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1 **Combustion - Induced Turbulent Flow Fields in Premixed Flames**

2 D. Bradley^b, M. Lawes^b, M. E. Morsy^{a,b,*}

3 ^aFaculty of Engineering at El-Mattaria, University of Helwan, Cairo 11718, Egypt.

4 ^bInstitute of Thermofluids, School of Mechanical Engineering, University of Leeds, LS2 9JT, UK.

5 *Corresponding author: M_Morsy@m-eng.helwan.edu.eg.

6 **Abstract**

7 Combustion-induced turbulence is studied in explosions of methane/air in a steel sphere with
8 optical access. Rms turbulent velocities, u' , created by four peripheral variable speed fans, were
9 measured by Particle Image Velocimetry, PIV, which indicated near-uniform, isotropic
10 turbulence, with small mean velocities. A near-spherical propagating flame, and the gaseous
11 expansion generated a radially outwards velocity of unburned mixture, the intensity of which
12 depended upon the burning velocity and volume increase due to combustion. The study is to
13 measure any extra turbulence created by this outwards velocity pulse. Only wave lengths less
14 than the flame circumference can wrinkle the flame and increase the burning velocity, u_t .
15 Consequently the effective rms velocity at the flame front affecting its propagation, u'_k , less
16 than u' . Analysis shows, u'_k , to be a function of flame radius. The velocity pulse generated
17 additional turbulence, enhancing u'_k . This enhanced u_t , giving further positive feedback. This
18 higher rms value is designated as a spatial rms turbulent velocity, u'_s . PIV-measured gas
19 velocities are resolved into a mean radial velocity, \bar{U}_r and, u'_s , with their radial profiles. These
20 are derived from explosions at different equivalence ratios, pressures, and temperatures. At the
21 radii at which u_t are measured, u'_s/u'_k is enhanced by the high rates of burning and volumetric
22 expansion. This ratio attained a high value of 2.5, with stoichiometric CH₄/air. Values of u_t
23 measured in explosions are higher than those measured in steady-state burners, attributable to
24 the induced u'_s , enhancing u_t , in explosions, with no such effect in burners.

25 *Keywords: Combustion generated turbulence, Burning velocity, Premixed explosions, Turbulent*
26 *burning.*

27 Nomenclature

\bar{c}	mean reaction progress variable
\bar{k}_η	dimensionless wave number
L	turbulent integral length scale
n_k	number of integral length scales
P	pressure
r_f	flame radius for equal volumes
r_m	maximum flame radius, (=60 mm)
R_λ	Reynolds number, based on the Taylor scale λ
t	time
T_p	burned gas temperature
T_u	initial temperature
S_t	turbulent flame speed
$\bar{S}(\bar{k}_\eta)$	non-dimensional power spectral density
u_l	laminar burning velocity
u_t	turbulent burning velocity
U_r	radial velocity component at each(x, y) grid node
\bar{U}_r	mean radial velocity
\bar{u}_g	mean gas velocity
u'	rms turbulent velocity
u'_k	effective rms turbulent velocity, acting on flame
u'_s	spatial rms turbulent velocity acting on flame
f	fan speed
φ	equivalence ratio
η	Kolmogorov scale
λ	Taylor scale of turbulence
ρ_b	burned gas density
ρ_u	unburned gas density

29 **1. Introduction**

30 Since the early days of combustion science there has been an interest in combustion turbulence, namely
31 the turbulence generated by combustion. Advances in diagnostics, particularly Particle Image
32 Velocimetry, PIV, have greatly facilitated experimental studies of such generation. Vessels with fan-
33 stirred mixing of the contents, that create near-uniform, isotropic turbulence, are often employed to study
34 the effect of turbulence upon chemical reactions and phase changes, and the measurement of turbulent
35 burning velocities [1-3]. Peters [4] has shown that radial flame propagation will change the original
36 cold flow turbulence and Lawes [5] has employed single point Laser Doppler Anemometry, LDA, to
37 measure the velocity of unburned gases ahead of a turbulent flame.

38 However, LDA, unlike PIV, does not provide information on the spatial structure of the flow,
39 comparable to that provided by, PIV, which is able to provide a detailed temporal evolution of the flow
40 velocity at the measurement plane. It can also provide data on the mean velocity, higher-order moments,
41 and frequency spectra, with high accuracy. It has recently been used by the current authors to
42 characterise the cold flow turbulence, in the Leeds fan-stirred vessel, in the absence of chemical
43 reaction. This revealed good levels of uniformity and isotropy [6]. Spherical explosions, as a result of
44 the combined influences of a high burning rate and high volumetric expansion can generate a strong
45 outwards velocity pulse ahead of the flame. The present experimental study focuses on whether this
46 strong velocity pulse of outwards velocity is able to generate additional “combustion turbulence” and,
47 if so, to quantify its magnitude.

48 As will be shown, the technique has been developed further, to characterise the large radial expansion
49 velocities that are generated ahead of the flame by combustion in centrally ignited, radial, explosions,
50 and their interaction with the turbulence created by the fans. Closed vessel explosions, through the
51 associated gaseous expansion, generate a powerful velocity pulse that is related to the rate of
52 combustion and volumetric expansion. Interactions of the high velocity wave further enhance the
53 turbulence, that, in turn, further accelerates the oncoming flame. The development of this interaction is
54 a motivating aspect of the present study.

55 To this end, The paper reports comprehensive velocity measurements in methane/air mixtures, with
 56 initial rms turbulence velocities, u' , of up to 4 m/s and, equivalence ratios, φ , = 0.8, 1.0 and 1.3, at 300
 57 K and 400 K, and pressures of 0.5 and 1.0 MPa. In the measurement of turbulent burning velocity, u_t ,
 58 allowance must be made for the changes in the effective rms turbulence velocity, to which the explosion
 59 flame is exposed [2]. In the earlier stages of a turbulent spherical explosion, the flame surface is
 60 wrinkled only by length scales smaller than the flame circumference. If u' is the cold mixture rms
 61 turbulent velocity, then the effective rms velocity for flame surface wrinkling, u'_k , must be less than
 62 this. The ratio, u'_k/u' is found by integrating the non-dimensional power spectral density, $\bar{S}(\bar{k}_\eta)$, over
 63 the range of relevant wavelengths. Based on an original study of Abdel-Gayed et al. [2], Bradley et al.
 64 [1] derived the ratio u'_k/u' from:

$$\frac{u'_k}{u'} = \left[\frac{15^{0.5}}{R_\lambda} \int_{\bar{k}_{\eta 1}}^{\bar{k}_{\eta 2}} \bar{S}(\bar{k}_\eta) d\bar{k}_\eta \right]^{1/2}, \quad (1)$$

65 where R_λ is the Reynolds number, based on the Taylor scale λ , and $\bar{S}(\bar{k}_\eta)$ is the non-dimensional power
 66 spectral density, expressed in terms of \bar{k}_η , a dimensionless wavenumber, obtained from the
 67 wavenumber multiplied by the Kolmogorov length scale, η . $\bar{S}(\bar{k}_\eta)$ is given by [1]:

$$\bar{S}(\bar{k}_\eta) = \frac{0.01668R_\lambda^{2.5} + 3.74R_\lambda^{0.9} - 70R_\lambda^{-0.1}}{1 + (0.127R_\lambda^{1.5}\bar{k}_\eta)^{5/3} + (1.15R_\lambda^{0.622}\bar{k}_\eta)^4 + (1.27R_\lambda^{0.357}\bar{k}_\eta)^7}, \quad (2)$$

68 The limits $\bar{k}_{\eta 1}$ and $\bar{k}_{\eta 2}$, in Eq. (1) represent the smallest and largest possible wavelengths conveniently
 69 expressed by $n_k L$, where n_k is the number of integral length scales and L is the integral length scale (=
 70 20 mm) [6], as:

$$\bar{k}_{\eta k} = \frac{2\pi\eta}{n_k L} = \left(\frac{32\pi}{15^{0.25}n_k} \right) R_\lambda^{-1.5}. \quad (3)$$

71 The lower limit $\bar{k}_{\eta 1}$, in Eq. (1) is assumed to be the flame diameter, D_f ($= 2r_f$), as it is based on the
 72 maximum wavelength, $n_k L$, that can wrinkle the flame. In the case of explosions, the upper limit
 73 $\bar{k}_{\eta 2}$ depends upon the size of the smallest eddy that can be chemically acting on the flame during its
 74 lifetime. In the present study, the lower limit, $\bar{k}_{\eta 1}$, corresponds to the maximum possible wavelength,
 75 which occurs when the flame approaches the internal diameter of the vessel, namely 380 mm. The upper

76 limit, $\bar{k}_{\eta 2}$, corresponds to the smallest wavelength, taken to be the Kolmogorov scale, η . Consequently,
 77 $n_k L$ in Eq. (4) is η and $\bar{k}_{\eta 2}$ is 2π . Figure 1 shows the development of u'_k/u' with r_f for stoichiometric
 78 CH_4/air at 300 K and 0.1 MPa for three different values of u' . For the present experimental, u' is related
 79 to the fan speed rpm, f , by [6]:

$$u' = 0.00124f \quad (\text{m/s}). \quad (4)$$

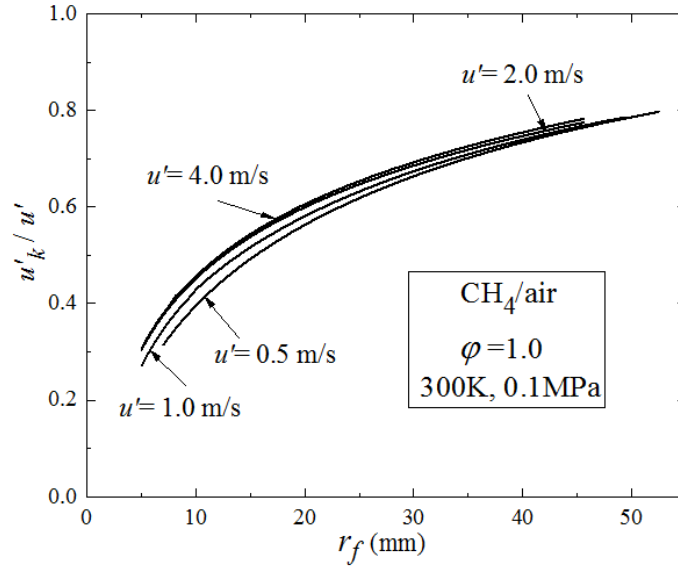


Fig. 1. Development of u'_k/u' with r_f .

81 During an explosion, PIV-measured gas velocities are resolved into a mean radial velocity, \bar{U}_r ,
 82 and, u'_s , the spatially effective rms turbulent velocity. To calculate it from the PIV measurements, a
 83 zone of specified thickness, ~ 1 mm ahead of the flame front, is defined. Within this zone, the radial
 84 velocity profile, surrounding the flame front, is deduced and divided into a number of circumferential
 85 sectors, N_i . The spatial rms turbulent velocity, u'_s , was then calculated for each sector and averaged
 86 over the velocity profile around the flame front from:

$$u'_s(x, y) = \frac{1}{N_i} \sum_{i=1}^{N_i} \left[\sqrt{\left(\frac{1}{N_v} \sum_{v=1}^{N_v} [U_r(x, y) - \bar{u}_g(x, y)]^2 \right)} \right]. \quad (5)$$

87 Here U_r is the radial velocity component at each (x, y) grid node, and \bar{u}_g is the mean gas velocity
 88 within each sector. N_v is the total number of velocity vectors in each sector. Importantly, u'_s is not only
 89 influenced by the spectrum of turbulence but, as will be shown, it is also affected by any turbulence
 90 generated by the velocity field created ahead of the flame by the combustion process.

91 The calculation of $U_r(x, y)$ was executed in three steps, using a series of MATLAB scripts. The first
92 detects the flame front, and converts it into, (x, y) , Cartesian coordinate. The second is to match the
93 flame front coordinates with the nearest unburned gas velocity measurement. The final step is to
94 calculate the radial velocity component, $U_r(x, y)$, from which u'_s is calculated in Section 5. The polar
95 transformation of the velocities starts from the determination of the global centre (x_c, y_c) , which
96 indicates the spark position. The local angle of each velocity, around the flame front, is then calculated
97 from:

$$\theta = \arctan \{ (y - y_c) / (x - x_c) \}, \quad (6)$$

98 with the radial velocity calculated from the velocity components in:

$$U_r(x, y) = u(x, y) \cos(\theta) + v(x, y) \sin(\theta). \quad (7)$$

99 Here a positive value of $U_r(x, y)$ implies an outward direction, $u(x, y)$ is the velocity component in
100 the x -direction and $v(x, y)$ the velocity component in the y -direction.

101 **2. Methodology**

102 Measurements were made in the Leeds fan-stirred vessel of spherical stainless steel, with an inner radius
103 of 190 mm, and three pairs of optically flat quartz windows of 150 mm diameter. These allowed full
104 visualisation of the central region of the vessel and the flame propagation at essentially constant
105 pressure. Each of the four identical fans is powered by an 8 kW three phase electric motor, was located
106 close to the wall of the vessel. The fans were arranged in a regular tetrahedron configuration, in an
107 attempt to optimise homogenous, isotropic turbulence. Their speed was controlled by individual solid
108 state variable frequency convertors, within a control range of 200-10,000 rpm (3.3-176 Hz), in
109 increments of 20-30 rpm. Further details of the vessel and comprehensive characterisation of the non-
110 reacting, single phase, turbulent flow can be found in [6].

111 A high repetition rate double pulsed Nd:YAG laser (DM60-DH, Photonics), generated pulses of 12 mJ
112 at a wavelength of 532 nm at 5 KHz. The laser beam expanded into a vertical sheet of about 1.0 mm
113 thickness, passing through the centre of the vessel. Here it uniformly illuminated the dispersed 1 μ m
114 diameter seeding particles of olive oil, generated by six jet atomisers (9010F0021, DANTEC). The
115 measuring system comprised two spherical lenses of -300 mm and 650 mm focal lengths, and a

116 cylindrical lens of 20 mm focal length. Laser pulses, were synchronized with a high-speed camera
117 perpendicular to the laser sheet, to record a 12-bit image pair of (1024×1024 pixels), under the control
118 of Dantec dynamics studio software. An adaptive algorithm was employed to process images. This
119 algorithm is an iterative and automatic way of calculating velocity vectors, based on the seeding particle
120 density. A minimum interrogation area of (8×8 pixels) and a maximum of (32×32 pixels) were
121 employed, with a magnification ratio of 0.117 mm/pixel. More details of the PIV system and adaptive
122 algorithm appear in [7].

123 It is advisable to image as large an area as possible, in order to ascertain how the flame front propagation
124 develops in its interaction with the turbulent flow field. Bearing in mind the distance to the vessel wall,
125 the window diameter, and the capture angle of the lens, the maximum area that could be physically
126 imaged at the central plane of the vessel was a region 150 mm square. However, due to the finite
127 resolution of the camera (1024×1024 pixels), this would result in poor spatial resolution of the measured
128 velocity fields. It was therefore, necessary to establish the maximum possible spatial resolution of the
129 turbulent structures and their flame interactions, while also preserving information of bulk-flow
130 behaviour.

131 The integral scale of turbulence, L , is about 20 mm [6], indicative of a relatively large scale flow
132 structure, relative to the flame brush thickness. The Taylor microscale, λ , under atmospheric conditions,
133 is respectively, 2.24 mm, 1.53 mm and 0.71 mm, respectively, for u' values of 1, 2 and 4 m/s. The
134 Kolmogorov length scale, η , was calculated to be between 0.18 mm and 0.07 mm in the u' range of 1
135 - 4 m/s. The minimum possible interrogation area size, which could be used in conjunction with the PIV
136 adaptive method without excessive loss in accuracy, was 8 (~0.94 mm) pixels square. This is about 5-
137 12 times larger than η . Clearly, it is not possible to capture the velocity fluctuations associated with η ,
138 whilst also recording the larger scales, between L and λ .

139 Consequently, key characteristics were centred around the integral scale, L , of 20 mm, a value of, u_l ,
140 of 0.358 m/s, for stoichiometric methane/air at atmospheric conditions [8], an inner reaction zone
141 thickness of 0.75 mm and an rms turbulent velocity u' , of between 1 and 4 m/s. Combustion then
142 occurred in the corrugated flamelet region of the Borghi diagram [9]. Here the influence of turbulence

143 scales larger than the flame thickness are the more important. For this reason, an area of interest larger
144 than the integral length scale is embraced, in conjunction with an interrogation area size around the
145 same size as λ . Based on this, a square area of $120 \times 120 \text{ mm}^2$ was selected. The duration of each
146 experiment was about 30 ms, at a frequency of 5 kHz. This ensured capture of turbulent motion in the
147 key range between λ and L , the most controlling influences upon flame structure.

148 **3. Velocity field in explosions**

149 Figure 2 shows the velocity vector maps, measured during explosions of stoichiometric CH_4/air at an
150 initial pressure of 0.1 MPa, and an initial temperature of 300 K with $u' = 1, 2$ and 4 m/s. The same
151 vector colour code, shown on the right of Fig. 2, is used for all values of u' . Flame contours are shown
152 at several elapsed times after ignition. One representative experiment of five is shown, at each value
153 of u' . Such figures show the interaction between the unburned flow field and the flame front. As u'
154 increases, the propagation of the flame changes from a loosely spherical nature, at $u' = 1$ m/s, to one
155 that is more highly deformed and convoluted, at $u' = 4$ m/s. Clearly, the flow structures before each
156 ignition are highly variable, as is the response of the flame front to them, with some sections of the
157 flame initially moving away from the point of ignition. These sections can drag the flame front along
158 with them, giving the appearance of rapid flame propagation in that direction. This is clear with $u' = 4$
159 m/s. In contrast, where the bulk cold flow moves towards the flame, burned gas flame propagation is
160 noticeably arrested. Clearly, the response of the flame to the flow movement, is due to the relative
161 difference between the burning velocity of the mixture and the flow velocity ahead of the flame.

162 The local changes in flow velocity are significantly higher than those in burning velocity. As a result,
163 the flow wrinkles the flame front before a particular flow structure is consumed by the flame. With $u' =$
164 1.0 m/s, the flow velocity is small and the flame front is only slightly wrinkled. As u' increases, the
165 flame is distorted and moved by the flow, with wrinkling and stretching of the flame front, as it departs
166 from its original nearer-spherical nature. For all values of the rms velocity, as the flame propagates, the
167 velocity of the unburned gas ahead of it is being forced outwards, by the expanding burned gases. This
168 phenomenon is most noticeable at $u' = 1.0$ m/s, due to the relatively slow moving flow field structures,
169 but it is still evident at $u' = 4.0$ m/s. This is indicative of the symbiotic relationship between the flow

170 structures contained within the reactants, and the propagating flame front. The flame is affecting the
 171 structure of the flow, and the flow is affecting the structure of the flame.

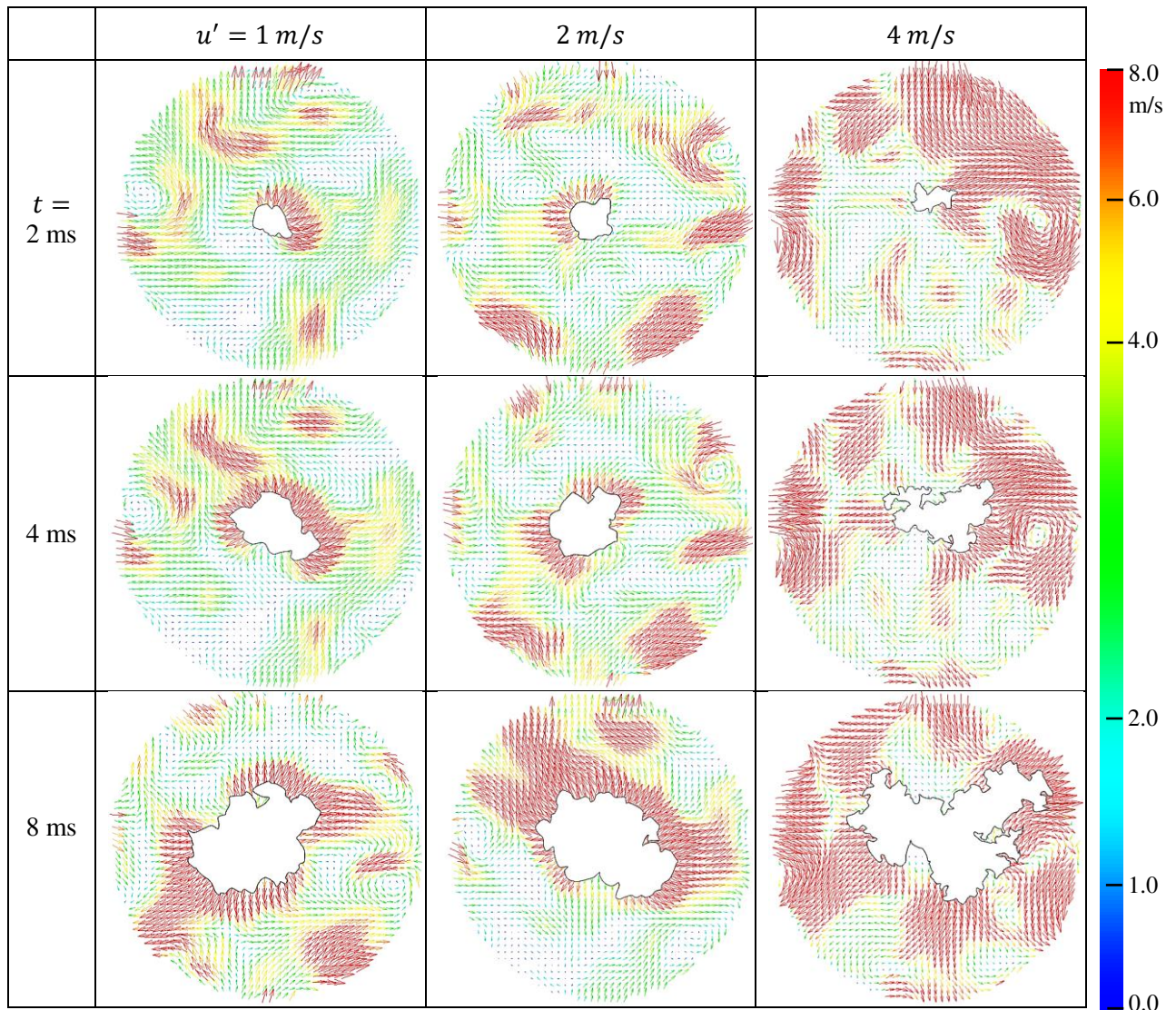


Fig. 2. Development of CH₄/air turbulent flames, with $\phi = 1.0$ at 0.1 MPa and 300 K, for $u' = 1, 2$ and 4 m/s.

172 4. Combustion mean and rms velocities

173 The lower fluctuations in Fig. 3a are those in the local mean radially outwards velocity, U_r , just ahead
 174 of a stoichiometric CH₄/air flame front, at atmospheric pressure at $t = 2.4 \text{ ms}$, after ignition. The small
 175 flame front shows few wrinkles, as it is exposed to but a small part of the full spectrum of turbulence.
 176 This phenomenon is also clearly seen in the velocity vectors fields, in Fig. 2, in which small wrinkles
 177 move faster, and increase the unburned gas exposure significantly. As time passes, the flame front
 178 grows, and the front becomes affected by small to progressively larger scales. This can be seen in Fig.

179 3b, from the increasing the fluctuations of radial velocity, and flame front wrinkling, after 8.6 ms. There
 180 are consequent increases in the turbulent burning velocity.

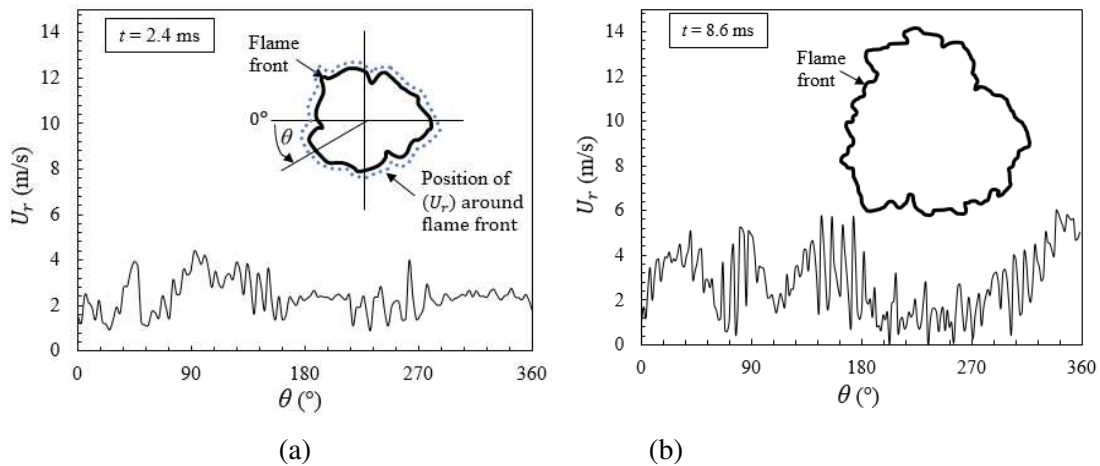


Fig. 3. Local mean radial velocity, U_r , around the flame front, for stoichiometric CH_4/air mixture, $u' = 1.0$ m/s, 300 K and 0.1 MPa, at (a) $t = 2.4$ ms ($r_f = 14$ mm), and (b) $t = 8.6$ ms ($r_f = 30$ mm).

181 The all-important measured radial variations of the mean gas velocities, \bar{U}_r , of the unburned mixture
 182 ahead of the flame radial are shown, at three different times after ignition in Fig. 4. The three times
 183 were 4, 8 and 12 ms, with again, a stoichiometric CH_4/air flame, at atmospheric pressure, and 300 K,
 184 with $u' = 1$ m/s, and gas velocity measurements up to a radius of 60 mm. The local radial
 185 velocity, $U_r(x, y)$, was first identified at each grid node within an annulus area of thickness ~ 1 mm,
 186 around the flame front, and averaged over the entire circumferential area, to yield, \bar{U}_r . The calculation
 187 started at the tip of the leading edge of the flame front, moving radially outwards from there. The
 188 velocity profile before ignition is also shown. As a turbulent flame develops from a point ignition
 189 source, the flame propagation is laminar-like, as shown from the velocity profile at $t = 4$ ms. As the
 190 flame grows, the turbulent flame speed increases, along with \bar{U}_r . The strong velocity pulse that is
 191 generated, moving ahead of the flame is apparent.

192 The corresponding radial rms velocity profiles for the same three time intervals, are shown in Fig. 5.
 193 Values of the rms velocity were calculated for the same annulus areas, moving from the flame tip
 194 towards the window edge. As the flame propagates, the flame front is exposed to an increasing range
 195 of turbulent wave lengths and, as a result, the rms velocity acting on the growing flame front increases.
 196 It might also be anticipated that the strength of the velocity impulse generated ahead of the flame is

197 related to both the rapidity of the combustion, and the magnitude of the associated increase in volume.
 198 Any associated generation of turbulence would augment u'_k , increasing the value of u'_s/u'_k .
 199 Consequently, the influences of changes in ϕ , temperature, and pressure upon u'_s were investigated,
 200 using CH₄/air mixtures.

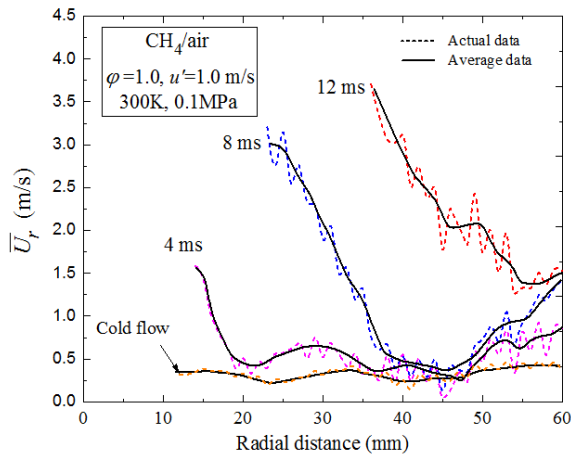


Fig. 4. Variation of mean radial gas velocity, \bar{U}_r with the radial distance.

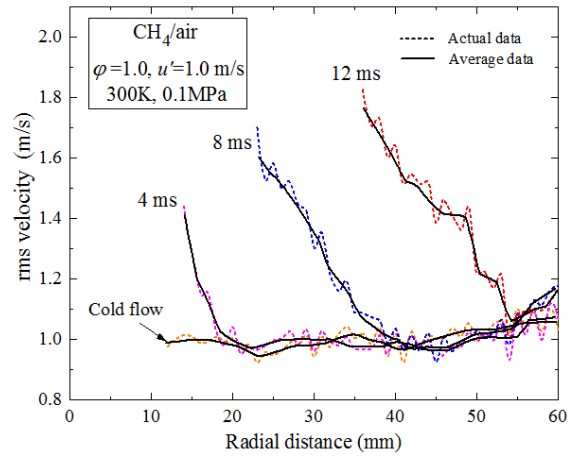


Fig. 5. Variation of spatial rms velocity with the radial distance.

202 To study further the effect of different enhancements of the velocity impulse generated by the flame on
 203 the enhancement of u'_s further, changes in ϕ , temperatures, and pressures of CH₄/air mixtures were
 204 investigated. The results are shown in Figs. 6. and 7. Again this involved the study of radial profiles of
 205 u'_s , this time normalised by u' , plotted against r_f/r_m . In Fig. 6 the vertical line at $r_f/r_m = 0.2$ marks the
 206 limit of the zone within which ignition and its associated reactions occur. Here, there is a transition from
 207 an igniting plasma to a propagating flame, with developing turbulence.

208 This involved the measurement of flame speeds and u'_s/u' as a function of $\phi = 1.0$ and 1.3, temperatures
 209 of 300 and 400 K, and pressures of 0.1 and 0.5 MPa. The PIV measured vectors around the flame front
 210 were processed at each instant during the evolution of the flame, enabling u'_s to be calculated. This was
 211 repeated for $u' = 0.5, 1.0, 2.0$ and 4 m/s. Figs. 6 and 7 cover stoichiometric CH₄/air, at 300 K and 0.1
 212 MPa. In addition, Fig. 6 covers 400 K, 0.1 and also 0.5 MPa, and 300 K. Fig. 7 also covers CH₄/air with
 213 $\phi = 1.3$ at 300 K and 0,1 MPa. Each curve in a figure represents mean values from five explosions. For
 214 all values of u' , the value of u'_s/u' increases with r_f/r_m .

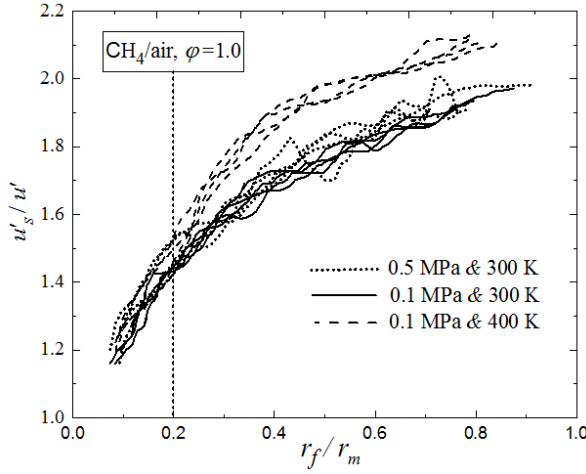


Fig. 6 Influence of pressure and temperature on u'_s .

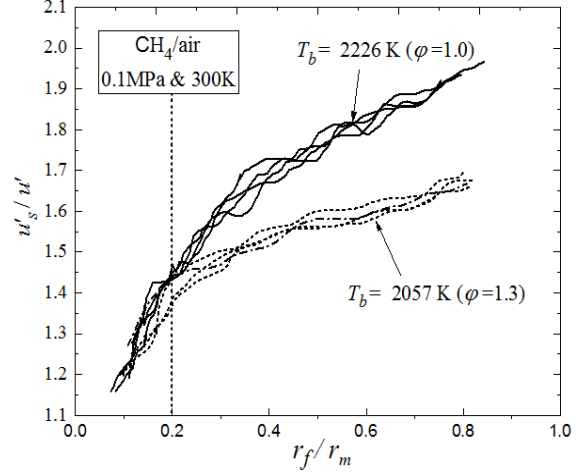


Fig. 7. Influence of equivalence ratio on u'_s . T_b is burned gas temperature.

215 Figure 6 shows little effect of pressure, but at the higher initial temperature of 400 K, higher values of
 216 u'_s/u' develop with increasing radius. In Fig. 7, T_b is the adiabatic temperature of the burned mixture.
 217 The stoichiometric mixture had the higher adiabatic temperature and higher flame speed/. The slower
 218 burning, less expansive, $\phi = 1.3$ mixture, generates the lowest values of u'_s/u' . Both figures confirm
 219 that both a higher burn rate and a higher volume increase u'_s/u' .

220 The overall quantitative findings from Figs. 7 and 8 can be empirically correlated by the following
 221 relationship:

$$u'_s = \left[\frac{1 - 0.49 \ln(r_f/r_m)}{280} \right] \cdot f \cdot \left(\frac{T_u}{T_0} \right)^{0.81} \left(\frac{P}{P_0} \right)^{0.01} \left(\frac{\phi}{\phi_0} \right)^a \quad (8)$$

222 Here r_f is the mean flame radius, f the fan speed in rpm, T_u and P are the initial temperature and pressure,
 223 respectively, $T_0 = 300 \text{ K}$, $P_0 = 0.1 \text{ MPa}$, $\phi_0 = 1.0$. Where $a = 0.36$ for $\phi < 1.0$ and $a = -0.55$ for $\phi >$
 224 1. Eq. (8) can be used to quantify the spatial rms velocity, u'_s , ahead of turbulent methane flames at
 225 pressures, up to 0.5 MPa.

226 5. Turbulence created by the velocity pulse

227 Figs 6 and 7 clearly show u'_s/u' to increase as the flame propagates outwards. The value of u' is
 228 determined solely by the speed of the fans and is an asymptotic value for the flame. The enhanced
 229 turbulence cannot be directly generated solely by the velocity pulse, because, in the absence of fan-

230 generated turbulence, in a laminar explosion, no turbulence is created ahead of the flame. From Figs. 4
 231 and 5 it can be seen that turbulence intensities, measured by u'_s/\bar{U}_r , are at their highest at the smaller
 232 radii. The enhancement of the turbulence would appear to originate directly at the wrinkled flame front,
 233 and be attributable to the existing turbulence beyond that front. In Section 5 it is suggested that a
 234 stronger velocity impulse, arising from both a high burning velocity and a high volumetric expansion
 235 might increase the value of $\frac{u'_s}{u'}$, and this is supported by Figs. 6 and 7. Bearing in mind that u' is constant
 236 during a single explosion these results show u'_s to be increasing by such a mechanism, albeit at a
 237 diminishing rate, throughout the explosion.

238 This view is more directly assessed in Fig. 8., which plots u'_s/u'_k against r_f/r_m , throughout explosions
 239 for a variety of velocity pulses of different strengths. Throughout the explosion, higher values of u'_s/u'_k
 240 are generated by mixtures of higher reactivities. The highest values of u'_s/u'_k are generated by the most
 241 reactive and most expansive mixture, that of stoichiometric CH₄/air at 400 K. and 0.1 MPa. The lowest
 242 values of u'_s/u'_k occur with the least reactive and least expansive mixture, that of CH₄/air, with $\phi = 1.3$
 243 at 300 K and 0.1 MPa. Figs 6 and 7 show u'_s to be increasing throughout the explosion. There is an
 244 interesting interplay between u'_s and u'_k . Fig. 1 shows u'_k to increase throughout the explosion. From
 245 Fig. 8, it is clear that, for these explosions, the increases in u'_k must be greater than those in u'_s . For the
 246 large flame radii ($0.2 > r_f/r_m > 0.7$), u'_s can be correlate with u'_k by:

$$(u'_s/u'_k) = -1.18 (r_f/r_m) + 2.61. \quad (9)$$

247 Hence, the effective rms turbulent burning velocity based on the power spectral density, u'_k , can still be
 248 used with the correction factor proposed in Eq. (9). During the early transition to a propagating flame
 249 up to $r_f/r_m = 0.2$, there is a sharp change in u'_s/u'_k . Later, in the regime where turbulent burning
 250 velocities are measured, the spatial rms turbulent velocity acting on flame is about $2.5 u'_k$, for
 251 stoichiometric CH₄ mixtures, and about 2.2 for mixtures with $\phi = 1.3$.

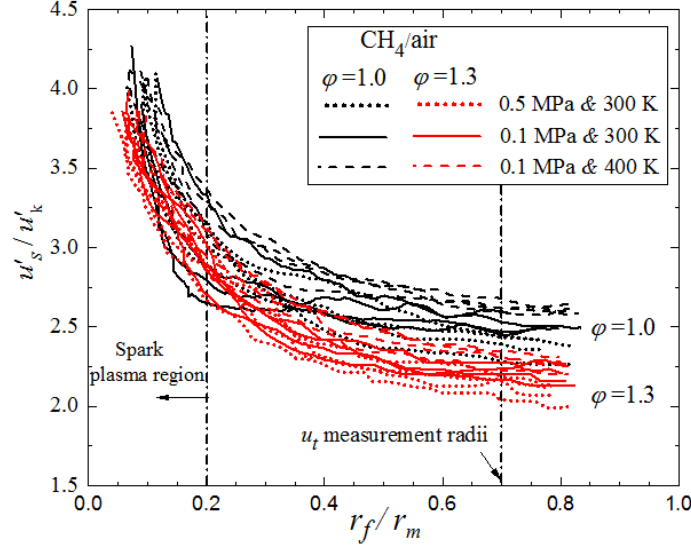


Fig. 8. Variation of u'_s/u'_k with r_f/r_m , for stoichiometric and rich methane.

252 6. Burning velocities: Comparisons with some burner results

253 To be meaningful, a burning velocity, u_t , requires an associated area. A practical rationale for the
 254 selection of such an area is that, when multiplied by the burning velocity and the appropriate density, it
 255 yields the mass burning rate. A convenient approach is to balance the volume of burned gas outside a
 256 spherical surface of radius, r_f , with the volume of unburned gas inside it [10, 11]. In spherical flame
 257 propagation, the mass burned can be regarded as contained within the sphere of radius r_f with a density
 258 ρ_b , and a mass burning rate of $4\pi r_f^2 u_t \rho_u$. Balancing this with the rate of accumulation of burned gas
 259 yields:

$$u_t = (\rho_b/\rho_u) dr_f/dt \quad (10)$$

260 Other surfaces might be selected [12]. For example, standardisation of measurements might be achieved
 261 through a particular value of the reaction progress, \bar{c} . With a spherical flame the surface area is large,
 262 at low \bar{c} , but with a conical flame the surface area is large, at high \bar{c} .

263 As in [11] Mie scattering from very fine particles was employed to obtain sheet images through the
 264 spherical flame balls. From these, areas of burned and unburned gas could be found and, from these, it
 265 was possible to derive the radius r_f . The mass burning rate turbulent velocity, u_t , was found from Eq.
 266 (10), with the density ratio found from [13].

267 Measured values of the variations of turbulent burning velocities with ϕ , for CH₄/air, with $u' = 1\text{ m/s}$, at
 268 300 K and 0.1MPa, from four different sources, are shown in Fig. 9. The bold solid curve shows the
 269 current values, from Eq. (10). The data from [14] and [16] are also from explosion flames, whilst the
 270 lowest values, [15], are from conical flames on cylindrical burners. with the turbulence generated by
 271 upstream by flow through perforated plates. With this steady state configuration there is no strong
 272 velocity pulse to generate further spatial rms turbulent velocities such as u'_s , as is the case with the
 273 explosion flames. The higher values of u_t for the explosion flames in Fig. 9 can be explained by this
 274 mechanism. All the rigs were different and flames would have different flow patterns, and consequently,
 275 different modes of generating and dissipating turbulence.

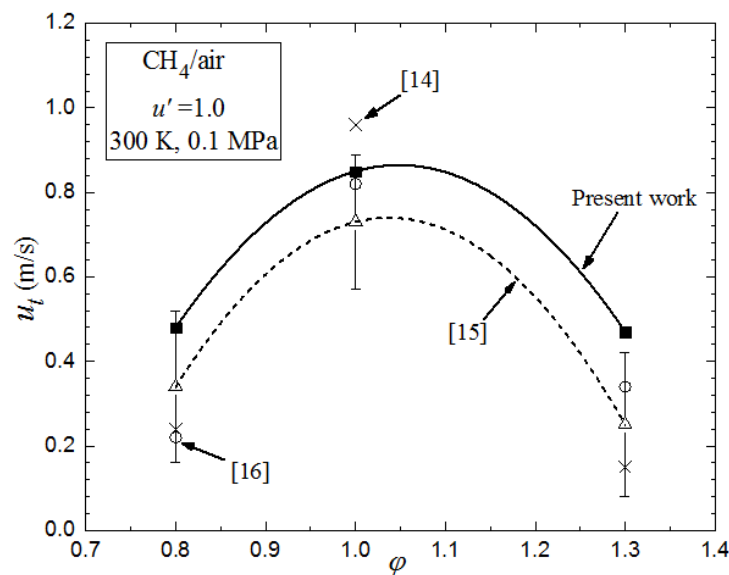


Fig. 9. Variation of u_t with ϕ . Burner measurements [15]. Others are explosions.

276 7. Conclusions

- 277 1. A fan-stirred explosion vessel, with a central region of good uniformity and isotropy has been
 278 employed to measure the mean and rms velocities ahead of explosion flames of CH₄/air.
- 279 2. As the initially small flame kernel grows into the full spectrum of turbulence length scales, on
 280 this count, the effective rms velocity acting on the flame front, u'_k , increases, and this has been
 281 evaluated.
- 282 3. No turbulence generation was observed in explosions in the absence of initial turbulence.

- 283 4. With initial turbulence, the measured turbulence velocity u'_s , just ahead of the flame front
284 increased during the explosion. This is termed the spatial rms turbulent velocity.
- 285 5. Part of the increase in u'_s , is due to the fuller active spectrum of turbulence, u'_k , see Figs. 1 and
286 8, with the remainder arising from further combustion-generated turbulence. Both u'_k and u'_s
287 increase during an explosion, but that in u'_k is the greater.
- 288 6. The existing fan-stirred turbulence at the wrinkled flame front is enhanced by the high
289 expansion velocity induced by combustion beyond that front.
- 290 7. This role of a high expansion velocity is confirmed experimentally, as is its generation by a
291 combination of a high rate of combustion and a high increase in gaseous volume. Higher values
292 of these parameters increase u'_s .
- 293 8. Isotropy and uniformity are difficult to achieve in many of the rigs employed for the
294 measurement of turbulent burning velocities, u_t and the spatial distribution of the turbulence
295 can affect the burning rate.
- 296 9. In Fig. 9 the lowest burning velocities were measured in burners with steady state conical
297 flames, with no impulsive pulse to enhance the turbulence. As a result, explosion flames yielded
298 higher, differing, values, and this is attributed to differences in the generation of u'_s .
- 299 10. The present results suggest that the principal factors enhancing the existing turbulence are a
300 high burning velocity and a high gaseous expansion due to the combustion. In the generation
301 of the turbulence by the velocity pulse, in all cases turbulence was already present. Bearing in
302 mind that turbulent enhancement arises at the flame surface, another possibility is that it might
303 also arise from wrinkling of the flame surface by thermo diffusive instabilities. Evidence for
304 this possibility is provided in [17], which reports unstable mixtures with more negative
305 Markstein numbers, generating Thermo Diffusive and Darius -Landau instabilities. These
306 wrinkled the flames, causing a sudden acceleration in the burning rate and strong oscillations.
307 However, the introduction of fan stirred turbulence reduced this effect as u'/u_l increased.

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