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# Cellulose dissolution and regeneration using a non-aqueous, non-stoichiometric protic ionic liquid system

Laura Berga · Isobel Bruce · Thomas W. J. Nicol · Ashley J. Holding · Noriyuki Isobe · Seishi Shimizu · Adam J. Walker · Joshua E. S. J. Reid

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**Abstract** The solubility of cellulose has been studied as a function of composition in the binary mixture of 1,1,3,3-tetramethylguanidine and propionic acid. In amine-rich compositions, greater quantities of cellulose can be dissolved than in the equimolar composition, a.k.a. the protic ionic liquid [TMGH][OPr]. By applying a methodology of a short period of heating followed by cooling, similar concentrations of cellulose can be achieved in a much shorter time period. Finally, regeneration of cellulose from solution can be

achieved by altering the acid:amine molar ratio. In comparison to cellulose regenerated from these solutions using water as an antisolvent, cellulose regenerated with propionic acid exhibit a lower crystallinity as inferred from x-ray diffractometry, but a greater average molecular weight as inferred from gel permeation chromatography.

**Keywords** Cellulose · Solubility · Protic ionic liquids · Binary mixtures · Solvent effects · XRD

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## Introduction

Ionic liquids (ILs) are a class of materials broadly described as salts which have melting points below 100 °C (Plechkova and Seddon 2008; Hallett and Welton 2011; Austen Angell et al. 2012; Greaves and Drummond 2015). By varying the anion and cation structure, a wide range of properties can be obtained which have led to a number of different applications. Of particular interest is their use as solvents for cellulose processing, as they have been demonstrated to readily dissolve high concentrations of cellulose (Swatloski et al. 2002; Kosan et al. 2008; Wang et al. 2012; Verma et al. 2019). Of the ILs known to dissolve cellulose there are two distinct groups: “aprotic” ILs (AILs) formed of discreet ionic species such as 1-butyl-3-methylimidazolium chloride ([BMIm][Cl]) (Pinkert et al. 2009; Hallett and Welton 2011; Petkovic et al. 2011) and “protic” ILs (PILs) formed from the proton transfer reaction between a Brønsted acid and base such as 1,1,3,3-tetramethylguanidinium propionate ([TMGH][OPr]) (Walker 2004; King et al. 2011; Hauru et al. 2012; Greaves and Drummond 2015; Meenatchi et al. 2017; Becherini et al. 2019). Ionic liquids in mixtures with dipolar aprotic solvents such as dimethyl sulfoxide,  $\gamma$ -valerolactone and 1-methylimidazole have also been shown to solubilize cellulose quite readily (Xu et al. 2013; Zhao et al. 2013; Gale et al. 2016; Holding et al. 2017), which has greatly enabled the spinning of cellulose fibers using ionic liquids (Hauru et al. 2014; Sixta et al. 2015; Ma et al. 2019). Spinning of fibres requires extrusion of highly viscous cellulose solution into a coagulant bath (Hauru et al. 2014, 2016; Sixta et al. 2015). There the cellulose undergoes regeneration (Medronho and Lindman 2015), which uses antisolvent to induce precipitation (Lindman et al. 2017). Hence, solvents mix with anti-solvent in the process.

The reality of an industrial application of an IL as a solvent for cellulose processing is greatly limited by certain obstacles, typically (1) the number of synthesis steps and ultimately the cost to manufacture the IL (Clark and Tavener 2007; Jessop 2011; George et al. 2015), (2) the potential hazards to both operators and the environment posed by the IL such as toxicity, biodegradability and mutagenicity (Docherty et al. 2006; Jordan and Gathergood 2015; Reid et al. 2015; Clarke et al. 2018) and (3) the purification of the IL from its mixtures with other solvents, such as

antisolvents used to regenerate cellulose from its solution (Seddon et al. 2000). In general, PILs address the first of these points as they can be prepared for much lower costs than AILs due to their straightforward preparation (George et al. 2015). Paired with the suggested low microbial toxicity and biodegradability of PILs with the 1,1,3,3-tetramethylguanidinium cation (Pratap Singh et al. 2017) and carboxylic anions (Reid et al. 2018) the use of PIL systems such as [TMGH][OPr] for cellulose processing has clear advantages over their AIL counterparts.

The separation of antisolvent from IL remains a common problem in both PIL and AIL based cellulose dissolution processes. For example, small quantities of water significantly reduces the ability for AILs and PILs to dissolve cellulose (Mazza et al. 2009; Hauru et al. 2012). The complete separation of water from ILs is very challenging, due in a large part to water becoming more and more discrete at diminishing concentrations in ILs (Reid et al. 2017b). Additionally, it has recently been shown that many superbases including TMG are susceptible to hydrolysis in aqueous mixtures, raising concern over the applicability of water as an antisolvent for TMG-based cellulose/PIL solutions (Hyde et al. 2019). The use of alternative antisolvents such as compressed CO<sub>2</sub> show a potentially facile separation of antisolvent from IL, yet the processing costs of high pressure CO<sub>2</sub> in general make their applicability less feasible (Sun et al. 2014). A range of molecular solvents including (but not limited to) acetone, ethanol and dimethyl sulfoxide, have also been employed to regenerate cellulose from ionic liquid solutions (Gupta et al. 2013; Huo et al. 2013; Holding et al. 2014, 2017).

One potential solution to antisolvent separation from a PIL may lie in exploiting the nature of PILs as binary mixtures of a Brønsted acid and base. We have recently shown that changing the stoichiometry in a binary mixture of acetic acid and *N,N*-dimethylethanolamine has a profound effect on the apparent solvent–solute interactions (Reid et al. 2019). Applying that same methodology to the system of propionic acid (HOPr) and 1,1,3,3-tetramethylguanidine (TMG), we show how changing the composition can lead to an increase in cellulose solubility, as well as a means of regenerating cellulose from solution without the need of a dedicated antisolvent.

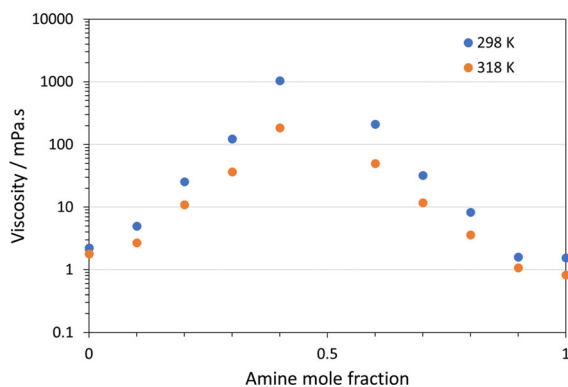
## Results and discussion

### Viscosity of binary mixtures of 1,1,3,3-tetramethylguanidine and propionic acid

Prior to performing the trials of cellulose dissolution, we wanted to characterise the viscosity of the mixtures, as it is an important property for their application as solvents (Marcus 1998; Reid et al. 2017a). Unfortunately, due to the high melting point of the equimolar PIL, we were unable to accurately measure its viscosity within the operating temperatures of our equipment. For all other mixtures and the pure TMG and PrOH we successfully recorded the viscosity as a function of temperature between 298.15 K and 318.15 K (Fig. 1). Generally speaking, we find that the acid-rich compositions have greater viscosities than the corresponding amine rich mixtures, with the 0.4 Amine mole fraction mixture exhibiting the highest viscosities of all the mixtures studied in this temperature range.

### Dissolution of cellulose

The solubility of cellulose in a binary mixture of HOPr and TMG is significantly affected by the solvent mixture composition. We have found that microcrystalline cellulose (MCC) is completely insoluble in all acid rich compositions of these mixtures, as well as the pure precursor materials. Dissolution was confirmed using microscopy to observe any undissolved crystals of the cellulose which could not be observed by the human eye. Surprisingly, the solubility of cellulose



**Fig. 1** Viscosity of binary mixtures of HOPr and TMG as a function of amine mole fraction at 298 and 318 K. The full set of experimental data can be found in the supporting information

was greater in the 60:40 molar ratio mixture of TMG and HOPr (12.5 wt%) than in the equimolar system (10 wt%). Furthermore, the 70:30 molar ratio mixture could dissolve a large concentration of MCC (7.5 wt%) but higher molar ratios of TMG to HOPr could not dissolve MCC.

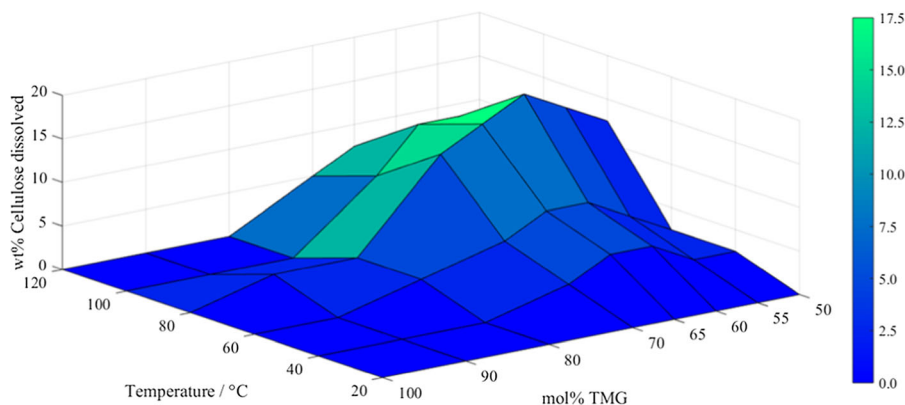
That an amine-rich composition of TMG-HOPr can dissolve a greater quantity of cellulose than the equimolar composition is likely due to the increased hydrogen bond basicity of the binary mixture. Certainly, it is well understood that a balance of hydrogen bond basicity and hydrogen bond acidity plays an active role in cellulose solubility (Hauru et al. 2012; Parviainen et al. 2013). It is likely that a combination of the propionate anion and neutral TMG result in an increase in cellulose solubility. To explore this hypothesis further, the temperature dependence of cellulose solubility was also studied, as varying the temperature can significantly affect the proton transfer equilibrium in acid–base binary mixtures (Abbott et al. 2018).

We found that cellulose solubility under isothermal conditions is also highly dependent on temperature as well as on composition (Fig. 2). By raising the temperature from 20 °C to 120 °C, we find the optimum temperature to be 80 °C for all systems. Above this temperature, cellulose solubility decreases due probably to a shift in the proton transfer equilibrium, resulting in the formation of neutral species with subsequently lower hydrogen bond basicity (Reid et al. 2017a).

Typically, the PIL [TMGH][OPr] has a melting point of around 63 °C (King et al. 2011), yet the solvent appeared stable even at 40 °C with gradual cooling, demonstrating supercooling common in PILs (Angell et al. 2007). However the amine-rich mixtures, which were liquid at all temperatures studied, were able to dissolve more cellulose at lower temperatures as well (Fig. 2).

We also explored the solubility of cellulose in the 55% and 65% molar percentage of TMG mixtures and find a smooth trend in composition dependence on cellulose solubility, with 60% molar percentage of TMG having the greatest cellulose solubility (Fig. 2). When held under isothermal conditions at 80 °C for 15 h, the maximum concentration of MCC we could obtain was 17.5 wt%.

A chance discovery during this work was that after a short period of heating, followed by subsequent



**Fig. 2** Dependence of composition and temperature in the TMG-HOPr binary mixture on the solubility of cellulose after 15 h under isothermal conditions

cooling to room temperature, it was possible to obtain cellulose solutions in a much shorter period of time than previously believed. From this, we pursued a systematic study on heating systems at two temperatures (80 °C and 100 °C) for a set period of time (2 h), followed by removing from the vial block to cool to room temperature (Table 1). As a control, samples of each TMG-HOPr mixture screened were heated for 2 h at 100 °C and analysed using  $^1\text{H}$  NMR to confirm that the compositions of each mixture had not changed during the solubility screening tests (See supporting information Figures S1 to S8).

This method of cellulose dissolution resulted in a greater solubility of cellulose in each of the four compositions (50%, 55%, 60% and 65% TMG) at either temperature compared to isothermal conditions over 15 h (Table 1). For the 50%, 55% and 65% TMG systems, a greater amount of cellulose could be dissolved when heated at 80 °C compared to 100 °C, with the 65% TMG system having the same maximum observed cellulose solubility under both conditions. The maximum concentration of MCC obtained using this method, 20 wt%, was achieved using the 55% and 60% TMG mixtures after a total time of 3 h. As expected, these high concentration cellulose solutions had an appearance that was more gel-like as opposed to a free flowing solution; with better mixing technology it may even be possible to obtain greater cellulose solubilities in the 55% and 60% TMG mixtures. While there was the development of a yellow colour to some cellulose solutions in both methods of dissolution, there was no discernible trend on the formation of this

solution colour with cellulose concentration, acid-amine ratio or duration of the heating condition.

Why this cooling step, along with the temperature of heating, is important towards cellulose solubilisation is not straightforward. While the ionic nature certainly plays an important role in the mechanism of cellulose solubilisation, the thermodynamics and kinetics of this heat/cool dissolution process when compared to isothermal conditions requires further experimental and theoretical investigation, which is currently underway in our laboratory.

The increase in solubility with temperature can be explained through the temperature dependence of cellulose disentanglement and decrystallisation (Ghasemi et al. 2017a). Free energy of mixing is touted as an overarching driving force of dissolution (Lindman et al. 2017). The physical processes within the cellulose dissolution mechanism that most closely correspond to this driving force are solvent diffusivity and chain disentanglement (Ghasemi et al. 2017a, b). Ghasemi et al. have shown that solvent diffusivity and chain disentanglement predominantly affect swelling and dissolution, respectively. In order for cellulose molecules to remain in solution after disentanglement, they must be stabilised in solution. In cellobiose and other short chain cellulose molecules, the molecular interactions which provide this stabilisation consist of “charging up” caused by ion accumulation around the molecule in solution (Medronho and Lindman 2015; Bialik et al. 2016; Nicol et al. 2017). These molecular interactions could be present in cellulose. In fact, ion accumulation has been observed in simulation studies of ILs; [Bmim]Cl shows anion accumulation around

**Table 1** Solubility of cellulose (displayed in weight percentage of cellulose in final solution) as a result of heating at 80 °C (blue) and 100 °C (orange) for 2 h followed by subsequent cooling

Cooling time / minutes	50% TMG / wt%	55% TMG / wt%	60% TMG / wt%	65% TMG / wt%
0	7.5	7.5	7.5	7.5
10	10.0	12.5	12.5	10.0
20	15.0	15.0	17.5	15.0
30	15.0	15.0	17.5	15.0
45	15.0	15.0	17.5	15.0
60	17.5	20.0	20.0	17.5
75	17.5	20.0	20.0	17.5
90	17.5	20.0	20.0	17.5
105	17.5	20.0	20.0	17.5
120	17.5	20.0	20.0	17.5
0	7.5	7.5	7.5	7.5
10	7.5	10.0	10.0	7.5
20	7.5	12.5	12.5	10.0
30	10.0	12.5	12.5	12.5
45	12.5	12.5	12.5	12.5
60	12.5	15.0	15.0	15.0
75	15.0	15.0	15.0	15.0
90	15.0	15.0	15.0	15.0
105	15.0	15.0	15.0	15.0
120	15.0	17.5	17.5	17.5

cellulose as a stabilisation interaction within the IL (Gross et al. 2011). By lowering the temperature of the system, the proton exchange equilibrium will be shifted towards ionic species over neutral species, which in turn would promote greater ion accumulation around cellulose and thus stabilise the cellulose in solution (Reid et al. 2017a; Abbott et al. 2018).

### Regeneration of cellulose

The nil solubility of cellulose in the acid-rich compositions of the TMG-HOPr systems inspires the use of propionic acid as an alternative antisolvent (AS) to water which is commonly used for the same purpose. The separation of excess HOPr from an acid-rich

composition of TMG-HOPr is expected to be more straightforward than the separation of water from the PIL, due to the non-zero volatility of the binary mixtures in this study. The equimolar protic ionic liquid, [TMGH][OPr] has already been shown to be readily distillable using high temperature and high vacuum. (King et al. 2011) We attempted to distil an acid-rich mixture of TMG and HOPr and found that we were able to distil pure propionic acid from this acid-rich mixture, indicating the practical applicability of this method. However, we soon realised that to properly assess the feasibility of solvent recovery from this mixture will require a more in-depth study of the vapour-liquid equilibria of this binary mixture, which is beyond the scope of this paper. We hope to address this topic in a future publication.

We have demonstrated that propionic acid can indeed act as an effective antisolvent for cellulose. By injecting a 15 wt% solution of cellulose at 80 °C into a precipitation bath at the same temperature using a homogenizer, we were successful in regenerating cellulose as a white, granular powder. The material was then subsequently washed further using the same antisolvent, before being dried using acetone to remove residual TMG and HOPr. When comparing cellulose solutions using 50 mol% TMG and 60 mol% TMG, the regeneration process was effectively identical. To compare on the quality of regenerated cellulose, water was used as a reference antisolvent.

To verify the effects of our regeneration process on the molecular weight and polydispersity of cellulose, we performed gel permeation chromatography (GPC), X-ray diffractometry (XRD), thermogravimetric analysis (TGA) and infrared spectroscopy (FT-IR).

From GPC measurements, we have found that all regenerated samples have reduced degree of polymerisation,  $DP_n$  and  $DP_w$ , than the reference MCC. Furthermore, samples regenerated from 50% TMG solutions exhibited lower polydispersity,  $D$ , and a greater  $DP_n$  and  $DP_w$  than from the 60% TMG solutions (Table 2). Also, regenerating cellulose using PrOH results in higher  $DP_n$  and  $DP_w$  than compared to using  $H_2O$ , however the polydispersity of regenerated cellulose increases regardless of the regeneration solvent used. (Table 2). From this, we can see that both the stoichiometry of the dissolution media and the choice of antisolvent can have an impact on the properties of the regenerated cellulose polymer chain lengths. Regarding antisolvent, it is well known that



cellulose can undergo hydrolysis in water, most often in acidic conditions. (Vanhatalo and Dahl 2014) It is therefore likely that by combining water with this cellulose solution during regeneration, hydrolysis of the cellulose takes place. By using PrOH in place of water as the antisolvent, this mechanism of cellulose molecular weight reduction is avoided, hence the observed trends in  $DP_n$  and  $DP_w$ .

These differences due to the choice of antisolvent also affect the thermal degradation behaviour. TGA analysis initially showed that the choice of antisolvent resulted in a slightly different decomposition of cellulose (Fig. 3), which is more apparent when considering the differential of thermogravimetric (DTG) curve (Fig. 4). The DTG curves of each sample showed a maxima rate of loss for volatiles for all regenerated samples at approximately 75 °C. This temperature region is consistent with the boiling point of acetone (56 °C) as oppose to 1,1,3,3-tetramethylguanidine (160–162 °C) or propionic acid (141 °C). The DTG curve showed the maxima rate of mass loss on decomposition to be dependent on the regeneration solvent and not the composition of the dissolution solvent. Furthermore, all regenerated cellulose materials underwent decomposition at lower temperatures than the reference MCC material. This is most likely due to a change in the crystalline allomorph and crystallinity of the cellulose as a result of dissolution and regeneration. (Kilpeläinen et al. 2007; Wang et al. 2013).

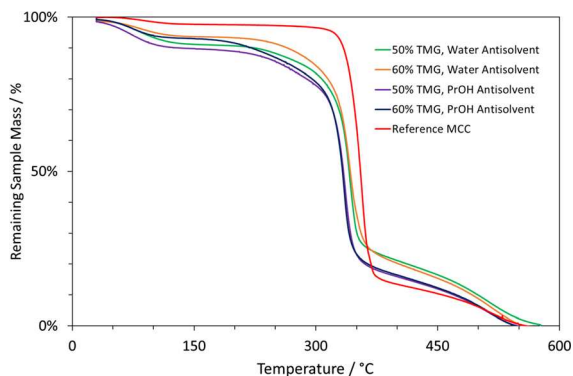
The change of cellulose crystalline allomorph as it undergoes dissolution and regeneration is a well-understood phenomena (Kilpeläinen et al. 2007; Ciolacu et al. 2011). By performing XRD analysis of the regenerated cellulose materials and the precursor microcrystalline cellulose, we demonstrate that cellulose has undergone a change in crystalline allomorph

from cellulose I to II through our process steps (Fig. 5). Specifically, the presence of major peaks at a  $2\theta$  scattering angle of approximately 15°, 20° and 22.5° in the MCC sample, consistent with the crystal structure of cellulose I (Nishiyama et al. 2002; French 2014; Liu et al. 2015), are absent in all of the regenerated cellulose samples, regardless of the regeneration antisolvent used. The types of antisolvent had a great impact on the crystallinity of the regenerated materials. The cellulose materials regenerated with water showed typical profiles of cellulose II (Langan et al. 2001; Ciolacu et al. 2011; French 2014; Liu et al. 2015), whereas regeneration using propionic acid results in amorphous structure as evidenced by the absence of clear peaks in the scattering profiles. This picture is consistent with the observed differences in the DTG and TGA curves.

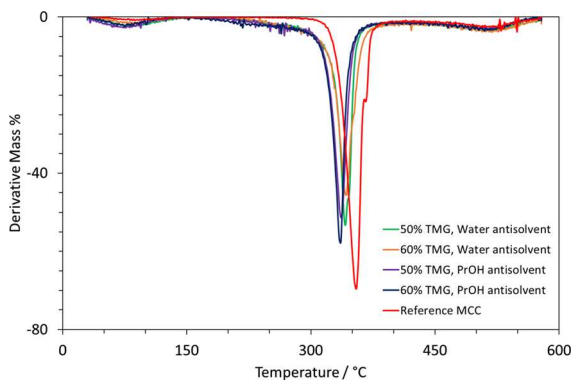
Infrared spectroscopy is often employed as a complementary technique for XRD analysis. The change in crystalline allomorph and crystallinity can be captured with the peak shape and position in the FT-IR spectra due to the difference in hydrogen bonding network between cellulose I and II, specifically in the 3000–3500  $\text{cm}^{-1}$  region, where the information on the O–H groups are included (Marrinan and Mann 1956; Carrillo et al. 2004; Makarem et al. 2019). The MCC showed typical spectra of cellulose I as evidenced by the two sharp peaks at 3400 and 3350  $\text{cm}^{-1}$  (Marrinan and Mann 1956; Carrillo et al. 2004; Makarem et al. 2019). The samples regenerated by water showed two striking peaks at 3490 and 3450  $\text{cm}^{-1}$  that correspond to the intramolecular hydrogen bonds in cellulose II crystal (Marrinan and Mann 1956; Carrillo et al. 2004; Makarem et al. 2019), indicating that the samples regenerated by water had crystalline cellulose II structure. However, these peaks were not observed in the samples regenerated from propionic acid,

**Table 2** Gel Permeation Chromatography (GPC) analysis of the regenerated cellulose materials and the reference starting material, MCC

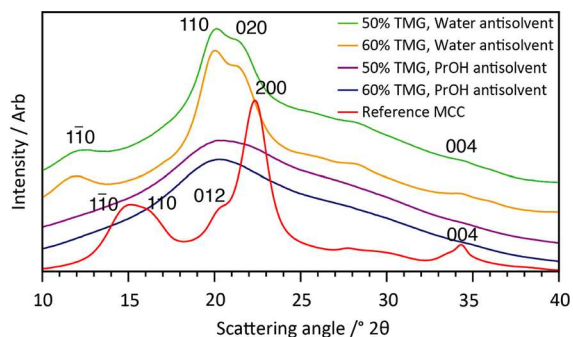
Sample	Polydispersity (D)	$DP_n$	$DP_w$
Reference MCC	1.41	97 ± 5	137 ± 10
50% TMG, PrOH AS	1.58	82 ± 5	135 ± 10
60% TMG, PrOH AS	1.75	71 ± 4	124 ± 8
50% TMG, H <sub>2</sub> O AS	1.56	77 ± 4	120 ± 9
60% TMG, H <sub>2</sub> O AS	1.68	58 ± 5	94 ± 8



**Fig. 3** TGA thermograms of the recovered cellulose materials and reference microcrystalline cellulose. Individual thermograms of each sample can be located in the supporting information



**Fig. 4** DTG thermograms of the recovered cellulose materials and reference microcrystalline cellulose. Individual thermograms of each sample can be located in the supporting information



**Fig. 5** XRD scattering of the recovered cellulose materials and reference microcrystalline cellulose with assignment of peaks to their corresponding polymorph of cellulose (Langan et al. 2001; Nishiyama et al. 2002)

reflecting the amorphous structure. This results further reinforces the structural difference observed in XRD analysis. Additionally, there is a noticeable additional peak around  $1600\text{ cm}^{-1}$  for the regenerated cellulose samples which is not present in the MCC sample. This is most likely due to residual acetone on each regenerated sample as shown by the DTG data (Figs. 4, 6).

## Conclusions

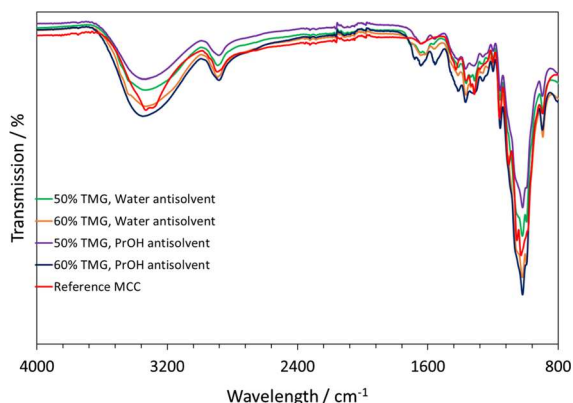
To summarise, the dissolution of cellulose has been shown to not be limited to the equimolar composition of 1,1,3,3-tetramethylguanidine and propionic acid; we have found new maximum solubilities of microcrystalline cellulose in a 60:40 molar ratio of the Brønsted base and acid, respectively. By employing a short heating period with a gradual cooling period, up to 20 wt% MCC solution can be obtained within 3 h of processing. In addition, exploiting the antisolvent nature of propionic acid, cellulose can be regenerated from these solutions by altering the acid–base ratio towards an acid-rich composition, making additional antisolvent such as water entirely redundant. Thus, our novel solvent media, dissolution conditions and the choice of antisolvent provides a new strategy towards the processing of cellulose in acid–base binary mixtures.

## Experimental section

Propionic acid (HOPr), 1,1,3,3-tetramethylguanidine (TMG) and microcrystalline cellulose (MCC) were purchased from Sigma Aldrich and used without further purification.

*Typical cellulose solubility experiments* the required amount of TMG was charged into a 20 ml scintillation vial, with propionic acid being slowly titrated into the vial with stirring within a fume cupboard to produce the binary mixture. The mixture is sealed in the vial and placed onto a heating block, ensuring there are no cold spots on the reaction vial. The mixture is then brought to temperature and MCC is added, producing a final mass of solution of 10 g. Dissolution is confirmed by 1) visual inspection of the solution turbidity and 2) microscope image at  $40\times$  magnification of the cellulose solution to





**Fig. 6** Infrared spectra of the recovered cellulose materials and reference microcrystalline cellulose. Individual spectra of each sample can be located in the supporting information

confirm whether any undissolved MCC can be observed. Cellulose solubility was tested in intervals of 2.5 wt% of the total solution.

**Typical regeneration experiment** cellulose solution (approximately 8 g) at 80 °C was transferred to a 20 ml syringe, where it was then injected into a precipitation solution (approximately 25 g) at 80 °C with constant high shear mixing from a homogenizer. Once all cellulose solution has been injected, the solution was homogenized for 10 min to ensure complete precipitation has taken place, producing a suspension of cellulose in acid-rich binary mixture/acid-amine-water tertiary mixture. The solution was then vacuum filtered and washed with a further 2 × 25 g of antisolvent before being left to dry under vacuum for 1 h. Samples were then suspended in acetone (approximately 20 g) at room temperature before being dried under vacuum for a further 2 h.

**Gel permeation chromatography** The method outlined is similar to the method used by Silbermann. (Silbermann et al. 2017) The sample, (approximately 0.03 g) was swollen overnight in DMSO. The solvent was then exchanged for DMAc by rinsing × 3 with the solvent over vacuum. The solvent-wet sample was placed in 3 ml of 8.7 w/v% DMAc/LiCl and stirred overnight at room temperature. 0.2 ml of the sample was diluted with 1.9 ml pure DMAc and filtered through a 0.2 μm PTFE syringe filter into an autosampler vial, prior to injection. The GPC samples were run on a PSS SECURITY system (Agilent 1260 Infinity II) with a SLS 7100 MALLS detector and RI detection for determination of slice concentration, with 2 × PSS

GRAM Columns and 1 Pre-Column. Flow rate was 1.0 ml/min, injection volume was 20 μL and the resulting MMD was calculated using the PSS Injected Mass method in WinGPC, using the accurate concentration and on-line determination of  $dn/dc$ , assuming that the entire sample mass had eluted. Results are an average of 3 injections, with the standard deviation of the values used to represent the margin of error in the samples.

**Thermogravimetric analysis** Samples were analysed using a PerkinElmer TGA4000 instrument. Approximately 10 mg of material was used for each analysis. Each sample was heated at 20 °C min<sup>-1</sup> from 30 °C to 600 °C under air. Differential of the thermogravimetric curve was calculated using Pyris software.

**X-Ray Diffraction** Sample measurements were performed using a Samples measurements were carried out by the use of a flat-plate vacuum camera mounted on a rotating anode X-ray generator (Rigaku MircoMax-007HF). The diffraction patterns were recorded at room temperature with Ni-filtered Cu K $\alpha$  radiation source ( $\lambda = 1.5432 \text{ \AA}$ , 40 kV, 30 mA) and Fuji imaging plates (IPs). The sample-to-IP distance was calibrated by the use of NaF powder ( $d = 0.23166 \text{ nm}$ ).

**Infrared Spectroscopy** Samples were analysed using a PerkinElmer Spectrum 2 FT-IR Spectrometer with an ATR attachment. All samples were measured at 293 K. Spectra recorded are the average of 16 scans in the region 4000 – 800 cm<sup>-1</sup>.

**<sup>1</sup>H NMR Spectroscopy:** Samples were analysed in D<sub>2</sub>O using a Bruker 400 MHz Ultrashield Plus spectrometer with a BBFO probe. All samples were measured at 298.2 K.

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