

This is a repository copy of Towards a Phaeodactylum tricornutum biorefinery in an outdoor UK environment.

White Rose Research Online URL for this paper: <a href="https://eprints.whiterose.ac.uk/id/eprint/180534/">https://eprints.whiterose.ac.uk/id/eprint/180534/</a>

Version: Accepted Version

## **Article:**

Butler, T.O., Padmaperuma, G., Lizzul, A.M. et al. (2 more authors) (2022) Towards a Phaeodactylum tricornutum biorefinery in an outdoor UK environment. Bioresource Technology, 344 (Part B). 126320. ISSN: 0960-8524

https://doi.org/10.1016/j.biortech.2021.126320

© 2021 Elsevier Ltd. This is an author produced version of a paper subsequently published in Bioresource Technology. Uploaded in accordance with the publisher's self-archiving policy. Article available under the terms of the CC-BY-NC-ND licence (https://creativecommons.org/licenses/by-nc-nd/4.0/).

#### Reuse

This article is distributed under the terms of the Creative Commons Attribution-NonCommercial-NoDerivs (CC BY-NC-ND) licence. This licence only allows you to download this work and share it with others as long as you credit the authors, but you can't change the article in any way or use it commercially. More information and the full terms of the licence here: https://creativecommons.org/licenses/

#### Takedown

If you consider content in White Rose Research Online to be in breach of UK law, please notify us by emailing eprints@whiterose.ac.uk including the URL of the record and the reason for the withdrawal request.



# 1 Towards a *Phaeodactylum tricornutum* biorefinery in an

# 2 outdoor UK environment

- 3 Thomas O. Butler<sup>1\*</sup>, Gloria Padmaperuma<sup>1</sup>, Alessandro M. Lizzul<sup>2</sup>,
- 4 Joe McDonald<sup>2</sup>, and Seetharaman Vaidyanathan<sup>1</sup>
- <sup>1</sup>Department of Chemical and Biological Engineering, The University of Sheffield,
- 6 Sheffield, S1 3JD, UK; S.vaidyanathan@sheffield.ac.uk (S.V.)
- <sup>2</sup> Varicon Aqua Solutions Ltd., Ball Mill Top Business Park, Unit 12, Hallow, WR2 6PD,
- 8 UK

9

21

\* Correspondence: thomas.butler@lgem.nl

## 10 Abstract

A series of commercial powdered media (Cell-Hi F2P, JWP and 11 12 WP) and a hydroponics medium (FloraMicroBloom) were investigated for 13 the cultivation of *P. tricornutum*, and compared with f/2 (a commonly employed laboratory cultivation medium; costlier to scale). Cell-Hi JWP 14 showed good performance characteristics including cost-effectiveness. 15 Outdoor cultivation of *P. tricornutum* in an airlift photobioreactor, using 16 17 Cell-Hi JWP in the United Kingdom (UK) during September and October (average daily temperature ranging between 8-18°C and natural sunlight) 18 was comparable to cultivation indoors under controlled temperature and 19 20 lighting. A strong positive correlation between fucoxanthin and chlorophyll

a content, and a weak inverse correlation between eicosapentaenoic (EPA)

content and temperature were observed. Commensal bacterial counts
revealed a sinusoidal growth profile with a change in community dominance
from *Halomonas sp.* to *Marinobacter* sp. This investigation reveals for the
first time that a multi-product approach can be adopted with *P. tricornutum*in a UK outdoor environment using commercially viable powdered media. **Keywords**: microalgae; *Phaeodactylum*, outdoor cultivation, airlift,

### 1.1 Introduction

photobioreactor, biorefinery

The five most important microalgae in terms of annual biomass production (>29 tons per annum valued at >US \$650 million) are Spirulina (*Arthrospira*), *Chlorella*, *Dunaliella*, *Haematococcus* and *Nannochloropsis* with biomass selling prices of US \$13-120 kg<sup>-1</sup> (Olaizola & Grewe, 2019). It has previously been shown that biomass productivities up to 146 tons dry cell weight (dcw) ha<sup>-1</sup> y<sup>-1</sup> in small scale cultivations and 60–75 tons dcw ha<sup>-1</sup> y<sup>-1</sup> in mass cultivations are possible (Sethi et al., 2020). It is important in the Microalgae Biotechnology sector to develop novel species/strains and production platforms.

\*\*Phaeodactylum tricornutum\* is a model diatom cultivated industrially for high value products; fucoxanthin (AlgaTechnologies, Israel) and eicosapenatenoic acid (EPA) (Simris, Sweden). \*\*P. tricornutum\* is a

potential biorefinery chassis which can be exploited for a range of natural

43 products with market potential including high value products such as fucoxanthin (US \$175 kg<sup>-1</sup> for biomass containing 1 % fucoxanthin, US 44 45 \$0.20-0.74 in capsular/softgel form) and lower value products; EPA (US 46 \$200-500 kg<sup>-1</sup>)/chrysolaminarin) for nutraceuticals and protein for animal and aquaculture feed, via sequential extraction (Butler et al., 2020; Butler, 47 48 2021). It is a commercially viable species, and is cultivated industrially by 49 at least eight companies in Europe (eicosapentaenoic acid, whole cell 50 biomass for aquafeed, and extracts for cosmetics) with an estimated annual 51 production of four tonnes of dry biomass (Araújo & García-tasende, 2021). 52 P. tricornutum dominates and often outcompetes other microalgal species in 53 mixed cultures and is able to tolerate high pH/light intensities and can also 54 grow under low light (Huete-Ortega et al., 2018; Butler et al., 2020). It is 55 robust at laboratory, pilot and demonstration scale, and can be cultivated in a range of cultivation media (Walnes, f/2 and COMBO), enriched seawater 56 and fertiliser media without the requirement for silica (Branco-Vieira et al., 57 2020; Sethi et al., 2020). 58 59 P. tricornutum can be cultivated indoors and outdoors in a range of photobioreactors (PBRs), including tubular, flat-plate, and bubble-columns, 60 61 and open (raceway) ponds with biomass and product yields described in 62 Butler et al. (2020). The biomass productivity of *P. tricornutum* has been reported to range from 0.03-1.7 g L<sup>-1</sup> d<sup>-1</sup> (Fernández et al., 1998; Veronesi et 63

al., 2015). To date the highest biomass concentration (25.4 g L<sup>-1</sup>), 64 productivity (1.7 g L<sup>-1</sup> d<sup>-1</sup>) and EPA productivity (56 mg L<sup>-1</sup> d<sup>-1</sup>) were 65 66 obtained in an outdoor split-cylinder airlift PBR (60 L) in Almeria, Spain 67 utilising mixotrophic cultivation with 0.1 M glycerol using P. tricornutum UTEX 640 (Fernández Sevilla et al., 2004). Comparatively, the highest oil 68 (TAG) yield (58.5 mg L<sup>-1</sup> d<sup>-1</sup>) in the same strain was attained in flat-panel 69 70 PBRs (Green Wall Panel III) using photoautotrophic conditions (up to 45 % TAG dry weight) (Rodolfi et al., 2017). The highest fucoxanthin 71 productivity (4.7 mg L<sup>-1</sup> d<sup>-1</sup>) was also obtained in a flat-plate system using 72 73 photoautotrophic conditions (Baoyan et al., 2017). Flat-panel 74 configurations have been shown to be optimal for biomass, EPA and 75 fucoxanthin productivities attributable to their low shear stress and effective 76 illumination (Guler et al., 2019), but are nevertheless constrained by high rates of biofouling and the resultant difficulty to clean (Lizzul, 2016). To 77 78 date the majority of studies on outdoor productivity have been performed in 79 temperate countries such as Spain and Italy, with high irradiances resulting 80 in high growth. Only limited studies are available from higher latitudes where microalgae are grown in cold climates with lower irradiances and 81 82 photoperiods, for example from Norway (Steinrücken et al., 2018). 83 Interestingly, low light appears to favour the accumulation of fucoxanthin and EPA (Gómez-Loredo et al., 2016; McClure et al., 2018), whereas higher 84

light intensities favour storage compounds (carbohydrate and TAG) with the degradation of the carbohydrate chrysolaminarin in the dark under N-limitation (Wagner et al., 2016).

PBRs result in higher productivities and more hygienic processes than raceway cultivation and can provide (to some degree) a physical barrier against contamination and grazers (Chiaramonti et al., 2013), but they are cost prohibitive for most microalgal production facilities. The cost of a hypothetical large scale microalgal production is estimated to be in the region of  $\epsilon$ 3-10 kg<sup>-1</sup> DW in PBRs (biorefinery at 100 hectare scale in the south of Spain) compared with  $\epsilon$ 0.3-1.8 kg<sup>-1</sup> in open raceway systems (Slade & Bauen, 2013; Ruiz et al., 2016). However, no such facility exists. The cost of production in aquaculture hatcheries is  $\epsilon$ 329 kg<sup>-1</sup> (25 m<sup>2</sup> scale) in a greenhouse setting and decreases to  $\epsilon$ 43 kg<sup>-1</sup> through the use of artificial illumination at 1500 m<sup>2</sup> scale (Oostlander et al., 2020) which is a more realistic cost of microalgal cultivation.

High productivities of microalgal cells require the formulation of suitable culture media, since standard media typically result in low productivities. The development of a standardised, optimal cell medium is of paramount importance because deviations can induce alterations in cell growth and product formation. The preparation of cell culture media is typically complex (requiring chemical compatibility), expensive (labour,

sterilisation, water purification, mixing, chemical storage), requires refrigeration, and is time consuming. In industrial scale operations, the large number of process steps and the numerous components required for media formulation can lead to reduced efficiency and increased costs in conjunction with the potential introduction of variability which can impact the growth of the cells; care has to be taken when adding components to enable dissolution and avoid precipitation Butler, 2021).

Dry media powder formulation is desirable to ensure a standardised product which does not vary from batch to batch and does not affect cell growth or composition. These can be cost-effective as they decrease preparation time, simplify the workflow, and reduce the complexity of the media preparation, all of which are important in a commercial setting.

Dry powdered media have traditionally been manufactured using ball-milling technology and the constituents are simultaneously crushed and mixed under controlled temperatures and humidity whilst avoiding contaminating dust (Jayme et al., 2002). The Varicon range of Cell-Hi dry powder preparations (F2P, WP, and JWP) are available as cost-effective solutions. To date Cell-Hi F2P has been used in at least 24 studies for cultivation of microalgae in the published literature with concentrations ranging from 0.1 to 0.5 g L<sup>-1</sup> (Butler, 2021). Cell-HI WP has been used in at least 8 publications with a concentration ranging from 0.1 to 0.67 L<sup>-1</sup>

(Butler, 2021). The JWP range has not been tested for microalgal cultivation in the published literature and to date no study has evaluated the performance of these powdered media formulations with standardised liquid media commonly used for microalgae in terms of growth and biochemical analysis. It has been found that media can have a dramatic effect on the growth and biochemical composition of microalgae (Butler et al., 2017; Praba et al., 2016) and this warrants investigation.

In the current study the aim was to investigate parameters important for the development of a *P. tricornutum* biorefinery. The first aim of this work was to determine the optimal cost-effective medium for obtaining high biomass and product (fucoxanthin, EPA, protein, carbohydrate and total fatty acid - TFA) productivities towards a biorefinery approach for the model strain *P. tricornutum* CCAP 1055/1. The next step was to cultivate *P. tricornutum* CCAP 1055/1 outdoors (under natural light and temperatures) in a prototype airlift photobioreactor, comparing it with cultivation indoors (under controlled lighting and temperature) to investigate the effect of fluctuations in temperature and light on biochemical composition and evaluate the potential of multiple products outdoors for potential industrial exploitation. The effect of cultivation time, light, and temperature on biochemical composition was investigated. The commensal

and outdoors. 148 1.2 Materials and methods 149 1.2.1 Phaeodactylum tricornutum culture and routine maintenance 150 P. tricornutum CCAP 1055/1 stock cultures were routinely 151 152 maintained as detailed within the literature (Butler et al., 2021) but with white lights ca. 150 µmol photons m<sup>-2</sup> s<sup>-1</sup> surface irradiance (2700 k Hansa 153 ECO Star silver lamps) with cultivation in f/2 medium (0.882 mM nitrate 154 155 and 0.036 mM phosphate). 156 1.2.2 Shake flask experimental approach for powdered media performance 157 testing 158 Powdered media formulations Cell-Hi F2P, WP and JWP were prepared from stock solutions to a final concentration of 0.1, 0.15, and 0.1 g 159 L<sup>-1</sup> as recommended by the manufacturer (Butler, 2021). A pre-optimised 160 FloraSeries Hydroponic fertiliser medium (GHE, Fleurance, France) [(2 mL 161 L<sup>-1</sup> FloraMicro (M) and 1 mL L<sup>-1</sup> FloraBloom (B)] (M2B1) was also tested 162 163 for comparison, along with f/2 medium (sterile and non-sterile) which have both been adopted for microalgae cultivation (Gómez-Loredo et al., 2016; 164 Butler et al., 2017; Song et al., 2020; Butler, 2021). Each culture was pre-165 166 acclimatised in the respective medium for one week before experimentation (preliminary experimentation). The cultures (150 mL in 250 mL flasks) 167

bacterial population was monitored and compared in the airlift PBR indoors

147

168 were incubated at 21°C (Series 4, LMS incubator, UK) and agitated at 120 rpm using a Stuart reciprocating table shaker (SSL2, UK) under continuous 169 light at  $142 \pm 33 \,\mu$ mol photons m<sup>-2</sup> s<sup>-1</sup> (2700 k Hansa ECO Star silver 170 lamps) for 7 days. Growth was monitored daily by measuring cell count and 171 biomass concentration (determined by dry weight) (Butler, 2021). The 172 173 maximum growth rate ( $\mu$ ) was calculated according to Butler et al. (2017). 174 Except for the control (f/2 medium) all media formulations were made up with tap water, under non-sterile conditions to compare the microbial 175 176 community profile. 177 1.2.3 Indoor/outdoor cultivation in a prototype airlift photobioreactor A proprietary demonstration scale 10 L airlift glass tubular 178 179 photobioreactor (ALR) PhycoLift (8 L working volume) similar to that previously described (Lizzul, 2016; Butler, 2021) was supplied by Varicon 180 Agua Solutions Ltd. and setup at The University of Sheffield for outdoor 181 cultivation in a greenhouse without temperature control and utilising only 182 natural sunlight for illumination. Details about the reactor configuration can 183 184 be found in Butler (2021). For the indoor trial the PBR was illuminated with dimmed light 185 emitting diode (LED) lamps (4000K, 10 W, BD03, RoHS) at 143 µmol 186 photons m<sup>-2</sup> s<sup>-1</sup> for the first 7 days and increased to 221 umol photons m<sup>-2</sup> s<sup>-1</sup> 187 (12 h light:dark) (representative of the outdoor PBR) until day 15. The 188

temperature was controlled at  $22 \pm 1^{\circ}$ C. The PBR was aerated at 5 L min<sup>-1</sup> (0.625 vvm) using a 20 W ACO-308 air compressor (Hailea, China) and controlled through flow gauges and connected using 8 mm polypropylene tubing. The pH was controlled on demand at pH 7.8 which ensured >95 % of the carbonic species were in the form of bicarbonate. The average DIC concentration after 1 d was 3327 and 2847  $\mu$ mol kg<sup>-1</sup> for the indoor and outdoor PBR respectively (Butler, 2021).

*P. tricornutum* cells were obtained from an inoculum preacclimatised in Cell-Hi JWP (Butler, 2021). Cell-Hi JWP (0.4 g L<sup>-1</sup>) was added at two time points: 0 and 7 d to avoid nutrient limitation. On day 15, the reactor was harvested (estimated biomass concentration of 0.1-0.2 g L<sup>-1</sup>) for the repeated batch run and supplied with fresh JWP medium.

Light impinging on the reactor surface was monitored using a digital lux meter MM-LM01 (Max Measure, UK) and logged every 5 mins (LuxMeter Communication Tool). The daily total irradiance (mol photons  $m^{-2} d^{-1}$ ) was obtained from the sum of the recorded light intensity ( $\mu$ mol photons  $m^{-2} s^{-1}$ ). PBR temperature was monitored every 30 mins using an RC-4 temperature logger (Ellitech, UK).

A sample was taken daily at the same time (11 am) for OD<sub>750</sub>, cell count, DW, dissolved inorganic nitrate (DIN) and dissolved inorganic phosphate (DIP). Samples for bacterial enumeration (1 mL) were taken

210	every other day. Samples for biochemical composition determination (5 mL
211	triplicate aliquots) were taken every 2 days for the indoor and outdoor
212	system and lyophilised. All methods were previously described in full in
213	Butler (2021).
214	1.2.4 Commensal bacterial isolation, identification, enumeration,
215	and growth experiments
216	Commensal, cultivable bacteria from the Cell-Hi media screen
217	experimental cultures, and the indoor/outdoor PBRs were isolated by
218	streaking out 100 $\mu$ L culture to form single colonies on a 'modified marine
219	agar medium' with the growth medium supplemented with 33 g L <sup>-1</sup> Instant
220	Ocean, 5 g $L^{-1}$ peptone (Sigma, UK), 1 g $L^{-1}$ yeast extract (Sigma, UK) and
221	15 g L <sup>-1</sup> agar. Isolated cultures were identified by 16S rRNA molecular
222	typing (Butler, 2021).
223	Growth $(OD_{600})$ experiments with bacterial isolates in monocultures
224	were performed in 24-well microtiter plates (Corning® Costar) with f/2

were performed in 24-well microtiter plates (Corning® Costar) with f/2
marine broth (modified marine agar without agar) (Butler, 2021). Fatty
acid methyl ester (FAME) analysis of the bacteria was conducted using a
modified version of the protocol described elsewhere (Kapoore et al., 2019).
Briefly, 5 mL of the frozen (-20°C) wet biomass culture was directly
transesterified with methanolic-HCl (7%) replacing BF3 as the acid catalyst.
In addition, a bacterial biofilm and the *P. tricornutum* culture obtained from

231	the outside PBR run 2 after 15 d were analysed to determine the FAME
232	profiles.
233	1.2.5 Analytical methods
234	Dissolved inorganic nitrogen (DIN) in the media was determined at
235	OD <sub>220</sub> nm and dissolved inorganic phosphate (DIP) in the media was
236	determined at OD <sub>885</sub> (Kapoore et al., 2019; Butler, 2021). Combined
237	extraction of chlorophyll a, carbohydrate, and protein (biochemical
238	composition) was carried out according to Chen & Vaidyanathan (2013) and
239	Butler (2021) using lyophilised biomass.
240	FAME analysis was conducted as above using direct
241	transesterification but using dry biomass (Butler, 2021). Fucoxanthin
242	content was determined using the spectrophotometric method of Wang et al.
243	(2018) ensuring the biomass was washed with MilliQ water before analysis
244	for maximum fucoxanthin recovery.
245	1.2.6 Scanning electron micrograph imaging of biofilm
246	The biofilm was spread evenly on a glass slide and allowed to dry in
247	a laminar flow. Fixed cells were examined using a JSM-6010LA
248	InTouchScope <sup>TM</sup> Multiple Touch Scanning Electron Microscope (JEOL
249	Ltd., Japan) at an accelerating voltage of 15Kv (Butler, 2021).

## 1.2.7 Statistical analysis

250

270

All statistics were conducted as detailed elsewhere (Butler et al., 251 252 2021), unless stated otherwise. Statistical analysis of the experimental data was conducted using SPSS statistical software (SPSS Statistics 28, IBM). 253 The data was tested for normality using a Shapiro-Wilk test and if these data 254 were normally distributed (P > 0.05) they were subsequently tested for equal 255 variance using Levene's test. A one-way/two-way ANOVA and a post-hoc 256 Tukey's test was utilised to understand where the differences were. If 257 258 samples were not normally distributed (P < 0.05) or equal variance was not 259 observed (P < 0.05), then a Kruskal-Wallis and post-hoc Dunn's nonparametric comparison was undertaken to understand the differences. 260 261 1.3 **Results and discussion** Evaluation of powdered Cell-Hi range culture media 262 1.3.1 A maximum cell density (1.69 x 10<sup>7</sup> cells mL<sup>-1</sup>) and biomass 263 concentration (0.45 g L<sup>-1</sup> DW) was observed with Cell-Hi JWP after 7 d 264 cultivation. The maximum specific growth rate ( $\mu = 1.27$ ) was highest in 265 266 Cell-Hi JWP medium (1.9-fold higher than f/2) but was not significantly higher with Cell Hi-JWP. Comparatively, the biomass productivity (0.08 g 267 L<sup>-1</sup> d<sup>-1</sup>) was significantly higher (Kruskal-Wallis and *post hoc* Dunn's non-268 269 parametric comparison, H=11.87, df=5, P<0.05) for Cell-Hi JWP compared

to the other media, with a 1.3-fold increase compared with f/2 (Figure 1A.

271 B). The biomass concentration attained after 7 days with f/2 medium (0.34) g L<sup>-1</sup> DW) was similar to that reported elsewhere (Penhaul Smith et al., 272 273 2020). The EPA (3.31 % DW) and fucoxanthin (1.33 % DW) contents 274 obtained with Cell-Hi JWP were significantly higher than with f/2 (2.10 and 0.74 % DW respectively) (ANOVA and post hoc Tukey's test, F=3.57, 275 P < 0.05, df= 12) (ANOVA and post hoc Tukey's test, F=22.77, P < 0.001, 276 df= 12) (Figure 1D). The protein content (26.87 % DW) was 1.71-fold 277 278 higher than f/2 medium (Figure 1E). 279 The effectiveness of the nitrate and phosphate uptake per unit 280 biomass were compared, as their content in the media differed (see supplementary material). The nitrate and phosphate uptake per unit biomass 281 (both average and maximum) for nitrate (2.16 and 2.56 mM g<sup>-1</sup> respectively) 282 and phosphate (0.49 and 0.57 mM g<sup>-1</sup> respectively) were the lowest for the 283 JWP medium (Figure 1B and C). The highest product yields and 284 productivities were also observed with Cell-Hi JWP which were 285 significantly higher than the other media (P < 0.05) (Table 1). It is possible 286 287 that the higher phosphate (0.1 mM), magnesium (138.2 mM), sulphur (138.5 mM), calcium (70.0 mM), manganese (12.6 μM), and molybdenum (2.9 288 µM) in Cell-Hi JWP contributed to its better performance (see 289 290 supplementary material). Since the interest was mainly on the production of high value products (fucoxanthin and EPA) and protein from P. 291

*tricornutum*, it was thus decided that Cell-Hi JWP was the optimal medium for scale-up.

In a commercial setting, agricultural fertilisers typically replace pure chemicals (Acién et al., 2012). When evaluating the cost of a medium two key factors need to be taken into account, the cost of the medium itself and the time taken for preparation. Varicon Aqua's Cell-Hi powders were found to be more economical than the hydroponics medium (FloraMicroBloom) and laboratory media with Cell-Hi F2P being the most economical (£2.56 per m³), followed by Cell-Hi JWP (£2.69 per m³), both > 2-fold cheaper than laboratory f/2 in terms of media cost alone (Butler, 2021). Overall, due to the medium cost and biomass concentrations attained, the most economical medium for *P. tricornutum* was Cell-Hi JWP (£6.03 per kg dry biomass) compared with £16.88 per kg dry biomass for laboratory f/2.

At industrial scale, axenic conditions are nearly impossible to attain, especially in open cultivation systems (Croft et al., 2005; Kazamia et al., 2012). Microalgae live in close association with heterotrophic bacteria which can have synergistic influences (Buhmann et al., 2016; Vuong et al., 2019). Commensal bacterial populations isolated from the culture media employed in the study were therefore characterised to observe dominant associations with *P. tricornutum*. Three bacterial species were identified with *Marinobacter* sp. and *Halomonas* sp. detected in all media but

313	Algoriphagus sp. was only detected in f/2 (both sterile and non-sterile) and
314	Cell-Hi F2P. After 7 days of cultivation in each medium, the highest
315	bacterial content was observed in P. tricornutum cultivated with M2B1
316	$(1.52 \ x \ 10^5 \ cells \ mL^{-1})$ and the lowest content was observed with Cell-Hi
317	F2P (2.67 x 10 <sup>4</sup> cells mL <sup>-1</sup> ) (see supplementary material). <i>Halomonas</i> sp.
318	was dominant (>94 %) on day 1, in all media compositions but on day 4 the
319	composition decreased to <79 % and on day 7 to <50 %, with a subsequent
320	increase in Marinobacter sp Comparatively, Algoriphagus sp. was only
321	observed in f/2 and Cell-Hi F2P throughout the cultivation period but was
322	<2 % of the bacterial composition. The bacteria detected here are similar to
323	those reported in the literature, where in addition to these species other
324	species have been reported; Muricauda sp., Devosia sp., Alcanivorax spp.,
325	Stappia sp. and Isomarina sp. (Chorazyczewski et al., 2021; Vuong et al.,
326	2019).
327	As Cell-Hi JWP is a cost-effective medium that showed higher
328	biomass productivities and yields/productivities of fucoxanthin, EPA, and
329	protein, and a relatively low bacteria content it was further investigated for
330	comparing growth and biochemical composition in an indoor and outdoor
331	prototype airlift PBR.
332	1.3.2 Outdoor cultivation in a prototype airlift PBR
333	1.3.2.1. Biomass and product yields in outdoor cultivations

334	During the one-month cultivation there was no relationship observed
335	between irradiance and temperature (Butler, 2021). This was surprising as
336	irradiance and temperature were strongly correlated in Bergen, Norway
337	(Steinrücken et al., 2018). The minimum temperature (daily average)
338	observed during run 1 in September was 8°C, the maximum was 18°C and
339	the overall cultivation period average and median were 13°C (Figure 2,
340	Table 1). There was significant variation in light and temperature during the
341	outdoor cultivation run and also within a given day (14-21°C during the day
342	and as low as 1°C to 14°C at night) (Figure 2). The greatest fluctuation in a
343	24 h period was between 10°C at night and 21°C during the day (Figure 2).
344	In contrast, the indoor temperature and light intensity were controlled (Table
345	1).
346	In the current study P. tricornutum CCAP 1055/1 always
347	predominated as the fusiform morphotype (>97 %) with the remainder being
348	a mixture of oval and triradiate (data not shown). CCAP 1055/1 has
349	previously been observed to dominate in the fusiform morphotype (De
350	Martino et al., 2007).
351	The final biomass concentration attained indoors was 1.6 g L <sup>-1</sup> DW
352	after 15 days, whilst it was lower for the outdoor cultivations (1.13 g L <sup>-1</sup> and
353	0.93 g L <sup>-1</sup> for runs 1 and 2, respectively) (Figure 3A). The lower biomass
354	concentration in the second run was likely due to lower light and colder

temperatures towards the end of the run. A similar biomass concentration

(1.3 g L<sup>-1</sup>) was achieved in indoor cultivation using a 20 L hanging bag PBR

at a similar light intensity and temperature to the current study (120 μmol

photons m<sup>-2</sup> s<sup>-1</sup> and 23°C) with continuous CO<sub>2</sub> supply at 1 % (Wang et al.,

2018).

The volumetric biomass productivity indoors (0.10 g L<sup>-1</sup> d<sup>-1</sup>) was

significantly higher than the final volumetric productivities outdoors for run 1 (0.07 g L<sup>-1</sup> d<sup>-1</sup>) and run 2 (0.05 g L<sup>-1</sup> d<sup>-1</sup>) (Table 1). However, the maximum biomass yield on light was higher for outdoor runs (Table 1). This could be attributed to the higher average light intensity and temperature indoors compared with fluctuating conditions outdoors.

Typically, higher biomass productivities have been achieved in southern latitudes, (1.4 g L<sup>-1</sup> d<sup>-1</sup> in Spain) (Acién Fernández et al., 2003) and 0.43 g L<sup>-1</sup> d<sup>-1</sup> in Italy (Rodolfi et al., 2017). However, data in Western Europe is lacking. In The Netherlands, the biomass productivity has been found to range from 0.02-0.27 g L<sup>-1</sup> d<sup>-1</sup> cultivated in outdoor flat panel PBRs in October (average of 9.58 mol photons m<sup>-2</sup> d<sup>-2</sup>, 200 μmol photons m<sup>-2</sup> d<sup>-1</sup>, temperature control at 20-22°C), with a higher biomass productivity attained at lower biomass densities (0.4 g L<sup>-1</sup> DW compared with 1.1 g L<sup>-1</sup>) (Gao et al., 2020).

375 The lower biomass productivities in our study were most likely attributable to the limited irradiance (average 82-117 µmol photons m<sup>-2</sup> s<sup>-1</sup>, 376 3-5 mol photons m<sup>-2</sup> d<sup>-1</sup>) and temperature (average 12-13 °C) as higher 377 productivities have been observed in spring and summer in The Netherlands 378 and Norway (Steinrücken et al., 2018; Gao et al., 2020). Nitrate and 379 380 phosphate were not found to be limiting throughout growth (data not shown) but light limitation and photorespiration at night could also have accounted 381 382 for the lower biomass productivity (Kroth et al., 2008). 383 EPA yield was higher in the outdoor cultivations (3.42 and 3.74 % 384 DW) for run 1 and run 2 respectively compared with indoor cultivation (2.57 % DW), and the same was true for fucoxanthin (1.18 and 1.21 % DW 385 386 indoors vs 1.15 % DW indoors) but these were not significantly different 387 (Figure 3G, Table 1). The biochemical composition was observed to be more stable in indoor cultivations than in outdoor runs (Butler, 2021). 388 There was no statistically significant difference in fatty acid composition 389 between the indoor and outdoor runs (Butler, 2021). 390 391 A weak inverse correlation between temperature and EPA was observed (Figure 4A). EPA is known to be accumulated under low 392 393 temperature and a reduction in temperature to 10°C from 25°C for 12 h has 394 been shown to result in a 120 % increase in EPA yield (Jiang & Gao, 2004). The rapid accumulation of EPA in colder conditions appears to be a 395

response to maintain membrane fluidity, allowing acclimation to low temperature stress (Jiang & Gao, 2004).

The lower temperatures observed outdoors likely resulted in an increase in EPA. Another interesting finding was that fucoxanthin and chlorophyll *a* were positively correlated (Figure 5B) and this appears to indicate that chlorophyll *a* could be a good indicator and a proxy for cellular fucoxanthin content in the airlift PBR.

## 1.3.2.2 Commensal bacterial population dynamics

During cultivation no eukaryotic contaminants, such as protozoa or rotifers, were observed outdoors or indoors. The *P. tricornutum* cultures remained unialgal. Unsurprisingly, commensal bacteria were found to be present and the genera present were in agreement with the flask experiments, *Halomonas sp.* and *Marinobacter sp.* being the predominant species (Figure 5). The bacteria numbers were higher in outdoor cultivation compared with indoors and the bacterial populations both indoors and outdoors were less numerous than *P. tricornutum* (Figure 5). Interestingly, the bacteria showed a sinusoidal profile with a population shift occurring between *Halomonas sp.* and *Marinobacter sp.*, both indoors and outdoors.

Further work is required to understand the interactions between bacteria and *P. tricornutum* through whole-transcriptome and metabolome analyses and future work should determine under which conditions bacterial

417 levels are elevated and suppressed. Further work should also be conducted 418 on determining which bacteria are beneficial for growth and product 419 formation, for example, *Stappia* sp. K01 has been revealed to increase 420 growth, chlorophyll, and fucoxanthin content in *P. tricornutum* (Vuong et 421 al., 2019). 1.3.3 Growth and characterisation of commensal bacteria identified during 422 cultivation 423 424 Only dominant and cultivable bacteria were recovered from *P*. 425 tricornutum cultures after conducting spread plates using a modified marine 426 agar medium. The bacteria were all found to grow in co-culture with P. tricornutum (without any added organic carbon source) implicating that 427 428 Halomonas, Marinobacter and Algoriphagus solely utilised diatom-derived carbon. The commensal bacteria also grew on f/2 modified marine agar and 429 in liquid f/2 marine medium when supplemented with peptone and yeast 430 extract but could not grow in f/2 medium or seawater nutrient agar alone. 431 The bacteria were osmotolerant and could be grown on freshwater and 432 433 seawater modified marine agar (Butler, 2021). As the bacterial strains developed in microalgal cultures without organic carbon supplementation, it 434 435 is suspected that they were able to grow on organic carbon released by the 436 microalgal cells, indicating interactions between the bacteria and P.

tricornutum.

437

Interestingly *Algoriphagus marincola* (red colony) was only observed in f/2 and Cell-Hi F2P in flask studies (albeit low in number) but was not detected indoors or outdoors when using JWP medium. *Halomonas* sp. was a large white colony and *Marinobacter* was a small white colony.

When the growth rates of all three bacterial species were compared, *Halomonas sp.* had the highest growth rate (lowest doubling time) (Figure 6B). The bacteria were all found to have a unique fatty acid profile which could be used as biomarkers for their presence (Figure 6D). The predominant fatty acids for *Halomonas* sp. and *Algoriphagus* sp. were C18:1 (57 and 51 % TFA respectively) which has also been found in the literature (Sánchez-Porro et al., 2010) and C16:0 was dominant in *Marinobacter* sp. In comparison, *P. tricornutum* had only <2 % C18:1. It was also confirmed that only *P. tricornutum* was capable of the synthesis of the long-chain polyunsaturated fatty acids (LC-PUFAs) EPA and DHA.

During the outdoor cultivation a bacterial biofilm was observed within areas of low flow in the PBR. This was surprising, as the total run outside was only 45 days, and this finding had not been reported in earlier pilot scale trials (Borowitzka, 1999; Steinrücken et al., 2018). The biofilm appeared to primarily be composed of *P. tricornutum* with *Halomonas sp.* and *Marinobacter sp.* also being present, which was confirmed by 16 S sequencing, SEM, and fatty acid analysis. The bacteria were observed to

adhere to *P. tricornutum* cells (Figure 6C). The planktonic *P. tricornutum* in suspension culture predominated as the fusiform morphotype but the benthic form predominated as the oval morphotype. Interestingly, both cell types were revealed to have a similar fatty acid profile, however, the fusiform morphotype appeared to have a higher EPA composition of TFAs (Figure 6B, C). This is similar to reported by Desbois et al. (2010) who found that fusiform cells had a higher EPA content than the oval morphotype cells. The transition to the oval morphotype in the benthic stage is likely because only oval morphotypes can adhere strongly to surfaces (Buhmann et al., 2016).

Further work should be conducted on determining the conditions which result in biofouling in PBRs, to prevent production downtime.

Further work should also be conducted on understanding the microalgal-bacterial relationships in PBRs to determine which bacteria are 'friend' and 'foe' and if they can be exploited for improved biomanufacturing for the implementation of a biorefinery chassis (Padmaperuma et al., 2018).

#### 1.4 Conclusion

Cell-Hi JWP was the optimal cost-effective medium for cultivating *P. tricornutum* CCAP 1055/1 for a multi-product approach. Outdoor UK cultivation was possible utilising a prototype PhycoLift PBR under natural light and temperature fluctuations comparing favourably with controlled indoor cultivation. A weak inverse correlation between temperature and

480 EPA content was observed, and a higher EPA content was observed in the outdoor cultivations. Commensal bacteria showed a sinusoidal growth 481 482 profile. Halomonas sp. was dominant at low algal densities but 483 *Marinobacter* sp. was more dominant at higher algal densities. This investigation reveals potential for developing the biorefinery concept 484 485 towards realisation in an outdoor UK setting. 487

486

488

489

490

491

492

493

494

495

496

497

498

499

E-supplementary data for this work can be found in the e-version of this paper online.

## Acknowledgements

TOB acknowledges financial assistance from UK-EPSRC (DTA 1912024). Phyconet (now Algae-UK) provided funding for the equipment and reagents involved (PHYCBIV-28). ML and JM from Varicon Aqua Solutions Ltd. provided the Phyco-Lift PBR and powdered media as in-kind contribution.

#### **Conflicts of interest**

The authors declare no conflict of interest. The founding sponsors had no role in the writing of the manuscript. ML and JM from Varicon Aqua Solutions Ltd. supplied the powders and airlift PBR.

# References

500 Acién, F. G., Fernández, J. M., Magán, J. J., & Molina, E. (2012). Production cost of a real microalgae 501 production plant and strategies to reduce it. Biotechnology Advances, 30(6), 1344–1353.

- Acién Fernández, F. G., Hall, D. O., Cañizares Guerrero, E., Krishna Rao, K., & Molina Grima, E.
   (2003). Outdoor production of *Phaeodactylum tricornutum* biomass in a helical reactor. *Journal of Biotechnology*, 103(2), 137–152.
- Araújo, R., & García-tasende, M. (2021). Current Status of the Algae Production Industry in Europe: An
   Emerging Sector of the Blue Bioeconomy. 7, 1–24.
- Baoyan, G., Ailing, C., Wenyuan, Z., Aifen, L., Chengwu, Z., Gao, B., Chen, A., Zhang, W., Li, A., &
   Zhang, C. (2017). Co-Production of Lipids, Eicosapentaenoic Acid, Fucoxanthin, and Chrysolaminarin
   by *Phaeodactylum tricornutum* Cultured in a Flat-Plate Photobioreactor Under Varying Nitrogen
   Conditions. J. Ocean Univ. China (Oceanic and Coastal Sea Research, 16(5), 916–924.
- 5. Borowitzka, M. A. (1999). Commercial production of microalgae: ponds, tanks, tubes and fermenters.
   Journal of Biotechnology, 70, 313–321.
- Branco-Vieira, M., San Martin, S., Agurto, C., Freitas, M. A. V., Martins, A. A., Mata, T. M., & Caetano,
   N. S. (2020). Biotechnological potential of Phaeodactylum tricornutum for biorefinery processes. *Fuel*,
   268(December 2019), 117357.
- Buhmann, M. T., Schulze, B., Förderer, A., Schleheck, D., & Kroth, P. G. (2016). Bacteria may induce
   the secretion of mucin-like proteins by the diatom Phaeodactylum tricornutum. *Journal of Phycology*,
   52(3), 463–474.
- 8. Butler, T., 2021. The diatom *Phaeodactylum tricornutum* as a sustainable microalgal cell factory:
  towards a biorefinery approach (Doctoral dissertation, University of Sheffield).
- Butler, T., Kapoore, R. V., & Vaidyanathan, S. (2020). *Phaeodactylum tricornutum*: A Diatom Cell
   Factory. *Trends in Biotechnology*, 1–17.
- Butler, T. O., Acurio, K., Mukherjee, J., Dangasuk, M. M., Corona, O., & Vaidyanathan, S. (2021). The
   transition away from chemical flocculants: Commercially viable harvesting of *Phaeodactylum tricornutum*. Separation and Purification Technology, 255(August 2020), 117733.
- Butler, T. O., McDougall, G. J., Campbell, R., Stanley, M. S., & Day, J. G. (2017). Media Screening for
   Obtaining *Haematococcus pluvialis* Red Motile Macrozooids Rich in Astaxanthin and Fatty Acids.
   *Biology*, 7(1), 2.
- Chen, Y., & Vaidyanathan, S. (2013). Simultaneous assay of pigments, carbohydrates, proteins and lipids
   in microalgae. *Analytica Chimica Acta*, 776, 31–40.
- 13. Chiaramonti, D., Prussi, M., Casini, D., Tredici, M. R., Rodolfi, L., Bassi, N., Zittelli, G. C., & Bondioli,
   P. (2013). Review of energy balance in raceway ponds for microalgae cultivation: Re-thinking a
   traditional system is possible. *Applied Energy*, 102, 101–111.

- 14. Chorazyczewski, A. M., Huang, I., Abdulla, H., Mayali, X., & Zimba, P. V. (2021). The influence of
   bacteria on the growth, lipid production, and extracellular metabolite accumulation by *Phaeodactylum tricornutum* (Bacillariophyceae). *Journal of Phycology*, 57(3), 931–940.
- 15. Croft, M. T., Lawrence, A. D., Raux-Deery, E., Warren, M. J., & Smith, A. G. (2005). Algae acquire
   vitamin B12 through a symbiotic relationship with bacteria. *Nature*, 438(7064), 90–93.
- De Martino, A., Meichenin, A. S., Shi, J., Pan, K., Bowler, C., Martino, A. De, Meichenin, A. S., Shi, J.,
  Pan, K., Bowler, C., De Martino, A., Meichenin, A. S., Shi, J., Pan, K., & Bowler, C. (2007). Genetic
  and phenotypic characterization of *Phaeodactylum tricornutum* (Bacillariophyceae) accessions. *Journal*of *Phycology*, 43, 992–1009.
- Desbois, A. P., Walton, M., & Smith, V. J. (2010). Differential antibacterial activities of fusiform and
   oval morphotypes of *Phaeodactylum tricornutum* (bacillariophyceae). *Journal of the Marine Biological Association of the United Kingdom*, 90(4), 769–774.
- Fernández, F. G. A., Camacho, F. G., Perez, J. A. S., Fernandez Sevilla, J. M., & Grima, E. M. (1998).
   Modeling of Biomass Productivity in Tubular Photobioreactors for Microalgal Cultures: Effects of
   Dilution Rate, Tube Diameter, and Solar Irradiance. *Biotechnology and Bioengineering*, 58, 605–616.
- Fernández Sevilla, J. M., Cerón García, M. C., Sánchez Mirón, A., Belarbi, E. H. E. H., García Camacho,
   F., & Molina Grima, E. (2004). Pilot-plant-scale outdoor mixotrophic cultures of *Phaeodactylum tricornutum* using glycerol in vertical bubble column and airlift photobioreactors: Studies in fed-batch
   mode. *Biotechnology Progress*, 20(3), 728–736.

553

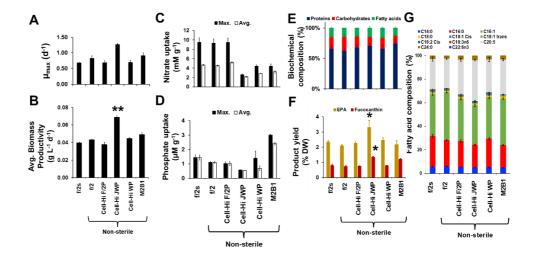
554

555

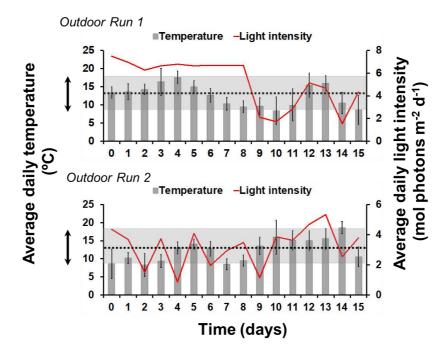
- Gao, F., Marta, S., Teles, I., Wijffels, R. H., & Barbosa, M. J. (2020). Production and monitoring of biomass and fucoxanthin with brown microalgae under outdoor conditions. *Biotechnology and Bioengineering*, November, 1–11.
- Gómez-Loredo, A., Benavides, J., & Rito-Palomares, M. (2016). Growth kinetics and fucoxanthin
   production of *Phaeodactylum tricornutum* and *Isochrysis galbana* cultures at different light and agitation
   conditions. *Journal of Applied Phycology*, 28(2), 849–860.
- Guler, B. A., Deniz, I., Demirel, Z., Oncel, S. S., & Imamoglu, E. (2019). Comparison of different
   photobioreactor configurations and empirical computational fluid dynamics simulation for fucoxanthin
   production. *Algal Research*, 37(May 2018), 195–204.
- Huete-Ortega, M., Okurowska, K., Kapoore, R. V., Johnson, M. P., Gilmour, D. J., & Vaidyanathan, S.
   (2018). Effect of ammonium and high light intensity on the accumulation of lipids in *Nannochloropsis oceanica* (CCAP 849/10) and *Phaeodactylum tricornutum* (CCAP 1055/1). *Biotechnology for Biofuels*,
   11(1), 1–15.

- 566 24. Jayme, D., Fike, R., Radominski, R., Dadey, B., Hassett, R., & Cady, D. (2002). A novel application of
- granulation technology to improve physical properties and biological performance of powdered serum-
- free culture media. In Animal Cell Technology: Basic & Applied Aspects (pp. 155-159). Springer,
- 569 Dordrecht.
- 570 25. Jiang, H., & Gao, K. (2004). Effects of lowering temperature during culture on the production of
- 571 polyunsaturdated fatty acids in the marine diatom *Phaeodactylum tricornutum* (Bacillariophyceae).
- Journal of Applied Phycology, 40, 651–654.
- 573 26. Kapoore, R. V., Huete-Ortega, M., Day, J. G., Okurowska, K., Slocombe, S. P., Stanley, M. S., &
- Vaidyanathan, S. (2019). Effects of cryopreservation on viability and functional stability of an
- 575 industrially relevant alga. *Scientific Reports*, 9(1), 1–12.
- 576 27. Kazamia, E., Czesnick, H., Nguyen, T. T. Van, Croft, M. T., Sherwood, E., Sasso, S., Hodson, S. J.,
- Warren, M. J., & Smith, A. G. (2012). Mutualistic interactions between vitamin B12-dependent algae
- and heterotrophic bacteria exhibit regulation. *Environmental Microbiology*, 14(6), 1466–1476.
- 579 28. Kroth, P. G., Chiovitti, A., Gruber, A., Martin-Jezequel, V., Mock, T., Schnitzler Parker, M., Stanley, M.
- 580 S., Kaplan, A., Caron, L., Weber, T., Maheswari, U., Virginia Armbrust, E., & Bowler, C. (2008). A
- 581 Model for Carbohydrate Metabolism in the Diatom *Phaeodactylum tricornutum* Deduced from
- Comparative Whole Genome Analysis. *PLoS ONE*, *3*(1), e1426.
- 583 29. Lizzul, A. (2016). Integrated production of algal biomass. In *Doctoral thesis, UCL (University College*
- 584 *London*). (Issue September).
- 585 30. McClure, D. D., Luiz, A., Gerber, B., Barton, G. W., & Kavanagh, J. M. (2018). An investigation into
- the effect of culture conditions on fucoxanthin production using the marine microalgae *Phaeodactylum*
- 587 tricornutum. Algal Research, 29, 41–48.
- 588 31. Olaizola, M., & Grewe, C. (2019). Commercial microalgal cultivation systems. In Grand challenges in
- 589 *algae biotechnology* (pp. 3–34).
- 590 32. Oostlander, P. C., van Houcke, J., Barbosa, M. J., & Wijffels, R. H. (2020). Microalgae production cost
- in aquaculture hatcheries. *Aquaculture*, 525(August 2019), 735310.
- 592 33. Padmaperuma, G., Kapoore, R. V., Gilmour, D. J., & Vaidyanathan, S. (2018). Microbial consortia: a
- 593 critical look at microalgae co-cultures for enhanced biomanufacturing. Critical Reviews in
- **594** *Biotechnology*, *38*(5), 690–703.
- 595 34. Penhaul Smith, J. K., Hughes, A. D., McEvoy, L., & Day, J. G. (2020). Tailoring of the biochemical
- profiles of microalgae by employing mixotrophic cultivation. Bioresource Technology Reports, 9(August
- **597** 2019), 100321.

- 598 35. Praba, T., Ajan, C., Citarasu, T., Selvaraj, T., Dhas, A. S., Gopal, P., & Babu, M. M. (2016). Growth and Oil Yield in Selected Marine. *Journal of Aquaculture in the Tropics*, 31(3/4), 165–177.
- 600 36. Rodolfi, L., Biondi, N., Guccione, A., Bassi, N. O., D'Ottavio, M., Arganaraz, G., Tredici, M. R., Ottavio,
- M. D., Arganaraz, G., & Tredici, M. R. (2017). Oil and eicosapentaenoic acid production by the diatom
- Phaeodactylum tricornutum cultivated outdoors in Green Wall Panel (GWP®) reactors. *Biotechnology*
- *and Bioengineering*, 114(10), 2204–2210.
- 604 37. Ruiz, J., Olivieri, G., De Vree, J., Bosma, R., Willems, P., Reith, J. H., Eppink, M. H. M., Kleinegris, D.
- M. M., Wijffels, R. H., & Barbosa, M. J. (2016). Towards industrial products from microalgae. *Energy*
- and Environmental Science, 9(10), 3036–3043.
- 607 38. Sánchez-Porro, C., Kaur, B., Mann, H., & Ventosa, A. (2010). Halomonas titanicae sp. nov., a halophilic
- bacterium isolated from the RMS Titanic. International Journal of Systematic and Evolutionary
- 609 *Microbiology*, 60(12), 2768–2774.
- 39. Sethi, D., Butler, T. O., Shuhaili, F., & Vaidyanathan, S. (2020). Diatoms for carbon sequestration and
- bio-based manufacturing. *Biology*, 9(8), 1–29.
- 40. Slade, R., & Bauen, A. (2013). Micro-algae cultivation for biofuels: Cost, energy balance, environmental
- impacts and future prospects. *Biomass and Bioenergy*, 53(0), 29–38.
- 41. Song, Z., Lye, G.J. and Parker, B.M., 2020. Morphological and biochemical changes in Phaeodactylum
- tricornutum triggered by culture media: Implications for industrial exploitation. Algal Research, 47,
- **616** p.101822.
- 42. Steinrücken, P., Prestegard, S. K., de Vree, J. H., Storesund, J. E., Pree, B., Mjøs, S. A., & Erga, S. R.
- 618 (2018). Comparing EPA production and fatty acid profiles of three *Phaeodactylum tricornutum* strains
- under western Norwegian climate conditions. *Algal Research*, 30, 11–22.
- 43. Veronesi, D., Idà, A., D'Imporzano, G., & Adani, F. (2015). Microalgae cultivation: Nutrient recovery
- from digestate for producing algae biomass. Chemical Engineering Transactions, 43, 1201–1206.
- 622 44. Vuong, T. T., Kwon, B. R., Eom, J. I., Shin, B. K., & Kim, S. M. (2019). Interaction between marine
- bacterium Stappia sp. K01 and diatom *Phaeodactylum tricornutum* through extracellular fatty acids.
- *Journal of Applied Phycology*, 71–82.
- 45. Wagner, H., Jakob, T., Lavaud, J., & Wilhelm, C. (2016). Photosystem II cycle activity and alternative
- 626 electron transport in the diatom *Phaeodactylum tricornutum* under dynamic light conditions and nitrogen
- 627 limitation. *Photosynthesis Research*, 128(2), 151–161.
- 46. Wang, L.-J., Fan, Y., Parsons, R., Hu, G.-R., Zhang, P.-Y., & Li, F.-L. (2018). A Rapid Method for the
- Determination of Fucoxanthin in Diatom. *Marine Drugs*, 16(2), 33.



**Fig 1.** Performance of Varicon Cell-Hi range powders compared with f/2 control (sterile), f/2 (non-sterile) and optimal FloraMicroBloom formulation (M2B1): A) maximum specific growth rate, B) average biomass productivity, C) nitrate uptake, D) phosphate uptake, E) normalised biomass biochemical composition (proteins, carbohydrates and fatty acids), F) product yield (eicosapentaenoic acid (EPA) and fucoxanthin content), and G) fatty acid composition (%). \* indicates that the component is significantly greater than f/2 medium and \*\* significantly greater than all media



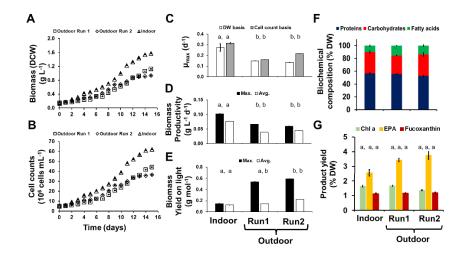
**Fig. 2.** Outdoor cultivation conditions in 8L PhycoLift PBR. Daily average temperature (°C) and light intensity (mol photons m<sup>-2</sup> d<sup>-1</sup>) profiles in the outdoor cultivation run 1 (September) and run 2 (late-September/October) (the median temperature over the period is indicated for both the runs as a black dotted line with the grey shaded area as well as the arrows on the left of the y-axis indicating the operational temperature range)

Table 1. Climatic conditions, biomass (specific growth rate and productivity) and biochemical composition of *P. tricornutum* after 15 d cultivation indoors and outdoors using a fed-batch approach

#### Indoor Outdoor run 1 Outdoor run 2 Median temperature (°C) 22 13 12 21 2 Minimum temperature (°C) 22 Maximum temperature (°C) 23 21 12:12 Photoperiod (L:D) 12:12 12.5:11.5 Mean total daily light (mol 6.22 (first 7 days), 9.61 (8-15 d) $5.19 \pm 2.07$ $3.22 \pm 1.29$ photons m<sup>-2</sup> d<sup>-1</sup>) Mean light intensity (µmol 143 (first 7 days), 221 (8-15 d) $117 \pm 45$ $82 \pm 33$ photons m<sup>-2</sup> s<sup>-1</sup>) Maximum light intensity 221 298 384 (µmol photons m<sup>-2</sup> s<sup>-1</sup>) **Biomass** Specific growth rate (d-1) Average $0.16 \pm 0.00$ $0.14 \pm 0.00$ $0.12 \pm 0.00$ Maximum Biomass concentration (g L-1 d-1) Final $1.57 \pm 0.01$ $1.13 \pm 0.01$ $0.93 \pm 0.01$ Volumetric productivity (g L<sup>-1</sup> d<sup>-1</sup>) Final $0.10 \pm 0.00$ $0.07 \pm 0.00$ $0.05 \pm 0.00$ Areal productivity (g m<sup>-2</sup> d<sup>-1</sup>) Final $4.26 \pm 0.01$ $2.90 \pm 0.01$ $2.34 \pm 0.02$ $0.54 \pm 0.00$ $0.43 \pm 0.01$ $0.82 \pm 0.03$ Yield on light (g mol<sup>-1</sup>) Final

633

634



**Fig. 3** Performance in outdoor compared to indoor cultivation in 8L PhycoLift bioreactor. Biomass concentration over the cultivation period, as DCW (A) and cell counts (B), the maximum specific growth rate (C), on DW and cell count basis, the maximum and average volumetric biomass productivity over the cultivation period (D), as well as the biomass yield on light supplied (E) are plotted alongside the normalised biomass biochemical composition (proteins, carbohydrates, fatty acids) (F) and product yield on biomass for chlorophyll a, EPA and fucoxanthin (G) for the outdoor, compared to the indoor cultivations. Note: The same letter on each bar indicates that the difference is not significant (P<0.05), and different letters indicate a significant difference (P<0.05)

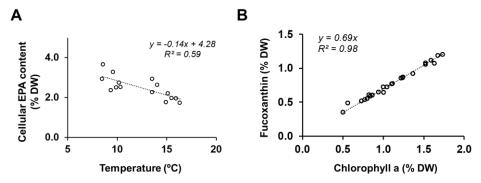
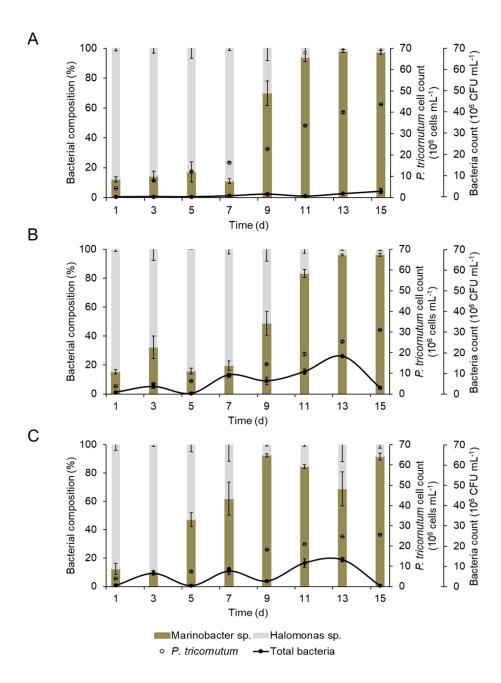
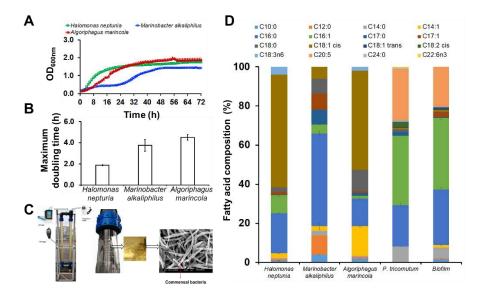


Fig. 4. Relationship between temperature and EPA content (A) in outdoor cultivations, and chlorophyll a and fucoxanthin (B), in indoor and outdoor cultivations, over the course of the one month



**Fig. 5.** *P. tricornutum* and bacteria profile variation over 15 d cultivation; a) indoor, b) outdoor run 1 and c) outdoor run 2



**Fig. 6.** Characterisation of bacteria detected in outdoor cultivation A) growth of bacteria, B) average doubling time of bacteria, C) fouling biofilm formation on the airlift photobioreactor (ALR) at low flow zones, with scanning electron micrograph (SEM) sample from biofilm with bacteria clearly observed adhering to cells, and D) fatty acid analysis of bacteria, *P. tricornutum* (after 15 d growth outdoor run 2) and biofilm obtained after 15 d growth for outdoor run 2 showcasing commensal bacteria attached to *P. tricornutum*