



This is a repository copy of *Thermal treatment of Cs-exchanged chabazite by hot isostatic pressing to support decommissioning of Fukushima Daiichi nuclear power plant.*

White Rose Research Online URL for this paper:
<https://eprints.whiterose.ac.uk/171073/>

Version: Accepted Version

Article:

Gardner, L.J. orcid.org/0000-0003-3126-2583, Walling, S.A., Corkhill, C.L. et al. (1 more author) (2021) Thermal treatment of Cs-exchanged chabazite by hot isostatic pressing to support decommissioning of Fukushima Daiichi nuclear power plant. *Journal of Hazardous Materials*, 413. 125250. ISSN 0304-3894

<https://doi.org/10.1016/j.jhazmat.2021.125250>

Article available under the terms of the CC-BY-NC-ND licence
(<https://creativecommons.org/licenses/by-nc-nd/4.0/>).

Reuse

This article is distributed under the terms of the Creative Commons Attribution-NonCommercial-NoDerivs (CC BY-NC-ND) licence. This licence only allows you to download this work and share it with others as long as you credit the authors, but you can't change the article in any way or use it commercially. More information and the full terms of the licence here: <https://creativecommons.org/licenses/>

Takedown

If you consider content in White Rose Research Online to be in breach of UK law, please notify us by emailing eprints@whiterose.ac.uk including the URL of the record and the reason for the withdrawal request.



eprints@whiterose.ac.uk
<https://eprints.whiterose.ac.uk/>

1 **Thermal treatment of Cs-exchanged chabazite by hot isostatic pressing to support**
2 **decommissioning of Fukushima Daiichi Nuclear Power Plant**

3

4 Laura J. Gardner¹, Sam A. Walling¹, Claire L. Corkhill¹ and Neil C. Hyatt^{1*}

5

6 ¹*NucleUS Immobilisation Science Laboratory, Department of Materials Science and Engineering,*

7 *University of Sheffield, Sir Robert Hadfield Building, Sheffield, S1 3JD, UK*

8

9

10 **To whom correspondence should be addressed. Email: n.c.hyatt@sheffield.ac.uk*

11

12 **ABSTRACT**

13 Ion exchange materials are used widely for the removal of radionuclides from contaminated water at
14 nuclear licensed sites, during normal operating procedures, decommissioning and in accident clean-up,
15 such as the ongoing recovery operation at the Fukushima Daiichi nuclear power plant. Framework silicate
16 inorganic ion exchange materials, such as chabazite $((\text{Na}_{0.14}\text{K}_{1.03}\text{Ca}_{1.00}\text{Mg}_{0.17})[\text{Al}_{3.36}\text{Si}_{8.53}\text{O}_{24}]\cdot 9.7\text{H}_2\text{O})$, have
17 shown particular selectivity towards ^{137}Cs uptake, but their safe storage poses a number challenges
18 requiring conditioning into passively safe waste packages of minimal volume. We demonstrate the
19 transformation of Cs-exchanged chabazite into a glass-ceramic wastefrom by hot isostatic pressing to
20 produce a durable consolidated monolith. The application of heat and pressure resulted in the collapse of
21 the chabazite framework, forming crystalline Cs-substituted leucite $(\text{Cs}_{0.15(3)}\text{K}_{0.57(4)}\text{Al}_{0.90(4)}\text{Si}_{2.24(5)}\text{O}_6)$
22 incorporated within a $\text{K}_2\text{O}-\text{CaO}-\text{MgO}-\text{Al}_2\text{O}_3-\text{SiO}_2$ glass. The Cs partitioned preferentially into the Cs/K-
23 feldspar which incorporated ~77% of the Cs_2O inventory. Analysis of the chemical durability of the glass-
24 ceramic wastefrom revealed that the Cs release rates were comparable or lower than those reported for
25 vitrified high level and intermediate level wastes. Overall, hot isostatic pressing was demonstrated to be
26 an effective processing technology for conditioning spent inorganic ion exchange materials by yielding
27 durable and passively safe wastefroms.

28 **Key Words:** Hot isostatic pressing, ion exchange materials, nuclear waste management, characterisation,
29 chemical durability

30

31 1. Introduction

32 On March 11th, 2011, the Great East Japan earthquake (9.0 magnitude) occurred, which resulted in the
33 automatic shutdown of the operating reactors (Units 1-3) at the Fukushima Daiichi nuclear power plant
34 (NPP) [1, 2]. In the series of events that followed, the nuclear fuel melted with the cladding and there
35 were a series of hydrogen explosions in Units 1, 3 and 4 [1]. To cool the damaged reactor cores and remove
36 residual decay heat, sea water was injected into the reactor buildings and turbine halls using fire trucks
37 for approximately two weeks, after which fresh water circulation was reinstated with restored access to
38 the power supply [3]. The emergency and post-accident reactor cooling resulted in the generation of large
39 volumes of highly radioactive water (due to contact with molten/damaged fuel) of which ^{137}Cs is the
40 largest component of the total activity [3]. ^{137}Cs is a short-lived radionuclide ($t_{1/2} = 30.2$ years) that poses
41 a radiological risk to humans and the environment, due to high energy beta and gamma emissions (^{137}Cs
42 beta decay to $^{137\text{m}}\text{Ba}$ (0.512 MeV) followed by gamma decay to ^{137}Ba (0.662 MeV)) [4], the ease of exchange
43 for K and Na salts in biological organisms, and its high solubility in water.

44 To facilitate ^{137}Cs removal from the contaminated coolant water, two water treatment facilities were
45 installed on the Fukushima Daiichi NPP site, Kurion and SARRY, which used the framework silicate
46 inorganic ion exchange materials herschelite [5] and IONSIV (Honeywell UOP [6]). These facilities have
47 since treated contaminated water volumes of 394,720 m³ and 1,827,290 m³, respectively [7] (values
48 correct as of April 2020). Similar framework silicate ion exchange materials are used in the routine
49 treatment of radionuclide contaminated water at nuclear licensed sites, for example, the SIXEP plant at
50 Sellafield (UK).

51 After selective uptake of radionuclides, the storage of spent ion exchange materials poses several
52 challenges. This is particularly the case at Fukushima Daiichi NPP where on-site storage space is extremely
53 limited, and there are strong incentives for the rapid decommissioning of the site. Spent ion exchange
54 materials pose a particular challenge, due to: potential dispersal in the event of a loss of containment, as
55 a result of their granular nature; very high dose rates and radiogenic heating, as a result of their selectivity
56 for short-lived radionuclides (e.g. ^{90}Sr , ^{137}Cs); and production of hydrogen from the radiolysis of entrained
57 water, which poses a potential explosion risk [8]. Since spent ion exchange materials are generated not
58 only at Fukushima, but also at other nuclear licenced sites as described above, there is a clear need to
59 develop suitable conditioning routes to minimise the risk associated with these highly radioactive and

60 dispersible materials, whilst producing passively safe waste packages of minimal volume, to reduce
61 storage and disposal costs.

62 One potential conditioning route for spent ion exchange materials is to apply hot isostatic pressing
63 (HIPing), which uses the concurrent application of temperature (up to 2200 °C) and pressure (typically
64 100-200 MPa) to a work-piece (HIP canister) within a pressure vessel. The changes imposed to the work-
65 piece include the conversion into a passively safe solid monolith product, with exclusion of porosity and
66 voidage (with respect to powder and granular materials) [9]. For these reasons, HIPing is currently under
67 consideration as a thermal treatment process for conditioning radioactive wastes ranging from sludges
68 [10, 11] and high level wastes [12, 13] to portions of the UK Pu stockpile [14-17]. Typically, the resulting
69 HIPed wastefrom will be a ceramic or glass-ceramic matrix, where the waste is an integral component of
70 the host matrix [18, 19]. HIPing radioactive waste provides several advantages: the batch to batch
71 processing provides inventory and criticality control, where desirable; it is possible to achieve high waste
72 loadings by conversion of adequately dried waste directly to a monolith of acceptable phase assemblage;
73 there is no requirement for a fluid melt, as in the application of conventional vitrification; and there is
74 minimal off-gas and secondary waste generated, due to the hermetically sealed nature of the HIP can.
75 There is potential for waste volume reduction between 20-70%, which could provide significant storage
76 and disposal cost savings [18, 19]. In principle, a single HIP unit could also process multiple waste feeds,
77 due to the batch wise and contained nature of the process and the wide range of accessible process
78 conditions [19].

79 At present, there are no full-scale HIP plants operational for nuclear waste treatment, however the
80 Australian Nuclear Science and Technology Organisation (ANSTO) are commissioning a HIP plant (Synroc
81 Waste Treatment Plant; SWTF) that is expected to be completed in 2020, with an estimated annual
82 capacity to process ~5000 L of wastes generated from medical isotope production [20]. The UK Nuclear
83 Decommissioning Authority (NDA) have proposed HIPing as a credible option for processing a portion of
84 the civil PuO₂ stockpile [21] (and plutonium-residues) with several research programmes underway. In the
85 USA, the Department of Energy (DoE) have considered HIPing for conditioning calcined high level wastes
86 generated at the Idaho Nuclear Technology and Engineering Center (INTEC) from spent fuel reprocessing
87 operations. HIPing INTEC calcined wastes is reported to be capable of saving an estimated \$2 billion in
88 disposal costs, which is equivalent to a 50% reduction when compared with the baseline immobilisation

89 option of a borosilicate glass matrix (based on analysis reported in 2004) [12]. As such, there is a clear
90 mandate and need to continue underpinning HIP wastefrom characterisation and performance for a wide
91 variety of nuclear wastes (including spent ion exchange materials investigated here) to enable/assist
92 waste management decisions by appropriate governmental bodies and waste owners.

93 In this study, the application of HIPing as a consolidation technique for the conversion of Cs-exchanged
94 inorganic ion exchange material was demonstrated based on small-scale (~35 g) wastefroms, which
95 resulted in a multiphase glass-ceramic at 70 wt. % waste loading. Cs-exchanged chabazite
96 $((\text{Na}_{0.14}\text{K}_{1.03}\text{Ca}_{1.00}\text{Mg}_{0.17})[\text{Al}_{3.36}\text{Si}_{8.53}\text{O}_{24}]\cdot 9.7\text{H}_2\text{O})$, which is reasonably similar in composition to herschelite
97 $(\text{Na}_2,\text{K}_2,\text{Ca},\text{Sr},\text{Mg}_2)[\text{Al}_2\text{Si}_4\text{O}_{12}]_2\cdot 12\text{H}_2\text{O}$ deployed by Kurion (now part of Veolia Nuclear Solutions) at
98 Fukushima Daiichi NPP [3]) was employed to simulate this waste. The HIP parameters were optimised by
99 the variation of pressure (50-100 MPa) and temperature (1050-1250 °C) at a fixed duration (4 h) and the
100 resulting small-scale wastefrom was characterised by XRD, XRF and SEM/EDX techniques and, to assess
101 its passive safety, a durability assessment was performed.

102

103 2. Experimental Methodology

104 2.1 Materials and Methods

105 Natural chabazite was sourced as the product “Zeover” from Verdi S.p.A. The particle size range was 0.1
106 to 0.7 mm, the overall composition was $(\text{Na}_{0.14}\text{K}_{1.03}\text{Ca}_{1.00}\text{Mg}_{0.17})[\text{Al}_{3.36}\text{Si}_{8.53}\text{O}_{24}]\cdot 9.7\text{H}_2\text{O}$ with a cation
107 exchange capacity (CEC) of 2.2 ± 0.2 meq/g [22]. However, being derived from a natural source, 70% of
108 the material was chabazite, with the remaining fraction including contributions from: volcanic glass (18%);
109 phillipsite (2%); K-feldspar (5%); biotite (2%) and; pyroxene (3%) [22]. The natural chabazite in this proof
110 of concept study was previously utilised in vitrification studies as a reasonable simulant of a proprietary
111 ion exchange deployed by Kurion (now part of Veolia Nuclear Solutions) [23]. Therefore, the HIPed
112 wastefoms developed here could be relevant to the processing of spent high dose materials at Fukushima
113 Daiichi NPP, at a 70 wt. % waste loading (chabazite) with approximately 30 wt. % additives of suitable
114 composition (as a mixture of oxides or precursor glass frit), as described above.

115 Chabazite (250 g) was ion-exchanged using a solution of 0.1 M $^{133}\text{CsNO}_3$ (Sigma Aldrich, 99% purity)
116 dissolved in ultrapure deionized H_2O (18.2 M Ω) to simulate ion exchange operations at nuclear licensed
117 sites. The ion-exchange solution and chabazite were equilibrated on a roller mill for 24 h at room
118 temperature, after which the exchange solution was replaced and the process repeated for a second
119 exchange (cumulative 48 h exchange). The ion exchanged chabazite, hereafter referred to Cs-chabazite,
120 was vacuum filtered and washed three times using 1 L of distilled H_2O . The Cs-chabazite was dried at 95
121 °C for 48 h, the resulting material had a Cs_2O concentration of 2.88 ± 0.07 wt. % (determined *via* fused
122 bead X-ray Fluorescence (XRF) spectroscopy, Table 1), which was equivalent to 0.72 ± 0.02 mol. %. The Cs
123 uptake within chabazite was calculated to be 0.27 meq/g after a 48 h exchange period, which was
124 equivalent to a Cs loading of ~12%, based on the CEC for this natural source material. This is considered
125 reasonably representative of the operational deployment of this material, which does not target complete
126 exchange of Cs to the maximum sorption capacity, so as to maintain a high decontamination factor and
127 to enable the spent ion exchange material to be managed within acceptable dose rate constraints. The
128 exchange process occurred predominately with Ca (with minor changes for K, Mg and Na); CaO, decreased
129 from 8.23 ± 0.07 mol. % (as-received) to 7.68 ± 0.06 mol. % in the Cs-exchanged chabazite (Table 1). The
130 reported selectivity of chabazite (based on the Gibbs free energies of exchange) follows the order: $\text{Cs}^+ >$

131 $K^+ > Rb^+ > Na^+ = Ba^{2+} > Sr^{2+} > Ca^{2+} > Li^+$ [24, 25], which is broadly in agreement with our reported XRF data
132 (Table 1).

133 **Table 1.** XRF oxide composition of as-received chabazite and Cs-chabazite (errors indicated in parenthesis)

Oxide	Wt. %		Mol. %	
	As-received	Cs-chabazite	As-received	Cs-chabazite
Al ₂ O ₃	20.25 (± 0.06)	19.57 (± 0.10)	13.72 (± 0.03)	13.56 (± 0.06)
CaO	6.68 (± 0.03)	6.09 (± 0.05)	8.23 (± 0.02)	7.68 (± 0.06)
Cs ₂ O	0.00 (± 0.00)	2.88 (± 0.07)	0.00 (± 0.00)	0.72 (± 0.02)
Fe ₂ O ₃	5.48 (± 0.01)	5.46 (± 0.03)	2.37 (± 0.01)	2.42 (± 0.01)
K ₂ O	7.20 (± 0.03)	7.00 (± 0.07)	5.28 (± 0.04)	5.25 (± 0.06)
MgO	2.08 (± 0.02)	2.08 (± 0.01)	3.57 (± 0.04)	3.64 (± 0.03)
Na ₂ O	0.89 (± 0.01)	0.85 (± 0.01)	1.00 (± 0.01)	0.96 (± 0.01)
SiO ₂	56.73 (± 0.31)	55.38 (± 0.05)	65.24 (± 0.07)	65.15 (± 0.01)
TiO ₂	0.69 (± 0.02)	0.70 (± 0.02)	0.59 (± 0.01)	0.62 (± 0.02)

134

135 Thermal analysis and mass spectroscopy data were collected on the as-received chabazite using a Perkin
136 Elmer TGA 4000 instrument in conjunction with a HPR-20 QIC benchtop Gas Analysis System (MS) using
137 alumina crucibles under a N₂ atmosphere; the sample was heated to 1000 °C at a ramp rate of 10 °C/min.
138 All HIP samples were pre-calcined to remove water at 300 °C for 12 h in a muffle furnace prior to HIP
139 canister packing. Immediately following the pre-calcination step, ~35 g of Cs-chabazite was packed into
140 each HIP canister (manufactured in-house using 316 stainless steel) using a hydraulic press to increase the
141 packing density and, thus, the waste loading per HIP canister. Following this, each canister was qualified
142 for HIPing through a two-step evacuation and bake-out verification process. This involved evacuating the
143 HIP canister until a vacuum of <8 Pa was achieved, followed by exposure to 300 °C until the initial vacuum
144 recovered, at which point, the canister was crimped and sealed (welded) to create a hermetically sealed
145 work piece. These stages remove excess volatiles/water from the canister, which could have a deleterious
146 effect on the densification achieved and lead to porosity in the HIPed wastefrom [14, 26].

147 To determine the effectiveness of hot isostatic pressing (HIPing) as a thermal treatment application for
148 ion exchange materials, Cs-chabazite was HIPed at 1050 °C, 1150 °C and 1250 °C under two pressure

149 regimes, 100 MPa and 50 MPa ($\text{Ar}_{(g)}$ used as the pressurising media) with a fixed 4 h dwell period using
150 the AIP-630H research HIP at the University of Sheffield. Our choice of processing temperature was
151 governed by prior studies on high temperature treatment of ion exchange materials, which demonstrated
152 collapse and reaction of the aluminosilicate framework in the range 1000-1300 °C [27-29]. The HIPed
153 canisters were sectioned using a Buehler Abrasimet 250 saw and the extracted monoliths were further
154 sectioned for analysis using a Buehler Isomet 100 saw. Powder X-ray diffraction patterns were collected
155 between $5^\circ < 2\theta < 50^\circ$ using a Bruker D2 Phaser diffractometer with a Lynxeye detector and Ni filtered Cu
156 K_α radiation (1.5418 Å) using a step size of $0.02^\circ 2\theta$ and a count time of 1 s per step. Scanning Electron
157 Microscopy (SEM) images were collected using a low vacuum Hitachi TM3030 analytical benchtop SEM
158 with an integrated Bruker EDX system (Quantax 70) at 15 kV and a ~ 7.0 mm working distance on polished
159 ($1 \mu\text{m}$ diamond finish) and carbon coated specimens. Reported semi-quantitative compositions were
160 calculated based on the average of 10 spot analyses per phase with assumed oxygen stoichiometry (due
161 to the low accuracy of EDX for oxygen determination).

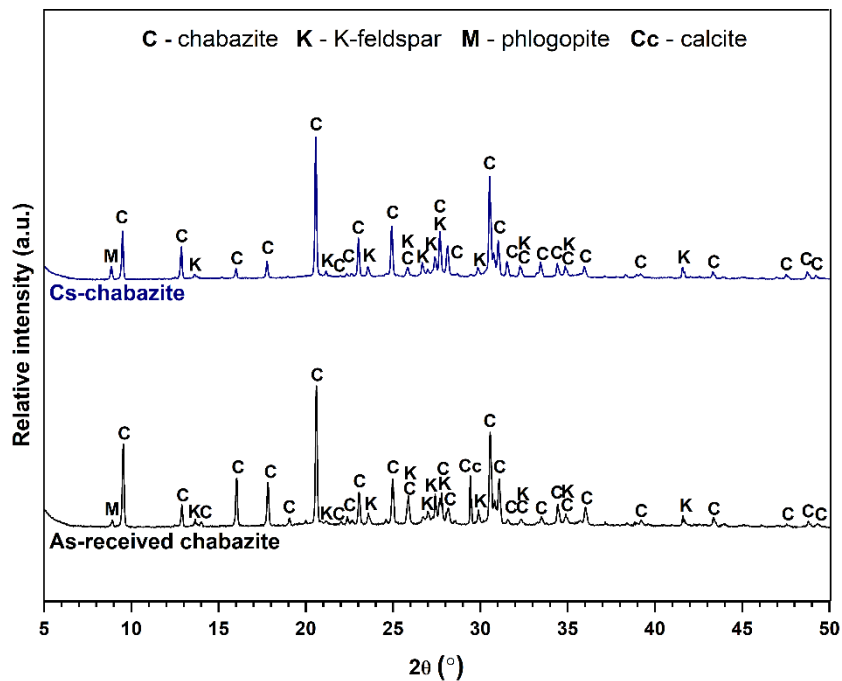
162 A durability assessment was performed using with ASTM C1285 methodology (PCT-B) [30]. Samples were
163 crushed and sieved to a size fraction of $150 - 75 \mu\text{m}$ and washed several times with isopropanol alcohol
164 to remove residual fines from the fraction. The desired sample mass was added to pre-cleaned PFA vessels
165 with 10 mL of ultrapure deionized H_2O (18.2 MΩ) to achieve a surface area to volume ratio of 2000m^{-1} .
166 The vessels were prepared in triplicate with duplicate blanks (ultrapure deionised H_2O only) and placed
167 within an oven at $90 \pm 1^\circ\text{C}$, with vessels being sacrificed for sampling at 1, 3, 7, 14 and 28 days. For each
168 time point, vessels were allowed to cool to room temperature before recording the total vessel mass (to
169 calculate evaporative loss) and monitoring the pH. An aliquot of the leachate was removed from each
170 vessel, filtered using a $0.2 \mu\text{m}$ cellulose acetate syringe filter and acidified using high purity nitric acid
171 (Fisher Scientific, Ultrapure NORMATOM, 67-69% HNO_3). The elemental concentration of Cs was
172 determined using by Inductively Coupled Plasma-Mass Spectroscopy (ICP-MS, Thermo Fisher Scientific
173 iCAP RQ), all other elements were measured using an Inductively Coupled Plasma-Optical Emission
174 Spectrometer (ICP-OES, Thermo Fisher Scientific iCAP Duo6300). The reported data were normalised to
175 the surface area to volume ratio and mass fraction of each element in the material, as determined by bulk
176 XRF analysis (Table 2).

177

178 **3. Results and Discussion**

179 **3.1 Chabazite characterisation**

180 Characterisation of the as-received and Cs-chabazite (Fig. 1) revealed that the phase assemblage
181 constituents were: chabazite (powder diffraction file (PDF) #00-034-0137), K-feldspar matched to sanidine
182 (KAlSi_3O_8 , PDF #00-010-0357) and mica, matched to phlogopite ($\text{KMg}_3(\text{AlSi}_3\text{O}_{10})(\text{OH})_2$, PDF #00-010-0495).
183 Calcite (CaCO_3 , PDF #00-005-0586) was also observed in the as-received chabazite (unwashed). It is likely
184 that other alkali feldspars (albite, microcline, orthoclase and anorthite) were present in minor fractions
185 but they could not be differentiated as they have similar diffraction patterns. Alkali feldspars exist as a
186 ternary solid solution within volcanic rocks (which was the source of chabazite in this study [22]) and are
187 typically comprised of albite ($\text{NaAlSi}_3\text{O}_8$), orthoclase (KAlSi_3O_8) and anorthite ($\text{CaAl}_2\text{Si}_2\text{O}_8$) [31]. With the
188 exception of a reduced calcite contribution, no significant differences were observed in the phase
189 assemblage between the as-received chabazite and the Cs-chabazite, which indicated that Cs was
190 incorporated *via* exchange into the chabazite framework.

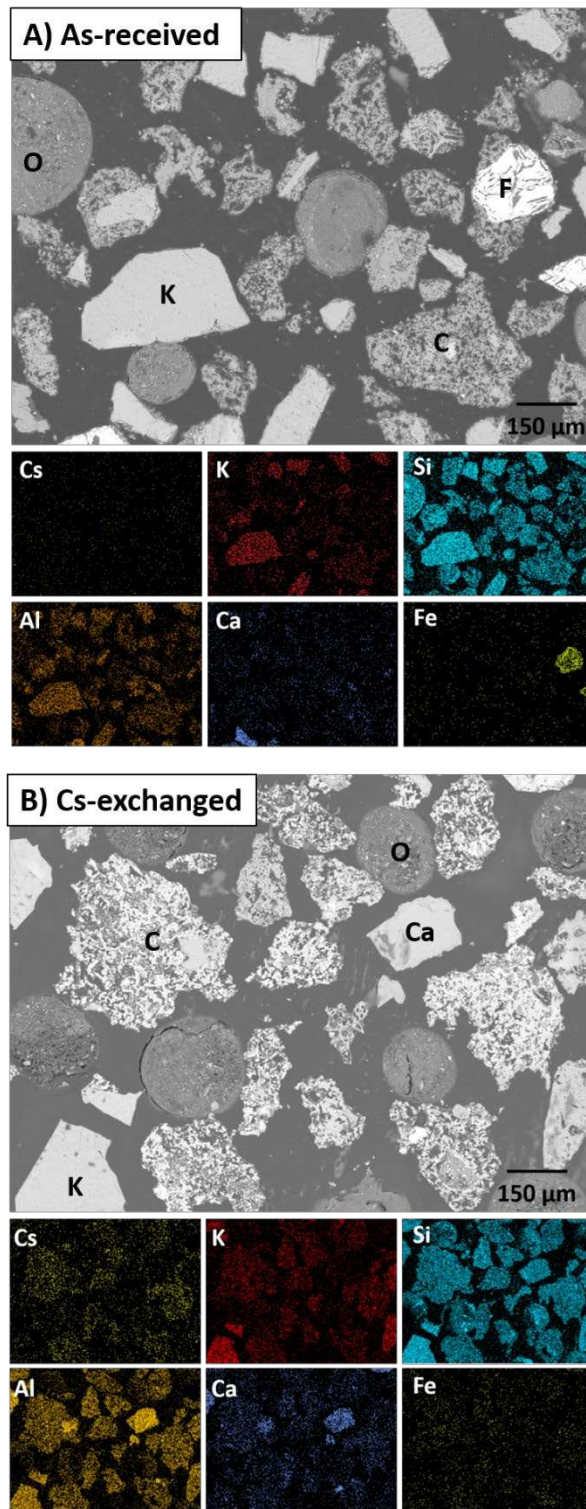


191

192

Figure 1. X-ray diffraction patterns of as-received chabazite and Cs-chabazite

193 The microstructures reported in Fig. 2 further demonstrates the heterogeneity of the natural chabazite.
194 The porous particles of various sizes were representative of chabazite, with strong elemental correlations
195 observed between Ca, K, Al and Si (Fig. 2A) with the addition of Cs in Fig. 2B (post exchange). The spherical
196 particles represent vitreous silica, which has a reported concentration of 18 wt. % in the as-received
197 chabazite [22]. The vitreous silica composition in the as-received chabazite was calculated by semi-
198 quantitative EDX analysis on an oxides basis as mol. % to be: 79.23 ± 2.48 SiO₂, 4.04 ± 0.94 Al₂O₃, $4.01 \pm$
199 0.88 CaO, 2.62 ± 0.39 K₂O, 1.21 ± 0.48 MgO and 0.26 ± 0.13 TiO₂ (the oxygen stoichiometry was assumed
200 on the basis of electroneutrality, due to the low accuracy of EDX for oxygen determination). This
201 composition is within the range of reported values for rhyolitic obsidian, which contains >66 mol. % SiO₂
202 [32]. Aluminosilicate particles rich in either Ca or K were also observed, which could represent anorthite
203 and K-feldspar (sanidine, orthoclase, microcline). To assess the potential for Cs incorporation in the
204 additional minor phases, K-feldspar (K), anorthite (Ca) and vitreous silica (O), EDX spectra of the as-
205 received chabazite and Cs-chabazite were compared in Fig. S1 (Supplementary Information). No distinct
206 signal could be detected for Cs (based on the L α_1 emission at 4.285 keV) except for within the Cs-chabazite
207 grain, confirming Cs exchange within this phase, as shown in Fig. 2B.



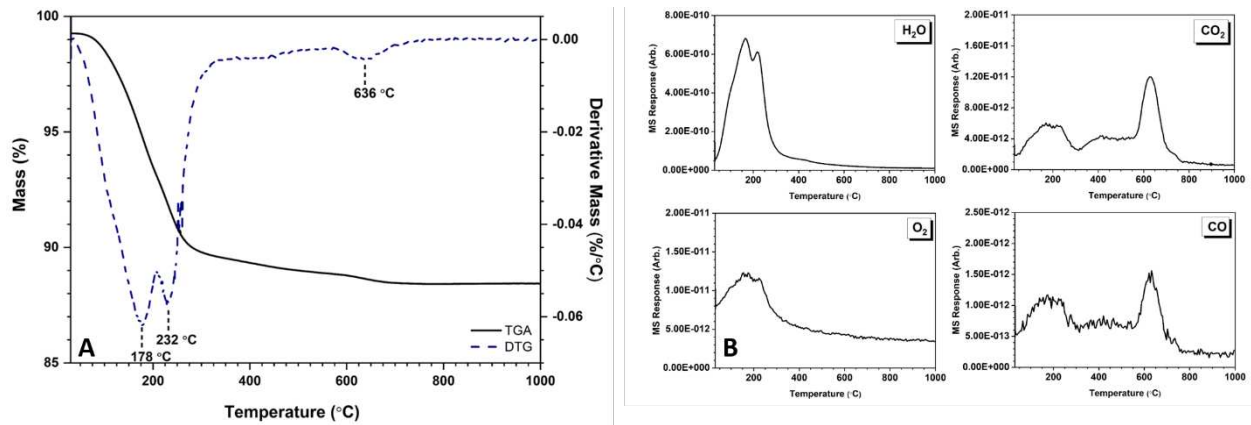
208

209 **Figure 2.** SEM/EDX of A) as-received chabazite and B) Cs-chabazite where labels indicate: C (chabazite), K
 210 (K-feldspar), Ca (Ca-feldspar), O (vitreous silica) and F (iron oxide).

211 The dehydration behaviour of as-received chabazite (Fig. 3) revealed that the main mass loss occurred
212 between 30-350 °C (equivalent to ~10%), which was determined by MS (Fig. 3B) to be associated with
213 water desorption from the chabazite structure (nominally $(\text{Na}_2\text{K}_2\text{CaMgAl}_2\text{Si}_{12}\text{O}_{24}\cdot 6\text{H}_2\text{O})$ and CO_2 from
214 decomposition of accessory carbonate minerals. The main mass loss feature presented as two distinct but
215 overlapping peaks centred at 178 °C and 232 °C (± 2 °C), which indicates that water was adsorbed on two
216 sites within chabazite in accordance with the published crystal structure [33]. A second minor mass loss
217 (~0.5%) was observed between 580-700 °C (centred at 636 ± 2 °C), which was associated with release of
218 CO_2 from accessory carbonate minerals (Fig. 3B). The TGA/MS data were used to determine a suitable
219 bake-out temperature during HIP canister preparation. Using Fig. 3, the pre-calcination and bake-out
220 temperature was fixed to 300 °C, which would ensure that all water was removed from the sample whilst
221 avoiding Cs volatilisation, which should not occur below 400 °C [34].

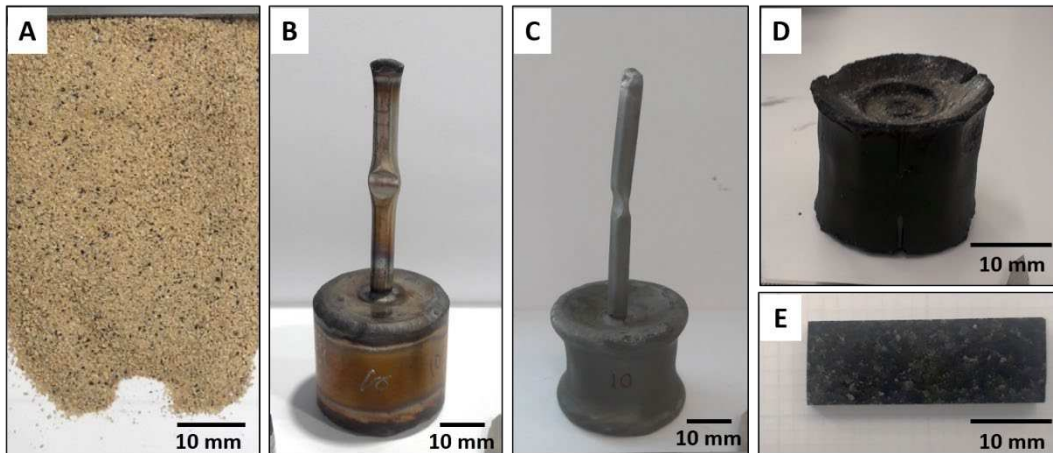
222 The photographs in Fig. 4 show the HIP canister deformation after HIPing (for the 1250 °C/100 MPa
223 sample). The internal volume was measured to decrease from $29.3 \pm 1 \text{ cm}^3$ to $16.9 \pm 0.8 \text{ cm}^3$, equivalent
224 to an internal volume reduction of 42.5%. Post-HIP, each canister was sectioned to enable
225 characterisation, which revealed that HIPing Cs-chabazite resulted in the formation of a dense monolith
226 with no visible porosity but obvious heterogeneity across the sample, as evidenced by particles of varying
227 colour within a black matrix (Fig. 4D). The conversion *via* HIPing of the highly dispersible Cs-chabazite
228 granular particles (Fig. 4A) into a solid monolith is unmistakable in Figs. 4D-E, which clearly improved the
229 passive safety of the material.

230



231
 232 **Figure 3.** A) TGA/DTG thermograph and B) MS response of as-received chabazite up to 1000 °C.

233



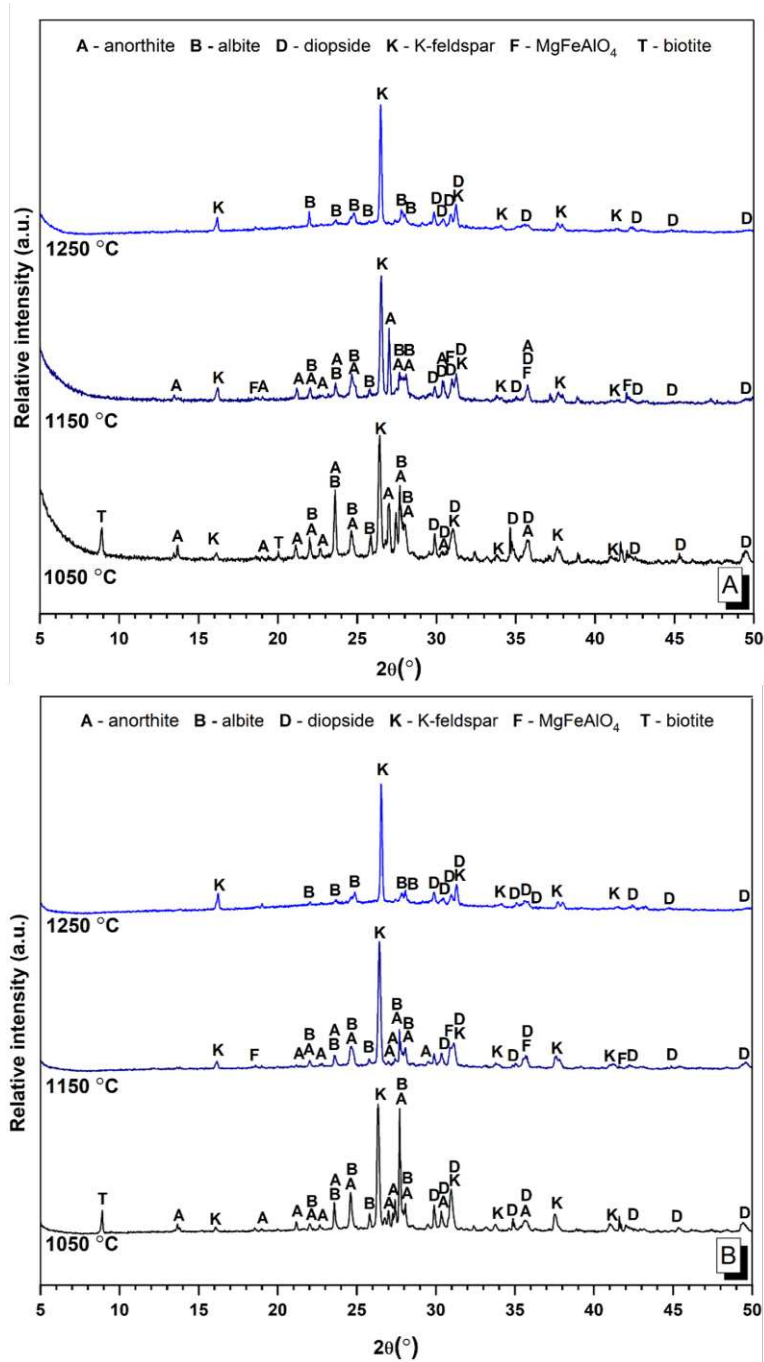
234
 235 **Figure 4.** Photographs of 1250 °C/100 MPa Cs-chabazite, A) Cs-chabazite, B) prepared HIP canister (post
 236 evacuation/bake-out), C) canister post-HIP, D) HIPed Cs-chabazite with canister removed and, E) a
 237 polished section from D. Note: Photographs D-E are from a larger HIP can processed under the same
 238 conditions, these images are shown to highlight the heterogeneity of the HIPed wasteform.

239

240 **3.2 Characterisation of HIPed Cs-chabazite**

241 In Figs. 5A-B, the XRD analysis revealed that the chabazite reflections identified in the pre-HIPed material
242 (Fig. 2) were absent, indicative of a complete collapse of the chabazite framework, irrespective of the
243 process conditions. At 1050 °C, the transformed phase assemblage could be described as a combination
244 of framework feldspars, including: anorthite ($\text{CaAl}_2\text{Si}_2\text{O}_8$, PDF #00-041-1486); albite ($\text{NaSi}_3\text{AlO}_8$, PDF #00-
245 010-393) and; leucite (KAlSi_2O_6 , PDF #01-076-2298), with minor reflections attributed to diopside
246 ($\text{CaMgSi}_2\text{O}_6$, PDF #01-075-1092). At 1150 °C, the relative intensities of all phases except leucite decreased,
247 in a trend which continued up to 1250 °C, resulting in leucite being the dominant crystalline phase in HIPed
248 Cs-chabazite. Diffuse scattering observed between $15^\circ < 2\theta < 35^\circ$ was noted to increase as the HIPing
249 temperature increased, which is associated with the formation of a vitreous aluminosilicate phase; given
250 the reduced relative intensity (or absence) of reflections associated with in anorthite, albite and diopside.
251 As confirmed by EDX analysis, shown below, the glass phase likely has a composition rich in Ca, K, Na, Mg,
252 Al and Si, consistent with vitrification of the aforementioned minerals. The XRD data revealed that a
253 systematic change in the phase assemblage of HIPed Cs-chabazite when the temperature was varied, in
254 materials processed under both 100 MPa and 50 MPa (Fig. 5B). Therefore, it is possible to conclude that
255 the conversion of Cs-chabazite to a glass-ceramic by HIPing was controlled by the temperature regime
256 rather than pressure. However, production of a satisfactory wasteform at a lower pressure of 50 MPa is
257 preferable, from an operational safety perspective, to reduce risk to as low as reasonably practicable.

258 The K-feldspar identified after conversion of Cs-chabazite at all temperatures was the high-temperature
259 polymorph, leucite (KAlSi_2O_6) with a cubic structure. This is somewhat unexpected since at temperatures
260 of $> 625^\circ\text{C}$, leucite is known to undergo a tetragonal ($I4_1/a$) to cubic ($Ia\bar{3}d$) inversion [35, 36] but, on
261 cooling, it should revert back to the tetragonal structure [37]. Since it was not possible to index any of the
262 reflections to the cubic ($Ia\bar{3}d$) Cs-feldspar endmember pollucite ($\text{CsAlSi}_2\text{O}_6$) [38], a plausible explanation
263 for the room temperature cubic structure could be Cs incorporation within the KAlSi_2O_6 lattice [39, 40].
264 The tetragonal and cubic structures of leucite can be differentiated by the cavity size in which the K^+ ion
265 resides, with average K-O bond lengths of $\sim 2.93\text{-}3.00\text{ \AA}$ and $3.35\text{-}3.54\text{ \AA}$, respectively [36, 37]. Given that
266 the ionic radius of Cs^+ is larger than that of K^+ , incorporation of Cs^+ within the framework channels of
267 leucite could prevent conversion to the lower symmetry structure on cooling. The Cs/K ratio within leucite
268 will be considered further in the following discussion.



269

270 **Figure 5.** XRD patterns of Cs-chabazite HIPed between 1050-1250 °C and A) 100 MPa or B) 50 MPa

271 XRF analysis (Table 2) confirmed successful retention of Cs₂O was achieved *via* HIPing with an average of
 272 2.50 wt. % measured across the three processing temperatures at 100 MPa. There was variability in the
 273 measured Cs₂O content of the HIPed material, ranging from 2.33 to 2.73 wt. % (Table 2), which was

274 thought to be associated with the high heterogeneity of this material, resulting in slightly different feed
 275 composition and hence Cs₂O content. The Cs₂O retention was calculated to be 85% (mean), 80%
 276 (minimum; 1150 °C) and 95% (maximum; 1250 °C) when compared to Cs-chabazite feed (using Tables 1-
 277 2). Following HIP canister preparation (discussed in Section 2.1), the canisters were hermetically sealed
 278 prior to thermal treatment and thus, there is no expectation that Cs volatilisation would occur during
 279 successful HIP processing, irrespective of processing temperature (i.e. where successful represents
 280 consolidated canisters with no weld failures).

281

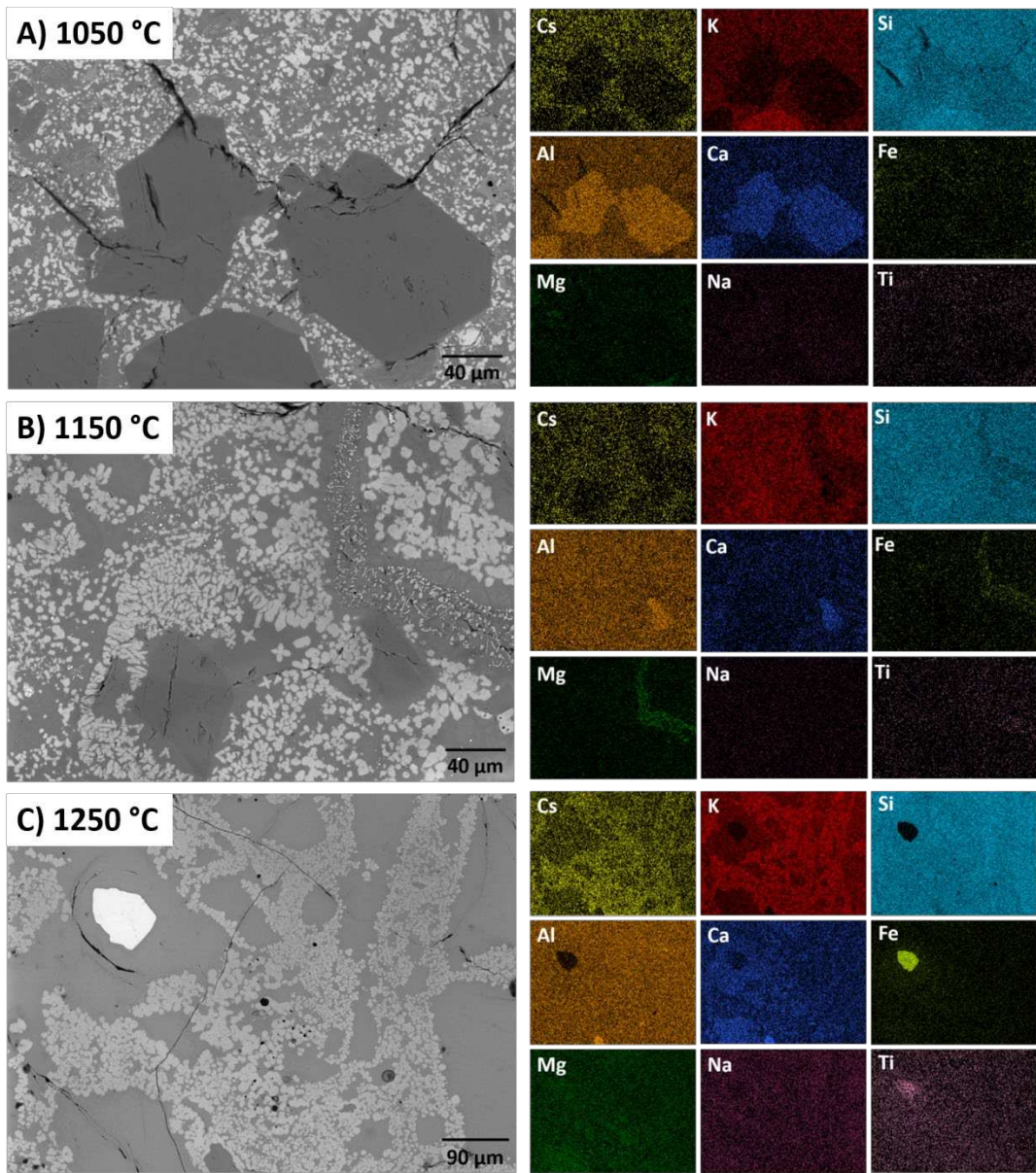
282 **Table 2.** XRF spectroscopy of HIPed Cs-chabazite at varying temperatures (wt. %), errors indicated in
 283 parenthesis

Oxide	1050 °C	1150 °C	1250 °C
Al ₂ O ₃	20.07 (± 0.13)	20.27 (± 0.16)	20.64 (± 0.11)
CaO	6.25 (± 0.01)	6.04 (± 0.02)	5.62 (± 0.06)
Cs ₂ O	2.45 (± 0.07)	2.33 (± 0.03)	2.73 (± 0.03)
Fe ₂ O ₃	6.43 (± 0.15)	5.67 (± 0.19)	4.59 (± 0.09)
K ₂ O	6.85 (± 0.08)	7.11 (± 0.09)	7.03 (± 0.04)
MgO	2.12 (± 0.01)	2.12 (± 0.01)	1.77 (± 0.02)
Na ₂ O	0.75 (± 0.01)	0.80 (± 0.02)	0.80 (± 0.04)
SiO ₂	53.93 (± 0.24)	54.57 (± 0.36)	55.67 (± 0.37)
TiO ₂	0.75 (± 0.02)	0.70 (± 0.03)	0.63 (± 0.02)
Density (g/cm³)	2.7226 (± 0.0036)	2.6639 (± 0.0024)	2.6489 (± 0.0016)

284

285 The microstructure of HIPed Cs-chabazite (Figs. 6-7) confirmed the presence of a multi-phase glass-
 286 ceramic composite at all temperatures and pressures investigated. The proportion of the glass fraction in
 287 the HIPed wastefrom appeared to increase with increasing processing temperature from 1050 to 1250 °C,
 288 which is attributed to a reduction in phases containing Ca, Mg, Al and Si, identified by XRD as anorthite,
 289 albite and diopside minerals. The bright grains, interspersed throughout the glass matrix, were rich in Cs,
 290 K, Al and Si, and represent cubic Cs/K-leucite as identified in Fig 5. At 1050 °C, there was also evidence for
 291 a K-feldspar with no Cs incorporation (Fig. 6A, centre bottom); which is likely present as a trace component

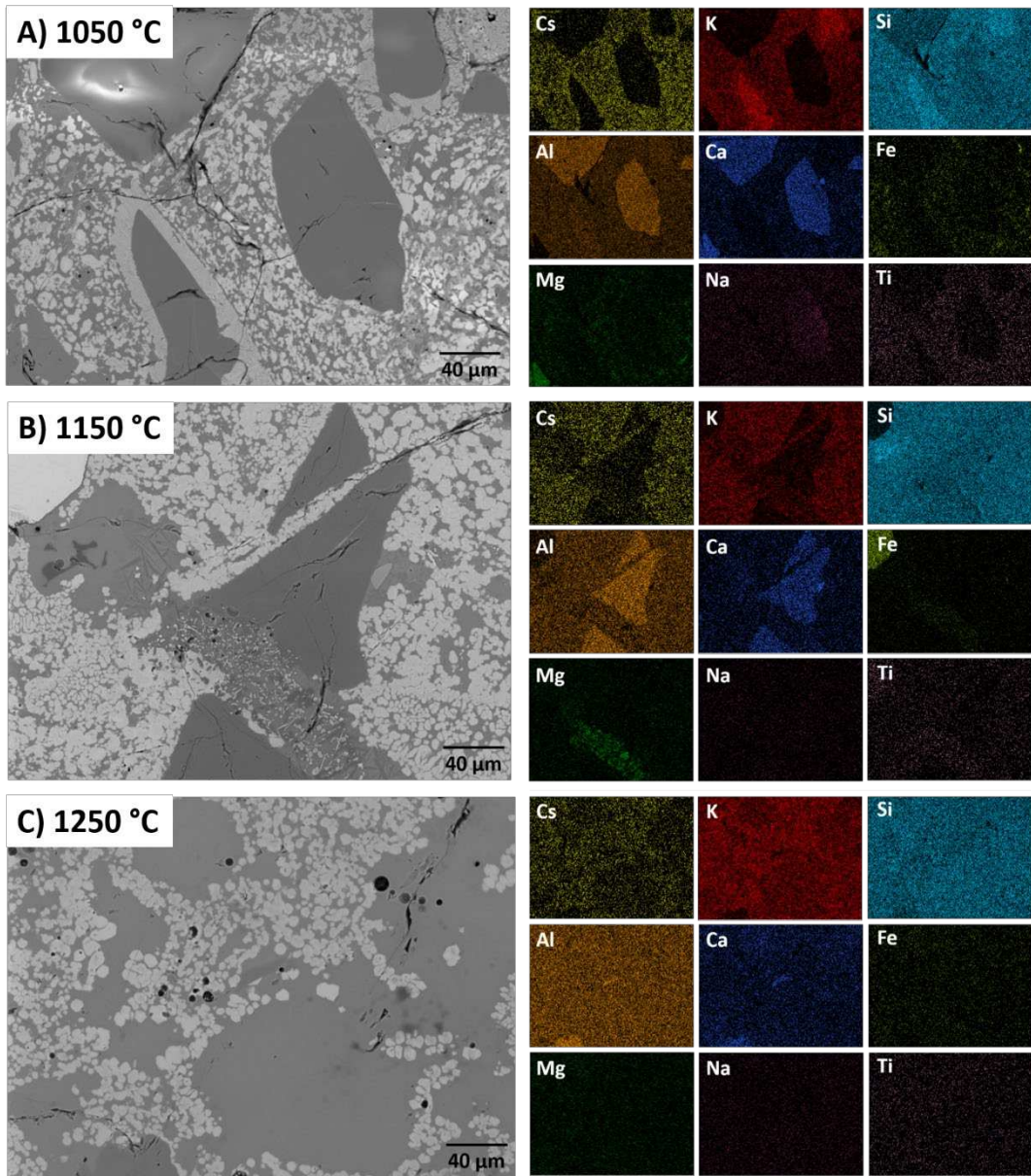
292 from the starting material (sanidine; KAlSi_3O_8) that was not detectable in the XRD data due to complex
293 diffraction patterns. At 1150 °C under both the 100 and 50 MPa regimes (Figs. 6B and 7B), the formation
294 of a spinel phase (rich in Mg and Fe) was observed, indicating that its formation is temperature dependent
295 over a narrow range. At 1250 °C (both pressures; Figs. 6C and 7C), the microstructure agreed with the XRD
296 (Fig. 5) where a reduction in the overall phase heterogeneity was observed in favour for a Cs-rich phase
297 (bright areas) and a Cs-deficient (mid-grey) phase, which were assigned to Cs/K-leucite and a glassy phase,
298 respectively. The SEM/EDX data revealed that the microstructure was independent of the pressure
299 imposed on the system, in agreement with the XRD results and, furthermore, that tailored microstructures
300 could be achieved *via* HIPing.



301

302

Figure 6. SEM/EDX of Cs-chabazite HIPed between 1050-1250 °C at 100 MPa



303

304

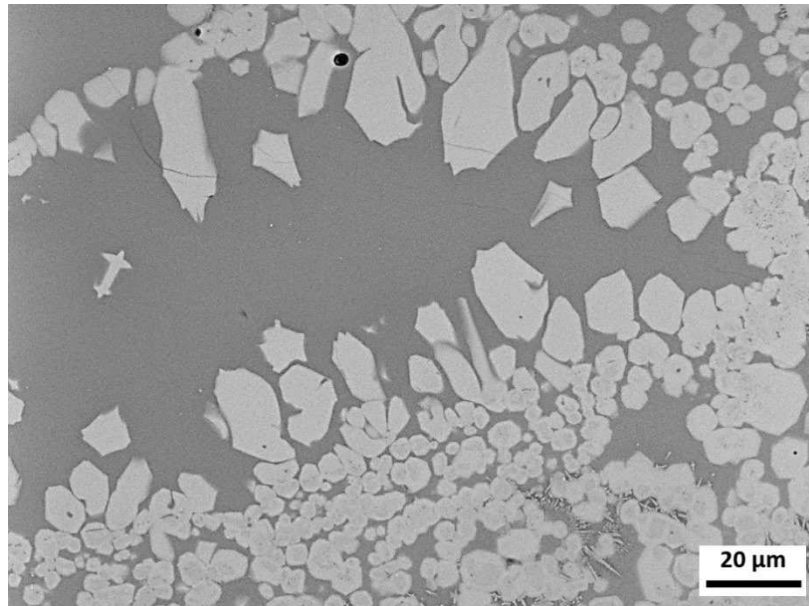
Figure 7. SEM/EDX of Cs-chabazite HIPed between 1050-1250 °C at 50 MPa

305

306 To evaluate the partitioning of Cs between the ceramic and glass phase, semi-quantitative EDX analysis
 307 was performed on Cs-chabazite HIPed at 1250 °C and 100 MPa (Fig. 8). The calculated composition was
 308 based on the average of 10 spot analyses per phase and are reported to one standard deviation (Table 3).

309 The crystallites were determined to have a composition of $Cs_{0.15(3)}K_{0.57(4)}Al_{0.90(4)}Si_{2.24(5)}O_6$ (herein referred

310 to as Cs/K-feldspar). Compared to the typical feldspar composition of $MA\text{Si}_2\text{O}_6$ (where M represents alkali
311 metals), this phase is Si-rich and Al/alkali metal-deficient. The Al/Si ratio for leucite feldspar should be 0.5
312 whereas, in this study, an Al/Si ratio of 0.32 ± 0.10 (Table 3) was achieved. The elemental Cs/K ratio was
313 0.25:1, with the total alkali metal content of the feldspar calculated to be 11.39 ± 1.10 mol. %. The Cs/K-
314 feldspar was incorporated within a $\text{K}_2\text{O-CaO-MgO-Al}_2\text{O}_3\text{-SiO}_2$ (alkali alkaline earth aluminosilicate) glass
315 with a high SiO_2 content and an Al/Si ratio of $\sim 1:12$. This contained 0.71 ± 0.17 mol. % Cs_2O , which is
316 equivalent to 23% of the measured Cs_2O inventory within the wasteform (Table 3). Based on these results,
317 it is possible to state that Cs preferentially partitioned into crystalline phases, however, a lower
318 concentration also partitioned into the vitreous phase.



319

320 **Figure 8.** BSE micrograph of Cs-chabazite HIPed at 1250 °C/100 MPa used for compositional analysis,
321 showing crystallites of Cs-containing leucite distributed within a glass matrix.

322

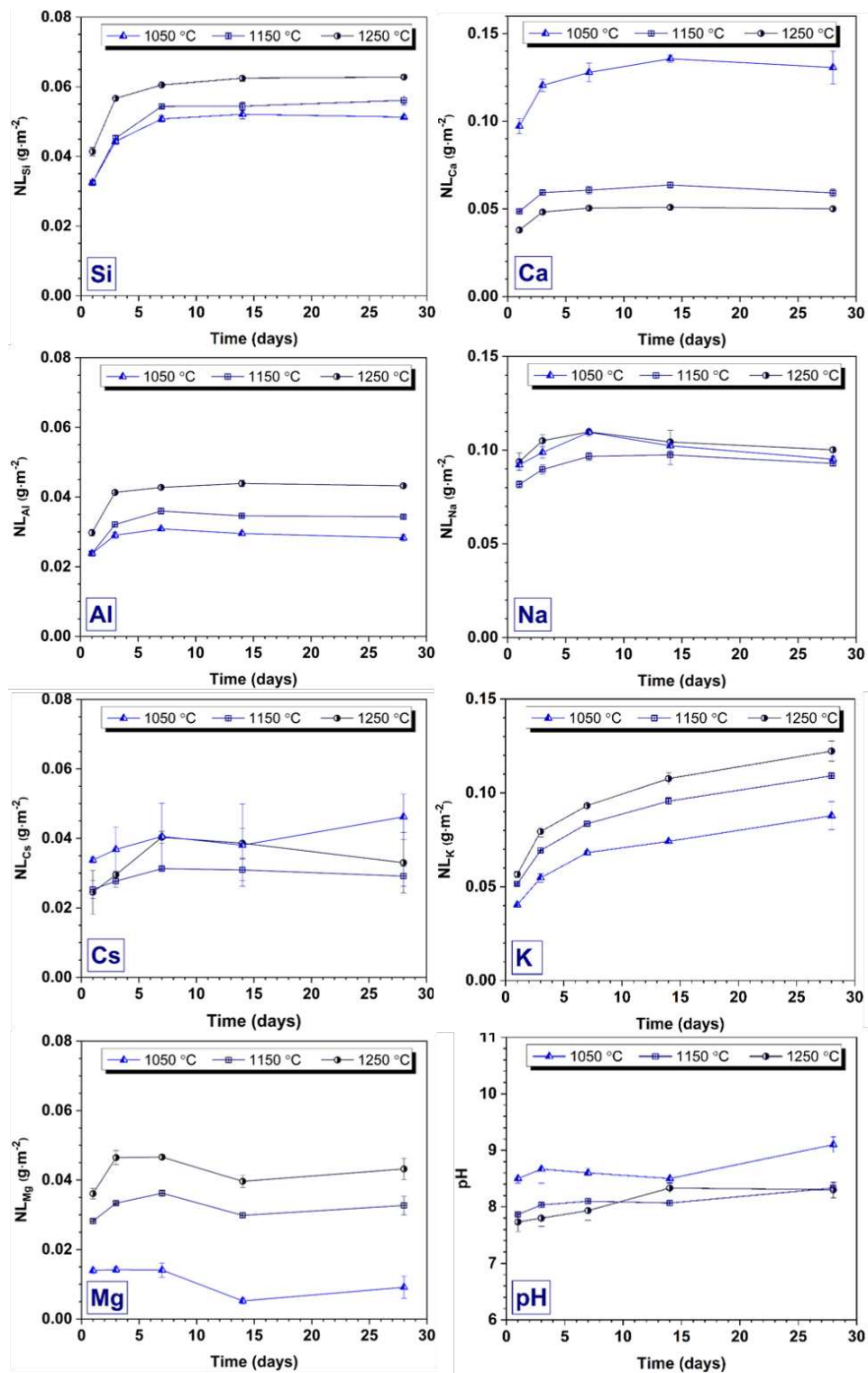
323 **Table 3.** Semi-quantitative EDX analysis of the 1250 °C/100 MPa HIPed chabazite in Figure 8 (errors
 324 indicated in parenthesis)

Oxide mol. %	Feldspar	Glass
Al ₂ O ₃	14.27 (± 0.61)	11.62 (± 0.71)
CaO	1.41 (± 0.79)	7.53 (± 1.37)
Cs ₂ O	2.40 (± 0.43)	0.71 (± 0.17)
Fe ₂ O ₃	1.07 (± 0.30)	1.24 (± 0.58)
K ₂ O	8.99 (± 0.67)	6.11 (± 0.89)
MgO	0.81 (± 0.47)	1.81 (± 0.78)
Na ₂ O	0.00 (± 0.00)	0.21 (± 0.21)
SiO ₂	71.06 (± 1.64)	70.77 (± 2.12)
Element at. %	Feldspar	Glass
<i>Al/Si</i>	0.40 (± 0.02)	0.33 (± 0.01)
<i>Cs+K/Si</i>	0.32 (± 0.02)	0.19 (± 0.03)
<i>Cs+K/Al</i>	0.80 (± 0.07)	0.57 (± 0.08)
<i>Cs/K</i>	0.25 (± 0.05)	0.12 (± 0.02)

325

326 **3.3 Durability Assessment**

327 PCT-B durability studies, to evaluate the performance of Cs-chabazite wastefoms, were conducted
 328 according to ASTM standard C1285-14 [30] up to 28 days for samples fabricated at 1050-1250 °C and 100
 329 MPa. The pH and elemental normalised mass loss (NL_i) values are presented in Fig. 9. All HIPed Cs-
 330 chabazite wastefoms had a relatively low pH throughout the duration of the experiment, which ranged
 331 between pH 8.6-8.7 ± 0.3 (1050 °C) and 7.8-8.2 ± 0.2 (1250 °C), with the 1050 °C samples consistently
 332 achieving a higher pH than the wastefoms processed at higher temperatures (Table 4). These values are
 333 lower than high level waste (HLW) glasses under similar conditions, consistent with the relatively low alkali
 334 and alkaline earth content of the aluminosilicate glass network. In compositions where the Si content is
 335 >67 mol. %, there are fewer interconnected non-bridging Si-O bonds, which provide dissolution pathways
 336 [41]. Therefore, the glass produced at 1250 °C (SiO₂ at 70.77 ± 2.12 mol. %; Table 3) has the potential to
 337 suppress ion migration and reduce dissolution (and thus, stabilise a low pH) leading to improved durability
 338 performance.



339

340

Figure 9. Normalised elemental mass loss for Cs-chabazite HIPed between 1050-1250 °C/100 MPa

341 The general trend for the Cs-chabazite wastefoms followed the typical behaviour of HLW waste glasses,
342 with a rapid elemental release (initial regime, 1-7 d) followed by a rate drop and attainment of pseudo-
343 steady state (residual regime, 7-28 d) for NL_{Si} , NL_{Al} and NL_{Ca} . Whilst the trend was similar, HLW glass
344 dissolution occurs congruently, which cannot be assumed (nor expected) in this study due to the presence
345 of mixed crystalline and vitreous phases. For NL_{Mg} , the elemental release decreased at 14 d, which is also
346 commonly observed for Mg-bearing HLW glasses (e.g. UK MW glass). Mg will readily scavenge Si to form
347 secondary phyllosilicate phases, often with a drop in pH and promotion of glass dissolution [42-44].
348 However, in conditions where the $pH \leq 8$, the precipitation of Mg-bearing phyllosilicates is reduced and
349 in-turn, this decreases the rate of glass alteration [44], which could be ascribed to the relatively low NL_{Si}
350 values.

351 For almost all elements (Fig. 9) the effect of processing temperature was the same, where a higher
352 processing temperature resulted in higher elemental release (*i.e.* $1250\text{ }^{\circ}\text{C} > 1150\text{ }^{\circ}\text{C} > 1050\text{ }^{\circ}\text{C}$). By SEM
353 analysis, the glass fraction was observed to increase commensurately with processing temperature (in
354 agreement with XRD data. Therefore, the higher elemental release at $1250\text{ }^{\circ}\text{C}$ indicates the glass phase is
355 more soluble than the crystalline phase (Cs/K-feldspar), as evidenced in Figs. S2-S7. The incongruent
356 dissolution of the HIPed Cs-chabazite wastefoms (at all temperatures) can be understood by exploring
357 the NL_{Cs} and NL_{K} relationship. Cs and K are inextricably linked in the crystalline phase (Cs/K-feldspar) and
358 both have similar ΔG_{hyd} of Cs^{+} (-250 kJ mol^{-1}) and K^{+} (-295 kJ mol^{-1}) [45]. This suggests that if the Cs/K-
359 feldspar was dissolving, NL_{Cs} and NL_{K} should follow the same trend, however, unlike NL_{Cs} , there was no
360 steady-state achieved for NL_{K} (Fig. 9) but rather continued elemental release. This dissimilarity in NL_{Cs} and
361 NL_{K} must therefore arise from the distribution of these elements across the crystalline and glass phases,
362 where Cs favoured the more durable crystalline phase compared to K (Table 3), which was distributed
363 between both the crystalline and less durable glass phase. This concurs with a recent study that compared
364 the dissolution behaviour of a crystalline feldspar ($Na_{0.83}K_{0.02}Ca_{0.07}Al_{1.06}Si_{2.96}O_8$) and a glass of the same
365 chemical composition, which ascertained that the glass phase dissolved more rapidly (up to 10-20 times
366 faster at pH 10) than the crystalline feldspar [46]. This difference was attributed to the local atomic
367 structure of the material, with the open structure of the glass encouraging ion exchange between water
368 and alkali elements whilst such diffusion related phenomenon were not observed in the crystalline
369 material [46].

370 An exception to the trend where elemental release is higher commensurate with processing temperature,
 371 was Ca. The highest Ca release was observed for the material processed at 1050 °C, in which the majority
 372 of the Ca was located within anorthite and diopside as distinct grains within the bulk matrix (based on
 373 SEM/EDX; Fig. 6), whereas at 1250 °C, no such features were identified. Whilst for NL_{Cs} , there was no clear
 374 trend associated with the processing temperature or Cs_2O concentration (Table 2). This was attributed to
 375 relatively low NL_{Cs} values (consistent with Cs preferentially partitioned in the durable crystalline phase),
 376 which were within one or two standard deviations at each time point. This close relationship was dissimilar
 377 to all other elements where there was a clear separation between the processing temperatures (and error
 378 bars) allowing for trends to be observed.

379 Examination of the HIPed Cs-chabazite grains at 28 d post dissolution (Figs S2-S7) revealed cracking
 380 damage evident on the periphery of the glassy portions of grains, while the crystalline regions remained
 381 largely intact, confirming the hypothesis that the glass dissolved preferentially. At all temperatures, no
 382 evidence of the formation of secondary minerals resulting from dissolution was found. A silica gel layer,
 383 containing Si and Al, responsible for the observed “rate drop” was apparent at the surface of some grains
 384 (e.g. Fig. S5), although it was not possible to undertake a detailed analysis of its composition at the
 385 resolution employed. Future investigation using direct surface retreat rate observation, e.g. vertical
 386 scanning interferometry (VSI), could be utilised to elucidate and define the contribution of each
 387 component phase present in the HIPed Cs-chabazite to the overall dissolution.

388 **Table 4.** Dissolution rates of HIPed Cs-chabazite at varying temperatures during the $NL_{i,initial}$ (1-7 d) and
 389 $NL_{i,residual}$ (7-28 d) regimes

Sample	Day	Av. pH	Na ($g\ m^{-2}\ d^{-1}$)	Si ($g\ m^{-2}\ d^{-1}$)	Cs ($g\ m^{-2}\ d^{-1}$)
1050	1-7	8.6 ± 0.2	(2.87 ± 0.12) × 10 ⁻³	(3.24 ± 0.92) × 10 ⁻³	(1.21 ± 0.16) × 10 ⁻³
1150	1-7	8.0 ± 0.1	(2.43 ± 0.49) × 10 ⁻³	(3.41 ± 0.82) × 10 ⁻³	(0.95 ± 0.05) × 10 ⁻³
1250	1-7	7.8 ± 0.2	(1.96 ± 0.79) × 10 ⁻³	(1.15 ± 0.68) × 10 ⁻³	(2.69 ± 0.03) × 10 ⁻³
1050	7-28	8.7 ± 0.3	(6.63 ± 0.95) × 10 ⁻⁴	(0.13 ± 0.34) × 10 ⁻⁴	(3.21 ± 1.70) × 10 ⁻⁴
1150	7-28	8.2 ± 0.1	(1.85 ± 0.45) × 10 ⁻⁴	(0.78 ± 0.26) × 10 ⁻⁴	(0.99 ± 0.15) × 10 ⁻⁴
1250	7-28	8.2 ± 0.2	(4.55 ± 0.31) × 10 ⁻⁴	(1.10 ± 0.21) × 10 ⁻⁴	(3.18 ± 0.52) × 10 ⁻⁴

390

391 The normalised dissolution rates (NR_i) quantified by linear regression for the $NR_{i,initial}$ and $NR_{i,residual}$ regimes
392 are shown in Table 4. The initial Na release rate, $NR_{Na,initial}$, determined for the material produced at
393 1050 °C, $(2.87 \pm 0.12) \times 10^{-3} \text{ g m}^{-2} \text{ d}^{-1}$, was marginally higher than for the material produced 1250 °C, $(1.96$
394 $\pm 0.79) \times 10^{-3} \text{ g m}^{-2} \text{ d}^{-1}$. It was demonstrated (Table 3) that Na was exclusively located in the vitreous phase
395 at 1250 °C, and, as such, supports the conclusion that alkali alkaline earth aluminosilicate glass underwent
396 dissolution in this study. The residual rates of Na release, $NR_{Na,residual}$, were reduced by an order of
397 magnitude compared to the initial rates, following the rate drop at > 7 d. In HLW (UK MW with 25 wt. %
398 waste loading), the NR_{Na} at 90 °C and pH 8 was $(1.583 \pm 0.209) \text{ g m}^{-2} \text{ d}^{-1}$, which increased to $(1.91 \pm$
399 $0.25) \text{ g m}^{-2} \text{ d}^{-1}$ at a higher waste loading (30 wt. % MW glass) [47]. Whilst in an ILW glass wastefrom
400 proposed for Mg-rich wastes, the NR_{Na} was observed to be $(2.62 \pm 0.45) \times 10^{-2} \text{ g m}^{-2} \text{ d}^{-1}$ and $(4.06 \pm$
401 $0.16) \times 10^{-3} \text{ g m}^{-2} \text{ d}^{-1}$ in the initial and residual regimes, respectively [48]. The NR_{Na} values in the current
402 study were at least an order of magnitude lower than both the HLW and ILW proposed glass wastefroms,
403 demonstrating that these HIPed wastefroms have an improved performance compared to vitrified
404 wastefroms intended for geological disposal in the UK, at least in short term experiments designed to
405 assess the inherent material dissolution rate. Nevertheless, further investigation is warranted to examine
406 the long term dissolution behaviour of this composite vitreous wastefrom and the potential for rate
407 resumption.

408 Since there are few studies related to the durability of thermally treated chabazite spent ion exchange
409 material, we compare the results from the present study with those from thermally-treated Cs-exchanged
410 clinoptilolite $((\text{Na,K,Ca})_{2-3}\text{Al}_3(\text{Al,Si})_2\text{Si}_{13}\text{O}_{36} \cdot 12\text{H}_2\text{O})$, which is also a natural zeolite-based aluminosilicate
411 framework mineral used in radionuclide water treatment. The thermal treatment of Cs-clinoptilolite
412 (containing ~1 wt. % Cs_2O) *via* HIPing (1200 °C, 100 MPa) was achieved with 5 wt. % addition of glass
413 additives (sodium aluminate or borax) [29]. The chemical durability assessment was performed under
414 almost identical conditions as those used in the current investigation (SA/V, T, t and solution) with the
415 NL_{Cs} reported to be $(4.91 \text{ and } 6.79) \times 10^{-4} \text{ g m}^{-2} \text{ d}^{-1}$ after 28 days for the sodium aluminate and borax
416 modified compositions, respectively [29]. In the current study, the overall normalised release rate for Cs
417 (1-28 d) was calculated to be $(8.69 \pm 0.62) \times 10^{-5} \text{ g m}^{-2} \text{ d}^{-1}$ at 1250 °C, an order of magnitude better than
418 HIPed Cs-clinoptilolite, with respect to Cs release.

419 Whilst the full Cs-feldspar endmember (pollucite, $\text{CsAlSi}_2\text{O}_6$) was not attained (nor targeted) in this study,
420 Cs incorporation into feldspars has been investigated as an immobilisation matrix for radiocaesium at the

421 Hanford site, USA [49]. Pollucite, which can contain up to 34 wt. % Cs₂O [50], was found to be a suitable
422 candidate for ¹³⁷Cs due to its high durability, low solubility and thermal stability [49], and has been
423 suggested as an appropriate immobilisation matrix for ¹³⁷Cs [49, 51-53]. For example, under hydrothermal
424 conditions (200 °C/30 MPa for 4 weeks), the measured release of Cs from pollucite was just 0.04% in
425 deionised water [54]. Therefore, it is plausible that the formation of Cs_{0.15(3)}K_{0.57(4)}Al_{0.90(4)}Si_{2.24(5)}O₆ feldspar
426 (composition formed by processing at 1250 °C/100 MPa) could provide a durable host matrix for
427 radiocaesium, in addition to the HIP process itself minimising the risk of Cs volatilisation and secondary
428 waste generation. Overall, the elemental release rates were low throughout the duration of this study
429 and at all processing temperatures, which indicates that the hot isostatic pressing of spent ion exchange
430 materials can lead to the formation of durable glass-ceramic wasteforms.

431

432 **4. Conclusions**

433 The passive safety of spent ion exchange materials was improved by conversion into a chemically and
434 physically stable monolith wasteform by thermal treatment of Cs-chabazite *via* HIPing. A multi-phase
435 glass-ceramic with a high Cs retention was achieved at 1050, 1150 and 1250 °C under two pressure
436 regimes. Characterisation of HIPed wasteforms by XRD and SEM/EDX revealed the complete collapse of
437 the chabazite framework structure at all temperatures, with the processing temperature observed to
438 control the phase assemblage. At 1250 °C, a Cs/K-leucite was formed which contained 77 % of the total
439 Cs₂O inventory, with the remaining fraction (23%) located within an alkali alkaline earth aluminosilicate
440 glass (K₂O-CaO-MgO-Al₂O₃-SiO₂). The normalised Na release rates were observed to be an order of
441 magnitude lower than values reported for HLW and ILW glasses, whilst the Cs release rate remained low for
442 the duration of the experiment at all temperatures, which was thought to be released preferentially from
443 the glass fraction rather than the Cs/K-feldspar.

444 For Cs-loaded ion exchange materials, the radiological risk will be significantly reduced within ~300 years
445 (Cs¹³⁷ t_{1/2} = 30.2 years) without any engineering imposed on the waste. Therefore, the fact that these
446 HIPed Cs-chabazite wasteforms perform (up to day 28) better than or comparable to reported values for
447 HLW glasses (with a longer required service life for long-lived radionuclides) is a good indication that
448 HIPing would be a suitable treatment method for spent ion exchange materials. However, additional data

449 is required at extensive time periods (months to years) to determine the long-term durability of
450 Cs-chabazite, with particular emphasis on larger-scale wastefoms (*i.e.* greater than 35 g) to support
451 potential scale-up operations. Future work should investigate the impact of chlorine incorporation within
452 Cs-chabazite on the wastefom phase assemblage and interaction with the HIP canister (sea water was
453 used at Fukushima Daiichi NPP for emergency cooling the damaged reactors) [55].

454 Overall, this study demonstrated the efficacy of HIPing to convert inorganic ion exchange materials into
455 durable glass-ceramic wastefoms in addition to a notable volume reduction and a relatively high waste
456 loading (70 wt. %). HIPing was shown to be a suitable thermal treatment technology with respect to
457 increasing the passive safety of conditioned spent ion exchange materials, whilst also reducing the risk
458 associated with loss of containment of these stored wastes. This study focussed specifically on the waste
459 management for Fukushima Daiichi NPP, however, the thermal treatment of spent ion exchange materials
460 *via* HIPing could successfully be applied on a wider scale to all sites where these types of inorganic wastes
461 are generated.

462

463 **Supplementary Information**

464 Additional SEM/EDX data of as-received chabazite, Cs-chabazite and HIPed Cs-chabazite (post-dissolution)

465

466 **ACKNOWLEDGMENTS**

467 The authors are grateful to UKRI EPSRC for sponsorship of this research under grant references
468 EP/N017617/1, EP/P013600/1, EP/S01019X/1 and EP/S032959/1. CLC is grateful to the University of
469 Sheffield for the award of a Vice Chancellor's fellowship and EPSRC for the award of an Early Career
470 Fellowship under grant reference EP/N017374/1. This research utilised the HADES/MIDAS facility and
471 Henry Royce Institute at the University of Sheffield established with financial support from UKRI EPSRC
472 and BEIS, under grant EP/T011424/1 and EP/P02470X/1 [56]. We are grateful to the eight anonymous
473 reviewers for their careful consideration of our draft manuscript and suggestions for improvement.

474

475 **Competing interest statement**

476 The authors declare that they have no known competing financial interests or personal relationships that
477 could have appeared to influence the work reported in this paper.

478

479 **REFERENCES**

480 [1] Tokyo Electric Power Company, Fukushima nuclear accident analysis report, in, Tokyo Electric Power
481 Company Holdings, Inc., Tokyo, Japan, , 2012.

482 [2] International Atomic Energy Agency, The Fukushima Daiichi accident. Technical Volume 1: Description
483 and context of the accident, in, International Atomic Energy Agency, Vienna, Austria, 2015.

484 [3] J. Lehto, R. Koivula, H. Leinonen, E. Tusa, R. Harjula, Removal of Radionuclides from Fukushima Daiichi
485 Waste Effluents, Separation & Purification Reviews, 48 (2019) 122-142.

486 [4] D. Delacroix, J. P. Guerre, P. Leblanc, C. Hickman, Radionuclide and radiation protection data handbook
487 2002, Radiation Protection Dosimetry, Nuclear Technology Publishing, 98 (2002) 1-168.

488 [5] M.S. Denton, J.L. Mertz, W.D. Bostick, Fukushima nuclear crisis recovery: a modular water treatment
489 system deployed in seven weeks, in: Waste Management, AZ, USA, 2012.

490 [6] UOP, IONSIV™ selective media: water decontamination at Japan's Fukushima Daiichi nuclear power
491 plant, in, UOP LLC, USA, September 2013.

492 [7] Tokyo Electric Power Company, Situation of storage and treatment of accumulated water including
493 highly concentrated radioactive materials and Fukushima Daiichi nuclear power station (448th release)
494 - April 20, 2020, in, Tokyo Electric Power Company Holdings, Inc, Toyko, Japan, 2020.

495 [8] I. Yamagishi, R. Nagaishi, C. Kato, K. Morita, A. Terada, Y. Kamiji, R. Hino, H. Sato, K. Nishihara, Y.
496 Tsubata, S. Tashiro, R. Saito, T. Satoh, J. Nakano, W. Ji, H. Fukushima, S. Sato, M. Denton, Characterization
497 and storage of radioactive zeolite waste, Journal of Nuclear Science and Technology, 51 (2014) 1044-1053.

498 [9] H.V. Atkinson, S. Davies, Fundamental aspects of hot isostatic pressing: an overview, Metallurgical and
499 Materials Transactions A, 31A (2000) 2981-3000.

500 [10] P.G. Heath, Stewart, Martin W. A., Moricca, Sam. Hyatt, Neil C., Hot-isostatically pressed wastefoms
501 for Magnox sludge immobilisation, Journal of Nuclear Materials, 499 (2018) 233-241.

502 [11] L.J. Gardner, Walling, S. A., Hyatt, N. C., Hot isostatic pressing: thermal treatment trials of inactive
503 and radioactive simulant UK intermediate level waste, IOP Conference Series: Materials Science and
504 Engineering, 818 (2020) 012009.

- 505 [12] K.J. Bateman, E.P. Hart, W.M. McCartin, D.L. Wahlquist, Summary of calcine disposal development
506 using hot isostatic pressing, in, Idaho National Laboratory, Idaho, USA, 2013.
- 507 [13] E.R. Vance, M.W.A. Stewart, S.A. Moricca, Progress at ANSTO on SYNROC, Journal of the Australian
508 Ceramic Society, 50 (2014) 38-48.
- 509 [14] S.M. Thornber, P.G. Heath, G.P. Da Costa, M.C. Stennett, N.C. Hyatt, The effect of pre-treatment
510 parameters on the quality of glass-ceramic wasteforms for plutonium immobilisation, consolidated by hot
511 isostatic pressing, Journal of Nuclear Materials, 485 (2017) 253-261.
- 512 [15] Nuclear Decommissioning Authority, Progress on plutonium consolidation, storage and disposition in,
513 2019.
- 514 [16] L.R. Blackburn, L.J. Gardner, S.K. Sun, E.R. Maddrell, M.C. Stennett, C.L. Corkhill, N.C. Hyatt, Hot
515 Isostatically Pressed Zirconolite Wasteforms for Actinide Immobilisation, IOP Conference Series: Materials
516 Science and Engineering, 818 (2020) 012010.
- 517 [17] S.M. Thornber, L.M. Mottram, A.R. Mason, P. Thompson, M.C. Stennett, N.C. Hyatt, Solubility,
518 speciation and local environment of chlorine in zirconolite glass-ceramics for the immobilisation of
519 plutonium residues, RSC Advances, 10 (2020) 32497-32510.
- 520 [18] M.W.A. Stewart, S.A. Moricca, T. Eddowes, Y. Zhang, E.R. Vance, G.R. Lumpkin, M.L. Carter, M.
521 Dowson, M. James, The use of hot-isostatic pressing to process nuclear waste forms, in: Proceedings of
522 the 2009 12th International Conference on Environmental Remediation and Radioactive Waste
523 Management ICEM2009, Liverpool, UK, 2009, pp. ICEM2009-16253.
- 524 [19] E.R. Vance, S. Moricca, B.D. Begg, M.W.A. Stewart, Y. Zhang, M.L. Carter, Advantages hot isostatically
525 pressed ceramic and glass-ceramic waste forms bring to the immobilization of challenging intermediate-
526 and high-level nuclear wastes, Advances in Science and Technology, 73 (2011) 130-135.
- 527 [20] D.J. Gregg, Farzana, Rifat, Dayal, Pranesh, Holmes, Rohan, Triani, Gerry, Synroc technology:
528 Perspectives and current status (Review), Journal of the American Ceramic Society, 00 (2020) 1-18.
- 529 [21] Nuclear Decommissioning Authority, NDA plutonium topic strategy: Credible option technical analysis.
530 SAF/081208/006/02, in, Nuclear Decommissioning Authority, 2009.
- 531 [22] Verdi S.p.A, Zeover data sheet, in, Verdi S.p.A, Torino, Italy, 2015.
- 532 [23] D. Pletser, R.K. Chinnam, M. Kamoshida, W.E. Lee, Immobilisation process for contaminated zeolitic
533 ion exchangers from Fukushima, MRS Advances, 1 (2016) 4089-4094.
- 534 [24] R.M. Barrer, J.A. Davies, L.V.C. Rees, Thermodynamics and thermochemistry of cation exchange in
535 chabazite, Journal of Inorganic and Nuclear Chemistry, 31 (1969) 219-232.
- 536 [25] M. Kong, Z. Liu, T. Vogt, Y. Lee, Chabazite structures with Li⁺, Na⁺, Ag⁺, K⁺, NH₄⁺, Rb⁺ and Cs⁺ as extra-
537 framework cations, Microporous and Mesoporous Materials, 221 (2016) 253-263.

- 538 [26] D. Wahlquist, K. Bateman, T. Malewitz, Remote Sealing of Canisters for Hot Isostatic Pressing, in:
539 ASME 2014 International Mechanical Engineering Congress and Exposition, 2014.
- 540 [27] R. Kimura, Y. Inagaki, K. Idemitsu, T. Arima, Vitrification processes of simulated cesium sorbing zeolite
541 waste, *Progress in Nuclear Energy*, 108 (2018) 497-502.
- 542 [28] T.-Y. Chen, E.R. Maddrell, N.C. Hyatt, A.S. Gandy, M.C. Stennett, J.A. Hriljac, Transformation of Cs-
543 IONSIV® into a ceramic wastefrom by hot isostatic pressing, *Journal of Nuclear Materials*, 498 (2018) 33-
544 43.
- 545 [29] P.G. Heath, Alternative procesing methods for the thermal treatment of radioactive wastes, in:
546 *Materials Science and Engineering*, Univeristy of Sheffield, 2015.
- 547 [30] ASTM International, C1285-14 Standard Test Methods for Determining Chemical Durability of
548 Nuclear, Hazardous, and Mixed Waste Glasses and Multiphase Glass Ceramics: The Product Consistency
549 Test (PCT), in, West Conshohocken, PA, 2014.
- 550 [31] W.A.F. Deer, R.A. Howie, J. Zussman, An Introduction to the Rock-Forming Minerals, in, *Mineralogical*
551 *Society of Great Britain and Ireland*, 2013.
- 552 [32] J.E. Ericson, A. Makishima, J.D. Mackenzie, R. Berger, Chemical and physical properties of obsidian: a
553 naturally occuring glass, *Journal of Non-Crystalline Solids*, 17 (1975) 129-142.
- 554 [33] J.L. Stakebake, Characterization of natural chabazite and 5A synthetic zeolites: Part I. Thermal and
555 outgassing properties, *Journal of Colloid and Interface Science*, 99 (1984) 41-49.
- 556 [34] M.I. Ojovan, W.E. Lee, An introduction to nuclear waste immobilisation - 2nd edition, 2 ed., Elsevier,
557 Oxford, UK, 2013.
- 558 [35] K. Hirao, N. Soga, M. Kunugi, Thermal expansion and structure of leucite-type compounds, *The*
559 *Journal of Physical Chemistry*, 80 (1976) 1612-1616.
- 560 [36] F. Mazzi, The crystal structure of tetragonal leucite, *American Mineralogist*, 61 (1976) 108-115.
- 561 [37] C. Palmer David, T. Dove Martin, M. Ibberson Richard, M. Powell Brian, Structural behavior, crystal
562 chemistry, and phase transitions in substituted leucite: High-resolution neutron powder diffraction
563 studies, in: *American Mineralogist*, 1997, pp. 16.
- 564 [38] D. Taylor, C.M.B. Henderson, The thermal expansion of the leucite group of minerals, *American*
565 *Mineralogist*, 53 (1968) 1476-1489.
- 566 [39] P. He, Z. Yang, J. Yang, X. Duan, D. Jia, S. Wang, Y. Zhou, Y. Wang, P. Zhang, Preparation of fully
567 stabilized cubic-leucite composite through heat-treating Cs-substituted K-geopolymer composite at high
568 temperatures, *Composites Science and Technology*, 107 (2015) 44-53.
- 569 [40] P. He, D. Jia, M. Wang, Y. Zhou, Effect of cesium substitution on the thermal evolution and ceramics
570 formation of potassium-based geopolymer, *Ceramics International*, 36 (2010) 2395-2400.

- 571 [41] C.M. Jantzen, K.G. Brown, J.B. Pickett, Durable Glass for Thousands of Years, *International Journal of*
572 *Applied Glass Science*, 1 (2010) 38-62.
- 573 [42] B.M.J. Thien, N. Godon, A. Ballester, S. Gin, A. Ayrat, The dual effect of Mg on the long-term
574 alteration rate of AVM nuclear waste glasses, *Journal of Nuclear Materials*, 427 (2012) 297-310.
- 575 [43] E. Curti, J.L. Crovisier, G. Morvan, A.M. Karpoff, Long-term corrosion of two nuclear waste reference
576 glasses (MW and SON68): A kinetic and mineral alteration study, *Applied Geochemistry*, 21 (2006) 1152-
577 1168.
- 578 [44] H. Aréna, N. Godon, D. Rébiscoul, R. Podor, E. Garcès, M. Cabie, J.P. Mestre, Impact of Zn, Mg, Ni and
579 Co elements on glass alteration: Additive effects, *Journal of Nuclear Materials*, 470 (2016) 55-67.
- 580 [45] Y. Marcus, Thermodynamics of solvation of ions. Part 5.—Gibbs free energy of hydration at 298.15 K,
581 *Journal of the Chemical Society, Faraday Transactions*, 87 (1991) 2995-2999.
- 582 [46] A. Perez, D. Daval, M. Fournier, M. Vital, J.-M. Delaye, S. Gin, Comparing the reactivity of glasses with
583 their crystalline equivalents: The case study of plagioclase feldspar, *Geochimica et Cosmochimica Acta*,
584 254 (2019) 122-141.
- 585 [47] C.L. Corkhill, A.J. Fisher, D.M. Strachan, R.J. Hand, N.C. Hyatt, Corrigendum to “The dissolution rates
586 of simulated UK Magnox – ThORP blend nuclear waste glass as a function of pH, temperature and waste
587 loading” [*Miner. Mag.* 79, (2015) 1529–1542], *Mineralogical Magazine*, 82 (2018) 939-942.
- 588 [48] S.A. Walling, M.N. Kauffmann, L.J. Gardner, D.J. Bailey, M.C. Stennett, C.L. Corkhill, N.C. Hyatt,
589 Characterisation and disposability assessment of multi-waste stream in-container vitrified products for
590 higher activity radioactive waste, *Journal of Hazardous Materials*, (2020) 123764.
- 591 [49] D.M. Strachan, W.W. Schulz, Characterisation of pollucite as a material for the long term storage of
592 Cesium-137 (ARH-SA-294), in, *Atlantic Richfield Hanford Company, Richland, Washington*, 1977.
- 593 [50] H.L. Finston, M.T. Kinsley, The radiochemistry of cesium, in, *Brookhaven National Laboratory, New*
594 *York, USA*, 1961.
- 595 [51] Y. Yokomori, K. Asazuki, N. Kamiya, Y. Yano, K. Akamatsu, T. Toda, A. Aruga, Y. Kaneo, S. Matsuoka, K.
596 Nishi, S. Matsumoto, Final storage of radioactive cesium by pollucite hydrothermal synthesis, *Scientific*
597 *Reports*, 4 (2014) 4195.
- 598 [52] E.R. Vance, B.E. Scheetz, M.W. Barnes, B.J. Bodnar, Studies of pollucite, in: *MRS Proceedings*, 1981.
- 599 [53] K. Yanagisawa, M. Nishioka, N. Yamasaki, Immobilization of cesium into pollucite structure by
600 hydrothermal hot-pressing, *Journal of Nuclear Science and Technology*, 24 (1987) 51-60.
- 601 [54] S. Komarneni, R. Roy, Hydrothermal reaction and dissolution studies of CsAlSi₅O₁₂ in water and brines,
602 *Journal of the American Ceramic Society*, 66 (1983) 471-474.

603 [55] R. Harjula, E. Tusa, R. Koivula, Performance of zeolite, silicotitanate, CsTreat® and SrTreat® ion
604 exchange materials in Fukushima clean up, in: WM2017 Conference, Phoenix, AZ, 2017, pp. 17114.

605 [56] N.C. Hyatt, C.L. Corkhill, M.C. Stennett, R.J. Hand, L.J. Gardner, C.L. Thorpe, The HADES facility for high
606 activity decommissioning engineering & science: Part of the UK national nuclear user facility, IOP
607 Conference Proceedings: Materials Science and Engineering, 818 (2020) 012022.

608