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**Article:**

Du, H, Xu, Z, Hu, M et al. (7 more authors) (2020) Natural organic matter decreases uptake of W(VI), and reduces W(VI) to W(V), during adsorption to ferrihydrite. *Chemical Geology*, 540. 119567. ISSN 0009-2541

<https://doi.org/10.1016/j.chemgeo.2020.119567>

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1           **Natural organic matter decreases uptake of W(VI), and reduces**  
2                           **W(VI) to W(V), during adsorption to ferrihydrite**

3  
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23 **Abstract**

24 Tungsten is both naturally occurring and an anthropogenically released contaminant  
25 metal in soils, sediments and water systems that typically exists as the soluble tungstate  
26 oxyanions,  $W(VI)O_4^{2-}$ . Tungsten mobility and fate are strongly dependent on the  
27 adsorption of tungstate to mineral surfaces. However, environmental mineral surfaces  
28 are commonly coated with natural organic matter (NOM), and the role of this coating  
29 in the tungsten adsorption process, and thus in controlling tungsten reactivity and  
30 transport, is unclear. This study investigates W(VI) adsorption to ferrihydrite (Fh), a  
31 ubiquitous iron (hydr)oxide in soils and sediments, both in the absence and presence of  
32 humic acid (HA), a widely occurring type of NOM, using batch experiments coupled  
33 with spectroscopic and thermodynamic techniques. Kinetic results indicate that access  
34 to the adsorption sites for W(VI) on the organomineral surfaces is limited when Fh is  
35 coprecipitated with HA. Commensurate with this observation, batch experiments show  
36 that HA decreases W(VI) adsorption to Fh over a wide pH range (4-11), and this  
37 inhibitory effect is more pronounced at higher HA concentration. X-ray photoelectron  
38 spectroscopy (XPS) measurements demonstrate the formation of inner-sphere type W  
39 complexes on both the Fh and HA fraction of the Fh-HA binary composite. In particular,  
40 ~40% of the adsorbed W(VI) species is reduced to W(V) in the presence of HA.  
41 Attenuated total reflectance Fourier transform infrared spectroscopy (ATR-FTIR)  
42 results show the presence of poly tungstate species on Fh, particularly at lower pH and  
43 in the presence of HA. Isothermal titration calorimetry shows that W(VI) adsorption to  
44 Fh is an exothermic process both in the presence and absence of HA, and that process

45 is accompanied by a positive entropy. The findings of this work suggest that NOM not  
46 only mobilizes tungstate but also reduces tungstate from W(VI) to W(V) at  
47 environmental iron (hydr)oxide-water interfaces, which is of significance for evaluating  
48 the migration and bioavailability of tungsten in both natural and contaminated  
49 environments.

50

51 **Keywords:** tungsten, adsorption, iron (hydr)oxide, NOM, organo-mineral association,  
52 tungsten reduction, isothermal titration calorimetry

53

## 54 **1. Introduction**

55 Tungsten (W) is both a naturally occurring element and an anthropogenic contaminant,  
56 that is increasingly released into the environment as a result of its use in a wide range  
57 of industrial products that require high heat resistance and mechanical toughness, such  
58 as light bulbs, bullets and many metal alloy (Koutsospyros et al., 2006). Recent reports  
59 of W contamination in groundwater and soil systems have raised concerns about its  
60 potential toxicity to plants, animals and humans (Kennedy et al., 2012; Tuna et al., 2012;  
61 Datta et al., 2017; Lindsay et al., 2017; Mohajerin et al., 2014a; 2014b; Oburger et al.,  
62 2018), and because of its risk to natural systems, W has been listed as an emerging  
63 contaminant by the United States Environmental Protection Agency (EPA)  
64 (<https://www.epa.gov/fedfac/technical-fact-sheet-tungsten>). Despite its listed status  
65 however, the biogeochemical behavior and potential risks of W to human and  
66 environmental health are still poorly understood.

67       Metallic W is generally insoluble with little or no mobility, however, under near-  
68 surface conditions W is present in an oxidized state, and forms a variety of oxyanionic  
69 species, such as the W(VI) species tungstate  $\text{WO}_4^{2-}$  and poly tungstate  $\text{W}_7\text{O}_{24}^{6-}$ , which  
70 dissolve in water and are mobile in the environment (Dermatas et al., 2004; Clausen  
71 and Korte, 2009). When W is present as dissolved tungstate oxyanions (e.g.,  $\text{WO}_4^{2-}$ ),  
72 strong uptake may occur at mineral-water interfaces, influencing its mobility and fate  
73 in soils, sediments and water systems (Johannesson et al., 2013). Recently, iron-bearing  
74 minerals such as ferrihydrite, hematite, goethite, iowaite and pyrite have been reported  
75 as an important sink for tungstate oxyanionic species (Gustafsson, 2003; Cui and  
76 Johannesson, 2017; Iwai and Hashimoto, 2017; Rakshit et al., 2017; Sallman et al.,  
77 2018; Cao et al., 2019). For example, iowaite, an iron-bearing layered double hydroxide  
78  $[\text{Mg}_6\text{Fe}_2(\text{OH})_{16}\text{Cl}_2 \cdot 4\text{H}_2\text{O}]$ , can sorb up to 71.9 mg/g tungstate from aqueous solution  
79 (Cao et al., 2019). In general, tungstate adsorption increases with decreasing pH  
80 (Gustafsson, 2003; Cui and Johannesson, 2017; Sallman et al., 2018), and spectroscopic  
81 measurements, such as those made using attenuated total reflectance Fourier transform  
82 infrared spectroscopy (ATR-FTIR) and X-ray absorption spectroscopy (XAS),  
83 demonstrate the formation of inner-sphere type adsorption complexes during tungstate  
84 binding to iron (hydr)oxides including ferrihydrite and hematite (Sun and Bostick, 2015;  
85 Rakshit et al., 2017; Sallman et al., 2018), and the strength of this interaction is greater  
86 with decreasing pH. Tungsten oxyanions can also polymerize to form poly tungstate  
87 species (Strigul et al., 2009; Strigul, 2010), which can decrease tungstate adsorption  
88 onto ferrihydrite (Gustafsson, 2003), thereby potentially mobilizing W in the

89 environment (Bostick et al., 2018). Of particular relevance to natural systems,  
90 competing oxyanions such phosphate (P) can inhibit the retention of tungstate on  
91 hematite (Sallman et al., 2018), and the surface complexation of tungstate in the  
92 competitive system differs from that in the absence of  $\text{PO}_4^{3-}$ . This indicates that  
93 moieties that compete with tungstate for available sorption sites on iron (hydr)oxides  
94 are able to significantly modify W mobility and fate in soils and sediments.

95 One such competing moiety that is widely distributed in soils, sediments and water  
96 systems is natural organic matter (NOM). This is known to bind strongly with iron  
97 (hydr)oxides via surface adsorption and/or (Sposito, 1984; Chen et al., 2014; Kleber,  
98 2015). These processes result in the formation of an organo-mineral composite (Kleber  
99 et al., 2015), in which surface properties are quite different from those of pure iron  
100 (hydr)oxide, thereby potentially affecting the transport and eventual fate of trace  
101 elements (Moon and Peacock, 2012; Liang et al., 2013; Seda et al., 2016; Du et al.,  
102 2016; Wang et al., 2016; Flynn and Catalano, 2017; Otero-Fariña et al., 2017; Du et al.,  
103 2018a; 2018b; Fariña et al., 2018; Woodward et al., 2018; Xue et al., 2019). However,  
104 whether and to what extent NOM affects the binding of soluble tungstate oxyanions to  
105 mineral surfaces is still unknown. Moreover, W has several oxidation states (+4 ~ +6),  
106 and whether oxidation-reduction occurs in the presence of NOM is unclear. This  
107 fundamental information is vital to understand the controls on tungstate mobility,  
108 bioavailability and toxicity in natural systems.

109 The purpose of this study was to examine the influences of NOM, represented by  
110 the widely abundant organic moiety humic acid (HA), on tungstate adsorption and

111 oxidation/reduction at typical iron (hydr)oxide-water interfaces. By varying total W  
112 concentration, pH or equilibration time, a variety of experimental analogues were  
113 investigated to simulate complex natural systems. In addition, the structures of adsorbed  
114 W species and the thermodynamic binding properties were also investigated using X-  
115 ray photoelectron spectroscopy (XPS), attenuated total reflection Fourier transform  
116 infrared spectroscopy (ATR-FTIR) and isothermal titration calorimetry (ITC). Two  
117 different NOM concentrations were also considered, which represent either OM poor  
118 or rich environments. Our results shed new light on the role of NOM in tungstate  
119 adsorption and valence state changes at typical mineral-water interfaces. Such  
120 information is required to accurately predict the mobility and thus eventual fate of W  
121 in natural soils, sediments and water systems.

122

## 123 **2. Experimental methods**

124 All chemicals and reagents used were of analytical grade. All solutions were made with  
125 ultrapure water (18.2 M $\Omega$ ·cm). The W(VI) stock solution was prepared from sodium  
126 tungstate dihydrate (Na<sub>2</sub>WO<sub>4</sub>·2H<sub>2</sub>O). The background electrolyte was sodium chloride  
127 (NaCl) prepared at 0.01 M. Plastic labware was used throughout the experiments and  
128 cleaned with dilute nitric acid before use.

129

### 130 **2.1 Synthesis of ferrihydrite and ferrihydrite-HA binary composite**

131 A commercial peat-derived HA (No: H16752, Sigma-Aldrich (Shanghai) Trading  
132 Co.Ltd., China) was selected as an analogue for natural organic matter, and purified

133 followed the protocols of Du et al. (2016). Pure ferrihydrite (Fh) was synthesized by  
134 hydrolysis of a 0.1 M  $\text{Fe}^{3+}$  salt solution to pH  $\sim 7.5$  with NaOH. For preparation of the  
135 Fh-HA binary composite, 0.1 M  $\text{Fe}^{3+}$  salt solution was first reacted with two known  
136 amounts of HA solution for 2 h, generating C/Fe molar of 0.47 and 2.33, respectively,  
137 then subjected to a base hydrolysis to pH  $\sim 7.5$ . These preparations resulted in Fh-HA  
138 composites with approximately 5 wt% and 15 wt% C (Du et al., 2018b), and were  
139 abbreviated as FhHA\_5%C and FhHA\_15%C, respectively. Both pure Fh and Fh-HA  
140 composite were rinsed several times until no dissolved organic carbon (DOC) was  
141 detected in the supernatant liquid (Du et al., 2018b).

142

## 143 **2.2 W(VI) adsorption experiments**

144 Adsorption experiments were performed in batch systems at room temperature ( $\sim 25^\circ\text{C}$ ).  
145 In each centrifuge tube, a mixed solution ( $\sim 30$  mL) contained known amounts of  
146 adsorbent (Fh or Fh-HA, 0.05 g/L), W(VI) and background electrolyte (0.01 M NaCl).  
147 For adsorption kinetics, the initial concentration of W(VI) was fixed at  $\sim 0.165$  mmol/L  
148 ( $\sim 30$  mg/L), and the pH was controlled at pH 6.5. During the kinetic experiments, an  
149 aliquot of adsorption suspension ( $\sim 1$  mL) was taken successively by pipette at 1, 5, 15,  
150 25, 50, 150, 300 and 900 min intervals. For adsorption edge experiments (pH 4-11), the  
151 initial concentration of W(VI) was fixed at  $\sim 0.165$  mmol/L, and the pH was adjusted to  
152 the target pH using dilute  $\text{HNO}_3$  or NaOH. For adsorption isotherms experiments (pH  
153 6.5 as a representative) experiments, the concentration of W(VI) was varied from 0 to  
154  $\sim 0.43$  mmol/L. Centrifuge tubes for adsorption edges and isotherms were lightly shaken



155 continuously for ~15 h to reach equilibrium. The suspensions were then centrifuged and  
156 filtered through 0.22  $\mu\text{m}$  membrane filters and 3k Dalton ultrafilters (Du et al., 2018b).  
157 The W(VI) concentration was measured using ICP-OES (PerkinElmer Optima 8300)  
158 and the supernatant thick paste was recovered for XPS analyses. All adsorption  
159 experiments were performed in duplicate.

160

### 161 **2.3 XPS experiments**

162 The residual thick pastes left in the adsorption experiments were freeze-dried and  
163 ground into powder samples, then sealed in polyethylene bags for XPS analysis. Spectra  
164 of W 4f (5p), O 1s and C 1s were measured using the KRATOS Axis Ultra X-ray  
165 photoelectron spectrometer (Thermo Fisher Scientific, US) equipped with a  
166 monochromatic Al  $K\alpha$  source and a charge compensation system. During data  
167 collection, the step size was 0.05 eV, and 10 scans for each sample were averaged. For  
168 XPS analyses, the C 1s peak at ~284.8 eV was used to calibrate the binding energy, and  
169 the curve-fitting program XPSPEAK41 was used to fit the spectra (Xue et al., 2019).

170

### 171 **2.4 In situ ATR-FTIR experiments**

172 *In situ* ATR-FTIR experiments were performed on a PerkinElmer FT-IR spectrometer  
173 equipped with an advanced 6 reflection ATR system (ZnSe crystal, 45° angle) for the  
174 infrared analysis of liquids and pastes. The flow cell consists of a rectangular holder  
175 coated with a thin film of either Fh or Fh-HA, prepared by overnight drying of 1 mL of  
176 suspension evenly spread across the crystal surface. Background electrolyte (0.01 M

177 NaCl) was first pumped through the reaction vessel at a rate 1 mL/ min, until the IR  
178 signals were no longer increasing. Then a freshly prepared W(VI) stock solution was  
179 introduced through the flow cell, and the spectra were recorded every 40 min, until the  
180 IR signals were no longer increasing. The characteristic IR absorbances of adsorbed W  
181 species were predominately in the range of 1400 to 700  $\text{cm}^{-1}$  (Rakshit et al., 2017). All  
182 experiments were conducted at pH 4.5, 6.5 and 8.5.

183

## 184 **2.5 ITC experiments**

185 Adsorption calorimetry was conducted using a TAM III thermal activity monitor system  
186 (TA Instruments, US) equipped with a 1 mL reaction cell and a 500  $\mu\text{L}$  micro-syringe.  
187 Prior to measurements, 0.7 mL of sorbent solution (5 g/L) was placed in the reaction  
188 cell string at 120  $\text{rev min}^{-1}$ . The sample was left to stabilize to achieve a highly stable  
189 heat flow (i.e., a signal excursion  $< 250$   $\text{nw/hr}$ ). The W(VI) solution ( $\sim 5.44$   $\text{mmol/L}$ )  
190 was subsequently titrated into the sorbent solution at a rate of 1  $\mu\text{L/s}$ , and the adsorption  
191 heat flow ( $\mu\text{W}$ ) was recorded continuously. Each titration was 10  $\mu\text{L}$  with an interval of  
192 600 s. A control experiment was conducted by titrating W(VI) solution into the  
193 background electrolyte to exclude the dilution heat that was not caused by W(VI)  
194 adsorption. All measurements were performed at pH 6.5 and 298 K. Data processing  
195 was accomplished using the software TAM assistant (ver. 1.4) and NanoAnalyze (ver.  
196 3.6, TA Instruments, US) for the determination of  $\Delta G$ ,  $\Delta H$ ,  $\Delta S$  and binding affinity ( $K$ )  
197 (Du et al., 2018c; 2019). The experimental ITC data were fit by an independent-site  
198 model (dotted lines in Fig. 6) described in Freire et al. (1990):

199 
$$Q = V[M] \frac{n\Delta HK[L]}{1+K[L]}$$

200 where  $V$  is the volume of the reactor,  $\Delta H$  is enthalpy (kJ/mol),  $K$  ( $M^{-1}$ ) represents the  
201 thermodynamic affinity,  $[L]$  is the total W concentration,  $[M]$  is the sorbent  
202 concentration, and  $n$  is the number of binding sites. The Gibbs free energy ( $\Delta G$ ) was  
203 calculated by:  $\Delta G = -RT \ln K_a$ , where  $R = 8.314$  J/mol/K,  $T = 298$  K. The entropy  
204 change  $\Delta S$  was calculated by:  $\Delta S = (\Delta H - \Delta G)/T$ .

205

### 206 **3. Results**

#### 207 **3.1 Macroscopic adsorption phenomena**

208 Tungstate adsorption kinetics are investigated to explore whether the presence of HA  
209 affects the W(VI) adsorption rate onto Fh surfaces, and the results are shown in Figure.  
210 S1. The plots represent the adsorbed amount of W(VI) (mmol/kg) plotted against time  
211 (h). For all the systems studied, a two-stage kinetic behavior is apparent: a fast initial  
212 adsorption in the first 1 h, followed by a slow adsorption, and it is apparent that after 3  
213 h reaction W(VI) adsorption reaches equilibrium. Herein, a Pseudo-second order model  
214 (solid lines in Fig. S1) provides a good fit to the data ( $\geq 0.92$ ), and is used to obtain the  
215 kinetic adsorption parameters. This model has been widely used in describing the  
216 kinetics of metal adsorption to a variety of sorbents (Zhu et al., 2011; Du et al., 2017;  
217 Yan et al., 2017). The Pseudo-second order model can be expressed as:  $1/(q_e - q_t) = 1/q_e$   
218  $+ kt$ , where  $q_e$  is the equilibrium adsorption amount and  $k$  represents the rate constant.  
219 The model fits in Figure. S1 show that W(VI) adsorption rates on different sorbents  
220 follow the order Fh (19.9) > FhHA\_5 wt% C (17.3) > FhHA\_15 wt% C (11.5). This

221 observation shows that the W(VI) adsorption rate decreases for increasingly organic-  
222 rich minerals, and suggests that access to the adsorption sites on the organomineral  
223 surfaces is limited when Fh is coprecipitated with NOM.

224 Tungstate adsorption edge results are shown in Figure. 1. Over a wide pH range  
225 from 4 to 11, W(VI) adsorption decreases with increasing pH, in agreement with W(VI)  
226 adsorption trends observed for other mineral sorbent systems such as hematite (Sallman  
227 et al., 2018), birnessite, gibbsite, goethite, montmorillonite (Iwai and Hashimoto, 2017),  
228 boehmite (Hur and Reeder, 2016), iowaite (Cao et al., 2019) and pyrite (Cui et al., 2017).  
229 A reverse adsorption edge is expected for adsorption of W(VI) oxyanionic species on  
230 Fh, as with a  $pH_{pzc}$  between 7-9 (Schwertmann and Fechter, 1989). The surface  
231 adsorption sites become increasingly negatively charged with increasing pH, therefore  
232 increasing the repulsive force between the adsorbing ions and the mineral surface.  
233 Results show that humic acid inhibits the adsorption of W(VI) to Fh, and the inhibitory  
234 effect of HA increases with increasing HA concentration. This phenomenon is reported  
235 for the adsorption of metal cations onto iron (hydr)oxide organominerals (Moon and  
236 Peacock, 2012; Du et al., 2016; 2018a; 2018b; Otero-Fariña et al., 2017; Woodward et  
237 al., 2018), but is less commonly investigated for oxyanions (Xue et al., 2019).

238 Tungstate adsorption isotherms are adequately described by the Langmuir model  
239 ( $R^2$  values  $\geq 0.92$ ) (Fig. 2, Table S1). The Langmuir parameter  $Q_{max}$  (mmol/kg) is the  
240 maximum adsorption capacity;  $K$  (L/mol) is the binding energy constant, and greater  $K$   
241 values indicate a higher affinity between W(VI) and the sorbent (Sparks, 2002). Results  
242 show that the Fh-HA binary composites have lower  $Q_{max}$  tungstate adsorption capacities

243 (857-1272 mmol/kg) than pure Fh (1847 mmol/kg) and moreover, that the binding  
244 affinities ( $K$ ) for W(VI) adsorption to the Fh-HA binary composites are lower than that  
245 for pure Fh (Table S1). These two aspects together indicate that increasing  
246 concentrations of NOM associated with iron (hydr)oxide increasingly inhibit W(VI)  
247 adsorption to organomineral surfaces.

248

### 249 **3.2 Molecular W(VI) adsorption characteristics**

250 X-ray photoelectron spectroscopy is a powerful surface analysis technique, providing  
251 valuable information about the elemental composition and local chemical environments  
252 of adsorbed species, and therefore offers W(VI) molecular binding information for  
253 W(VI) adsorption on Fh and Fh-HA surfaces. Figure 3 shows the O 1s XPS spectra of  
254 the Fh and Fh-HA composite before and after the adsorption of W(VI). In general, the  
255 O 1s peaks at ~531 eV become broader after the binding of W(VI) for both the Fh and  
256 Fh-HA composite. The O region can be decomposed into three components: oxygen in  
257 the crystal lattice of Fh (Fe-O-Fe), ~530 eV; oxygen on the surface of Fh, ~531 eV, and  
258 oxygen in the adsorbed water molecules, 532.6 eV (Xue et al., 2019). For pure Fh, the  
259 component at ~531 eV increases from ~29% to ~40% after W(VI) adsorption; for the  
260 Fh-HA binary composite, this increment is ~9%. These spectral changes suggest that  
261 the surface hydroxyl groups of the Fh and Fh-HA composite interact with the W(VI)  
262 oxyanion species, likely forming inner-sphere type complexes in which one or more of  
263 the O atoms in the W(VI) oxyanion are exchanged with O atoms of Fe-OH surface  
264 adsorption sites. Using EXAFS, similar inner-sphere type adsorption complexes on

265 boehmite ( $\gamma$ -AlOOH) were also found by Hur and Reeder, (2016; 2018). The smaller  
266 increase in the  $\sim$ 531 eV component before and after adsorption for the Fh-HA binary  
267 composite is likely due to the smaller amount of W(VI) adsorbed to the composite,  
268 compared to Fh, as observed in the batch adsorption results above.

269 The W (4f, 5p) higher resolution XPS spectra in Figure. 4 also clearly show the  
270 presence of W associated with the Fh and Fh-HA composite after adsorption, and the  
271 peak intensity is more pronounced for pure Fh (blue line), which again agrees with the  
272 smaller amount of W(VI) adsorbed to the composite, compared to Fh. Importantly, the  
273 W 4f<sub>5/2</sub> and W 4f<sub>7/2</sub> peak binding energies shift from 37.9 eV and 35.6 eV for the W-  
274 loaded Fh to 37.6 eV and 35.0 eV for the W-loaded Fh-HA, respectively. These  
275 observations suggest that the oxidation state of some proportion of the adsorbed W(VI)  
276 is reduced during binding to the Fh-HA composite. In order to evaluate the contribution  
277 of oxidized W(VI) and reduced W to the total adsorption, a typical peak (W 4f<sub>7/2</sub>, 34-  
278 37 eV) for W-loaded Fh-HA can be decomposed and fitted into two peaks (Fig. 4): one  
279 located at  $\sim$ 35.0 eV, which is assigned to W<sup>6+</sup>, accounting for  $\sim$ 60% of the total adsorbed  
280 W, and one located at  $\sim$ 35.6 eV, corresponding to W<sup>5+</sup>, and accounting for  $\sim$ 40% of the  
281 total adsorbed W species (Xie et al., 2012; Yang et al., 2018). Results therefore suggest  
282 that the presence of NOM at iron (hydr)oxide surfaces reduces a significant proportion  
283 of W(VI) to W(V) during adsorption.

284 To investigate whether complexation occurs between the HA fraction of the Fh-  
285 HA composites and W oxyanions. The C 1s XPS peaks (Fig. S2) can be decomposed  
286 into three components, C<sub>x</sub>H<sub>y</sub> ( $\sim$ 284.6 eV), C-O ( $\sim$ 286.0 eV) and COO ( $\sim$ 288.5 eV)

287 (Schild and Marquardt Christian, 2000). Results show an increase of the C-O fraction  
288 from 9.4% to 24.6% after the adsorption of W(VI). This increased peak intensity  
289 suggests there is complexation between W and HA, such that this new species  
290 contributes to the C-O peak intensity. Overall, our W and C XPS results show that W  
291 oxyanions form complexes with both the Fh and HA adsorption sites present in the Fh-  
292 HA binary composite, and this process is also accompanied by the reduction of ~40%  
293 of the W(VI) to W(V).

294 Attenuated total reflection Fourier transform infrared spectra were also adopted to  
295 further evaluate the molecular interaction of W(VI) with the Fh and Fh-HA composite  
296 (15 wt% C) at different pHs 4.5, 6.5 and 8.5. The most characteristic peaks for adsorbed  
297 W species occur between 700~1000  $\text{cm}^{-1}$  (Sallman et al., 2018). As shown in Figure. 5,  
298 one strong peak at ~930  $\text{cm}^{-1}$  and one broad peak at 810  $\text{cm}^{-1}$  are observed,  
299 corresponding to the symmetric and antisymmetric stretching modes of W-O vibrations,  
300 respectively (Sallman et al., 2018). This confirms that the adsorption of W on Fh and  
301 Fh-HA surfaces occurs via a strong inner-sphere type surface complexation of W(VI)  
302 with surface O atoms. The band intensities increase with decreasing pH, owing to the  
303 decreased amount of W adsorbed. However, the spectra show some changes in the shape  
304 of the IR peak at ~810  $\text{cm}^{-1}$  (Fig. 5). Specifically, for W-adsorbed Fh samples at pH 6.5  
305 and 4.5, and all W-adsorbed Fh-HA composite samples, the IR peak broadens towards  
306 higher frequencies. Interestingly, the W-O-W stretching vibrations, which are  
307 characteristic of polymeric tungstate species can appear at ~860–880  $\text{cm}^{-1}$  (Davantès et  
308 al., 2016; Rakshit et al., 2017; Tribalis et al., 2014). Results therefore suggest the

309 presenece of poly tungstate species on Fh and Fh-HA at  $\text{pH} \leq 6.5$ . Moreover, the  
310 polymerization appears to be more pronounced at lower pH and in the presence of NOM,  
311 as evident from the spectra differences in Figure 5.

312

### 313 **3.3 Thermodynamic adsorption characteristics**

314 To gain a deeper insight into the fundamental driving mechanisms for W adsorption,  
315 ITC was performed to obtain the thermodynamic parameters describing W(VI)  
316 adsorption on the Fh and Fh-HA composite. Figure 6 shows that W(VI) adsorption onto  
317 the both Fh and Fh-HA composite is an exothermic process. The peak amplitudes and  
318 areas gradually decrease as more W(VI) is added, most likely due to a decrease of  
319 available adsorption sites as added W(VI) is taken up. The adsorption trend of W(VI)  
320 on pure Fh is strikingly different from those on the Fh-HA composite. For pure Fh,  
321 continued releases of heat are detected for the first 10 injections, after which there is a  
322 relatively gradual decline; for FhHA\_5%C, the first 5 injections produce comparable  
323 amounts of heat, but then heat flow decreases sharply; while for FhHA\_15%C, the  
324 released heats decrease almost linearly over the whole titration period. Moreover, the  
325 total heat produced follows the order of  $\text{Fh} > \text{FhHA}_5\% \text{C} > \text{FhHA}_{15}\% \text{C}$ . These  
326 observations corroborate the batch adsorption, spectroscopic and thermodynamic  
327 results, that more W(VI) is adsorbed on pure Fh than on Fh-HA composites

328 The Gibbs free energy (ranges from -20.64 to -14.31 kJ/mol) in Table 1 shows that  
329 the binding of W(VI) on the Fh and Fh-HA composites is a spontaneous process ( $\Delta G <$   
330 0), particularly for pure Fh. Moreover, the  $K_a$  values imply that pure Fh exhibits a higher



331 affinity for W(VI) than Fh-HA binary composites. When looking at the enthalpy, results  
332 show that W-Fh interaction gives rise to a larger enthalpy change (16.1 kJ/mol)  
333 compared to the W-Fh-HA interactions (10.2-15.43 kJ/mol). These findings also  
334 corroborate that W(VI) adsorption is suppressed in the presence of HA. The entropy  
335 changes ( $\Delta S$ ) can further provide information on the coordination environments of the  
336 adsorbed W oxyanions, i.e., inner-sphere complex formation commonly generates a  
337 positive  $\Delta S$  while outer-sphere complex formation produces a negative  $\Delta S$  because the  
338 former displaces solvating water molecules from the adsorption coordination sites,  
339 whereas the latter does not (Nancollas, 1970; Gorman-Lewis et al., 2006; Du et al.,  
340 2017). Our  $\Delta S$  data (12.96-15.03 J/mol/K) therefore provide clear evidences for the  
341 formation of inner-sphere type of W species on Fh and Fh-HA surfaces.

342

#### 343 **4. Discussion**

344 Adsorption onto mineral surfaces is an important process controlling tungsten mobility  
345 and thus the eventual fate of natural and anthropogenic tungsten in soils, sediments and  
346 aquatic systems. However, the ubiquitous existence of natural organic matter (NOM) is  
347 known to significantly influence the adsorption process of many metals because NOM  
348 strongly interacts with mineral phases, giving rise to a change in the mineral surface  
349 charge and/or number and type of reactive surface adsorption sites, and thus the  
350 interaction of mineral surfaces with natural and contaminant metals. This study  
351 represents a scenario in which tungstate oxyanion species occur in natural environments  
352 where iron (hydr)oxides are associated with NOM. Results show, for the first time, that

353 the presence of NOM coprecipitated with iron (hydr)oxide at environmentally  
354 representative concentrations of NOM (~5 wt% and 15 wt% OC) inhibits the adsorption  
355 of W(VI) to the resulting organominerals over a wide pH range (4-11) at both  
356 environmentally representative (~5 wt% OC) and high level (15 wt% OC) of NOM. In  
357 this way, natural organic matter can act to increase the mobility of tungsten in the  
358 environment. Several explanations for this phenomenon are possible, notably: 1) it is  
359 well known that NOM can decrease the specific surface area and pore volume of Fh  
360 (Mikutta et al., 2014), which likely reduces the number and density of surface  
361 adsorption sites available for tungsten uptake; 2) it is also observed that NOM can  
362 competitively adsorb to iron (hydr)oxides via ligand exchange of the carboxylic and  
363 phenolic functional groups with Fe-OH (Du et al., 2018b; Oren and Chefetz, 2012;  
364 Chen et al., 2014; Mikutta et al., 2014), thus reducing the number of surface adsorption  
365 sites available for tungsten uptake; 3) the Fh surface is known to undergo changes in  
366 surface charge (Moon and Peacock, 2012; Du et al., 2018a, b), and in particular the  
367  $pH_{PZC}$  is known to significantly reduce such that the surface adsorption sites become  
368 more negatively charged when coated with NOM (Xue et al., 2019), which likely  
369 enhances electrostatic repulsion between tungstate oxyanions and surface adsorption  
370 sites; and 4) results here show that NOM promotes the formation of poly tungstate  
371 species (shown in ATR-FTIR) which have a lower affinity towards the adsorbent  
372 surfaces (Sun and Bostick, 2015). It is notable that the inhibitory effect of NOM on  
373 W(VI) adsorption is not equal over the whole pH range, and instead decreases with  
374 increasing pH. This can be explained by that fact that NOM binding to iron (hydr)oxide

375 is strongly pH dependent, with favorable adsorption at acidic or slightly acidic pH  
376 conditions (Davis, 1982; Murphy et al., 1992; Gu et al., 1994). With increasing pH, the  
377 binding affinity between NOM and iron (hydr)oxide decreases, and as such the  
378 inhibitory effect, as a result of the four reasons outlined above, also decreases. Moreover,  
379 our ATR-FTIR results show clearly the presence of polymeric tungstate species on Fh  
380 surfaces, in particular at pH 4.5. And also because polymeric tungstate species have  
381 lower adsorption affinities for mineral surfaces than tungstate monomers (Sun and  
382 Bostick, 2015), therefore, the inhibitory effect of NOM on W(VI) adsorption is more  
383 pronounced at lower pH.

384 Natural organic matter in the form of humic acid not only inhibits the retention of  
385 tungstate to Fh, but also results in the reduction of a significant proportion (~40%) of  
386 adsorbed W(VI) to W(V). This reductive phenomenon is likely due to the fact that HA  
387 normally contains a variety of reductive functional groups, including substituted  
388 phenols,  $\alpha$ -hydroxyl carboxylic acids, oxalic acid and  $\alpha$ -carbonyl carboxylic acids,  
389 which are capable of reducing high-valence metals, with previous studies showing that  
390 NOM can reduce Cr(VI) (Elovitz and Fish, 1995; Jiang et al., 2014), Pu(V) (André and  
391 Choppin Gregory, 2000), Vanadium(V) (Wilson and Weber, 1979) and Np(V) (Zeh et  
392 al., 1999), to lower valence species. The reduction of W(VI) to W(V) at iron (hydr)  
393 oxide organomineral surfaces could significantly change the stability and thus the  
394 mobility properties of tungsten in natural environments, compared to that predicted  
395 using pure iron (hydr)oxide adsorbents. Although the humic acid sample used in this  
396 study may not be representative of all natural NOM, general rules on the effects of

397 NOM on tungsten adsorption, speciation and resulting mobility are still highly  
398 applicable because both humic acid and NOM are known to be abundant in similar O-  
399 containing functional groups. Hence, our results indicate that NOM can facilitate the  
400 mobility of dissolved tungsten oxyanionic species, especially at acidic to mildly acidic  
401 pH, and can promote the reduction of adsorbed tungstate to lower valence species,  
402 which likely have different affinity for the organomineral surfaces and thus may  
403 similarly contribute to tungsten mobility in soils, sediments and aquatic systems.  
404 Overall, both NOM and iron (hydr)oxides coated with NOM should be considered in  
405 the prediction of tungsten mobility in the environment.

406

## 407 **5. Conclusions**

408 In this study, we examine the adsorption of W(VI) on ferrihydrite in the absence and  
409 presence of HA over a range of environmentally relevant W(VI) concentrations,  
410 ferrihydrite-HA organomineral couplings and pH values. Results reveal HA inhibits  
411 W(VI) uptake to ferrihydrite, with increasing inhibition observed with increasing HA  
412 association with the ferrihydrite surfaces, and in particular at acidic to mildly acidic pH.  
413 Kinetic results reveal that the adsorption rate of W(VI) on ferrihydrite is decreased in  
414 the presence of HA. XPS analysis confirms the formation of W surface complexes on  
415 both the ferrihydrite and HA fraction of the organominerals and the presence of HA  
416 reduces a significant fraction (~40%) of adsorbed W(VI) to lower valence W(V). Poly  
417 tungstate species are observed on ferrihydrite and ferrihydrite organomineral surfaces,  
418 particularly at lower pH and in the presence of HA. The adsorption of W(VI) to

419 ferrihydrite and ferrihydrite-HA composite is an energetically favourable process both  
420 in terms of the exothermic heat exchange and increase in entropy experienced during  
421 adsorption. The results presented here reveal that natural organic matter is a key factor  
422 influencing the sequestration and speciation (oxidation state) of tungstate at natural iron  
423 (hydr)oxide surfaces, and therefore that organomineral composites, in addition to pure  
424 mineral phases, must be considered when modeling tungsten mobility and fate in  
425 natural environments.

426

#### 427 **Acknowledgements**

428 We acknowledge the National Natural Science Foundation of China (41907015), China  
429 Postdoctoral Science Foundation (2019M662782), Scientific Research Fund of Hunan  
430 Provincial Education Department, China (18B120), and the Royal Society Newton  
431 Mobility Grant (No. IE151033) for financial support. We acknowledge the help from  
432 Prof. Qiaoyun Huang, Chenchen Qu, Mingkai Ma and Ding Liang (Huazhong  
433 Agricultural University) for ITC.

434

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**Table 1.** Adsorption calorimetry parameters for W(VI) adsorption on ferrihydrite (Fh) and ferrihydrite-HA composites at pH 6.5 and 0.01 M ionic strength.

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	$\Delta G$ (kJ/mol)	$\Delta H$ (kJ/mol)	$\Delta S$ (J/mol/K)	$K_a$ (M <sup>-1</sup> )
Fh	-20.64	-16.1	15.08	380
FhHA_5 wt.% C	-14.31	-10.12	13.93	312
FhHA_15 wt.% C	-19.33	-15.43	12.96	226

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641 **Figure Caption**

642 **Figure 1.** W(VI) adsorption edges (pH 4-11) on ferrihydrite (Fh) and ferrihydrite-HA  
643 composites (FhHA, 5 wt.%C and 15 wt.%C) at 0.01 M ionic strength.

644 **Figure 2.** W(VI) adsorption isotherms on ferrihydrite (Fh) and ferrihydrite-HA  
645 composites (FhHA, 5 wt.%C and 15 wt.%C) at pH 6.5 and 0.01 M ionic strength. Lines  
646 are Langmuir fits.

647 **Figure 3.** O (1s) XPS spectra of ferrihydrite and ferrihydrite-HA composite (FhHA\_15%  
648 C) before and after the binding of W(VI). The blue, red and green lines represent  
649 different O species at energies of ~529.9, 531.2 and 532.6 eV, respectively. The  
650 corresponding percentages (%) are shown in the brackets.

651 **Figure 4.** Tungsten (4f, 5p) XPS spectra of ferrihydrite and ferrihydrite-HA composite  
652 (FhHA\_15% C) before and after the binding of W(VI). The red spectrum in the range  
653 34.5-36.5 eV is divided into  $W^{5+}4f_{7/2}$  and  $W^{6+}4f_{7/2}$ .

654 **Figure 5.** ATR-FTIR spectra of sorbed W(VI) on ferrihydrite and ferrihydrite-HA  
655 composite (FhHA\_15% C) at fixed ionic strength (0.01 M NaCl) and varying pH values  
656 of 4.5, 6.5 and 8.5.

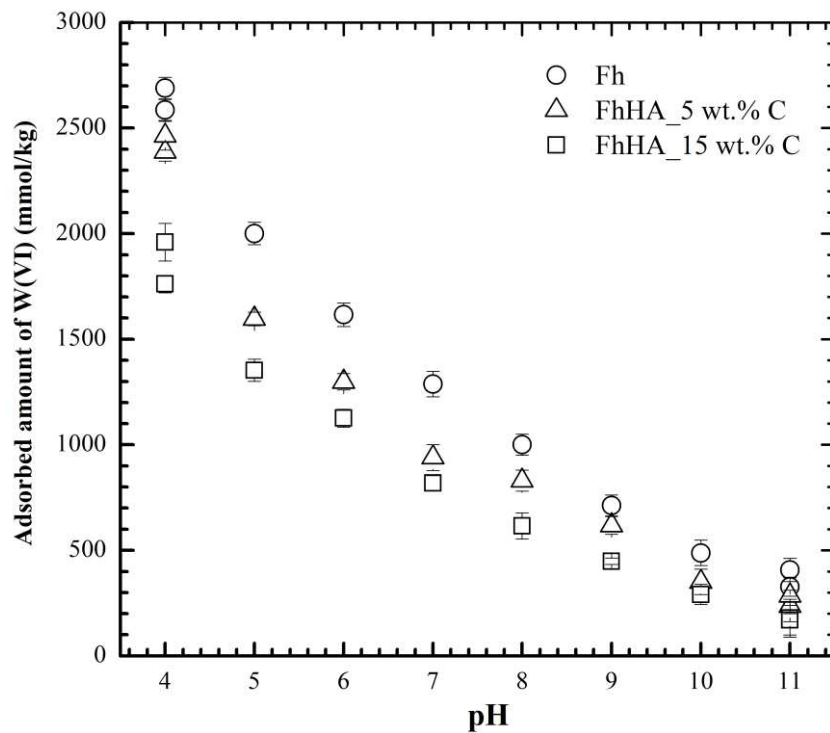
657 **Figure 6.** Isothermal titration calorimetry for W(VI) binding to ferrihydrite and  
658 ferrihydrite-HA composites (FhHA, 5 wt.%C and 15 wt.%C). The upper panels  
659 represent the raw heat flow ( $\mu$ W) *versus* time (s); the lower panels are the heat exchange  
660 ( $\mu$ J) *versus* per titration, each heat exchange is the integral heat of each peak in the  
661 upper panels; solid lines are the independent model fits.

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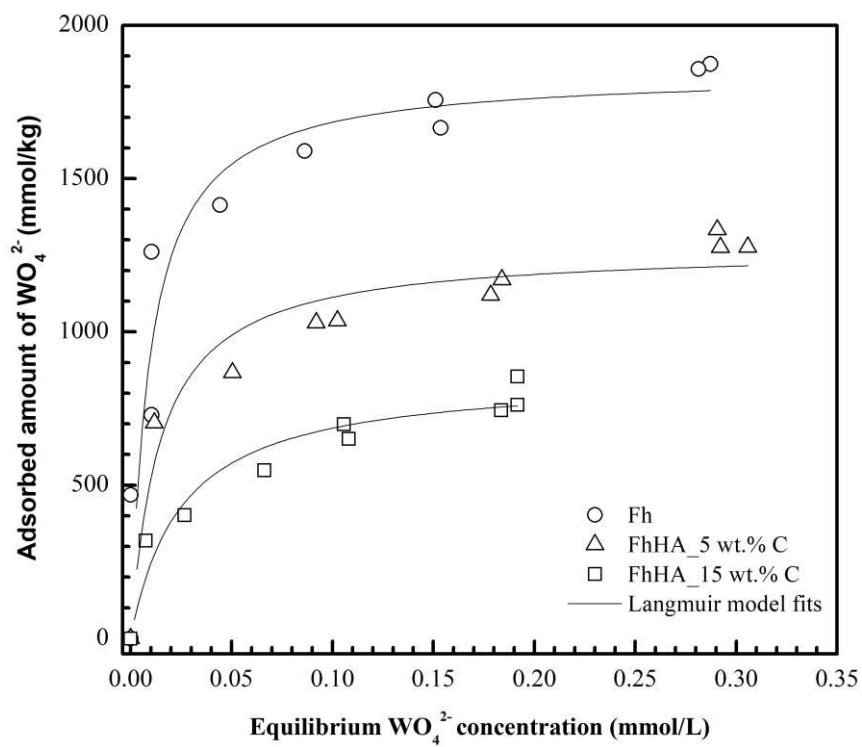
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**Fig. 1**



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**Fig. 2**



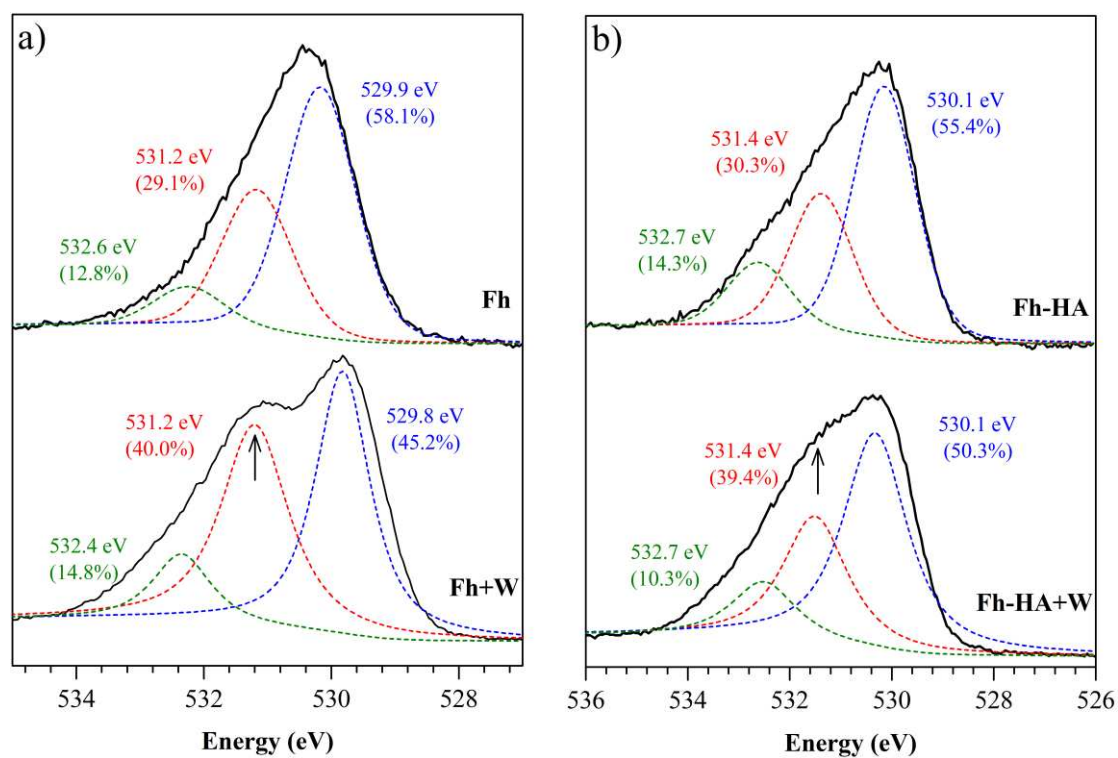
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Fig. 3

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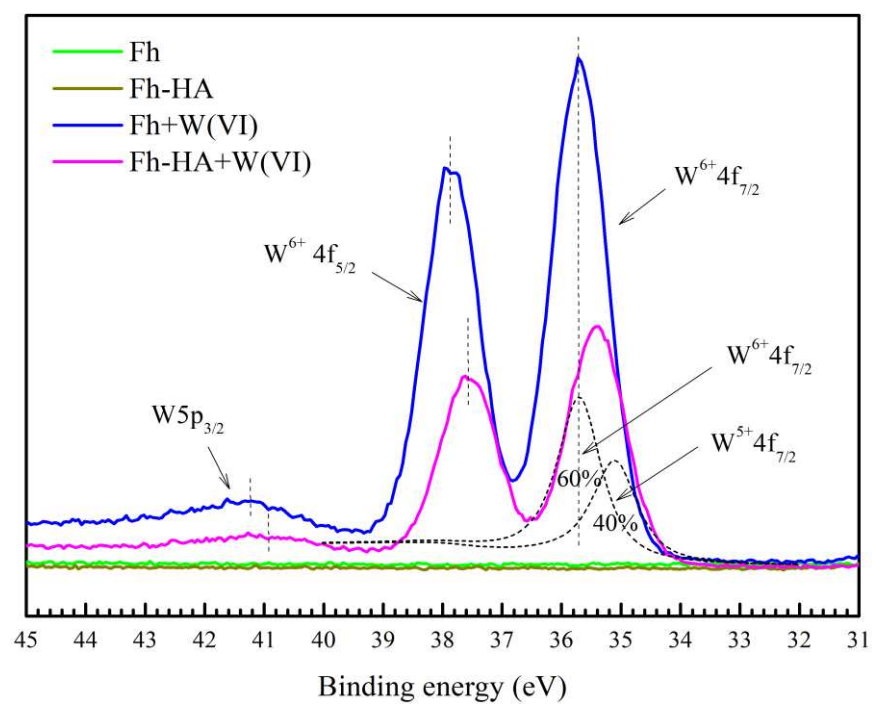
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Fig. 4

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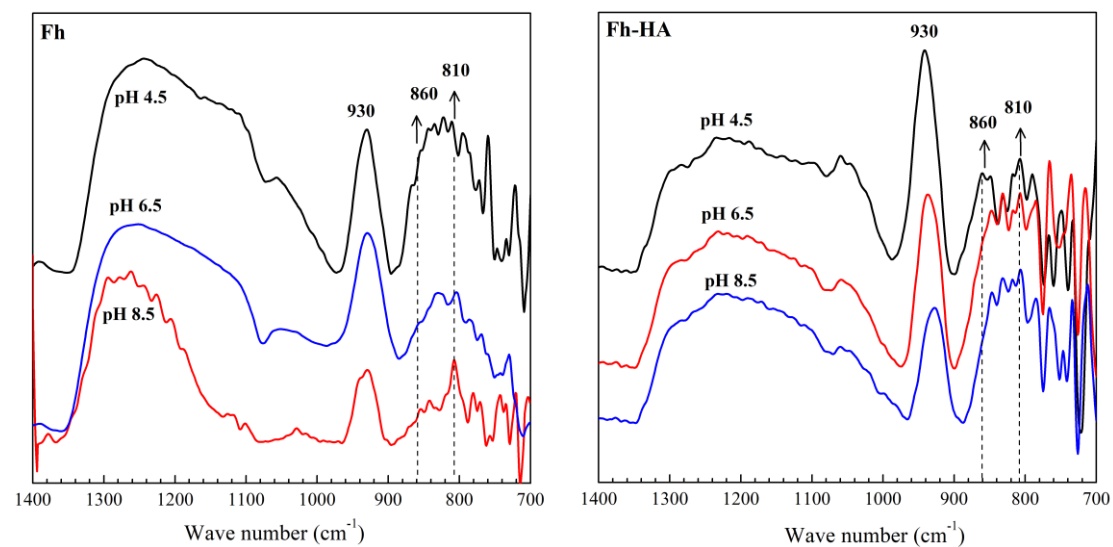
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**Fig. 5**

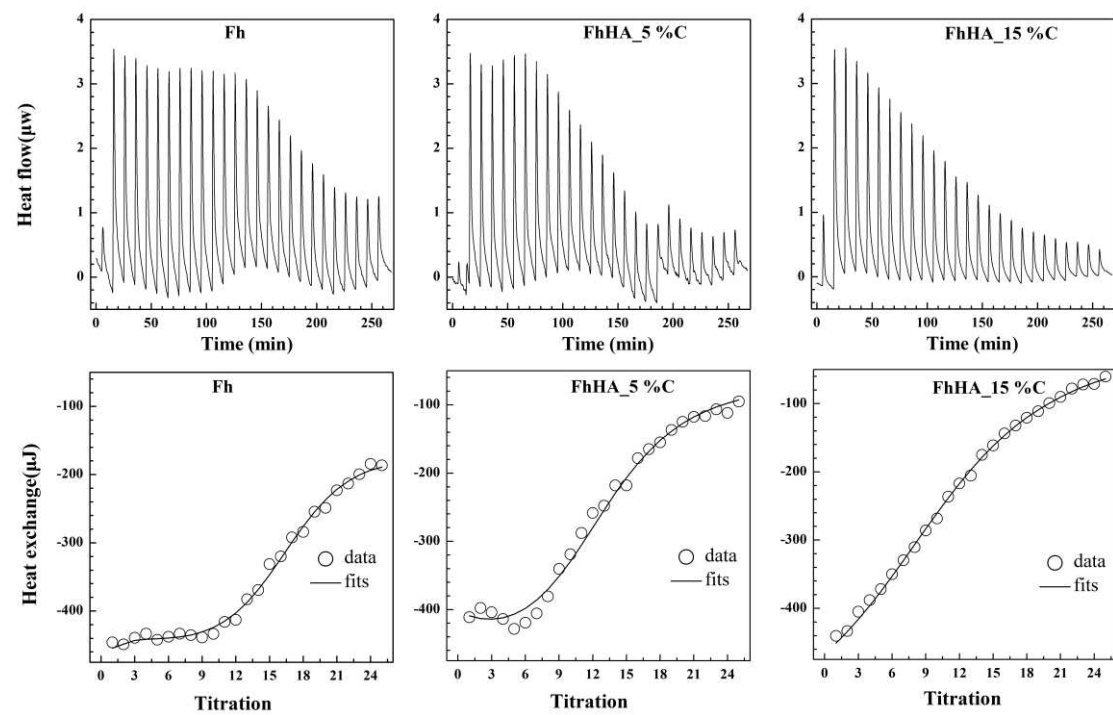


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**Fig. 6**



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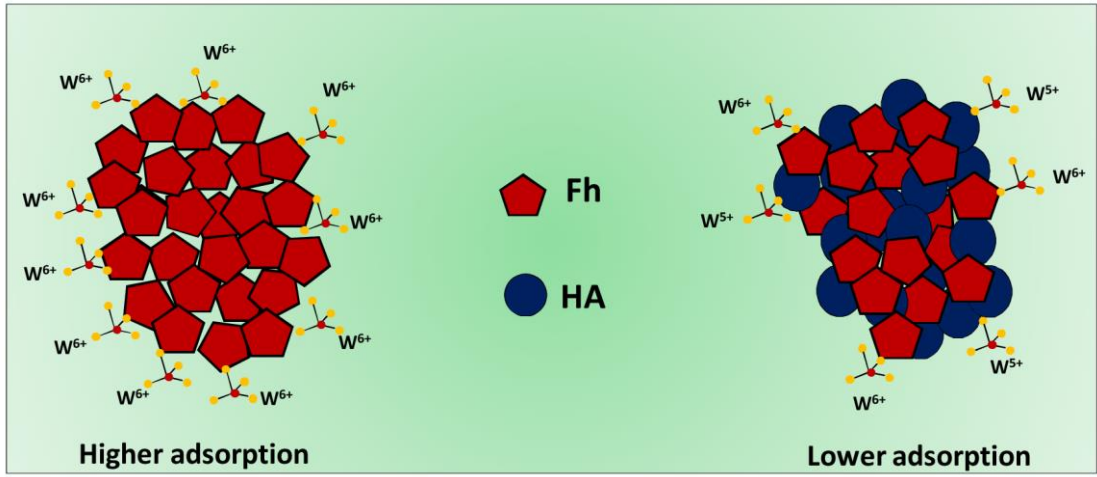
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**Graphical Abstract**



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