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Waste Management

Ecofriendly conversion of algal waste into valuable plant growth-promoting rhizobacteria (PGPR) biomass --Manuscript Draft--

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Abstract:	With the development of marine biorefinery concept, utilisation of algal waste during industrial processing as well as some "green tide" waste biomass has become an important research topic. In this work, a single-step microwave process was used to hydrolyse Laminaria japonica processing waste (LJW) and Enteromorpha prolifera (EP), producing a growth medium suitable for microbial cultivation. The medium contained a range of mono- and polysaccharides as well as macro- and micronutrients that could be used by the microbes. The cultivation behavior of three plant growth-promoting rhizobacteria (PGPR) strains (Bacillus subtilis strain Tpb55, Bacillus amyloliquefaciens strain Cas02, and Burkholderia pyrrocinia strain Lyc2) in the two media were investigated. LJW hydrolysate from 180 o C and EP hydrolysate from 150 o C performed better cultivation efficiency than those hydrolysates from other microwave conditions. Saccharide analysis showed that microbes metabolized some monosaccharide such as glucose, mannose during cultivation, leaving polysaccharide unused in the medium. Furthermore, hydrolysate-Strain cultivation mixtures were applied to pepper growth. The EP hydrolysate-Cas02 broth showed better plant growth-promoting effect compared to other treatments, which might be attributed to the higher indole-3-acetic acid (IAA) production of Cas02 in the EP hydrolysate. This work shed lights on the conversion of algal waste to PGPR biomass as well as the co-application of algal hydrolysates- strains cultivation broth for a better plant growth promotion.

We have carefully revised our manuscript following reviewer's comment and suggestion. Thank you very much for your time.

Reviewer	Reviewer Comment	Author' Response	Revised Text
Number			
	1.It is suggested to rewrite the introduction. Authors didn't cite from all	We have made some changes to the introduction.	Page 4, line 81-84
	modern references. I propose to see reference (10.1016/j.matpr.2019.08.071;	However, the references suggested by the	
	https://doi.org/10.1016/j.cis.2020.102160 ,	reviewer are about the photocatalysis of some	
	https://doi.org/10.1016/j.jcis.2020.03.105 ;	novel materials (e.g. $BiPO_4$, $Ca_3(PO)_4$), which are	
	https://doi.org/10.1016/j.jece.2019.103075 ,	not quite relevant to our research. Therefore, we	
	https://doi.org/10.1016/j.jece.2018.02.009,	think it is not suitable to cite these references.	
щ1	https://doi.org/10.1007/s11356-020-08039-1,		
#1	https://doi.org/10.1016/j.seppur.2019.116286,		
	https://doi.org/10.1016/j.molliq.2020.113832).		
	2. Manuscript contains some typographical errors. Make sure that these	Corrected	
	should be avoid during revision		
	3. Conclusions section should be improved. It looks similar to the abstract.	We have made corrections.	Page 15, line 351-
	further recommendations or indicative importance or relevance to the field		366
	should be discussed		
	1. There are many English grammar mistakes in the text. A detailed check is	Corrected	
	required in the further revision.		
	2. In the introduction section, the authors did not mention the reasons or	We have made some changes to the introduction.	Page 4, line 81-84
#2	advantages of using the microwave.		
#2	3. The reviewer suggests the authors change Fig. 1B to a table, which will make	According to Guide for Authors, articles are limited	
	it clearer to describe the elemental composition and C/N data.	to a combined total of 8 tables and figures,	
		therefore, we presented our results in the	
		combined form of Fig. 1A and 1B.	

	4. A lot of abbreviations were used in this manuscript and sometimes	We have listed abbreviations	Page 3, line 45-
	repeated. It had better list them one by one.		line 60
	5. The conclusion needs to be rewritten with more content.	We have made corrections.	Page 15, line 351-
			366
#3	Some grammar and typing errors must be revised	Corrected	

Highlights

- Up to 50% (w/w%) hydrolysate yield was obtained from waste algal biomass.
- Microwave-assisted hydrolysis process is a practical approach.
- PGPR strains were successfully cultivated in hydrolysate without extra nutrients.
- Pepper growth was significantly promoted by hydrolysate-PGPR cultivation broth.

1	Ecofriendly conversion of algal waste into valuable plant growth-
2	promoting rhizobacteria (PGPR) biomass
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23 Abstracts

With the development of marine biorefinery concept, utilisation of algal waste during 24 25 industrial processing as well as some "green tide" waste biomass has become an 26 important research topic. In this work, a single-step microwave process was used to 27 hydrolyse Laminaria japonica processing waste (LJW) and Enteromorpha prolifera (EP), 28 producing a growth medium suitable for microbial cultivation. The medium contained 29 a range of mono- and polysaccharides as well as macro- and micronutrients that could 30 be used by the microbes. The cultivation behavior of three plant growth-promoting 31 rhizobacteria (PGPR) strains (Bacillus subtilis strain Tpb55, Bacillus amyloliquefaciens 32 strain Cas02, and Burkholderia pyrrocinia strain Lyc2) in the two media were 33 investigated. LJW hydrolysate from 180°C and EP hydrolysate from 150°C performed 34 better cultivation efficiency than those hydrolysates from other microwave conditions. 35 Saccharide analysis showed that microbes metabolized some monosaccharide such as 36 glucose, mannose during cultivation, leaving polysaccharide unused in the medium. 37 Furthermore, hydrolysate-strain cultivation mixtures were applied to pepper growth. 38 The EP hydrolysate-Cas02 broth showed better plant growth-promoting effect 39 compared to other treatments, which might be attributed to the higher indole-3-40 acetic acid (IAA) production of Cas02 in the EP hydrolysate. This work shed lights on 41 the conversion of algal waste to PGPR biomass as well as the co-application of algal 42 hydrolysates- strains cultivation broth for a better plant growth promotion.

43 Keywords: Algal waste; PGPR; Microwave; Cultivation; Pepper

44

45 **Abbreviations**

- 46 PGPR -- plant growth-promoting rhizobacteria
- 47 LJW -- Laminaria japonica processing waste
- 48 EP -- Enteromorpha prolifera
- 49 IAA -- indole-3-acetic acid
- 50 LB Luria-Bertani
- 51 TFA -- trifluoroacetic acid
- 52 NTC None treatment control
- 53 Man mannose
- 54 Rha rhamnose
- 55 GlcA glucuronic acid
- 56 GalA galacturonic acid
- 57 Glc glucose
- 58 Gal galactose
- 59 Xyl xylose
- 60 Fuc fucose

61 1. Introduction

62 Macroalgae offer a credible feedstock for food consumption and production of 63 commodity and specialty chemicals. During the last few decades, the commercial market 64 of chemical products extracted from macroalgae has been increasing and accounting for 65 high value. The most well-established industries of these chemical products are alginate 66 from brown seaweed, agar and carrageenan from red seaweed, accounting for \$500 million on an annual basis(FAO, 2003). Global production of wild and cultivated 67 68 macroalgae more than doubled from 10.4 million tonnes in 2000 to 28.4 million tonnes 69 in 2014(FAO, 2016). Increased seaweed production resulted in increased seaweed waste, 70 especially from those industrial processes. For instance, carrageenan and alginate 71 production yields are generally in the range of 30-40%, leaving approximately 60-70% 72 solid waste (Kim et al., 2013; Uju et al., 2015). The seaweed residue are presumed to 73 contain high concentrations of carbohydrate, which have great potential for valorisation. 74 In addition, large scale green algal blooms occurred across the world in recent years, 75 which severely endangered the costal ecology. With the development of marine 76 biorefinery concept, efficient conversion and utilisation of these waste biomass has 77 certainly become an important research topic(Yuan et al., 2018).

78 Currently, macroalgae waste valorisation can be collaterally achieved by extraction of 79 bioactive compounds and conversion of biomass into renewable bioenergy via a variety 80 of thermochemical and biochemical processing methods (Sankaran et al., 2020; Yuan & 81 Macquarrie, 2015c). With selective and efficient heating, microwave technology has 82 been proved to be a promising approach for treatment of biomass(Zhou et al., 2018). 83 The successful demonstration of microwave reactor at both pilot and industrial scale 84 makes its real applications commercially feasible(Abeln et al., 2019). Furthermore, there 85 is a huge potential for converting the macroalgae biomass through microbial processing 86 due to its high carbohydrate, nitrogen and sulphur contents. Recent research for 87 microbial conversion of macroalgae mainly focused on biofuels such as bioethanol,

biobutanol, biodiesel, and biogas production (<u>Abeln et al., 2019</u>; <u>Tedesco & Daniels, 2018</u>;
<u>Yuan & Macquarrie, 2015a</u>).

90 Plant growth-promoting rhizobacteria (PGPR) are rhizobacteria that can benefit plants 91 by stimulating growth and suppressing disease(Kloepper et al., 1980). Increased 92 incidence of abiotic stresses, i.e., overuse of chemical fertilize, drought stress, soil 93 function degradation, impacting adversely plant growth and productivity in crops are 94 being witnessed all over the world. Numerous researches demonstrated that application 95 of PGPR based biocontrol agents, have great potential to increase plant growth and 96 control plant diseases (Islam et al., 2016; Myo et al., 2019), in particular under stressful 97 growing conditions(Lyu et al., 2019). A range of bacteria including genera of 98 Pseudomonas, Azospirillum, Azotobacter, Enterobacter, Burkholderia, Bacillus and 99 Serratia have reported as PGPR to enhance plant growth (Durairaj et al., 2018; 100 Maheshwari et al., 2015).

101 With the increasing use of PGPR in practice, preparation of bacterial strains, especially 102 the efficient and low-cost fermentation broth of biocontrol bacteria, have gradually 103 attracted people's attention(Iwanicki et al., 2020). Different types of microorganisms 104 have a certain preference for nutritional requirements. Although a medium can be 105 produced in the laboratory to satisfy the most efficient fermentation of most 106 microorganisms, small-scale shake flask fermentation cannot meet the production 107 needs(Embaby et al., 2018). Moreover, the expensive medium in the laboratory is not 108 suitable for large-scale fermentation. Generally, in microbial fermentations, 109 fermentation medium costs more than 30% of the total cost, representing a critical aspects of the total cost(Salari et al., 2019). The use of waste biomass or industrial by-110 111 products as energy sources for PGPR production is a way to reduce costs and provide an 112 ecological alternative for waste management.

We, therefore, investigated the use of algal waste hydrolysates as medium for cultivationof PGPR, coupling energy-efficient microwave hydrolysis of waste biomass offers

additional benefits for a more economic route to PGPR production(Yuan & Macquarrie,
2015a). Three strains (*Bacillus subtilis* Tpb55, *Bacillus amyloliquefaciens* Cas02, and *Burkholderia pyrrocinia* Lyc2) isolated previously were selected for their ability to
promote plant growth(Han et al., 2016; Wang et al., 2014). To the best of our knowledge,
this is the first report in which low cost culture medium from algal waste was used to
produce PGPR biomass.

121 **2. Materials and reagents**

122 2.1 Materials and reagents

The *Enteromorpha prolifera* (EP) was collected from the intertidal region from the coastal area of Qingdao (36°10'N; 120°47'E), China, during August 2019. The fresh seaweed was washed, air dried and ground to powder, and then stored at room temperature. The *Laminaria japonica* processing waste (LJW) was the residues after alginate production, and was kindly supplied by Bright Moon Seaweed Group, Qingdao, China. The waste was air dried, ground and stored at room temperature. Chemicals and reagents were purchased from Sigma-Aldrich for standards analytical grade.

130 **2.2 Microwave assisted hydrolysis of algal waste**

131 Microwave assisted hydrolysis of algal waste was carried out using a CEM Mars 6 132 microwave reactor (CEM Corporation, USA). Briefly, 2 g of dried biomass was subjected 133 to 20 mL distilled water in a 75 mL reaction tube. The sample was subsequently placed 134 in the microwave and irradiated under the dynamic mode to enable the system to 135 achieve the desired temperature (120-180 °C), and hold for 20 min. After irradiation, the 136 suspensions were centrifuged to separate the residual biomass, which was washed with 137 distilled water and dried at 105°C until constant weight. The liquid was freeze dried for 138 further use.

139 2.3 Microorganisms

Bacillus subtilis strain Tpb55 (CGMCC No.2853), Bacillus amyloliquefaciens strain Cas02
(CGMCC No.15514), Burkholderia pyrrocinia strain Lyc2 were isolated from the healthy
tobacco rhizosphere, Shandong province, China. All strains were preserved at -80 °C in
Luria-Bertani (LB) broth with 20% (v/v %) glycerol.

144 **2.4 PGPR cultivation in the algal waste hydrolysates**

145 The bacterial strains were cultured at 28°C on Luria-Bertani (LB) agar medium. To 146 prepare the seed culture of the strains, single colony of the bacteria was picked up with 147 sterilized bamboo sticks and cultured in LB broth in an orbital shaker at 28 °C and 175 148 rpm for 24 h. This pre-culture was adjusted to an optical density OD₆₀₀ of 0.3 with LB 149 medium before inoculation on algal hydrolysates. In shake flasks, 5 g/L algal hydrolysates 150 were inoculated with pre-culture at 0.1% (v/v) of total culture volume. The flasks were 151 sealed with gas-permeable film to avoid evaporation and were incubated at 28 °C and 152 175 rpm for 120 h, with readings of OD₆₀₀ performed every 24h. The OD₆₀₀ values of non-153 inoculated algal hydrolysates were subtracted from the final OD₆₀₀. The number of viable 154 cells was determined by counting colonies formed on the LB agar plates using the plate 155 dilution method every 24 h. After cultivation, the broth cultures were centrifuged at 156 7500g for 5min and pass through a sterile microfiltration membrane (0.22-μm pore size) 157 to collect supernatant for further saccharide utilization analysis.

158 **2.5 Seeding growth test**

To test the application of the PGPR cultivation mixture on the growth of pepper seedlings,
12 treatments were designed, including EP hydrolysate-PGPR cultivation mixtures (EP+T,
EP+C, EP+L), LJW hydrolysate-PGPR cultivation mixtures (LJW+T, LJW+C, LJW+L), PGPR
suspensions (T, C, L), algal hydrolysates (EP, LJW) and water control. Briefly, bacteria were
cultivated in algal hydrolysates as described above for 96 h. Bacterial cells were collected

via centrifugation at 5000 g for 5 min at room temperature, and pellet was resuspended
in cultivation supernatant (for EP hydrolysate- PGPR cultivation mixtures and LJW
hydrolysate-PGPR cultivation mixtures) or sterile water (for PGPR suspensions) to a final
OD₆₀₀ of 0.3. Algal hydrolysates treatment broths were prepared by dissolving the
hydrolysates at 5 g/L without bacterial cultivation.

For the greenhouse experiment, 180 g of the sterilized soil was placed in a 10 cm diameter plastic pot, and one pepper seedling with 4-5 leaves was transplanted from the seedling tray to the pot. Approximately 300 pots of seedlings were prepared and acclimated for one week with watering on alternate days. 18 pots were picked randomly as one treatment group. Each pot received 20 mL broth of different treatments for 3 times at 1 week intervals. After harvest, the stem height, number of leaves, maximum leaf length, maximum leaf width and dry weight of the plants were measured.

176 2.7 Analytical methods

177 Saccharide analysis was carried out using our previous method (Yuan et al., 2019). For 178 polysaccharide compositional analysis, the samples were treated with 2M trifluoroacetic 179 acid (TFA) for 2 h at 121 °C, while liquid extracts were first nitrogen-dried before being 180 treated with TFA. The resulting monosaccharides were treated with the PMP derivation 181 method and analysed by HPLC (e2695, Waters) on a Hypersil ODS-2(C18) column with 182 UV detection. For monosaccharide analysis, the sample was directly treated with the 183 PMP derivation method and detected. The monosaccharides were quantified using 184 external calibration with an equimolar mixture of nine monosaccharide standards 185 (mannose, rhamnose, glucose, galactose, xylose, arabinose, fucose, galacturonic acid 186 and glucuronic acid).

187 Elemental analysis of carbon, hydrogen, nitrogen and sulfur contents was performed 188 using a FlashSmart Elemental Analyzer (Thermal Scientific, USA). The mineral element 189 concentrations were determined using an Atomic Absorption Spectrometer 900T

190 (PerkinElmer, USA).

191 Indole acetic acid (IAA) production was evaluated as described by (Bric et al., 1991) with 192 slight modifications. Briefly, 100 mL of algal hydrolysates medium (5 g/L) containing 5 193 mM L-tryptophan was inoculated with 100 μ L bacterial suspension (OD=0.3) and 194 incubated at 28 °C for 96 h in a shaking incubator at 175 rpm. Fully grown cultures were 195 extracted by centrifugation (8000 g; 5 min), and the supernatant (2 mL) was mixed with 196 4 mL of the Salkowski reagent (1:30:50 ratio of 0.5 M FeCl₃/ 98% (w/w) H₂SO₄/ distilled 197 water). The pink color developed was measured at 530 nm. The medium without 198 inoculation of strains was used as the control.

199 **2.8 Statistical analysis**

200 Results were presented as means \pm standard deviation. Statistical analyses were 201 determined at P <0.05 by one-way ANOVA followed by a Duncan's significant test using 202 SPSS v19.0 (SPSS Inc., Chicago, USA).

203 **3. Results and discussion**

3.1 Microwave assisted hydrolysis of algal waste

205 Microwave heating is a volumetric heat source, which can rapidly heat up water to highly 206 elevated temperatures, allowing for simple and rapid hydrolysis. Depolymerization by 207 microwave heating has been employed for a variety of lignocellulosic materials (Fan et 208 al., 2013; Mihiretu et al., 2017). In this work, a single-step microwave assisted hydrolysis 209 process was applied for decomposition of algal biomass without catalytic addition. 210 Figure 1A shows the effect of temperature on the hydrolysis process. The yields of 211 hydrolysates from two waste biomass both increased with temperature, and the highest 212 yields for LJW and EP were 15.88% and 54.70% (w/w), respectively. Microwave assisted 213 hydrolysis was found to be highly suitable for Enteromorpha prolifera, and the 214 hydrolysates yield (>50%) was considerably higher than lignocellulosic biomass such as 215 bamboo(~20% w/w) under similar treatment conditions(Luo et al., 2017). The lower 216 yield of LJW was presumably due to the pre-extraction of alginate, which removes the 217 majority of soluble materials in the Laminaria japonica. Additionally, the pH value of the 218 culture medium is a crucial parameter for microbial cultivation. As the temperature 219 increased, the pH value of LJW hydrolysates remained at around 8.0. This alkaline result 220 was attributed to the dilute alkaline pre-extraction of alginate. Meanwhile, the pH value 221 of EP hydrolysates significantly decreased from 7.42 at 120 °C to 5.34 at 180 °C, 222 suggesting the secondary degradation of saccharide to organic acids under severe 223 microwave conditions(Mihiretu et al., 2017).

224 The elemental composition of waste biomass and hydrolysates was investigated and 225 shown in Figure 1B. Macro- and micronutrients were all abundant in hydrolysates from 226 both waste biomass, indicating their suitability for microbial processes. It is noted that 227 C/N ratio of the LJW waste biomass was 11.21, which was much lower than the 228 previously reported data of *Laminaria japonica* (28.6)(Xia et al., 2016). The low ratio was 229 caused by the pre-extraction of carbohydrate content-alginate. Thus, during microwave 230 treatment, limited soluble carbohydrate was hydrolyzed, resulting in even lower C/N 231 ratios of hydrolysates (around 7). The carbon-nitrogen (C/N) ratio of Enteromorpha 232 prolifera was 26.0, in the range of reported data of macroalgae (Korzen et al., 2015). 233 Hydrolysates from EP had similar ratios with original biomass, which were 23.4 to 28.1. 234 No correlation could be elucidated between the extent of decomposition and the 235 elemental composition of the hydrolysates from waste algal biomass.

3.2 Evaluation of algal waste hydrolysates as medium for PGPR cultivation

Algal waste hydrolysates were directly supplied to three strains as carbon and nutrient sources for cell cultivation. The growth of bacteria in hydrolysates was assessed by reading OD values and counting viable cells. The results showed that all three strains could grow in the hydrolysates of both algal waste without any extra nutrient added, but

241 showed different growth patterns. B. subtilis strain Tpb55 showed a higher OD value in 242 the LJW hydrolysates than in the EP hydrolysates, and the most suitable culture medium 243 was the LJW hydrolysate from microwave treatment at 180 °C, with an OD value of 0.45 244 for120 h cultivation (Figure 2A). While B. amyloliquefaciens strain Cas02 preferred EP 245 hydrolysates, especially the one from 150 °C microwave treatment, showing an OD value 246 of 0.23 for 120 h cultivation (Figure 2B). Similar to strain Tpb55, *B. pyrrocinia* strain Lyc2 247 had the highest OD value in the LJW hydrolysate from microwave 180 °C (Figure 2C). 248 Moreover, strains Tpb55 and Cas02 were not able to grow in the slightly acidic EP 249 hydrolysate from 180 °C, while strain Lyc2 still had a growth curve in that medium, 250 indicating the better acid tolerance of Lyc2. It was also observed that the cell growth of 251 all three strains was achievable in 24 h in LB medium, whereas 24-48 h was required for 252 strains to thrive in the hydrolysates medium. This phenomenon is in consistent with 253 previous studies in which bacterial strain was cultivated in acidic hydrolysates from 254 potato peel waste(Abdelraof et al., 2019). Out of expectation, the maximal OD values of 255 three strains in their favorable hydrolysates medium were all comparable with those in 256 LB medium, which could be considered attractive for future commercialization.

257 The numbers of viable cells were determined daily in these cultures. The results for 96 h 258 incubation were shown in Table S1, as the highest OD values were obtained in 96 h in 259 most cases for hydrolysates medium. The CFU ml⁻¹ values of bacteria were in good 260 agreement with the OD values. For the LJW waste hydrolysates, the CFU ml⁻¹ values were similar for strains Tpb55 and Lyc2 (more than 10⁷ CFU mL⁻¹), which were higher than that 261 262 for strain Cas02 (less than 10⁷ CFU mL⁻¹). For the EP hydrolysates, the CFU ml⁻¹ values for 263 the three strains were in the order of Tpb55>Cas02>Lyc2. Additionally, a pH increase to 264 slightly basic value was observed in all cases (Figure 3), indicating that bacteria 265 metabolized proteins and amino acids, releasing NH₄⁺ into the medium(Abeln et al., 266 <u>2019</u>).

267 The results demonstrate that microwave processing without any catalytic addition can

produce suitable medium from algal waste for PGPR cultivation. However, it should be noted that different strains favor different medium, and selection of the best algal waste/PGPR strain combination is of necessity.

271 **3.3 Carbohydrate utilization during cultivation**

272 The carbohydrate content in the substrate is considered as a key factor for suitability of microbial propagation(Xia et al., 2016). According to the growth analysis of bacterial 273 274 strains in Section 3.2, LJW waste hydrolysate from 180 °C treatment and EP hydrolysate 275 from 150 °C were chosen as the most suitable medium for three PGPR strains. Figure 4 276 shows the carbohydrate analysis of the hydrolysates. As no catalyst was added, the 277 majority of carbohydrate were present in polysaccharide form (>95%), with less than 5% 278 in monosaccharide form in both hydrolysates. In the LJW hydrolysate, polysaccharide 279 consisted of a variety of monosaccharide, with the highest content of fucose, which is 280 the typical backbone block of fucoidan (Yuan & Macquarrie, 2015b). Thus, the major polysaccharide in the LJW hydrolysate was consider to be fucoidan, a unique 281 282 polysaccharide found in brown macroalgae. In the EP hydrolysate, polysaccharide was 283 mainly composed of rhamnose, glucose and xylose, which is in agreement with the 284 polysaccharide extracted from green macroalgae Enteromorpha prolifera(Yu et al., 2017).

285 Figure 5 shows the carbohydrate content changes in the medium before and after the 286 cultivation process. All three strains consumed glucose and mannose in both 287 hydrolysates, leaving fucose in the LJW hydrolysate and rhamnose in the EP hydrolysate 288 unused, respectively (Figure 5A and 5B). This is similar to many microbial strains used for 289 biofuel fermentation such as Saccharomyces cerevisiae, and Metschnikowia pulcherrima, 290 which favor 6-carbon sugar rather than 5-carbon sugar or sugar acid (Abeln et al., 2019; 291 Yuan & Macquarrie, 2015a). Furthermore, polysaccharides in both hydrolysates 292 remained unconsumed (Figure 5C and 5D), and the unchanged molecular weight of 293 polysaccharides also suggested the same results (data not shown). Recently, macroalgae 294 polysaccharides have been found to exhibit great potential to enhance plant growth, and

show ability to activate multiple plant defense mechanisms against a broad spectrum of plant pathogens(<u>Stadnik & de Freitas, 2014</u>; <u>Zheng et al., 2020</u>). Therefore, it is likely that the co-application of PGPR and polysaccharide in the medium after cultivation will provide a stacking effect on plant growth and protection, as well as remove the cost for bacterial cell separation in the overall process.

300 **3.4 Effect of hydrolysates-PGPR cultivation mixture on pepper growth**

301 To investigate whether the hydrolysates-PGPR cultivation mixture can be jointly applied 302 for promoting plant growth, 12 treatments were conducted on pepper seedlings. 303 Agricultural parameters including stem height, leaf number, maximum leaf length, 304 maximum leaf width, and dry weight of biomass were measured (Table 1). The images 305 of plants after treatment are shown in Figure 6. As can be seen, application of three 306 strains alone all showed promotions on pepper growth, but generally without significant 307 difference compared with the H_2O control, except for the leaf number of Tpb55, and 308 biomass dry weight of Tpb55 and Lyc2 (P<0.05). When applied hydrolysates-PGPR 309 cultivation mixture, the EP hydrolysate-PGPR cultivation mixtures performed much 310 better than the LJW hydrolysate-PGPR cultivation mixture, probably because of the 311 higher polysaccharide content which could promote the growth of the pepper seedlings 312 as well(<u>El Modafar et al., 2012</u>). Although the LJW hydrolysate-PGPR cultivation mixtures 313 exhibited a positive effect on pepper growth compared with the H₂O control, there was 314 no significant difference compared with the PGPR only treatments. However, peppers 315 treated by the EP hydrolysate-PGPR cultivation mixtures not only had significantly better 316 growth than H_2O control in terms of all parameters measured (P<0.05), but also showed 317 an increased growth trend compared with PGPR only treatments. Recent study 318 demonstrated that plant polysaccharides (e.g. pectin, xylan, etc.) can serve as a carbon 319 source used to produce the extracellular matrix and can act as an environmental cue 320 that triggers biofilm formation (Beauregard et al., 2013), thereby, stimulating the 321 colonization of PGPR, which is one of key factors determining the performance of the

bacterium (Xu et al., 2017). This is probably the reason that the EP hydrolysate-PGPR
cultivation mixtures that contained a high content of polysaccharide showed better plant
growth-promoting effects.

In particular, the EP hydrolysate-CasO2 cultivation mixture showed the best plant promoting effect among all treatments, with stem height, leaf number, maximum leaf length, maximum leaf width, and dry weight being increased by 136%, 131%, 131%, 128%, and 219%, respectively, compared with the H₂O control. Nevertheless, the promotion effect of EP hydrolysate-CasO2 treatment was significantly higher (P<0.05) than that of CasO2 alone, EP hydrolysate alone, or H₂O control.

331 To explain the plant growth--promoting performance of different treatments, the 332 production of indole-3-acetic acid (IAA) of three strains in two hydrolysates media was 333 measured. PGPR play a crucial role in affecting the physiology of plants by altering their 334 hormonal balance(Ping & Boland, 2004). IAA is an important phytohormone that plays a 335 major role in cell proliferation, leading to root and stem elongation(Puri et al., 2020). It 336 can be seen in Table 2 that all three strains were able to synthesize IAA, but with different 337 production quantity in different hydrolysates media. Tpb55 could produce IAA in both 338 media, with 2.48 μ g/mL in the EP hydrolysate medium and 1.07 μ g/mL in the LJW 339 hydrolysate medium. Cas02 could only produce IAA in the EP hydrolysate medium, while 340 Lyc2 could only produce IAA in the LJW hydrolysate medium. It is also noted that strain 341 Cas02 in the EP hydrolysate medium produced significantly higher amounts of IAA 342 compared to other cultivation situations (P<0.05). Therefore, the best plant growth-343 promoting effect observed for EP hydrolysate-Cas02 treatment may have resulted from 344 both the high production of IAA from Cas02 in EP the hydrolysate medium, as well as the 345 EP polysaccharides. However, in conjunction with the phytohormone modulation, 346 mechanisms including improved nutrient acquisition(Tang et al., 2020), phytopathogen 347 suppression(Zhang et al., 2017) and protection from abiotic stress(Singh & Jha, 2017) 348 have also been proved to be working during plant growth. Further work needs to be

349 conducted to deeply reveal the plant growth-promoting effects of the three strains350 combined with algal hydrolysates.

351 4. Conclusion

352 Non-catalytic microwave assisted hydrolysis process could efficiently convert solid algal 353 waste to liquid hydrolysates, which were directly used as microbial cultivation growth 354 medium for PGPR without any extra nutrient added. Bacterial cells could be applied 355 alone or together with cultivation broth for plant growth-promoting purpose. The 356 combined use of the PGPR strains and the hydrolysates achieved an additive effect 357 compared with the PGPR strains or the algal hydrolysates alone. Notably, the 358 combination of strain Cas02 and EP hydrolysate showed the best results on both cell 359 cultivation and plant growth promotion application. The results paved a new path for 360 the efficient conversion and comprehensive utilisation of algal waste. However, the 361 mechanism of how the PGPR strains and the hydrolysates synergistically synergize is still 362 unclear, especially the synergetic effect between EP hydrolysate and strain Cas02 363 requires more in-depth research.

364 Conflicts of interest

365 There are no conflicts of interest to declare.

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- 487

488 Tables and Figures

Table 1. Growth indices of pepper with different treatment

492					
Treatment	Stem height /mm	Leaf number	Maximum leaf length/mm	Maximum leaf width/mm	Dry weight /mg
H ₂ O control	88.80±3.01 ^d	8.40±0.27 ^e	70.13±2.18 ^d	37.20±1.24 ^d	61.64±10.99 ^c
т	104.60±5.17 ^{abcd}	10.20±0.24 ^{abc}	82.53±2.67 ^{abcd}	42.93±1.15 ^{abcd}	108.04±10.81 ^{ab}
С	100.40±3.50 ^{bcd}	9.53±0.29 ^{bcd}	72.80±1.94 ^d	37.33±0.64 ^d	90.08±11.45 ^{bc}
L	96.67±4.43 ^{cd}	9.73±0.33 ^{bcd}	76.60±3.56 ^{cd}	40.73±1.58 ^{bcd}	104.36±7.89 ^{ab}
EP hydrolysates	105.60±3.21 ^{abcd}	9.20±0.20 ^{cde}	81.73±2.72 ^{bcd}	42.40±1.14 ^{bcd}	85.08±4.75 ^{bc}
EP+T	124.00±5.67ª	10.60±0.24 ^{ab}	85.67±2.65 ^{abc}	44.40±1.50 ^{abc}	111.00±9.17 ^{ab}
EP+C	121.17±5.11 ^{ab}	11.00±0.29ª	92.13±3.92ª	47.67±2.17ª	135.04±12.50 ^a
EP+L	113.33±6.84 ^{abc}	10.93±0.27ª	90.73±2.52 ^{ab}	46.27±1.19 ^{ab}	109.60±4.76 ^{abc}
LJW hydrolysates	100.33±4.06 ^{bcd}	9.00±0.17 ^{de}	70.87±2.08 ^d	37.73±0.77 ^d	71.30±10.77 ^{bc}
LJW+T	88.93±4.14 ^d	9.07±0.28 ^{cde}	70.53±3.23 ^d	38.00±1.81 ^d	79.60±11.99 ^{abc}
LJW+C	116.53±5.90 ^{abc}	10.13±0.29 ^{abcd}	79.80±2.49 ^{bcd}	41.13±1.32 ^{bcd}	118.97±8.23 ^{abc}
LJW+L	106.13±5.68 ^{abcd}	9.67±0.21 ^{bcd}	77.67±2.55 ^{cd}	39.67±0.74 ^{cd}	89.27±1.76 ^{abc}
493					

494 Different letters in the same column indicate significant difference between different groups (P<0.05).

497 498 499 500 Table 2. Indole-3-acetic acid (IAA) production of strains in different culture media 501

Culture medium	Strains	IAA production (ug/mL)
	Т	2.48±0.21 ^b
EP hydrolysate	С	3.74±0.23 ^a
	L	0.06±0.01 ^c
	т	1.07±0.42 ^c
LJW hydrolysate	С	0.01±0.01 ^c
	L	1.02±0.36 ^c

502 Different letters in the same column indicate significant difference between different groups (P<0.05).



505 Figure 1. Microwave assisted hydrolysis of algae waste biomass. (A) Yields and pH of

506 hydrolysates from different microwave conditions; (B) Elemental composition and carbo-

507 nitrogen (C/N) ratio of hydrolysates from different microwave conditions

508



511 Figure 2. Growth of PGPR strains in hydrolysates from different microwave conditions.

- 512 (A) Bacillus subtilis strain Tpb55; (B) Bacillus amyloliquefaciens strain Cas02; (C)
- 513 Burkholderia pyrrocinia strain Lyc2
- 514
- 515



518 Figure 3. pH change after 120 h cultivation of strains in different hydrolysates



521 Figure 4. Carbohydrate analysis of (A) EP hydrolysate from microwave assisted hydrolysis

522 at 150 °C; (B) LJW hydrolysate from microwave assisted hydrolysis at 180 °C



525 Figure 5. Carbohydrate consumption of PGPR during cultivation in hydrolysates from two algae waste biomass. Monosaccharide consumption of 526 three strains in (A) LJW hydrolysate from microwave assisted hydrolysis at 180 °C and (B) EP hydrolysate from microwave assisted hydrolysis at 527 150 °C; Polysaccharide consumption of three strains in (C) LJW hydrolysate from microwave assisted hydrolysis at 180 °C and (B) EP hydrolysis at 180 °C a

528 from microwave assisted hydrolysis at 150 °C



Figure 6. Effect of different treatments on pepper growth

1	Ecofriendly conversion of algal waste into valuable plant growth-
2	promoting rhizobacteria (PGPR) biomass
3 4 5 6 7	Yuan Yuan ^{a#} , Depeng Chu ^{a#} , Jiajun Fan ^b , Ping Zou ^a , Yimin Qin ^c , Yuting Geng ^a , Zhenzhen Cui ^a , Xiaohui Wang ^c , Chengsheng Zhang ^a , , Xiangdong Li ^d , James Clark ^b , Yiqiang Li ^{a*} , Xiaoqiang Wang ^a *
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23 Abstracts

24 With the development of marine biorefinery concept, utilisation of algal waste during 25 industrial processing as well as some "green tide" waste biomass has become an 26 important research topic. In this work, a single-step microwave process was used to 27 hydrolyse Laminaria japonica processing waste (LJW) and Enteromorpha prolifera (EP), 28 producing a growth medium suitable for microbial cultivation. The medium contained 29 a range of mono- and polysaccharides as well as macro- and micronutrients that could 30 be used by the microbes. The cultivation behavior of three plant growth--promoting 31 rhizobacteria (PGPR) strains (Bacillus subtilis strain Tpb55, Bacillus amyloliquefaciens 32 strain Cas02, and Burkholderia pyrrocinia strain Lyc2) in the two media were 33 investigated. LJW hydrolysate from 180°C and EP hydrolysate from 150°C performed 34 better cultivation efficiency than those hydrolysates from other microwave conditions. 35 Saccharide analysis showed that microbes metabolized some monosaccharide such as 36 glucose, mannose during cultivation, leaving polysaccharide unused in the medium. 37 Furthermore, hydrolysate-strain cultivation mixtures were applied onto pepper 38 growth. The EP hydrolysate-Cas02 broth showed better plant growth-promoting effect 39 compared to other treatments, which might be attributed to the higher indole-3-40 acetic acid (IAA) production of Cas02 in the EP hydrolysate. This work-opens a new 41 avenue of shed lights on the conversion of algal waste to PGPR biomass as well as the 42 co-application of algal hydrolysates- strains cultivation broth for a better plant growth 43 promotion.

44 Keywords: Algal waste; PGPR; Microwave; Cultivation; Pepper

46 **Abbreviations**

- 47 PGPR -- plant growth-promoting rhizobacteria
- 48 LJW -- Laminaria japonica processing waste
- 49 <u>EP -- Enteromorpha prolifera</u>
- 50 <u>IAA -- indole-3-acetic acid</u>
- 51 <u>LB Luria-Bertani</u>
- 52 <u>TFA -- trifluoroacetic acid</u>
- 53 <u>NTC None treatment control</u>
- 54 <u>Man mannose</u>
- 55 <u>Rha rhamnose</u>
- 56 <u>GlcA glucuronic acid</u>
- 57 <u>GalA galacturonic acid</u>
- 58 <u>Glc glucose</u>
- 59 <u>Gal galactose</u>
- 60 <u>Xyl xylose</u>
- 61 <u>Fuc fucose</u>

62 1. Introduction

63 Macroalgae offer a credible feedstock for food consumption and production of 64 commodity and specialty chemicals. During the last few decades, the commercial market 65 of chemical products extracted from macroalgae has been increasing and accounting for high value. The most well-established industries of these chemical products are alginate 66 67 from brown seaweed, and agar and carrageenan from red seaweed, accounting for \$500 68 million on an annual basis(FAO, 2003). Global production of wild and cultivated 69 macroalgae more than doubled from 10.4 million tonnes in 2000 to 28.4 million tonnes 70 in 2014(FAO, 2016). Increased seaweed production resulted in increased seaweed waste, 71 especially from those industrial processes. For instance, carrageenan and alginate 72 production yields are generally in the range of 30-40%, leaving approximately 60-70% 73 solid waste (Kim et al., 2013; Uju et al., 2015). The seaweed residue are presumed to 74 contain high concentrations of carbohydrate, which have great potential for valorisation. 75 In addition, large scale green algal blooms occurred across the world in recent years, 76 which severely endangered the costal ecology. With the development of marine 77 biorefinery concept, efficient conversion and utilisation of these waste biomass has 78 certainly become an important research topic(Yuan et al., 2018).

79 Currently, macroalgae waste valorisation can be collaterally achieved by extraction of 80 bioactive compounds and conversion of biomass into renewable bioenergy via a variety 81 of thermochemical and biochemical processing methods (Sankaran et al., 2020; Yuan & 82 Macquarrie, 2015c). With selective and efficient heating, microwave technology has 83 been proved to be a promising approach for treatment of biomass(Zhou et al., 2018). The successful demonstration of microwave reactor at both pilot and industrial scale 84 85 makes its real applications commercially feasible(Abeln et al., 2019). Furthermore, 86 t+here is a huge potential for converting the macroalgae biomass through microbial 87 processing due to its high carbohydrate, nitrogen and sulphur contents. Recent research 88 for microbial conversion of macroalgae mainly focused on biofuels such as bioethanol,

biobutanol, biodiesel, and biogas production (<u>Abeln et al., 2019</u>; <u>Tedesco & Daniels, 2018</u>;
<u>Yuan & Macquarrie, 2015a</u>).

91 Plant growth_-promoting rhizobacteria (PGPR) are rhizobacteria that can benefit plants 92 by stimulating growth and suppressing disease(Kloepper et al., 1980). Increased 93 incidence of abiotic stresses, i.e., overuse of chemical fertilize, drought stress, soil 94 function degradation, impacting adversely plant growth and productivity in crops are 95 being witnessed all over the world. Numerous researches demonstrated that application 96 of PGPR based biocontrol agents, have great potential to increase plant growth and 97 control plant diseases (Islam et al., 2016; Myo et al., 2019), in particular under stressful 98 growing conditions(Lyu et al., 2019). A range of bacteria including genera of 99 Pseudomonas, Azospirillum, Azotobacter, Enterobacter, Burkholderia, Bacillus and 100 Serratia have reported as PGPR to enhance plant growth (Durairaj et al., 2018; Maheshwari et al., 2015). 101

102 With the increasing use of PGPR in practice, preparation of bacterial strains, especially 103 the efficient and low-cost fermentation broth of biocontrol bacteria, have gradually 104 attracted people's attention(Iwanicki et al., 2020). Different types of microorganisms 105 have a certain preference for nutritional requirements. Although a medium can be 106 produced in the laboratory to satisfy the most efficient fermentation of most 107 microorganisms, small-scale shake flask fermentation cannot meet the production 108 needs(Embaby et al., 2018). Moreover, the expensive medium in the laboratory is not 109 suitable for large-scale fermentation. Generally, in microbial fermentations, 110 fermentation medium costs more than 30% of the total cost, representing a critical aspects of the total cost(Salari et al., 2019). The use of waste biomass or industrial by-111 112 products as energy sources for PGPR production is a way to reduce costs and provide an 113 ecological alternative for waste management.

114 We, therefore, investigated the use of algal waste hydrolysates as medium for cultivation 115 of PGPR, coupling energy-efficient microwave hydrolysis of waste biomass offers

additional benefits for a more economic route to PGPR production(Yuan & Macquarrie,
2015a). Three strains (*Bacillus subtilis* Tpb55, *Bacillus amyloliquefaciens* Cas02, and *Burkholderia pyrrocinia* Lyc2) isolated previously were selected for their ability to
promote plant growth(<u>Han et al., 2016</u>; <u>Wang et al., 2014</u>). To the best of our knowledge,
this is the first report in which low cost culture medium from algal waste <u>were was</u> used
to produce PGPR biomass.

122 **2.** Materials and reagents

123 2.1 Materials and reagents

The *Enteromorpha prolifera* (EP) was collected from the intertidal region from the coastal area of Qingdao (36°10′N; 120°47′E), China, during August 2019. The fresh seaweed was washed, air dried and ground to powder, and then stored at room temperature. The *Laminaria japonica* processing waste (LJW) was the residues after alginate production, and was kindly supplied by Bright Moon Seaweed Group, Qingdao, China. The waste was air dried, ground and stored at room temperature. Chemicals and reagents were purchased from Sigma-Aldrich for standards analytical grade.

131 **2.2 Microwave assisted hydrolysis of algal waste**

132 Microwave assisted hydrolysis of algal waste was carried out using a CEM Mars 6 133 microwave reactor (CEM Corporation, USA). Briefly, 2 g of dried biomass was subjected 134 to 20 mL distilled water in a 75 mL reaction tube. The sample was subsequently placed 135 in the microwave and irradiated under the dynamic mode to enable the system to 136 achieve the desired temperature (120-180 °C), and hold for 20 min. After irradiation, the 137 suspensions were centrifuged to separate the residual biomass, which was washed with 138 distilled water and dried at 105°C until constant weight. The liquid was freeze dried for 139 further use.

140 2.3 Microorganisms

Bacillus subtilis strain Tpb55 (CGMCC No.2853), Bacillus amyloliquefaciens strain Cas02
(CGMCC No.15514), Burkholderia pyrrocinia strain Lyc2 were isolated from the healthy
tobacco rhizosphere, Shandong province, China. All strains were preserved at -80 °C in
Luria-Bertani (LB) broth with 20% (v/v %) glycerol.

145 **2.4 PGPR cultivation in <u>the</u> algal waste hydrolysates**

146 The bacterial strains were cultured at 28°C on Luria-Bertani (LB) agar medium. To 147 prepare the seed culture of the strains, single colony of the bacteria was picked up with 148 sterilized bamboo sticks and cultured in LB broth in an orbital shaker at 28 °C and 175 149 rpm for 24 h. This pre-culture was adjusted to an optical density OD₆₀₀ of 0.3 with LB 150 medium before inoculation on algal hydrolysates. In shake flasks, 5 g/L algal hydrolysates 151 were inoculated with pre-culture at 0.1% (v/v) of total culture volume. The flasks were 152 sealed with gas-permeable film to avoid evaporation and were incubated at 28 °C and 153 175 rpm for 120 h, with readings of OD₆₀₀ performed every 24h. The OD₆₀₀ values of non-154 inoculated algal hydrolysates were subtracted from the final OD_{600} . The number of viable 155 cells was determined by counting colonies formed on the LB agar plates using the plate 156 dilution method every 24 h. After cultivation, the broth cultures were centrifuged at 157 7500g for 5min and pass through a sterile microfiltration membrane (0.22-μm pore size) 158 to collect supernatant for further saccharide utilization analysis.

159 **2.5 Seeding growth test**

In order to <u>To</u> test the application of the PGPR cultivation mixture on <u>the</u> growth of
 pepper seedlings, 12 treatments were designed, including EP hydrolysate-PGPR
 cultivation mixtures (EP+T, EP+C, EP+L), LJW hydrolysate-PGPR cultivation mixtures
 (LJW+T, LJW+C, LJW+L), PGPR suspensions (T, C, L), algal hydrolysates (EP, LJW) and water
 control. Briefly, bacterial <u>was-were</u> cultivated in algal hydrolysates as described above

for 96 h. Bacterial cells were collected via <u>certification_centrifugation</u> at 5000 g for 5 min at room temperature, and pellet was resuspended in cultivation supernatant (for EP hydrolysate- PGPR cultivation mixtures and LJW hydrolysate-PGPR cultivation mixtures) or sterile water (for PGPR suspensions) to a final OD₆₀₀ of 0.3. Algal hydrolysates treatment broths were prepared by dissolving the hydrolysates at 5 g/L without bacterial cultivation.

171 For the greenhouse experiment, 180 g of the sterilized soil was placed in a 10 cm 172 diameter plastic pot, and one pepper seedling with 4-5 leaves were was transferred 173 transplanted from the seedling tray to the pot. Around Approximately 300 pots of 174 seedlings were prepared and acclimated for one week with watering on alternate days. 175 18 pots were picked randomly as one treatment group. Each pot received 20 mL broth 176 of different treatments for 3 times at 1 week intervals. After harvest, the stem height, 177 number of leaves, maximuma leaf length, maximumal leaf width and dry weight of the 178 plants were measured.

179 2.7 Analytical methods

180 Saccharide analysis was carried out using our previous method (Yuan et al., 2019). For 181 polysaccharide compositional analysis, the samples was were treated with 2M 182 trifluoroacetic acid (TFA) for 2 h at 121 °C, while liquid extracts were first nitrogen-dried 183 before being treated with TFA. The resulting monosaccharides were treated with the 184 PMP derivation method and analysed by HPLC (e2695, Waters) on a Hypersil ODS-2(C18) 185 column with UV detection. For monosaccharide analysis, the sample was directly treated 186 with the PMP derivation method and detected. The monosaccharides were quantified 187 using external calibration with an equimolar mixture of nine monosaccharide standards 188 (mannose, rhamnose, glucose, galactose, xylose, arabinose, fucose, galacturonic acid 189 and glucuronic acid).

190 Elemental analysis of carbon, hydrogen, nitrogen and sulfur contents was performed

using a FlashSmart Elemental Analyzer (Thermal Scientific, USA). The mineral element
concentrations were determined using an Atomic Absorption Spectrometer 900T
(PerkinElmer, USA).

194 Indole acetic acid (IAA) production was evaluated as described by (Bric et al., 1991) with 195 slight modifications. Briefly, 100 mL of algal hydrolysates medium (5 g/L) containing 5 196 mM L-tryptophan was inoculated with 100 μ L bacterial suspension (OD=0.3) and incubated at 28 °C for 96 h in a shaking incubator at 175 rpm. Fully grown cultures were 197 198 extracted by centrifugation (8000 g; 5 min), and the supernatant (2 mL) was mixed with 199 4 mL of the Salkowski reagent (1:30:50 ratio of 0.5 M FeCl₃/ 98% (w/w) H₂SO₄/ distilled 200 water). The pink color developed was measured at 530 nm. The medium without 201 inoculation of strains was used as the control.

202 2.8 Statistical analysis

203 Results were presented as means \pm standard deviation. Statistical analyses were 204 determined at P <0.05 by one-way ANOVA followed by a Duncan's significant test using 205 SPSS v19.0 (SPSS Inc., Chicago, USA).

206 **3. Results and discussion**

207 **3.1 Microwave assisted hydrolysis of algal waste**

Microwave heating is a volumetrically heat source, which can rapidly heat up water to highly elevated temperatures, allowing for simple and rapid hydrolysis. Depolymerization by microwave heating has been employed for a variety of lignocellulosic materials (Fan et al., 2013; Mihiretu et al., 2017). In this work, a singlestep microwave assisted hydrolysis process was applied for decomposition of algal biomass without catalytic addition. Figure 1A shows the effect of temperature on the hydrolysis process. The yields of hydrolysates from two waste biomass both increased

215 with temperature, and the highest yields for LJW and EP were 15.88% and 54.70% (w/w), 216 respectively. Microwave assisted hydrolysis was found to be highly suitable for 217 Enteromorpha prolifera, and the hydrolysates yield (>50%) is-was_considerably higher 218 than lignocellulosic biomass such as bamboo(~20% w/w) under similar treatment 219 conditions(Luo et al., 2017). The lower yield of LJW is-was presumably due to the pre-220 extraction of alginate, which removes the majority of soluble materials in the Laminaria 221 japonica. Additionally, the pH value of the culture medium is a crucial parameter for 222 microbial cultivation. As the temperature increased, the pH value of LJW hydrolysates 223 remained at around 8.0,-. and this-This alkaline result are-was attributed to the dilute 224 alkaline pre-extraction of alginate. Meanwhile, the pH value of EP hydrolysates 225 significantly decreased from 7.42 at 120 °C to 5.34 at 180 °C, suggesting the secondary 226 degradation of saccharide to organic acids under severe microwave conditions(<u>Mihiretu</u> 227 et al., 2017).

228 The elemental composition of waste biomass and hydrolysates were was investigated 229 and shown in Figure 1B. Macro- and micronutrients were all abundant in hydrolysates 230 from both waste biomass, indicating their suitability for microbial processes. It is noted 231 that C/N ratio of the LJW waste biomass was 11.21, which was much lower than the 232 previously reported data of Laminaria japonica (28.6)(Xia et al., 2016). This The low ratio 233 was caused by the pre-extraction of carbohydrate content-alginate. Thus, during 234 microwave treatment, limited soluble carbohydrate was hydrolyzed, resulting in even 235 lower C/N ratios of hydrolysates (around 7). The carbon-nitrogen (C/N) ratio of 236 Enteromorpha prolifera was 26.0, in the range of reported data of macroalgae (Korzen 237 et al., 2015). Hydrolysates from EP had similar ratios with original biomass, which were 238 23.4 to 28.1. No correlation could be elucidated between the extent of decomposition 239 and the elemental composition of the hydrolysates from waste algal biomass.

3.2 Evaluation of algal waste hydrolysates as medium for PGPR cultivation

241 Algal waste hydrolysates were directly supplied to three strains as carbon and nutrient

242 sources for cell cultivation. The growth of bacterial in hydrolysates was assessed by 243 reading OD values and counting viable cells. The results showed that all three strains 244 could grow in the hydrolysates of both algal waste without any extra nutrient added, but 245 show<u>ed</u> different growth patterns. *B. subtilis* strain Tpb55 showed a higher OD value in 246 the LJW hydrolysates than in the EP hydrolysates, and the most suitable culture medium 247 was the LJW hydrolysate from microwave treatment at 180 °C, with the an OD value of 248 0.45 for120 h cultivation (Figure 2A). While B. amyloliquefaciens strain Cas02 preferred 249 EP hydrolysates, especially the one from 150 °C microwave treatment, showing the an 250 OD value of 0.23 for 120 h cultivation (Figure 2B). Similar with to strain Tpb55, B. 251 pyrrocinia strain Lyc2 had the highest OD value in the LJW hydrolysate from microwave 252 180 °C (Figure 2C). Moreover, strains Tpb55 and Cas02 were not be-able to grow in the 253 slightly acidic EP hydrolysate from 180 °C, while strain Lyc2 still had a growth curve in 254 that medium, indicating the better acid tolerance of Lyc2. It is was also observed that 255 the cell growth of all three strains was achievable in 24 h in LB medium, whereas 24-48 256 h was needed required for strains to get used to thrive in the hydrolysates medium. This 257 phenomenon is in accordance-consistent with previous studies in which bacterial strain 258 was cultivated in acidic hydrolysates from potato peel waste(Abdelraof et al., 2019). Out 259 of expectation, the maximal OD values of three strains in their favorable hydrolysates 260 medium were all comparable with those in LB medium, which could be considered 261 attractive for future commercialization.

262 The numbers of viable cells were determined daily in these cultures. The results for 96 h 263 incubation were shown in Table S1, as the highest OD values were obtained in 96 h in 264 most cases for hydrolysates medium. As can be seen, the The CFU ml⁻¹ values of bacterial 265 were in good agreement with the OD values. For the LJW waste hydrolysates, the CFU 266 ml⁻¹ values were similar for strains Tpb55 and Lyc2 (more than 10⁷ CFU mL⁻¹), which were 267 higher than that for strain Cas02 (less than 10⁷ CFU mL⁻¹). For the EP hydrolysates, the 268 CFU ml⁻¹ values for the three strains were in the order of Tpb55>Cas02>Lyc2. Additionally, 269 a pH increase to slightly basic value was observed in all cases (Figure 3), indicating that

bacterial metabolized proteins and amino acids, releasing NH₄⁺ into the medium(<u>Abeln</u>
<u>et al., 2019</u>).

The results demonstrate that microwave processing without any catalytic addition can produc<u>eing</u> suitable medium from algal waste for PGPR cultivation. However, it should be noted that different strains favor different medium, and selection of <u>the</u> best algal waste/PGPR strain combination is of necessity.

276

277 3.3 Carbohydrate utilization during cultivation

278 The carbohydrate content in the substrate is considered as a key factor for suitability of microbial propagation(Xia et al., 2016). According to the growth analysis of bacterial 279 280 strains in section-Section 3.2, LJW waste hydrolysate from 180 °C treatment and EP 281 hydrolysate from 150 °C were chosen as the most suitable medium for three PGPR strains. 282 Figure 4 shows the carbohydrate analysis of the above hydrolysates. As no catalyst was 283 added, the majority of carbohydrate were present in polysaccharide form (>95%), with 284 less than 5% in monosaccharide form in both hydrolysates. In the LJW hydrolysate, 285 polysaccharide consisted of a variety of monosaccharide, with the highest content of 286 fucose, which is the typical backbone block of fucoidan (Yuan & Macquarrie, 2015b). 287 Thus, the major polysaccharide in the LJW hydrolysate was consider to be fucoidan, a 288 unique polysaccharide from found in brown macroalgae. In the EP hydrolysate, 289 polysaccharide was mainly composted composed of rhamnose, glucose and xylose, 290 which is in agreement with the polysaccharide extracted from green macroalgae 291 Enteromorpha prolifera(Yu et al., 2017).

Figure 5 shows the carbohydrate <u>content</u> changes in the medium before and after the cultivation process. All three strains consumed glucose and mannose in both hydrolysates, leaving fucose in <u>the</u> LJW hydrolysate and rhamnose in <u>the</u> EP hydrolysate unused, respectively (Figure 5A and 5B). This is similar <u>with-to</u> many microbial strains

296 used for biofuel fermentation such as Saccharomyces cerevisiae, and Metschnikowia 297 pulcherrima, which favor 6-carbon sugar rather than 5-carbon sugar or sugar acid (Abeln 298 et al., 2019; Yuan & Macquarrie, 2015a). Furthermore, polysaccharides in both 299 hydrolysates remained unconsumed (Figure 5C and 5D), and the unchanged molecular 300 weight of polysaccharides also suggested the same results (data not shown). Recently, 301 macroalgae polysaccharides have been found to exhibit great potential to enhance plant 302 growth, and show ability to activate multiple plant defense mechanisms against a broad 303 spectrum of plant pathogens(Stadnik & de Freitas, 2014; Zheng et al., 2020). Therefore, 304 it is likely that the co-application of PGPR and polysaccharide in the medium after 305 cultivation will provide a stacking effect on plant growth and protection, as well as 306 remove the cost for bacterial cell separation in the overall process.

307 **3.4 Effect of hydrolysates-PGPR cultivation mixture on pepper growth**

308 To investigate whether the hydrolysates-PGPR cultivation mixture can be jointly applied 309 for promoting plant growth, 12 treatments were conducted on pepper seedlings. 810 Agricultural parameters including stem height, leaf number, maximal-maximum leaf 311 length, maximumal leaf width, and dry weight of biomass were measured (Table 1). The 312 images of plants after treatment were are shown in Figure 6. As can be seen, application 313 of three strains alone all showed promotions on pepper growth, but generally without B14 significant difference compared with the H_2O control, except for the leaf number of 315 Tpb55, and biomass dry weight of Tpb55 and Lyc2 (P<0.05). When applied hydrolysates-316 PGPR cultivation mixture, <u>the</u> EP hydrolysate-PGPR cultivation mixtures performed much 317 better than the LJW hydrolysate-PGPR cultivation mixture, probably because of the 318 higher polysaccharide content which could promote the growth of the pepper seedlings 319 as well(El Modafar et al., 2012). Although the LJW hydrolysate-PGPR cultivation mixtures 320 exhibited a positive effect on pepper growth compared with the H2O control, there is 321 was no significant difference compared with the PGPR only treatments. However, 322 peppers treated by the EP hydrolysate-PGPR cultivation mixtures not only had

323 significantly better growth than H₂O control in terms of all parameters measured B24 (P<0.05), but also showed an obviously-increased growth trend compared with PGPR 325 only treatments. Recently study demonstrated that plant polysaccharides (e.g. pectin, 326 xylan, etc.) can serve as a carbon source used to produce the extracellular matrix and 327 can act as an environmental cue that triggers biofilm formation (Beauregard et al., 2013), 328 therefore thereby, stimulating the colonization of PGPR, which is one of key factors 329 determining the performance of the bacterium (Xu et al., 2017). This is probably the 330 <u>reason that the</u> why EP hydrolysate-PGPR cultivation mixtures that contained <u>a high</u> 831 content of polysaccharide showed better plant growth--promotingon effects.

In particular, <u>the</u> EP hydrolysate-CasO2 cultivation mixture showed the best plant promoting effect among all treatments, <u>of which thewith</u> stem height, leaf number, <u>maximal-maximum</u> leaf length, <u>maximal-maximum</u> leaf width, and dry weight <u>being</u> increased by 136%, 131%, 131%, 128%, <u>and</u> 219%, respectively, compared with <u>the</u> H₂O control. Nevertheless, the promotion effect of EP hydrolysate-CasO2 treatment was significantly higher (P<0.05) than <u>that of</u> CasO2 alone, EP hydrolysate alone, <u>and-or</u> H₂O control.

339 To explain the plant growth--promotion-promoting performance of different treatments, 340 the production of indole-3-acetic acid (IAA) of three strains in two hydrolysates media 341 was measured. PGPR play a crucial role in affecting the physiology of a plants by altering 342 their hormonal balance(Ping & Boland, 2004). IAA is an important phytohormone that 343 has plays a major role in cell proliferation, leading to toot root and stem elongation (Puri 344 et al., 2020). It can be seen in Table 2 that all three strains were able to synthesize IAA, 345 but with different production quantity in different hydrolysates mediummedia. Tpb55 346 could produce IAA in both media, with 2.48 µg/mL in the EP hydrolysate medium and 347 1.07 µg/mL in the LJW hydrolysate medium. Cas02 could only produce IAA in the EP 348 hydrolysate medium, while Lyc2 could only produce IAA in <u>the</u> LJW hydrolysate medium. 349 It is also noted that strain Cas02 in the EP hydrolysate medium produced significantly

350 higher amounts of IAA compared to other cultivation situations (P<0.05). Therefore, the B51 best plant growth--promoting effect observed for EP hydrolysate-Cas02 treatment may 352 have resulted from both the high production of IAA from Cas02 in EP the hydrolysate 353 medium, as well as the EP polysaccharides. However, despite of in conjunction with the 354 phytohormone modulation, mechanisms including improved nutrient acquisition(Tang 355 et al., 2020), phytopathogen suppression(Zhang et al., 2017) and protection from abiotic 356 stress(<u>Singh & Jha, 2017</u>) have also been proved to be working during the plant growth. 357 Further work needs to be done-conducted to deeply reveal the plant growth--promoting 358 effects of the three strains combined with algal hydrolysates.

359 4. Conclusion

360 Non-catalytic Microwave microwave assisted hydrolysis process could efficiently convert B61 solid algal waste to liquid hydrolysates, which were directly used as microbial cultivation 362 growth medium for PGPR cultivation without any extra nutrient added. Bacterial cells 363 can-could be applied alone or together with cultivation broth for plant growth-promoting 364 purpose. The combined use of the PGPR strains and the hydrolysates achieved an 365 additive effect compared with the PGPR strains or the algal hydrolysates alone. Notably, 366 the combination of strain CasO2 and EP hydrolysate showed the best results on both cell 367 cultivation and plant growth promotion application. The results paved a new path for 368 the efficient conversion and comprehensive utilisation of algal waste. Notably, the 369 combination of strain Cas02 and EP hydrolysate showed the best results on both cell 370 cultivation and plant growth promotion application, compared with other strain-371 hydrolysate combinations. However, the mechanism of how the PGPR strains and the 372 hydrolysates synergistically synergize is still unclear, especially the synergetic effect 373 between EP hydrolysate and strain Cas02 requires more in-depth research.Further 374 studies are required to better understand the specific mechanism involved in synergetic 375 effect between EP hydrolysate and strain Cas02.

376 Conflicts of interest

377 There are no conflicts of interest to declare.

378 Acknowledgement

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500 Tables and Figures

Table 1. Growth indices of pepper with different treatment

Treatment	Stem height /mm Leaf number		Maxim <u>um</u> al leaf length/mm	Maxim <u>um</u> al leaf width/mm	Dry weight /mg	
H₂O control	88.80±3.01 ^d	8.40±0.27 ^e	70.13±2.18 ^d	37.20±1.24 ^d	61.64±10.99 ^c	
т	104.60±5.17 ^{abcd}	10.20±0.24 ^{abc}	82.53±2.67 ^{abcd}	42.93±1.15 ^{abcd}	108.04±10.81 ^{ab}	
С	100.40±3.50 ^{bcd}	9.53±0.29 ^{bcd}	72.80±1.94 ^d	37.33±0.64 ^d	90.08±11.45 ^{bc}	
L	96.67±4.43 ^{cd}	9.73±0.33 ^{bcd}	76.60±3.56 ^{cd}	40.73±1.58 ^{bcd}	104.36±7.89 ^{ab}	
EP hydrolysates	105.60±3.21 ^{abcd}	9.20±0.20 ^{cde}	81.73±2.72 ^{bcd}	42.40±1.14 ^{bcd}	85.08±4.75 ^{bc}	
EP+T	124.00±5.67ª	10.60±0.24 ^{ab}	85.67±2.65 ^{abc}	44.40±1.50 ^{abc}	111.00±9.17 ^{ab}	
EP+C	121.17±5.11 ^{ab}	11.00±0.29ª	92.13±3.92ª	47.67±2.17ª	135.04±12.50ª	
EP+L	113.33±6.84 ^{abc}	10.93±0.27ª	90.73±2.52 ^{ab}	46.27±1.19 ^{ab}	109.60±4.76 ^{abc}	
LJW hydrolysates	100.33±4.06 ^{bcd}	9.00±0.17 ^{de}	70.87±2.08 ^d	37.73±0.77 ^d	71.30±10.77 ^{bc}	
LJW+T	88.93±4.14 ^d	9.07±0.28 ^{cde}	70.53±3.23 ^d	38.00±1.81 ^d	79.60±11.99 ^{abc}	
LJW+C	116.53±5.90 ^{abc}	10.13±0.29 ^{abcd}	79.80±2.49 ^{bcd}	41.13±1.32 ^{bcd}	118.97±8.23 ^{abc}	
LJW+L	106.13±5.68 ^{abcd}	9.67±0.21 ^{bcd}	77.67±2.55 ^{cd}	39.67±0.74 ^{cd}	89.27±1.76 ^{abc}	
505						

506 Different letters in the same column indicate significant difference between different groups (P<0.05).

509 510 511 512 Table 2. Indole-3-acetic acid (IAA) production of strains in different culture media 513

Culture medium	Strains	IAA production (ug/mL)
	т	2.48±0.21 ^b
EP hydrolysate	С	3.74±0.23ª
	L	0.06±0.01 ^c
	т	1.07±0.42 ^c
LJW hydrolysate	С	0.01±0.01 ^c
	L	1.02±0.36 ^c

514 Different letters in the same column indicate significant difference between different groups (P<0.05).



517 Figure 1. Microwave assisted hydrolysis of algae waste biomass. (A) Yields and pH of

- 518 hydrolysates from different microwave conditions; (B) Elemental composition and carbo-
- 519 nitrogen (C/N) ratio of hydrolysates from different microwave conditions
- 520
- 521



523 Figure 2. Growth of PGPR strains in hydrolysates from different microwave conditions.

- 524 (A) Bacillus subtilis strain Tpb55; (B) Bacillus amyloliquefaciens strain Cas02; (C)
 525 Burkholderia pyrrocinia strain Lyc2



529530 Figure 3. pH change after 120 h cultivation of strains in different hydrolysates



533 Figure 4. Carbohydrate analysis of (A) EP hydrolysate from microwave assisted hydrolysis

at 150 °C; (B) LJW hydrolysate from microwave assisted hydrolysis at 180 °C



537 Figure 5. Carbohydrate consumption of PGPR during cultivation in hydrolysates from two algae waste biomass. Monosaccharide consumption of 538 three strains in (A) LJW hydrolysate from microwave assisted hydrolysis at 180 °C and (B) EP hydrolysate from microwave assisted hydrolysis at

539 150 °C; Polysaccharide consumption of three strains in (C) LJW hydrolysate from microwave assisted hydrolysis at 180 °C and (B) EP hydrolysate

540 from microwave assisted hydrolysis at 150 °C



Figure 6. Effect of different treatments on pepper growth



Treatment		Incubate time (96h)						
		LJW 120°C	LJW 150°C	LJW 180°C	EP 120°C	EP 150°C	EP 180°C	LB
	Tbp55	7.74	7.71	7.87	7.13	7.40	0	7.27
Log CFU/ml	Cas02	6.30	6.48	6.51	6.70	6.85	0	6.87
	Lyc2	7.30	7.70	7.88	6.20	6.06	6.22	7.88

TableS1. Evaluation of cultivation efficiency of strains under different culturemedium

Count of viable cells in each treatment at 96h incubation. The strains Tbp55, Cas02 and Lyc2 were incubated in LJW and EP hydrolysate medium, LB was used as control. Pipette each medium separately for gradient dilution, the culture medium with different dilutions were spread on LB solid medium for colony counting. The number of viable cells per ml of culture medium in different treatments is converted into log form for display. Each treatment was repeated 5 times, and the data display in the table is the average of 5 repeats

Declaration of interests

 \boxtimes The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

□The authors declare the following financial interests/personal relationships which may be considered as potential competing interests: