

This is a repository copy of Measuring and enhancing the ionic conductivity of chloroaluminate electrolytes for Al-ion batteries.

White Rose Research Online URL for this paper: <u>https://eprints.whiterose.ac.uk/201833/</u>

Version: Published Version

Article:

Lucio, A.J. orcid.org/0000-0003-0034-4914, Sumarlan, I., Bulmer, E. et al. (5 more authors) (2023) Measuring and enhancing the ionic conductivity of chloroaluminate electrolytes for Al-ion batteries. The Journal of Physical Chemistry C, 127 (28). pp. 13866-13876. ISSN 1932-7447

https://doi.org/10.1021/acs.jpcc.3c02302

Reuse

This article is distributed under the terms of the Creative Commons Attribution (CC BY) licence. This licence allows you to distribute, remix, tweak, and build upon the work, even commercially, as long as you credit the authors for the original work. More information and the full terms of the licence here: https://creativecommons.org/licenses/

Takedown

If you consider content in White Rose Research Online to be in breach of UK law, please notify us by emailing eprints@whiterose.ac.uk including the URL of the record and the reason for the withdrawal request.



eprints@whiterose.ac.uk https://eprints.whiterose.ac.uk/



pubs.acs.org/JPCC

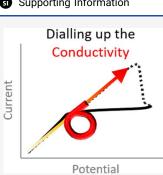


Measuring and Enhancing the Ionic Conductivity of Chloroaluminate Electrolytes for Al-Ion Batteries

Anthony J. Lucio,* Iwan Sumarlan, Elena Bulmer, Igor Efimov, Stephen Viles, A. Robert Hillman, Christopher J. Zaleski, and Karl S. Ryder

Cite This: J. Phys. Chem. C 2023, 127, 13866–13876			Read Online	I	
ACCESS	III Metrics & More		E Article Recommendations		s Supporting Information

ABSTRACT: At the core of the aluminum (Al) ion battery is the liquid electrolyte, which governs the underlying chemistry. Optimizing the rheological properties of the electrolyte is critical to advance the state of the art. In the present work, the chloroaluminate electrolyte is made by reacting AlCl₃ with a recently reported acetamidinium chloride (Acet-Cl) salt in an effort to make a more performant liquid electrolyte. Using AlCl₃:Acet-Cl as a model electrolyte, we build on our previous work, which established a new method for extracting the ionic conductivity from fitting voltammetric data, and in this contribution, we validate the method across a range of measurement parameters in addition to highlighting the model electrolytes' conductivity relative to current chloroaluminate liquids. Specifically, our method allows the extraction of both the ionic conductivity and voltammetric data from a single, simple, and routine measurement. To bring these results in the context of current methods, we compare our results to two independent



standard conductivity measurement techniques. Several different measurement parameters (potential scan rate, potential excursion, temperature, and composition) are examined. We find that our novel method can resolve similar trends in conductivity to conventional methods, but typically, the values are a factor of two higher. The values from our method, on the other hand, agree closely with literature values reported elsewhere. Importantly, having now established the approach for our new method, we discuss the conductivity of $AlCl_3$:Acet-Cl-based formulations. These electrolytes provide a significant improvement (5–10× higher) over electrolytes made from similar Lewis base salts (e.g., urea or acetamide). The Lewis base salt precursors have a low economic cost compared to state-of-the-art imidazolium-based salts and are non-toxic, which is advantageous for scale-up. Overall, this is a noteworthy step at designing cost-effective and performant liquid electrolytes for Al-ion battery applications.

INTRODUCTION

The need for alternative energy storage, transmission, and conversion technologies is urgent in order to meet growing global demands. Renewable energy sources, such as wind and solar, are playing a vital role in the move toward net zero targets.¹⁻³ However, due to the intermittent nature of these renewable sources, there is a real need for competitive, stationary (grid-scale) energy storage options. Lithium (Li)ion battery technology represents the most mature and widespread form of electrochemical energy storage with overwhelming adoption in portable electronic devices. The uneven distribution of critical raw materials and the high economic costs, however, significantly reduce the appeal of Liion batteries for large-scale stationary storage.⁴⁻⁶ Aluminum (Al)-ion-based batteries are a promising alternative due to the large and wide abundance of Al; they are often made from inexpensive non-toxic materials, and in theory, they can provide competitive energy densities (e.g., 13.4 W h cm⁻³ for Al versus 6.2 W h cm⁻³ for Li).⁷ As a result, non-aqueous Al battery chemistries are receiving significant interest from the scientific community.^{8–13}

At the heart of the Al-ion battery is the liquid electrolyte. These electrolytes, often called chloroaluminate liquids, are formed by an acid–base reaction between a Lewis acid (LA; i.e., AlCl₃ salt) and a Lewis base (LB; e.g., Cl⁻-containing salt). To date, the majority of research has been done on chloroaluminate liquids made from the solid (at room temperature) salt 1-ethyl-3-methylimidazolium chloride (EMIM-Cl);^{14–21} this electrolyte is commercially available.²² The electrochemical and rheological performance is promising, but it comes with a high economic cost of the starting material, which ultimately is not advantageous for scale-up. Other liquid electrolytes, often called ionic liquid analogues (ILAs), can be formed by reaction with AlCl₃ and softer Lewis bases (e.g., urea^{23–28} or acetamide^{29–34}). These are much more cost effective options, but they are limited by their electrochemical and rheological performance.

We have recently reported the formation of chloroaluminate liquids from amidine-based (chloride) salts that exhibit

 Received:
 April 6, 2023

 Revised:
 June 19, 2023

 Published:
 July 6, 2023





chemistries (i.e., reduce moisture sensitivity, minimize leakage,

and allow for the generation of flexible but tough

materials).^{36,37} All of this work is aimed at developing performant electrolytes for Al-ion batteries. The mole ratio of the LA and LB has a significant impact on not only the rheological properties of the electrolyte but also its ability to form a stable liquid. The stable compositional range depends on the LB salt. Specifically, at mole LA:LB ratios <1, the liquids are termed Lewis basic; at LA:LB ratios = 1, the liquid is termed neutral; and at LA:LB ratios >1, the liquids are termed Lewis acidic.^{38,39} Consequently, there is often an ideal mole ratio between the LA and LB that seeks to increase the conductivity (>5 mS cm^{-1}) and decrease the viscosity (<50 cP). The Lewis acidity also impacts the electroactive Al species present. Previous literature suggests that Lewis acidic formulations (>1:1) are needed in order for Al deposition to proceed, $^{27,28,34,39-43}$ where there is a mixture of both anionic (e.g., $AlCl_4^-$ and $Al_2Cl_7^-$) and cationic (e.g., $[AlCl_2(LB)_n]^+$) species present. For example, EMIM-Cl based liquids can be formed within a mole ratio ranging from 0.8:1 to 2:1 (LA:LB).⁴⁴ Zhu et al. reported conductivities increasing from 15 to 17.5 mS cm⁻¹ for AlCl₃:EMIM-Cl liquid for mole ratios between 1.4:1 and 1.7:1 (LA:LB).⁴⁵ Conversely, Azimi et al. reported conductivities decreasing from 22.6 to 14.7 mS cm⁻¹ for LA:LB compositions between 1:1 and 2:1 with AlCl₃:EMIM-Cl liquids.¹⁴ Other reports have found conductivities of 16.1,⁴⁶ 15.5,⁴⁷ and 9.2 mS cm⁻¹⁴⁸ for AlCl₃:EMIM-Cl liquids with a 1.5:1 mole ratio. On the other hand, for urea-based liquids, the conductivities are an order of magnitude lower than that of EMIM-Cl based liquids. The Azimi group report conductivities increasing from 0.91 (LA:LB = 1.1:1) to 1.45 mS cm⁻¹ (LA:LB = 1.3:1) and then decreasing to 1.27 mS cm⁻¹ (LA:LB = 1.5:1) for AlCl₃:urea liquids.² Alternatively, Angell et al. found an increasing conductivity from 1.02 (LA:LB = 1:1) to 1.17 mS cm⁻¹ (LA:LB = 1.5:1) for AlCl₃:urea liquids.²⁵ It is apparent that there are several factors that can impact the conductivity, such as using different measurement methods, varying purities of LA/LB salts, and temperature. There is a significant need to improve the conductivity to enhance the performance of the liquid electrolyte, and this point has been reiterated by several groups.^{14,25,40,49-51}

Conductivity (σ) is an important rheological metric, and increasing the ionic conductivity for chloroaluminate electrolytes is an important step toward advancing Al-ion battery chemistries. Conductivity is conventionally measured using commercially available sensors via an impedance measurement. These often consist of two to four electrodes arranged in a fixed position relative to one another. An AC voltage (singlefrequency impedance measurement) is applied to the electrodes that generates a current response in the medium, and the corresponding ohmic resistance (R) is used to calculate a conductivity value. The cell constant (K) of the sensor, which is dependent on the geometrical arrangement and surface area of the electrodes, governs this calculation. Commercial sensors are often equipped with a thermocouple to accurately measure

the solution temperature as conductivity is a temperaturedependent parameter. A more formal method to measure the conductivity can be achieved using frequency response analysis. Here, a broadband impedance spectrum is collected across a range of frequencies and subsequently modeled using an appropriate electrochemical equivalent circuit to extract the resistance value. This method requires that the experimental cell is previously calibrated (ideally against standard conductivity solutions) to find the cell constant. With the resistance and cell constant values, it is straightforward to calculate the conductivity via $\sigma = K/R$. An obvious benefit to this method is a cost-effective, bespoke measurement cell that can be readily produced from common laboratory materials. Lastly, previous work has demonstrated that the conductivity can even be extracted from pulsed voltammetric potentiostatic techniques.52

The work presented herein is a detailed exploration into a novel method of measuring ionic conductivity via voltammetric data for ILAs made from the LA salt AlCl₃ and the LB salt acetamidinium chloride (Acet-Cl). In our earlier work, we established the concept and theory.³⁵ We have now taken this one step further, and in the present work, our method is benchmarked to standard AC impedance conductivity measurements. We explore several perturbations on the voltammetric measurement in an effort to optimize individual parameters, and we compare our novel method to a range of other state-of-the-art ILAs. The voltammetric method yields conductivity values of the same order of magnitude (although a factor of two larger) as standard AC impedance techniques and follows similar conductivity trends. Therefore, this method allows for the estimation of conductivity without the need for an additional measurement or sensor. Another aspect of this work is aimed at enhancing the conductivity of electrolyte formulations for Al-ion batteries. With our AlCl₃:Acet-Cl formulations, we find substantial improvements $(5-10 \times$ higher ionic conductivity) over analogous liquids made from similar LB salts. Overall, the AlCl₃:Acet-Cl electrolyte represents a significant step toward improving electrolyte materials for Al-ion battery systems.

EXPERIMENTAL SECTION

Chemicals. The solid Lewis base (LB) salts acetamidinium chloride (Acet-Cl; >98%, Acros-Organics), acetamide (Acet; 99%, Alfa Aesar), urea (ReagentPlus, \geq 99.5%, pellets, Sigma-Aldrich), and 1-ethyl-3-methylimidazolium chloride (EMIM-Cl; \geq 95%, Aldrich) were used as received. The solid Lewis acid (LA) salt aluminium chloride (AlCl₃; anhydrous, granular, 99%, Alfa Aesar) was used as received. Paraffin oil (puriss., meets analytical specification of Ph. Eur., BP, viscous liquid, Sigma-Aldrich) was used as received. Conductivity standards (certified traceable to NIST, VWR) of 44,479, 11,419, 8863, 1249, 885, 442, and 74 μ S cm⁻¹ (at 19 °C) were used as received.

Electrolyte Synthesis. The ILA electrolytes were prepared by mixing the desired Lewis base salt and Lewis acid salt, at a specified molar ratio, with heating under a protective hydrocarbon layer until all AlCl₃ dissolved, as demonstrated previously.^{28,35} The liquid was allowed to stir at 50 °C for 1 h before use. This synthesis method produced stable, dark brown liquid electrolytes for electrochemical testing.

Simultaneous Cyclic Voltammetry (CV) and Quartz Crystal Microbalance (QCM) Measurements. The electrochemical CV/QCM measurements were done with a Reference600 potentiostat (Gamry) coupled to an eQCM10M resonator (Gamry), which allows for simultaneous collection of voltammetric and acoustic signals. The working electrode was a 9.00 MHz (±30 kHz) AT-cut quartz crystal resonator (Seiko) with Pt (electrolyte facing) and Pt (air facing)-coated sides. The Pt surfaces are sputtered to a thickness of 300 nm and polished to a mirror finish with a surface roughness of approximately 60 nm. The total surface area of the Pt working electrode is 0.236 cm², but the exposed surface area was controlled with the cell geometry to be approximately 0.196 cm². The counter electrode was a coiled 2.0 mm dia. Al wire (99.9998%, metals basis, Alfa Aesar) that had a surface area 50x that of the working electrode. The quasi reference electrode (QRE) was a straight, bare 2.0 mm dia. Al wire (99.9998 %, metals basis, Alfa Aesar) that provided reproducible potentials. The counter electrode and QRE were positioned 1.5 and 1 cm away from the working electrode, respectively. The CV/QCM cell was made in-house to physically fit the resonator electrodes (refer to ESI 1, Figure S1a, b). A PEEK material was used to provide both chemical inertness against the electrolytes examined and robustness for positioning. All CV/QCM measurements were done directly after EIS measurements at a temperature of 23 ± 3 °C. The measurement solution was quiescent.

For temperature-dependent CV/QCM measurements, the working electrode was a 10 MHz AT-cut polished shear-mode quartz crystal resonator (ICM Manufacturing) with Pt (electrolyte facing) and Au (air facing)-coated sides. The total surface area of the Pt working electrode is 0.21 cm^2 , but the exposed surface area was controlled with the cell geometry to be approximately 0.153 cm^2 . The counter electrode was an Al flag (surface area = 2.34 cm^2), and a straight, bare 2.0 mm dia. Al wire was used as a QRE. The counter electrode and QRE were positioned 3.5 and 1 cm away from the working electrode, respectively. The temperature-dependent CV/QCM cell was made in-house using a jacketed glass cell with a PTFE cap that provided reproducible positioning. The temperature was varied from 25 to 70 °C using a heated water bath. The measurement solution was quiescent.

Electrochemical Impedance Spectroscopy (EIS) Measurements. The EIS measurements were done using a COMPACTSTAT.h mobile electrochemistry potentiostat (Ivium). A two-electrode setup was employed in a bespoke jacketed glass cell and a Teflon cap with ports for the two electrodes and gas purging (refer to ESI 1, Figure S1c). Straight, identical length Al wires of 2.0 mm diameter (99.9998%, metals basis, Alfa Aesar) were used for the electrodes. The EIS conductivity cell was calibrated using seven conductivity standards to obtain the cell constant, K, 0.377 (\pm 0.002) cm⁻¹ that was used to convert measured resistance (R; Ω) values from ILAs into conductivity (σ ; S cm⁻¹) values using the equation $\sigma = K/R$ (refer to ESI 2, Figure S2). All EIS measurements were performed directly after synthesis at a temperature of 27 ± 2 °C. Approximately 35 mL of the ILA was pipetted into the glass cell underneath a protective paraffin oil layer. The measurement solution was quiescent. The broadband EIS data were collected at 0 V within a frequency range of 100,000 and 10 Hz with 15 points per decade and an AC voltage amplitude of 10 mV. Complex impedance (Nyquist) data were analyzed by fitting to an electrochemical equivalent circuit consisting of a resistor in series with a constant phase element (i.e., R-CPE). A

traditional minimization objective function, complex nonlinear least squares method, was used to perform the data fitting.⁵³

Commercial Conductivity Probe. A commercial chemical-resistant type conductivity probe (SC72SN-31-AA; Yokogawa) and meter (SC72 Personal Conductivity Meter; Yokogawa) were used to compare to values from the voltammetric- and impedance-based methods. The cell constant for the commercial conductivity probe was 5.2 \pm 0.5 cm⁻¹, and it has an integrated temperature sensor (accuracy within \pm 0.7 °C). Measurements were taken at 25 \pm 2 °C.

RESULTS AND DISCUSSION

The following sections outline the Al deposition/dissolution chemistry and our novel voltammetric-based conductivity measurement method in detail before examining the effects of experimental and environmental variables, including different potential scan rates, the width of potential excursion, voltammetric cycling, iR compensation effects, temperature, and compositional dependencies. The AlCl₃:Acet-Cl electrolyte was selected as the main candidate for this study in an effort to not only benchmark against more traditional conductivity measurement methods but also to highlight its physiochemical properties compared to other ILAs. A LA:LB mole ratio of 2:1 was used in our tests as it demonstrated the best electrochemical and rheological performance from our compositional work (discussed below). The final section explores the applicability of the voltammetric-based conductivity method to measure different ILA electrolytes with comparisons to literature references.

Al Deposition/Dissolution. The experimental cyclic voltammogram in Figure 1a shows the response associated with Al deposition and dissolution from the AlCl₃:Acet-Cl 2:1 formulation on a Pt working electrode at 100 mV s⁻¹. The cathodic scan direction is denoted with a solid black line, and the anodic scan direction is a dashed black line. In the cathodic potential scan direction from +0.6 V (vs Al QRE; unless stated otherwise, all potentials are referenced to an Al quasi-reference electrode) to -0.15 V, there are only small (ca. 95 μ A cm⁻²) currents that are insignificant on the scale of the redox process being probed. At -0.15 V, the current begins to increase sharply due to the electrochemical reduction of Al³⁺ and consequent deposition of the Al metal on the working electrode. This response continues until the selected vertex potential of -0.5 V. The current signal then shows a very characteristic, linear response in the anodic potential scan direction from -0.5 V to just over +0.4 V, where electrochemical deposition of Al occurs at all potentials negative of -0.15 V and electrochemical dissolution of Al takes place at all potentials positive of -0.15 V. This type of linear voltammetric behavior has been reported previously for similar chloroalu-minate liquids.^{20,24,34,35,41,42,54,55} Finally, at +0.5 V, the dissolution current peaks and then falls abruptly as it goes to +0.6 V (the second switching potential), indicating that the deposited Al has been removed.

This redox cycle can also be viewed from electrochemical QCM data obtained concomitantly with the voltammetric data. Figure 1b shows a plot of the mass change (Δm) as a function of potential (E) with the solid black line representing the cathodic scan and the dashed black lines corresponding to the anodic scan. Here, we can see that the scan starts at +0.3 V at the baseline (labeled with the solid gray line) and the potential is swept in the anodic direction to +0.6 V where it increases

i =

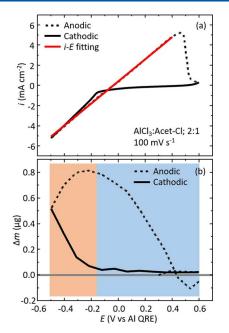


Figure 1. (a) Exemplar experimental cyclic voltammogram (solid and dashed black traces represent cathodic and anodic scans, respectively) demonstrating the *i*–*E* curve-fitting (solid red line) method with the AlCl₃:Acet-Cl 2:1 electrolyte at a scan rate of 100 mV s⁻¹. (b) Corresponding QCM plot at 100 mV s⁻¹ showing the mass change as a function of potential. The orange shaded region visually represents deposition potentials, whereas the blue shaded region represents dissolution potentials. A solid gray line is included at the zero mass mark for clarity.

slightly over the baseline. In the cathodic direction from +0.6 to -0.15 V, there is a slight increase in the mass (due to non-Faradic processes such as potential-dependent adsorption), but beyond -0.15 V, the mass increases significantly as a result of Al deposition on the Pt resonator electrode. The negative vertex potential is reached at -0.5 V, but the mass still increases as the anodic scan direction commences since the current is still negative of the onset deposition potential for Al. The mass increase peaks at 0.8 μ g near -0.2 V, indicating a switch from Al deposition to Al dissolution. As the anodic scan continues, the mass decreases and drops below 0 μ g. This hysteresis indicates that slightly more mass is lost in the dissolution phase than was deposited in the deposition; however, such responses are often found in the QCM data of similar liquids and may be attributed to the presence of adsorbed species on the Al coating or on the crystal. Taken together, the CV/QCM data indicate that the Al (deposition/ dissolution) redox cycle is behaving in a chemically reversible manner.

Voltammetric-Based Conductivity Measurement. The characteristic linear voltammetric response we see in the anodic potential scan direction can be fit to extract the conductivity. The i-E curve-fitting method was first established in our previous work,³⁵ but for clarity (see eqs 1 and 2), i is the experimental current density, σ is the conductivity, ϕ is the overpotential $E-E_0$ (i.e., E_0 is taken as the zero current point from the voltammogram), i_0 is the exchange current density, n is the number of electrons, F is the Faraday constant, α is the dimensionless charge-transfer coefficient, R is the universal gas constant, and T is the absolute temperature.⁵⁶

$$T = \frac{\sigma\varphi i_0 \left(\exp\left(\frac{nF(1-\alpha)\varphi}{RT}\right) - \exp\left(\frac{-nF\alpha\varphi}{RT}\right)\right)}{\sigma\varphi + i_0 \left(\exp\left(\frac{nF(1-\alpha)\varphi}{RT}\right) - \exp\left(\frac{-nF\alpha\varphi}{RT}\right)\right)}$$
(1)

$$-\frac{\sigma\varphi i_0 \exp\left(\frac{-m\alpha\varphi}{RT}\right)}{\sigma\varphi + i_0\left(1 - \exp\left(\frac{-nF\alpha\varphi}{RT}\right)\right)}$$
(2)

Equation 1 describes the anodic scan direction (dissolution), whereas eq 2 describes the cathodic scan (deposition). However, as we typically observe a characteristic nucleation loop in the cyclic voltammogram (refer to Figure 1a), which is not considered in this relation, eq 2 is of limited use. Nonetheless, the i-E curve-fitting method using eq 1 only has three fit parameters, which are i_0 , E_0 , and σ . All other parameters are constants, but it is worth noting that the charge-transfer coefficient, α , is set equal to 0.5 in our calculations. The charge-transfer coefficient can be a variable, e.g., for electrolytes with a more pronounced inflection at E_0 potential, but we do not observe this with the AlCl₃:Acet-Cl electrolytes. Furthermore, allowing α to vary as a fit parameter had a negligible effect on the resulting fits. A traditional objective minimization function (see eq 3) is used to fit the data via the chi-squared method.^{57,58}

$$\chi^{2} = \Sigma \frac{(\text{observed} - \text{expected})^{2}}{\text{expected}}$$
(3)

We typically find χ^2 values on the order of 10^{-3} , which show the goodness of fit between theory and experiment. As can be seen in Figure 1a, we find good agreement between the experimental CV trace and the predicted current based on eq 1 over the 900 mV potential fitting range. As can be seen in Table 1, we estimate a conductivity of 12.9 ± 1.4 mS cm⁻¹,

Table 1. All *i*-E Curve-Fitting Parameters⁴

parameter	value				
fit pa	arameters				
$\sigma ~({\rm mS~cm^{-1}})$	12.9 ± 1.4				
$i_0 ({\rm mA}{\rm cm}^{-2})$	4.7 ± 2.2				
E_0 (V)	-0.06 ± 0.02				
constants					
А	0.5				
n	3				
F (C mol ⁻¹)	96,485				
$R (J \text{ mol}^{-1} \text{ K}^{-1})$	8.314				
<i>T</i> (K)	296				

^{*a*}The top three show the fitting (variable) parameters, whereas the bottom shows the five constant values.

and we find good agreement in the predicted i_0 and E_0 fitted values to experimental data in Figure 1a. A simpler linear regression analysis to the voltammetric data can also be used. Specifically, by taking the best fit line to this current—potential data (0.00168 A V⁻¹) and considering the separation distance (1.5 cm) between the working and counter electrodes, in addition to the working electrode surface area (0.196 cm²), we calculate a conductivity of 12.8 mS cm⁻¹. This simply highlights that our modified Butler—Volmer formalism is estimating values expected from a rudimentary specific conductivity calculation. For reference, our previous work reported a conductivity of 9.7 mS cm⁻¹, but this was for an AlCl₃:Acet-Cl 1.5:1 mole ratio formulation.³⁵ The larger conductivity value in the present study is attributed to the higher concentration of Al species resulting from the 2:1 mole ratio (discussed in more detail below). We postulate that the amidine-based ILA used here has a relatively high conductivity (compared to liquids made from similar LB salts, e.g., urea) as a result of the increased Lewis acidity that provides a higher concentration of charge carriers, in addition to the fact that it is an ionic Lewis base salt. Recent work by Schoetz et al. has utilized this method to extract conductivity values from imidazolium-based liquids.⁵⁹ One shortcoming of the method we discuss is that it may only be applicable to concentrated electrolyte solutions typified by the AlCl₃:Acet-Cl formulations demonstrated here for which ion concentrations are ca. 7 M. As such, these do not typically yield diffusion-limited voltammetric responses. In contrast, work in dilute aqueous media generally show peaked voltammetric responses governed by diffusion. Therefore, our methodology is not applicable to the latter situation. We are only in the early stages of developing this theory, and the limitations will become clearer as we explore more diverse chemical systems. Nonetheless, the methodology presented here represents a novel approach to extract conductivity from voltammetric data, and in the next section, we will compare it to more traditional measurement methods.

Impedance-Based Conductivity Measurements. A common way to estimate the ionic conductivity of electrolyte solutions is through AC impedance measurements. Broadband EIS data are often collected and fitted to an electrochemical equivalent circuit to find the ohmic resistance.^{42,46,60} The resistance can be used to calculate the conductivity in a previously calibrated cell using a cell constant, which is specific to the geometrical arrangement of the measurement electrodes and exposed surface area. As detailed in the Experimental Section and in ESI 2, a bespoke jacketed glass cell and PTFE cap were calibrated solutions. We find a cell constant of $K = 0.377 \pm 0.002$ cm⁻¹, which is used to calculate conductivity values from similar measurements with our ILA electrolytes.

An exemplar Bode plot showing the impedance (Z) modulus from a broadband EIS spectrum is presented in Figure 2, which was collected at 0 V over the frequency (f) range from 100,000 to 10 Hz for the AlCl₃:Acet-Cl 2:1 formulation. The filled black squares are the experimental data, and the solid red line

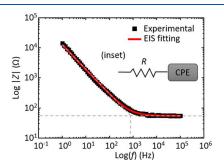


Figure 2. Experimental impedance modulus plot (filled black squares) and corresponding fit (solid red line) to an R-CPE electrochemical equivalent circuit (see the inset) for the $AlCl_3:Acet-Cl 2:1$ formulation. The dashed gray lines are overlaid as a visual aid for estimating the capacitance and resistance. Collected at 0 V with a perturbation amplitude of 10 mV.

is the fit to an electrochemical equivalent circuit (R-CPE; see the inset of Figure 2). From the plot, we can estimate the capacitance (C) and resistance (R) values. At high frequencies (>1 kHz), the resistive element dominates, and the plateau with respect to the y-axis in the high-frequency region suggests an R value of ca. 50 Ω . Alternatively, at low frequencies (<1 kHz), the capacitive element dominates. By approximating the crossover frequency point between the high and low regions on the x-axis (using the dashed gray lines in Figure 2), we estimate a frequency of ca. 750 Hz, which corresponds to the maximum frequency in an admittance plot. By a simple estimation of $C = -1/(2 \cdot \pi \cdot f \cdot Z)$, we calculate a capacitance of ca. 20 μ F cm⁻². More formally, the data are fitted to an *R*-CPE electrochemical equivalent circuit using a χ^2 -based minimization objective function via the complex nonlinear least squares method. As can be seen, we find good agreement between the experimental and predicted data over the entire frequency range, and we typically find χ^2 values on the order of 10^{-3} . The fit estimates a C value of 17 \pm 4 μ F cm⁻² and an R value of $53.9 \pm 4.9 \Omega$, which confirm our visual estimations. Finally, by using this R value in conjunction with the cell constant from the calibrated cell, we calculate a conductivity of 7.0 \pm 0.6 mS cm⁻¹ for the AlCl₃:Acet-Cl 2:1 formulation from the EIS-based method. It is worth noting that even if we only examine the low-frequency portion of the EIS spectrum, the estimated resistance values are similar to values when the entire broadband EIS spectrum is fit.

For comparative purposes, a commercial conductivity probe returns a conductivity value of 5.8 \pm 0.2 mS cm⁻¹ for the AlCl₃:Acet-Cl 2:1 formulation. Interestingly, there appear to be differences in the estimated conductivity based on the measurement technique. The commercial conductivity probe is likely using an (undisclosed) single-frequency impedance measurement, whereas a broadband EIS measurement collects data over a wide range of frequencies. This difference could have an impact on the conductivity estimates, but it is likely to be relatively small as they are both based on an AC impedance measurement. The voltammetric method does suggest a higher conductivity value, by a factor of two, compared to the impedance-based methods, but importantly, they are all of the same order of magnitude. This provides some support to the underlying model we have outlined in the previous section. These observed variances in outcome between techniques may originate either in the differences of the surface condition of the measurement electrode or perhaps from the relative time scales over which the measurements are made. The translational modes of the dominant current carrying species may vary according to frequency. In the following sections, we will examine several different measurement parameters to test the voltammetric-based conductivity measurement method.

Potential Scan Rate Effects. The voltammetric response was next examined across a range of potential scan rates (ν). Figure 3a shows representative cyclic voltammograms for the AlCl₃:Acet-Cl 2:1 formulation at 10, 20, 40, 60, 100, and 200 mV s⁻¹ scan rates. Interestingly, we find very minimal scan rate dependence for the Al deposition/dissolution redox process. The onset potential for Al deposition occurs at -0.15 V, and the Al dissolution current peaks at 5 mA cm⁻² at +0.5 V for all curves. The characteristic, symmetrical current–potential response is retained for all scan rates, and this includes the linear region from -0.5 to +0.4 V in the anodic scan direction that is fit to eq 1 to estimate the conductivity. The data in Figure 3b show the calculated conductivity as a function of

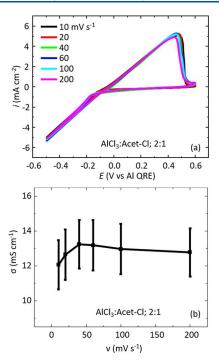


Figure 3. (a) Overlay of cyclic voltammograms at five potential scan rates for the $AlCl_3$:Acet-Cl 2:1 formulation and (b) plot of conductivity (from *i*-*E* curve fitting) as a function of scan rate. Error bars represent the standard deviation of 3 replicate measurements.

scan rate. The conductivity values are independent of the scan rate at 13 mS cm⁻¹ (within experimental uncertainty). Therefore, unless stated otherwise, the 100 mV s⁻¹ scan rate was used for testing. The lack of any observed scan rate dependence here suggests that there is no mass-transport limitation. This may be due to the very high concentration of reducible Al^{3+} species (ca. 7 M) present and may also reflect a dynamic balance between the depletion of Al^{3+} in the diffusion layer and the rapid growth of the Al metal phase on the electrode surface.

Width of Potential Excursion. Another variable to consider is the width of potential excursion for the Al deposition/dissolution redox response (i.e., the absolute values of the anodic and cathodic limits). These limits are important as they dictate which processes occur (thermodynamics) and the rate (kinetics) at which they take place. The width of the potential window in which the deposition/dissolution process is stable and repeatable also impacts directly the operational specifications for any battery system containing such an electrolyte. For example, it would determine the maximum voltage limits applicable during charging. Cyclic voltammograms of the AlCl₃:Acet-Cl 2:1 electrolyte were recorded using three different potential excursion values and two potential scan rates, Figure 4. Here, the solid line traces correspond to 100 mV s⁻¹ $\rm CV$ data (Figure 4a), and the dashed line traces represent 20 mV s⁻¹ CV data (Figure 4b). As we have previously mentioned, for the 1.1 V potential width, we see only negligible differences in the voltammetric signal between the two scan rates. This trend is also observed for the 2.3 V potential width. The 3.5 V potential width, however, does show some small differences with the slower 20 mV s⁻¹ scan rate. Specifically, a slightly decreased peak dissolution current

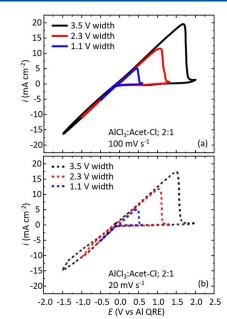


Figure 4. Overlay of cyclic voltammograms for the $AlCl_3$:Acet-Cl 2:1 formulation at 1.1, 2.3, and 3.5 V potential widths collected at (a) 100 and (b) 20 mV s⁻¹.

is observed, and the cathodic potential region shows signs of deviation from the linear response.

Interestingly, for the 100 mV s^{-1} traces, the cyclic voltammograms effectively build on top of each other as the potential width is increased. The i-E gradients in the anodic sweep remain identical, displaying the characteristic linear response, which yield similar (within error) conductivity values $(12.9 \pm 1.4, 12.5 \pm 1.4, \text{ and } 12.0 \pm 1.6 \text{ mS cm}^{-1}$ for the 1.1, 2.3, and 3.5 V potential widths, respectively). The linear response is largely retained at the 20 mV s⁻¹ scan rate for the 2.3 and 3.5 V potential widths, but they do show some minor deviations. As a result, this does have a quantifiable impact on the estimated conductivity values, i.e., 12.6 ± 1.4 , 11.5 ± 1.4 , and 10.8 \pm 1.5 mS cm⁻¹ for the 1.1, 2.3, and 3.5 V potential widths, respectively. It is interesting that we are able to push the limits of the i-E curve-fitting method to fit data over nearly a 3 volt potential range. Importantly, the change in potential excursion does not appear to alter the underlying (electro)chemistry we are observing but merely the extent to which it occurs.

Voltammetric Cycling Data. The CV cycle number was also examined to see if there was any effect. Data in Figure 5a show that there are no discernible differences from the 1st cycle (solid black trace) to the 30th cycle (dashed red trace) in the CV response associated with Al deposition/dissolution. The curve shape remains identical (i.e., the correlation coefficient between the two data sets is $R^2 = 0.999$). The *i*– *E* curve-fitting method was used to extract the conductivity, and we find over the 30 cycles that the conductivity remains constant at 12.9 mS cm⁻¹ (see Figure 5b). While this is not the focus of the present study, it presages well for future practical applications where this electrolyte may experience 100s to 1000s of cycles.

Lastly, it is worth commenting here on our reference electrode. It is accepted practice in the community to use a quasi-reference electrode that consists of a bare metal wire in non-aqueous RTIL/ILA/DES liquids. In Sections 3.4 to 3.6, we provide evidence throughout all the CV data that the Al

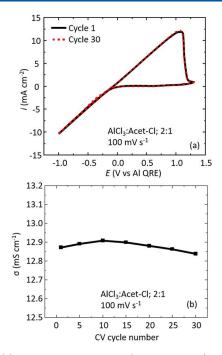


Figure 5. (a) Overlay of CV cycle 1 (solid black line) and cycle 30 (dashed red line) for the AlCl₃:Acet-Cl 2:1 formulation at a scan rate of 100 mV s⁻¹. (b) Corresponding conductivity data estimated from i-E curve fitting as a function of CV cycle number.

QRE is stable across multiple (repeat) measurements that have been carried out over months of use. The position of the i-Egradient on the potential axis does not impact the conductivity estimated from our method, but rather it is the magnitude of the gradient itself that is the principal factor in influencing the conductivity value.

iR **Compensation Effects.** The characteristic linear current-potential behavior was examined to see if *iR* effects were influencing the data. Cyclic voltammograms were corrected for ohmic drop by using the measured resistance for the AlCl₃:Acet-Cl 2:1 liquid (53.9 \pm 4.9 Ω). Figure 6

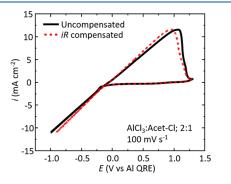


Figure 6. Overlay of cyclic voltammograms with uncompensated (solid black trace) and *iR*-compensated (dashed red trace) data for the AlCl₃:Acet-Cl 2:1 liquid at a scan rate of 100 mV s⁻¹.

overlays an *iR* uncompensated cyclic voltammogram (solid black trace) and an *iR*-compensated cyclic voltammogram (dashed red trace) at a scan rate of 100 mV s⁻¹. The *iR*-compensated cyclic voltammogram shows a very similar response to the uncompensated cyclic voltammogram, but the current-potential gradient (from -1 V to ca. +1 V) is slightly increased. We estimate conductivities of 13.0 and 14.3

mS cm⁻¹ for the uncompensated and *iR*-compensated data, respectively. While this is a quantifiable difference, the overall observation is not sufficient to suggest that the *iR* effects are giving rise to the characteristic linear current–potential behavior.

For this formulation, AlCl₃:Acet-Cl 2:1, we do not observe a peaked response for the electrochemical deposition of Al under the studied parameters. Therefore, under these experimental conditions, our data suggest that the Al deposition response is not limited by mass transport and diffusion of the electroactive species to/from the electrode surface.

Temperature-Dependent Conductivity. The temperature-dependent behavior of the AlCl₃:Acet-Cl 2:1 electrolyte was examined in a jacketed glass cell. The temperature was varied from 25 to 70 °C. The cyclic voltammograms in Figure 7a show similar behavior to what we have reported in previous

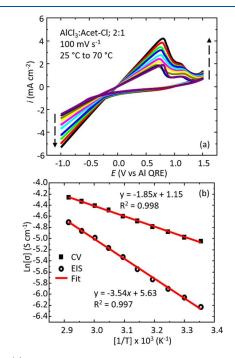


Figure 7. (a) Overlay of cyclic voltammograms measured from 25 to 70 °C at 100 mV s⁻¹. The dashed black arrows point toward increasing temperatures. (b) Arrhenius plots of temperature-dependent conductivity data from EIS data (empty black circles) and CV data (filled black squares). The best fit line is shown for the two data sets along with the line equation and R^2 coefficient.

sections, where a characteristic linear response is observed over a potential range in excess of 1.5 volts. As the temperature increases, the current response (and subsequently the i-Egradient, which informs on the conductivity) increases. One noticeable difference is the appearance of a second, smaller anodic oxidation peak around +1.2 V that follows the larger main Al dissolution peak. The additional dissolution peak could be a consequence from the formation of different morphological Al deposits (e.g., nanodeposits versus bulk metal deposits)^{61,62} or result from an alloy formed between Al and the Pt working electrode.⁵⁵ For the purposes of the discussion here, however, the second dissolution peak assignment is out of the scope of our work.

The energy of activation (E_a) can be estimated from temperature-dependent data. Figure 7b shows an Arrhenius plot of temperature-dependent conductivity data measured from the CV method and conductivity measured from EIS data. We find activation energies of 15 kJ mol⁻¹ for CV data and 30 kJ mol⁻¹ from EIS data. The difference in E_a values suggests that we may be probing different phenomena (on different timescales) between the two conductivity measurements. Nonetheless, these activation energies are consistent with previous reports for similar ILAs demonstrating Arrhenius behavior.^{17,29,35,42,44,63,64} Overall, we have demonstrated that the voltammetric-based conductivity measurement can be performed across a range of different measurement parameters.

Effect of the Lewis Acid:Base Ratio. In the previous sections, the focus was the effect of physical measurement parameters. In this section, we shift the focus to chemical parameters, namely, the composition of the liquid. To examine the effect of the mole ratio of LA:LB, we have prepared a range of liquids for testing. Specifically, we find that a liquid is formed within the range LA:LB of 1.50:1 to 2.50:1. Outside this range, a stable liquid is not formed. Data in Figure 8a show

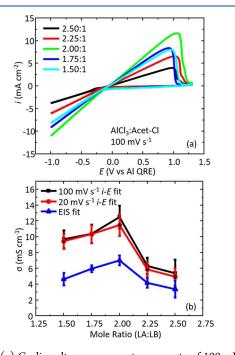


Figure 8. (a) Cyclic voltammograms at a scan rate of 100 mV s⁻¹ for different mole ratios of LA:LB for the AlCl₃:Acet-Cl system. (b) Overlays of the conductivity as a function of mole ratio for three different methods: 100 mV s⁻¹ *i*–*E* fitting (black squares), 20 mV s⁻¹ *i*–*E* fitting (red circles), and EIS fitting data (blue triangles). Error bars represent the standard deviation of 3 replicate measurements.

the voltammetric behavior of the liquids as a function of mole ratio. They all show similar peak shapes, yet very different

current magnitudes, but importantly, they all show the characteristic linear response suitable for i-E curve fitting. The 2.00:1 mole ratio shows the largest current signal and the highest i-E gradient. Moving higher or lower from this mole ratio, we find that the response decreases. A plot of the conductivity versus mole ratio is shown in Figure 8b, which highlights conductivity data measured from three methods: (i) i-E fitting at 100 mV s⁻¹, (ii) i-E fitting at 20 mV s⁻¹, and (iii) EIS fit data. Here, we see an increase in the conductivity from 1.50:1 to 2.00:1 followed by a decrease in conductivity toward higher mole ratios above 2.00:1. There are only minor differences between the voltammetric-based conductivity methods at the two different scan rates (as expected), and the EIS measured conductivity data trend mirrors that from the voltammetric method. The conductivities from the voltammetric-based method are a factor of two higher than those determined by the EIS-based method for all compositions studied. Earlier, we have speculated regarding the origins of these differences; however, the conductivity values are of the same order of magnitude and the compositional trends are the same, which provides validity to the underlying i-E curvefitting model. It is worth noting that any changes in the, e.g., Lewis acidity, viscosity, and electrode surface area during the measurement are not significant to impact the bulk conductivity we are extracting from this method.³⁵ Additionally, the small amount of impurities (1-2%); refer to Experimental Section) may impact the numerical value of conductivity for a liquid, but, as we demonstrate, it does not impact the validity of the i-E curve-fitting method we outline.

The majority of reports with similar chloroaluminate electrolytes find a related trend in conductivity as a function of mole ratio,^{17,29,31,44,64} where there is an optimal mole ratio to maximize conductivity for a particular electrolyte, yet some reports indicate that this trend may not always be the case.^{14,25,45} To the best of our knowledge, formulations of chloroaluminate liquids >2.00:1 are not common. Using our synthetic method, we have been able to generate liquids across a wide compositional range. These are highly Lewis acidic formulations with concentrations of [Al] ranging from 6.7 to 7.7 mol dm⁻³ for AlCl₃:Acet-Cl 1.50:1 and 2.50:1, respectively (for reference, the AlCl₃:EMIM-Cl 1.50:1 liquid has a [Al] of 5.7 mol dm^{-3}). It is worth noting, however, after sitting overnight at room temperature that the AlCl₃:Acet-Cl 2.50:1 formulation does solidify into small grainy/crystalline solids. This suggests that we could be making a supersaturated solution that eventually crystallizes upon cooling/sitting but could also indicate the formation of higher-order polymeric anions of the form $[Al_xCl_{3x+1}]^-$ as noted previously.^{25,65} The solution can be re-heated/stirred, but the electrochemical

Table 2. Tabulated Data for Several Different ILA Electrolytes Providing the Mole Ratio (LA:LB) and Conductivity (σ) as Measured from Voltammetric Fitting, Broadband EIS, and from a Commercial Conductivity Probe^{*a*}

electrolyte	mole ratio LA:LB	$\sigma/{\rm mS~cm^{-1}}$ voltammetric fitting (23 ± 3 °C)	$\sigma/{ m mS~cm^{-1}}$ broadband EIS (27 ± 2 °C)	$\sigma/mS \text{ cm}^{-1}$ commercial probe (25 ± 2 °C)	$\sigma/{ m mS~cm^{-1}}$ literature [ref.]
AlCl ₃ :Acet-Cl	2.0:1	12.5 ± 1.4	7.02 ± 0.63	5.8 ± 0.2	
AlCl ₃ :Acet-Cl	1.5:1	9.7 ± 1.1	4.65 ± 0.77	4.0 ± 0.4	9.7 (18 °C) ³⁵
AlCl3:EMIM-Cl	1.5:1	19.7	10.7	13.7	17 (25 °C) ⁴⁵
AlCl ₃ :acetamide	1.5:1	2.8	1.5	1.2	2.5 (40 °C) ³¹
AlCl ₃ :urea	1.5:1	0.77	0.63	0.49	1.15 (25 °C) ²⁵

^{*a*}Literature values are also provided.

performance is significantly diminished when retested. We do not find this behavior for the AlCl₃:Acet-Cl 2:1 formulation.

Lastly, we have also included viscosity data in ESI 3, Figure S3, for the mole ratio study. Here, we can see that the lowest viscosity is achieved from the AlCl₃:Acet-Cl 2:1 electrolyte with a value of 37 ± 4 cP. At lower and higher mole ratios than 2:1 (LA:LB), we find that the viscosity increases and the error (standard deviation) in the measurement increases as well. Nonetheless, the viscosity data are in agreement with the conductivity data, which show an inverse relationship with one another.

Applicability of the *i*–*E* Fitting Method with Various ILAs. In the final section, we have prepared a range of different liquids for testing against our voltammetric conductivity measurement method. Table 2 shows data for four different ILAs, i.e., two AlCl₃:Acet-Cl formulations, AlCl₃:acetamide, and AlCl₃:urea, alongside a more conventional IL electrolyte AlCl₃:EMIM-Cl. The Lewis acid:base mole ratio is listed for comparative purposes along with conductivity data measured from the voltammetric-based method (potential scan rate of 100 mV s⁻¹), broadband EIS, and a commercial probe. Literature values are also provided with the corresponding measurement temperature. The CV data are shown in ESI 4, Figure S4, and demonstrates the characteristic linear *i*–*E* response suitable for data fitting for all liquids.

Interestingly, there are differences in the conductivity measured between the techniques for the same liquid, which indicates that to some extent, the value is dependent on the method. However, the difference is less pronounced when comparing the EIS and commercial probe data. This is probably because these two techniques are based on the same impedance measurement principle. Importantly, the voltammetric-based conductivity measurement method does estimate reasonable conductivity values, even when compared to literature values. We may in fact expect some differences in the conductivity values measured in our work compared to literature values simply as a result of the different synthetic methods employed. Our liquids are not prepared under rigorous inert atmospheric conditions (such as provided with a glovebox), and we utilize heating during the reaction. There may also be some minor variability between our work and previously published data due to different purities of the salts used and different measurement temperatures. Nonetheless, our novel voltammetric-based conductivity measurement method provides a reasonable estimation of ionic conductivity for chloroaluminate electrolytes without the need for an additional measurement or sensor. Lastly, this work has highlighted the significant improvement in conductivity achieved with the AlCl₃:Acet-Cl 2:1 formulation, which is a substantial improvement in electrolyte development for Al-ion battery materials.

CONCLUSIONS

In this work, we have demonstrated a novel, simple, and effective method for extracting the conductivity of ILA electrolytes based on fitting the characteristic linear portion of the voltammogram. The new method is benchmarked to data from both broadband impedance-based measurements and that from a commercial conductivity probe. The data derived from voltammetric curve fitting gives values of conductivity that are close to a factor of two larger than the impedance-based measurements but are nevertheless in close agreement with other literature values. This may be the result

of differences in the response times of molecular dynamics imposed by DC and AC methods. The measured values of conductivity for all methods are of the same order of magnitude, and the new method predicts similar conductivity trends with respect to compositional data. We observe no dependence on the potential scanning rate and CV cycle number. The absolute values of the cathodic and anodic potential limits examined and uncompensated iR effects only have a minor influence on the estimated conductivity. Arrhenius behavior is observed with temperature-dependent conductivity data, and we find activation energies comparable to literature sources. We also show that the voltammetricbased method is applicable to measure the conductivity of a range of other ILAs. Another significant result from this work is the high conductivity obtained with the AlCl₃:Acet-Cl 2:1 formulation at ca. 7 mS cm⁻¹. This represents a substantial improvement over conductivities from urea- and acetamidebased electrolytes. Lastly, it is important to reiterate that the amidine-based salts are a much more cost-effective option compared to current state-of-the-art imidazolium-based salts, which is important when considering scale-up of these electrolytes for Al-ion battery applications. Future work will examine the time-dependent rheological performance of the AlCl₃:Acet-Cl 2:1 electrolyte and its electroplating characteristics.

ASSOCIATED CONTENT

Data Availability Statement

Data will be made available on request.

Supporting Information

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/acs.jpcc.3c02302.

Electrochemical cells, EIS conductivity cell calibration, mole ratio-dependent viscosity data, and demonstration of the i-E fitting method for different ILAs (PDF)

AUTHOR INFORMATION

Corresponding Author

Anthony J. Lucio – Centre for Sustainable Materials Processing, School of Chemistry, University of Leicester, Leicester LE1 7RH, U.K.; o orcid.org/0000-0003-0034-4914; Email: anthonyluciophd@outlook.com

Authors

- Iwan Sumarlan Centre for Sustainable Materials Processing, School of Chemistry, University of Leicester, Leicester LE1 7RH, U.K.; Department of Chemistry, University of Mataram, Mataram 83115 Lombok, Indonesia
- Elena Bulmer Centre for Sustainable Materials Processing, School of Chemistry, University of Leicester, Leicester LE1 7RH, U.K.

Igor Efimov – Department of Chemical and Biological Engineering, University of Sheffield, Sheffield S1 3JD, U.K.

- **Stephen Viles** Centre for Sustainable Materials Processing, School of Chemistry, University of Leicester, Leicester LE1 7RH, U.K.
- A. Robert Hillman Centre for Sustainable Materials Processing, School of Chemistry, University of Leicester, Leicester LE1 7RH, U.K.
- Christopher J. Zaleski Biotechnology Group, School of Chemistry, University of Leicester, Leicester LE1 7RH, U.K.

Karl S. Ryder – Centre for Sustainable Materials Processing, School of Chemistry, University of Leicester, Leicester LE1 7RH, U.K.; © orcid.org/0000-0003-2803-6884

Complete contact information is available at: https://pubs.acs.org/10.1021/acs.jpcc.3c02302

Notes

The authors declare no competing financial interest.

A.J.L.: conceptualization, methodology, validation, formal analysis, investigation, writing-original draft, writing-review and editing, visualization, supervision, and project administration. I.S.: methodology, validation, formal analysis, investigation, and visualization. E.B.: methodology, validation, formal analysis, investigation, and visualization. I.E.: conceptualization, methodology, formal analysis, and writing-review and editing. S.V.: conceptualization, methodology, resources, writing-review and editing, supervision, project administration and funding acquisition. C.J.Z.: conceptualization, methodology, resources, writing-review and editing, supervision, project administration project administration, and funding acquisition. I.S. and E.B. contributed equally.

ACKNOWLEDGMENTS

The authors would like to thank the European Commission for support of the H2020-FETOPEN-1-2016-2017 (G.A. No. 766581; SALBAGE) and FETPROACT-EIC-06-2019 (G.A. No. 951902; AMAPOLA) funded projects. IS would like to acknowledge the funding from the Directorate General of Higher Education, Research, and Technology. Ministry of Education, Culture, Research, and Technology of The Republic of Indonesia.

REFERENCES

(1) Renné, D. S. Progress, opportunities and challenges of achieving net-zero emissions and 100% renewables. *Sol. Compass* **2022**, *1*, No. 100007.

(2) Obobisa, E. S. Achieving 1.5 $^{\circ}$ C and net-zero emissions target: The role of renewable energy and financial development. *Renewable Energy* **2022**, *188*, 967–985.

(3) Anika, O. C.; Nnabuife, S. G.; Bello, A.; Okoroafor, R. E.; Kuang, B.; Villa, R. Prospects of Low and Zero-Carbon Renewable fuels in 1.5-Degree Net Zero Emission Actualisation by 2050: A Critical Review. *Carbon Capture Sci. Technol.* **2022**, *5*, No. 100072.

(4) Nitta, N.; Wu, F.; Lee, J. T.; Yushin, G. Li-ion battery materials: present and future. *Mater. Today* **2015**, *18*, 252–264.

(5) Muldoon, J.; Bucur, C. B.; Gregory, T. Quest for Nonaqueous Multivalent Secondary Batteries: Magnesium and Beyond. *Chem. Rev.* **2014**, *114*, 11683–11720.

(6) Grosjean, C.; Miranda, P. H.; Perrin, M.; Poggi, P. Assessment of world lithium resources and consequences of their geographic distribution on the expected development of the electric vehicle industry. *Renewable Sustainable Energy Rev.* **2012**, *16*, 1735–1744.

(7) Leisegang, T.; Meutzner, F.; Zschornak, M.; Münchgesang, W.; Schmid, R.; Nestler, T.; Eremin, R. A.; Kabanov, A. A.; Blatov, V. A.; Meyer, D. C. The Aluminum-Ion Battery: A Sustainable and Seminal Concept? *Front. Chem.* **2019**, *7*, 268.

(8) Tu, J.; Song, W.-L.; Lei, H.; Yu, Z.; Chen, L.-L.; Wang, M.; Jiao, S. Nonaqueous Rechargeable Aluminum Batteries: Progresses, Challenges, and Perspectives. *Chem. Rev.* **2021**, *121*, 4903–4961.

(9) Hu, Z.; Zhang, H.; Wang, H.; Zhang, F.; Li, Q.; Li, H. Nonaqueous Aluminum Ion Batteries: Recent Progress and Prospects. *ACS Mater. Lett.* **2020**, *2*, 887–904. (10) Zhang, Y.; Liu, S.; Ji, Y.; Ma, J.; Yu, H. Emerging Nonaqueous Aluminum-Ion Batteries: Challenges, Status, and Perspectives. *Adv. Mater.* **2018**, *30*, No. 1706310. , 10.1002/adma.201706310 (accessed 10 Oct, 2022).

(11) Schoetz, T.; de Leon, C. P.; Ueda, M.; Bund, A. Perspective— State of the Art of Rechargeable Aluminum Batteries in Non-Aqueous Systems. J. Electrochem. Soc. **2017**, *164*, A3499–A3502.

(12) Kravchyk, K. V.; Kovalenko, M. V. Aluminum electrolytes for Al dual-ion batteries. *Commun. Chem.* **2020**, *3*, 120.

(13) Ma, D.; Yuan, D.; Ponce de León, C.; Jiang, Z.; Xia, X.; Pan, J. Current Progress and Future Perspectives of Electrolytes for Rechargeable Aluminum-Ion Batteries. *Energy Environ. Mater.* **2023**, *6*, No. e12301. , 10.1002/eem2.12301 (accessed 22 Feb, 2023).

(14) Ng, K. L.; Lu, Z.; Wang, Y.; Singh, C. V.; Azimi, G. Fundamental Insights into Electrical and Transport Properties of Chloroaluminate Ionic Liquids for Aluminum-Ion Batteries. *J. Phys. Chem.* C 2021, 125, 15145–15154.

(15) Kravchyk, K. V.; Seno, C.; Kovalenko, M. V. Limitations of Chloroaluminate Ionic Liquid Anolytes for Aluminum–Graphite Dual-Ion Batteries. *ACS Energy Lett.* **2020**, *5*, 545–549.

(16) Böttcher, R.; Ispas, A.; Bund, A. Anodic dissolution of aluminum and anodic passivation in [EMIm]Cl-based ionic liquids. *Electrochem. Commun.* **2020**, *115*, No. 106720.

(17) Ferrara, C.; Dall'Asta, V.; Berbenni, V.; Quartarone, E.; Mustarelli, P. Physicochemical Characterization of AlCl3–1-Ethyl-3methylimidazolium Chloride Ionic Liquid Electrolytes for Aluminum Rechargeable Batteries. J. Phys. Chem. C 2017, 121, 26607–26614.

(18) Wang, C.; Creuziger, A.; Stafford, G.; Hussey, C. L. Anodic Dissolution of Aluminum in the Aluminum Chloride-1-Ethyl-3-methylimidazolium Chloride Ionic Liquid. *J. Electrochem. Soc.* 2016, 163, H1186-H1194.

(19) Lin, M.-C.; Gong, M.; Lu, B.; Wu, Y.; Wang, D.-Y.; Guan, M.; Angell, M.; Chen, C.; Yang, J.; Hwang, B.-J.; et al. An ultrafast rechargeable aluminium-ion battery. *Nature* **2015**, *520*, 324–328.

(20) Bakkar, A.; Neubert, V. A new method for practical electrodeposition of aluminium from ionic liquids. *Electrochem. Commun.* 2015, *51*, 113–116.

(21) Liu, Q. X.; Zein El Abedin, S.; Endres, F. Electrodeposition of Nanocrystalline Aluminum: Breakdown of Imidazolium Cations Modifies the Crystal Size. *J. Electrochem. Soc.* **2008**, *155*, D357.

(22) https://www.sigmaaldrich.com/GB/en/product/aldrich/ 742872. Sigma-Aldrich, (accessed 10 Oct, 2022).

(23) Malik, M.; Ng, K. L.; Azimi, G. Physicochemical characterization of AlCl3-urea ionic liquid analogs: Speciation, conductivity, and electrochemical stability. *Electrochim. Acta* **2020**, *354*, No. 136708.

(24) CvetkoviĆ, V. S.; VukiĆEviĆ, N. M.; JoviĆEviĆ, N.; StevanoviĆ, J. S.; JoviĆEviĆ, J. N. Aluminium electrodeposition under novel conditions from AlCl3–urea deep eutectic solvent at room temperature. *Trans. Nonferrous Met. Soc. China* **2020**, *30*, 823– 834.

(25) Angell, M.; Zhu, G.; Lin, M.-C.; Rong, Y.; Dai, H. Ionic Liquid Analogs of AlCl3 with Urea Derivatives as Electrolytes for Aluminum Batteries. *Adv. Funct. Mater.* **2020**, *30*, No. 1901928. , 10.1002/ adfm.201901928 (accessed 13 Mar, 2021).

(26) Jiao, H.; Wang, C.; Tu, J.; Tian, D.; Jiao, S. A rechargeable Alion battery: Al/molten AlCl3-urea/graphite. *Chem. Commun.* **2017**, *53*, 2331-2334.

(27) Angell, M.; Pan, C.-J.; Rong, Y.; Yuan, C.; Lin, M.-C.; Hwang, B.-J.; Dai, H. High Coulombic efficiency aluminum-ion battery using an AlCl3-urea ionic liquid analog electrolyte. *Proc. Natl. Acad. Sci. U. S. A.* **2017**, *114*, 834.

(28) Abbott, A. P.; Harris, R. C.; Hsieh, Y.-T.; Ryder, K. S.; Sun, I. W. Aluminium electrodeposition under ambient conditions. *Phys. Chem. Chem. Phys.* **2014**, *16*, 14675–14681.

(29) Paterno, D.; Rock, E.; Forbes, A.; Iqbal, R.; Mohammad, N.; Suarez, S. Aluminum ions speciation and transport in acidic deep eutectic AlCl3 amide electrolytes. J. Mol. Liq. **2020**, 319, No. 114118. (30) Canever, N.; Bertrand, N.; Nann, T. Acetamide: a low-cost alternative to alkyl imidazolium chlorides for aluminium-ion batteries. *Chem. Commun.* **2018**, *54*, 11725–11728.

(31) Liu, C.; Chen, W.; Wu, Z.; Gao, B.; Hu, X.; Shi, Z.; Wang, Z. Density, viscosity and electrical conductivity of AlCl3-amide ionic liquid analogues. *J. Mol. Liq.* **2017**, *247*, 57–63.

(32) Hu, P.; Zhang, R.; Meng, X.; Liu, H.; Xu, C.; Liu, Z. Structural and Spectroscopic Characterizations of Amide–AlCl3-Based Ionic Liquid Analogues. *Inorg. Chem.* **2016**, *55*, 2374–2380.

(33) Li, M.; Gao, B.; Liu, C.; Chen, W.; Shi, Z.; Hu, X.; Wang, Z. Electrodeposition of aluminum from AlCl3/acetamide eutectic solvent. *Electrochim. Acta* **2015**, *180*, 811–814.

(34) Abood, H. M. A.; Abbott, A. P.; Ballantyne, A. D.; Ryder, K. S. Do all ionic liquids need organic cations? Characterisation of [AlCl2nAmide]+AlCl4- and comparison with imidazolium based systems. *Chem. Commun.* **2011**, *47*, 3523–3525.

(35) Lucio, A. J.; Efimov, I.; Efimov, O. N.; Zaleski, C. J.; Viles, S.; Ignatiuk, B. B.; Abbott, A. P.; Hillman, A. R.; Ryder, K. S. Amidinebased ionic liquid analogues with AlCl3: a credible new electrolyte for rechargeable Al batteries. *Chem. Commun.* **2021**, *57*, 9834–9837.

(36) Gregorio, V.; García, N.; Tiemblo, P. Ionic Conductivity Enhancement in UHMW PEO Gel Electrolytes Based on Room-Temperature Ionic Liquids and Deep Eutectic Solvents. *ACS Appl. Polym. Mater.* **2022**, *4*, 2860–2870.

(37) Sun, X.-G.; Fang, Y.; Jiang, X.; Yoshii, K.; Tsuda, T.; Dai, S. Polymer gel electrolytes for application in aluminum deposition and rechargeable aluminum ion batteries. *Chem. Commun.* **2016**, *52*, 292–295.

(38) Katayama, Y. Chapter 9: Electrodeposition of Metals in Ionic Liquids; John Wiley & Sons, 2005.

(39) Zhao, Y.; VanderNoot, T. J. Electrodeposition of aluminium from nonaqueous organic electrolytic systems and room temperature molten salts. *Electrochim. Acta* **1997**, *42*, 3–13.

(40) Ng, K. L.; Malik, M.; Buch, E.; Glossmann, T.; Hintennach, A.; Azimi, G. A low-cost rechargeable aluminum/natural graphite battery utilizing urea-based ionic liquid analog. *Electrochim. Acta* **2019**, *327*, No. 135031.

(41) Pulletikurthi, G.; Bödecker, B.; Borodin, A.; Weidenfeller, B.; Endres, F. Electrodeposition of Al from a 1-butylpyrrolidine-AlCl3 ionic liquid. *Prog. Nat. Sci.: Mater. Int.* **2015**, *25*, 603–611.

(42) Jiang, T.; Chollier Brym, M. J.; Dubé, G.; Lasia, A.; Brisard, G. M. Electrodeposition of aluminium from ionic liquids: Part II - studies on the electrodeposition of aluminum from aluminum chloride (AICl3) - trimethylphenylammonium chloride (TMPAC) ionic liquids. *Surf. Coat. Technol.* **2006**, *201*, 10–18.

(43) Lai, P. K.; Skyllas-Kazacos, M. Aluminium deposition and dissolution in aluminium chloride—n-butylpyridinium chloride melts. *Electrochim. Acta* **1987**, *32*, 1443–1449.

(44) Elterman, V. A.; Shevelin, P. Y.; Yolshina, L. A.; Borozdin, A. V. Physicochemical characteristics of 1-ethyl- and 1-butyl-3-methylimidazolium chloroaluminate ionic liquids. *J. Mol. Liq.* **2022**, *364*, No. 120061.

(45) Zhu, G.; Angell, M.; Pan, C.-J.; Lin, M.-C.; Chen, H.; Huang, C.-J.; Lin, J.; Achazi, A. J.; Kaghazchi, P.; Hwang, B.-J.; et al. Rechargeable aluminum batteries: effects of cations in ionic liquid electrolytes. *RSC Adv.* **2019**, *9*, 11322–11330.

(46) Shinde, P.; Ahmed, A. N.; Nahian, M. K.; Peng, Y.; Reddy, R. G. Conductivity of 1-Ethyl-3-Methylimidazolium Chloride (EMIC) and Aluminum Chloride (AlCl3) Ionic Liquids at Different Temperatures and AlCl3 Mole Fractions. *ECS Trans.* **2020**, *98*, 129–139.

(47) Böttcher, R.; Ispas, A.; Bund, A. Determination of transport parameters in [EMIm]Cl-based Ionic Liquids – Diffusion and electrical conductivity. *Electrochim. Acta* **2021**, *366*, No. 137370.

(48) Elia, G. A.; Hoeppner, K.; Hahn, R. Comparison of Chloroaluminate Melts for Aluminum Graphite Dual-Ion Battery Application. *Batteries Supercaps* **2021**, *4*, 368–373. (accessed 04 Nov, 2022).

(49) Puttaswamy, R.; Mondal, C.; Mondal, D.; Ghosh, D. An account on the deep eutectic solvents-based electrolytes for rechargeable batteries and supercapacitors. *Sustainable Mater. Technol.* **2022**, 33, No. e00477.

(50) Abu Nayem, S. M.; Ahmad, A.; Shaheen Shah, S.; Saeed Alzahrani, A.; Saleh Ahammad, A. J.; Aziz, M. A. High Performance and Long-cycle Life Rechargeable Aluminum Ion Battery: Recent Progress, Perspectives and Challenges. *Chem. Rec.* **2022**, *22*, No. e202200181. (accessed 20 Oct, 2022).

(51) Di Pietro, M. E.; Mele, A. Deep eutectics and analogues as electrolytes in batteries. *J. Mol. Liq.* **2021**, 338, No. 116597.

(52) Cobb, S. J.; Macpherson, J. V. Enhancing Square Wave Voltammetry Measurements via Electrochemical Analysis of the Non-Faradaic Potential Window. *Anal. Chem.* **2019**, *91*, 7935–7942.

(53) Lucio, A. J.; Shaw, S. K. Effects and controls of capacitive hysteresis in ionic liquid electrochemical measurements. *Analyst* **2018**, *143*, 4887–4900.

(54) Ispas, A.; Wolff, E.; Bund, A. An Electrochemical Quartz Crystal Microbalance Study on Electrodeposition of Aluminum and Aluminum-Manganese Alloys. *J. Electrochem. Soc.* **2017**, *164*, H5263–H5270.

(55) Giridhar, P.; Zein El Abedin, S.; Endres, F. Electrodeposition of aluminium from 1-butyl-1-methylpyrrolidinium chloride/AlCl3 and mixtures with 1-ethyl-3-methylimidazolium chloride/AlCl3. *Electrochim. Acta* **2012**, *70*, 210–214.

(56) Bard, A. J.; Faulkner, L. R. Electrochemical Methods: Fundamentals and Applications; Wiley, 2001.

(57) Orazem, M. E.; Tribollet, B. Electrochemical Impedance Spectroscopy; Wiley, 2017.

(58) Macdonald, J. R.; Schoonman, J.; Lehnen, A. P. Applicability and power of complex nonlinear least squares for the analysis of impedance and admittance data. *J. Electroanal. Chem. Interfacial Electrochem.* **1982**, *131*, 77–95.

(59) Schoetz, T.; Xu, J. H.; Messinger, R. J. Ionic Liquid Electrolytes with Mixed Organic Cations for Low-Temperature Rechargeable Aluminum–Graphite Batteries. *ACS Appl. Energy Mater.* **2023**, *6*, 2845–2854.

(60) Bonanos, N.; Steele, B. C. H.; Butler, E. P.; Macdonald, J. R.; Johnson, W. B.; Worrell, W. L.; Niklasson, G. A.; Malmgren, S.; Strømme, M.; Sundaram, S. K.; et al. Applications of Impedance Spectroscopy. In *Impedance Spectroscopy*, 2018; pp 175–478.

(61) Abbott, A. P.; Barron, J. C.; Frisch, G.; Ryder, K. S.; Silva, A. F. The effect of additives on zinc electrodeposition from deep eutectic solvents. *Electrochim. Acta* **2011**, *56*, 5272–5279.

(62) Smith, E. L.; Barron, J. C.; Abbott, A. P.; Ryder, K. S. Time Resolved in Situ Liquid Atomic Force Microscopy and Simultaneous Acoustic Impedance Electrochemical Quartz Crystal Microbalance Measurements: A Study of Zn Deposition. *Anal. Chem.* **2009**, *81*, 8466–8471.

(63) Wang, H.; Gu, S.; Bai, Y.; Chen, S.; Zhu, N.; Wu, C.; Wu, F. Anion-effects on electrochemical properties of ionic liquid electrolytes for rechargeable aluminum batteries. *J. Mater. Chem. A* **2015**, *3*, 22677–22686.

(64) Hsu, H.-Y.; Yang, C.-C. Conductivities of Room Temperature Molten Salts Containing AlCl3, Measured by a Computerized Direct Current Method. *Z. Naturforsch. A* **2001**, *56*, 670–676. (accessed 08 Nov, 2022).

(65) Dymek, C. J.; Wilkes, J. S.; Einarsrud, M. A.; Øye, H. A. Spectral identification of Al3Cl10- in 1-methyl-3-ethylimidazolium chloroaluminate molten salt. *Polyhedron* **1988**, *7*, 1139–1145.