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Degradation of anthraquinone dyes from effluents: a review focusing on enzymatic dye degradation with industrial potential

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Abstract

Up to 84,000 tons of dyes can be lost in water and 90 million tons of water are attributed annually to dye production and their application, mainly in the textile and leather industry, making dyestuff industry responsible for up to 20% of the industrial water pollution. The majority of dyes industrially used today are aromatic compounds with complex, reinforced structures, with anthraquinone dyes being the 2nd largest produced in terms of volume. Despite the progress on decolourisation and degradation of azo dyes, very little attention has been given to anthraquinone dyes. Anthraquinone dyes pose a serious environmental problem as their reinforced structure makes them difficult to be degraded naturally. Existing methods of decolorisation might be effective but are neither efficient nor practical due to extended time, space and cost requirements. Attention should be given to the emerging routes for dye decolorisation via the enzymatic action of oxidoreductases, which have already a strong presence in various other bioremediation applications. This review will discuss the presence of anthraquinone dyes in the effluents and ways for their remediation from dyehouse effluents, focusing on enzymatic processes.

28 **1. INTRODUCTION – THE PROBLEM**

29

30 A very important factor of our life is water, as it is not only vital for our physical existence but
31 it is also necessary for numerous activities in domestic and industrial fields, varying from
32 cleaning and agriculture to cooking and product formation¹. Unsustainable exploitation and
33 uncontrollable contamination are currently the “hot issues” regarding water management. The
34 limited water resources need to be adequately distributed and carefully used to fulfil the
35 constantly rising agricultural and industrial demand due to population growth¹. The main
36 strategies to address water scarcity are prevention, demand management and revalorization of
37 water². Following that perspective, industrial wastewater should be recycled and reused.

38 The dye sector and the sectors relevant to dye applications (textile, tannery, paper) are
39 recognized among the most polluting industries, based on both the volume and the composition
40 of effluents^{3,4}. Effluents released in the water bodies create aesthetic and environmental issues
41^{5,6} with a high societal unacceptance. Furthermore, they can cause pipe corrosion, blockages
42 and bioaccumulation⁷, and result in the production of hazardous sludge⁷. The presence of
43 dyes in effluents makes their reuse difficult, as the presence of colour – and other substances –
44 affects consecutive dyeing cycles⁷.

45 Awareness of environmental protection has increased and minimization of water usage and
46 wastewater production is required, in addition to the limitation on the amount of pollutants
47 released to the environment. There are legislations regulating and monitoring the dyeing
48 industry in Europe and the United States^{8,9}, however these are not clearly defined and not
49 comparable across countries in regards to the colour intensity of the discharged effluents⁹.
50 These issues make the monitoring of coloured effluents released in the environment quite a
51 challenge. The problem of the dye contaminated water is especially evident in Asia, which
52 contributes to about 50 % of textile exports and more than 50 % of world’s consumption of

53 dyes. However, many of the countries involved lack sufficient legislation about environmental
54 protection relevant to textile industries¹⁰. Having said that, there have been efforts for colour
55 restrictions to be included in legislation⁷.

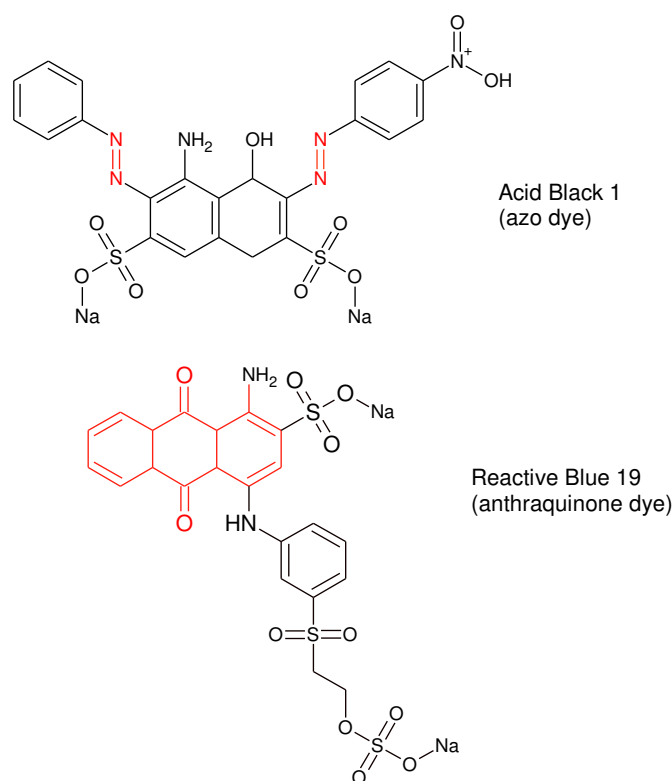
56 Although currently the relevant legislation might be vague and not properly applied¹¹⁻¹⁶, it is
57 clear that not only the volume of discharged effluents needs to be minimized, but the quality
58 of industrial effluents discharged in the environment needs to be fully monitored as well.

59 The dyeing and textile industry is responsible for dye discharge in the effluents, as well as for
60 a plethora of other hazardous and potentially hazardous substances. Such substances, mostly
61 surfactants and persistent organics, are used to accentuate dye stability/fastness or colour
62 intensity, to assist the process of dyeing and to give specific characteristics to textiles among
63 others^{3, 17}.

64 It is difficult to quantify the amount of dyes lost during production or during application on
65 textiles, as the available figures from the literature are based on estimations, or are
66 representative of very specific types of dyes or applications. Nevertheless, it is important to
67 discuss those data to understand the importance of the problem. Dye production may vary
68 between 10,000⁸ and 770,000¹⁸ tons per year and the losses are estimated around 2 % during
69 production and around 10 % during application⁷, with wastewaters being discarded directly
70 into the environment in developing countries¹⁹. Based on the data from 2013, the annual
71 production of textiles was around 30 million tons, increasing every year¹⁸. Each ton of textile
72 requires around 30 tons of water for the dyeing process¹⁰, while each ton of dye production
73 requires an average of 200 tons of water^{5, 20}. That means a total of 80 million tons and 90
74 million tons of water respectively is attributed to dye production and textile dyeing process of
75 per year. Taking into account the amount of contaminated water (2 % and 10 % respectively
76 during their production and application), a staggering sum of about 11 million tons of water is

77 polluted per year, making the dyestuff industry responsible for about 20 % of the total industrial
78 water pollution ²¹ . It is thus evident that water pollution from dyes is an existing and growing
79 problem that demands attention.

80 The majority of dyes industrially used today are aromatic compounds with complex, reinforced
81 structures, leading to difficult degradation ¹⁸ . Of the industrially important dye categories
82 (Figure 1), the most common “azo” dyes are making up of almost 60 % of the synthetic dyes
83 used industrially, followed by “anthraquinones” (15 %), and indigoids in respect of the
84 chromophore group present²².



85

86 *Figure 1:* Representation of the two most important chromophore groups, with examples shown being Acid
87 Black 1 (azo dye) and Reactive Blue 4 (anthraquinone dye).

88 While for azo dyes, relevant data is easily available, it is difficult to find current or accurate
89 data for the annual production of AQ dyes. Nevertheless, data found from previous years can
90 be used to roughly estimate a production volume. For the US, within a period of about 15 years
91 (1986-2002), the annual production of anthraquinone (a precursor for dyes and other

92 chemicals) had a staggering 5,000 % increase (from 500 to 25,000 tons)²³. Given the increase
93 in production volume of dyes, it is safe to assume that the production of AQ dyes increased as
94 well; a rough estimation of about 100,000 tons of AQ dyes per year can be made.

95 The specific chemistry of the anthraquinone group is based on the anthracene and consists of
96 three fused benzene rings (basic anthracene structure) with two carbonyl groups on the central
97 ring (highlighted in Figure 1). This structure is naturally colourless, but substitution of the
98 aromatic rings gives colour and controls its intensity²⁴. Colour gets deeper with increased
99 basicity of the substituents, for an aniline-based substituent (NHC₆H₅) is used, the maximum
100 absorption length rises to from 327nm (case of H) to 508nm²⁴.

101 The difference from azo dyes is that in the anthraquinone structure, the carbonyl group acts as
102 an electron acceptor, thus requiring an electron donor to react and break their structure⁵. This
103 combined with resonance effects among the anthracene structure leads to higher difficulty in
104 AQ dyes degradation compared to azo dyes^{19, 25} and makes the choice of an appropriate
105 degradation/decolorisation method challenging²⁶. The majority of the industrially important
106 AQ dyes are derived from anthraquinonesulfonic acids, using sulfonation or nitration²⁷, and
107 research has shown that presence of sulfone groups in dye structure can reduce their
108 degradability²⁸. Due to their highly stable structure, AQ dyes are known for their great fastness,
109 stability and brightness²⁴.

110 **2. AVAILABLE METHODS FOR DECOLORISATION**

111 **2.1. Industrially available methods**

112

113 The most known and extensively applied methods in the industry are adsorption, coagulation,
114 membrane filtration, as well as various oxidative processes^{10,29}. Regarding biological methods,
115 aerobic and anaerobic processes are currently widely applied for general water treatment,
116 offering distinct advantages compared to physicochemical methods (e.g. products of added

117 value, environmentally friendlier), but also facing challenges regarding their efficiency (e.g.
118 sensitivity, long contact time)²⁹. There are many examples of papers reviewing the current and
119 future industrial methods for general dye decolorisation^{3, 8, 30-34}. Every method has advantages
120 and disadvantages related to the following criteria: efficiency under various conditions,
121 practicality, requirements of pre- and post-treatment and environmental impact; ultimately
122 relating to the cost. Given this complexity, a single method can rarely satisfy these demands
123 simultaneously⁵, hence, typically, a combination of available and under-development methods
124 is preferred, maximizing their strengths and compromising their disadvantages^{17, 29}.

125 Despite the significant amount of research about the decolorisation and degradation methods
126 applied for azo dyes^{6, 35-39}, not much research is available on AQ dyes, with only two reviews
127 available, both discussing AQ dye decolorisation mainly by biological methods^{40, 41} and
128 comparably fewer research papers compared to those available on azo dyes^a. What is worth
129 mentioning, is that there is a review paper focusing on the degradation of a specific AQ dye,
130 reactive Blue 19, covering various methods and research examples dated up to 2011⁴².

131 **2.2. Physical, chemical and biological methods applied for AQ** 132 **dye removal** 133

134 The most common physical methods for treatment of dye house effluents are adsorption, and
135 filtration (using membranes and reverse osmosis). As there are numerous research studies on
136 dye removal assisted by adsorption, we have summarised the best performing literature
137 findings on AQ dye removal and degradation in Table 1, with associated comments, while
138 below we discuss selected examples. Best performance was arbitrarily evaluated based on the
139 amount of dye removed per litre, per hour, assuming continuous use of the system described at
140 the optimal state identified by the researchers. This arbitrary metric allows for a comparison

^a about 500 papers on anthraquinone dye degradation compared to about 8,700 for azo dyes, according to Web of Knowledge search engine over the period of 1975 to 2019.

141 between results found in literature, as given the lack of a consistent approach followed,
142 superficial comparison of results does not produce valuable conclusions.

143 **2.2.1. Physical methods**

144 Amongst many adsorbents explored such as activated carbon, peat, silica-based adsorbents,
145 zeolites or other naturally derived substances, activated carbon is widely studied for dye
146 adsorption. It is also the dominant adsorbent in industry, based on its great adsorption ability,
147 high surface area, stability and homogeneity⁴³, which compromise the high cost of production
148 and regeneration and the possibility of decreased efficiency due to material loss during
149 regeneration^{8,44,45}. A few examples using activated carbon for AQ dye adsorption showed that
150 uptake was higher for acidic solutions⁴⁶⁻⁴⁸, and that pore structure of the materials could
151 facilitate^{46,48} or hinder⁴⁷ adsorption. Another frequently discussed option in the area of
152 adsorption are the abundant in nature zeolites, with substantially lower adsorption capacity and
153 again facing high regeneration costs^{49,50}. Silicon based materials have been studied extensively
154 for pollutants adsorption as well^{51,52}. Their interesting properties such as ability for a wide
155 range of pore size and surface areas, durability, ease of functionalisation and relatively cheaper
156 regeneration compared to activated carbon, have made them excellent candidates for water
157 treatment with many examples on dye adsorption⁵³⁻⁵⁶. However, issues such as manufacturing
158 and regeneration cost as well as diffusional limitations arising from high throughput in
159 industrial scale applications, have prevented them from being widely applied in water treatment
160 yet, although research is showing positive signs on their industrial implementation⁵⁷. Newer
161 trends in adsorption, with application for AQ dyes, include the use of agricultural waste^{58,59}.
162 As per filtration, the usually encountered textile effluent treatments include nanofiltration (pore
163 diameter up to 10 nm) and reverse osmosis⁶⁰, but there was no example of their application on
164 AQ dyes found in literature.

165 Major issues about the application of physical methods for dye removal are the relatively high
166 required contact time, hence large spaces required, as well as the need for adsorbent (or
167 membrane) regeneration, issues that are not usually addressed in literature, but are of great
168 importance for industrial implementation.

169 **2.2.2. Chemical methods**

170 **2.2.2.1. Coagulation – Flocculation**

171 The most common chemical treatment methods applied to textile effluents are chemical
172 coagulation and oxidation processes, while electrochemical methods are gaining attention as
173 well (Table 1). Chemical coagulation or flocculation is being replaced by newer methods or
174 used in combination with other methods, in order to reduce the effect of some major drawbacks
175 such as potentially toxic sludge production and need for further treatment of the effluent ⁶¹.
176 The principle of coagulation and flocculation methods is the opposite charge between the
177 soluble pollutant (e.g. dye) and the usually aluminum, iron, or most recently polymeric
178 coagulant, that makes the pollutant become insoluble ⁶¹. The factors of importance during
179 coagulation are the type and dose of coagulant needed and the size and “sturdiness” of the
180 floccs (coagulated pollutants), which dominates their ease of removal ⁶². Table 1 summarises
181 some distinct examples of AQ dye treatment using chemical methods, while we elaborate on
182 relevant research below. When degradation of Reactive Blue 19 and 49, individually and in a
183 mixture, was attempted using active chlorine, it was shown that degradation was much faster
184 for individual dyes ⁶³. Contradicting these findings, decolorisation of Disperse Blue 3 via
185 coagulation with magnesium chloride or ferrous sulphate, as individual dye or in mixture with
186 azo dyes, showed that there is a synergistic effect. Dye removal increased from 68 %
187 (individual dye) to up to 90 % (mixture with azo dyes) in presence of ferrous sulphate, whereas
188 for magnesium chloride the decolorisation percentage was maintained very high, at 93 %,
189 regardless the presence of other dyes ⁶⁴.

2.2.2.2. Advanced Oxidation Processes (AOP)

190 The available oxidative methods include Fenton's process with or without external energy
191 supply, or ozonation, and they operate via the production of active OH⁻ radicals that non-
192 selectively oxidise dyes⁶⁵. Their application in water treatment has been illustrated recently²⁸,
193^{34, 65, 66} gaining much attention over the last few years. Selected stellar examples of AOP applied
194 for AQ dye degradation are shown in Table 1 and some of them are discussed below. Studies
195 on Reactive Blue 19 conducted by different groups, using the same starting concentration (100
196 mg/mL) but different combination of AOP, showed highly different results. It was shown that
197 using a combination of methods such as Fenton reaction coupled with adsorption on pyrite ash
198⁶⁷, or ozonation coupled with UV radiation⁶⁸ can be much more efficient compared to ozonation
199 only⁶⁹, based on the . Using the same dye on a much higher starting concentration (about 2,000
200 mg/L) and examining its decolorisation by Fenton's reaction, photocatalysis and UV radiation,
201 as single methods or combined, Radovic resulted in generally very high dye removal (above
202 90 % for a combination of Fenton reagent coupled with photocatalysis)⁷⁰. This shows that
203 combination of AOP methods does work synergistically, and usually better than single
204 methods. What is worth highlighting about AOP when applied in AQ dye degradation, is the
205 very short reaction times required, usually few minutes, their very good efficiency and
206 mineralisation of dye, but also their high cost, which poses difficulties on their consideration
207 for scale-up^{71, 72}.

2.2.2.3. Combination of methods

209 Emerging combinations of the once very popular chemical coagulation with newer dye removal
210 methods are implemented, in order to reduce the effect of some major drawbacks such as sludge
211 production and need for further treatment of the effluent⁶¹. Electrochemical coagulation
212 producing in-situ coagulants based on aluminium or iron, showed great dye removal potential
213 (Reactive Blue 19 was used as a representative AQ dye, but other dyes were studied as well)
214 and associated time⁷³. That work also presented an economic evaluation of some

216 decolorisation processes, which suggested that electrochemical and oxidative processes are
217 advantageous to adsorption, however, biological/enzymatic methods were not included.
218 Furthermore, what was only acknowledged but not commented further is sludge production
219 and the need to deal with it, but, it was shown qualitatively that use of different conditions can
220 have an effect on the amount and type of produced sludge. In the area of coupling
221 photocatalysis with nanoparticles, a study optimised the degradation of Acid Green 25 using
222 immobilised TiO₂ nanoparticles coupled with UV light photocatalysis, resulting at an
223 optimised system operating at a relatively low dye concentrations (18 mg/mL) ⁷⁴. The same
224 group examined the importance of the chemical structure of various dyes in degradation
225 through the same method ²⁸. Their critical review analysis showed that degradation of AQ dyes
226 was more difficult compared to azo dyes –without further elaboration on the differences
227 between the dye structures– and also that presence of sulfone groups reduces the efficiency of
228 dye degradation. The application of other nanomaterials for AQ dye degradation from effluents
229 is gaining more and more attention, although not yet thoroughly developed, but their potential
230 advantages lead to an increased interest for their industrial application ⁷⁵. A study coupling use
231 of zinc and titanium oxides with photocatalysis by irradiation, showed that nanoparticles can
232 be quite effective in degradation of a model AQ dye, but their efficiency depends on the type
233 ²⁵. A more recent study examined the degradation of Reactive Blue 4 based on the coupled use
234 of copper nanoparticles and showed that initially the dye gets adsorbed onto the nanoparticles
235 and then is oxidised based on the production of hydroxyl radicals from added mediators and
236 the action of monovalent copper ⁷⁶.

237 **2.2.3. Biological methods**

238

239 The available biological methods can be divided on whether they are performed inside a cell
240 (of bacteria, fungi, yeasts, algae), or using isolated enzymes. The challenge is to create methods

241 based on bioremediation that can bypass the disadvantages of conventional methods, yet be
242 efficient, cost-effective and environmentally benign^{77, 78}.

243 Degradation of AQ dyes using aerobic and anaerobic cultures has been reviewed recently^{40, 41},
244 so in Table S1 we report some newer (or unreported) examples on biological degradation of
245 AQ dyes. Some of the clear differences between research examples on biological and non-
246 biological methods include the usually low starting concentration of dyes examined and the
247 longer time needed for decolorisation in biological methods. Although usually individual
248 cultures are examined in research papers, a recent study⁷⁹ showed that when the
249 microorganisms were acting in a consortium, the decolorisation of Reactive Blue 4 and 19 was
250 dramatically improved. Another study⁸⁰ examined *Escherichia coli* cultures for degradation of
251 AQ dyes at higher concentration and found that dye decolorisation occurred primarily due to
252 microbial induced precipitation, followed by adsorption on cells and cell metabolism. A very
253 interesting observation was that the dye structure affected the decolorisation mechanisms and
254 the kinetics, indicating that this method might not be applicable in real effluents where a
255 mixture of dyes is present. When the degradation of a mixture of dyes was examined, (including
256 Acid Blue 350 of AQ structure) using a specific strain of *Trametes Versicolor*, over 90 %
257 degradation could be achieved for after 48 h of treatment, that being slightly lower to the almost
258 complete decolorisation achieved for the individual dyes⁸¹.

259 Upon comparison of the –arbitrary- throughput value calculated for the examples shown for
260 physical/chemical and biological methods, it is evident that biological methods cannot compare
261 in terms of efficiency with the chemical and physical methods examined. This leads to the
262 conclusion that biological methods might not be as effective as physical and chemical methods
263 However, biological methods are generally recognised as more benign, environmentally
264 friendly and economically viable, with the ability for in-situ degradation of pollutants,

265 compared to physical removal of the dye or transformation to other substances requiring further
266 treatment ^{82, 83}.

267 **2.3. Challenges with current methods**

268

269 Based on the data discussed and presented in Table 1, it is clear that AQ dye removal, is highly
270 specific to the dye and the method used. It has been shown that different degrees of
271 decolorisation are observed for a single dye when using different treatment methods ^{84, 85}. It
272 can be quite difficult to choose an appropriate method among the available conventional
273 methods to decolorise AQ dyes, due to their fused ring structure that enhances their stability
274 ⁸⁶. Although anthraquinone on its own is not toxic ²³, research has shown that some AQ dyes
275 as well as their degradation intermediates (often unidentified), can be potentially toxic, few of
276 them are mutagenic and/or potentially carcinogenic ^{26, 87-90}. Also the lack of data on the
277 intermediate degradation products ⁹¹ makes it difficult to speculate any residual toxicity, as
278 well as to find appropriate degradation pathways ²⁶. There are research examples where a
279 degradation pathway for a specific AQ dye has been proposed, based on collected data and in
280 few cases the pathway has been fully determined, usually using analytical techniques to
281 identify the by-products. This indicates that methods which can result in complete destruction
282 of the dye structure rather than isolation or coupling with other chemicals, are in need. In these
283 examples, anthraquinone dyes were degraded using ozonation ^{68, 69, 92, 93}, electrochemical
284 methods and their combinations ⁹⁴ or via enzymatic degradation ⁹⁵⁻⁹⁷. A discussion on the
285 degradation pathways on a model AQ dye by various techniques is available in Section 4.

286 We note that most studies examined a lower dye concentration spectrum, sometimes coupled
287 with quite a low concentration of adsorbent. These scenarios may be ideal for scanning a
288 method or optimizing the process conditions, but they do not give information on realistic
289 conditions of industrial applications and may cause barriers during commercialisation.

290 When using physical and chemical methods for dye removal, there is sludge generation, which
291 can be difficult to handle, as well as the materials used cannot be regenerated easily, if at all.
292 In addition some of these methods are not very efficient due to the large cost, time and space
293 requirements ¹⁰.

294 Existing literature on decolorisation of AQ dyes from water effluents, acknowledges the
295 problem and explores potential solutions, however, the lack of consistency on the way the issue
296 is approached highlights the need for an evaluation of proposed solutions on a consistent basis,
297 on the merit of the potential of industrial implementation and socially acceptable practices.

298

299 Table 1: Exceptional performance of decolorisation of anthraquinone dyes by various physical and chemical methods. Please refer to Table S1 for biological methods.

Decolorisation method	Dye name/ initial dye concentration (mg/L)	% max decolorisation * /timescale (h)	Throughput (mg/L/h)**	Comments	Ref.
Adsorption (activated carbon from <i>T. dealbata</i>)	Reactive Brilliant Blue X-BR / 150	About 81 % / 0.5	121.5	Pseudo second order kinetic model used, higher capacity than commercial carbon products)	46
Adsorption (on silica)	Reactive Blue 19 / 800	99 % / 4	198	Amount of silane affects decolorisation (the more the better) and elution of dye	55
Adsorption (on clay)	Acid Blue 25 /100	About 100 % / 1	100	Full material characterization and adsorption kinetics analysis, chemisorption dominates, lower pH facilitates adsorption	98
AOP (wet air, wet peroxide, photocatalytic, Fenton)	Reactive Blue 4 / 100	100 %, 100 %, 99 % / 1 and 100 % / 0.75	100	Very high degrees (>75 %) of mineralization, wet peroxide oxidation worked best, examination of degradation pathway	93
AOP (Photodegradation) + nanoparticles	Reactive Blue 19 / 30-70	Over 95 % / 0.5	126	Degradation based on ZnO and TiO ₂ nanoparticles assisted by photocatalysis, multifactorial design analysis and optimization, ZnO performs better (both cost of energy + dye degradation effect), TOC analysis shows low residual toxicity, activity of ZnO regulated only by pH	25
AOP (Photodegradation + TiO ₂)	Reactive Blue 19 / 800	About 75 % / 3	200	Examination of various factors affecting dye degradation such as dye, catalyst and peroxide concentration, identification of intermediate products through UPLC-MS, fragments show reduced cytotoxicity	99
AOP (ozonation)	Reactive Blue 19 / 200	Almost 100 % / 0.3	200	Ozone feed rate and presence of electrolytes affect decolorisation, identification of oxidation products through IC	100
AOP (Fenton reaction) coupled with Pyrite Ash	Reactive Blue 4 / 100	100 % /0.5	200	Coupled process enhances degradation due to enhancement of Fenton process reaction, high concentration of dye is prohibitive, metal removal is necessary	67
Ozonation and UV radiation	Reactive Blue 19 / 111	100 % / 0.1	1665	Ozonation is better for decolorisation, combination with UV radiation is better for mineralization, proposed degradation pathway, toxicity studies	68
AOP (Fenton/ photo-Fenton reaction), UV radiation	Reactive Blue 19/ 2500	81 %-98 %-42 %/ 0.3	1050-2450	Decolorisation examined in pure dye (higher) and simulated effluent (lower), AOPs are more effective than UV radiation, dye structure affects efficiency of each process, optimization study for each process	70
Electrochemical coagulation	Reactive Blue 19/ 2000	95 % /0.1	19000	Use of Fe (better action) and Al (can have reversed effect depending on pH) as coagulants, higher voltage increases removal percentage, overall quite fast method, no mention of proposed sludge treatment	73

300 * values shown are for the optimised methods as presented by researchers and refer to removal of colour unless stated otherwise.

301 ** arbitrary value calculated to show the maximum removal capacity of any given method within an hour, based on the best results presented in each reference. In cases where
302 the timescale of the decolorisation is within a few minutes, the assumption of decolorisation ability over continuous use for 1 h is made.

303 **3. FOCUS ON ENZYMATIC DECOLORISATION**

304

305 Isolated enzymes are very effective as they are highly specific catalysts that produce by-
306 products of lower toxicity and volume. The overall process is considered environmentally
307 friendly and less intrusive. The enzymes responsible for dye degradation belong mainly to the
308 family of oxidoreductases, including peroxidases, reductases and laccases ^{17, 101}. These
309 enzymes have the ability to act on dyes by either creating precipitants that can be easily
310 removed or chemically transforming the dyes into compounds easily dealt with ¹⁰².

311 The use of both isolated enzymes and the whole cell/micro-organism has considerable
312 advantages and disadvantages. Use of isolated enzymes does not depend on
313 culture/microorganism's "well-being" or growth rate ^{101, 103, 104}. Also, diffusional limitations of
314 substrate and/or product in-between the cell compartments can be avoided as well as any other
315 actions besides enzymatic ¹⁰⁵⁻¹⁰⁷. Isolated enzymes are relatively easier to use under harsher
316 conditions, offer higher specificity and easier regulation of catalytic activity, as well as easier
317 handling/storage compared to whole cells ^{8, 77, 108}. It is also easier to implement the use of
318 isolated enzymes in an industrial context since their development as biocatalysts can be faster
319 than whole cells. Further, recombinant enzymes and/or their immobilisation is possible to
320 improve the performance ¹⁰⁸⁻¹¹¹. On the other hand, some enzymes may require co-factors or
321 mediators ¹⁷ and may be too specific/selective to degrade multiple dyes simultaneously ^{108, 109}.

322 **3.1. Oxidoreductases – Peroxidases**

323

324 The enzymes responsible for dye decolorisation belong to the family of oxidoreductases (EC:
325 1), which catalyse oxidation and reduction reactions, finding application in various domains
326 varying from diagnostics to wastewater treatment and production of chemicals or potentially
327 biofuels ¹¹²⁻¹¹⁸. They have been studied extensively for dye decolorisation and bioremediation,

328 with much research focusing on the oxidative action of laccases and peroxidases as well as the
329 reductive action of azoreductases (azo dye specific enzymes), with many review papers
330 available targeting dye degradation in general^{104, 110, 119-121} or focusing on azo dyes^{6, 38, 39}, but
331 none focusing specifically on anthraquinone dyes.

332 Peroxidases catalyse the reduction of peroxides simultaneously with the oxidation of various
333 organic and inorganic substrates. This “dual action” mechanism has been named ping-pong bi
334 bi mechanism due to the fact that the electrons liberated by the enzyme from the reduction of
335 peroxides are recovered through the oxidation of the main substrate, with the aid of the
336 intermediate enzymatic compounds¹²².

337 Recently peroxidases from white-rot fungi (WRF) have attracted interest in the general area of
338 bioremediation^{84, 104}, as actions such as lignin degradation and dye degradation are dominated
339 by similar mechanisms, around structurally similar substrates^{123, 124}. The advantage of non-
340 specific binding of WRF peroxidases allows them to act on a wide range of substrates^{125, 126}.
341 Enzymes secreted from WRF include various known peroxidases, like manganese, lignin and
342 versatile peroxidase and a less known category of enzymes, dye decolorising peroxidases
343 (DyPs). DyPs were first reported almost 20 years ago, showing a great activity over the
344 decolorisation of anthraquinone dyes^{97, 127}, followed by lignin-like compounds¹²⁸. Although
345 their action mechanism resembles that of other peroxidases, anthraquinone dye degradation is
346 not yet fully mapped¹²⁹⁻¹³⁴. The characterization of DyPs can be found in recent reviews<sup>135-
347 138</sup>. Anthraquinone dyes used as a model system to examine decolorisation using DyPs include
348 Reactive Blue 19 (RB19 or RBBR)^{129, 139-143} and Reactive Blue 5 (RB5)^{97, 130, 144-151}.

349 **3.2. Oxidoreductases in enzyme-based bioremediation**

350

351 There are quite a few examples of isolated oxidoreductases applied in dye degradation and
352 decolorisation, some of them focusing on anthraquinone dyes (Table 2). Focusing on DyPs,

353 there are many research examples qualitatively examining their activity on anthraquinone dyes
354 and a few researchers have tried to consider an industrial implementation. For example,
355 recombinant DyP was used to treat Reactive Blue 19 in a single batch system and also in a step
356 fed batch reactor ¹⁰⁷ to assess a cyclic operation, leading to a very high decolorisation
357 performance, regardless the soluble nature of the enzyme. However, a major concern for
358 industrial application is the continuous ingress of effluents that can make batch treatment
359 tricky. Another study tested free horseradish peroxidase on a single anthraquinone dye and a
360 real effluent. The results showed that although single dye degradation was very fast and
361 effective (90 % within 2 mins), only 52 % decolorisation was achieved for the real effluent
362 (undefined period of time) ¹⁵². Research conducted using again horseradish peroxidase for the
363 decolorisation of 2 anthraquinone dyes, showed that the structure of the dye affected its
364 decolorisation, despite the similar optimised operational conditions and the high decolorisation
365 degrees achieved ¹²². When laccase was examined for dye decolorising potential on several
366 types of dyes, it was shown that there was better affinity towards the anthraquinone Reactive
367 Blue 19, resulting in almost 90% decolorisation over 30 mins¹⁵³. The preference of laccase
368 towards anthraquinone dyes compared to other types was also confirmed by a different study,
369 where complete decolorisation of the same dye concentration was achieved in the much higher
370 time point of 72 h ¹⁵⁴. However, whereas in the aforementioned cases laccase did not need a
371 mediator, this has not been always the case. Soares ¹⁰³ used laccase for the decolorisation of
372 Reactive Blue 19 and reported that in absence of mediator almost no decolorisation was
373 observed, but upon use of mediators decolorisation was able to reach 100 % success. The
374 different results obtained by the same combination of enzyme and dye allows us to understand
375 the complexity of decolorisation and the difficulty to generalise results and expectations. When
376 degradation of a mixture of 3 azo and 1 anthraquinone dye was examined using isolated enzyme
377 extracts from *Funalia Frogii*, it was shown that degradation of dyes in the mixture followed a

378 pattern based on the ease of structure breakdown. Once the Reactive Blue 69 anthraquinone
379 dye (easiest to degrade) was almost fully degraded, degradation of the other dyes would occur,
380 leading to a time dependant decolorisation and resulting to 84 % colour removal after 48 h ¹⁵⁵.

381 Although enzyme use in dye degradation specifically can be quite effective under laboratory
382 conditions, their application to an industrial scale has many limitations, mainly due to the
383 production cost (culture, isolation, equipment) and operational cost (use/reuse, downstream
384 processing) of the enzymes ^{29, 112, 156-158}. Also, some of the by-products can inhibit the
385 enzymatic action ^{146, 159, 160}, thus limiting potential reusability of the enzymes. Furthermore, as
386 the pH for enzymatic action is important, difficulties can occur when treating real effluents as
387 it was shown in literature ^{152, 161, 162}.

388 There are mainly three ways to address the aforementioned limitations from isolated enzyme
389 use, which can be applied alone or together. The “invasive” way is altering the properties of
390 the enzyme via genetic engineering. The “excluding” way is screening for new, better enzymes.
391 The “external improvement” way refers to the improvements and optimization of the process
392 and enzyme ^{109, 163}, e.g. immobilisation, optimization of reactor configurations and design of
393 effective downstream processing. In order for isolated enzymes to become applicable for water
394 treatment of industrial potential, they have to be immobilised. Even if enzymatic action has
395 been improved via genetic engineering and screening, the production cost of “optimised
396 enzyme” can be inhibitory for application at industrial scale, without the option of reuse.
397 Hence, even after overcoming limitations through the invasive or the exclusive way, external
398 improvement –usually via immobilisation– needs to be applied. In the next section we shed
399 light on the applicability of immobilisation, focusing on immobilised oxidoreductases and their
400 application for dye removal.

401 Table 2: Decolorisation of anthraquinone dyes by isolated enzymes

Decolorisation method	Dye name/ initial dye concentration (mg/L)	% max decolorisation* /timescale (h)	Throughput (mg/L/h)**	Comments	Ref.
Horseradish peroxidase	Reactive Blue 19 / 120	96 % / 0.1	115.2	Better results shown for anthraquinone dyes compared to other types, reduction of toxicity after degradation	106
Horseradish peroxidase	Remazol Blue / 1000	35 % / 9	38.8	Inactivation of enzyme due to dye concentration, precipitation can occur depending on dye	164
Horseradish peroxidase	Lanaset Blue 2R/ 10-100	90 % / 0.033	270-2700	Very good decolorisation of single anthraquinone dye, examination of enzyme performance on real effluents (see discussion), examination of 2 bioindicators on toxicity of effluents before and after treatment	152
Horseradish peroxidase	Acid Blue 225, Acid Violet 109/ 30	83 %, 70% / 0.5, 0.25 (for AB225 and AV109 respectively)	53, 113	Different anthraquinone dye structures lead to different decolorisation degrees under the same conditions, decolorisation of AB225 is affected more by temperature and concentration of enzyme, but dye concentration affects AV109 decolorisation more	122
Laccase	Reactive Blue 19/ 100	89 %/ 0.5	178	Laccase showed better decolorisation performance on anthraquinone dyes, compared to azo, triphenylmethane or indigo dyes, no mediators were necessary	153
Laccase	Reactive Blue 19/ 300	100 %/ 72	100	Laccase showed better decolorisation performance on anthraquinone dyes compared to other types of dyes. Furthermore, activity of purified enzyme was higher than use of mother culture.	
Laccase followed by biosorption	Reactive Blue 4 / 1000	90 (61+29) % / 12	50.8+24.1	Reduced phytotoxicity, individually, biosorption works better, enzymatic degradation results in brown-ish products, dye fragments are more polar compared to original dye	165
Dye-decolorising peroxidase	Reactive Blue 19/ 150	95 % / 0.167	855	Decolorisation examined in batch reactor and fed batch reactor, examination of stepwise and continuous feed of H ₂ O ₂ , batch and continuous fed reactor, residual activity of DyP is 80 % after 80 mins, increased dye concentration prolongs the decolorisation time, increased addition of H ₂ O ₂ deactivated the enzyme, through batch fed system one dose of enzyme managed to decolorise 3,650 mg/L RB19	107

402 * values shown are for the optimised methods as presented by researchers and refer to removal of colour unless stated otherwise

403 ** arbitrary value calculated to show the maximum removal capacity of any given method within an hour, based on the best results presented in each reference. In cases where
404 the timescale of the decolorisation is within a few minutes, the assumption of decolorisation ability over continuous use for 1 h is made.

405

406 **3.3. Immobilisation**

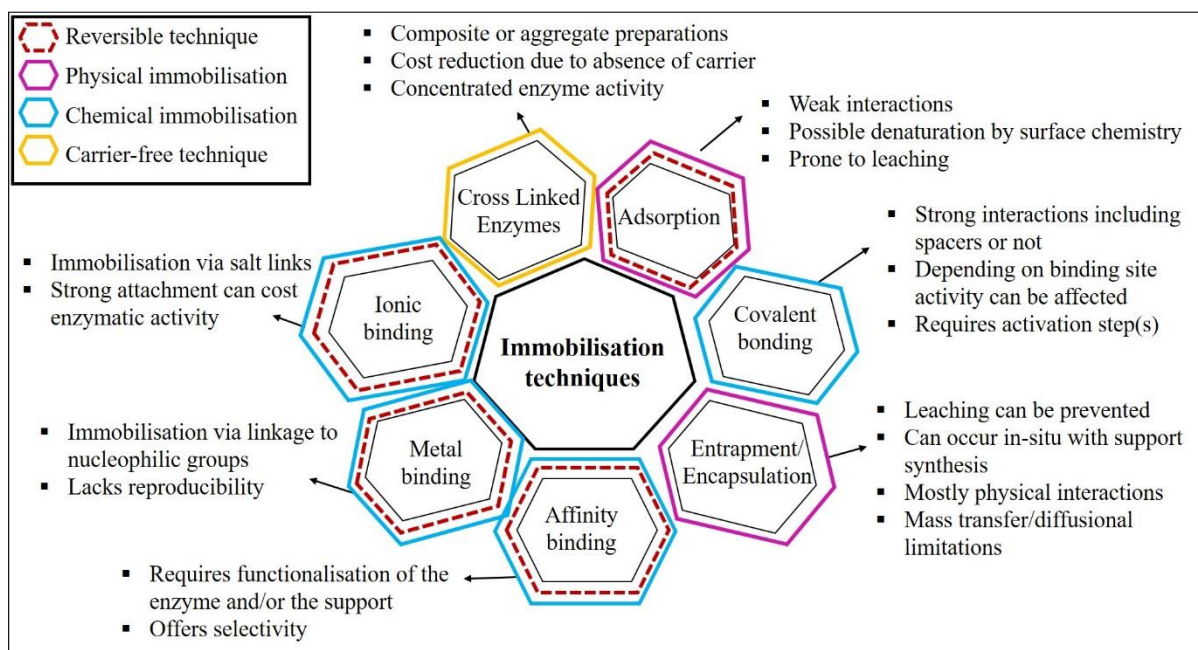
407 **3.3.1.General information**

408

409 The stability of enzymes under “un-natural” conditions, enzyme production cost and the need
410 for downstream separation are crucial for their industrial potential ¹⁶⁶. Immobilisation is an
411 established technique with the aim to facilitate separation and reuse of enzymes as well as
412 maintain the most active conformation ^{167, 168} by “securely attaching” the enzyme onto usually
413 solid supports that offer molecular rigidity ¹⁶⁹. Major advantages of immobilisation include the
414 ability for enzyme reuse and the simplified downstream processing, as well as the enhancement
415 of operational stability of enzymes and the option for cascade reactions; ultimately offering
416 cost effective solutions ^{166, 170}. However, distinct disadvantages include the rigorous design of
417 the system, which has to be tailored to the enzyme and application in mind, minimising mass
418 transfer limitations between the enzyme and the substrates and the possibilities for enzyme
419 deactivation ^{166, 170}. It should be noted that immobilisation does not necessarily aim to make
420 the enzyme perform better when it is applied in its optimal operational conditions, but to
421 maintain or ideally increase its performance when the conditions are not optimal ¹⁷¹.

422 **3.3.2.Methods and supports for immobilization**

423 There are many extensive reviews on methods and supports used for enzyme immobilisation¹⁷²,
424 ¹⁷³ focusing on a specific support (e.g.¹⁷⁴), immobilisation method (e.g.^{175, 176}) or enzyme
425 (e.g.¹⁷⁷). Among many available ways of immobilisation as shown in Figure 2, the most widely
426 preferred ones are adsorption, entrapment or encapsulation and covalent bonding ¹⁷⁴. The
427 typical enzyme content in the final product is usually less than 10 % by weight, remaining
428 being the support ¹⁷⁶.



429

430 Figure 2: Brief description of immobilisation methods, with the most common methods underlined (adapted
431 from ^{167, 176, 178}).

432 There is not a set combination of technique, support and enzyme, as immobilisation highly
433 depends on the targeted reaction/process, the given conditions and the possible interactions.
434 Thus for achieving a golden mean for the factors affecting its efficiency, approaches ranging
435 from trial and error to predictive designing of the targeted system are used ¹⁷⁹. The selected
436 combination should satisfy both catalytic (productivity, stability and specificity) and non-
437 catalytic requirements (control of the process, separation, robustness and need for further
438 processing)¹⁸⁰. A suitable support for enzyme immobilisation should fulfil requirements in
439 regards to mechanical properties, ease of synthesis and functionalization, environmental
440 friendliness, leaching prevention, toxicity, loading capacity, low steric hindrance effects but
441 high availability of reactive groups ^{167, 172, 181}. Also, it should fulfil requirements about the
442 microenvironment and mass transfer during enzymatic actions ^{169, 182}. What is aimed is to create
443 a stable and active biocatalyst that can be applied on an industrial level ^{172, 183}, at an acceptable
444 total cost ^{184, 185}. Immobilised enzymes can be cost-effective if the cost of immobilisation (total
445 cost of every step of the process) is lower than the cost of separation of soluble enzymes from

446 the product (and of further product purification if needed), in addition to the cost of using fresh
447 enzyme in every “catalytic round”¹⁸⁶.

448 **3.3.3. Anthraquinone dye decolorisation by immobilised** 449 **oxidoreductases**

450
451 There are some reviews available on water decontamination by immobilised enzymes, focusing
452 either on specific pollutants or on specific enzymatic sub-categories of oxidoreductases^{119, 120,}
453 ^{125, 177, 187, 188}. Generally, the operational stability of enzymes is enhanced by immobilisation
454 but the activity of the enzyme is reduced, mainly due to disruption of the active conformation,
455 difficulty of the substrate to reach the enzyme, or deactivation of the enzyme due to
456 accumulation of toxic substances. The decontamination efficiency highly depends on the
457 combination of enzyme and support used, as well as on the system investigated (dye structure
458 and concentration, presence of other substances). Hence, enzymatic performance is typically
459 investigated by varying some of those parameters, as well as operational parameters like
460 temperature and pH (Table 3). From Table 3 it is clear that immobilisation enhances the
461 stability and it facilitates enzyme reusability. Some examples include increased performance
462 of the immobilised enzyme compared to free (7 % higher performance was noted when
463 polyphenol oxidase was immobilised)¹⁸⁹. It is also worth mentioning that both the available
464 examples of immobilised DyP showed great performance of the composite, with high
465 reusability and stability^{190, 191} and very high throughput, comparable to the values observed for
466 AOPs..

467

468

469

470 Table 3: Decolorisation of anthraquinone dyes by immobilised oxidoreductases.

Enzyme	Method/Support	Substrate/ Dye concentration (mg/L)	Throughput (mg/L/h)*	Comments	Ref.
Horseradish peroxidase	Covalent binding/ methacrylated polysulfones	Reactive Blue 19/ 40	34	85 % decolorisation within 1h, decent reuse potential (7 times, 20 % activity left by 7th), increased storage stability. Increased T stability	192
Dye-decolorising peroxidase	Adsorption/ immobilized FSM-16 and AISBA-15	Reactive Blue 19 /150	1800	100% removal within 5mins, immobilisation support affects enzymatic activity hence decolorisation, pH affects decolorisation and enzyme leaching from support	190
Dye-decolorising peroxidase	Adsorption/ Meso Cellular Foam	Reactive Blue 19 /150	3600	High adsorption yield but low residual activity, pH affects decolorisation and enzyme leaching from support, very good reuse potential (20 cycles) in pH4	191
Polyphenol oxidase	Adsorption/ Celite 545	Reactive Blue 4 /50-100	43.5-87	Immobilised enzyme shows better results than free, pH affects decolorisation, immobilized enzyme treatment leads to reduced TOC post-treatment compared to free enzyme	189
Horseradish Peroxidase	Cross linked Enzyme Aggregates	Acid Violet 109 /30	36-46	High decolorisation degree (70-90 %), decolorisation experiments in batch/packed bed reactors (packed bed performs better), enhanced pH stability and higher dye and peroxide concentration tolerance, reduced toxicity after enzymatic treatment of dye solution	193
Horseradish Peroxidase	Adsorption/activated kaolin	Acid Violet 109 /40	52.2	Adsorption conditions examined, good decolorisation (87% after 40mins), improved pH stability during decolorisation, better tolerance of high dye concentration, considerably lower substrate affinity but not very lower initial rate, high (7) reuse cycles (35 % activity left)	19
Hematin (not enzyme, but of structure resembling peroxidases) and Horseradish Peroxidase	Covalent adsorption/ chitosan and APTS	Alizarin red/ 200	97.4 for Hematin 40 for Horseradish Peroxidase	Decolorisation is based on action of hematin as peroxidase active site, comparison with immobilised horseradish peroxidase is taking place, about 50 % efficiency on 1 st cycle, after 6 cycles efficiency drops to 34%, identification of possible reasons for decreased activity, comparison between 2 dyes (anthraquinone and azo)	194
Laccase	Adsorption/ magnetic carbon capsules	Reactive Blue 19/ 100-300 Acid Green 25/ up to 2000	18-54 for Reactive Blue 19, 18- 360 for Acid Green 25	Decolorisation experiments for the 2 dyes were under different conditions, very high loading achieved (1g enzyme/g support), almost 80 % decolorisation within 1 st hour, 90 % within 5 hours, excellent reusability (activity almost intact after 6 cycles), acknowledgment of dye adsorption on support, good storage stability (10 % activity loss after 2 months)	195
Horseradish Peroxidase	Adsorption/ chitosan	Reactive Blue 19 / 100	17.5	Use of glutaraldehyde for added functionalisation, about 70% decolorisation regardless of the dye concentration (25 mg/L and 100 mg/L)	196

				examined), biocatalysts were reused for up to 7 cycles with more than 60% residual activity, main body of the work was done for an azo dye	
Laccase	Adsorption/ silanised silica beads	Disperse Blue 3, Reactive Blue 19 / ~20	0.9 for Disperse Blue 3 and 3.2 for Reactive Blue 19	Examination of various dye structures, decolorisation of 80-90 % of AQ dyes within 5 h for Reactive Blue 19 and 17 h for Disperse Blue 3, reduction of toxicity further to free enzyme, free laccase leads to a throughput of about 34 for both AQ dyes,	197

- 471 * arbitrary value calculated to show the maximum removal capacity of any given method within an hour, based on the best results presented in each reference. In cases where
- 472 the timescale of the decolorisation is within a few minutes, the assumption of decolorisation ability over continuous use for 1 h is made.

473 Immobilisation of laccase on silanised alumina pellets has also shown to reduce the inhibitory
474 effects of components usually present in industrial dye-baths such as wetting, soaping or
475 sequestering agents ¹⁹⁸. When decolorisation of two structurally similar anthraquinone dyes
476 (Reactive Blue 19 and Acid Blue 25) was examined using immobilized laccase in epoxy
477 activated Sepabeads, researchers got greatly different results (almost 0 % for Reactive Blue 19
478 and about 40 % for Acid Blue 25), indicating that structure of dye –even if of the same general
479 type– has an important role ¹⁹⁹. Presence of a mediator in the examined systems increased the
480 decolorisation of Reactive Blue 19 from 0 % to about 30 %, whereas the effect on
481 decolorisation of Acid Blue 25 was negligible. Following the same argument, researchers ¹⁹⁵
482 studying the decolorisation of two anthraquinone dyes (Reactive Blue 19 and Acid green 25)
483 using again laccase but immobilised on magnetic carbon nanoparticles, achieved highly
484 positive results (more than 80 % decolorisation efficiency, good reusability potential, stability)
485 for both dyes. This shows that the immobilisation support also has a great effect on
486 decolorisation efficiency, since using the same enzyme (laccase) acting on the same dye
487 (Reactive Blue 19) yield different results when different supports were examined. In terms of
488 methods and matrixes used for immobilisation, looking at Table 3 one can see that adsorption
489 on inorganic matrices – usually silicates – is highly favoured over other methods and matrices
490 combinations. This is possibly due to the extensive research available on those materials ^{174, 200}
491 and their wide industrial presence ²⁰¹, thus allowing easier industrial implementation of the
492 immobilized biocatalyst. An issue usually faced with immobilisation supports is adsorption of
493 dye on the actual support instead of decolorisation due to enzymatic action, which might lead
494 to false results if it is not accounted for. Indeed, another study showed an initial step of dye
495 adsorption onto the carrier (silica beads), followed by decolorisation by the enzyme (laccase),
496 allowing for fresh substrate to be used ²⁰². Also, another issue is the adsorption of degradation
497 products ^{192, 202}, which might lead to enzyme deactivation.

498 It should be noted that researchers have developed artificial enzyme mimics – namely
499 nanozymes – that mimic specific enzymatic actions. Their action is based on a chemically
500 synthesized active site that is very similar to the one of the targeted natural enzyme, e.g.
501 enzymes that contain metals or metal oxides ²⁰³. So far, there have been examples mimicking
502 the action of peroxidases ²⁰⁴⁻²⁰⁸ but only two reports of peroxidase mimetic nanozymes for dye
503 decolorisation exist (for an azo, a xanthene ²⁰⁹ and a thiazine dye ²⁰⁶), and none on
504 anthraquinone dyes. . It has been reported that nanozymes are easy to use over natural enzymes
505 due to lower cost, easier scale-up production, higher durability and stability. However,
506 nanozymes applications are very limited due to lack of selectivity and substrate recognition, as
507 well as lower activity compared to natural enzymes ^{203, 210, 211}.

508 **4. ON THE DEGRADATION PATHWAY OF** 509 **ANTHRAQUINONE DYES**

510 As it has been already mentioned, it is quite difficult to confirm the degradation pathway of a
511 dye, mainly due to the possibility of spontaneous oxidations and our inability to quickly isolate
512 fragments. Nevertheless, there are few examples where based on the initial dye structure, some
513 identified fragments and the identified as final products, researchers have been able to propose
514 a degradation pathway for model anthraquinone dyes. Although Li et al.⁴¹ discuss the
515 degradation pathway of AQ dyes by biological methods and Siddique et al.⁴² have collected
516 examples of Reactive Blue 19 degradation by different methods without however touching on
517 the degradation pathway, a comprehensive discussion around the degradation pathway of AQ
518 dyes by various methods is missing. In Table 4 one can see a list of research examples studying
519 the degradation of a model AQ dye (Reactive Blue 19, structure shown in Figure 1) using 4
520 different methods and proposing degradation pathways based on the identified fragments. The
521 chemical structure of fragments is shown in Table S2. By comparing the identified fragments,
522 it is evident that each method can lead to different results. Degradation of Reactive Blue 19

523 using thermal-pressure hydrolysis ²¹² was the only case where the identified fragments were
524 not of aromatic structure (small carboxylic acids were detected). In every other research
525 example studied the identified fragments were considerably larger, especially for the
526 examination of degradation via enzymatic action. In this case, the proposed degradation
527 pathway did not progress much further than the deamination of the anthraquinone structure and
528 the ring's rupture, as well as the deamination and desulfonation of the main auxiliary structure
529 ⁹⁵. The AOPs, chemical and biological methods used for Reactive Blue 19 degradation (Table
530 4) resulted in phthalic acid and its derivatives (as identified products), with expectations for
531 further degradation to lower by products, which however were not confirmed by the analytical
532 methods used. What can be assumed based on the degradation pathways proposed is that the
533 anthraquinone structure is eventually broken down to simpler aromatic derivatives, allowing
534 for easier manipulation afterwards. However, this is not the case for the enzymatic methods,
535 where degradation seems to be a more lengthy procedure ^{95,97}. Based on that absence of further
536 degradation might be attributed to loss of enzymatic activity over prolonged time of use and/or
537 exposure to the reaction mixture.

538 A first comparison between the identified as final fragments across different methods used,
539 show that electrochemical methods lead to generally smaller fragments, with higher
540 mineralization potential compared to biological methods. As it can be seen in Table S3, of the
541 most common fragments identified were phenol, phthalic acid, their derivatives and low
542 molecular hydrocarbons. These fragments were mainly produced by the cleavage and
543 subsequent degradation of the anthraquinone ring through various steps. In some cases it was
544 noted that different dyes (Reactive Blue 19 ²¹³ and Reactive Blue 4 ²¹⁴) treated with the same
545 method led to the same degradation products (as derived by the anthraquinone ring). This
546 observation could be an indication of some control over the end products if a specific method
547 is applied. However, looking more in depth into a specific method, ozonation, for the

548 degradation of the same dye, Reactive Blue 19, results from different researchers showed
549 slightly different fragments. Identified fragments ranged from a mixture of phenol, acetic acid
550 and propandioic acid ⁶⁸, to a mixture of phenol, acetic acid and oxalic acid ⁹² and to a mixture
551 of phthalic acid and unspecified carboxylic acids ⁶⁹. Upon examination of the conditions used,
552 Fanchiang et al. ⁶⁹ used slightly higher ozone feed rate compared to the other studies, which
553 might have been responsible for the higher mineralisation potential.

554 Based on the few research examples showing a degradation pathway and fragments of AQ dyes
555 treated using biological methods as shown in the lower end of Table S3, we can see that the
556 identified fragments are not different to those shown for chemical and AOP methods. However,
557 the identified fragments upon degradation using enzymes were substantially larger compared
558 to those identified by other methods, as shown in Table S3. This observation shows that
559 although isolated enzymes can potentially be very efficient in decolorisation, when it comes to
560 dye breakdown and mineralisation, the requirements for degradation are higher than what
561 currently available from enzymes. That being said, combination of enzymes, as it is the case in
562 biological systems, might be a potential avenue to explore.

563 It should be noted that in all the research examples examined, the suggested degradation
564 pathways based on some identified fragments and the discussion around the specific
565 breakdown mechanisms, show that the initial fragments could not be identified by the
566 analytical methods used, but were speculated retrospectively. This shows the lack of control
567 over the dye degradation reactions and the existence of spontaneous reactions that can lead to
568 the same lower fragments via multiple paths ^{69, 74}. With regards to the auxiliary groups present
569 on the dye structures (such as amino-groups, sulfone-groups, halogen-groups), mapping down
570 their degradation pathway was more difficult. Research examples either did not identify further
571 degradation past the original rupture from the dye structure ^{93, 95, 214}, or identified big fragments
572 and even polymerized by-products ⁹⁷.

573 Table 4: Final identified fragments during degradation of Reactive Blue 19 via various methods. Please refer to Table S2 for the chemical structures of the identified fragments.

Method	Final identified fragments	Identification methods* and relevant comments	Ref.
Thermal-pressure hydrolysis	Acetic acid, oxalic acid	Use of GC-MS, comprehensive table with identified fragments and their time occurrence during degradation	212
Ozonation	Phthalic acid, carbon dioxide, water	Use of UV-Vis, FTIR, LC-MS and GC-MS, comprehensive discussion around proposed degradation pathway	69
Photodegradation on nano-TiO ₂ in presence of H ₂ O ₂	3,6-dihydroxyphthalic acid, ethyl-sulfate-phenyl-sulfone	Use of UPLC-MS	99
Electrochemical degradation in presence of chloride	1,3 indanone, phthalide, phthalic anhydride, phthalimide, benzoic acid	Use of GC-MS, potential for further breakdown upon increased contact time, no chlorinated by-products detected	213
Biological (bacterial flora <i>DDMY2</i>)	benzenesulfonic acid, hexan-1-amine, 3,6-dihydroxyphthalic acid,	Use of UV-Vis, FTIR and LC-TOF-MS, comparative discussion on degradation products with literature	215
Enzymatic (immobilised laccase)	5-sodium-benzenesulfonyl-ethanone, opened anthraquinone ring fragment	Use of LC-MS, 2 intermediates and 2 final products identified, no observations for backward reactions	95

574 *H/UPL/C: high/ultra pressure liquid chromatography, GC: gas chromatography, MS: mass spectrometry, TLC: thin layer chromatography, UV-

575 Vis: Ultra Violet-Visible Spectrophotometry, FTIR: Fourier Transformation Infra-Red Spectroscopy, TOF: Time of flight

576 **5. CONCLUSIONS AND FUTURE CHALLENGES**

577 Degradation of anthraquinone dyes poses an environmental problem that has been ignored due
578 to their smaller volume compared to azo dyes. Existing research shows that anthraquinone dyes
579 can be sturdier when it comes to decolorisation due to their structure. Furthermore, their
580 removal is highly specific on the dye and method used, hence it can be quite difficult to choose
581 a single solution among the available conventional methods. Comparing the existing
582 physical/chemical methods with the biological ones, it is clear that while every method has
583 their distinctive advantages and disadvantages, Advanced Oxidation Processes and isolated
584 enzymes stand out in terms of fastness of degradation. In this review we focused mainly on
585 enzymatic decolorisation of anthraquinone dyes, and showed that it has gone a long way but
586 still needs extensive research before industrial implementation. Immobilisation can help create
587 powerful biocatalysts that can be both environmentally friendly and industrially applicable.
588 Currently, immobilized oxidoreductases can show activity comparable to free enzyme when it
589 comes to smaller substrates, but they sometimes suffer when it comes to dyes of larger sizes
590 causing inaccessibility to the enzyme inside a porous support.

591 A main challenge we identified during literature review, was the lack of consistency in
592 approaches used in various research examples. This makes the comparison of the ability of
593 suggested methods to treat anthraquinone dyes (or pollutants in general) quite tricky, as we
594 showed that different conditions using the same method and the same dye, or using a method
595 under the same conditions for different dyes can lead to different results. A way to
596 circumnavigate that would be to set a benchmark set of parameters per available method,
597 making comparison across methods easier. For example, setting a standard dye concentration
598 for experiments, a fixed ratio of dye to enzyme, nanomaterial, oxidant or energy used. It could
599 also mean setting an arbitrary unit that allows to compare results on a common basis, such as

600 productivity. These approaches would make comparison across methods easier, showing the
601 strong and weak points of each method in a more comparable manner.

602 Another challenge that became obvious across examined literature is the unrealistic approach
603 usually followed, pinpointed by the fully controlled systems used. Although some level of
604 control is needed to define and characterise a dye degradation system, a more realistic approach
605 towards system development should be adopted, incorporating research on real effluents or
606 mixtures of dyes. Although it is mainly the mixtures of dyes that are encountered in the actual
607 effluents from textile industry, there are very limited reports examining such mixtures of dyes
608 ²¹⁶⁻²¹⁸ and even fewer that include an anthraquinone dye within the dye mixture ^{155, 219, 220}. The
609 absence of extended research on dye mixtures (only one review paper on dye mixture
610 decolorisation was found ²²¹) highlights the need to investigate the ability of existing
611 technologies to treat a more realistic form of effluent, that being dye mixtures, or solutions
612 containing other auxiliaries used in the textile industry. Focusing on decolorisation of
613 anthraquinone dyes by immobilized oxidoreductases, the lack of information of the
614 performance of such systems on real (or realistic) effluents was also noted. This can be
615 attributed to the high sensitivity of biocatalysts towards operational conditions, but if such
616 methods are aimed to be applied industrially, then a more realistic approach is ought to be
617 explored.

618 Another identified challenge with respect to dye degradation is the relatively limited available
619 information on the degradation pathways. All the research examples proposing a degradation
620 pathway, reached their conclusions based on a few identified fragments via analytical
621 techniques, assuming previous and further reaction steps. The existence of free radicals and the
622 recalcitrant structure of anthraquinone dyes make oxidation, hence degradation, difficult to
623 predict. In a few examples in literature, there were more than one pathways proposed for the
624 degradation of an anthraquinone dye, indicating the need for better control over the process of

625 degradation. This could be achieved through more careful control of the reaction and the
626 development of techniques to pause the reaction before progressing further, or techniques to
627 slow it down enough so that samples during the initial stages can be withdrawn.

628 Finally, with regards to immobilised oxidoreductases, future studies need to tackle the “value
629 for money” equation when it comes to the synthesis of a biocatalyst for such a specific, yet
630 absolutely crucial application. So far the main aim of the studied examples seems to be the
631 performance of the biocatalyst, without trying to minimise synthesis cost. Majority of examples
632 examined are using lengthy synthesis procedures with many subsequent steps for the materials
633 synthesis and the immobilisation of the enzyme, and further hazardous chemicals and
634 unsustainable practices are usually employed^{189, 192, 196, 197, 199, 222-224}. These lead to final
635 products which might tick the performance brief, but by no means tick the industrial
636 implementation brief, rendering them basically unusable. Research should focus on the
637 identification of a golden means between synthesising a material-enzyme complex able to
638 perform as a powerful dye degradation agent, but also have the potential for easy and
639 economical scale up in order to be industrially relevant. Alternatively, research could also
640 focus on the combination of methods in order to address their limitations and enhance their
641 advantages. For example, initially treating anthraquinone dyes – or effluents generally – with
642 immobilised oxidoreductases and following up with AOPs, could help minimise the energy
643 cost associated with AOPs and prevent biocatalysts from prolonged use, hence increase their
644 industrial potential.

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