Fagervold et al., 2010; Chai et al., 2011;

96 Chai et al., 2012). Although the ACs represented a wide range of particle size and pore size
97 distributions, they were equally effective in eliminating the bioavailability of TCDD, making
98 them viable candidates for remediation. In this study, we pursued an additional line of
99 investigation to determine if these same ACs could be functionalized using *in situ* synthesis
100 of Fe_3O_4 for subsequent magnetic retrieval (Indhu et al., 2015; Choi et al., 2016) without
101 compromising their affinity for dioxins.

102 AC-Fe_3O_4 composites were synthesized using the same GACs/PAC used in prior
103 bioavailability studies (Boyd et al., 2017; Sallach et al., 2019). The specific goals of the
104 current work were to (1) synthesize GAC/PAC-Fe_3O_4 composites using ACs shown to be
105 effective in eliminating TCDD bioavailability in mammals, with emphasis on gaining new
106 physicochemical insight into the interaction between GAC/PAC and Fe_3O_4, (2) characterize
107 the composites using a combination of X-ray diffraction (XRD), scanning electron
108 microscopy (SEM), N_2-BET and micropore analysis, and superconducting quantum
109 interference device (SQUID); and (3) evaluate sorption characteristics (kinetics and
110 equilibration) of GAC/PAC, Fe_3O_4, and the GAC/PAC-Fe_3O_4 composite for aqueous phase
111 dibenzo-p-dioxin (DD). The compound DD served as an isostructural conservative surrogate
112 for PCDD/Fs, which are important targets for sequestration using environmental geosorbents
113 due to their extreme recalcitrance in natural environments (Van Den Berg et al., 1998;
114 Sallach et al., 2019; Johnston et al., 2012).

115 **2. Materials and methods**

116 2.1. Chemicals and materials

117 All solutions were prepared with deionized water. Fe_3O_4 was synthesized from ferrous

118 sulfate $FeSO_4$ (> 99.9%, Fisher Scientific, USA) and sodium hydroxide NaOH (99.5%,

119 Fisher Scientific, USA). Dibenzo-p-dioxin (99% pure) was purchased from ChemService

120 (West Chester, PA, USA) and was used as received. All the reagents are of analytical grade

121 and used without further purification. Five GACs (DSRA, G60, FM-1, TOG-LF, and, F400)

122 and one fine textured PAC (WPC) were purchased/obtained from USEPA, Sigma Aldrich,

123 Cabot, Calgon Carbon Corp,. Selected physical properties of the six GACs/PAC are given in

124 Table 1.

125 2.2. Synthesis procedure for magnetic AC-Fe_3O_4 composites

126 The magnetic GAC/PAC-Fe_3O_4 composite synthesis followed two synthesis procedures

127 modified from our previously published method (Tu et al., 2013). Method A was performed

128 using 0.01 M $FeSO_4$ at T=338 K, pH 10, and a reaction time of 2 h. Method B was carried

129 out using 0.1 M $FeSO_4$ at T=298 K, pH 10, and the same 2 h reaction time. Briefly, one gram

130 of GAC/PAC material was dried under vacuum at room temperature for 20 h using a vacuum

131 oven (Model 280 A, Fisher Scientific, USA). Dried GAC/PAC was then immersed in 0.01 M

132 (Method A) or 0.1 M (Method B) $FeSO_4$ solution (0.5 L) and mixed continuously at room

133 temperature for 20 h. After mixing, the pH was adjusted to 10 by dropwise addition of 0.1 M

134 NaOH and then air was bubbled to the solution to initiate the reaction. The synthesis

135 reactions were carried out at 338 K (Method A) or 298 K (Method B) for 2 h while

136 maintaining the pH at 10. Finally, the resultant AC-Fe_3O_4 material was rinsed 5x with DI

137 water to remove free Fe_3O_4, and successfully magnetized GAC/PAC-Fe_3O_4 composites was

138 separated from the solution via magnet. The corresponding synthetic reaction of Fe_3O_4 can be

139 described as Eq. 1 (Tu et al., 2013).

140 $3\ Fe^{2+} + 6\ OH^- + 1/2\ O_2 \rightarrow Fe_3O_4 + 3\ H_2O$ .....(1)

141 2.3. Characterization of AC-Fe_3O_4 composite

142 The crystal phases were determined by X-ray diffraction (XRD; X'Pert Pro, Philips,

143 Netherlands) using graphite monochromatic cobalt radiation over the 2θ range 10-80°. The

144 surface morphology and particle size were examined by scanning electron microscopy (SEM;

145 Nova NanoSEM, Oxford instruments, UK). The saturation magnetization of the adsorbent

146 was measured using a Superconducting Quantum Interference Device (SQUID

147 magnetometer; MPMS-3, Quantum Design, USA) at 300 ±1 K. N_2 BET and micropore

148 analysis was conducted using a Micromeritics 3Flex Multiport Chemi/Physi/Micropore

149 Analyzer.

150 2.4. Measurement of adsorption isotherm

151 Batch adsorption experiments were conducted in duplicate using five initial aqueous DD

152 concentrations (0.18, 0.3, 0.4, 0.6 and 0.8 mg/L) prepared by a serial dilution of 800 mg/L of

153 DD methanol stock solution. The amount of methanol in the aqueous solutions was 0.1%
154 which is considered to have minimal cosolvent effects. Aqueous solutions of DD were
155 sonicated for 60 min at room temperature in a water bath sonicator prior to mixing with the
156 GAC/PAC (Branson 120, Branson Ultrasonics, Danbury, CT, USA).

157 Two and half (2.5) mg of the adsorbent (GAC, PAC, GAC-Fe_3O_4, PAC-Fe_3O_4) was
158 placed in 30 mL Corex glass tubes (Kimble, Vineland, NJ, USA) with
159 polytetrafluoroethylene (PTFE)-lined screw caps, and mixed with a 30 mL aliquot of DD in
160 aqueous solutions (methanol 0.1 %). Control samples containing the initial aqueous DD
161 solutions 0.6 and 0.8 mg/L of DD solution without AC were prepared for calibration to
162 determine the losses of DD in the batch reactor. Measured values of DD in the control
163 samples ranged from 0.58 to 0.62 mg/L and 0.78 to 0.82 mg/L for the 0.6 and 0.8 mg/L DD
164 solutions, respectively. These results indicated that loss of DD to glassware can be ignored.

165 The suspensions were sonicated for 30 sec prior to shaking at a speed of 60 rpm in a rotary
166 shaker (Glas-Col, Terre Haute, IN, USA) at room temperature for 10-48 h to achieve the
167 apparent sorption equilibrium. The supernatant and adsorbent were separated by
168 centrifugation for GAC/PAC and by external magnetic field for GAC/PAC-Fe_3O_4
169 composites. An aliquot of 1.0 mL of supernatant and DD standards (0.0, 0.18, 0.3, 0.4, 0.6
170 and 0.8 mg/L) were transferred to HPLC vials. In order to prevent any sorption of DD by
171 HPLC vials, 0.5 mL of methanol (99.9%) was added to each vial prior to the addition of the

172 supernatant. HPLC vials containing supernatant and methanol were vortexed for 30 sec using

173 a digital mini-vortexer (VWR, Radnor, PA, USA). Samples were then analyzed for DD

174 concentrations by direct injection of 50 µL into a Thermo Scientific high-performance liquid

175 chromatography (HPLC) system (Ultimate 3000) equipped with a UV detector and a 150×

176 4.60 mm 5 micron Luna 5 µm C8(2) 100 Å column (S/N 514816-4). Isocratic elution was

177 performed using a mobile phase of 80% methanol: 20% water (v/v) with a flow rate of 1.0

178 mL/min and wavelength of 223 nm for detection.

179 The amount of DD sorbed (q_e, mg/kg) was calculated as the difference between the

180 amount initially added and that remaining in the solution after equilibration (Eq. 2):

181 $$q_e = \frac{(C_o - C_e) \times V}{m_{ads}} \quad (2)$$

182 where C_o and C_e are DD concentration in liquid phase at time zero and after equilibration

183 (mg/L), respectively; V is the solution volume used in DD adsorption (L); m_{ads} is GAC/PAC

184 mass (kg).

185 2.5. Desorption

186 Following collection of the supernatant after equilibrium had been reached, the remaining

187 supernatant was carefully decanted and the solid phase was re-suspended in a 30 mL solution

188 of 25% and 99.9% methanol and water (v/v). Tubes were sonicated for 30 sec prior to

189 shaking 24 h at 60 rpm to ensure equilibrium. Then, the supernatant and adsorbent were

190 separated by either centrifugation (GAC/PAC) or external magnetic field (GAC/PAC-Fe_3O_4

191 composite). Approximately 1.5 mL aliquots of supernatant and standards of 0.18, 0.3, 0.4, 0.6

192 and 0.8 mg/L were transferred to HPLC vials for HPLC analysis. The amount of DD

193 desorbed was calculated directly from the concentration of DD present in the supernatant

194 following equation Eq. 3:

195 $$\text{Desorption efficiency} = \frac{C \times V}{X} \times 100\% \quad (3)$$

196 where C (mg/L) is the concentration of DD in the desorption solution, V (L) is the volume of

197 the desorption solution, and X (g) is the amount of DD adsorbed.

198

199 **3. Results and discussion**

200 3.1. Adsorbent characterization in GAC

201 Six activated carbon materials consisting of five granular activated carbon (GAC)

202 materials (F400, FM-1, G60, TOG-LF, and DSRA) and one fine textured powdered activated

203 carbon powder (PAC) (WPC) were functionalized with Fe_3O_4. Selected physical properties of

204 the six materials are given in Table 1. All but one of these GAC/PAC materials (DSRA)

205 were used in recent TCDD bioavailability studies and were found to be highly effective in

206 eliminating mammalian bioavailability of TCDD (Boyd et al., 2017; Sallach et al., 2019).

207 The activated carbon materials (Table 1) were functionalized using two different

208 magnetite synthesis methods. Given their large specific surface areas and micropore (0-2 nm

209 pores) volumes (Table 1), some magnetite synthesis was expected to occur in the micro- and

210 mesopores (2-50 nm pores) of the GAC/PAC, along with surface decoration of exterior

211 surfaces of the GAC/PAC particles rendering the GAC/PAC-Fe_3O_4 composites magnetic.

212 Fe_3O_4 synthesis Method A was performed at elevated temperature (338 K) using 0.01 M

213 $FeSO_4$. The resulting magnetization of the PAC-Fe_3O_4 composite was successful with a value

214 of 9.7 emu/g (Table 1). In contract, observed magnetization values measured at 300 K for the

215 five GACs were weak with values of 0.61 (DSRA), 0.54 (FM-1), 0.49 (TOG-LF), 0.46 (G60)

216 and 0.35 (F-400) emu/g (Table 1). For comparison, the magnetization of Fe_3O_4 synthesized

217 using Synthesis Method A without GAC/PAC was 71.9 emu/g. Weak magnetization values

218 in the ranged of 0.35-0.61 emu/g were not sufficient to allow rapid magnetic separation.

219 Because the magnetization values resulting from synthesis Method A for the granular

220 activated carbon samples were weak (0.35-0.61 emu/g), the Fe_3O_4 synthesis procedure was

221 modified using synthesis Method B, which utilized a higher concentration of $FeSO_4$ (0.1 M)

222 and a lower temperature of 298 K. The granular activated carbon sample DSRA was selected

223 because it showed the highest level of magnetization among the five GAC materials

224 evaluated using Method A (Table 1). Synthesis Method B resulted in a DSRA-Fe_3O_4

225 composite with a significantly improved magnetization value of 5.38 emu/g (Table 1). No

226 residual magnetism was detected in either of the GAC(DSRA)-Fe_3O_4 (Synthesis Method B)

227 or PAC(WPC)/Fe_3O_4 (Synthesis Method A) composites indicating that these two materials

228 are superparamagnetic (Table 1). For simplicity, the GAC(DSRA)-Fe_3O_4 complex (using

229 Synthesis Method B) will be referred to as GAC-Fe_3O_4(B) and the PAC(WPC)-Fe_3O_4

230 complex (using Synthesis Method A) will be referred to as PAC-Fe_3O_4(A), where (A) and

231 (B) refer to Synthesis Methods A and B, respectively.

232 The GAC-Fe_3O_4(B) composite in aqueous suspension was efficiently recovered by

233 applying an external magnetic field. The complete (~100%) separation of the GAC-Fe_3O_4(B)

234 composite from solution using a magnet was achieved within only 20 seconds (Supplemental

235 Information Fig. S1). When the external magnetic field was removed, the GAC-Fe_3O_4(B)

236 composite could be readily dispersed again in water by physical shaking.

237 The XRD patterns of the GAC-Fe_3O_4(B) and PAC-Fe_3O_4(A) composites are shown in

238 Fig. 2. The observed diffraction peaks at d-spacings of 4.846, 2.968, 2.531, 2.423, 2.099,

239 1.713, 1.615, and 1.484 Å matched the XRD reflections of Fe_3O_4 (JCPDS file number 04-

240 007-9093). No other peaks were detected in the XRD pattern of the GAC-Fe_3O_4(B)

241 confirming that the only crystalline phase present is Fe_3O_4 nanoparticles in the GAC-

242 Fe_3O_4(B) composite. In addition to the Fe_3O_4 peaks, the PAC-Fe_3O_4(A) composite had small

243 peaks at 24.2, 31.0 and 58.5 °2θ.

244 Further characterization of the GAC and the GAC-Fe_3O_4(B) composite was provided by

245 SEM imaging of the two materials at different levels of magnification (Figs. 3a-3f). The

246 average bulk size of the GAC was ~1 mm with <5% passing through a 40 US Mesh sieve

247 (420 μm) (Fig. 3a); 'large' pores were observed ranging in size from several μm to >10 μm

248 (Figs. 3b and 3c). The synthesized Fe_3O_4 particles were observed to be spherical, and their

249 primary particle size ranged between 20 and 120 nm (Fig. 3d). From the SEM images it is

250 evident that the synthesized Fe_3O_4 nanoparticles were randomly distributed on the surfaces

251 and pores of the GAC particles (Fig. 3f).

252 3.2 N_2 BET and Textural Analysis

253 N_2 BET and micro-textural analysis of the activated carbon materials prior to magnetite

254 synthesis are presented in Table 1. The supplier of the activated carbon, feedstock, along with

255 N_2 BET surface area and micropore analysis are presented in Table 1. The five granular

256 activated carbon samples ranged in percentage micropore (0-2 nm) volume from 29 to 82%

257 of the total micropore and mesopore (2-50 nm) volume. The fine textured WPC powder had

258 very little mesoporosity with 91% of its pore volume in the micropore range. Of the six

259 samples, five were used in prior toxicology studies to assess TCDD bioavailability (Boyd et

260 al., 2017; Sallach et al., 2019). Although these ACs represented a wide range of particle size

261 and pore size distributions, they were equally effective in eliminating the bioavailability of

262 TCDD, making them viable candidates for remediation. After Fe_3O_4 synthesis, the specific

263 surface area of the GAC(DSRA)-Fe_3O_4 composite decreased from 822 to 633 m^2/g along

264 with a modest reduction in micropore volume (0.388 to 0.262 g/cc) indicative of some partial

265 pore blocking by the magnetite particles (Table 1).

266 3.3. Batch equilibrium sorption and kinetics

267 Batch sorption isotherms of dibenzo-p-dioxin (DD) to GAC and GAC-Fe_3O_4(B) are
268 shown in Fig. 4. Both GAC and GAC-Fe_3O_4 composite showed a high affinity for aqueous
269 phase DD at low equilibrium concentrations (<0.005 mg/L) up to a sorbed concentration
270 about of about 4000 mg/kg. At higher equilibrium concentrations (0.005-0.12 mg/L), sorption
271 isotherms showed some nonlinear behavior exhibiting high affinity at low equilibrium
272 concentration followed by an "S-shaped" response (Giles and Smith, 1974). The GAC-
273 Fe_3O_4(B) isotherm is shifted to higher equilibrium concentrations (i.e., lower affinity)
274 compared the GAC, however, both materials sorbed > 8000 mg/kg. These results could be
275 explained by sorption processes involving easily accessible external sites and less accessible
276 pores. Since Fe_3O_4 demonstrated no sorption affinity for DD, its presence within the GAC
277 composite likely blocked some sorption sites or access to certain pores manifesting a slight
278 decrease in DD affinity.

279 The kinetics of DD sorption by GAC and GAC-Fe_3O_4 composite were evaluated over a
280 period of 40 h using the batch equilibration method (described above) with initial aqueous
281 phase DD concentrations of 0.18, 0.4, and 0.8 mg/L (Fig. 5). Sorption kinetics of DD can be
282 separated into two phases. Initially, within the first 10 h, both GAC and GAC-Fe_3O_4
283 demonstrated comparatively rapid uptake of DD for all three initial concentrations. This was
284 followed by a slower phase (>50 h) to reach apparent equilibrium.

285 For the lower and intermediate initial DD concentrations of 0.18 and 0.4 mg/L, DD
286 uptake from aqueous solution by GAC was rapid and nearly complete within the first 10 h;
287 the percent DD removal approached 100 percent (Fig 5c-f). However, at the higher initial DD
288 concentration of 0.8 mg/L, there is a more gradual approach to apparent equilibrium over
289 time (Fig. 5a-b). For the initial concentrations of 0.18 and 0.4 mg/L, DD adsorption by GAC
290 was essentially complete by 10 h, and the total uptake of DD from aqueous solution
291 approached 100 percent. For the initial concentration of 0.8 mg/L the data indicate that
292 equilibrium had not been achieved after 50 h for GAC-Fe_3O_4.
293 For this system, it is assumed that sorption kinetics are controlled surface adsorption with
294 associated resistance to film diffusion followed by an emerging contribution to DD sorption
295 via intraparticle diffusion. Pseudo-second order kinetic models are commonly used to
296 describe sorption kinetics for these types of interactions (Ho and, McKay, 1999;
297 Amarasinghe and Williams, 2007). The pseudo-second order kinetic model was able to fit
298 the experimental data well (see Table 2). The pseudo-second order model results are plotted
299 on the kinetics data shown in Fig. 5.

300 The correlation coefficients (R^2) and kinetic parameters derived from the pseudo-second
301 order models are summarized in Table 2. These results suggest that the rate-limiting step may
302 be some type of site-specific mechanism involving direct interaction between the sorbent and
303 sorbate (Amarasinghe and Williams, 2007). The kinetic rate constant (k_2) from the pseudo-

304 second order model decreased with increasing initial DD concentrations (Table 1), indicating
305 that the DD adsorption rates are faster at lower concentrations. In other words, the time
306 required to reach equilibrium increased as the initial DD concentration increased. This is
307 likely due to competition for active surface sites and pores of the sorbent which is greater at a
308 higher DD concentration.

309 3.4 Desorption of DD

310 Desorption of DD into solutions of either 25% or 99.9% methanol and water (v/v)
311 desorption solutions were used to evaluate the reversibility of DD sequestration by GAC and
312 the GAC-Fe_3O_4 composite. Desorption of DD from GAC and GAC-Fe_3O_4 in 99.9% methanol
313 was 19% and 14.3% (after 20 h), respectively, and 11.2% and 12.4% for 25%
314 methanol/water, respectively. These results agree with our prior study that showed 22-27%
315 of TCDD bound to three of the activated carbons samples used in the present study could be
316 desorbed after 64 hours of Soxhlet extraction using toluene (Sallach et et., 2019).
317 Magnetizing GAC with Fe_3O_4 had little to no effect on the propensity of DD to desorb. That
318 the fraction of released DD was less than 20% even for 99.9% methanol clearly indicated the
319 strong affinity between DD and GAC; once sorbed DD appears to be largely irreversibly-
320 sequestered within the pore structure of GAC. The resistance to desorption, even into
321 methanol, is consistent with our prior observation that sequestration of 2,3,7,8-TCDD by AC
322 eliminated its mammalian bioavailability (Boyd et al., 2017; Stedtfeld et al., 2017).

323 3.5 Sorption removal comparison of fine-textured AC-Fe_3O_4 to GAC-Fe_3O_4

324 The uptake of DD by GAC, GAC-DSR-Fe_3O_4(B), PAC and PAC-Fe_3O_4(A) as a function
325 of time are shown in Fig. 6. As expected, uptake of DD by the fine-textured AC (WPC) was
326 rapid and nearly stoichiometric. More than 90% of the WPC has a particle size of < 45 μm
327 (Sallach et al., 2019). In contrast, sorption kinetics for DD uptake by the coarse-textured
328 GAC and GAC-Fe_3O_4(B) were considerably slower. Although the surface area of the PAC,
329 GAC and their Fe_3O_4 derivatives are comparable, most of the surface area in GAC can only
330 be accessed through intraparticle diffusion, resulting in slower sorption kinetics (Figs. 5-6).

331 **4. Discussion**

332 The activated carbon materials, including GAC and PAC, used here to form the magnetic
333 variants were also used in our prior bioavailability studies (Boyd et al., 2017; Stedtfeld et al.,
334 2017; Sallach et al., 2019), along with natural geosorbents including clay minerals and silica
335 (Boyd et al., 2011; Kaplan et al., 2011; Chai et al., 2016). Among these, only GAC and PAC
336 eliminated the bioavailability of sorbed TCDD to a mammalian (mouse) model.
337 Mammalian bioavailability was evaluated in our prior work using two highly sensitive
338 bioassays, hepatic induction of cyp1A1 mRNA, an indirect measure of TCDD exposure, and
339 immunoglobulin M antibody-forming cell response, a direct measure of immune response
340 (Boyd et al., 2017; Sallach et al., 2019). In contrast to the complete elimination of TCDD
341 bioavailability achieved via sequestration by GAC/PAC, TCDD bound to clay minerals and

342 silica was found to be 100% bioavailable. The lack of mammalian bioavailability of TCDD
343 bound to GAC/PACs was consistent with a related study showing contaminant bioavailability
344 to lower organisms was significantly decreased in the presence of AC (Chai et al., 2012). In
345 addition, attempts to extract sorbed TCDD from ACs using Soxhlet extraction revealed that
346 only a minor fraction of the total TCDD present could be recovered (Sallach et al., 2019).
347 From an applied perspective, these laboratory results are now leading to the use of GAC/PAC
348 sorbent amendments in large-scale remediation efforts for impacted soils, sediments and
349 water bodies (Samuelsson et al., 2017; Payne et al., 2019; Cornelissen et al., 2016;
350 Beckingham et al., 2011). Given our earlier results showing elimination of mammalian
351 TCDD bioavailability, creating magnetic GAC/PAC composites that could be used as a
352 retrievable form of GAC/PAC sorbent amendments was attempted. The ability to retrieve
353 magnetized GAC/PAC would enhance their utility as passive samplers in field settings and in
354 ongoing laboratory studies. For example, our earlier mammalian studies would have
355 benefited from using a magnetic AC to determine the amount TCDD in fecal pellets from
356 mice that were dosed with TCDD–AC (Boyd et al., 2017; Stedfeldt et al., 2017; Sallach et al.,
357 2018). Likewise, the ability to ultimately retrieve (magnetized) GAC/PAC sorbent
358 amendments used to remediate areas with especially high levels of contamination would
359 provide both an immediate benefit, i.e., bioavailability reduction, and make contaminant
360 removal possible in the longer term.

361 The synthesis procedure using a lower concentration of $FeSO_4$ (0.01 M) at an elevated
362 temperature (338 K), Synthesis Method A, was successful in synthesizing a magnetic PAC-
363 Fe_3O_4 composite (PAC-Fe_3O_4(A)). In the case of the PAC, magnetization most likely
364 occurs on the external surfaces of fine-textured AC and this could be accomplished using the
365 lower concentration of $FeSO_4$. However, Method A only produced weak magnetization
366 values for the GAC-Fe_3O_4 composites. One could argue that this procedure was not able to
367 synthesize Fe_3O_4 particles within the coarse textured GACs. The procedure was modified
368 using a higher concentration of $FeSO_4$ (0.1 M) and lower temperature that resulted in a
369 sufficiently magnetic GAC-Fe_3O_4(B) composite.

370 Both the GAC-Fe_3O_4(B) and PAC-Fe_3O_4(A) composites revealed the presence of Fe_3O_4
371 based on X-ray diffraction analysis (Fig. 2) and it is possible that careful XRD studies could
372 be used as a surrogate for the more difficult to obtain SQUID magnetization results. N_2 BET
373 surface area and textural analysis showed that both the GAC and PAC materials were
374 characterized by high N_2-surface area (802-822 m^2/g). The specific surface area of the
375 GAC-Fe_3O_4(B) composite showed a modest reduction in both surface area (822 to 633 m^2/g)
376 and micropore volume (0.38 g/cc to 0.26 g/cc) compared to the starting GAC (Table 1).
377 The batch sorption isotherms of dibenzo-p-dioxin (DD) on the GAC and GAC-Fe_3O_4(B)
378 composites showed that sorption affinity of DD was slightly reduced due to the presence of
379 magnetite particles (GAC-Fe_3O_4(B)) compared GAC. The decrease in surface area and DD

380 sorption is interpreted as some blocking of pore throats. Overall, the sorption isotherms for
381 both GAC and GAC-Fe_3O_4(B) showed some sorption nonlinearity, consistent with a range of
382 sorption sites of varying accessibility.

383 The sorption kinetics of DD uptake by GAC, GAC-Fe_3O_4(B), PAC and PAC-Fe_3O_4(A)
384 were strongly dependent on particle size. Uptake of DD by the fine textured PAC and PAC-
385 Fe_3O_4(A) composite was rapid and complete within 10 hours. In contrast, sorption uptake
386 was much slower for GAC and the GAC-Fe_3O_4(B) composite (Fig. 4 and 5) owing to the
387 larger particle size. Sorption equilibria had not been reached for the GAC-Fe_3O_4(B)
388 composite after 40 h. These results are consistent with prior work showing the influence of
389 particle size on sorption kinetics of hydrophobic organic solutes on activated carbon and
390 biochars (Ahn et al., 2005; Kang et al., 2018). As shown, the rate of DD uptake by the fine
391 textured AC and AC-Fe_3O_4(A) is rapid with showing 97% removal of DD from aqueous
392 solution after one hour. The larger sized GAC, with particle diameters ~ 1 mm (5% < 420
393 μm), showed much slower uptake (Fig. 6a) and is attributed to the longer diffusion pathways
394 to binding sites and pore structures in GAC.

395 We demonstrated that both a GAC and a PAC could be magnetized and, more
396 importantly, the GAC-Fe_3O_4(B) and PAC-Fe_3O_4(A) composites maintained high sorption
397 affinity for dioxin. Particle size was a dominant factor in controlling sorption kinetics, with
398 the fine-textured PAC showing nearly complete uptake of dioxin within 1 hour compared to

399 considerably slower uptake by the coarse texture GAC. These differences could be significant
400 in animal dosing studies but less significant for materials deployed as passive samplers over
401 periods of months to years. Finally, these results could prove useful in the design of large-
402 scale recoverable geosorbents manufactured for contaminant removal.

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410

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Table titles:

Table 1. Selected physical properties of GAC, GAC-Fe_3O_4 and PAC.

Table 2. Kinetic parameters at different concentration for adsorption of DD by using DSRA and GAC-Fe_3O_4 composite.

Figure Captions

Fig. 1. Saturation magnetization of GACs and PAC-Fe_3O_4 composites measured by SQUID.

Fig. 2. X-ray powder diffraction (XRD) patterns of the GAC-Fe_3O_4(B) and PAC-Fe_3O_4(A) composites along with reference reflections for magnetite Fe_3O_4.

Fig. 3. Scanning electron microscopy (SEM) images of (a) DSRA (120X magnitude); (b) DSRA (500X magnitude); (c) DSRA (800X magnitude); (d) GAC-Fe_3O_4 composite (50000X magnitude); (e) GAC-Fe_3O_4 composite (150000X magnitude); and (f) GAC-Fe_3O_4 composite (350000X magnitude).

627 Fig. 4. Batch equilibrium sorption isotherms of dibenzo-p-dioxin (DD) on GAC (black

628 squares) and GAC-Fe_3O_4(B) (red circles). Conditions: T=298 K, solution volume=30

629 mL, adsorbent =2.5 mg, contact time=10-48 h.

630 Fig. 5. Sorption kinetics of dibenzo-p-dioxin (DD) uptake by GAC and GAC-Fe_3O_4(B) over

631 40 h of contact. Top figure shows results from initial concentration of 0.8 mg/L,

632 middle figure shows results from initial concentration of 0.4 mg/L, and lower figure

633 shows initial concentration of 0.18 mg/L. GAC is represented by black squares and

634 GAC-Fe_3O_4(B) is represented by red circles. Conditions: T=298 K, solution

635 volume=30 mL, adsorbent =2.5 mg.

636 Fig. 6. Sorption kinetics of dibenzo-p-dioxin (DD) uptake by GAC, GAC-Fe_3O_4(B), PAC and

637 PAC-Fe_3O_4(A) over 18 h of contact. PAC is represented by black squares, PAC-

638 Fe_3O_4(A) is represented by solid red circles, GAC is represented by open black

639 squares, and GAC-Fe_3O_4(B) is represented by open red circles. Conditions: T=298 K,

640 solution volume=30 mL, adsorbent =2.5 mg. Conditions: DD concentration=0.8

641 mg/L, T=298 K, solution volume=30 mL, adsorbent=2.5 mg, contact time=1 h.

642

1 Figure Captions

2 Fig. 1. Saturation magnetization of GACs and PAC-Fe_3O_4 composites measured by SQUID.

3 Fig. 2. X-ray powder diffraction (XRD) patterns of the GAC-Fe_3O_4(B) and PAC-Fe_3O_4(A)

4 composites along with reference reflections for magnetite Fe_3O_4.

5 Fig. 3. Scanning electron microscopy (SEM) images of (a) DSRA (120X magnitude); (b)

6 DSRA (500X magnitude); (c) DSRA (800X magnitude); (d) GAC-Fe_3O_4 composite

7 (50000X magnitude); (e) GAC-Fe_3O_4 composite (150000X magnitude); and (f) GAC-

8 Fe_3O_4 composite (350000X magnitude).

9 Fig. 4. Batch equilibrium sorption isotherms of dibenzo-p-dioxin (DD) on GAC (black

10 squares) and GAC-Fe_3O_4(B) (red circles). Conditions: T=298 K, solution volume=30

11 mL, adsorbent =2.5 mg, contact time=10-48 h.

12 Fig. 5. Sorption kinetics of dibenzo-p-dioxin (DD) uptake by GAC and GAC-Fe_3O_4(B) over

13 40 h of contact. Top figure shows results from initial concentration of 0.8 mg/L,

14 middle figure shows results from initial concentration of 0.4 mg/L, and lower figure

15 shows initial concentration of 0.18 mg/L. GAC is represented by black squares and

16 GAC-Fe_3O_4(B) is represented by red circles. Conditions: T=298 K, solution

17 volume=30 mL, adsorbent =2.5 mg.

18 Fig. 6. Sorption kinetics of dibenzo-p-dioxin (DD) uptake by GAC, GAC-Fe_3O_4(B), PAC and

19 PAC-Fe_3O_4(A) over 18 h of contact. PAC is represented by black squares, PAC-

Fe_3O_4(A) is represented by solid red circles, GAC is represented by open black squares, and GAC-Fe_3O_4(B) is represented by open red circles. Conditions: T=298 K, solution volume=30 mL, adsorbent =2.5 mg. Conditions: DD concentration=0.8 mg/L, T=298 K, solution volume=30 mL, adsorbent=2.5 mg, contact time=1 h.

Figure 1

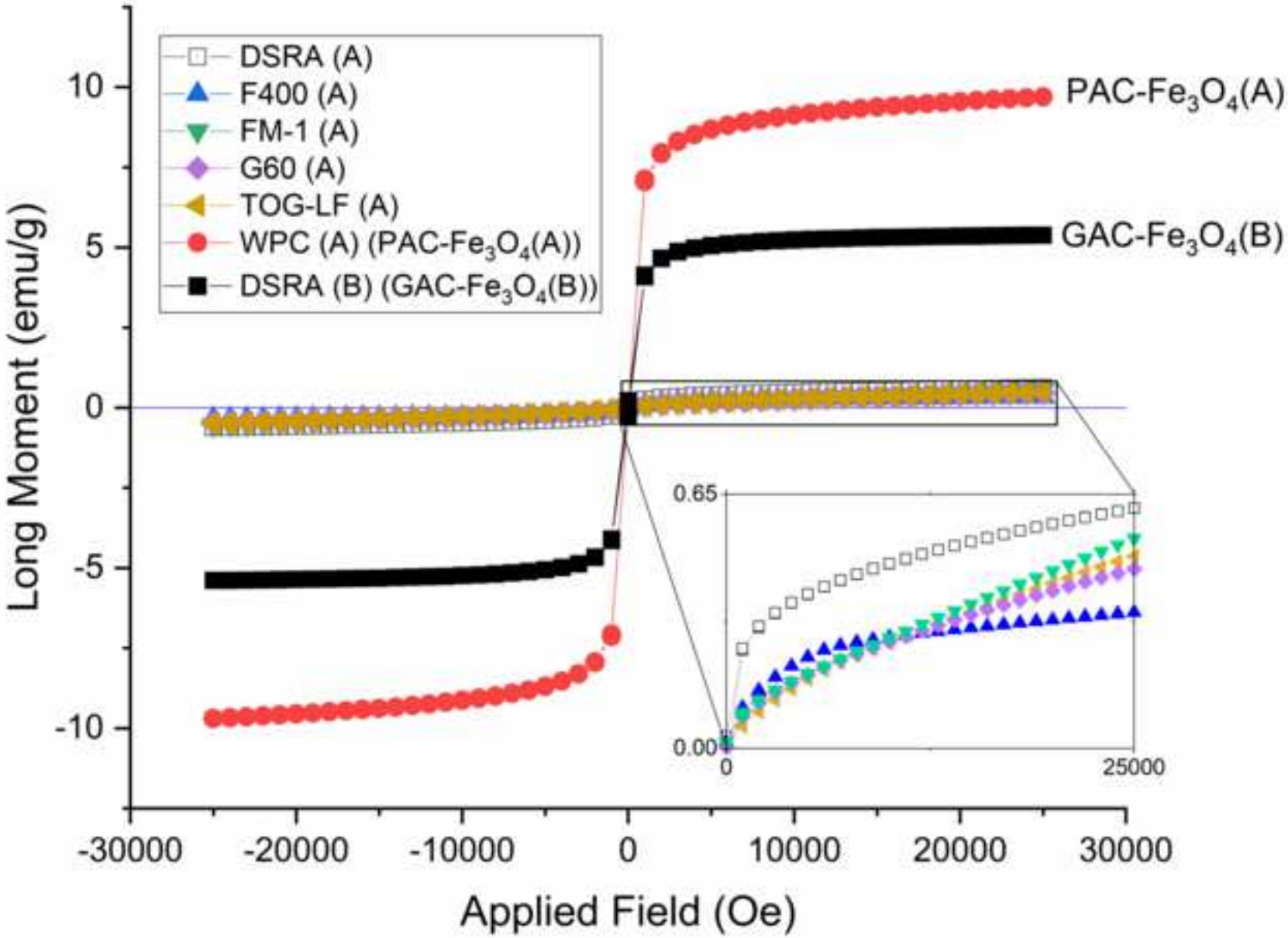

Figure 2

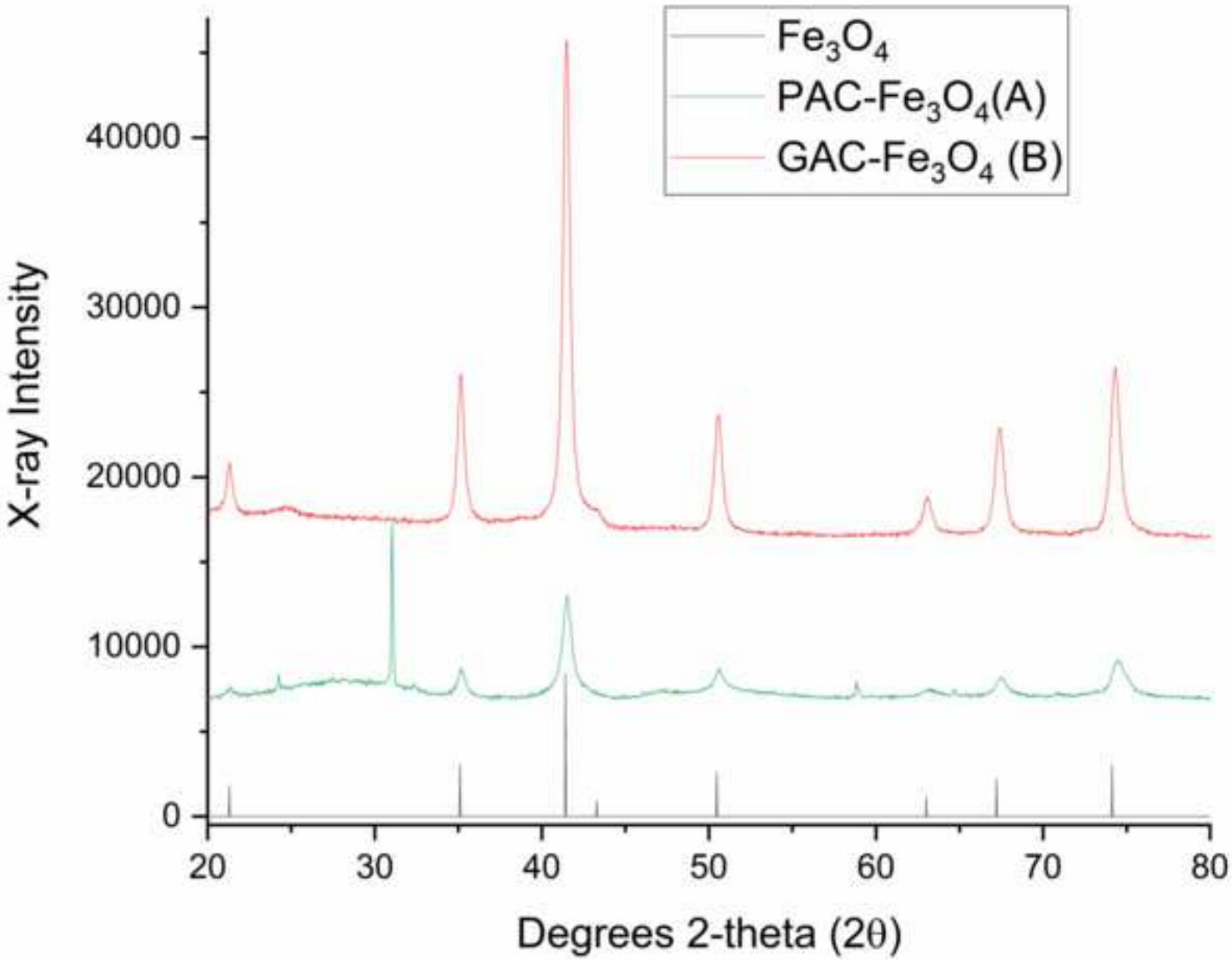

Figure 3

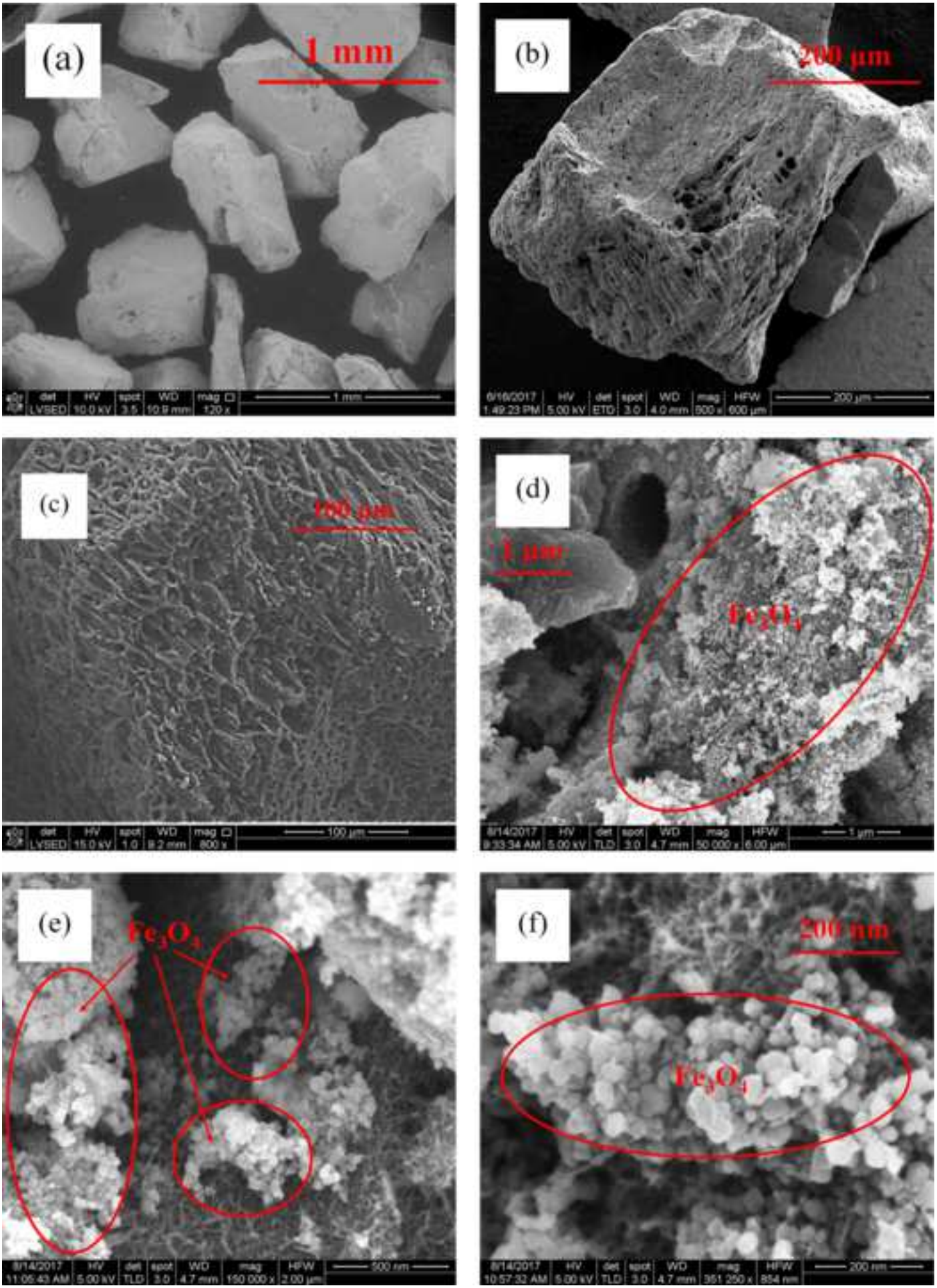

Figure 4

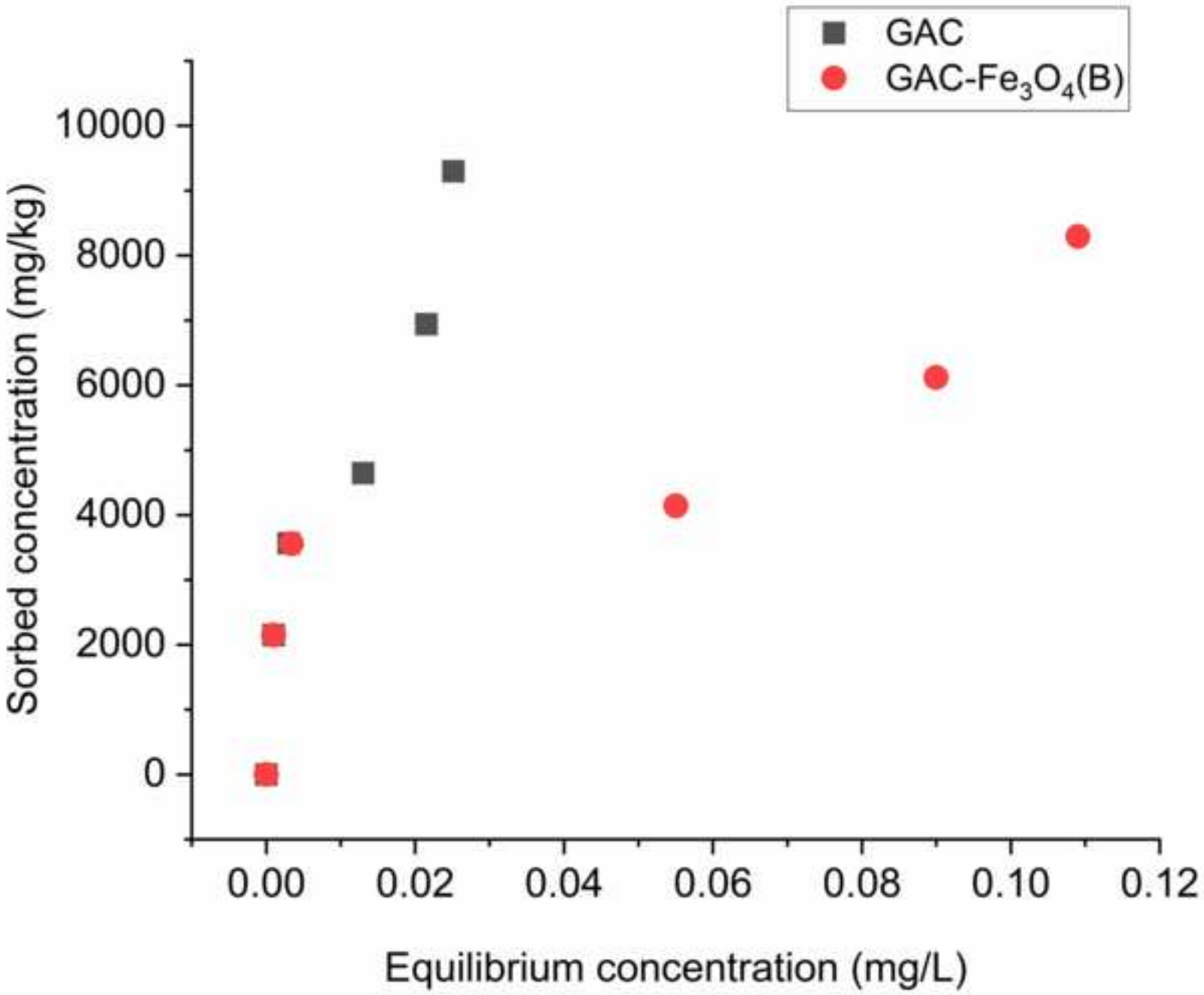

Figure 5

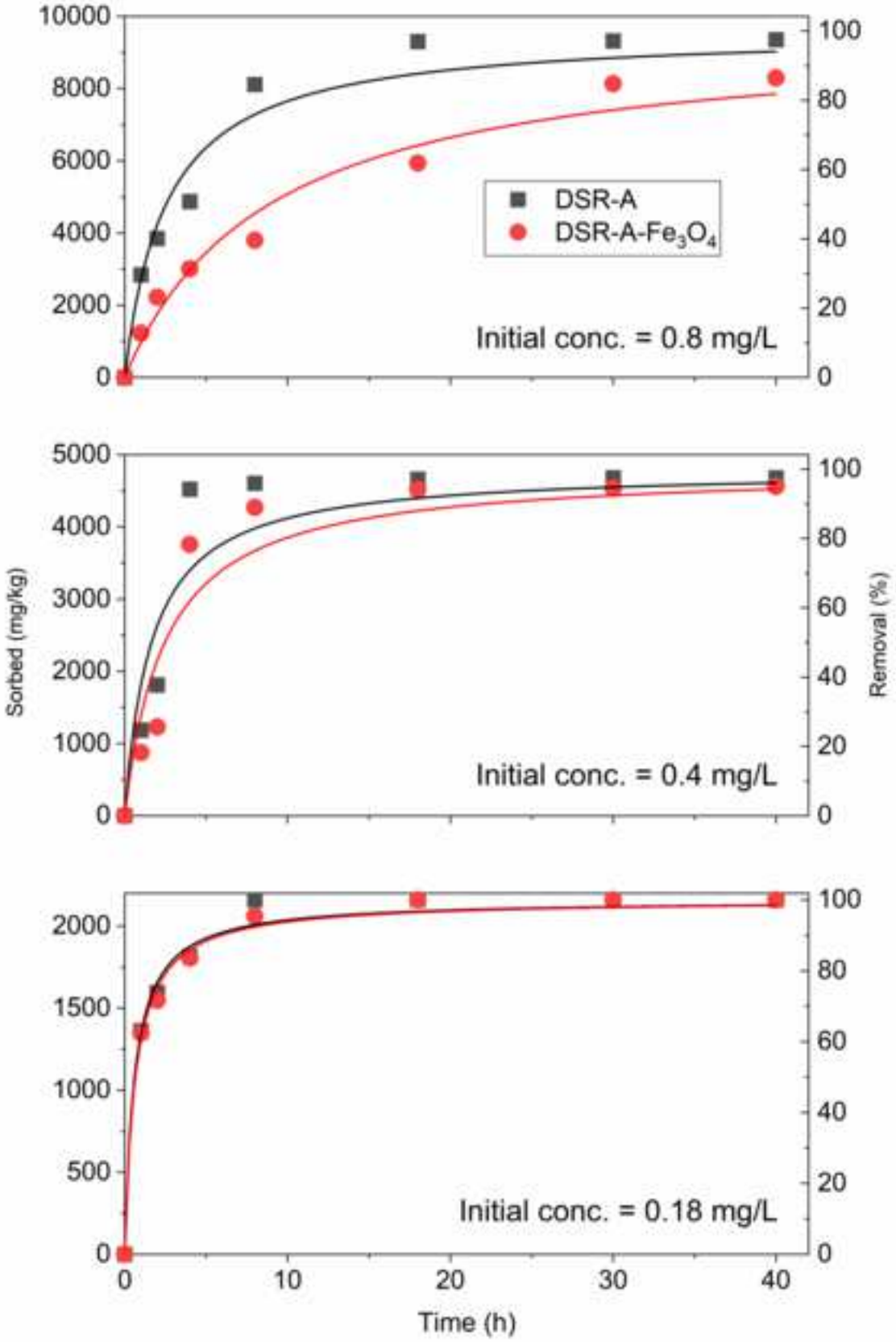

Figure 6

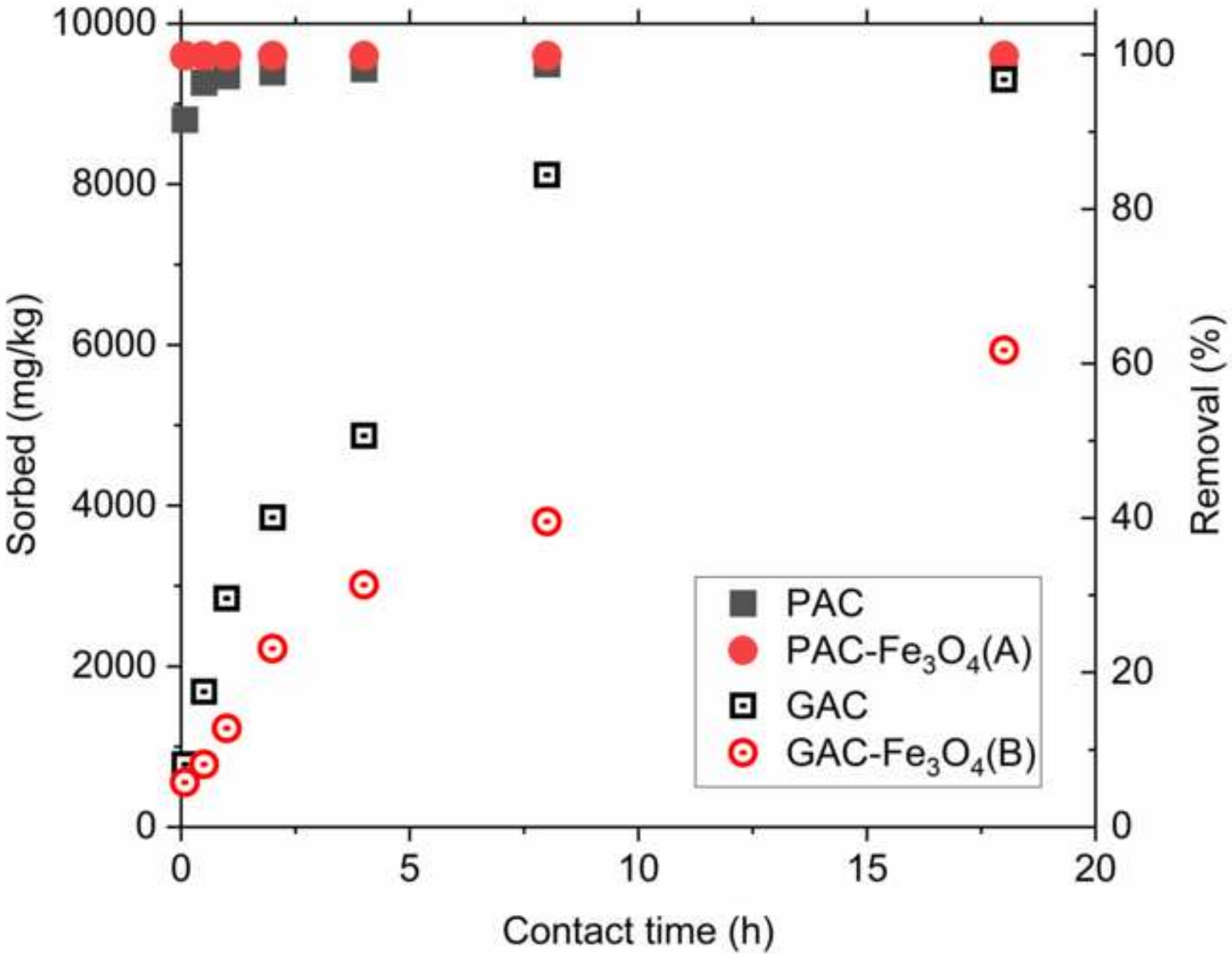

Table 1. Selected physical properties of the activated carbon materials

Material	Supplier	Source	Surface Area (m^2/g)	Mesopore vol. g/cc (% of total)	Micropore vol. g/cc (% of total)	[a]Magnetization after Syn. Method A (emu/g)	[b]Magnetization after Syn. Method B (emu/g)
G60	Cabot	Lignite	987	0.38 (57%)	0.29 (43%)	0.46	
FM-1	Cabot	Lignite	520	0.36 (71%)	0.15 (29%)	0.54	
TOG-LF	Calgon	Coal	916	0.15 (33%)	0.30 (67%	0.49	
F-400	Calgon	Coal	1044	0.16 (31%)	0.36 (69%)	0.35	
WPC (AC)	Calgon	Coconut	802	0.03 (9%)	0.29 (91%)	9.7	
DSRA (GAC)	Calgon	Pool Rej.	822	0.11 (22%)	0.38 (78%)	0.61	
DSRA-Fe_3O_4	Calgon	Pool Rej.	633	0.06 (18%)	0.26 (82%)		5.38

Note:

[a]: Magnetization after Fe_3O_4 impregnation at conditions of 338 K and 0.01 M $FeSO_4$.

[b]: Magnetization after Fe_3O_4 impregnation at conditions of 298 K and 0.1 M $FeSO_4$.

Table 2. The pseudo-second order kinetic model for GAC (DSRA) and GAC-Fe_3O_4(B)

	GAC (DSRA)			GAC-Fe_3O_4 (B)		
	q_e	k_2	Adjusted R Square	q_e	k_2	Adjusted R Square
0.18 mg/L	2160	7.62E-04	0.990	2160	7.02E-04	0.994
0.4 mg/L	4800	1.26E-04	0.893	4800	8.47E-05	0.916
0.8 mg/L	9600	4.10E-05	0.967	9600	1.17E-05	0.973