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1 Bioethanol from autoclaved municipal solid  
2 waste: assessment of environmental and  
3 financial viability under policy contexts

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13

1 **Abstract**

2 Globally, 2.01 billion tonnes of municipal solid waste (MSW) were generated in 2016,  
3 about 37% of which was disposed of into landfills. This study evaluates the  
4 environmental and financial viability of producing ethanol from autoclaved MSW via  
5 fermentation. Experimental screening of four different microorganisms (i.e., *S.*  
6 *cerevisiae*, *Z. mobilis*, *E. coli*, and *S. pombe*) and process modelling indicate that  
7 MSW-derived ethanol can significantly reduce greenhouse gas emissions relative to  
8 gasoline (84% reduction following EU Renewable Energy Directive accounting  
9 methodology, and by 156% to 231% reduction following the US Energy Independence  
10 and Security Act methodology). Utilisation of wastes for biofuel production in the UK  
11 benefits from policy support and financial support for renewable fuels (Renewable  
12 Transport Fuel Certificates). Financial analysis highlights that microorganisms  
13 achieving higher ethanol yield and productivity (*S. cerevisiae* and *Z. mobilis*) can  
14 achieve financial viability with higher cumulative net present value than *E. coli*, *S.*  
15 *pombe*. However, the positive net present value can be achieved primarily due to the  
16 benefit of gate fees received by diverting wastes to autoclave and ethanol production  
17 (64% of total revenues), rather than from revenues from ethanol sales (7% of total  
18 revenues). Key process improvements must be achieved to improve the financial  
19 viability of ethanol production from MSW and deliver a clear advantage over waste  
20 incineration, specifically improving hydrolysis yield, reducing enzyme loading rate and,  
21 to a lesser extent, increasing solid loading rate. The results provide significant insights  
22 into the role of policy and technology development to achieve viable waste-to-biofuel  
23 systems.

24

25 **Keywords**

26 Municipal solid waste, Waste autoclaving, Fermentation, Incineration, Ethanol, Life  
27 cycle assessment, Techno-economic analysis

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## 1 Introduction

The development of biofuels from waste impacts significantly on current waste treatment within the context of a more circular economy, while also providing low carbon renewable fuels for transport sectors. Municipal solid waste (MSW) has been identified as a useful bioenergy source as it has a high organic content such as paper, card, garden, and food waste. There is potential for waste-derived fuels to simultaneously address the environmental impacts of conventional treatment processes, while providing biorenewable fuels that avoid land use implications of crop-based fuels. However, achieving financial viability can be challenging, due to the complex composition of wastes and presence of contaminants that may inhibit bioprocesses (enzymatic hydrolysis, fermentation). Comprehensive analyses of the environmental and financial performance of waste based biofuels are needed to better understand the waste-to-biofuel opportunity, to target technology development, and to inform the role for regulation in encouraging the uptake of viable waste-to-fuel technologies.

In the UK 14.6 million tonnes of MSW were landfilled in 2018 of which 49% (7.2million tonnes) was biodegradable material [1]. Globally, 2.01 billion tonnes of MSW was generated annually in 2016 and about 37% of waste is disposed of in some form of a landfill, only 8% of which is disposed of in sanitary landfills with landfill gas collection systems. Open dumping accounts for about 31 percent of waste, 19 percent is recovered through recycling and composting, and 11 percent is incinerated for final disposal [2]. Landfill and incineration are the least desirable steps in circular waste management as they contribute significantly to greenhouse gas (GHG) emissions and environmental pollution, while recovering minimal value from wastes. It was estimated that 1.6 billion tonnes of carbon dioxide equivalents (CO<sub>2</sub>eq) were generated from solid waste treatment and disposal in 2016, or 5% of global emissions and is expected to increase to 2.38 billion tonnes of CO<sub>2</sub>eq per year by 2050 if no efficiencies are introduced in this sector [2].

In 2014, global GHG emission was over 36 billion tonnes CO<sub>2</sub>eq per year while about 20% of global emissions were the result of transportation [3]. The EU's climate change targets have already stated transport emissions must be cut by 60% by 2050 compared with 1990 levels [4]. The EU Renewable Energy Directive (RED) requires that renewable energy content should account for at least 10% of the energy used in transportation by 2020, increasing to 32% renewable energy share by 2030 under the revised RED II directive [5], which can be achieved through the use of biofuels. The overall production of biofuels in the EU has increased dramatically since the turn of the century, growing from 722,000 to 15.7 million metric tonnes of oil equivalent in 2018, largely from food crops [6]. In the US, total renewable fuel production was 26 billion gallons (~80 million metric tonnes of oil equivalent) in 2018. The EU RED II regulates that renewable biofuels must achieve a 60% life cycle GHG emission reduction compared to fossil fuel [7]. Similarly, the US Energy Independence and Security Act of 2007 (EISA) requires biofuels to achieve a life cycle GHG reduction threshold as compared to a 2005 petroleum baseline for different types of biofuels (e.g., 60% reduction for cellulosic biofuel), thereby boosting the long-term goal towards 36 billion US gallons of renewable fuel by 2022 [8]. In the UK, the Renewable Transport Fuel Obligation specifically provides a stricter limitation on crop-based fuels, incentivising waste-based fuels from classes of waste residue waste by awarding

1 double Renewable Transport Fuel Certificates (RTFC) per litre of liquid renewable  
2 fuels. These credits are tradeable and have a market value of £0.12 to £0.22 per RTFC,  
3 thus financially supporting biofuels production from waste [9].

4 Since the introduction of the RED quotas [5], concerns continue to rise about the  
5 impact of biofuels upon world food prices, tropical deforestation and biodiversity. The  
6 EU Fuel Quality Directive [10] restricts biofuel production from feedstocks grown on  
7 virgin land or land with high carbon stocks. Second generation biofuels using non-food  
8 feedstocks, agricultural wastes thus address concerns associated with first generation  
9 biofuels related to food security, climate change, non-renewable energy use, air  
10 pollutant emissions, energy security, and land use change [11]. Due to the high  
11 lignocellulosic content of MSW, it has considerable potential as a renewable biomass  
12 feedstock for biofuel production as it is abundant, low cost and does not compete with  
13 agricultural production or purposely collected for biofuel production [12]. Furthermore,  
14 producing biofuels from waste may offer advantages over current disposal techniques  
15 (composting, anaerobic digestion, refuse derived fuel, incineration and landfilling) by  
16 addressing environmental concerns with some current methods while producing a  
17 valuable output [13].

18 Autoclaving is a process by which high pressure and steam are used to sterilise  
19 organic and/or inorganic materials. It is a commercially proven method for the  
20 separation of a heterogeneous MSW stream into several component parts: converting  
21 the biogenic content of MSW to a biofibre material and enabling the recovery of  
22 sterilized metal, glass, and plastic materials[14]. Autoclave conditions also act as a  
23 mild hydrothermal pre-treatment for lignocellulosic material, increasing cellulose  
24 accessibility for sugar production by enzymes while producing fewer inhibitory  
25 compounds compared to other, harsher pre-treatments [15]. Several researchers have  
26 studied the production of biofuels from the organic content of MSW produced through  
27 autoclaving [12, 13, 16-18]. Compared to other lignocellulosic feedstocks such as  
28 agricultural by-products, the organic fraction of MSW from autoclaving is typically  
29 highly variable and heterogeneous in composition. The organic fraction contains  
30 contaminants such as metals and other pollutants at levels that could potentially be  
31 inhibitory to enzymes and/or fermentative microorganisms. Developing a viable  
32 fermentation process for conversion of autoclave pretreated MSW therefore requires  
33 a robust microorganism that has an intrinsic ability to ferment this complex feedstock  
34 [13].

35 Life cycle assessment (LCA) has been widely used as a tool to examine environmental  
36 implications of lignocellulosic biofuel production in the past decades. LCA allows  
37 potential impacts to be identified at an early stage of process design, providing the  
38 opportunity for decision making and improved process sustainability before scaling up  
39 or commercialisation. Previous LCA studies have been widely reported in the literature  
40 for bioethanol production from various feedstocks including corn stover, wheat straw,  
41 poplar, eucalyptus and waste paper amongst others [19-24]. These studies suggest  
42 that the use of lignocellulosic material will lead to a range of reductions in GHG  
43 emissions (46-90% compared to conventional gasoline) compared to first generation  
44 production using food crop feedstocks [20].

1 The selection of feedstocks or design of the production process must consider both  
2 environmental and social criteria, in addition to capital and operational costs for  
3 economic feasibility [25]. The National Renewable Energy Laboratory (NREL)  
4 conducted a techno-economic analysis for lignocellulosic ethanol production and  
5 reported a minimum selling price (MSP) of ethanol of 2.15 US\$/gal [26]. Similarly,  
6 previous techno-economic analyses have primarily compared the process designs,  
7 evaluated the potential to reduce the production cost and determined the MSP of  
8 ethanol [27-29]. Results of these techno-economic models vary significantly from one  
9 another although the same process technology methods and feedstock are taken into  
10 account [30]. Few techno-economic studies have focused on waste to biofuel for  
11 investment analysis, taking into account predicted biofuel prices whilst simultaneously  
12 considering life cycle environmental implications. This study performs a  
13 comprehensive investment analysis of autoclaved waste to ethanol conversion,  
14 considering relevant financial incentives provided to waste-derived fuel production  
15 and GHG emission accounting methods in life cycle analysis.

16 The study develops systematic models to comprehensively understand the technical,  
17 environmental and financial impacts of bioethanol production from autoclave pre-  
18 treated MSW and evaluate four microorganisms (i.e., *Saccharomyces cerevisiae*,  
19 *Zymomonas mobilis*, *Escherichia coli*, *Schizosaccharomyces pombe*) previously  
20 reported by Dornau, Robson [13] to robustly grow on this complex feedstock and  
21 produce bioethanol. The overall environmental impacts (i.e., primary energy demand  
22 and GHG emission) and investment case using net present value (NPV) are evaluated  
23 across the integrated unit operations, including autoclave, hydrolysis, fermentation,  
24 and distillation sited in the UK. The study follows current UK, EU and US renewable  
25 fuel policies within the context of sustainability frameworks by considering alternative  
26 system boundaries, allocation approaches, waste disposal gate fees and renewable  
27 fuel incentives, providing a global perspective on the viability of ethanol production  
28 from MSW via autoclave pretreatment. The results are then integrated to meaningfully  
29 inform the investment case for waste-to-biofuel systems.

## 30 **2 Methods**

31 The study assesses the current and future viability of bioprocessing of municipal solid  
32 waste feedstock pretreated by autoclaving to ethanol. Four fermentative  
33 microorganisms are screened (i.e., *S. cerevisiae* ATCC200062, *Z. mobilis* DSM424,  
34 *E. coli* LW06, *S. pombe* JB953), based on experimental results. The overall  
35 environmental and cost implications of converting MSW to ethanol using four  
36 fermentative microorganisms are compared via LCA and techno-economic analysis  
37 based on process simulation of operation at commercially relevant scale. We consider  
38 three different techno-economic scenarios: Base case (based on current experimental  
39 evidence); Process Improved case (with anticipated process improvements (solid  
40 loading rate, hydrolysis yield, fermentation productivity, and enzyme loading); and  
41 Best Case (with anticipated process improvements and favourable market conditions  
42 (gate fees; product markets)).

### 43 **2.1 Waste Composition**

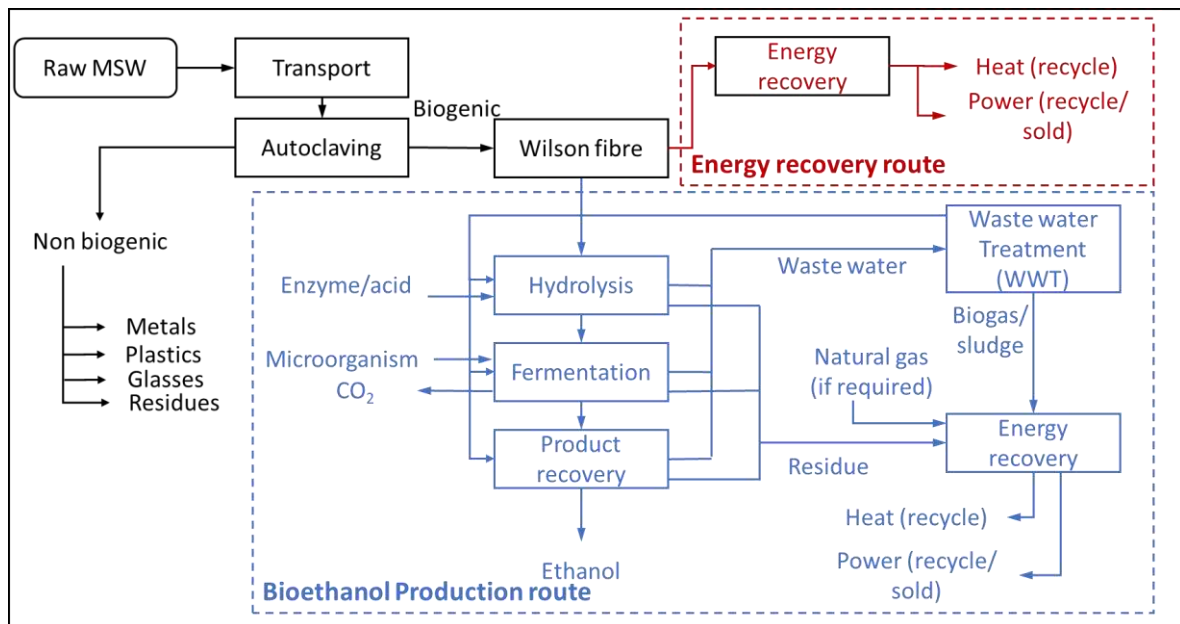
44 The study utilised a synthetic feedstock representative of UK MSW with the following  
45 wet composition by mass: paper and cardboard (22%), food waste (17%), wood  
46 (8.7%), plastic (22%), glass (1%), garden waste (3%), metals (4%), textiles (6.6%) and

1 others (15.7%). This was adjusted by removing the “Carpet, underlay and furniture”  
 2 and “Bricks, plaster and soil” as reported by Defra Digest of waste and resource  
 3 statistics, 2018 edition [31] based on most recent experimental data done by Wilson  
 4 BioChemicals.

## 5 2.2 Autoclave Pre-treatment

6 The MSW feedstock was subjected to autoclave pre-treatment in a pilot-scale Wilson  
 7 System®[32]. This involved autoclaving with dry steam at 160°C and 72 psig for 45  
 8 minutes in a baffled vessel rotating at 4 rpm. The pre-treated material was segregated  
 9 into organic and inorganic fractions using manual sorting and sieving. The organic  
 10 fibre fraction was homogenized and stored in ~1 kg bags at -20°C. This study assumes  
 11 a plant capacity of 150,000 tonne MSW/yr based on two 20 tonne batch size. Previous  
 12 studies [33] by the collaborating autoclave technology developer (Wilson Bio-chemical  
 13 Ltd) had confirmed that autoclaved biofibre generated using a 50 L vessel was  
 14 representative of full commercial scale. This study is based on this pilot scale,  
 15 generating commercially representative data suitable for engineering design and  
 16 scale-up. The pilot plant operation determined the process input requirements of 43  
 17 MJ electricity, 274 MJ natural gas and water consumption of 245 L per tonne of MSW.  
 18 As in Figure 1, two routes are considered to utilise autoclaved fibre: bioethanol  
 19 production; or energy recovery in an offsite incineration plant.

20



21

22

Figure 1 Overall diagram for MSW to ethanol/energy conversion.

## 23 2.3 Bioethanol Production from Autoclaved MSW

24 For bioethanol production, the autoclaved fibre is transferred to hydrolysis and  
 25 fermentation for conversion. After product recovery, the main product ethanol is  
 26 obtained while the wastewater is sent to treatment and residual biomass for energy  
 27 recovery.

### 1    **2.3.1 Enzymatic Hydrolysis**

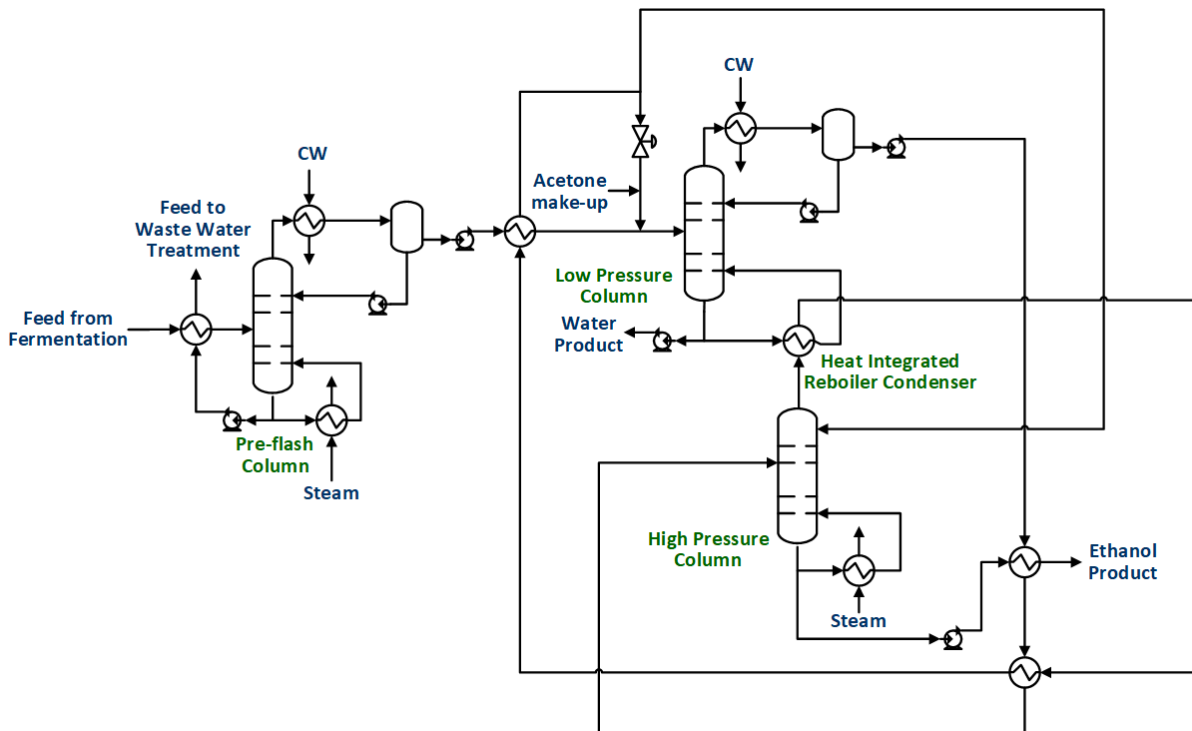
2    Samples of the MSW fibre were milled to a consistent particle size (0.5mm) and then  
3    loaded into the hydrolysis vessel, where the sample was diluted with water from the  
4    mains water tank into a dilute slurry (20wt% solids content). At this stage, adjustments  
5    may also be made to process conditions such as pH adjustment to 5 with concentrated  
6    H<sub>2</sub>SO<sub>4</sub>, which was the optimum for enzyme activity. The slurry was then dosed with  
7    an enzyme cocktail Cellic Ctec2 (Novozymes) solution (5% wt/wt enzymes to total  
8    available sugars) (15–60 filter paper units (FPU) per gram cellulase). Hydrolysis was  
9    carried out for 48 hours at 50°C. The resulting slurry was centrifuged (4000 x g, 15  
10   mins) to separate the hydrolysate from un-hydrolysed solids. This method gave a  
11   monosaccharide content as follows: glucose (40-45wt%), xylose (4-5wt%), galactose  
12   (0.7wt%) and arabinose (2.9wt%), where glucose is derived from cellulose and the  
13   other three monosaccharides are derived from hemicellulose [34].

### 14   **2.3.2 Fermentation experiments**

15   Dornau et al. [13] reports the detailed fermentative performance of the four  
16   microorganisms. Briefly: Each microorganism was cultivated in a fermentation medium  
17   consisting of 9.4 ml of filter sterilised MSW fibre hydrolysate supplemented with 1%  
18   w/v vitamin enriched yeast extract (Sigma) (to provide nutrients) and 40 mM MOPS  
19   buffer to a final volume of 10 ml. The fermentation medium was transferred to sterile  
20   conical flasks or serum bottles. Fermentations with *S. pombe*, *S. cerevisiae* and *E. coli*  
21   were carried out in conical flasks (100 ml) sealed with airlocks to promote microaerobic  
22   conditions. Fermentations with *Z. mobilis* were carried out under fully anaerobic  
23   conditions in serum bottles (100 ml). Preparing the inoculum, overnight cultures of  
24   each species were harvested in mid-exponential phase and re-suspended in  
25   fermentation medium to give a starting optical density (OD<sub>600</sub>) of 0.05. Fermentation  
26   cultures were incubated at each species' optimal temperature with shaking at 160 rpm.  
27   Samples were taken at regular intervals over 48 hours and used to measure OD<sub>600</sub>,  
28   sugar and ethanol concentration and final cell dry weight according to standard  
29   methods. Key fermentation yield parameters for each species (i.e., *S. cerevisiae*  
30   ATCC200062, *Z. mobilis* DSM424, *E. coli* LW06, *S. pombe* JB953) cultivated in MSW  
31   fibre hydrolysate were reported in our previous work [13].

### 32   **2.3.3 Distillation**

33   Ethanol and water form a minimum boiling azeotrope, preventing purification via  
34   simple distillation to a pure ethanol product. Pressure swing distillation using acetone  
35   as an entrainer was employed to circumvent the azeotropic point, heat integrated to  
36   reduce the overall energy consumption as in Figure 2. Given the minimum boiling  
37   azeotrope, a pre-flash column concentrated the ethanol in the distillate as feed to the  
38   pressure swing distillation, where the high- and low-pressure columns were heat  
39   integrated through a combined reboiler condenser. The separations network outlined  
40   in Figure 2 was rigorously simulated in Aspen HYSYS® v11.



1

2 Figure 2 Pressure swing distillation of ethanol and water using acetone as entrainer,  
 3 heat integrated for energy efficiency.

4 **2.4 Life cycle assessment**

5 **2.4.1 Scope and Functional Unit**

6 This study developed an LCA model of MSW-derived ethanol following the ISO  
 7 Standards 14040 and 14044 [35, 36]. The LCA was undertaken in GaBi 9.2 (2019)  
 8 using Ecoinvent 3.6 inventory databases supplemented from literature data and  
 9 available pilot plant operation. Two environmental impacts are quantified: primary  
 10 energy demand (PED) and (GHG) emissions, reported in MJ and gram CO<sub>2</sub>  
 11 equivalents (gCO<sub>2</sub>eq.) based on the most recent IPCC 100-year global warming  
 12 potential [37] respectively. The functional unit is defined as one MJ of ethanol, denoted  
 13 as MJ<sub>ethanol</sub>. When considering waste management, i.e., comparing bioethanol  
 14 production to landfill/incineration, results are also considered on the basis of 1 tonne  
 15 of treated MSW. The system boundaries start from the sorting and transportation of  
 16 MSW. Prior energy use and environmental burdens of the processes and products  
 17 that generated MSW are excluded in this study. Alternative LCA frameworks are used  
 18 to compare accounting methodologies dictated by biofuel policies in EU and US[7, 8].  
 19 The study employs energy allocation following current EU RED II policy to allocate co-  
 20 products benefits [7]: excluding avoided waste treatment, exergy allocation of  
 21 electricity and heat co-products (see Table S1 and Figure S1), and all other coproducts  
 22 evaluated by energy allocation. The study also considers the system expansion  
 23 method following US EISA/California LCFS policies: including avoided waste  
 24 treatment processes (credit to primary ethanol product) and all co-products evaluated  
 25 using system expansion (credit to primary ethanol product) [38].

## 1 2.4.2 Life Cycle Inventory

2 Inventory data was produced by adapting process models as developed for butanol  
3 and ethanol production previously [34] and supplemented from the Ecoinvent  
4 database and available literature data. The mass and energy balance data come from  
5 the process simulation model described in 2.3. The study assumes that the inventory  
6 data for the production of the inoculums of *S. cerevisiae*, *E. coli*, *S. pombe* would be  
7 similar to that of *Z. mobilis* [26, 39]. Inventory data of nutrients were obtained from  
8 publicly available data [40, 41] and GREET® Model developed by US Argonne  
9 National Laboratory [42]. The GHG emissions assigned to enzyme production in this  
10 study are 5.9 g CO<sub>2</sub>eq/g of produced enzyme (commercially Novozymes Cellic CTec2)  
11 [43], while studies investigating onsite enzyme production using cellulose as a  
12 feedstock have been reported to emit 4.1–11.5 g CO<sub>2</sub>eq/g cellulase [44, 45].

## 13 2.5 Financial Analysis

### 14 2.5.1 Capital and Operational Expenses

15 The study considers a plant capacity of 150,000 tonne MSW/yr operating 8000 hours  
16 per year. All major equipment items are designed (e.g., each fermenter has a fixed  
17 volume of 400 m<sup>3</sup>) and costed based on the material and energy flows from the model  
18 described in Section 2.1 using the factor method [46, 47]. Costs are then extrapolated  
19 to those of year 2019 based on the Chemical Engineering Plant Cost Index [48] as in  
20 equation 1:

$$C_{p,v,2018} = C_{p,u,r} \left(\frac{v}{u}\right)^n \left(\frac{I_{2019}}{I_r}\right) \quad (1)$$

21 where  $C_{p,v,2019}$  is the equipment purchase cost (free on board) with capacity  $v$  in the  
22 year of 2019,  $C_{p,u,r}$  is the reference equipment cost at capacity  $u$  in year  $r$ ,  $I_{2019}$  is cost  
23 index in the year of 2019 (= 607.5),  $I_r$  is cost index in year  $r$ . An exponent scaling factor  
24 ( $n$ ) of 0.6 is assumed. Due to economies of scale, the plant capital cost (CAPEX) per  
25 unit output decreases with increasing capacity. Similarly, for the same amount of  
26 feedstock input capacity, productivity and product yield influence CAPEX due to  
27 economies of scale.

28 The annual operating cost of the process is calculated as the sum of operating costs  
29 (OPEX) (labour, utility and chemical costs), plant overheads and maintenance cost  
30 (see Table 1). For the bioethanol production route, the fermentation turn-around time  
31 is 12 hours for all microorganisms while the batch cycle time differs amongst  
32 microorganisms: 36 hours for *S. cerevisiae* and *Z. mobilis*, 60 hours for *E. coli* and *S.*  
33 *pombe*, respectively [13]. Variable operational costs including materials and utilities  
34 are obtained from mass and energy balance model and publicly available data where  
35 appropriate. Enzyme (Novozymes Cellic CTec2/CTec3) used in this study has an  
36 indicative cost of 3-5 Euro/kg (3.4-5.7 \$/kg) [49].

1

Table 1 Summary of the cost model input data.

<b>Input Parameter</b>	<b>Value</b>	<b>Unit</b>	
<b><i>Fixed capital cost</i></b>			
OSBL	25%	[% compounded to erected cost]	
Installed Cost ISBL Lang factor	3.2	[-]	
Location factor	1.2	[-]	
Commissioning Cost	5%	[% FCI]	
Working Capital	10%	[% FCI]	
<b><i>Fixed Operating Cost</i></b>			
<b>Labour &amp; Supervision</b>	<b>Salary [\$] (2019)</b>	<b>Number</b>	<b>Cost [\$]</b>
Plant manager	154,460	1	154,460
Plant engineer	73,552	2	147,105
Maintenance supervisor	59,892	1	59,892
Maintenance technician	42,030	12	504,356
Lab manager	58,842	1	58,842
Lab technician	42,030	2	84,059
Shift supervisor	50,436	4	201,745
Shift operators	42,030	20	840,593
Yard employees	29,421	4	117,686
Clerks and secretaries	37,827	3	113,481
Total salaries			2,282,219
Labour burden	90 [%] of Total Salaries		2,053,997
<b>Total labor cost</b>			<b>4,336,215</b>
<b>Other overhead</b>			<b>Annual cost [\$]</b>
Maintenance	3 [%] of ISBL		2,090,429
Property insurance	0.7 [%] of FCI		573,201
<b>Total fixed operating cost</b>			<b>6,999,845</b>

2

### 3 2.5.2 Ethanol Selling Price

4 Time series analysis was used to forecast the long-term average price of ethanol.  
5 Takens' theorem was used as the basis for this analysis [50]. Takens' theorem states  
6 that for a deterministic system, the underlying state variables that created the time  
7 series are embedded within the data. Using this theorem; a deterministic, dynamic  
8 system can be reconstructed based on the observed time series. Such a forecast  
9 model, constructed using only the embedded state variables, assumes that the market  
10 drivers underpinning the trajectory of the state variables in phase space remain largely  
11 unchanged. Particularly, policy frameworks and market forces are assumed to remain  
12 largely unchanged over the forecast period. An embedding dimension of ten was used  
13 to reconstruct the ethanol price model from weekly spot price data obtained from  
14 publicly available daily price history between 2012 and 2018 [51]. In this work, a Radial  
15 Basis Function Neural Network (RBFNN) containing 8 neurons was used as a model

1 to predict the future ethanol price [52, 53]. The RBFNN was trained as a one step  
 2 ahead predictor by minimising the mean squared error of the difference between the  
 3 actual and predicted prices. Once trained, the RBFNN was evaluated (tested) in free  
 4 run mode, where successive predicted prices (outputs) become inputs to the RBFNN.  
 5 The confidence limits corresponding to the trained RBFNN were calculated as a  
 6 reliability measure of the prediction Leonard, Kramer [53]. In addition to the forecast  
 7 long-term average ethanol price, the study considers sensitivity of results by  
 8 considering the minimum and maximum ethanol price within the dataset (2012 to  
 9 2018).

### 10 2.5.3 Investment Analysis

11 All sources of cost and income must be determined to inform an investment analysis.  
 12 This study used a discounted cash flow analysis, where capital and operational costs  
 13 are discounted and totalled to a cumulative NPV to determine the most cost-effective  
 14 option among different alternatives.

$$NPV = \sum_{t=0}^{20} \frac{I_t - C_t}{(1+i)^t} \quad (2)$$

15 where total sources of income  $I_t = I_{ethanol} + I_{electricity} + I_{by-products} + I_{RTFC} + I_{gate\ fee}$ , sources  
 16 of incomes are shown in Table 2; total sources of cost  $C_t = CAPEX + OPEX$ , we  
 17 assume an 8% of discounted rate ( $i$ ) of return for a plant life of 20 years ( $t$ ). We consider  
 18 a corporation tax rate of 20% and depreciation of 10 years.

19 Table 2 Sources of incomes for ethanol and incineration plant.

Sources of income	Price	Unit	Ref
Recovered metals	0.25	£/kg	[54]
	0.33	\$/kg	
Recovered plastic	0.01	£/kg	[54]
	0.013	\$/kg	
Landfill gate fee with tax	113.00	£/tonne	[55]
	147.53	\$/tonne	
Autoclave gate fee	85.00 (80.00-90.00)	£/tonne	[56]
	110.98	\$/tonne	
Autoclave fibre waste	20.00	£/tonne	[56]
	26.11	\$/tonne	
RTFC (Renewable Transport Fuel Certificates)	£0.18	£0.12-0.22 per RTFC	[9]
	\$0.24	\$0.17-0.32	
Ethanol	See section 2.5.2		Time series analysis model
Electricity wholesale	£0.0748	£/MJ	[57]
	\$0.027	\$/MJ	

1

## 2 **3 Results and Discussion**

### 3 **3.1 Material and Energy Balance**

4 The overall input to the process was 150,000 tonne MSW per annum, of which 31.8wt%  
5 was dry convertible lignocellulosic content (53wt% wet). Glucose and xylose content  
6 of the input waste stream was measured experimentally as 14.3wt% and 1.6wt%.  
7 Given a hydrolysis yield of 38% for glucose and 70% for xylose [34], total sugar  
8 production of 971 kg/hr glucose and 198 kg/hr xylose was achieved. Optimisation of  
9 the hydrolysis process may achieve higher sugar yields, which would proportionally  
10 increase the downstream output of ethanol. The implications of achieving hydrolysis  
11 yields as high as 85% is considered in Section 3.3.

12 As reported previously [13], ethanol yield from sugar varies significantly between the  
13 considered microorganisms, with *S. cerevisiae* and *Z. mobilis* achieving relatively high  
14 yields (70wt% of theoretical) compared to *S. pombe* (51wt% of theoretical) and *E. coli*  
15 (34wt% of theoretical). These yields are within the range of previous published results,  
16 ranging from 44% to 74% of theoretical ethanol yield [58, 59], but lower than ethanol  
17 yield from sugar derived from agricultural feedstocks (e.g., 90wt% from corn stover  
18 sugars [26]). Overall, ethanol production from MSW is approximately 22 kg ethanol/wet  
19 tonne MSW for the highest yielding microorganisms, *S. cerevisiae* and *Z. mobilis*. This  
20 is significantly lower than previous reported results, which range from ~70 to 160 kg  
21 ethanol/wet tonne MSW [58-60]. The low ethanol yield in the current study arises due  
22 to the relatively low hydrolysis sugar yield (38wt%), and the low lignocellulosic content  
23 of the MSW feedstock (53wt% in current study vs 79wt% to 100wt% in comparator  
24 studies as above). The difference may be also due to the geographical variations, i.e.,  
25 UK MSW in this study versus US MSW as reported in the above literatures.

26 Total energy yield from MSW, including ethanol and co-product electricity, ranges from  
27 14% to 16% of energy content of the input MSW. Including excess co-generated heat  
28 would increase the energy yield to ~24%, if useful applications can be found (e.g., co-  
29 location with an industrial process/district heating, for sterilization, or for cooling  
30 generation) (Table 3). Ethanol represents a small share of the energy outputs of the  
31 system, ranging from a maximum of 4.5% of the energy content of MSW for *S.*  
32 *cerevisiae* and *Z. mobilis*, to 2.2% for *E. coli*. In contrast, much higher overall energy  
33 yield of ethanol production from corn stover is reported at 47% [26], of which ethanol  
34 comprises 92%.

35

1 Table 3 Overall mass and energy balance of ethanol fermentation production from  
 2 MSW.

	<i>S. cerevisiae</i>		<i>Z. mobilis</i>		<i>E. coli</i>		<i>S. pombe</i>	
<b>Inputs</b>	Tonne/y	Value	Tonne/y	Value	Tonne/y	Value	Tonne/y	Value
	r	MW	r	MW	r	MW	r	MW
MSW (40% moisture)*	150000	64.6	150000	64.6	150000	64.6	150000	64.6
<b>Total input</b>		64.6		64.6		64.6		64.6
<b>Outputs</b>								
Ethanol	3277	2.9	3218	2.9	1592	1.4	2393	2.1
Recycled plastics	13830		13830		13830		13830	
Recycled metals								
Total heat generation		10.3		10.3		10.5		10.4
Total electricity generation		8.9		8.9		9.1		9.0
<b>Total output</b>		22.1		22.1		21.1		21.6
Total heat demand		4.7		4.7		4.7		4.7
<i>Autoclave+Biorefinery</i>		4.7		4.7		4.7		4.7
Total electricity demand		1.7		1.7		1.7		1.7
<i>Autoclave+Biorefinery</i>		0.5		0.5		0.5		0.5
Net heat surplus		5.5		5.6		5.8		5.7
Net electricity surplus		7.2		7.3		7.5		7.4
<b>Energy efficiency (main product - net electricity surplus)</b>		15.7%		15.7%		13.8%		14.7%
<b>Energy efficiency (main product - net electricity surplus)-Ethanol from cron stover (Humbird et al., 2011)</b>		47.0%		47.0%		47.0%		47.0%

3

## 4 3.2 Life Cycle Assessment

### 5 3.2.1 Greenhouse Gas Emissions Evaluated Under Current Policies

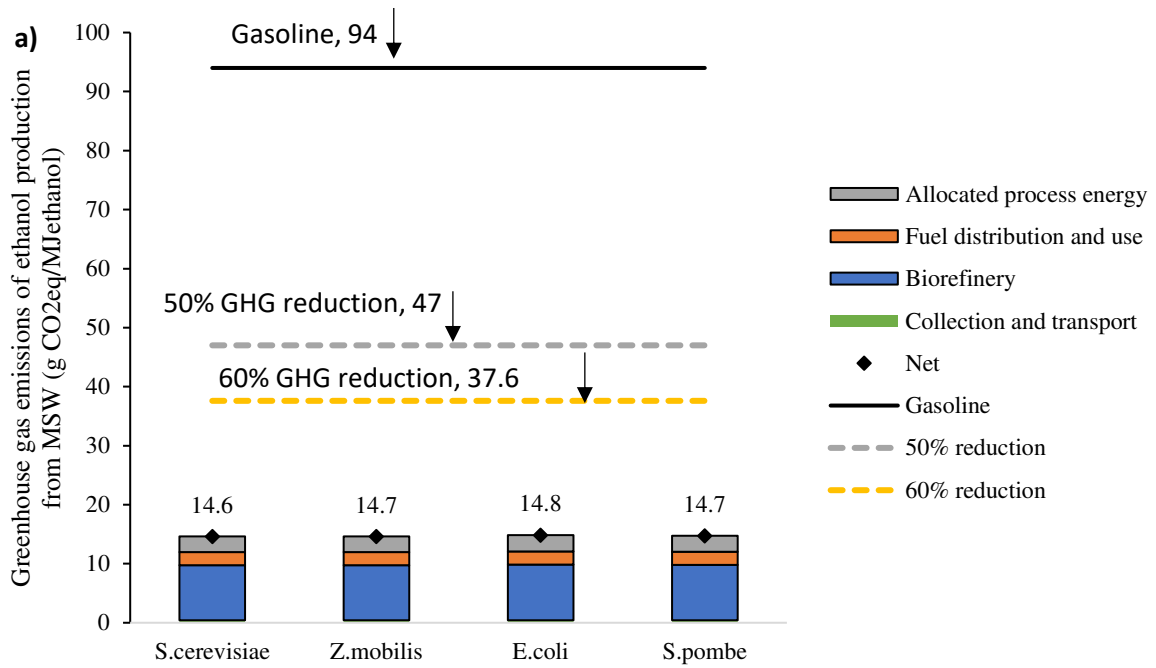
6 The assessment of GHG emissions for ethanol production from MSW varies  
 7 substantially between assessment methodologies mandated by EU and US policies  
 8 (Figure 3) (the results of PED can be found in Figure S2). However, in all cases, low  
 9 GHG emissions can be achieved compared to conventional fuels and emissions  
 10 reduction requirements can be met. Employing the EU RED II methodology (Figure  
 11 3a), biorefinery emissions are allocated between ethanol and co-product electricity.  
 12 Overall GHG emissions are nearly identical for all microorganisms (~15 gCO<sub>2</sub>eq./MJ  
 13 or 84% GHG emissions reduction relative to gasoline) due to the allocation approach.  
 14 Dependent on higher or lower ethanol yields, a proportional share of emissions  
 15 associated with waste collection and biorefinery operations is allocated to ethanol.  
 16 Ethanol production thus achieves classification as a renewable biofuel by exceeding  
 17 the emissions target of at least 50% lower than that of the fossil fuel they replace (pre  
 18 January 2018 installations) and 60% (installations from January 2018) [10].

1 When employing the system expansion method as in US EISA and CA LCFS policies,  
2 it is noted that the system under all microorganisms cases show large reductions in  
3 GHG emissions, but this result depends on microorganism-specific ethanol yield  
4 (Figure 3b). Net GHG emissions range from -53 to -124 gCO<sub>2</sub>eq./MJ ethanol (including  
5 co-products credits of excess electricity and recyclable materials, but excluding  
6 avoided waste treatment), reductions of 156% to 231% relative to gasoline. As  
7 reported previously (e.g., [61]), lower ethanol yield (i.e., lower denominator in the  
8 calculation) results in the greatest reduction in GHG emissions due to higher output of  
9 co-products per unit of ethanol produced. Inclusion of avoided waste treatment results  
10 in substantially negative net GHG emissions, due to diversion of biogenic wastes from  
11 landfill and of plastics from incineration. The study assumes that incoming MSW would  
12 otherwise be treated by incineration (71%) and landfilling (29%), based on current  
13 practices in UK [62]. Therefore, diverting MSW from current waste treatment  
14 contributes to reducing GHG emissions for the waste to ethanol process. On the basis  
15 of per MJ ethanol, MSW-derived ethanol remains carbon negative for all four strains  
16 with landfill/incineration avoidance (-544.8 to -1136.7 kg CO<sub>2</sub>eq/MJethanol or 680% to  
17 1309% GHG reduction relative to gasoline).

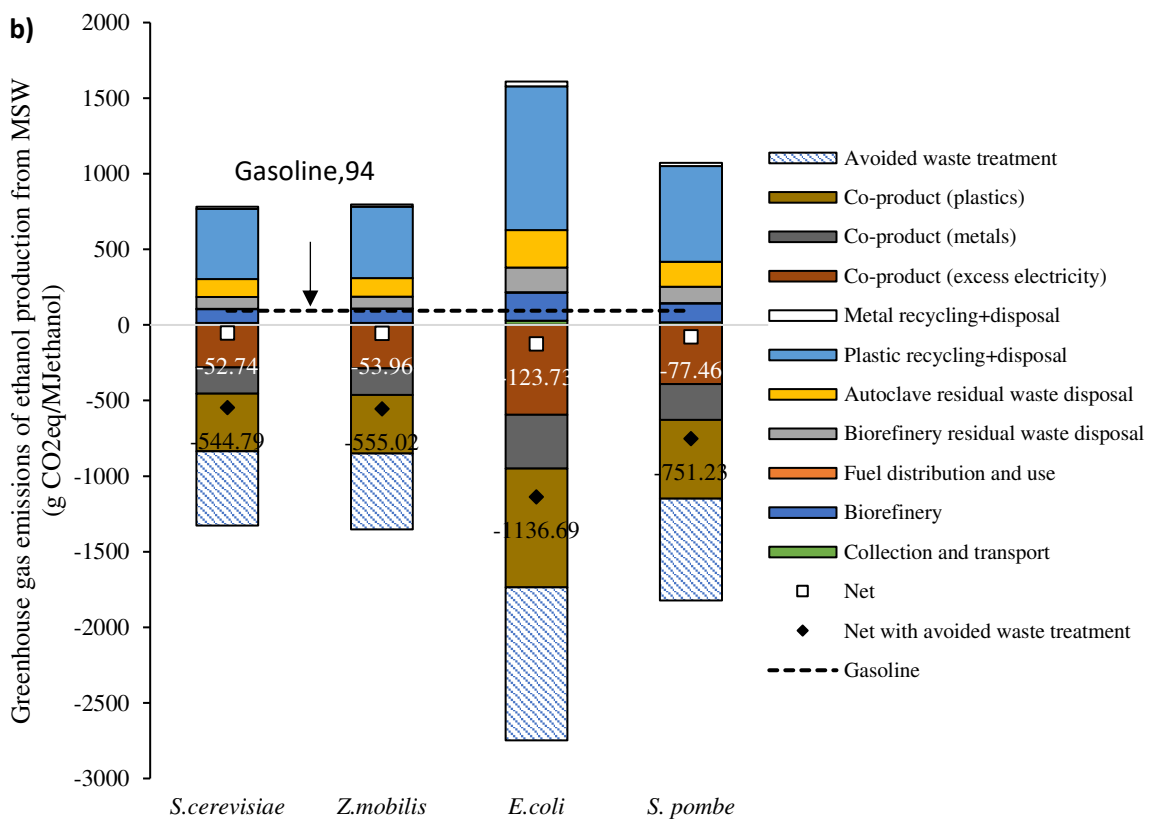
18 Primary due to the lower ethanol yield as stated above, LCA results are lower  
19 compared with previous reported GHG emissions of ethanol production from MSW,  
20 ranging from 35 to 68 gCO<sub>2</sub>eq./MJ ethanol when using the system expansion  
21 approach and excluding avoided waste treatment (see Figure S3) [58-60, 63]. LCA  
22 results are not directly comparable between studies, due to differences in study  
23 methodology (e.g., system boundaries; co-product considerations; treatment of  
24 residual wastes) and data/assumptions (waste composition; enzyme production  
25 impacts and enzyme loading; product yields) but provide a reasonable point of  
26 comparison. Generally, MSW derived liquid biofuels have smaller GHG emissions  
27 than ethanol produced from corn and sugarcane [23], primarily due to the credits from  
28 a diverse range of material and energy co-products even with the exclusion of credits  
29 from avoided waste treatment.

30 The LCA results presented here are specific to the UK context. With the system  
31 expansion approach, mandated by US policies, GHG emissions results are sensitive  
32 to 1) the electricity grid mix, as co-product electricity generates a “credit” by displacing  
33 grid generation; 2) the current waste treatment mix, as avoiding conventional  
34 treatment also generates a GHG emissions “credit”. In locations with a more GHG-  
35 intensive electricity mix, or a larger share of waste currently destined to landfill, the  
36 GHG emissions benefits of producing ethanol would be greater than the results here  
37 indicate. In contrast, results based on the allocation-based approach required by EU  
38 policy are independent of these factors, and so results are likely to be broadly similar  
39 in different locations.

40



1



2

3 Figure 3 Life cycle greenhouse gas emissions associated with ethanol production  
 4 from municipal solid waste under a) allocation method employed in EU RED  
 5 methodology, and b) system expansion method based on US EISA/CA LCFS policy.

6

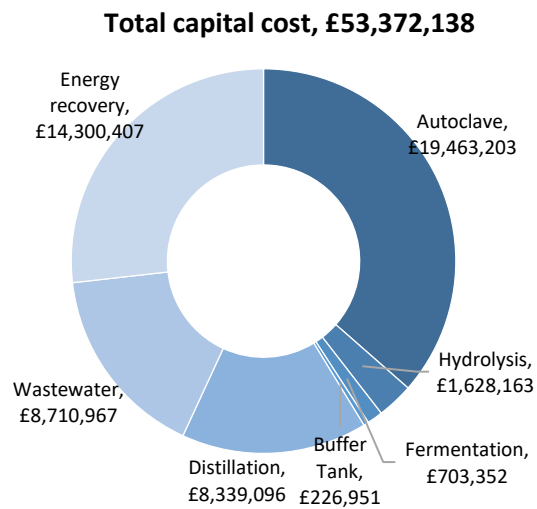
### 1 **3.3 Financial Analysis**

#### 2 **3.3.1 Costs of Bioethanol Production**

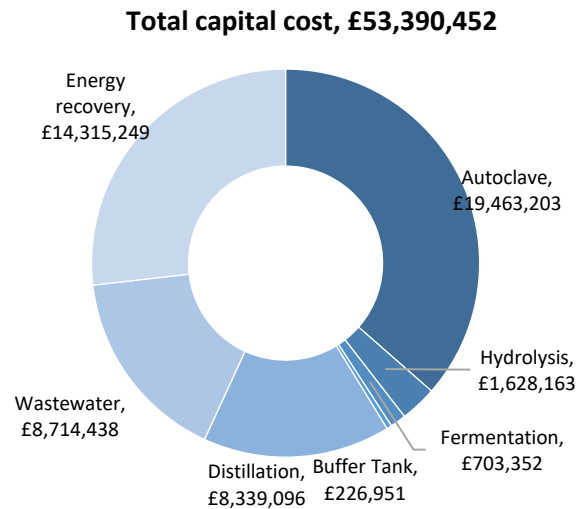
3 Biorefinery CAPEX (~£53 million (~\$70 million)) and OPEX (~£7.6 million (~\$9.9  
4 million)) is similar for all microorganisms considered (Figures 4 and 5, respectively),  
5 despite significant differences in fermenter equipment size and cost. Fermenter  
6 CAPEX is highly dependent on the volumetric productivity of the microorganisms, but  
7 accounts for only ~2% of total CAPEX and so has minimal overall impact. Installed  
8 Fermenter costs range from £0.7 million (\$0.92 million) to £1.4 million (\$1.84 million),  
9 for 36 hour batch cycle time (*S. cerevisiae* and *Z. mobilis*) and 60 hour batch cycle  
10 time (*E. coli* and *S. pombe*). Product yield has a minor influence (2% to 3%) on  
11 wastewater treatment CAPEX, as higher ethanol yields correspond to lower residual  
12 microbial biomass. Equipment costs for processes common to all microorganism  
13 scenarios dominate the CAPEX: the autoclave alone accounts for ~36% of CAPEX;  
14 energy recovery 27%; and distillation 16%.

15

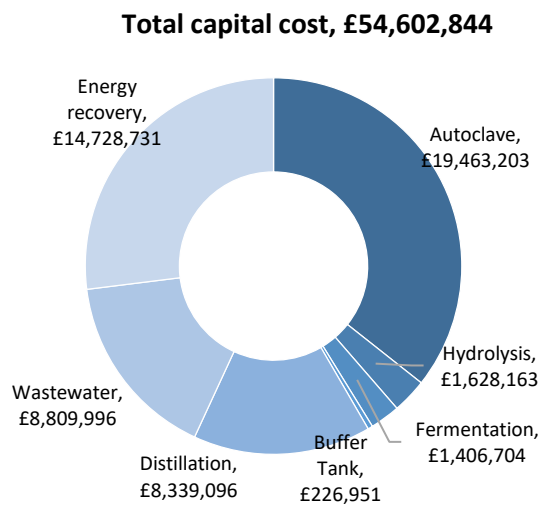
### *S. cerevisiae*



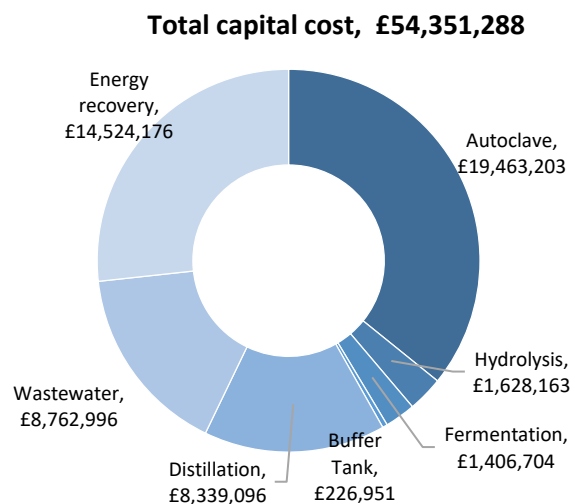
### *Z. mobilis*



### *E. coli*

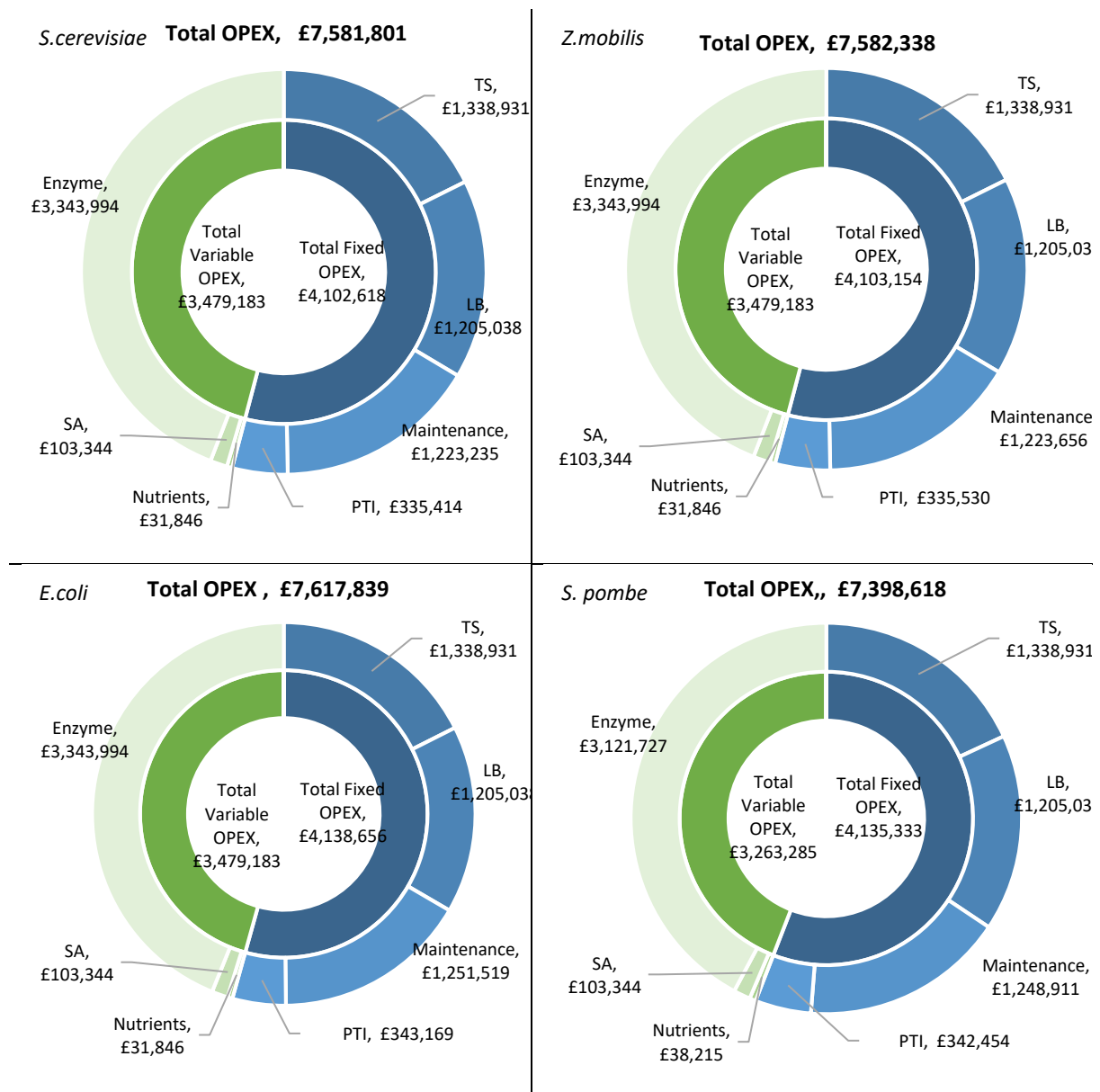


### *S. pombe*



1 Figure 4 Fixed capital cost of MSW to ethanol using four different microorganisms-  
2 *S. cerevisiae*, *Z. mobilis*, *E. coli*, *S. pombe*.

3 Fixed operating costs comprise approximately 54% of OPEX; of this total, labour costs  
4 are common for all scenarios, while maintenance, property taxes, and insurance are  
5 proportional to CAPEX and so little changed. Most variable OPEX items are common  
6 to all microorganisms, with enzyme costs for hydrolysis representing 96% of the total.  
7 The sensitivity of the financial analysis to enzyme costs is considered in Section 3.4.4.  
8 Nutrient requirements are dependent on the generation of microbial biomass, and so  
9 are higher for lower ethanol yielding microorganisms, but this difference does not  
10 substantially influence overall operating costs.



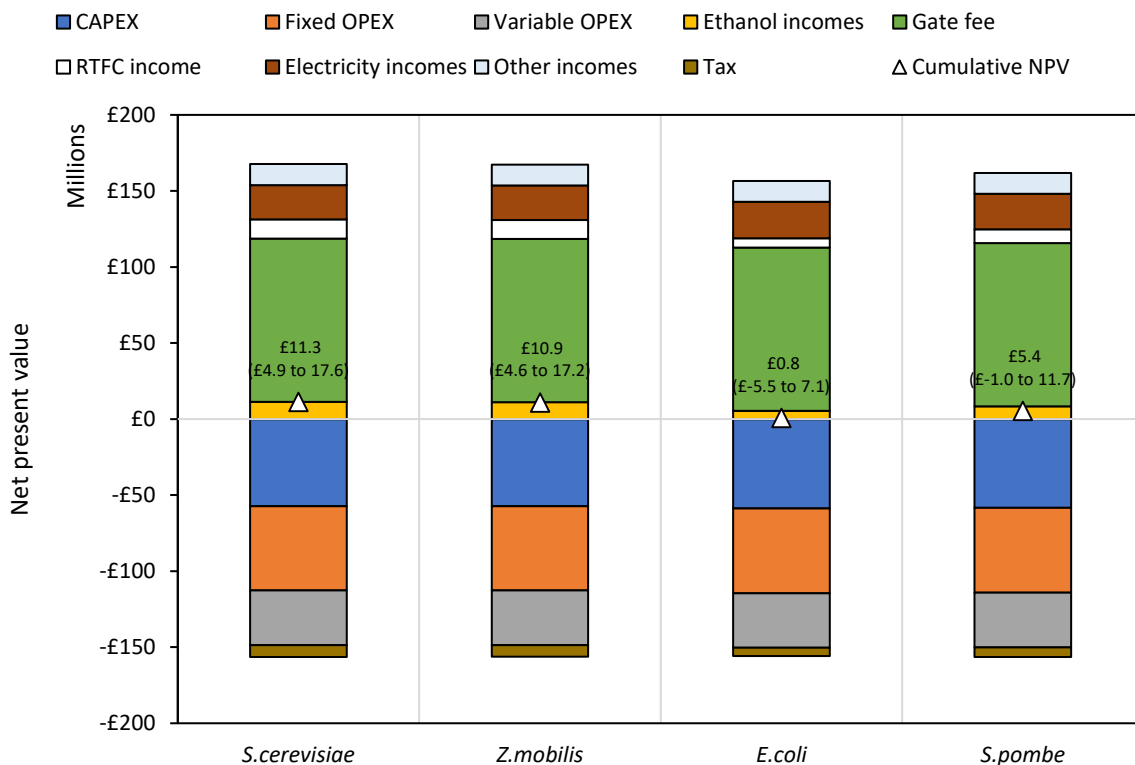
1 Figure 5 Total operating cost of MSW to ethanol using four different microorganisms-  
 2 *S. cerevisiae*, *Z. mobilis*, *E. coli*, *S. pombe*. Note: OPEX= Operating cost, TS= Total  
 3 salaries, LB= Labour burden, PTI= Property taxes and insurance, SA= Sulfuric acid  
 4 (93%)

5 **3.3.2 Revenues of Ethanol Biorefinery and Overall Investment Analysis**

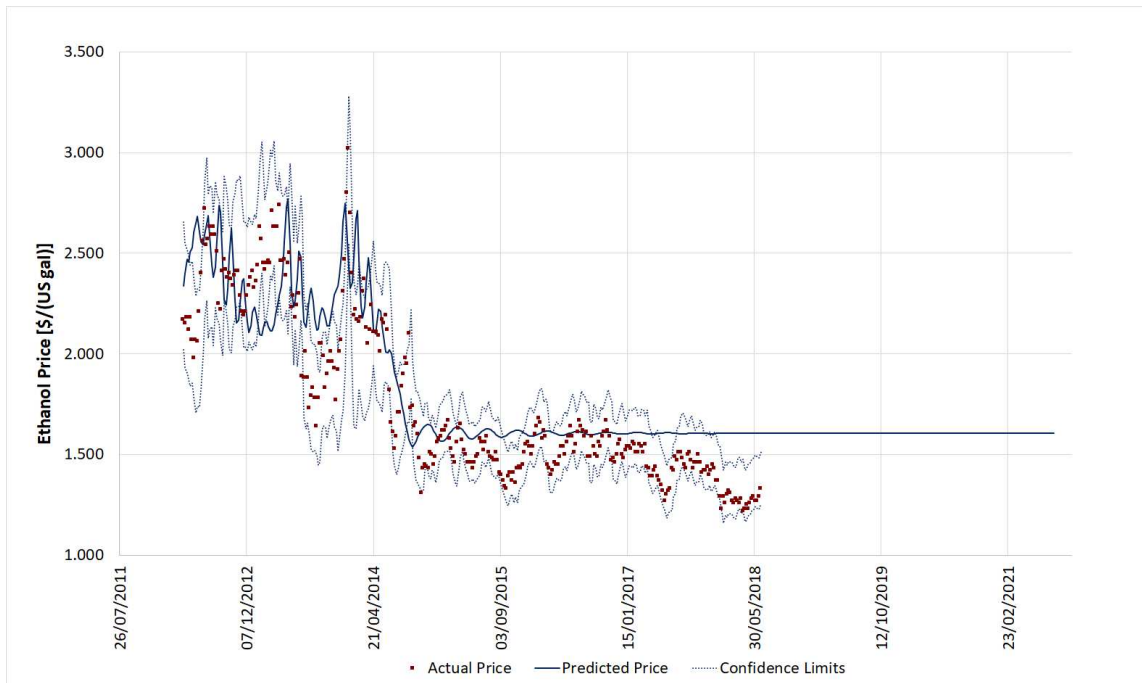
6 From Figure 6, a positive NPV can be achieved for all microorganisms (*S. cerevisiae*  
 7 achieves the largest cumulative NPV), indicating a viable investment. However, this  
 8 arises due to the benefit of gate fees received by diverting wastes to autoclave and  
 9 ethanol production (64% of total revenues), rather than from revenues from ethanol  
 10 sales (7% of total revenues) (Figure 6). As such, the financial viability of ethanol  
 11 production from MSW is heavily dependent on its competitiveness with other waste  
 12 treatment options, and on policy instruments, such as the RTFC. The UK's landfill tax  
 13 that provide financial disincentive to dispose of wastes in landfill does not directly  
 14 contribute to biofuel production. Ethanol sales (based on time series predicted ethanol

1 price of £1.23/US gal (\$1.61/US gal based on an exchange rate of 1.3 \$/£) in Figure  
 2 7) and the value of associated RTFCs make a relatively small contribution to the  
 3 overall financial viability of the process, representing between 8% and 15% of total  
 4 revenues for all microorganisms. Variable OPEX costs related specifically to ethanol  
 5 production – principally, the cost of enzyme input (£3,343,994/yr) – exceed revenues  
 6 from ethanol sales and RTFCs in the base case (£2,844,364/yr), indicating ethanol  
 7 production is not financially viable in these circumstances. In Section 3.3.3, the study  
 8 considers in greater detail the relative merits of ethanol production through a  
 9 comparison with an alternative scenario where autoclave fibre is instead incinerated  
 10 to generate renewable electricity in an offsite incineration plant.

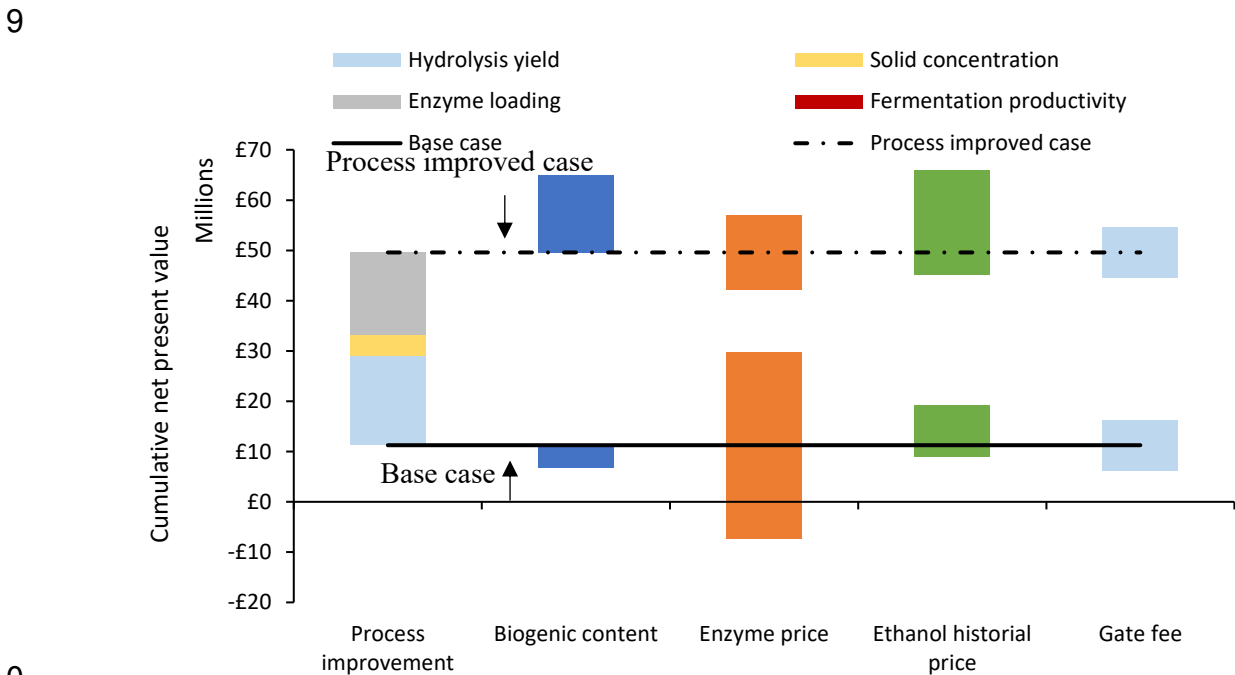
11 Key process improvements must be achieved to improve the financial performance of  
 12 ethanol production from MSW, specifically improving hydrolysis yield (to increase  
 13 ethanol output), reducing enzyme loading rate (to reduce variable OPEX), and, to a  
 14 lesser extent, increasing solid loading rate to the “Process improved case” as in Figure  
 15 8. Alongside these beneficial improvements, the production system would benefit  
 16 further from non-process improvements by identifying waste streams with higher  
 17 biogenic fraction, including residual waste from material recovery facilities (82wt%,  
 18 based on standard composition of waste collected from households with recyclates  
 19 removed at an material recycling plant prior to delivery to the autoclave plant, as in  
 20 Table S2), or by isolating the organic fraction of MSW (see Figure 8). Ethanol  
 21 production from MSW can be financially viable if key process improvements are  
 22 achieved. Enzyme cost has considerable gearing on the financial viability of the  
 23 process. Reducing enzyme unit cost and/or enzyme loading is critical for the financial  
 24 viability of this (and other) biofuel production processes. Moreover, ethanol selling  
 25 price influences ethanol sales revenues and thus has an impact on NPV.



1 Figure 6 Cost and cumulative NPV for MSW to ethanol using *S. cerevisiae*, *Z.*  
 2 *mobilis*, *E. coli*, *S. pombe cerevisiae* (the range of NPV values vary due to the range  
 3 of gate fee: £80–90/tonne).



4  
 5 Figure 7 Forecast for ethanol price, bounded by the confidence limits as obtained  
 6 for the radial basis function neural network trained on actual (historical) price data. It  
 7 shows the modelled ethanol price based on historical prices and the predicted long-  
 8 term average price as £1.23/US gal (\$1.61/US gal).



10

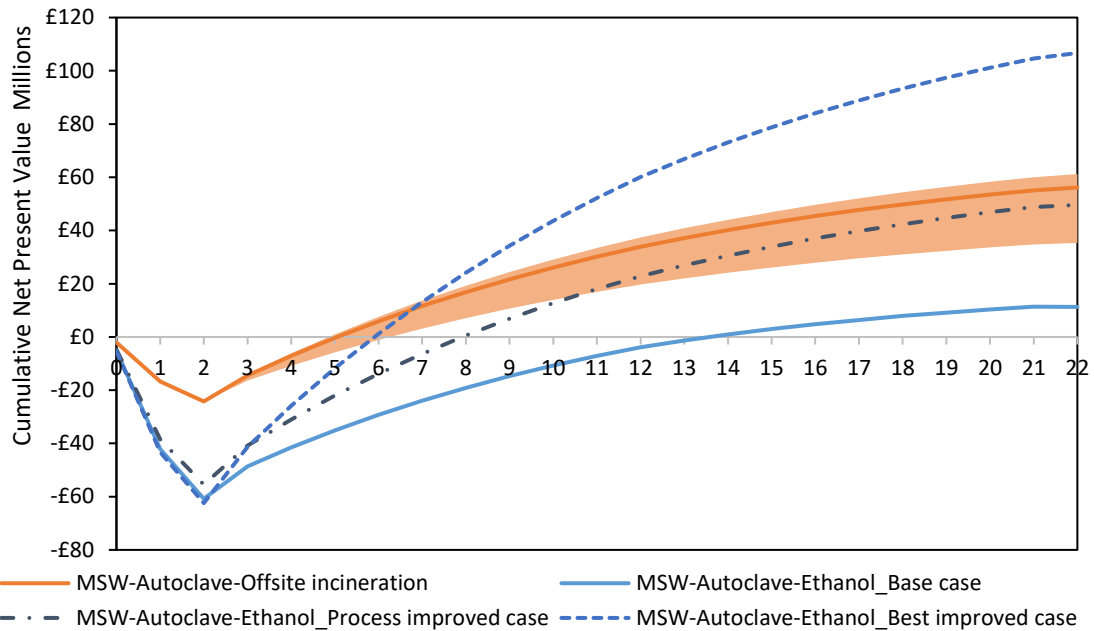
1 Figure 8 Sensitivity analysis of the values of cumulative net present value of MSW  
2 derived ethanol at various process parameters and enzyme prices based on *S.*  
3 *cerevisiae*. Solid line shows the “base case”, dashed line shows the “process  
4 improved case” (process variables: hydrolysis yield from 38% to 85%, solid  
5 concentration from 20% to 30%, enzyme loading from 5 wt% to 2 wt%, fermentation  
6 productivity from 0.75 g·L<sup>-1</sup>·h<sup>-1</sup> to 1.5 g·L<sup>-1</sup>·h<sup>-1</sup>). Non-process variables: biogenic  
7 content: 53wt%-82wt%, enzyme price: £0.87-£4.4/kg (€1-5/kg); ethanol historical  
8 price 2012-2018: £0.93-£2.31/US gal ((\$1.22-\$3.02/US gal) [51]; gate fee: £80-  
9 90/tonne.

10

### 11 3.3.3 Comparison with Offsite Incineration

12 The preceding results indicate that ethanol production from MSW can be financially  
13 viable if key process improvements are achieved. However, given the small  
14 contribution of ethanol product to revenues, it is worth considering if this option is  
15 competitive against other opportunities to divert waste from current waste treatment  
16 processes. Towards this aim, this study evaluates an alternative scenario where the  
17 autoclave fibre is instead sent to offsite incineration to generate renewable electricity.  
18 The aim of this strategy is to reduce the total quantity of waste requiring conventional  
19 landfill and thus avoiding landfill gate fees, while still enabling the recovery of non-  
20 biogenic recyclates. In this strategy, the autoclave technology remains central. This  
21 approach reduces CAPEX and OPEX requirements by excluding ethanol production  
22 but forgoes revenues from ethanol sales and RTFCs.

23 Incineration of autoclaved MSW fibre diverts 150,000 tonne/yr from conventional  
24 landfill disposal or direct incineration. After autoclave processing, a quantity of  
25 autoclaved fibre (biogenic content of MSW), 79,500 tonne/yr, would then be sold to an  
26 incineration plant receiving a potential revenue of £20/tonne (\$26/tonne) according to  
27 Wilson Bio-Chemicals [56]. This will increase overall gate fee benefits (£85/tonne  
28 incoming MSW + £20/tonne autoclaved fibre). Incineration of the autoclaved fibre  
29 provides a higher cumulative NPV from the generation of renewable electricity than  
30 the ethanol production base case, principally by reducing CAPEX expenditure by 60%  
31 (Figure 9). Annual revenues from the ethanol system (base case) exceed those of the  
32 alternative incineration scenario. As discussed previously, this is primarily from gate  
33 fees charged to the incoming wastes to autoclave. After ethanol production and  
34 recycle recovery, only ~28,000 t/yr of residual waste needs disposing of by  
35 conventional routes. Process improvements (the improved base case in Figure 8 or  
36 the medium improved case in Figure 9) for ethanol production from autoclaved MSW  
37 (hydrolysis yield; enzyme loading; solids loading) and enzyme/ethanol cost/gate fee  
38 improvements (forming the best improved case in Figure 9) would achieve a superior  
39 financial outcome to offsite renewable electricity energy recovery, with revenues from  
40 ethanol sales justifying the greater CAPEX investment required.



1

2 Figure 9 Cumulative NPV over project years for bioethanol production and offsite  
 3 incineration of autoclaved MSW. In the shaded areas, the bottom borderline  
 4 represents lower gate fee (£80/tonne) and the top borderline represents the higher  
 5 gate fee (£90/tonne) relative to the base case (£85/tonne, the orange line in the  
 6 middle). The solid line represents the base case MSW to ethanol production. The  
 7 dashed line represents the medium and best improved MSW to ethanol production,  
 8 respectively. Process improved case: with process improvements only; Best  
 9 improved case: process improvement and non-process improvement (i.e., external  
 10 enzyme/ethanol cost/gate fee improvements as in Figure 8).

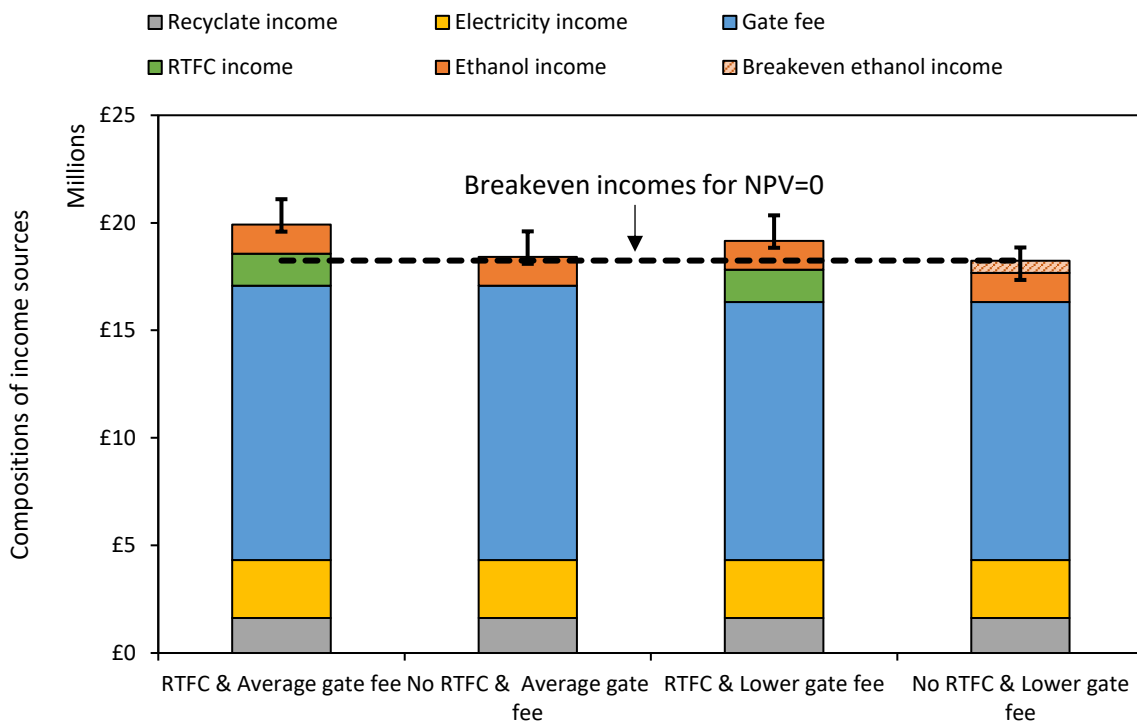
11

### 12 3.3.4 Role of Policy in Supporting Biofuel Production from Wastes

13 Utilisation of wastes for biofuel production in the UK benefits from significant policy  
 14 support to improve financial viability (RTFCs). This study compares the ethanol market  
 15 price required to break even (NPV = 0) in the absence of this policy support to  
 16 understand the viability of this opportunity in jurisdictions without equivalent support  
 17 (Figure 10). As discussed previously, RTFC (£0.12 to £0.22 per RTFC and waste  
 18 derived biofuels receive double RTFC per litre) is a key financial driver for ethanol  
 19 production from MSW. In the absence of RTFC, diversion of wastes to ethanol  
 20 production provides a much smaller benefit, requiring a break-even ethanol market  
 21 price of £1.75/US gal (\$2.29/US gal) under a lower gate fee (£80/tonne). As this is on  
 22 the high end of the range of historic ethanol market prices (£0.93-£2.31/US gal  
 23 (\$1.22-\$3.02/US gal), 2012 to 2018 [51]), ethanol production from MSW without  
 24 financial incentives is difficult to be financially viable. Producing a higher value  
 25 alternative to ethanol could potentially address this issue, looking outside of transport  
 26 fuel markets and can be the focus of future work.

1 RTFCs play a less significant role in the financial performance of MSW-derived ethanol  
 2 in the UK compared to gate fee incomes. With current gate fee (£80-90/tonne), ethanol  
 3 production from MSW remains financially viable in the absence of RTFCs, with a  
 4 breakeven gate fee of £83.8/tonne (Figure 10). Although the breakeven gate fee is  
 5 less than the median incineration gate fee of £89/tonne, it is less competitive than that  
 6 of in-vessel composting (£50/tonne) and anaerobic digestion of mixed food waste  
 7 (£27/tonne) [55].

8 Ethanol production from MSW delivers GHG savings, but the monetised value of  
 9 emissions reductions is far less than main revenue sources. The social cost of carbon  
 10 reported by UK Department for Business, Energy & Industrial Strategy is  
 11 £12.76/tCO<sub>2</sub>eq with a range of £2.33-25.51/tCO<sub>2</sub>eq [64]. As above, MSW-derived  
 12 ethanol can reduce approximately 79 gCO<sub>2</sub>eq/MJ relative to gasoline (Figure 3).  
 13 Therefore, it can save about 7,008 tCO<sub>2</sub>eq/year equivalent to a carbon value of about  
 14 £89,426/yr compared with much larger incomes from gate fee payments  
 15 (~£13,500,000/yr) and RTFC payments (~£1,495,220/yr). It is noted that the value of  
 16 GHG reduction is £0.02/L while the RTFC payment is £0.24-0.44/L. RTFC is well  
 17 beyond the value of achieved GHG reductions from MSW derived ethanol. In the future,  
 18 multiple viable opportunities may exist to utilise MSW (e.g., current anaerobic  
 19 digestion or composting process) and therefore the role of a single use in avoiding  
 20 conventional waste treatment would be questionable. The development of a relevant  
 21 policy support framework that can account for the complexities of waste-to-  
 22 biofuels/products is essential to promote the sustainable development of  
 23 decarbonisation of the waste management, energy and transportation sectors.



24

25 Figure 10 Compositions of income sources based on *S. cerevisiae* (error bars show  
 26 the range of historical ethanol prices in 2012-2018).

## 4 Conclusions

The study assesses the current and future viability of bioprocessing of municipal solid waste feedstock to ethanol. The overall environmental and cost implications of converting MSW to ethanol using four fermentative microorganisms (i.e., *S. cerevisiae*, *Z. mobilis*, *E. coli*, *S. pombe*) are compared via LCA and techno-economic analysis based on process simulation of operation at commercially relevant scale. We consider three different techno-economic scenarios: Base case (based on current experimental evidence); Process Improved case (with anticipated process improvements (solid loading rate, hydrolysis yield, fermentation productivity, and enzyme loading); and Best Case (with anticipated process improvements and favourable market conditions (gate fees; product markets)).

Results based on experimental data and process modelling indicate that MSW-derived ethanol can significantly reduce GHG emissions relative to gasoline (84% reduction following EU RED calculation methodology, and by 156% to 231% reduction following the US EISA methodology). Financial analysis highlights that microorganisms achieving high ethanol yield and productivity (*S. cerevisiae* and *Z. mobilis*) are promising candidates for waste biorefining. Key process improvements must be achieved to improve the financial viability of ethanol production from MSW and deliver a clear advantage over waste incineration for renewable electricity generation, specifically improving hydrolysis yield (to increase ethanol output), reducing enzyme loading rate (to reduce variable OPEX) or using non-enzymatic hydrolysis, e.g. using acid hydrolysis, and, to a lesser extent, increasing solid loading rate. Future work can investigate supply chain and facility design optimisation (e.g., capacity; co-location) for comprehensive system analysis towards commercialisation of waste to biofuel production.

Utilisation of wastes for biofuel production in the UK benefits from significant policy support and financial support for renewable fuels (RTFCs). A positive net present value can be achieved with ethanol production from MSW, but this arises due to the benefit of gate fees by diverting wastes to ethanol production and RTFCs, rather than from revenues from ethanol sales. As such, the financial viability of ethanol production from MSW is heavily dependent on its competitiveness with other waste treatment options, and on policy instruments, such as the UK's landfill tax, that provide financial disincentive to dispose of wastes in landfill and RTFCs, that provide incentives to waste to biofuels. The comparatively low market value of ethanol at present would favour the bio-production of higher value commodity chemicals from MSW; in future, the strategic requirement for low carbon liquid fuels to meet net zero emissions targets (e.g., aviation, long distance transport) could provide higher market value for biofuels than the current ethanol market.

## 5 Notes

The authors declare no competing financial interest.

## 6 Acknowledgment

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1 Biotechnology processes. Fermentation studies were supported by a BBSRC  
2 industrial Collaborative Award in Science and Engineering (iCASE) studentship with  
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#### 4 **Author Contributions**

5 Conceptualisation: F.M., A.D., S.M.M., A.C., J.M.; Methodology: F.M., A.D., A.C., J.M.;  
6 Software: F.M., A.D., A.C., J.M.; Formal Analysis: F.M., A.D., S.M.M., G.H.T., A.C.,  
7 J.M.; Investigation: F.M., A.D., A.C., J.M.; Writing – Original Draft: F.M.; Writing –  
8 Review & Editing: F.M., A.D., S.M.M., G.H.T., A.C., J.M.; Visualisation: F.M., A.D.,  
9 A.C., J.M.; Supervision: S.M.M., G.H.T., J.M.; Funding Acquisition: S.M.M., G.H.T.,  
10 A.C., J.M.

#### 11 **7 References**

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13 Waste. 2020. Available at:  
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15 [ment\\_data/file/918270/UK\\_Statistics\\_on\\_Waste\\_statistical\\_notice\\_March\\_2020\\_acc](https://assets.publishing.service.gov.uk/government/uploads/system/uploads/attachment_data/file/918270/UK_Statistics_on_Waste_statistical_notice_March_2020_accessible_FINAL_updated_size_12.pdf)  
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