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Article

Understanding How the Rate of C−H Bond Cleavage Affects Formate Oxidation Catalysis by a Mo-Dependent Formate Dehydrogenase

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ABSTRACT: Metal-dependent formate dehydrogenases (FDHs) catalyze the reversible conversion of formate into CO_2, a proton, and two electrons. Kinetic studies of FDHs provide key insights into their mechanism of catalysis, relevant as a guide for the development of efficient electrocatalysts for formate oxidation as well as for CO_2 capture and utilization. Here, we identify and explain the kinetic isotope effect (KIE) observed for the oxidation of formate and deuterioformate by the Mo-containing FDH from *Escherichia coli* using three different techniques: steady-state solution kinetic assays, protein film electrochemistry (PFE), and pre-steady-state stopped-flow methods. For each technique, the Mo center of FDH is reoxidized at a different rate following formate oxidation, significantly affecting the observed kinetic behavior and providing three different viewpoints on the KIE. Steady-state turnover in solution, using an artificial electron acceptor, is kinetically limited by diffusional intermolecular electron transfer, masking the KIE. In contrast, interfacial electron transfer in PFE is fast, lifting the electron-transfer rate limitation and manifesting a KIE of 2.44. Pre-steady-state analyses using stopped-flow spectroscopy revealed a KIE of 3 that can be assigned to the C−H bond cleavage step during formate oxidation. We formalize our understanding of FDH catalysis by fitting all the data to a single kinetic model, recreating the condition-dependent shift in rate-limitation of FDH catalysis between active-site chemical catalysis and regenerative electron transfer. Furthermore, our model predicts the steady-state and time-dependent concentrations of catalytic intermediates, providing a valuable framework for the design of future mechanistic experiments.
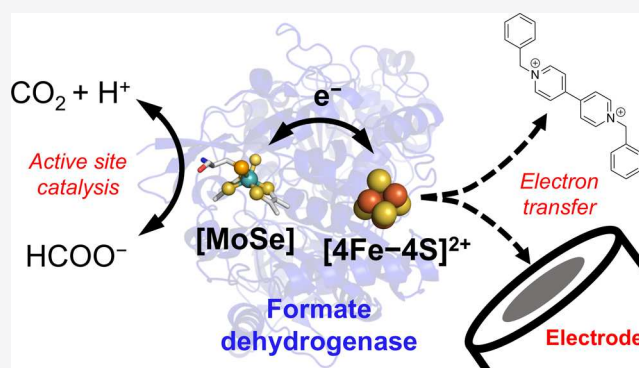
INTRODUCTION

Metal-dependent formate dehydrogenases (FDHs) are paradigm electrocatalysts for the interconversion of CO_2 and formate,[1,2] and play a versatile range of roles in biological systems.[3] The FDHs from several organisms, including *Desulfovibrio desulfuricans*,[4] *Rhodobacter capsulatus*,[5] *Cupriavidus necator* (formerly *Ralstonia eutropha*),[6] *Escherichia coli*,[2] *Syntrophobacter fumaroxidans*,[1,7] *Acetobacterium woodi*,[8] *Methylobacterium extorquens*,[9] *Rhodobacter aestuarii*,[10] and *Methanococcus maripaludis*,[11] have all been reported to catalyze both formate oxidation and CO_2 reduction in assays using solution electron donors/acceptors, although their relative rates of CO_2 reduction vary widely. The enzymes from *S. fumaroxidans*, *D. vulgaris* Hildenborough, and *E. coli*, which are the W-dependent FDHs *Sf*FDH1[1] and *Dv*FDH[12,13] and the Mo-dependent *Ec*FDH-H,[2] respectively, have further been shown to perform thermodynamically reversible (efficient) reduction of CO_2 to formate when immobilized on electrodes. In this case, the driving force for electron transfer to and from the enzyme active site to support catalysis is controlled by the electrode potential, and much greater rates of turnover can be

achieved than in solution, particularly for CO_2 reduction. Recently, the high activity of FDHs has motivated their incorporation into colloidal and electrochemical devices capable of efficient light-driven CO_2 reduction,[12−16] into enzymatic formate fuel cells,[17] and into semi-artificial mimics of formate hydrogenlyase systems.[18] These systems often function with high thermodynamic efficiency, enabled by FDH electrocatalysis.

Although FDHs provide an excellent opportunity to define an efficient mechanism for CO_2 activation and reduction, as well as for the reverse formate oxidation reaction, their mechanisms remain only poorly understood.[19] Several X-ray crystal structures of the oxidized states of Mo/W-containing FDHs have been described.[20−24] All show the active site
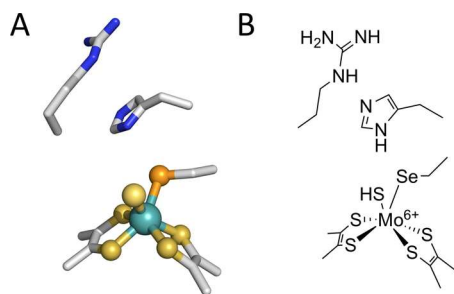
Figure 1. Active site of metal-dependent formate dehydrogenases. (A) X-ray crystal structure of the oxidized active site of EcFDH-N (PDB number: 1KQF).[20] (B) Schematic reproduction of (A).

(Figure 1), consisting of a central Mo or W ion coordinated by two pterin (dithiolene) cofactors, adjacent to an iron−sulfur cluster that collects or delivers electrons (via single-electron transfer) to couple catalysis at the Mo/W site to a partner reaction (for example, $NAD^+/NADH$ interconversion or quinone reduction) at a separate site. The Mo/W is also coordinated by a terminal sulfido group[22,25,26] and a selenocysteine (Sec)[27] or cysteine (Cys)[5] residue. Conserved arginine (Arg) and histidine (His) residues are present in the outer coordination sphere. The roles of the Sec (or Cys), His, and Arg residues in catalysis have not yet been confirmed, but they are probably involved in proton transfer and/or stabilizing substrates and intermediates.

A central question in FDH catalysis is whether the Sec remains coordinated to the metal center throughout catalysis[6] or whether it dissociates to provide a vacant site for substrate binding.[28] Although the reduced form of FDH-H from E. coli lacks definitive structural characterization because there are two conflicting interpretations of the only available crystallographic data,[21] evidence from iodoacetamide tagging[26,29] and inhibitor-binding experiments[28,30] has suggested that formate displaces Sec (or Cys) from the metal center. In contrast, this suggestion has recently been challenged by the crystal structure of FDH-AB from D. vulgaris Hildenborough, in which the active-site Sec is coordinated to the W center in the reduced W(IV) state—albeit in the absence of any substrate or product in the active site.[24]

Molybdoenzymes typically cycle among the Mo(VI), Mo(V), and Mo(IV) states.[31] Recently, a reduction potential of −0.265 V vs the standard hydrogen electrode (SHE) has been measured electrochemically and assigned to the Mo center of a truncated FDH from C. necator, though it is unclear whether this potential corresponds to the Mo(VI/V) or Mo(V/IV) couple.[32] Electron paramagnetic resonance (EPR) spectra of formate or dithionite reduced FDHs exhibit a characteristic Mo(V) signal.[33−35] Following the two-electron reduction of the Mo(VI) state by formate [Mo(VI) + $HCOO^-$ → Mo(IV) + H^+ + CO_2], the Mo(IV) state is oxidized by a nearby cofactor, generating the Mo(V) state. In FDHs such as EcFDH-H that contain only one iron−sulfur center, the Mo(V) state is stable in the absence of an external electron acceptor. EPR spectra have revealed strong magnetic coupling between the Mo(V) center and a solvent-exchangeable proton[33−35] that has been attributed to a Mo(V)−SH group, formed by a formal hydride transfer from formate to the Mo(VI)=S group, followed by one-electron oxidation of the resulting Mo(IV)−SH state.[27,34,35] The mechanism by which this formal hydride transfer occurs, either concerted hydride transfer[6] or proton-coupled electron transfer (PCET),[28]

remains under debate. Therefore, gaining a deeper understanding of the kinetics and intermediates present during FDH catalysis is crucial for developing a full picture of the CO_2/formate interconversion mechanism.

Here, we have investigated the kinetic isotope effect (KIE) for formate ($HCOO^-$ and $DCOO^-$) oxidation by EcFDH-H (referred to hereon as FDH) using three distinct kinetic methods: classical steady-state solution assays with an additional soluble electron acceptor, steady-state electrocatalysis with electrode-immobilized FDH and the electrode as electron acceptor, and single-turnover stopped-flow spectroscopy in which formation of the Mo(V) state is monitored in the absence of an external electron acceptor. The three methods provide different perspectives on the KIE and its relevance in determining the rate of catalysis. They allow us to explore two regimes of rate limitation, one in which formate oxidation catalysis is limited by electron transfer (solution assays), and the other in which chemical catalysis is more dominant (electrocatalysis and stopped-flow experiments). We propose a unifying kinetic model that allows the three datasets to be reconciled, despite their qualitative differences. When fitted to the data, our model provides a conceptual framework for the rationalization of FDH catalysis in terms of both the rate of active-site catalysis and the rate of electron transfer to terminal electron acceptors. As a result, it allows prediction of the steady-state and time-dependent concentrations of key FDH states, allowing us to hypothesize the conditions under which key intermediates in CO_2/formate interconversion may be observed during steady-state turnover, and the time scales of their transient lifetimes.

Understanding how the catalysis of reversible and efficient formate oxidation is achieved is directly relevant to the catalysis of reversible and efficient CO_2 reduction. Both reactions require the challenging feat of efficient, simultaneous formation/breakage of C−H and C=O bonds. Developing knowledge of them may be exploited in the design of advanced electrocatalysts for CO_2 reduction, just as hydrogenases have inspired the field of hydrogen evolution catalysis.[36,37] FDH provides a template for both the inner and outer coordination spheres of future bidirectional and reversible synthetic electrocatalysts.[38−40] Furthermore, understanding the fundamental behavior of FDHs will inform the development of future (photo)electrochemical devices, aiding the selection of appropriate electron donors/acceptors and optimal operating conditions.

■ EXPERIMENTAL SECTION

Materials. EcFDH-H was isolated and purified as reported previously.[2] 2-(N-Morpholino)ethanesulfonic acid (MES, Alfa Aesar), N-tris(hydroxymethyl)methyl-3-aminopropanesulfonic acid (TAPS, Sigma Aldrich), 4-(2-hydroxyethyl)-1-piperazineethane-sulfonic acid (HEPES, Sigma Aldrich), potassium acetate (Alfa Aesar), sodium hydrogen carbonate (Breckland Scientific), sodium carbonate (Breckland Scientific), sodium azide (Fisher), sodium nitrate (Sigma Aldrich), benzyl viologen (Sigma Aldrich), and disodium hydrogen phosphate (Sigma Aldrich) were purchased at the highest available quality and used as received. Sodium formate (Sigma Aldrich) and sodium deuterioformate (Sigma Aldrich, 99 atom%) were dried at 100 °C under vacuum before use to ensure accurate weight measurement. Buffer solutions were prepared using MilliQ water (18 MΩ cm, 25 °C) and their pH values corrected using NaOH, KOH, or H_2SO_4.

Solution Assays. Rates of formate oxidation by EcFDH-H were monitored by measuring the coupled reduction of benzyl viologen
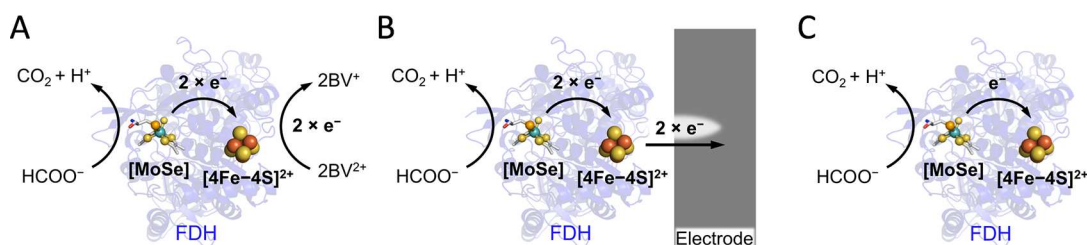
Figure 2. Summary of the methods used to study formate oxidation by *Ec*FDH−H. Formate is oxidized at the FDH Mo-containing active site; the active site transfers two electrons (one at once) to the $[4\text{Fe-4S}]^{2+}$ cluster, which in turn can transfer them to an external electron acceptor if available. (A) In solution assays, benzyl viologen (BV^{2+}) accepts the electrons from steady-state formate oxidation. (B) In PFE an electrode accepts the electrons from steady-state formate oxidation. (C) In stopped-flow spectrometry a single formate molecule is oxidized by the Mo(VI) active site, followed by the transfer of one electron to the $[4\text{Fe-4S}]^{2+}$ cluster.

(BV^{2+}) in solutions containing varying amounts of sodium formate, 1 mM BV^{2+}, and 50 mM phosphate buffer (pH 7.5, 25 °C). The increasing absorbance of BV^+ (ε_{578} = 8.65 mM^{-1} cm^{-1}) was monitored following addition of *Ec*FDH−H in 200 μL wells in a Molecular Devices microtiter plate reader housed in an anaerobic N_2-filled glovebox.

Protein Film Electrochemistry (PFE). PFE was performed using an Ivium Compactstat potentiostat in a N_2-filled glovebox (<1 ppm of O_2). A three-electrode cell, held at 23.5 °C using a circulated water jacket, was used to house a Pt mesh counter electrode, an Ag/AgCl/saturated KCl reference electrode, and a graphite−epoxy composite rotating disk electrode (RDE, area 0.09 cm^2, fabricated as described previously[2]) with a rotation rate of 2000 rpm.[28] Experiments were performed in pH-buffered solutions containing 25 mM each of MES, TAPS, HEPES, and K^+ acetate.

*Ec*FDH-H films were prepared as reported previously.[28] Sodium (deuterio)formate solutions were prepared at the same pH and buffer concentration as the cell solution. Chronoamperometric measurements of *Ec*FDH-H formate oxidation kinetics were performed by holding the electrode potential at 0 V vs SHE and continually titrating the solutions of sodium (deuterio)formate into the electrochemical cell while the current was monitored. Prior to measuring the rate of formate oxidation, the electrode potential was poised at −0.6 V vs SHE for 10 s to allow for reductive activation of FDH.[28] As reported previously, high-frequency noise from the RDE motor was removed using Fourier transformation (Figure S1A).[28] The degradation of the enzyme film was then described by taking linear fits of each step of the titration. The chronoamperometric data were divided by the resulting decay function (Figure S1B) to remove the effect of film degradation (Figure S1C).[41]

Stopped-Flow Experiments. The reduction of oxidized *Ec*FDH-H by formate was measured using a stopped-flow apparatus connected to a photodiode array spectrometer (Applied Photophysics Ltd.) housed in an anaerobic N_2-filled glovebox at 25 °C. Solutions of enzyme containing variable amounts of sodium azide were made up in 100 mM MES buffer at pH 6 (to improve the FDH stability) and then mixed in a 1:1 (v:v) ratio with a solution of 20 mM formate (also in 100 mM MES buffer at pH 6). Spectra were recorded from 300 to 723 nm with a step of 2 nm, and the sum of the absorbances at 436−444 nm was analyzed as first-order decay curves. Spectra recorded before and after reduction of FDH with formate are shown in Figure S2.

RESULTS AND DISCUSSION

Methods to Study the KIE of FDH Catalysis. The solution kinetic assay, protein film electrochemistry (PFE), and stopped-flow methodologies used to study formate oxidation by FDH are summarized in Figure 2.

The solution assays (Figure 2A) employ benzyl viologen ($BV^{2+} \rightarrow BV^+$) as electron acceptor to enable homogeneous formate oxidation with two molecules of BV^{2+} being required to oxidize one formate molecule. Electrons are transferred

sequentially, one-by-one, from the Mo-containing active site to two molecules of BV^{2+} via the $[Fe_4S_4]$ center. This diffusional and tetramolecular steady-state process has previously been described using reciprocal-plot analyses to determine basic kinetic parameters for FDH catalysis.[42] Measuring the initial rate of BV^{2+} reduction defines the steady-state rate of formate oxidation.

In contrast, PFE (Figure 2B) uses an electrode to drive heterogeneous formate oxidation. FDH, immobilized on an electrode surface, is immersed in a solution of formate in a standard 3-electrode cell. The electrode is rotated to supply formate and disperse the CO_2 product. Electronic communication between the electrode and the immobilized FDH units allows catalysis to be controlled by the electrode potential.[43] As interfacial electron transfer can be driven much faster than the diffusion-limited electron transfer required in solution assays, PFE offers an improved opportunity to focus attention on the fast enzyme-catalyzed reaction kinetics.

Finally, stopped-flow spectroscopy was used to monitor the single-turnover reduction of the $[4\text{Fe-4S}]^{2+}$ cluster of FDH upon mixing it with formate (in the absence of a terminal electron acceptor). The only electron-transfer step, following substrate oxidation, is the single electron transfer from the Mo to the $[4\text{Fe-4S}]^{2+}$ cluster (Figure 2C), which is reduced stoichiometrically due to its higher reduction potential. Therefore, stopped-flow kinetic data report only on reaction kinetics intrinsic to FDH.

Steady-State Formate Oxidation in Solution. Figure 3 shows the rate of formate oxidation (as a function of the $HCOO^-$ or $DCOO^-$ concentration) measured in solution kinetic assays with 1 mM BV^{2+}.[2,42] Both datasets are consistent with Michaelis−Menten kinetics, except that the rate decreases at high $HCOO^-$ concentrations (Figure 3, circled points). We are currently unable to provide a clear rationale for this observation: it is suggestive of inhibition from the binding of $HCOO^-$ to reduced FDH states, but a similar effect would then be expected for $DCOO^-$ and is not observed. Although the unexplained downward trend obscures definitive measurements at high concentration, the best fit to the data (discounting these points) suggests that there is no KIE in the substrate-independent rate of formate oxidation, V_{max} (V_{max}^H = 60.1 ± 1.6 $mol_{formate}$ s^{-1} mol_{FDH}^{-1}, V_{max}^D = 59.65 ± 0.95 $mol_{formate}$ s^{-1} mol_{FDH}^{-1}, V_{max}^H/V_{max}^D = 1.01 ± 0.03). This result implies that the rate-limiting step at high concentration is not C−H/D bond cleavage, or any reaction coupled strongly to it. Strikingly, however, a clear KIE is evident at low formate concentrations, where increasing the $HCOO^-$ concentration has a much stronger effect than increasing the $DCOO^-$
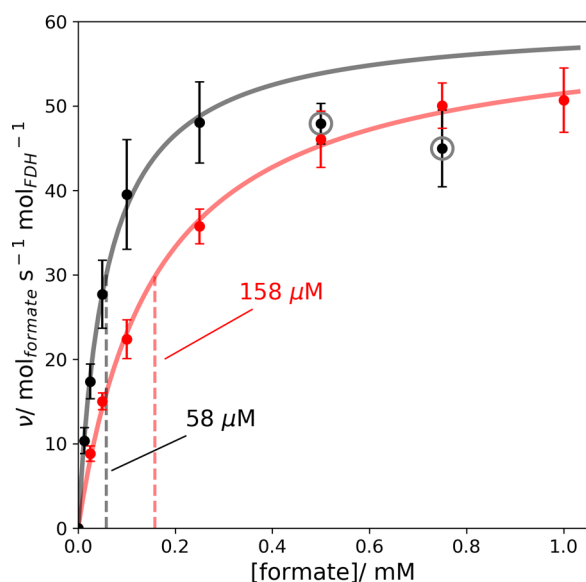
Figure 3. Rates of HCOO⁻ (black dots) and DCOO⁻ (red dots) oxidation determined by solution assays. Conditions: 1 mM BV^{2+}, 25 °C, pH 7.5, 25 mM MES, TAPS, HEPES, K^+ acetate. Error bars are ± standard error from triplicate experiments. The lines were calculated according to the Michealis−Menten equation (rate = $V_{max}[H/DCOO^-]/\{K_M + [H/DCOO^-]\}$) with K_M^H = 58 μM, V_{max}^H = 60.10 $mol_{formate}$ s^{-1} mol_{FDH}^{-1} (black), by neglecting the two highest concentration formate points (circled), K_M^D = 158 μM, V_{max}^D = 59.65 $mol_{formate}$ s^{-1} mol_{FDH}^{-1} (red).

concentration. This difference is reflected by K_M^D being higher than K_M^H (K_M^D = 158 ± 8 μM and K_M^H = 58 ± 8 μM) and by the second-order rate constant for DCOO⁻ being lower than for

HCOO⁻ (k_2^D = 0.37 ± 0.02 s^{-1} $μmol_{FDH}^{-1}$ and k_2^H = 1.0 ± 0.1 s^{-1} $μmol_{FDH}^{-1}$, k_2^H/k_2^D = 2.77 ± 0.41). The results suggest that

(i) HCOO⁻ binds more tightly or rapidly to the active site than DCOO⁻, and/or

(ii) at low formate concentrations, the rate limiting step is both isotope and concentration sensitive (at high concentrations the rate of this step increases sufficiently that it overtakes a new rate limiting step, such as electron transfer to BV^{2+}).

A difference in binding between HCOO⁻ and DCOO⁻ [hypothesis (i)] is hard to rationalize for only a simple formate binding step (without any degree of C−H bond cleavage), which must be essentially isotope independent. However, an initial binding step that is both concentration and isotope dependent may be rationalized either by strong kinetic coupling between the binding and C−H bond cleavage processes (a short-lived Michaelis complex that reacts as soon as it is formed) or by partial proton (or hydride) transfer upon binding, replacing the simple Michaelis complex by a "charge-transfer" intermediate such as the five-membered ring intermediate proposed previously.[28]

Electrocatalytic Formate Oxidation. Figure 4A compares previously published PFE data on the rate of HCOO⁻ oxidation[28] with new data for DCOO⁻ oxidation. Both datasets exhibit Michaelis−Menten profiles with no decrease in rate at high HCOO⁻ concentration. Although the unknown electroactive surface coverage of FDH on the electrode prevents the determination of turnover numbers, the ratio V_{max}^H/V_{max}^D was determined using a chronoamperometric method to directly compare the relative currents, and so account for irreproducibility and instability in the FDH film (Figure 4B). Specifically, catalytic currents were monitored while a solution consisting of HCOO⁻ was diluted stepwise by
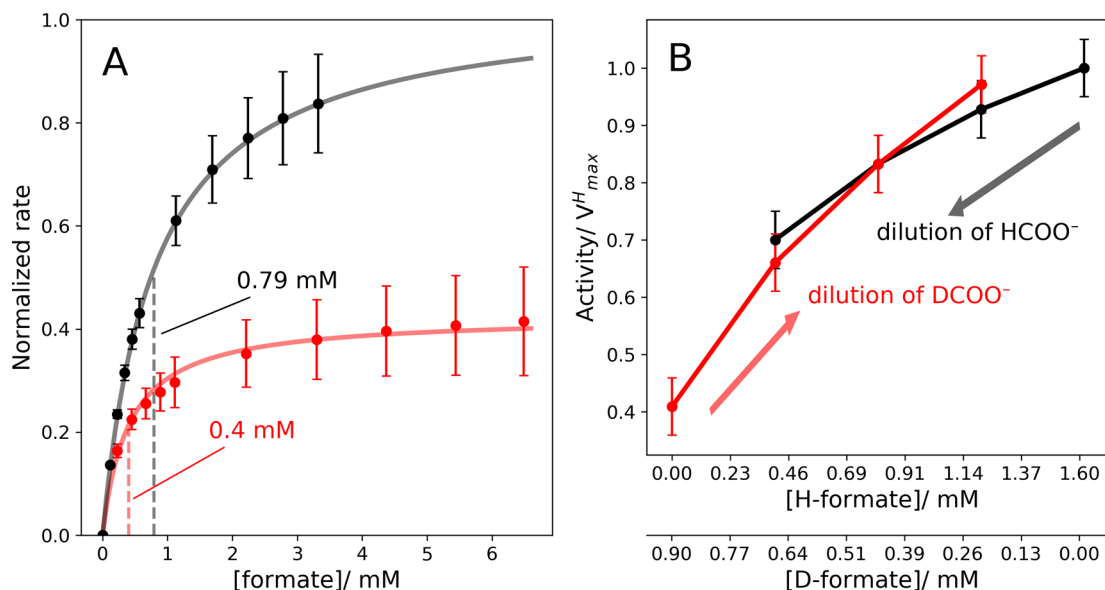
Figure 4. (A) Rates of HCOO⁻ (black) and DCOO⁻ (red) oxidation in PFE experiments (normalized so that V_{max}^H = 1 and V_{max}^D = 0.41). Dots: data, lines: fit to the Michaelis−Menten equation ($v = V_{max}[H/DCOO^-]/\{K_M + [H/DCOO^-]\}$) with K_M^H = 0.79 mM, K_M^D = 0.4 mM. Conditions: 0 V vs SHE, 23.5 °C, pH 7, 25 mM MES, TAPS, HEPES, and K^+ acetate. The HCOO⁻ oxidation PFE data have been presented previously.[28] The error bars show the standard error of the mean. (B) Determination of the KIE on V_{max} via PFE: Black dots: normalized currents in an experiment in which HCOO⁻ (concentration steps: 1.6, 1.2, 0.8, 0.4 mM) was diluted with DCOO⁻ (concentration steps: 0, 0.22, 0.44, 0.66 mM). Red dots: normalized currents in an experiment in which DCOO⁻ (concentration steps: 0.88, 0.66, 0.44, 0.22 mM) was diluted with HCOO⁻ (concentration steps: 0, 0.4, 0.8, 1.2 mM). The normalization constants were adjusted to overlay to the two datasets. Error bars denote estimated error values derived from several measurements in similar solution compositions.
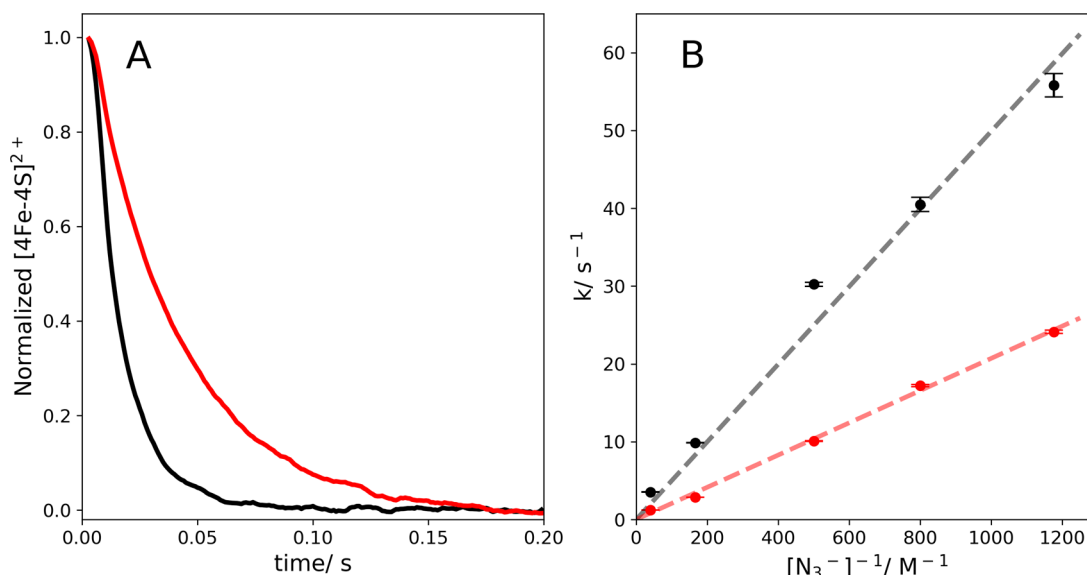
Figure 5. (A) Example stopped-flow data reporting on the rate of reduction of the $[4Fe\text{-}4S]^{2+}$ cluster (from the average decay in absorbance, A, from 436 to 444 nm) upon reaction of EcFDH-H with $HCOO^-$ (black trace) and $DCOO^-$ (red trace) in the presence of 0.85 mM N_3^-. Normalization applied = $(A - A_\infty)/(A_0 - A_\infty)$, and data were smoothed to remove noise. (B) Plots of $1/[N_3^-]$ vs k (rate constant for reduction of the $[4Fe\text{-}4S]^{2+}$ cluster) determined from stopped-flow data. Dots: experimental values from the data in panel A and Figure S4; lines: linear fits to data; error bars: the standard error of the fit. Red: $DCOO^-$, black: $HCOO^-$. Conditions: pH 6, 10 mM formate, 100 mM MES, 25 °C.

the addition of $DCOO^-$ (and vice versa) (Figure S3). The two datasets shared identical compositions of $DCOO^-/HCOO^-$, aside from the two extreme points, allowing the rate in $DCOO^-$ to be matched to that in $HCOO^-$. The ratio $V_{max}^H/V_{max}^D = 2.44 \pm 0.05$ is substantially larger than the value determined in solution assays, showing that the rate limiting step at high concentration is isotope dependent and involves C−H bond cleavage. As in the solution assays, there is also an isotope effect on K_M ($K_M^H = 0.79 \pm 0.03$ mM and $K_M^D = 0.4 \pm 0.1$ mM) and on the second-order rate constant ($k_2^H/k_2^D = 1.2 \pm 0.3$). The KIE observed for k_2 in PFE experiments is consistent with that observed in the solution assays, although smaller (1.2 and 2.77, respectively). However, the effects on K_M are in the opposite direction: in the PFE experiments, K_M^D is lower than K_M^H. Although this result seems counter-intuitive and suggestive of an inverse isotope effect, it arises only from the much lower V_{max} value with $DCOO^-$, which truncates the curve before the full substrate concentration dependence is exhibited.

Single-Turnover Stopped-Flow Kinetics. Stopped-flow experiments were used to follow $[4Fe\text{-}4S]^{2+}$ reduction as a proxy (assuming intramolecular electron transfer is fast) for the reaction of the Mo(VI) center in FDH with $HCOO^-$ or $DCOO^-$. Experiments were performed at pH 6 using 10 mM formate at several concentrations of N_3^-, a known reversible inhibitor of formate oxidation (Figure 5A, Figure S4). Inhibition was required as the rate of formate oxidation was otherwise too fast to monitor.[28,34,42] A similar stopped-flow study on *C. necator* FDH adopted a different strategy to overcome this challenge, by carrying out experiments at 10 °C to slow the reaction down.[35] Here, we have favored azide inhibition as a strategy to slow FDH catalysis, as we have characterized its inhibition mechanism previously.[28] The spectroscopic traces exhibited mono-exponential behavior, and pseudo-first-order rate constants determined from the spectroscopic time traces were proportional to $1/[N_3^-]$ (Figure 5B), consistent with the reversible inhibition[34] of

formate oxidation by N_3^- described previously,[28] and with fast N_3^- binding/dissociation pre-equilibria. Comparison of the pseudo-first-order rate constants revealed a KIE of 3.2 ± 0.3 (obtained by taking k_H/k_D at equivalent $[N_3^-]$). The isotope-dependence of the formate oxidation rate implies that cleavage of the formate C−H bond is a key rate-limiting process. The KIE determined in this work is of similar magnitude to that previously reported for *C. necator* FDH of 2.1.[35]

Development of a Kinetic Scheme to Describe the Data. The data from all three techniques may be explained using the single, unifying model shown in Scheme 1 (see Supporting Information, section 2 and Figure S5, for details and assumptions on the construction of Scheme 1). In Scheme 1, formate binds to the Mo(VI)=S state and formally transfers a hydride to generate the Mo(IV)-SH(CO$_2$) state.[35] CO$_2$ was

Scheme 1. Catalytic Cycle Used to Model Data on Formate Oxidation from Solution Assays, PFE, and Stopped-Flow Experiments[a]
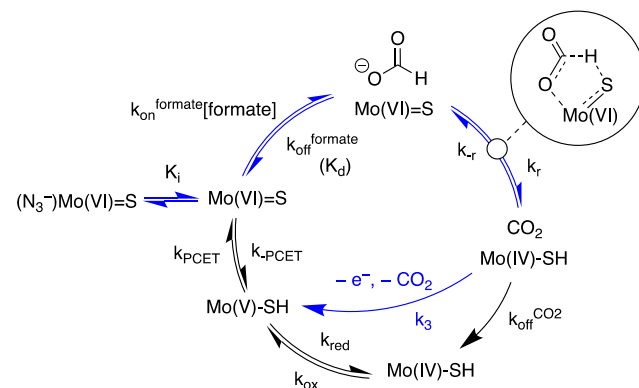
[a]Blue arrows represent the sub-scheme used to describe the stopped-flow data, ending at the Mo(V)-SH state. A proposed intermediate[28] is shown circled (top right).
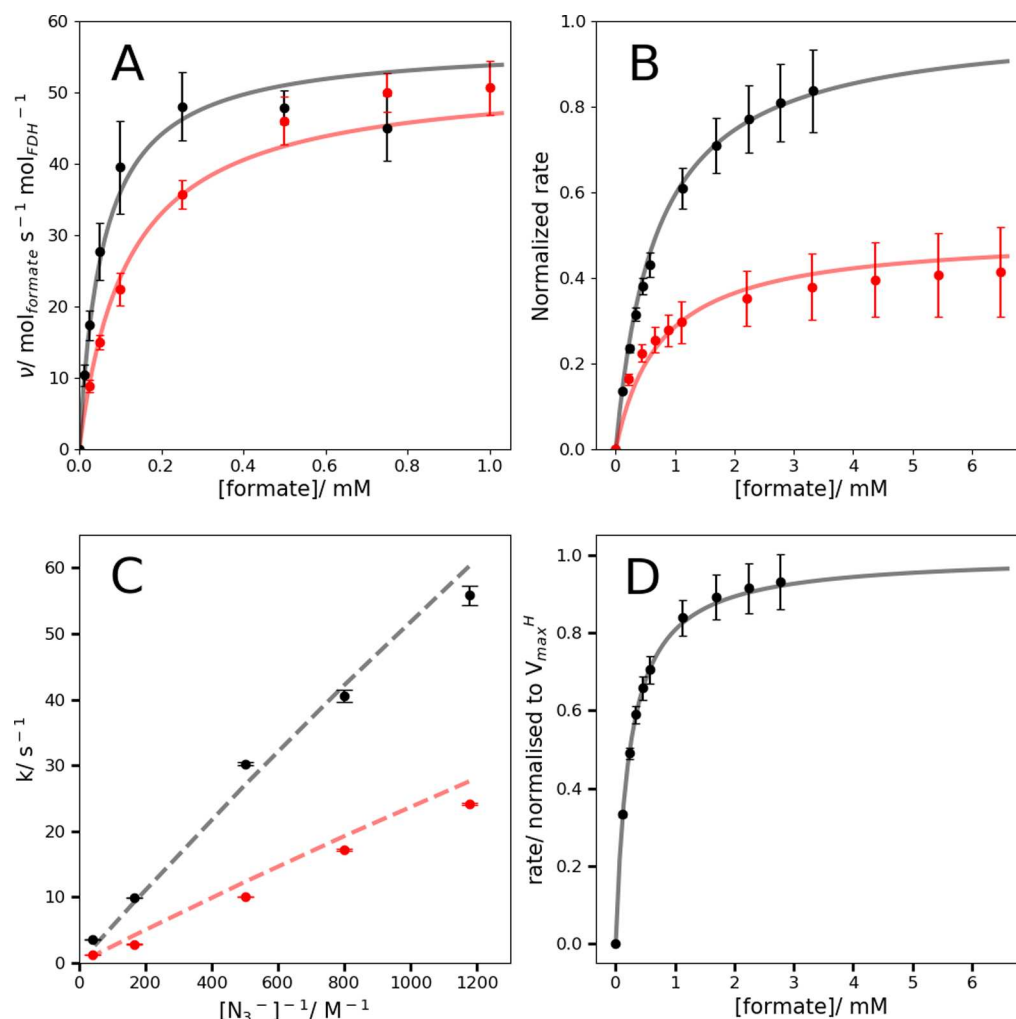
Figure 6. An example of fitting the data by using Scheme 1. (A) Solution kinetic assays of the rate of formate oxidation at pH 7.5 (black: HCOO⁻, red: DCOO⁻, dots: data from Figure 3, line: fit). (B) PFE measurement of the rate of formate oxidation at pH 7 (black: HCOO⁻, red: DCOO⁻, dots: data reproduced from Figure 4A, line: fit). (C) Stopped-flow data (dots: data from Figure 5, lines: fit). (D) PFE measurement of the rate of HCOO⁻ oxidation at pH 6, dots: data, line: fit. Fits to the data were calculated using eqs 1 and 2 with $K_d^{pH\ 7-7.5} = 0.83$ mM, $K_d^{pH\ 6} = 0.29$ mM, $k_r = 2480$ s⁻¹, $k_{-r} = 8060$ s⁻¹, $k_3 = 3930$ s⁻¹, $K_I = 2.00\ \mu$M, KIE = 4.7, $k_{ox}^{PFE} = 2.0 \times 10^5$ s⁻¹, $k_{red}^{PFE} = 7 \times 10^{-4}$ s⁻¹, $k_{PCET}^{PFE} = 1.9 \times 10^5$ s⁻¹, $k_{-PCET}^{PFE} = 1.7 \times 10^{-3}$ s⁻¹, $k_{ox}^{sol} = 693$ s⁻¹, $k_{red}^{sol} = 0$ s⁻¹, $k_{PCET}^{sol} = 683$ s⁻¹, $k_{-PCET}^{sol} = 0$ s⁻¹.

not added to experimental solutions and therefore dissociates irreversibly to produce the Mo(IV)-SH state, which is then oxidized by one electron to form the stable Mo(V)-SH intermediate. The stopped-flow experiment explores stoichiometric formate oxidation and terminates here (with an irreversible intramolecular k_{ox} step that combines with the preceding irreversible CO₂ dissociation to form k_3),[33−35] whereas in solution assays and PFE a PCET step regenerates the oxidized Mo(VI)=S state to sustain the catalytic cycle. In the latter two cases, electron transfer between the active site and the outside is considered as a single step, without taking into account intramolecular transfer to the [4Fe-4S]²⁺ cluster, which is considered fast (estimated[44] as 4×10^6 s⁻¹, much faster than turnover, from the short ∼7 Å distance[21,45] and a ΔE of −0.3 V, in excess of the ΔE estimated for the truncated FDH from *C. necator*[32]).

The steady-state equation for FDH catalysis, eq 1, was derived from Scheme 1 (along with similar equations to describe the population of each species, see Supporting Information, section 3, eqs S1−S20) by assuming formate binding is fast such that the ratio of Mo(VI)=S and

Mo(VI)=S(formate) is set by the equilibrium constant, K_d. The symbol [F] denotes formate concentration, and Γ denotes either the electroactive surface coverage or the solution concentration of FDH.

$$v = k_{off}^{CO_2}\Gamma \Big/ \left[\frac{k_{-r} + k_{off}^{CO_2}}{k_r} \frac{K_d + [F]}{[F]} + \left(\frac{k_{-PCET}}{k_{PCET}} \frac{K_d}{[F]} \frac{k_{-r} + k_{off}^{CO_2}}{k_r} \right. \right.$$
$$\left. \left. + \frac{k_{off}^{CO_2}}{k_{PCET}} \right) \left(1 + \frac{k_{red}}{k_{ox}} \right) + \frac{k_{off}^{CO_2}}{k_{ox}} + 1 \right] \tag{1}$$

Equation 2 is the pre-steady-state equation for Scheme 1 in which the reaction terminates at Mo(V)-SH. It describes how the population of the Mo(V)-SH state changes over time in stopped-flow experiments. It was derived, along with equations describing the time-dependent evolution of each species (see Supporting Information, section 4, eqs S21−S48), by assuming both N₃⁻ and formate binding are fast and can be considered as pre-equilibria.
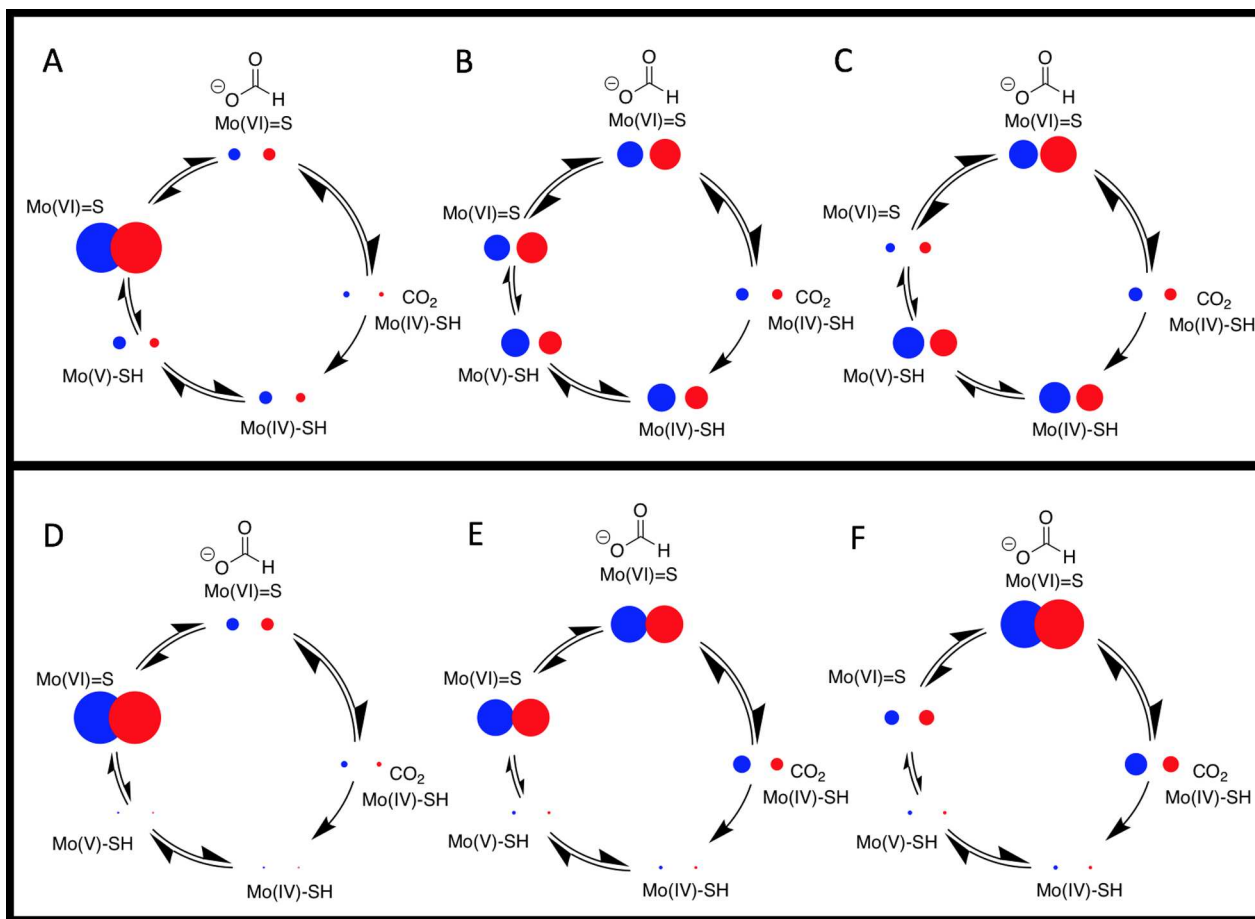
Figure 7. Steady-state populations of states calculated using eqs S16–S19 and the parameters used to determine the fit in Figure 6. Circled areas reflect the steady-state population of each state. (A) Simulations of solution kinetic assays with 40 μM formate. (B) Simulations of solution kinetic assays with 0.83 mM formate. (C) Simulations of solution kinetic assays with 10 mM formate. (D) PFE simulations with 40 μM formate. (E) PFE simulations with 0.83 mM formate. (F) PFE simulations with 10 mM formate. $HCOO^-$: blue, $DCOO^-$: red.

$$[Mo(V)\text{-}SH](t) =$$

$$[Mo(VI)]_0\left[1 - \frac{\beta}{\beta - \gamma}\,e^{-\gamma t} + \frac{\gamma}{\beta - \gamma}\,e^{-\beta t}\right] \quad (2)$$

where

$$\beta = \frac{1}{2}\left(k_{-r} + k_3 + \frac{k_r}{A}\right) + \frac{1}{2}\sqrt{\left(k_{-r} + k_3 + \frac{k_r}{A}\right)^2 - \frac{4k_r k_3}{A}}$$

$$\gamma = \frac{k_r k_3}{A\beta}, \quad \text{and} \quad A = \frac{K_d}{[F]}\left(1 + \frac{[N_3^-]}{K_i}\right) + 1$$

$[Mo(VI)]_0$ is the initial concentration ($t = 0$) of $[Mo(VI)]$ ($= [Mo(VI){=}S] + [Mo(VI){=}S(\text{formate})] + [Mo(VI){=}S(N_3^-)]$).

Finally, as the isotope-sensitive step is expected to be the C–H bond cleavage step, KIE was assigned as a divisor of k_r and k_{-r} in calculations of $DCOO^-$ oxidation rates in eqs 1 and 2.

Modeling the Data. Equations 1 and 2 were used to model the data in Figures 3–5 (Figure 6). An additional PFE dataset reporting on $HCOO^-$ oxidation as a function of its concentration at pH 6 (Figure 6D)[28] was included to aid incorporation of the stopped-flow data, which was obtained at pH 6 (lower than the solution and PFE data for experimental

and enzyme stability reasons). Table S1 summarizes the rate constants relevant to each dataset and the boundaries placed on the parameter space searched. Only the K_d values (which were allowed to vary with the pH) and the interfacial/intramolecular electron-transfer rate constants were allowed to vary between the datasets.

The parameter space was searched for combinations of parameters which best replicated the data using an evolutionary algorithm (see Supporting Information, section 5). Many different combinations that could reproduce the data equally well were identified, precluding definition of individual parameter values. However, all parameter combinations that fit the data defined similar steady-state populations and time courses for the different species that comprise Scheme 1, providing new insights into FDH catalysis.

Figure 6 shows a representative fit to the data. The model reproduces the similar V_{max} values observed for $DCOO^-$ and $HCOO^-$ in solution assays (Figure 6A) and the very different V_{max} values observed in PFE experiments (Figure 6B), which reflect the KIE revealed by the stopped-flow experiment that is focused most closely on C–H bond cleavage (Figure 6C). The model also reflects the KIEs observed at low formate concentrations in the solution kinetics and PFE experiments. Therefore, our model shows clearly how simple electron-transfer kinetics, independent of the reaction of interest, can place the reaction in different kinetic regimes that differ

significantly in the level and quality of information that they reveal. However, as may be anticipated for a simple, common model and parameter set applied to three very different experimental datasets, there are some limitations—the most substantial of which is that V_{max}^D for the solution assay data is underestimated. It is possible that the fit is compromised by the lack of a mechanism for substrate inhibition, which renders the model unable to capture the observed decrease in $HCOO^-$ oxidation rate at high concentrations in the solution kinetics. However, it may also result from the simplicity of the formate binding mechanism applied: as discussed above, an isotope-dependent substrate binding step raises the possibility that the product of binding is not a simple Michaelis enzyme—substrate complex in which the active-site-bound formate remains unreacted, but a "charge-transfer" intermediate in which the C−H bond is weakened. In the five-membered ring intermediate suggested in Scheme 1, the formate α-H is interacting with the sulfido ligand and electron density has shifted toward the Mo ion in either a PCET reaction (anti-clockwise), or a hydride-transfer reaction (clockwise).[28] Our current model does not account for an isotope sensitive formate binding rate constant.

Interpreting the Steady-State Data. Using the fit parameters outlined in Figure 6, the steady-state population of each catalytic intermediate can be calculated for both the solution and PFE conditions (see Supporting Information, section 4). Figure 7 depicts the population of each species as a circle area at three $DCOO^-$ and $HCOO^-$ concentrations: below K_d (Figure 7A,D), equal to K_d (Figure 7B,E), and above K_d (Figure 7C,F).

First, the effects of the different electron-transfer rates between the solution assays (slow) and PFE (fast) are clearly evident, especially at high concentrations, from the larger populations of the reduced Mo(V)-SH and Mo(IV)-SH states in the solution assay simulations (Figure 7A−C) than the PFE simulations (Figure 7D−F). Faster electron-transfer rates shift the FDH population toward the oxidized states, making isotope-dependent steps more strongly rate determining and the KIE more pronounced.

At formate concentrations much lower than K_d (e.g., Figure 7A,D), the population lies toward the Mo(VI)=S state, as expected for a binding equilibrium. The populations in both the PFE and solution assay simulations appear similar in this case. The active site can be regenerated rapidly, and the isotope- and formate concentration-dependent conversion reaction (binding through to CO_2 release) controls the overall rate of catalysis. As a result, a KIE is apparent at low formate concentrations. Upon increasing the concentration of formate to equal K_d (Figure 7B,E), the configurations diverge. In the fast electron-transfer regime (Figure 7E,F), the population of the Mo(VI)=S(formate) state increases (before the isotope-dependent step), in accordance with the binding equilibrium, while there is a minimal increase in the populations of the reduced states. In contrast, for slow electron transfer (Figure 7B,C), there is a larger shift of the population into reduced states. Here, the model indicates the transfer of rate control from chemical catalysis to electron transfer, and so the KIE is decreased. For the fast electron-transfer regime, electron transfer still outpaces chemical catalysis, and the system is held more in the Mo(VI)=S(formate) state. The KIE is thus larger at higher formate concentrations.

Using the predicted rate constants, it is also possible to estimate the absolute rate of formate oxidation in PFE experiments. PFE data have been normalized to account for lack of knowledge of the electroactive surface coverage. However, the behavior of FDH under high electron-transfer regimes can be simulated using eq 1 and the best-fit rate constants to give an estimated maximal rate for formate oxidation of 626 s^{-1}, around 11 times higher than in solution assays. This result underlines the importance of considering the rate of electron transfer with solution-phase electron donors or acceptors when elucidating active-site kinetics. Furthermore, if the rate of electron transfer in solution assays could be increased (e.g., by using an electron acceptor with a higher reduction potential) to mirror the PFE data (Figure 7F), then spectroscopic characterization of the important Mo(VI)=S(formate)/Mo(IV)-SH(CO_2) intermediate states may become possible, especially if the solution CO_2 concentration is increased.

Evolution of Species over Time in the Stopped-Flow Experiment. The time-evolution of the four FDH states detailed for stopped-flow experiments in Scheme 1 can be simulated using the best fit parameters detailed in Figure 6, eq 2, and eqs S41 and S42. Figure 8 shows the simulation for
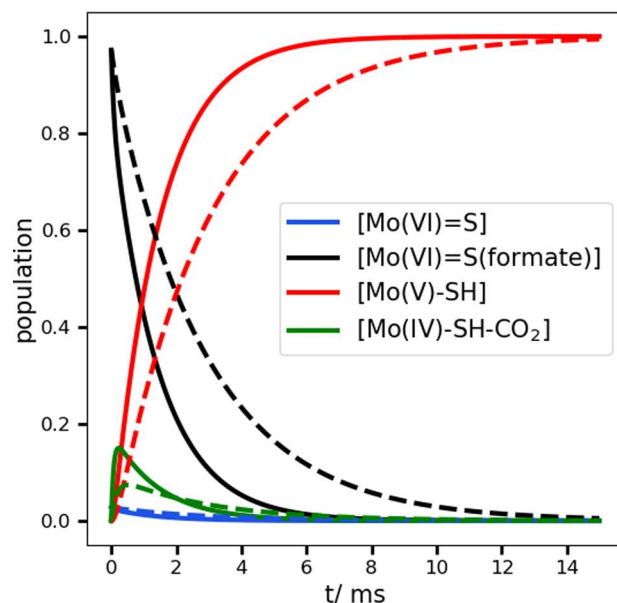
Figure 8. Calculated changes in pre-equilibrium populations of the Mo(VI)=S, Mo(VI)=S(N_3^-), Mo(VI)=S(formate), Mo(IV)-SH-(CO_2), and Mo(V)-SH states over time using eqs S41 and S42 and eq 2 and the same parameters as in Figure 6 with [$HCOO^-$] = 10 mM, [N_3^-] = 0 mM. Solid lines: $HCOO^-$, dashed lines: $DCOO^-$.

FDH reacting with 10 mM formate in the absence of N_3^-. Due to the fast formate binding equilibrium, a steady-state ratio of Mo(VI)=S(formate) and Mo(VI)=S is established immediately, weighted toward the Mo(VI)=S(formate) state and governed by K_d. As the reaction progresses, the Mo(IV)-SH(CO_2) population grows to around 15% at about 0.2 ms. For $DCOO^-$ oxidation, the buildup is lower (7.5%) and peaks at around 0.5 ms. Such a small buildup and lifetime of this species leads to the apparent first-order behavior of the reaction (rather than biphasic behavior in which formation of the Mo(V)-SH state would exhibit a lag phase). Thus, Mo(VI)=S(formate) is rapidly converted to the product Mo(V)-SH, and formate oxidation (C−H bond cleavage) exerts strong control over the net reaction rate. As a result, the

KIE revealed by the stopped-flow data is considered to represent closely the intrinsic KIE for formate oxidation.

These calculations further highlight the importance of steady-state measurements in observing FDH activity. If the key Mo(VI)=S(formate)/Mo(IV)-SH(CO_2) intermediate states could be spectroscopically characterized, transient measurements would only allow a small window of time for their detection. Bringing the system into steady state, either in solution assays or on an electrode surface, would provide a continuous observation period. The spectroscopic character-ization of electroactive proteins and enzymes on electrode surfaces via techniques such as surface Raman or attenuated total reflection−infrared spectroscopies are in current use and development.[46] The control over the distribution of FDH states enabled by the electrode potential, and the ability to dynamically change conditions (such as varying formate concentration by titration as reported here), should allow the population of key intermediates to be promoted, increasing the ease with which they may be spectroscopically characterized by these techniques.

CONCLUSIONS

Our unifying model for FDH catalysis shows how the distinct kinetic behaviors of the solution assay kinetics, PFE, and stopped-flow methods can be rationalized by considering the rates of chemical catalysis and intermolecular/interfacial electron transfer, and provides predictions to guide future experimental designs.

In solution assays, electron transfer between FDH and BV^{2+} is slow, and a KIE of 2.77 is only apparent at low formate concentration (<40 μM) when chemical catalysis is also slow. At higher formate concentrations (>40 μM) and accelerated chemical catalysis, the reaction rate is limited by isotope-insensitive electron transfer. The PFE technique lifts this rate limitation through fast interfacial electron transfer between FDH and the electrode. As a result, catalysis is again limited by the chemical conversion, and a KIE of 2.44 is observed. Stopped-flow kinetics enable the rate of chemical catalysis at the active site to be observed independently of intermolecular/interfacial electron transfer and reveal a KIE for formate oxidation of approximately 3, similar to that observed at low concentration and determined by PFE.

We observe that, under experimental conditions that focus on formate oxidation itself, catalysis is both formate concentration and isotope sensitive and can be modeled by tightly coupling the formate binding and conversion steps. This apparent coupling may suggest the possibility that the C−H bond is weakened in the initial formate-bound state, better represented as a bound intermediate between CO_2 and formate. Finally, by extrapolating our model to as-yet unexplored experimental conditions, we highlight the regimes of formate concentration and electron transfer under which the concentrations of key substrate/product-bound FDH states, including the proposed intermediate, may be enhanced to allow them to be observed spectroscopically. The presented model of FDH catalysis of formate oxidation could be easily transposed into a model for CO_2 reduction (or catalysis in both directions). Therefore, this framework will provide a starting point in rationalizing similar data for CO_2 reduction. Furthermore, since formate oxidation and CO_2 reduction are inextricably linked in a mechanistic sense, we expect our observations on formate oxidation to reflect on data for CO_2 reduction. A particularly crucial aspect is elucidating the

structure and behavior of the intermediate, which is likely formed during the catalytic interconversion step.

ASSOCIATED CONTENT

Ⓢ Supporting Information

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/jacs.0c03574.

Supporting data, further details on the mathematical model, equations and parameters, and a description of the fitting algorithm, including Figures S1−S7, Table S1, and eqs S1−S48 (PDF)

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Notes

ACKNOWLEDGMENTS

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