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1 Evaluation of physicochemical properties of honey powder using rice and pea proteins as

carriers

- 3 Taíse Toniazzo^a, Mar Collado-González^{b1}, Carmen Cecília Tadini^a*, Alan Mackie^b
- 4 ^aUniversidade de São Paulo, Escola Politécnica, Dept. of Chemical Eng., Main *Campus*, SP, Brazil.
- 5 Universidade de São Paulo, FoRC/NAPAN Food Research Center
- ⁶ ^bSchool of Food Science and Nutrition, University of Leeds, L82 9JT, UK.
- 7 *Corresponding author at the University of São Paulo, Escola Politécnica, Dept. of Chemical Eng.,
- 8 Main Campus, Butantã, São Paulo, SP 05508-010, Brazil.
- 9 E-mail address: catadini@usp.br (C.C. Tadini).

¹ Present address: Department of Cell Biology and Histology, Faculty of Biology, Campus de Espinardo, University of Murcia, 30100, Murcia, Spain.

10 ABSTRACT

Honey is a special product widely appreciated because of its peculiar flavor and aroma as well as its 11 12 beneficial effects on health due to its constituents. However, the use of honey in its natural form can 13 present several disadvantages to the food industry because of its high viscosity and density. This work aimed to obtain honey powder using rice, pea, or a mixture of both proteins as carriers by 14 15 spray drying and to characterize physiochemically. Also, the mass balance was performed to evaluate changes in humidity and temperature that occurred by the drying air during the process. 16 17 The honey showed acceptable physicochemical parameters by the legislation of honey quality 18 control in regard to color (143.43 \pm 4.34) mm Pfund, free acidity (46.41 \pm 0.53) meq/kg, pH (3.73 \pm 19 0.03), fructose content (46.52 \pm 0.56) g/100 g and glucose content (35.88 \pm 0.16) g/100 g, which leads to the production of honey powder. Among the carriers tested, the honey powder using rice 20 21 protein achieved the highest powder recovery yield at (64.88 ± 0.64) %. The physicochemical 22 properties were evaluated and the phenolic compounds were not negatively affected by spray drying 23 conditions, maintaining a value of gallic acid equivalent (GAE) content at (301.31 ± 20.95) mg/kg 24 of honey. Therefore, this work shows honey as an alternative food ingredient in powdered form, including the growing market for using alternative protein. 25

26 *Keywords*: honey; spray drying; microparticles; mass balance; plant protein; phenolic compounds.

27 **1. Introduction**

28 Honey is a natural product that has been considered an important carbohydrate source since the beginning of humanity (Bogdanov et al., 2008; Crane, 1975). Throughout human history, honey has 29 30 been used as a nutrient and for medical purposes (Bogdanov et al., 2008; Jones, 2009), and it is considered a natural preservative with antimicrobial properties due to its high osmolarity (Molan, 31 32 1992), acidity (Yatsunami & Echigo, 1984) and hydrogen peroxide produced by the glucose oxidase of honey (Alvarez-Suarez et al., 2010; Bogdanov, 1997; Samborska, 2019; White, Subers & 33 34 Schepartz, 1963;). 35 Honey composition has been shown to act synergistically and may contribute to several health benefits (Samat et al., 2018; Vică et al., 2021; Zainol, Yusoff & Yusof, 2013). Honey is mainly 36 composed of sugar (76 g/100 g), fructose being the major monosaccharide, and water (less than 20 37 38 g/100 g) (Afrin et al., 2020; Martinotti & Ranzato, 2018; White, 1979;). Honey also contains 39 minerals, vitamins, proteins, amino acids, and enzymes (White, 1979). The minor constituents are the phenolic acids and flavonoids (Dimitrova, Gevrenova & Anklam, 2007; Martos, Ferreres & 40 41 Yao, 2000) that have been shown to provide biological effects, such as antimicrobial (Estevinho et al., 2008), antioxidant (Biluca et al., 2020), anti-inflammatory (Sun et al., 2020), and antimutagenic 42

43 (Wang, Andrae & Engeseth, 2002).

44 The commercial production of honey in the world is approximately 1.2 million tons per year

45 (Bogdanov et al., 2008), suggesting an average global consumption of 0.64 g/day and the largest

46 consumption per capita is in the Central African Republic, which is 9.62 g/day (FAO, 2019b).

However, this is still a low value compared to the global sugar consumption, which is expected to increase to 65.20 g/day in 2027 (FAO, 2019a), exceeding the value of 50 g/day of sugar, which is the amount recommended by the World Health Organization to maintain healthy body weight and reduce the risks of noncommunicable diseases (WHO, 2015; WHO, 2021). Thus, to promote the

51 consumption of nutritional foods, it is important to increase the use of honey as an ingredient.

52 However, developing food products using honey can be a challenge due to its physical properties,

53	such as high viscosity and density (Cui et al., 2008; Hebbar, Rastogi, & Subramanian, 2008).
54	Additionally, honey is a supersaturated sugar solution, and can crystalize spontaneously during
55	storage, decreasing consumer acceptance (Cui et al., 2008; Hebbar, Rastogi, & Subramanian, 2008;
56	Samborska, 2019). Therefore, to significantly minimize such difficulties, an alternative is to use
57	honey in a powder form.
58	Several techniques are used for honey drying, such as spray drying (Nurhadi et al., 2012;
59	Samborska, Gajek, & Kamińska-Dwórznicka, 2015; Samborska, Sokołowska & Szulc, 2017;
60	Suhag, Nayik & Nanda, 2016), vacuum drying (Devi et al., 2016; Nurhadi et al., 2012), microwave
61	vacuum drying (Cui et al., 2008), vacuum foam drying (Sramek et al., 2016) and freeze-drying
62	(Sramek et al., 2016). However, spray drying is the usual technique applied to dry honey
63	(Samborska, 2019). It has some advantages because the food industry is used to convert liquid or
64	paste food into powder. Spray drying is characterized as a continuous method with a short
65	processing time, resulting in a product with low water activity. During the drying of the particles,
66	the high mass and heat transfer of the water allow for maintaining a low temperature, thus
67	permitting heat sensitive compounds to dry without excessively affecting their quality (Ré, 1998).
68	The efficiency is also comparable to other types of dryers and the process can be considered low-
69	cost (Filková & Mujumdar, 1995). However, drying honey can be a challenge due to its sugar-rich
70	composition causing it to remain as a syrup and stick to the drying chamber walls (Bhandari &
71	Howes, 1999), decreasing the powder recovery yield or not generating a powder (Samborska,
72	Gajek, & Kamińska-Dwórznicka, 2015). This phenomenon called the stickiness problem occurs
73	because of the low glass transition temperature (T_g) of monosaccharides: 31 °C for anhydrous
74	glucose and 5 °C for anhydrous fructose (Bhandari & Howes, 1999; Samborska et al., 2019). To
75	overcome this problem, it is necessary to add high molecular weight drying agents, which can
76	modify the drying process due to their high T_g (Samborska, Gajek, & Kamińska-Dwórznicka,
77	2015).

78 Polysaccharides are commonly used as carriers for dry honey, for example, maltodextrin and gum 79 arabic (Devi et al., 2016; Nurhadi et al., 2012; Samborska, Gajek, & Kamińska-Dwórznicka, 2015; Samborska et al., 2019; Suhag, Nayik, & Nanda, 2016). Plant protein derived from rice and pea has 80 81 already shown important functional properties strongly necessary to act as a carrier during the honey drying process, such as foaming stability and emulsifying capacity (Nesterenko et al., 2013). 82 83 In addition, rice belongs to the most important cereal crop in the world, and it can be a potential source of inexpensive high-quality proteins (Hamada, 2000; Saunders, 1990). Thus, plant protein 84 (rice protein and pea protein) was used as a carrier in this work, since it has gained significant 85 interest and reflects the current "green" trends in the food industry (Moser et al., 2020; Nesterenko 86 et al., 2013). Furthermore, the pea protein used in this study was micronized, which consists of a 87 technique applied to reduce the particle size at the micrometer level, resulting in changes in 88 89 structural, physicochemical, and functional properties. This size reduction is important to promote 90 functional and physicochemical properties, such as water retention capacity, swelling capacity, and solubility (Dhiman & Prabhakar, 2021). In this context, this study aims to develop honey powder by 91 92 spray drying with isolated rice protein or isolated micronized pea protein, or a mixture of both. To 93 the best of our knowledge, the use of pea protein to obtain honey powder by spray drying has not been explored previously in the literature. 94

95 **2. Materials and Methods**

96 2.1 Materials

Rowse honey (ETHIOPIAN honey) was purchased from a local market (Leeds, UK). Isolated rice
protein (ORYZAPRO) and micronized pea protein, used as carriers, were donated by Healy Group,

99 Leicestershire, UK. The protein content of the rice protein was (80.6 g/100 g) in dry matter.

100 Micronized pea protein was extracted from yellow peas, and the protein content was (84 g/100 g) in

101 dry matter, characterized by low viscosity, and excellent emulsifying properties. It is worth

102 mentioning that the tests were performed with pea protein without micronization. Therefore, it was

103 not possible to obtain a proper dispersion for the atomization. Ultrapure water (Direct Q3[®] system,

Millipore, USA) was used throughout the experiments. All the chemicals used were of analyticalgrade.

106 **2.2 Methods**

107 2.2.1 Physicochemical characterization of honey

108 2.2.1.1 Color

109 The color was determined by spectrophotometry (Cecil, CE 3021, 3000 series, Cecil Instruments,

110 England), according to Ferreira et al. (2009). For that purpose, (50 g/100 g) honey solutions with

111 ultrapure water were prepared and the absorbance value was measured at 635 nm. The honey was

112 classified according to the Pfund scale in millimeters after the conversion of the absorbance values,

113 according to White et al. (1984), using Eq. 1:

114
$$mmPfund = -38.70 + 371.39 \times Abs$$
 (1)

According to USDA classification (USDA, 1985), the color mm Pfund scale ranges from 8 or less
to over 114, classified as water (lighter in color) to dark (amber in color), respectively.

117 2.2.1.2 Free acidity and pH

The acidity of honey is caused by organic acids (tartaric, citric, oxalic, acetic, etc.), both from nectar 118 119 and bee secretions (Yadata, 2014). Free acidity was determined by potentiometric titration according to the International Honey Commission (2009). Briefly, 10 g of honey was dissolved in 120 50 mL of ultrapure water, the electrode of the pH meter (Mettler Toledo, SevenCompact S220, 121 Switzerland) was inserted into the solution and, under magnetic stirring, the solution was titrated 122 with NaOH (0.05 N) up to pH 8.5. The result was expressed by milliequivalents/kg of honey. The 123 pH of honey was measured using a pH meter (Mettler Toledo, SevenCompact S220, Switzerland). 124 125 2.2.1.3 *Total soluble solid content*

126 The total soluble solid content was determined using an optical handheld refractometer (Bellingham

127 & Stanley Ltd. Tunbridge Wells, UK). Honey was homogenized and submitted to a temperature of

128 50 °C to prevent any sugar crystals. The samples were analyzed after cooling the temperature to 20

¹²⁹ °C. The results were expressed as grams of total soluble solid content g/100 g of honey.

The honey sugar content was analyzed by HPLC, with an ELSD evaporative light scattering 131 detector (Shimadzu Prominence, Japan), according to Bogdanov et al. (1999) and the International 132 133 Honey Commission, (2009), with some modifications. Honey was diluted at 6.25 mg/mL, using methanol at a concentration of 25 mL/100 mL, and filtered in a MILIPPORE membrane of 0.45 134 um. The separation of sugar was performed in a Grace Davison Prevail Carbohydrate Es column 135 $(5 \,\mu\text{m}, 250 \,\text{mm} \times 4.6 \,\text{mm})$, using acetonitrile as mobile phase B and ultrapure water (Direct Q3[®]) 136 137 system, Millipore, USA) as mobile phase A. The mobile phases were delivered at 1 mL/min in a 138 binary gradient mode: (0.01-15 min: from 75 % to 60 % of B; 15.00-15.01 min: from 60 % to 75 % of B; 15.01-20 min: 75 % of B). Measurements were carried out at 25 °C, and the sample injection 139 volume was 10 µL. Sugar content quantifications were achieved in triplicate by the standard curve 140 of glucose ($Y = 2 \times 10^6 x - 10^6$, $r^2 = 0.9991$, retention time: 6.09 min), fructose ($Y = 2 \times 10^6 x - 10^6$, 141 $r^2 = 0.9992$, retention time: 6.87 min), and sucrose ($Y = 2 \times 10^6 x - 691932$, $r^2 = 0.9992$, retention 142 143 time: 7.84 min). The sugar content was expressed as grams of sugars (fructose, glucose, and

144 sucrose) per 100 g of honey.

145 2.2.1.5 Total phenolic compounds (TPC) in honey

146 The TPC was analyzed according to Dzugan et al. (2018) and Piljac-Žegarac, Stipčević & Belščak (2009), with some modifications. Honey solutions at (50, 25, and 12) mg/mL in ultrapure water 147 (Direct Q3[®] system, Millipore, USA) were prepared. Aliquots of 0.4 mL of the honey solutions 148 149 were mixed with 2 mL of Folin-Ciocalteu reagent 10 mL/100 mL (Merck, Germany) and 1.6 mL of sodium carbonate 7.5 g/100 mL (Sigma-Aldrich Co., EUA), and incubated at ambient temperature 150 for 2 h, protected from light. After that, the absorbance was measured using a spectrophotometer 151 152 (Cecil, CE 3021, 3000 series, Cecil Instruments, England) at 760 nm. The blank was prepared following the same procedure with ultrapure water. Gallic acid (Sigma Aldrich Co., USA) ranging 153 from (0.1 to 16) μ m/ mL was used to build the standard curve (Y = 0.0451x + 0.0013, $r^2 = 1$). 154

155 Results were expressed as gallic acid equivalent (GAE) content (mg/kg) of honey.

156 2.2.1.6 Total protein content

The standard orthophthaldialdehyde (OPA) spectrophotometric assay (Church et al., 1983) was 157 applied to quantify the total protein content of honey. The OPA reagent was prepared by dissolving 158 3.81 g of sodium tetraborate in approximately 80 mL Milli-Q water stirring at 50 °C. Then 0.088 g 159 of dithiothreitol and 0.1 g of sodium dodecyl sulfate (SDS) were added after cooling to ambient 160 161 temperature. Finally, 0.080 g of OPA dissolved in 2 mL of absolute ethanol was added to the solution and completed to 100 mL with Milli-Q water. In microtiter plates, 20 µl of standard/sample 162 163 were loaded into each well and mixed with 200 µl of OPA reagent, allowing the reaction to proceed 164 for 15 min at ambient temperature. The absorbance was then measured at 340 nm using a microplate photometer (Multiskan FC, ThermoFisher Scientific, USA). The standard curve was 165 obtained using L-leucine ranging from (0.16 to 4) mM of the standard solution made in 10 mM 166 phosphate buffer solution (Sigma Aldrich Co., USA). The standard curve obtained was: $r^2 = 0.9986$. 167

168 The results were expressed as L-leucine equivalent (L-leuE) content (g/100 g) of honey. Each

169 measurement was conducted in triplicate.

170 2.2.2 Production of powdered honey by spray drying

171 The initial honey content in the dispersions was chosen due to the first optimization study

(Toniazzo et al., 2023). The honey powders were produced according to Toniazzo et al. (2023), 172 with some modifications. Firstly, (16 g/100 g) of honey were mixed with ultrapure water (Direct 173 Q3[®] system, Millipore, USA), until complete dissolution. After that, (14 g/100 g) of isolated rice 174 175 protein or isolated micronized pea protein, or a mixture of both proteins ratio (50:50) were added, resulting in dispersions with a total solid concentration of (30 g/100 g) in dry matter. Dispersions 176 were kept under magnetic stirring at ambient temperature (25 °C) during the drying process to 177 178 prevent separation between liquid and solid phases. Finally, the dispersions were atomized in a laboratory scale spray dryer (Büchi, B290, Switzerland) coupled with a 0.7 mm diameter nozzle, 179 under the following conditions: drying air flow rate at 35 m³/h (corresponding to 100 % of its 180 capacity), average inlet/outlet air temperature at $(130.11 \pm 0.61, 75.58 \pm 2.55)$ °C, respectively, and 181

182 feed flow rate at 10 mL/min. Honey powder was collected at the bottom of the cyclone and stored 183 in the absence of light in an aluminum bag until analyses. It is worth mentioning that the analyzes 184 were performed only with freshly produced honey powder.

185 **2.2.3 Mass balance**

186 Spray drying mass balance can be performed from the dried product and the evaporated water.

However, it is useful to determine the conditions under which the food product will be dried. In this
situation, it is possible to evaluate the changes in humidity and temperature that occurred by the
drying air during the process. A mass balance to the component water was described, according to
Eq. 2:

191
$$m_{ms} \overline{X}_{w1} + m_{air} \overline{Y}_{w1} = m_{ms} \overline{X}_{w2} + m_{air} \overline{Y}_{w2}$$
(2)

wherein m_{ms} is the dry matter mass flow rate contained in the current of the material entered to be dried $[g \cdot s^{-1}]$, \overline{X}_{wl} is the initial moisture of the dispersion entered to be dried $[g_{water} \cdot g_{dry matter}^{-1}]$, m_{air} is dry air mass flow rate $[g \cdot s^{-1}]$, \overline{Y}_{wl} is the initial air absolute humidity $[g_{water} \cdot g_{dry air}^{-1}]$, \overline{X}_{w2} is the moisture of the honey powder $[g_{water} \cdot g_{dry matter}^{-1}]$, and \overline{Y}_{w2} is the final air absolute humidity $[g_{water} \cdot g_{dry}$ $air^{-1}]$.

Ambient temperature (°C) and relative humidity (%) were measured using a digital temperature
probe and a Thermometer/Humidity Monitor (Traceable[®] 4040, USA). Also, the air proprieties,
such as absolute humidity, wet-bulb temperature, and relative humidity were found with
Psychrometric Chart (Toledo, 1991) and psychrometric calculator auxiliary. The psychrometric
calculator was based on the formulations of thermodynamic properties of moist air, according to
Hyland & Wexter (1983a,b). The experimental wet-bulb temperature was measured according to
Beck (2021), using a thermometer with the wet bulb.

204 **2.2.4** Global and thermal efficiency of spray dryer

205 The global and thermal efficiency of the spray dryer (Masterd, 1972) were estimated, according to

206 Equations 3 and 4, respectively:

207
$$n_{global} = 100 \left(\frac{T_{air0} - T_{airf}}{T_{air0} - T_{amb}} \right)$$
(3)

208
$$\eta_{thermal} = 100 \left(\frac{T_{air0} - T_{airf}}{T_{air0} - T_{bu}} \right)$$
(4)

wherein: T_{air0} is the inlet air temperature, T_{airf} the outlet air temperature, T_{bu} the wet-bulb temperature,

210 and T_{amb} is the ambient air temperature.

211 **2.2.5** Physicochemical characterization of honey powder

- 212 2.2.5.1 Determination of moisture content and water activity (a_w)
- 213 The moisture content was determined according to AOAC (1996), using an oven (Memmert, UL
- 40, Germany) at 105 °C, until the samples achieved a constant weight. The results were expressed
- as grams of water content per 100 g of dry matter. Water activity was measured using a
- 216 HygroLabC1 water activity meter (Rotronic, Switzerland).
- 217 2.2.5.2 *Hygroscopy*
- 218 This procedure was conducted according to Cai & Corke (2000), with some modifications.
- Amounts of 1.2 g of honey powder were stored for 1 week in a desiccator containing a NaCl-
- saturated solution, with a relative humidity of (75.3) % in an incubator (SciQuip, Incu-80s, UK) at
- 221 25 °C. The mass of water adsorbed by the samples was expressed as grams of adsorbed water per
- 222 100 g of dry matter.
- 223 2.2.5.3 Sugar content and total phenolics compounds (TPC)
- The sugar content was determined following the same procedure detailed in session 2.2.1.4. The
- determination of the TPC followed the same procedure previously described with one modification:
- the honey powder solutions were prepared at 0.40 mg/mL with ultrapure water (Direct Q3[®] system,
- 227 Millipore, USA).

228 2.2.5.4 Total protein by the Kjeldahl method

229 Protein was analyzed using the Kjeldahl method according to AOAC (1996). The conversion factors

by Mariotti, Tomé & Mirand (2008) were 5.95 and 5.24 for honey powder with rice protein and pea

- protein, respectively. The total protein content was expressed as grams per 100 g of dry matter.
- 232 2.2.5.5 Morphology by Scanning Electron Microscopy (SEM)
- 233 Morphology was visualized using scanning electron microscopy (Carl Zeiss EVO MA15,
- Germany). The samples were first coated with 20 nm of Iridium (Ir) to act as an electricity
- conductor using the secondary electron detector. The images were obtained at 10 keV.

236 2.2.5.6 *Particle size distribution and mean particle diameter*

- 237 Particle size distribution and mean particle diameter were determined using low-angle laser light
- scattering (Mastersizer 2000, Malvern Panalytical, UK). The sample was dispersed in water and

remained under agitation during the procedure at 2500 rpm, including 1 min of ultrasonic agitation.

240 Volume-weighted mean diameter $(d_{4,3})$ was obtained using Eq. (5):

241
$$D[4,3] = \sum \frac{n_i d_i^4}{n_i d_i^3}$$
 (5)

wherein n_i is the number of particles with diameter d_i . Each measurement was carried out in triplicate.

244 2.3 Statistical analyses

All experiments were carried out in triplicate, and the data are presented as average plus standard deviations. Tukey tests were performed to compare the treatment means. The significance level for all tests was 5 %, which was calculated using SAS version 9.4.

248 **3. Results and discussion**

249 **3.1** Physicochemical characterization of honey

250 The color value found at (143.43 ± 4.34) mm Pfund can be considered dark amber, according to the

- 251 mm Pfund scale (USDA, 1985). The color of the honey is largely influenced by the chemical
- composition of nectar, associated with its botanical origin (Nordin et al., 2018; Scholz et al., 2020;

Solayman et al., 2016). Additionally, it can be influenced by the mineral content of honey, closely
linked with the soil characteristics and, therefore, geographic regions (Alvarez-Suarez et al., 2010;
Bobis et al., 2020;). Minor constituents of honey, such as flavonoids and carotenoids, can also
influence its color. Alvarez-Suarez et al. (2010), Bobis et al. (2020) and García-Tenesaca et al.
(2017) found high concentrations of these constituents in darker honey compared to lighter ones.
For that reason, dark honey was chosen to develop this work.

The measured pH of honey (3.73 ± 0.03) is low enough to avoid the growth of undesirable

260 microorganisms, maintaining its stability (Terrab et al., 2004). Free acidity is related to the presence

of organic acids in equilibrium with their lactones, or internal ester, and some inorganic ions, such

as phosphate or sulfate (Terrab et al., 2004; White, 1979). The free acidity value found in this work

of (46.41 ± 0.53) meq/kg is an acceptable value according to the legislation on honey quality

264 control (Brasil, 2000; Codex Alimentarius, 2001; International Honey Commission, 2009). The

maximum acceptable value is 50 meq/kg of honey; values above this limit can indicate the presence
of undesirable fermentation (Habib et al., 2014).

267 The total soluble solid content was (82 ± 0.2) g/100 g; therefore, the water content, which is the second major component in honey, was considered (18 ± 0.2) g/100 g. This value is acceptable, 268 according to Brasil (2000) and Codex Alimentarius (2001); both legislations limit the maximum 269 value of water content to 20 g/100 g. The water content of honey can naturally range from (13.6 to 270 23) g/100 g and is influenced by different factors, such as the source, nectar geographical origin, 271 272 climatic conditions, harvest season, and the manipulation by the beekeepers (Bogdanov & Martin, 2002; De-Melo et al., 2018;). However, according to Bogdanov & Martin (2002), fermentation 273 issues can only be avoided if honey contains less than 18 g/100 g of water; otherwise, it will be a 274 275 suitable medium for yeast proliferation, decreasing its quality. Fermentation is caused by osmophilic yeasts present in honey, which are responsible for forming ethyl alcohol and carbon 276 dioxide. Alcohol, in the presence of oxygen, breaks down into acetic acid and water, promoting a 277 sour taste in honey. The main yeast genus reported to be responsible for honey fermentation is 278

Saccharomyces spp. (Snowdon & Cliver, 1996). Note that drying honey could prevent spoilage by
yeast besides facilitating and increasing the application of the honey as an ingredient in the food
industry.

The fructose content was found at (46.52 ± 0.56) g/100 g and the glucose content at (35.88 ± 0.16) 282 g/100 g, while sucrose was not found in honey. Honey is mainly composed of sugar, and fructose is 283 normally the major monosaccharide (Afrin et al., 2020; Martinotti & Ranzato, 2018; White, 1979). 284 Sugars are directly related to honey crystallization, and the time over which this phenomenon 285 occurs depends mostly on the ratio of fructose to glucose (F/G), considering that glucose is less 286 soluble in water than fructose (Escuredo et al., 2014; Gleiter, Horn, & Isengard, 2006; Laos et al., 287 2011; Nascimento et al., 2018). Honey with an F/G ratio of >1.33 does not crystallize for a long 288 time; in turn, if the ratio is <1.11 the honey crystallizes very fast (Escuredo et al., 2014; Smanalieva 289 290 & Senge, 2009;). In this work, the F/G ratio of the samples was at (1.30 ± 0.02) , which suggests a 291 slow natural crystallization of honey.

In this work, the total phenolic compounds (TPC) found was GAE content at (301.31 ± 20.95) mg /kg of honey, and this value is consistent with those reported by several other authors. Nascimento et al. (2018) found similar values in honey collected from the south of Brazil, with a GAE content ranging from (260 to 1000) mg/kg of honey. Furthermore, Dżugan et al. (2018) analyzed TPC in Polish honey and the GAE content values ranged from (254.52 to 1353.66) mg/kg. Kavanagh et al. (2019) found values of GAE content ranging from (25.9 to 811) mg/kg of honey in Irish multifloral honey.

The total protein content found in this work was the L-leuE content at (0.0956 ± 0.0066) g/100 g of honey. According to De-Melo et al. (2018), total honey protein can range from (0.1 to 0.5) g/100 g of honey. Azeredo et al. (2003) evaluated total protein in honey of different floral origins and found values ranging from (0.0199 to 0.2236) g/100 g, within the average value found in the present work.

303 **3.1.1** Production of honey powder by spray drying

Tables 1 and 2 show the parameters and the water mass balance obtained from the production of 304 honey powder by spray drying. The spray drying conditions, such as ambient temperature, 305 306 relative humidity, inlet, and outlet air temperature indicated global efficiency of $(48.33 \pm 1.53,$ $(48.67 \pm 2.08 \text{ and } 54.00 \pm 1.00)$ % for the honey powder produced with rice protein, pea protein, or 307 308 a mixture of both proteins, respectively, which corresponds to the total heat fraction provided by the equipment used to dry. Spray drying has the advantage of completing the drying process within a 309 310 few seconds, maintaining the very low temperature of the droplets, and consequently drying heat-311 sensitive products without excessively affecting their quality (Ré, 1998; Tan, Zhong, & Langrish, 2020). Therefore, at a determined point of droplet drying, its temperature is the wet-bulb 312 temperature of the drying air (Bhandari, Datta & Howes, 1997; Ré, 1998), which was (38.00 ± 1.00, 313 314 36.67 ± 0.58 and 37.33 ± 2.08) °C for the honey powder produced with rice protein, pea protein, or 315 a mixture of both proteins, respectively. Only at the end of the drying process did the particles reach 316 the temperature close to the outlet air temperature of $(77.75 \pm 4.19, 77.00 \pm 2.16 \text{ and } 72.00 \pm 1.82)$ 317 °C for the honey powder produced with rice protein, pea protein, or a mixture of both proteins, respectively. Under these conditions, the inlet air temperature was not high enough to affect the 318 possible heat-sensitive components probably existing in the honey, for example, the phenolics 319 compounds. 320

For example, for the honey powder produced with rice protein, changes in air humidity during the process were due to the water lost in the initial dispersion moisture at 2.356 ± 0.001 g_{water}·g_{dry matter}⁻¹,

leading the air absolute humidity to increase from approximately 0.0051 ± 0.0001 to $0.0200 \pm$

324 0.0001 $g_{water} \cdot g_{dry air}^{-1}$, providing a thermal efficiency around 56.67 ± 2.08 %, which indicates the

325 approximation to the drying air saturation degree.

The powder recovery yield for the honey powder using rice protein, pea protein, or a mixture of

both proteins as carriers was $(64.88 \pm 0.64, 45.32 \pm 1.20 \text{ and } 52.34 \pm 4.59)$ %, respectively.

328 According to Bhandari et al. (1997), to consider a successful drying operation, the powder recovery yield for sugar-rich products should be above 50 %. As can be seen, using pea protein as a carrier, 329 the value of the powder recovery yield was lower compared to that produced with rice protein. In 330 331 addition, it was observed that in the honey powder produced with pea protein as a carrier, the particles easily stuck to the internal wall of the drying chamber, resulting in a low powder recovery 332 yield. However, with the honey powder produced with the mixture of proteins, the value found can 333 still be considered satisfactory. Therefore, when the objective is to obtain a high powder recovery 334 yield, with the drying parameters used in this study, it is suggested that for the formulation of honey 335 336 powder produced with the mixture of both proteins, the proportion of pea protein as a carrier should not exceed the (50:50) ratio. 337

338 3.2 Physicochemical characterization of honey powder

339 Table 3 presents the physicochemical characterization of the honey powder produced with rice 340 protein, pea protein, or a mixture of both proteins. According to Labuza (1980), it is very important to control water activity (a_w) to guarantee food stability, avoiding microbial growth and chemical 341 342 deterioration. The measured a_w values were similar and between (0.25 ± 0.07 and 0.427 ± 0.002) for all samples, and the honey powder produced with rice and pea protein did not show significant 343 differences during storage time. The honey powder produced with the mixture of both proteins 344 showed a significant difference on day 21. However, all samples remained below 0.6, which is 345 considered to indicate stability to microbial deterioration (Labuza, 1980). 346

Regarding moisture, the use of pea protein as a carrier resulted in higher moisture of the honey powder in comparison to rice protein, and the mixture of both proteins. According to Goula & Adamopoulos (2005), the powder moisture is influenced by the particle size, and when the powder has a smaller particle size, drying is facilitated. This is possible for two main reasons: (i) smaller particles have a larger surface area per unit mass; therefore, more surfaces are in contact with the heating air and, consequently, permit the moisture to escape; (ii) the heat capacity of the particles is reduced for smaller particles; the distance is also reduced for moisture to go from the center of the particle to the surface and escape. As can be seen in Figures 1A and 2, the honey powder produced with rice protein as a carrier has a higher quantity of smaller particles, when compared with the honey powder produced with pea protein as a carrier (Fig. 1B) and with the mixture of both proteins (Fig. 1C).

The honey powder produced with pea protein as a carrier presented a smooth surface morphology, with less porosity than the honey powder produced with rice protein and the mixture of both proteins, suggesting that this characteristic hindered the evaporation of water during drying. For all samples, the particles are observed to be linked by bridges; this morphology is typical for sugar-rich product powder (Samborska et al., 2019).

In dried honey, high values for hygroscopy are expected due to the high sugar content; however, the 363 powders obtained in this study did not show significant differences, and the hygroscopy values were 364 365 similar to those of other authors that also used spray drying, as can be seen in the review from 366 Samborska (2019). Tonon, Brabet & Hubinger (2008) dried açai (Euterpe oleraceae Mart.) by spray drying and found hygroscopy values ranging from $(12.48 \pm 0.10 \text{ to } 15.79 \pm 0.29) \text{ g/100 g}$. The 367 368 honey powder produced with rice protein as a carrier showed a lower moisture value. It has been suggested that the lower moisture increases the capacity to absorb moisture from the environment 369 due to the greater water concentration gradient between the powder and the surrounding air (Tonon, 370 Brabet & Hubinger, 2008). In addition, the morphology of the powder may influence its 371 hygroscopy. The honey powder produced with pea protein presented a smooth surface, with less 372 porosity than the one produced with the mixture of both proteins. Thus, the porosity of the honey 373 powder produced with the mixture of both proteins may influence the hygroscopy value, mainly 374 because rice protein increased the surface area of the particles and exposure to the moisture of the 375 376 environment.

The sugar content values of the honey powder produced with rice protein, pea protein or a mixture of both proteins corroborate the initial spray-drying feed formulations. For example, in the feed formulation for the honey powder produced with rice protein, the honey content was (53.37 ± 0.04) g/100 g, with the protein content of $(37.59 \pm 0.03) \text{ g}/100 \text{ g}$, both in dry matter. At the end of the process, the honey powder produced with rice protein had a sugar content of $(55 \pm 0.25) \text{ g}/100 \text{ g}$, and a protein content of $(37.38 \pm 1.26) \text{ g}/100 \text{ g}$, both in dry matter, indicating that these macromolecules did not decrease during the spray drying process.

In the TPC assay for the honey powder, the proteins were verified to interfere with the results, 384 increasing the TPC values. According to Ikawa et al. (2003), the use of the Folin-Ciocalteu phenol 385 386 reagent can also detect certain nitrogen compounds. To overcome this challenge, powders were 387 produced by spray drying only with rice protein, pea protein, or a mixture of both (without honey in 388 the composition), and the TPC assay was performed. Finally, the absorbances measured from the powders only with proteins were subtracted from the corresponding TPC results of the honey 389 powder. The values found after spray drying (Table 3) were similar to those found in the GAE 390 391 content of (301.31 ± 20.95) mg/kg of honey, suggesting that the phenolic compounds were not 392 negatively affected by the spray drying conditions and that the microencapsulation method was 393 effective in protecting these bioactive compounds.

394 The particle size distributions of the honey powder shown in Figure 2 support the images in Figure 1 and show that the honey powder produced with rice protein has smaller particles compared to the 395 honey powder produced with the pea protein and with the mixture of both proteins. The honey 396 powder showed a mean particle diameter of (12.154, 26.835, 17.905) µm for the honey powder 397 produced with rice protein, pea protein, or a mixture of both, respectively. This can be considered 398 399 an appropriate size when the aim is to add the particles to a food matrix. According to Hansen et al. (2002), the particle size should be less than 100 µm to avoid a negative influence on the food 400 401 texture.

402 **4.** Conclusions

In this work, the development of honey powder by spray drying using plant proteins as a carrier was
successively achieved. The honey used as raw material showed acceptable physicochemical
parameters by the legislation of honey quality control, leading to the production of honey powder.

The isolated rice protein provided a higher powder recovery yield compared to pea protein or a 406 mixture of both. The proportion of pea protein as the carrier should not exceed the (50:50) ratio to 407 obtain a high powder recovery yield. Total phenolic compounds were not affected by spray drying 408 conditions, since at a determined point of the droplets drying, their temperature is the wet-bulb 409 410 temperature of the drying air. High values for hygroscopy are expected as a result of the high sugar content; however, the honey powders showed values similar to those reported by other authors that 411 also used the spray drying process. The honey powders produced with two different plant proteins 412 and a mixture of both can be an option for food ingredients, even for individual consumption as a 413 sports supplement or for new product development (protein bars and cookies). Thus, this study 414 suggests that honey powder is a suitable ingredient to be applied to a real food matrix that can be 415 commercialized. 416

417 **Declaration of Competing Interest**

418 None declared

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428 Authors' contributions

429 Taíse Toniazzo: Conceptualization, Data curation, Formal analysis, Writing - original draft,

430 Review & Editing, Methodology, Investigation. Mar Collado-González: Investigation,

431 Methodology, Review Carmen Cecília Tadini: Supervision, Conceptualization, Writing - review

432 & editing, Funding acquisition. Alan Mackie: Supervision, Writing - review & editing.

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661 Figure Captions

- 662 **Fig. 1.** Morphology by scanning electron microscopy of the honey powder produced with isolated
- ⁶⁶³ rice protein (**A**), isolated micronized pea protein (**B**), or a mixture of both proteins (**C**) as carriers
- 664 during atomization. Magnification: 1,000 X.
- 665 Fig. 2. Distribution of the particle size of honey powder produced with isolated rice protein, isolated
- 666 micronized pea protein, or a mixture of both proteins as carriers during atomization.

667 **Table 1.**

669 micronized pea protein, or a mixture of both proteins as carriers

Sample	Honey powder	Honey powder	Honey powder
	Rice protein	Pea protein	Rice+Pea proteins
Inlet air temperature (°C)	$130.83^{a} \pm 0.75$	$130.17^{a} \pm 0.41$	$129.33^{a} \pm 1.63$
Outlet air temperature (°C)	$77.75^{a} \pm 4.19$	$77.00^{a} \pm 2.16$	$72.00^{a} \pm 1.82$
Ambient temperature (°C)	$22.10^{a} \pm 0.17$	$21.03^{b} \pm 0.40$	$21.57^{ab} \pm 0.12$
Relative humidity (%)	$31.00^{a} \pm 1.00$	$33.33^{ab} \pm 1.15$	$33.67^{b} \pm 0.58$
Experimental wet-bulb temperature (°C)	$38.00^{a} \pm 1.00$	$36.67^{a} \pm 0.58$	$37.33^{a} \pm 2.08$
Global efficiency (%)	$48.33^{a} \pm 1.53$	$48.67^{a} \pm 2.08$	$54.00^{b} \pm 1.00$
Thermal efficiency (%)	$56.67^{a} \pm 2.08$	$57.67^{a} \pm 2.89$	$62.00^{a} \pm 3.00$
Powder recovery yield (%)	$64.88^{a} \pm 0.64$	$45.32^{b} \pm 1.20$	$52.34^{\circ} \pm 4.59$

670 Means followed by the same lowercase letter in the same line were not significantly different (p>0.05) by Tukey's test.

671 **Table 2.**

672 Water mass balance from the spray drying process to obtain honey powder with isolated rice protein, isolated

673 micronized pea protein, or a mixture of both proteins as carriers

Sample	Honey powder	Honey powder	Honey powder
	Rice protein	Pea protein	Rice+Pea proteins
Dispersion mass flow rate (gdry mass ·s ·1)	0.0553 ± 0.0006	0.0554 ± 0.0002	0.0553 ± 0.0001
Initial dispersion moisture (gwater·gdry matter-1)	2.356 ± 0.001	2.336 ± 0.003	2.336 ± 0.003
Air mass flow rate (gdry air·s·1)	8.50 ± 0.01	8.50 ± 0.01	8.486 ± 0.002
Initial air absolute humidity (gwater gdry air ⁻¹)	0.0051 ± 0.0001	0.0051 ± 0.0002	0.0053 ± 0.0002
Final powder moisture (gwater gdry matter 1)	0.04 ± 0.01	0.08 ± 0.01	0.065 ± 0.005
Final air absolute humidity (gwater gdry air -1)	0.0200 ± 0.0001	0.0198 ± 0.0002	0.0201 ± 0.0001
Wet-bulb temperature (°C)	37.1 ± 0.5	36.9 ± 0.6	38.4 ± 0.5

674

675 Table 3.

676 Physicochemical characterization of honey powder produced with isolated rice protein, isolated micronized

677 pea protein, or a mixture of both proteins as carriers

	Honey powder	Honey powder	Honey powder
	Rice protein	Pea protein	Rice+Pea proteins
a_w			
Day 0	$0.28^{aA} \pm 0.10$	$0.32^{aA} \pm 0.06$	$0.25^{aA} \pm 0.07$
Day 21	$0.39^{\mathrm{aA}} \pm 0.02$	$0.398^{abA} \pm 0.007$	$0.427^{\mathrm{bB}} \pm 0.002$
Day 56	$0.31^{aA} \pm 0.01$	$0.327^{aA} \pm 0.002$	$0.324^{aA} \pm 0.003$
Moisture (g/100 g)	$3.36^{a} \pm 0.20$	$7.92^{b} \pm 0.04$	$6.82^{\circ} \pm 0.01$
Hygroscopy (%)	$21.18^{a} \pm 0.24$	$20.27 ^{\text{a}} \pm 0.02$	$21.26^{a} \pm 0.71$
Fructose content (g/100 g) of honey	$31.56^{a} \pm 0.21$	$31.39^{a} \pm 0.10$	$35.45^{b} \pm 0.43$
Glucose content (g/100 g) of honey	$23.43^{a} \pm 0.13$	$23.04^{a} \pm 0.34$	$27.66^{b} \pm 0.66$
Total protein content (g/100 g)	$37.38^{a} \pm 1.26$	$38.95^{a} \pm 1.77$	—
GAE content (mg/kg) of honey	$353.78^{a} \pm 30.48$	$318.58^{a} \pm 52.80$	$336.18^{a} \pm 52.80$

678 679 Means followed by the same lowercase letter in the same line were not significantly different (p>0.05) by Tukey's test. Means followed by the same uppercase letter in the same column were not significantly different (p>0.05) by Tukey's test.



Fig. 2



Figure 2



Credit Author Statement

Taíse Toniazzo: Conceptualization, Data curation, Formal analysis, Writing - original draft, Review & Editing, Methodology, Investigation.

Mar Collado-González: Investigation, Methodology, Review

Carmen Cecília Tadini: Supervision, Conceptualization, Writing - review & editing, Funding acquisition.

Alan Mackie: Supervision, Writing - review & editing.

Declaration of Competing Interest

None declared