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1 **Colloidal Aspects of Digestion of Pickering Emulsions:**

2 **Experiments and Theoretical Models of Lipid Digestion**

3 **Kinetics**

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21

22 **Abstract**

23 Lipid digestion is a bio-interfacial process that is largely governed by the binding of the lipase-colipase-
24 biosurfactant (bile salts) complex onto the surface of emulsified lipid droplets. Therefore, engineering
25 oil-water interfaces that prevent competitive displacement by bile salts and/or delay the transportation
26 of lipase to the lipidoidal substrate can be an effective strategy to modulate lipolysis in human
27 physiology. In this review, we present the mechanistic role of Pickering emulsions *i.e.* emulsions
28 stabilised by micron-to-nano sized particles in modulating the important fundamental biological process
29 of lipid digestion by virtue of their distinctive stability against coalescence and resilience to desorption
30 by intestinal biosurfactants. We provide a systematic summary of recent experimental investigations
31 and mathematical models that have blossomed in the last decade in this domain. A strategic examination
32 of the behavior and mechanism of lipid digestion of droplets stabilised by particles in simulated
33 biophysical environments (oral, gastric, intestinal regimes) was conducted. Various particle-laden
34 interfaces were considered, where the particles were derived from synthetic or biological sources. This
35 allowed us to categorize these particles into two classes based on their mechanistic role in modifying
36 lipid digestion. These are ‘*human enzyme-unresponsive particles*’ (*e.g.* silica, cellulose, chitin,
37 flavonoids) *i.e.* the ones that cannot to be digested by human enzymes, such as amylase, protease and
38 ‘*human enzyme-responsive particles*’ (*e.g.* protein microgels, starch granules), which can be readily
39 digested by humans. We focused on the role of particle shape (spherical, anisotropic) on modifying both
40 interfacial and bulk phases during lipolysis. Also, the techniques currently used to alter the kinetics of
41 lipid digestion using intelligent physical or chemical treatments to control interfacial particle spacing
42 were critically reviewed. A comparison of how various mathematical models reported in literature
43 predict free fatty acid release kinetics during lipid digestion highlighted the importance of the clear
44 statement of the underlying assumptions. We provide details of the initial first order kinetic models to
45 the more recent models, which account for the rate of adsorption of lipase at the droplet surface and
46 include the crucial aspect of interfacial dynamics. We provide a *unique decision tree* on model selection,
47 which is appropriate to minimize the difference between experimental data of free fatty acid generation
48 and model predictions based on precise assumptions of droplet shrinkage, lipase-binding rate, and

49 nature of lipase transport process to the particle-laden interface. Greater insights into the mechanisms
50 of controlling lipolysis using particle-laden interfaces with appropriate mathematical model fitting
51 permit better understanding of the key lipid digestion processes. Future outlook on interfacial design
52 parameters, such as particle shape, size, polydispersity, charge, fusion, material chemistry, loading and
53 development of new mathematical models that provide closed-loop equations from early to later stages
54 of kinetics are proposed. Such future experiments and models hold promise for the tailoring of particle-
55 laden interfaces for delaying lipid digestion and/or site-dependent controlled release of lipidic active
56 molecules in composite soft matter systems, such as food, personal care, pharmaceutical, healthcare
57 and biotechnological applications.

58

59 **Keywords:** Pickering emulsion; Particle-laden interface; Lipid digestion; Lipase; Mathematical
60 model

61 **1. Introduction**

62 Emulsions are ubiquitous in nature (*e.g.* milk, butter) and in engineered systems (*e.g.* cosmetics,
63 processed food, pharmaceuticals, paints). Emulsions are intimate dispersions of two immiscible liquids,
64 such as oil and water. In general, the liquid, which is present as micron- or sub-micron-sized droplets
65 in the other liquid is known as the dispersed, discontinuous or internal phase [1-3]. And, the liquid into
66 which the droplets are dispersed is known as the dispersion medium, continuous or external phase. From
67 a thermodynamic perspective, emulsions are metastable *i.e.* they are in a state far from the equilibrium.
68 Thus, emulsions tend to separate into their individual phases to attain an equilibrium configuration over
69 a period of time. This thermodynamic instability is commonly represented using Gibbs free energy
70 change, ΔG , during emulsification. Emulsification at a constant temperature of T alters both the
71 configurational entropy of the droplets, S_{config} , and the contact area between the immiscible phases, A ,
72 such that ΔG is given by:

73

$$74 \quad \Delta G = \Delta H - T\Delta S_{config} + \gamma_{ow}\Delta A \quad (1)$$

75

76 where, ΔH is the enthalpy change, which is almost zero for emulsification, and γ_{ow} is the
77 interfacial tension between the oil and water phases. The change in interfacial free energy ($\gamma_{ow}\Delta A$) is
78 always net-positive as the interfacial area increases after the homogenization process, and is generally
79 much larger than the term containing the configurational entropy change, ΔS_{config} , and thus the latter can
80 be ignored [3]. Hence, ΔG is mainly governed by $\gamma_{ow}\Delta A$. In the presence of an emulsifier, the magnitude
81 of $\gamma_{ow}\Delta A$ is diminished due to reduction of the interfacial tension between the two phases enabled by
82 adsorption of the emulsifier at the oil–water interface, consequently reducing the free energy. Though
83 interfacial energy is the key driving force for emulsion formation, the properties of emulsifiers, such as
84 surface charge and steric hindrance are crucial for providing kinetic stability to the emulsions.
85 Emulsifiers, such as mono or di-acylglycerols, proteins, modified starches play an important role in
86 imparting this kinetic stability to the oil droplets, however they tend to phase separate over a period of
87 weeks to few months.

88 Besides conventional surfactants, emulsions can also be stabilised by rigid or soft solid particles
89 that form a mechanical barrier *via* the Pickering stabilization mechanism [4, 5]. In fact, such Pickering
90 emulsions are often encountered in the crude oil refining process [6], homogenized milk stabilised by
91 casein micelles and aggregated milk proteins [7] and are engineered for soft material applications [4,
92 8]. In comparison to classical surfactant-stabilised emulsions, Pickering emulsions that are stabilised
93 by solid particles are distinctively more stable to coalescence and Ostwald ripening [4, 5]. This is due
94 to the large amount of desorption energy (ΔE) required to dislodge the particles from the interface [9].
95 In other words, for emulsions to destabilize, the free energy (ΔG) of the system has to significantly
96 increase at first, as the particles move from their preferred positions on the interface to one of the two
97 phases. The adsorption energy for a single particle can be expressed using equation (2) [5, 10, 11]:

$$98 \quad 99 \quad \Delta G = -\Delta E = -\gamma_{ow}\pi r_p^2(1 - |\cos \theta|)^2 \quad (2)$$

100 where, r_p is the radius of the particle and θ is the equilibrium three-phase contact angle [5, 12]
101 highlighting the wettability of the particles by oil or water phases. The actual energy required to dislodge
102 a particle from the surface has been shown to be even higher, at several times that given by equation
103

104 (2). This is due to dissipation of energy stored in the liquid neck, formed between the particle and
 105 interface, as the liquid relaxes back once the particle has departed from the surface [9, 13]. Hence, even
 106 nano-sized solid particles with $r \approx 50$ nm at a contact angle of 90° at the oil-water interface (typical
 107 value of $\gamma_{ow} \approx 50$ mN m⁻¹) will have $\Delta E \approx 10^5 k_B T$, where k_B is the Boltzmann's constant. This is several
 108 orders of magnitude higher than that for classical surfactants, which typically have $\Delta E \approx 5 k_B T$ and
 109 therefore tend to continuously “hop on and off” from the interface [14]. Thus, it is almost certain that
 110 solid particles once adsorbed under partial wetting conditions by the two phases, will remain
 111 irreversibly anchored to the interface making Pickering emulsions highly resilient to coalescence, when
 112 compared to similar droplets stabilised by typical molecular surfactants. Theoretically, wetting is
 113 represented by the classical Young's equation (equation 3), which is related to the balance of interfacial
 114 forces per unit length of the contact line at particle–oil (γ_{po}), particle–water (γ_{pw}), and oil–water (γ_{ow})
 115 surfaces:

$$117 \quad \cos \theta = \frac{\gamma_{po} - \gamma_{pw}}{\gamma_{ow}} \quad (3)$$

118
 119 If one of the liquids wets the solid particles more than the other, the better wetting liquid
 120 becomes the continuous phase and the other one becomes the dispersed phase. For instance, if θ
 121 measured in the aqueous phase is smaller than 90° (Fig. 1a), then particles are preferentially wetted by
 122 the aqueous phase (i.e. $\gamma_{pw} < \gamma_{po}$), with a large fraction of such particles residing in the continuous phase
 123 and stabilizing an O/W emulsion. Such hydrophilic biocompatible particles include protein microgels,
 124 zein particles and chitin nanocrystals [15-18]. However, if θ is greater than 90° (Fig. 1b), the particles
 125 tend to be preferentially wetted by oil phase and stabilizes a W/O emulsion, as demonstrated using zein
 126 particles in presence of lecithin [19]. Particles wetted equally by oil and water have contact angle of
 127 90° (Fig. 1c). It is noteworthy that when θ is relatively close to 90° , then particles effectively act as a
 128 Pickering stabilizer as particles tend to remain dispersed in either phases if they are too hydrophilic
 129 ($\theta \ll 90^\circ$) or too hydrophobic ($\theta \gg 90^\circ$) [20]. In order to overcome this latter issue, many studies have
 130 modified natural particles to varying degrees in order to make them partially wetted by both the polar
 131 and non-polar phases. For example, modified starch granules, prepared via reaction with octenyl

132 succinic anhydride [21] or modified cellulose prepared using stearyl chloride [22] have been used as
133 effective Pickering stabilizers of oil-in-water or water-in-oil emulsions, respectively.

134 Pickering stabilization of colloids using particles is a century-old concept, first introduced in
135 1904 by Ramsden [23] and proven experimentally by Pickering few years later [24]. The earliest
136 theoretical treatment, demonstrating how fine particles can stabilize emulsions and foams, seems to be
137 developed by Levine *et al.* dating back to 1989 [25]. Nevertheless, the study of particle-laden interface
138 has revived through a renaissance of research attention in the last two decades. This can partly be
139 attributed to the growing demands for designing ultra-stable emulsions using surfactant-free and ‘clean-
140 label’ emulsifiers. In part, such a resurgence of research interests in particle-stabilised interfaces are
141 also associated with tremendous progress in mining biocompatible particles from natural sources and
142 laboratory-scale synthesis of relatively low-cost biocompatible colloidal particles with tunable size
143 (micron-to-nanometers) [11, 26, 27] for use in food, pharmaceutical, cosmetics and other allied soft
144 matter applications. In such applications sustainability and biocompatibility are key requirements. Last
145 but not the least, particle-laden interfaces have been lately recognized as promising templates by colloid
146 scientists to address key biological processes, such as delaying lipid digestion [16, 28-30], drug delivery
147 [31], nutraceutical delivery [32] and controlled release of lipophilic molecules via oral and topical
148 administration routes [33, 34].

149 In particular, lipid digestion is a fundamental biological process that represents a major
150 bottleneck in the pathway to controlled delivery of lipophilic drugs and nutrients when administered
151 through oral routes in human physiology. Lipid digestion is an interfacial process and the kinetics of
152 lipid digestion is governed by the binding of enzymes (lipases, proteases, amylases), biosurfactants (bile
153 salts) and other cofactors onto the surface of emulsified droplets [35]. Simplistically, one might expect
154 lipid digestion to be controlled by tailoring and/or tuning the interfacial network. Hence, research efforts
155 have been directed in recent years to alter the kinetics of lipid digestion by modification of the interfacial
156 structures [1, 16, 29, 36-38]. In particular, solid particles have shown encouraging outcomes in this
157 direction in the past decade by a variety of interfacial mechanisms, which necessitates this review.
158 Progress on Pickering emulsion research has been well-described in the excellent reviews by Binks [4,
159 5, 39], Dickinson [7, 26, 27, 40, 41] and few other research groups [10, 11, 42-46], who have discussed

160 the physical chemistry, stabilization principle as well as design of elegant Pickering emulsions stabilised
161 by organic (biologically derived) particles. However, to our knowledge, there exists no review that has
162 discussed the mechanistic role of Pickering emulsions in modulating the important fundamental
163 biological process of lipid digestion.

164 Hence, the purpose of this review is to focus on the experimental investigations and theoretical
165 models on lipid digestion of Pickering emulsions stabilised by nano-to-micron-sized particles within
166 the last decade. In this review, only O/W emulsions are considered. We start with briefly discussing the
167 key physiological players in the biophysics of lipid digestion in the oral, gastric and intestinal regimes.
168 The ultimate step of conversion of lipids into self-assemblies, such as micelles, vesicles, and liquid
169 crystals that are essential for lipid absorption in the lower intestines is beyond the scope of this review.
170 A description of the colloidal aspects of digestion sets the scene for understanding how parameters
171 associated with the particle, such as size, shape, concentration, charge, packing density affect the
172 resilience of the particle-covered droplets to harsh physiological conditions. We have then summarized
173 the current knowledge of how such particles on their own or via suitable physical/ chemical tuning at
174 the interface play an integral role in modifying the kinetics of lipid digestion. Attention is then directed
175 towards reviewing the mathematical models in literature, highlighting the early first order kinetic
176 models to the more recent modelsd attempting to account for the adsorption kinetics of enzymes at the
177 droplet surface and the associated role of interfacial structure. We provide a decision tree on model
178 selection appropriate to likely to represent a given digestion behavior (*e.g.* droplets shrinking, enzyme
179 binding rate, nature of enzyme transport process to the surface of droplets). Finally, we provide
180 suggestions for future work in both theoretical and experimental domains to maximize the potential of
181 Pickering emulsions in order to address fundamental biological and biochemical challenges associated
182 with emulsified lipid digestion. Such knowledgebase can enable us to rationally design particle-laden
183 interfaces for site-dependent controlled release of lipid soluble active molecules in composite soft
184 matter systems, such as food, personal care and pharmaceutical applications.

185

186 **2. Key players in colloidal structuring of lipids in human physiology**

187 In this review, we are concerned mainly with the physiological re-structuring or resilience-to-
188 destabilization of Pickering emulsion during the trajectory of lipid digestion. Nevertheless, we provide
189 a concise summary of the three sequential regimes (Fig. 2) *i.e.* oral, gastric and intestinal, where
190 complex colloidal structuring might occur with the eventual conversion of lipids to free fatty acids
191 (FFAs) monomers. In particular, we highlight the interfacial role of the key enzymes and biosurfactants,
192 such as mucin (oral), amylase (oral, intestinal), pepsin (gastric), trypsin and chymotrypsin (intestinal),
193 bile salts (intestinal) and most importantly, lipase (gastric and intestinal. This is by no means to
194 underestimate the roles of the inorganic ions (Na^+ , K^+ , Ca^{2+} , HCO_3^-), pH (full spectrum effects from
195 saliva to gastrointestinal juices), and a range of shear-to-surface forces (oral shear, peristalsis, mixing
196 regimes, interactions with mucus-coated surfaces) throughout the aqueous oral-to-gastrointestinal tract
197 on colloidal structuring, aggregation of droplets and phase separation. Detailed information about
198 colloidal aspects of lipid digestion in surfactant stabilised systems can be found in number of review
199 articles [1, 2, 35, 38, 47-49].

200

201 *2.1 Oral phase*

202 Saliva is the first complex fluid that an emulsion encounters upon oral consumption. Emulsions reside
203 in the oral cavity for only a few seconds to minutes, depending upon the oral viscosity and coating
204 abilities. Nonetheless, during tis short time period, the emulsion droplets can undergo a diverse palette
205 of destabilization routes from flocculation (bridging, depletion) to coalescence and phase separation
206 depending upon their interactions with salivary components [50-53]. Human saliva has a neutral pH
207 and contains a range of ions, proteins (*e.g.* mucin, immunoglobulin, statherins, proline-rich proteins,
208 lysozymes, serum albumin), enzymes (amylase) and bacterial cells that are dispersed in 99% aqueous
209 phase [54].

210 *Highly glycosylated salivary mucin (MUC5B)*, which contributes to 10–25% of total salivary
211 proteins is deemed as one of the main components in the dilute saliva that can modify an emulsion's
212 dispersion state. Structurally, salivary mucins are 20% polypeptide core and 80% carbohydrates and
213 have a high molecular weight ($\geq 10^6$ Da) [55]. Emulsion structuring for ionic surfactant-stabilised or

214 protein-coated droplets in the mouth can occur by virtue of electrostatic interactions with mucin, which
215 is negatively charged at oral pH. The charge density of the mucin is associated with the sulphates and
216 sialic acid (*N*-acetylneuraminic acid) parts of the glycosylated constructs. Hence, positively charged
217 emulsions, such as, lactoferrin-coated droplets may undergo bridging flocculation with simulated or
218 real saliva whereas weakly negatively-charged emulsions, such as, β -lactoglobulin-coated droplets
219 undergo depletion flocculation in oral phase [51, 56-59]. The second important component that can
220 have a serious impact on colloidal instability is the enzyme, *salivary α -amylase*, which initiates the
221 hydrolysis of α -1-4 glycosidic bonds in starch in the oral phase. Therefore, α -amylase can rupture the
222 interfacial layer and lead to oil droplet accretion, conditional to the scenario that the interfacial layer
223 contain starch as structural motifs [60, 61]. Besides mucin and α -amylase, salivary ions may induce oral
224 flocculation of droplets via electrostatic charge screening and/or ion binding effects [50, 51, 56]. Oral
225 shear-, surface- and air- [60, 62, 63] induced interactions may also result in droplet coalescence or
226 partial coalescence, with the latter being dependent on the proportion of solid fat content in the droplets
227 at oral temperature.

228

229 2.2 Gastric phase

230 After this relatively short oral residence, emulsions travel through the oesophagus and are subjected to
231 harsh acidic environments (pH 1-3), ions, digestive enzymes (*pepsin* and *gastric lipase*) and mixing
232 vortexes induced by antral contractions as well as shear forces when they reach the stomach [1, 38, 47]
233 (Fig. 2). The physicochemical conditions (pH, ionic strengths) in the stomach may lead to aggregation
234 of the emulsion droplets in the stomach [64]. From a biochemical perspective, proteins are significantly
235 hydrolysed by pepsin to smaller peptides, lipids are only partially digested by acid stable gastric lipase
236 and carbohydrates see almost no breakdown in the gastric regime.

237 Pepsin is a proteolytic enzyme that breaks down the peptide bonds between hydrophobic
238 groups, preferably aromatic amino acids, such as phenylalanine, tryptophan, and tyrosine. Thus, pepsin-
239 induced cleavage can result in modification of the interfacial structure if the droplet surface that contains
240 proteinaceous materials. Pepsin-induced proteolysis may result in interfacial film drainage eventually
241 leading to droplet coalescence [1, 65-68]. Although the majority of lipolysis occurs in the intestinal

242 phase, gastric lipase can contribute to nearly 10-30% of lipid digestion resulting in generation of FFAs
243 in the stomach [69, 70]. Gastric lipase is active in the pH range of pH 3-6, which suggests that gastric
244 lipase-induced lipid hydrolysis can occur even in the first hours of gastric digestion where the pH of the
245 stomach is still elevated owing to the meal buffering capacity [38]. The gastric lipase-mediated fatty
246 acids released in the stomach may have some surface activity and competitive adsorption behaviour
247 versus the parent material at the interface and thus alter the interfacial composition of lipid droplets.
248 However, studies reported in literature on the interfacial aspects of gastric lipase-mediated lipolysis of
249 emulsified lipids are relatively scarce to enable commenting on the interfacial modification with any
250 certainty. This is because of the unavailability of reliable sources of lipases that behave like human
251 gastric lipases until very recently [71]. Depending on the initial interfacial structure (*e.g.* protein,
252 surfactants), lipid composition (*e.g.* solid/ liquid lipid ratio) and degree of interactions with organic and
253 inorganic players in the gastric phase, the fate of emulsion structure can vary from remaining intact to
254 flocculated, coalesced, partially coalesced and phase separated [1, 64, 68, 72].

255

256 2.3 Intestinal phase

257 The majority of the interfacial alteration of the droplets and lipid digestion (70–90%) occurs in
258 the upper part of the small intestine. The intestinal digestion is a complex process due to the presence
259 of a cocktail of amylolytic, lipolytic and proteolytic enzymes, biosurfactant and inorganic components.
260 As the droplets transcend from the stomach to intestine, the pH of the physiological medium reverts
261 back to nearly neutral [65]. Many, if not most colloid scientists have highlighted the key intestinal
262 players to be *trypsin* and *chymotrypsin* for proteolytic action on protein-coated interfaces [65],
263 *pancreatic amylase* for hydrolysis of starch-stabilised interfaces [73] and biosurfactant (*bile salts*) and
264 *pancreatic lipase* [35] for generating fatty acids, mono and/or diacylglycerols from the hydrophobic
265 lipid core besides cofactors (colipase) [74, 75] and other enzymes. For instance, trypsin predominantly
266 catalyses the peptide chains at the C-terminal of aliphatic amino acids, mainly lysine and arginine,
267 whereas chymotrypsin favours large aromatic residues, such as phenylalanine, tyrosine and tryptophan.
268 Such interfacial cleavage can have consequences on altering the interfacial composition in the case of

269 protein-stabilised droplets, such as those stabilised by β -lactoglobulin generating small molecular
270 weight peptides which might not have sufficient viscoelasticity like the parent protein film to prevent
271 droplet deformation [76].

272 The interfacial dynamics becomes most exciting in the intestinal phase as intestinal lipid
273 digestion is an interfacial process that involves a complex interplay between competitive adsorption of
274 lipase/colipase and bile salts at the O/W interface (Fig. 2). Bile salts are a very unconventional, planar-
275 type of biosurfactant that, unlike classical surfactants, do not have a typical hydrophobic head and a
276 hydrophilic tail group [77]. The facial amphiphilicity of bile salts originates from the flat steroidal structure,
277 with the polar hydroxyl groups on the concave side and methyl groups on the convex side. Because of
278 their high surface active properties, bile salts play a crucial role in lipid digestion by displacing the
279 initial adsorbed materials from the interface [78, 79] via orogenic displacement if the parent interfacial
280 film is viscoelastic, permitting lipase/colipase complex to act on the bile-coated oil droplets. The role
281 of the initial charge density at the droplet surface determines to a large extent the kinetics of the
282 sequential binding of negatively charged bile salts to the interfacial material or displacement of the
283 initial adsorbed layer by intestinal bile salts [1, 80]. Besides surface activity, bile salts also facilitate the
284 solubilisation of lipid digestion products into lamellar phase or mixed micelles. Often, bile salts can
285 also remove inhibitory surfactants, such as lipid digestion products (fatty acids, mono/ diglycerides)
286 from the interface via competitive displacement mechanism, thus accelerating and enabling
287 continuation of digestion of emulsified lipid droplets [36].

288 Pancreatic lipase is active approx. between pH 5.5 to pH 7.5 and hydrolyses the emulsified
289 lipids producing two FFAs and a 2-monoacylglycerol [35, 38, 49]. Lipase can only act in the presence
290 of co-lipase and in some cases the presence of co-lipase and bile salts. For lipid hydrolysis to take place,
291 the pancreatic lipase-colipase complex must first adsorb to bile salt-covered interface. Thus, interactions
292 of the adsorbed layer at the droplet surface and lipase are critical in determining the rate of lipid
293 hydrolysis. As lipolysis progresses there is a build-up of fatty acids and monoglycerides at the emulsion
294 interface, which might displace the adsorbed materials. Noteworthy that these lipid digestion products
295 may be surface active but not essentially colloidal stabilizers. Thus, the emulsions generally suffer from
296 droplet coalescence in case of most surfactant-stabilised emulsions in the intestinal stage [1, 72, 76].

297 Nevertheless, bile salts play a key role here in facilitating the desorption of fatty acids and
298 monoglycerides and their solubilisation into the micellar phase promoting further lipid digestion, and
299 some of the bile salts may remain adsorbed to the surface conferring a high negative charge, thus
300 promoting stability [36, 80].

301

302 **3. Experimental investigations on colloidal digestion of Pickering emulsions**

303 As it is obvious from the biophysical aspects of digestion in human physiology, conventional
304 emulsion droplets prepared using surfactants, such as polysorbates or proteins may eventually
305 shrink as the emulsified lipids in the interior of the droplets undergo easy conversion to FFAs
306 during lipid digestion. Therefore, engineering complex interfacial architecture (*e.g.* interface
307 composition and structural attributes) can be one of the promising solutions to modulate the
308 colloidal aspects of lipid digestion. Indeed, the significant advantage of particle-stabilised
309 emulsions over biopolymers- or other surfactant-stabilised emulsions for altering lipid digestion
310 is their unique resilience against coalescence, dissolution and shrinkage mechanisms [5, 27].
311 The mechanism behind such minimal decrease in the volume of the droplets during lipid
312 digestion is the significant energy barrier for particles to detach from the interface offering an
313 almost impossible exchange by the surface active materials in the physiological regimes (*e.g.*
314 bile salts, lipid digestion products). Moreover, the interfacial thickness and surface load are
315 much greater for particle-laden interface offering barrier properties to physiological
316 restructuring in comparison with conventional surfactant-stabilised counterparts [42].

317 Questions arise as to what happens to such particles and particle-covered droplets, when
318 they traverse the various stages of the human oral-to-gastrointestinal tract. Of course, the fate of
319 these systems might be affected by interference from the competing biochemical processes, such
320 as breakdown of Pickering layers of intact starch-based particles by α -amylase [81] or protein-
321 based particles by pepsin and/or trypsin [16]. However, such factors might not affect
322 polysaccharide-based particle- (*e.g.* chitin nanocrystals) [30], organic crystal-(*e.g.* flavonoids)
323 [82] or inorganic particle- (*e.g.* silica) [83] –covered droplets, which are unaffected by

324 gastrointestinal enzymes. This section thus summarizes the key colloidal mechanisms from the
325 experimental investigations of *in vitro* digestion of Pickering emulsions carried out in the last
326 decade (see Fig. 2 for the schematic). We have categorised particle-laden interfaces into two
327 discrete classes, namely, ‘human enzyme-unresponsive’ particles *i.e.* the ones that cannot be
328 digested by human enzymes (*e.g.* amylase, protease) and ‘human enzyme-responsive particles’,
329 latter that can be readily digested by human enzymes. Characteristics of the Pickering emulsions
330 and their digestion data are listed in Table 1.

331

332 *3.1 Enzyme-unresponsive particles*

333 **Silica nanoparticles.** In the case of inorganic particles, silica particles have received much attention
334 not only for their ability to stabilize Pickering emulsions [84] but also for their role in altering the extent
335 of lipid digestion [83]. Using artificial saliva formulation, Ruiz-Rodriguez *et al.* [83] showed that
336 Pickering emulsion droplets of mean size of 3-8 μm stabilised by silica nanoparticles (0.5-5 wt%) had
337 an inter-particle (in other words intra-droplet) aggregation at the interface influenced by the charge
338 screening effects of the salivary salts providing enhanced physical stability to the emulsion droplets.
339 This is unlike the inter-droplet aggregation behaviour observed in ionic surfactant- or protein-stabilised
340 emulsions in presence of artificial or real saliva [56, 58] (Fig. 2).

341 Interestingly, such silica-stabilised emulsions were stable across the physiological range of pH
342 values from 3 to 7, which is advantageous over many oral emulsion formulations that suffer from pH-
343 induced gastric instability. Finally, Ruiz-Rodriguez *et al.* [83] highlighted that bile salts were unable to
344 displace the practically irreversibly adsorbed silica nanoparticles from the interface, in line with another
345 study on silica-laden interface showing similar results with enhanced curcumin retention [85]. The
346 presence of silica particles at the interface reduced the maximum extent of lipid digestion (φ_{max} , %), but
347 interestingly did not affect the initial rate of lipolysis (k , s^{-1}) [83] (Table 1). This might be explained
348 primarily using the size of the gaps (interfacial pores) in the silica particle-laden interfaces. Such gaps
349 can be expected to be sufficiently large to allow the diffusion of angstrom-sized lipase/bile salts complex
350 to the surface to allow instantaneous onset of digestion, but small enough to allow the migration of the

351 FFAs generated during lipid digestion into the continuous phase. In addition, one might recognize that
352 for Pickering emulsions, there is ideally no shrinkage of droplets, so the volume of droplets should not
353 alter and a large portion of FFA produced must remain within the droplets. Hence, one might consider
354 not only measuring FFAs using ‘gold-standard’ titrimetric techniques that measures FFA only after it is
355 released in the continuous phase but also consider measuring the undigested triglycerides together with
356 other digestion products that might have been retained within the dispersed phase or still somehow
357 anchored to the adsorbed phase.

358 **Polysaccharide-based particles.** Besides inorganic particles, biodegradable polysaccharide-based
359 particles, such as cellulose nanocrystals (CNC) or nanofibrillated cellulose (NFC) [28, 29, 86, 87] and
360 chitin nanocrystals (ChN) [30] have been recognized among the most opportune materials as they are
361 not digested by human gastrointestinal enzymes yet are biodegradable. Both cellulose and chitin
362 obtained from plant cell walls and animal sources (sea food wastes), respectively, are essentially
363 naturally-abundant polysaccharides with semi-crystalline architecture containing alternate
364 nanocrystalline and amorphous domains [88-90]. Strong acid hydrolysis can remove the amorphous
365 domains leading to the formation of stiff rod-shaped nanocrystals of high aspect ratio (typically 5–50
366 nm in width and between 100 nm to several micrometers in lengths). Another favorable aspect of using
367 these nanocrystals at the O/W interface is that these anisotropic particles pack in a more ordered fashion
368 but inhomogeneously [91], thus, providing improved steric hindrance and mechanical strengths at the
369 interface even at lower particle loadings, and thus can bring advantage over spherical particles in
370 modulating lipid digestion.

371 One of the earliest studies in the field of digestion of Pickering emulsion was conducted by
372 Tzoumaki *et al.* [30] where the authors compared the digestibility of Pickering O/W emulsions
373 stabilised by ChN with that of the conventional emulsions stabilised by milk proteins. Interestingly,
374 ChN at the interface not only decreased the extent of lipid digestion (ϕ_{max} , %) by two-folds to 33% FFA
375 release (Table 1), as compared to that stabilised by milk proteins, but also significantly reduced the
376 initial rate of digestion (k , s^{-1}). This distinctive reduction in rate of digestion was also shown in studies
377 using NFC [86], which is unlike the behaviour that was observed in the spherical silica-laden interface
378 as discussed previously [83].

379 In addition to the irreversible adsorption of these rod-shaped particles at the interface and
380 inability to be desorbed by bile salts/ lipid digestion products, two other mechanisms [29, 30, 86, 92]
381 were proposed for this delay in lipid digestion (Fig. 2) - 1) the rod shaped particles formed a rigid inter-
382 particle (i.e. intra-droplet) network at the oil–water interface providing a strong mechanical barrier of
383 considerable interfacial viscosity around the droplets, 2) the rod shaped particles underwent isotropic
384 to nematic phase transition forming highly ordered and densely packed network structures in the
385 *aqueous phase*, which might have mechanically entrapped the emulsion droplets and decreased their
386 access to bile salts or lipase. Mechanism 1) is largely associated with packing of rods that can be much
387 more efficient than that of spheres at the interface. Mechanism 2) is similar to trapping emulsion
388 droplets in a gel-like network to create a tortuous path for lipase/colipase complex to reach the
389 hydrophobic lipid core [93, 94], which is achieved in these ChN and CNC particle-laden interfaces
390 without using an additional gelling agent. This highlights that particles can have interesting interfacial
391 as well as bulk rheology that can be carefully engineered to tailor lipid digestion kinetics and develop
392 controlled delivery applications. For instance, Pickering emulsions stabilised by chitosan
393 tripolyphosphate nanoparticles that are engineered *via* ionic gelation technique with lower extent of
394 FFA release have been applied to enhance bioaccessibility of encapsulated bioactive molecules, such as
395 curcumin as compared to nanoemulsion counterparts [95, 96].

396 **Flavonoid crystals.** Another important class of organic particles from biological origin that have been
397 investigated in literature are flavonoid crystals, which are secondary metabolites from plants.
398 Flavonoids, such as tiliroside, rutin and naringin have shown tendency to absorb at oil-water interface
399 [82, 97]. In fact, there has been only one study on flavonoid particles from *Ginkgo biloba* extract that
400 has investigated *in vitro* lipid digestion profile. Yang *et al.* [98] demonstrated that such particles behaved
401 as Pickering stabilizers, however the size and shape of the particles were not mentioned. Such particles
402 reduced both the rate ($k = 0.13 \mu\text{mol s}^{-1} \text{m}^{-2}$) and extent of FFA release ($\varphi_{max} \sim 24\%$) (Table 1) from
403 the flavonoid covered-lipid droplets by nearly two- and four-folds, respectively, as compared to a
404 surfactant-stabilised emulsion.

405

406 3.2 Enzyme-responsive particles

407 Assiduous research has been devoted to the lipid digestion of Pickering emulsions using digestive
408 particles (Table 1). These particles include starch granules and nanoparticles with or without
409 hydrophobic modification with octenyl succinic anhydride (OSA) and a range of protein particles from
410 animal (whey protein microgel, lactoferrin nanoparticles) sources and more recently plant (karifin
411 nanoparticles, zein protein particles, pea protein microgel particles). Such digestible particles have been
412 widely used in scientific investigation for lipid digestion as they are not only safe in theory as they are
413 digestible by human gastrointestinal enzymes but also perceived as relatively more natural, “clean
414 label” and “green” [99].

415 **Starch particle.** Native starch granules are semi-crystalline [100, 101] and the second-most abundant
416 particle after cellulose. The forms of starch used for making Pickering emulsions reported in literature
417 has ranged across length scales from native to OSA-modified starch granules of mean diameter of 1-50
418 μm [102-104] to starch nanoparticles and nanocrystals of mean diameter of few nanometers that have
419 been engineered physically or chemically [105-107]. Although overwhelming amount of research has
420 been conducted on starch particle-laden interface, investigations are relatively scarce when dealing with
421 lipid digestion of such droplets.

422 In fact, only two systematic studies from the Swedish research group [81, 108] demonstrated
423 lipid digestion behaviour of emulsions stabilised by hydrophobically modified quinoa starch granules
424 [81]. Marefati *et al.* [81] demonstrated that amolytic digestion in oral phase by α -amylase resulted in
425 significant size reduction of the emulsion droplets and release of some free starch particles. However,
426 a major proportion of the modified starch granule-coated droplets still retained their integrity and were
427 resilient to coalescence even after 60 min of salivary exposure, unlike the conventional emulsions
428 stabilised by OSA-modified starch, where the latter underwent dramatic coalescence within seconds
429 [60, 61]. The gastric digestion had no effect on these Pickering emulsions as it can be expected owing
430 to lack of any amylolysis. Interesting conclusions were highlighted about the lipid digestion profile in
431 the intestinal phase [81]. Although the starch granules were not likely to be displaced by bile salts, the
432 gaps between these micron-sized starch granules at the interface allowed rather easy accessibility of

433 bile salts and lipolytic enzymes to the interface in the particle-free area, leading to droplet coalescence.
434 **Protein particles from animal sources.** The acceptability of animal proteins and versatility to create
435 microgel, nanogel or nanoparticles using their heat-sensitivity (*e.g.* whey protein, lactoferrin) [15, 16,
436 109] have enabled creation of laboratory synthesized particle of tuneable size to create Pickering
437 emulsions. The distinctive feature of using protein-based particle is that they can offer both electrostatic
438 stabilization and steric hindrance when present as Pickering layers as opposed to starch granules, in
439 latter, the droplets are only sterically stabilised unless modified.

440 Work carried in our laboratory [16] has demonstrated interesting gastric and intestinal digestion
441 profile of emulsion droplets (mean diameter of 43 μm) stabilised using negatively-charged spherical
442 whey protein microgel particles (WPM, 300 nm). These particles were created using a top-down
443 approach of breaking a 10 wt% whey protein gel in a jet homogenizer as opposed to the bottom up
444 approach used previously [15]. The Pickering emulsions stabilised by WPM showed interesting
445 resilience to gastric coalescence unlike conventional whey protein-stabilised emulsions [68], where
446 dramatic increase in the droplet size has been reported due to pepsin-induced rupture of the interfacial
447 protein layer. Looking at confocal microstructure and polyacryl amide gel electrogram of the protein
448 bands from the adsorbed phase of the Pickering layer of WPM, it was concluded that pepsin was not
449 able to fully access some of the hydrophobic sites due to the reburial of those domains within the
450 microgel particles. Noteworthy is that the interfacial loading ($\sim 14 \text{ mg m}^{-2}$) was nearly 12-fold higher
451 than a whey protein monolayer at the interface indicating a substantial increase in substrate required to
452 be digested by pepsin [15] (Fig. 2). Such interesting gastric stability of protein particle versus protein
453 monolayer was also demonstrated in our laboratory also using lactoferrin nanogel particles [110], which
454 was further enhanced when electrostatically complexed with another enzyme-unresponsive
455 polysaccharide particle (inulin nanoparticles). Similar results were obtained by Shimoni *et al.* [109],
456 where kinetic stability to gastric coalescence was imparted when lactoferrin nanoparticles were
457 complexed with polysaccharide, such as alginate and carrageenan.

458 In the intestinal phase, there was stark difference in the digestion profile of protein microgel
459 particle-stabilised interface if the digestion was sequential versus if only bile salts-lipase-catalysed
460 (without any protease) scenario was considered. For instance, if it was a sequential gastric and intestinal

461 digestion [15], presence of WPM particles versus whey protein monolayer at the interface did not affect
462 the rate or extent of fatty acid release as it was a proteolysis-dominated lipid digestion phenomenon.
463 Similar results were obtained using lactoferrin nanoparticle-laden interface that the extent or rate of
464 FFA release was similar to that of a lactoferrin monolayer at droplet surface [111], which might be
465 associated with the proteolytic effect of the pancreatic lipase used that might have contained proteolytic
466 enzyme residues.

467 To understand this better, we carried out lipid digestion investigations with WPM-laden
468 interface in our laboratory using pure lipase and bile salts without any of the proteolysis that normally
469 occurs during the gastric or intestinal digestion stage [15]. The extent of FFA release was reduced by
470 two folds (20%) and initial rate of digestion was diminished (Table 1) when exposed to just pure lipase
471 as opposed to proteolytic-lipolytic mixture. This suggests the inability of bile salts to displace the intact
472 non-proteolysed WPM from the interface. In other words, a large portion of the surface was not
473 available for the adsorption of the lipase/colipase complex. This reduced the overall rate of FFA
474 generation. However, it is noteworthy that the Pickering layer of particles was not impervious but rather
475 semipermeable. Bile salts and lipase being small molecules could access the interface through the gaps
476 in the microgel-stabilised interface, similar to that discussed in starch granule-stabilised interface [81],
477 but bile salts could not displace the microgel particles, due to the very strong binding of the WPM to
478 the interface.

479 **Protein particles from plant sources.** There is burgeoning research interest in designing
480 biocompatible particles derived from plant proteins due to their limited contribution to environmental
481 footprints as compared to the counterparts derived from animal proteins. Filippidi *et al.* [112] took the
482 advantage of water insolubility and slow protease-induced digestibility of zein particles (a prolamin
483 rich protein from corn) to create Pickering emulsions. As discussed in the WPM digestion study [15],
484 the rate-limiting step was again the full or partial hydrolysis of zein particles by gastric/ intestinal
485 proteases, which eventually allowed access of the lipase to the inner lipid core. However, intelligent
486 design of the zein-particulate shell created by solvent precipitation to a greater thickness (4 μm versus
487 1.5 μm in the thinner layer) slowed the rate and extent of digestion remarkably [112]. Another study
488 highlighted that creating particles using zein hydrogen bonded with tannic acid can be an alternative

489 approach to provide protection to Pickering emulsion droplets against a harsh gastric environment
490 [113], facilitating a reduction in the release of FFA during *in vitro* intestinal digestion. Similar Pickering
491 layer approach has been also used using gliadin, another prolamine-rich protein precipitated with a
492 flavonoid (proanthocyanidins) to create particles that was successful in reducing the extent of FFA
493 release ($\varphi_{max} \sim 40\%$) [114] (Table 1).

494 Interestingly, the gastric instability of the plant protein particles was also observed in Pickering
495 emulsions stabilised by karifin particles [115, 116] (Fig. 2), another water-insoluble prolamin protein
496 derived from sorghum. In fact the oil droplets lost their integrity at the end of simulated gastric digestion
497 resulting in macroscopic phase separation as the particle-laden interface was readily pepsinolysed.
498 However, to investigate the possible effect of the kafirin particle layer on lipolysis of emulsified oil
499 droplets, the karifin particle-stabilised emulsions were subjected to intestinal digestion bypassing the
500 gastric regime. As expected, karifin-stabilised droplets showed three-fold slower FFA release kinetics
501 and extent of FFA release ($\varphi_{max} \sim 40\%$) (Table 1) as compared to the surfactant counterpart.

502 Work on Pickering stabilised emulsions created using pea protein nanoparticle aggregates at
503 pH 3 [117] and heated soy glycinin particles [118] have also shown enhanced protection for delivery of
504 a bioactive (β -carotene). However, careful attention needs to be provided in these studies as the reduced
505 extent of lipid digestion and bioactive release was associated with rheological properties of the gel-like
506 emulsion driven by volume fraction of the droplets rather than interfacial architecture of the particles.

507

508 **4. Future interfacial design strategies to control digestion profiles**

509 Particle-laden interface offer new opportunities to control digestion profile in addition to the obvious
510 energy barrier-associated mechanism *i.e.* almost irreversibly anchored particles are unable to be
511 desorbed by bile salts and other lipid digestion metabolites. We now propose a list of design strategies
512 that can be used to manipulate interfacial architecture and composition of particles to enable them to
513 act as transient or complete mechanical barrier to the diffusion of lipases in both gastric and intestinal
514 phases.

515

516 *4.1 Particle to droplet size ratio*

517 Particle size of the Pickering stabilizer plays a determinant role in the fate of the lipid digestion kinetics.
518 According to equation (2), the detachment energy for particles is proportional to the square of the radius
519 of the particle. Thus, the larger the size of the particle, the higher the thermal energy required to dislodge
520 them from the interface. However, one has to be careful about the role of gravitational force versus
521 thermal energy in such a scenario. The ratio of gravity forces to surface tension forces for a particle
522 adsorbed at an interface is represented by Bond number as shown in equation (4):

523

$$524 \quad B_o = \frac{(\rho_p - \rho_c)gd_p^2}{\gamma_{ow}} \quad (4)$$

525

526 where, ρ_p and ρ_c are the densities of the particle and the continuous phase, respectively, d_p is the average
527 diameter of the particle, γ_{ow} is the surface tension and g is acceleration due to gravity. So, it is only for
528 particles with $B_o \ll 1$, surface-tension forces tends to dominate [119]. Furthermore, if the particles are
529 too small, eventually the desorption energy required to dislodge the particles will be low, specifically
530 in presence of the bile salts, where γ_{ow} is small. Thus, use of particle-laden interface might not be
531 beneficial in such a case.

532 Also, it is worth to remind that mostly particle-laden interfaces are generally far from
533 possessing a complete monolayer at the interface and even if the Pickering layer is complete, inter-
534 particle gaps remain. These gaps will tend to allow the passage of the lipase-colipase/ bile salts to the
535 bare interfaces, as discussed previously. For instance, for an idealized case of monodispersed spherical
536 particles, the highest surface coverage is achieved when particles on the droplet surface are arranged on
537 a regular 2D triangular lattice. In such a scenario, the typical dimensions of the gaps between the
538 particles will be $(\sqrt{3} - 1) d_p / 2 \cong 37 \text{ nm}$ for particles of size $d_p = 100 \text{ nm}$. This is nearly fifteen-folds
539 higher than the typical dimension of lipase/colipase complex and thus may not have a substantial impact
540 on creating a barrier against the diffusion of lipolytic catalysts to the droplet interface [16]. Even though
541 the enzymes and bile will be able to access the droplet surface through the gaps between the particles,

542 the available amount of interface can be envisaged to be significantly reduced by the presence of the
543 particles, hence limiting the rate of lipolysis.

544 It is noteworthy that size of particles also determine the size of the emulsion droplets and that
545 the particles are significantly smaller than the targeted emulsion droplet size (at least one-to-two orders
546 of magnitude). Thus, lipid digestion kinetics largely depends on the available surface area of the
547 droplets. For example, emulsions with smaller droplet size will present a larger surface area and
548 therefore a greater number of anchoring sites for lipase. Consequently, to reduce the rate and extent of
549 lipolysis, a coarser emulsion with larger droplet size and lower surface area may be preferable. The
550 alternative to reduce these interstitial spaces will be to employ “polydispersity” of size distribution as a
551 tool to increase surface packing. Although colloid scientists have attempted to create monodisperse
552 particles and eventually monodisperse droplets, polydispersity of particles can be an elegant technique
553 to reduce inter-particle spaces and thus lipid digestion rate, provided such polydispersity is well-
554 controlled. Therefore, there exists a delicate compromise for determining the particles of optimum size
555 distribution to achieve the ideal energy barrier, gap dimension and consequently the droplet size.
556 Ultimately, this may govern the rate of diffusion of lipase and surface area available for lipolysis.
557 Finally, it is worth mentioning that it is always important to provide the FFA release data with the droplet
558 size so that a comparison can be made with the literature, as Pickering emulsion droplets are generally
559 larger in size as compared to surfactant-stabilised emulsions. So, it is important to understand whether
560 the reduction in lipolysis kinetics is linked to the size of the droplets or interfacial architecture created
561 by the Pickering layer of particles

562

563 *4.2 Particle charge*

564 Adsorbed charged particles can be useful to provide electrostatic repulsion between the oil droplets of
565 an o/w emulsion in a similar fashion as ionic emulsifiers. Moreover, they may also help to create an
566 electrostatic barrier to the possible approach of negatively-charged bile salts to the vicinity of a
567 negatively-charged particle-laden interface. However, with increasing magnitude of charge of the
568 particles, there will be a corresponding increase in the interstitial separation due to particle-particle
569 electrostatic repulsion at the interface. Such an approach can be useful to create a porous membrane at

570 the interface in order to accelerate digestion or enhance release of digestion products. However, if the
571 objective is to slow down digestion, one might attempt to increase the salinity of the system to screen
572 the charge so that the particles aggregate at the interface and provide the interfacial barrier effects to
573 lipolysis as was observed in silica-nanoparticle-stabilised interfaces [111].

574

575 *4.3 Particle fusion at interface*

576

577 One of the approaches that has been used to reduce this interfacial spacing has been to adopt the
578 complementary “interfacial particle fusion” *i.e.* sintering of particles once they have been already
579 adsorbed (Fig. 3a). This helps to take the advantage of the energy barrier of the particles combined with
580 a mechanical barrier effect of a cohesive “single” bulky layer. Interestingly, physical treatments, such
581 as use of heat, has been shown to fuse the particles once they are already absorbed in the interfaces.
582 This approach has been used in two independent studies using starch granules [99, 108] (Fig. 3b) and
583 whey protein microgels [16] (Fig. 3c) and has shown dramatic effects on improving the barrier property
584 and delay in FFA release. Since the gaps are expected to be significantly smaller due to this particle
585 fusion, the approach impedes all aspects of the process *i.e.* the diffusion of lipolysis-limiting digestion
586 products, such as FFA away from the reaction sites, as well as that of the lipase/colipase-bile salt
587 complex to the surface. Such fusion can also be brought about using pH shifts, using mono- and divalent
588 ions and/ or enzymatic crosslinking, depending upon the responsiveness of the particles to these aspects.
589 A study of such aspects will demand future research work.

590

591 *4.4 Particle shape*

592 As expected, the “spherical” particles have primarily been investigated to create Pickering
593 emulsions from inorganic silica nanoparticles to bio-derived protein microgels. However, the influence
594 of particle shape on interfacial packing and emulsion stability has attracted relatively little research
595 attention. The non-spherical particles, such as rods, cubes, peanut-shaped particles (Fig. 4) tend to have
596 more positive effects on the emulsion stability *via* differences in packaging density [120, 121]. Even at
597 a lower concentration, particles with higher aspect ratio, such as rod- and peanut-shaped particles can
598 improve the interfacial loading tremendously by creating interfacial stacking, leading to some sort of

599 interlocking structure at the interface. This is demonstrated by hermatite particles [120] and CNC
600 particles [121] in Fig. 4. For instance, Capron et al. [122] created stable o/w emulsions using <0.1 wt%
601 of CNC, as a result of the entanglements between the CNCs. Recently, lipid digestion work using rod-
602 shaped cellulose nanocrystals either at the surface or as a barrier layer are showing interesting lipid
603 digestion outcomes, as discussed previously [28, 29, 86]. In fact, now the time seems ripe for colloid
604 scientists to explore bio-derived anisotropic shaped particles, considering biocompatible processing
605 routes to create such particles and models to understand their emulsion stability during lipid digestion.
606 Such particles may help to control lipid digestion rate by particle networking attributes, not only at the
607 interface but also in the bulk phase as shown in Fig. 2 [30].

608

609 *4.5 Particle loading at the interface*

610

611 Under given emulsification conditions, the initial particle loading can influence the interfacial packing
612 behavior and structure, furthermore affecting the average droplet size and emulsion stability. Once
613 close-packing is established, the loading ceases to have an effect. For classical emulsions stabilised by
614 surfactants, the average droplet size reduces with increasing surfactant concentration until reaching a
615 critical concentration point and then droplet size reaches a plateau [4]. The decreasing trend of droplets
616 size relates to the process that larger droplets breakdown into smaller droplets creating more surfaces
617 due to the reduction of interfacial tension. Pickering emulsions also follow a similar trend in a classical
618 emulsion [43].

619 Chevalier et al. [45] summarized the three stages of Pickering emulsion formation based on the ratio
620 between solid particles (M_p) and the oil mass (M_o). At the low concentration, coalescence occurs due to
621 insufficient quantity of solid particles to cover the droplets. As the solid particle concentration increases,
622 the larger droplets are broken into smaller droplets, leading to a reduction in the average droplet
623 diameter (D_o) as shown in equation (5):

624

$$625 \quad D_o = \frac{6}{\rho_o a_s} \frac{M_o}{M_p} \quad (5)$$

626 where, ρ_o is the density of oil and a_s is the interfacial area covered by the solid particles. In the final

627 stage, the average droplet size reaches a steady state where a complete saturation is achieved. With a
628 high particle concentration, the excess solid particles create either a multilayer or do not get absorbed
629 to the interface and remain dispersed in the continuous phase. With fewer particles, a typical interfacial
630 structure can be a single bridging layer stabilizing the interface between two droplets [123]. Such
631 bridged network can be actually useful to create a network and reduce the surface available for lipase
632 to bind. Note that for incorrectly chosen contact angles, such bridging might instead cause coalescence
633 of droplets. Another option can be to increase the mechanical barrier of the interface by creating a
634 multilayered particle architecture [124] and eventually increase the adsorbed particle loading. If
635 carefully controlled, such multilayers of Pickering particles can help to form a tortuous path for the
636 diffusion of bile salts and lipases' ability to anchor to the interface and thus control the kinetics of lipid
637 digestion.

638

639 *4.6 Material chemistry of particle*

640 Of course, the material of the particles has a crucial role in determining their fate during the sequential
641 lipid digestion. In mind of the previous discussion, it is clear that human enzyme-responsive particles,
642 such as unmodified protein-based or starch-based particles might not be suitable to delay lipolysis if
643 sequential three-phase digestion is considered. As the particles are significantly influenced by
644 biochemical interferences due to their responsiveness to physiological enzymes, they lose their
645 particulate integrity before and during the lipolysis step. Hence, enzyme-responsive particle-stabilised
646 emulsions can only offer altered digestion profile if they are administered specifically at the site rather
647 than typical oral administration routes. One way to avoid this is to modify the interfacial thickness of
648 the particles by precipitation techniques [18] or protect the droplets from instantaneous digestion by
649 changing the particle material chemistry. Such modifications in particle chemistry can be obtained by
650 complexation with human enzyme-unresponsive polysaccharides, such as alginate [111, 125, 126], or
651 tannic acid/ flavonoids [113, 114] or binding with or another layer of enzyme-unresponsive particles,
652 such as inulin [110].

653 Interestingly, from an environmental viewpoint plant proteins are preferred for creating emulsifiers.

654 In fact most plant proteins have limited aqueous solubility [127-130] and are less digestible as compared
655 to animal proteins [18, 130], which restricts their use as classical biopolymeric surfactants. This offers
656 a great window of opportunity for colloid scientists to utilize plant protein aggregates or synthesize
657 particles derived from plant proteins for altering lipid digestion profile. This has indeed started to
658 capture attention of researchers relatively recently. Other opportunities include hydrophobic
659 modification of enzyme-unresponsive polysaccharide particles for tailoring lipid digestion, though
660 careful attention needs to be taken to allow compliance as being “safe” and also “clean-label”, if food
661 application is the ultimate goal.

662

663 **5. Mathematical models for lipid digestion kinetics**

664 In this section, we shift our focus from experimental investigations to review theoretical
665 models which is crucial to quantify lipid digestion kinetics and understand mathematically the
666 similarities and dissimilarities of Pickering emulsions versus a classical surfactant stabilised
667 emulsions. Typically, the pH-stat method is used to monitor the concentrations of FFAs released
668 during the lipid digestion upon introduction of lipase at neutral pH levels. Experimental
669 procedures may commit emulsions to simulated digestion processes by initial incubation in
670 simulated gastric fluid (SGF) and then subsequently in simulated intestinal fluid (SIF).
671 Monitoring and control of changes in pH permit quantification of the concentration of FFA
672 generated during digestion of the emulsified lipids. The percentage of FFA released may be
673 calculated from the number of moles of a base *e.g.* NaOH required to neutralize the FFA that
674 could be produced from the triacylglycerols present in the lipid under the assumption that 2
675 FFAs per triacylglycerol molecules are generated as can be seen in equation (6) [36, 131]:

676

$$677 \quad \%FFAs = \frac{V_{Base} \times M_{Base} \times M_w}{2W_w} \quad (6)$$

678

679

680 where, V_{Base} is the volume (mL) and M_{Base} the molarity (M) of the base respectively, M_w is the
 681 average molecular weight of the lipid (kg mol^{-1}) and W_w is the initial weight of the lipid (g). We
 682 denote the fraction of converted lipid in the emulsion at time t by $\alpha(t)$, which is equivalent to
 683 the fatty acid released $\varphi(t)/\varphi_{max}$ where φ_{max} is the maximum fatty acid level attained after
 684 digestion.

685 A major consideration in developing models to capture possible delays in digestion of
 686 emulsion droplets is to correctly account for the kinetics of arrival and adsorption of enzymes
 687 onto their surface. This is particularly important given that much of the discussion above
 688 concerns development of suitable means of slowing down such adsorption process. It is
 689 reasonable to assume that at any time t , the reaction rate will be a first order one varying linearly
 690 as the fraction of unconverted oil in a droplet, namely $(1-\alpha(t))$. This situation is true for
 691 relatively small droplets one encounters in most practical emulsion systems. For these, the
 692 composition of the droplet remains homogenous throughout, as would be the case if there is
 693 rapid diffusion of unconverted/converted oil between the surface and interior of the droplet (i.e.
 694 concentration gradients within the fine droplets remain small). Furthermore, since such
 695 reactions only occur at the surface of the droplets where the lipase is adsorbed, the reaction rate
 696 is expected to be proportional to the coverage of surface by enzyme at any given time t , i.e. $\Gamma(t)$.
 697 Accordingly, sub-maximal conversion rate constant (per unit area) at time t may be expressed
 698 as:

$$700 \quad \frac{\Gamma(t)}{\Gamma^{Max}} k \quad (7)$$

701 where it is assumed that the surface coverage achieves a maximum of Γ^{Max} , whereupon the lipid
 702 conversion rate constant also achieves its maximum value. Here, k ($\text{mol s}^{-1} \text{m}^{-2}$) is defined as
 703 lipid conversion rate per unit area of the droplet surface, occurring at maximum lipase surface
 704 coverage. In its simplest form, we may expect the value of k to be proportional to the exposed
 705 part of the surface, namely $k=k_o(I - S_p)$. Here, S_p is the fraction of the surface covered by the
 706 particles and k_o represents the rate of hydrolysis per unit area if all the surface of the droplets

707 was available for adsorption by lipase. The value of S_p itself is a sensitive function of the degree
 708 of polydispersity, the shape of the particles, the contact angle at surface and any possible inter-
 709 particle interactions. This makes it rather difficult to calculate S_p for a general case. However,
 710 for some specific ideal situations, a value may be given. For examples, if the particles were
 711 monodispersed hard spheres, then at maximum packing, obtained for a regular 2D triangular
 712 lattice arrangement (see section 4.1), the value of $S_p \approx 0.9$ if the contact angle is 90° , and ≈ 0.45
 713 when it is 45° [16]. Typically estimates for Γ^{Max} coverage can be calculated for the lipase-
 714 colipase complex using the molecular radius of gyration (*e.g.* 25\AA providing an estimate of 2.66
 715 $\times 10^{-7}$ moles m^{-2}) [132]. Thus, for a droplet of size d_0

716

$$717 \quad \frac{\pi d_0^3 \rho_0}{6 M_w} \frac{d\alpha}{dt} = \frac{\Gamma(t)}{\Gamma^{Max}} k \pi d_0^2 (1 - \alpha) \quad (8)$$

718

719 where πd_0^2 is the surface area of the droplet and M_w the molar weight of the lipid molecules. The
 720 general formal solution to the above equation is

721

$$722 \quad \alpha(t) = 1 - \exp\left(-\frac{6M_w}{d_0\rho_0} \frac{k}{\Gamma^{max}} \int_0^t \Gamma(t') dt'\right) \quad (9)$$

723

724 Different more specific forms of equation (9) now emerge depending on how $\Gamma(t)$ varies with
 725 time. Historically, to gain insight into the dynamics of lipid digestion, a first order rate kinetics
 726 model was initially introduced by Ye *et al.* [133]. This early model amounts to assuming that
 727 the adsorption kinetics of lipase onto the droplet surface is very rapid. In such a case the full
 728 lipase coverage is achieved almost immediately and $\Gamma(t) \sim \Gamma^{Max}$ from the onset. This situation
 729 would be appropriate for Pickering type emulsions, since the gaps between the adsorbed
 730 particles on the interfacial surface are sufficiently large to allow unhindered access of the lipase
 731 [16], given that the radius of gyration of the pancreatic lipase/co-lipase complex is
 732 approximately 25\AA [132]. Similarly, the long-time behaviour of any adsorption model, once

733 full coverage has been achieved past a reasonable period of time, increasingly approaches that
 734 predicted by the model of Ye *et al.* [133]. With $\Gamma(t)$ set to Γ^{Max} throughout the digestion process,
 735 equation (9) simplifies to (10) below:

736

$$737 \quad \varphi(t) = \varphi_{Max}(1 - \exp(-k_1 t)) \quad (10)$$

738

739 Here, k_1 (s^{-1}) is the rate of first order kinetics and t is the digestion time (s) in Ye et al model and
 740 can be related to parameters of the more general model according to $k_1 = 6M_w k / (d_0 \rho_0)$. This
 741 model has successfully been used by the same authors to explain the effect of calcium
 742 concentration in promoting lipase adsorption at the interfacial surface. The model has also
 743 proved useful in interpretation of experimental data, allowing an understanding of differences
 744 in reaction rates of emulsions stabilised by different interfacial materials (e.g. bile salts, protein,
 745 protein-particle composites) [29, 36] to be achieved.

746 When the dynamics of enzyme adsorption process is not sufficiently fast, it becomes
 747 important to take the variation of $\Gamma(t)$ with time into account. If arrival of the lipase to the
 748 interface is the limiting factor in determining the rate of adsorption to the surface, then for such
 749 a diffusion-limited process, $\Gamma(t) \approx [(2Dt/d_0) + 2(Dt/\pi)^{1/2}]n$ in the early stages of adsorption,
 750 where D denotes the diffusion coefficient of the enzyme (typically $10^{-9} - 10^{-10} \text{ m}^2 \text{ s}^{-1}$) in the
 751 continuous aqueous phase and n is their molar concentration in the bulk solution. Substituting
 752 this form of $\Gamma(t)$ in equation (9) gives:

753

$$754 \quad \alpha(t) = \frac{\varphi(t)}{\varphi_{Max}} = \left[1 - \exp \left(\frac{-6knM_w}{\rho_0 d_0^2 \Gamma^{Max}} \left(Dt^2 + \frac{4d_0\sqrt{D}}{3\sqrt{\pi}} t^{3/2} \right) \right) \right]$$

755 (11)

756 The second term in the above exponential becomes much smaller than the first one for time
 757 periods $t \gg d_0^2/D$. For typical values of D and emulsion drops of size say $10 \mu\text{m}$, this occurs

758 very early on, $t \sim 0.1$ to 1 seconds. Thus, while still in rather early stages of digestion, equation
 759 (11) can be further approximated to

760

$$761 \quad \alpha(t) = \frac{\varphi(t)}{\varphi_{Max}} = \left(1 - \exp\left(\frac{-6kM_w Dnt^2}{\rho_0 d_0^2 \Gamma^{Max}}\right) \right) \quad (12)$$

762 Equation (12) has a more convenient form for fitting to experimental data. The half-life ($t_{1/2}$)
 763 *i.e.* the time interval whereby half of the initial amount of lipids has been converted to FFA, for
 764 each of the two cases discussed above can be obtained by setting $\alpha(t)=1/2$ in equations (10) or
 765 (12). This yields

766

767

$$768 \quad t_{1/2} = \left(\ln(2) \frac{d_0^2 \rho_0 \Gamma^{Max}}{6kDnM_w} \right)^{1/2} \quad (73)$$

770

$$769 \quad t_{1/2} = \ln(2) \frac{d_0 \rho_0}{6kM_w} \quad (14)$$

771

772 Utilising the parameters k and half-life ($t_{1/2}$) provide valuable information with which to compare
 773 the digestion profiles of different emulsion samples. For example, Sarkar *et al.* [16] successfully
 774 used the above models to understand the differences in the digestion behaviour of Pickering
 775 type emulsions, stabilised by whey protein microgel particles, before and after their heat
 776 treatment. An interesting prediction of equation (12) is a rather slow start to hydrolysis and an
 777 initial “convex shaped” curve (Fig. 3c) for the variation of amount of converted lipid with time.
 778 Though regularly seen in experiments, prior to the work of Sarkar *et al.* [16], this feature was
 779 not fully appreciated and had often been ignored during the fitting of the data.

780

781 The linear variation of the coverage of interface by lipase with time, can also be applied
782 to analyse the early stages of digestion in systems where the adsorption is barrier limited. For
783 these

784

$$785 \quad \Gamma(t) \cong \lambda nt \quad (13)$$

786

787 where instead of $\lambda = 2D/d_0$ as for the diffusion limited case, now the value of λ depends on
788 the thickness, the material and porosity of the barrier layer formed around the droplets. Once
789 again it should be noted that equation (13) applies to time frame where the surface of droplets
790 are only scarcely covered and as yet far from reaching their maximum saturation by bile
791 salt/lipase. There are many models for the variation of $\Gamma(t)$, encompassing the entire adsorption
792 period for the barrier limited situation. However, the usefulness of these in the context of
793 digestion of lipid emulsions is as yet to be fully established. Therefore, for now at least, we
794 refrain from discussing these type of models in any greater detail, leaving such discussion to
795 possible future reviews.

796 The models discussed thus far all assume emulsion droplets that more or less maintain
797 their original size, as lipid is converted to FFA. This is a reasonable assumption for Pickering
798 type emulsions, as was discussed earlier. When the emulsions are stabilised by molecular layers
799 of surfactants or proteins, the picture alters significantly. For now such emulsifiers are displaced
800 by bile salt and in turn any generated FFA can favourably partition into the aqueous phase
801 without much difficulty, resulting in a shrinkage of droplet size. At the same time, the decrease
802 in the surface area that such shrinkage entails may result in desorption of bile salt/lipase,
803 depending on the kinetic of desorption and amount of enzyme already accumulated on the
804 surface at any given time. It is quite reasonable to consider droplets as entirely consisting of
805 unconverted lipids throughout the process, given that originally the aqueous phase is devoid of
806 FFA and the strong tendency of fatty acids to partition into water. This is to say that all
807 generated FFA migrate immediately out of oil droplets. With this assumption, and once again

808 considering the fact that hydrolysis only occurs at the surface, the governing equation for the
 809 variation of droplet size, d , with elapsed time t becomes:

810

$$811 \quad \frac{\pi\rho_0 d^2}{2M_w} \frac{d}{dt} (d) = -\pi d^2 k \frac{\Gamma(t)}{\Gamma^{max}} \quad (14)$$

812

813 Equation (14) together with the initial condition $d=d_0$ at time $t=0$, admits the following general
 814 solution

$$815 \quad d(t) = d_0 \left(1 - \frac{2M_w k}{d_0 \rho_0 \Gamma^{max}} \int_0^t \Gamma(t') dt' \right) \quad (15)$$

816

817 which in turn gives the amount of converted lipid as

$$818 \quad \varphi(t) = \varphi_{Max} \left[1 - \left(1 - \frac{2M_w k}{d_0 \rho_0 \Gamma^{max}} \int_0^t \Gamma(t') dt' \right)^3 \right] \quad (16)$$

819
 820 In general it is quite difficult to theoretically determine the form of $\Gamma(t)$, given the possibility of
 821 competitive adsorption occurring between the bile salt/lipase and an already existing protein,
 822 particularly where such protein has formed a viscoelastic cross-linked surface layer. This
 823 situation is further complicated if any subsequent enzyme desorption kinetics is slow compared
 824 to the rate of droplet shrinkage, thus giving rise to the possibility of $\Gamma(t)$ exceeding Γ^{Max} at some
 825 point during the shrinkage. However, for situations involving none-film forming proteins, as
 826 for example casein, or where the emulsion was stabilised by a relatively low molecular weight
 827 surfactants one may plausibly assume that such complications do not arise. In other words the
 828 kinetic of adsorption and possible desorption of lipase/bile salt are fast enough for enzyme
 829 surface coverage to always be maintained at Γ^{Max} , from the very early stages of digestion all
 830 the way to the end of the process. With this reasonable assumption, it is easy to see that the
 831 general equation ((16) readily simplifies to (17):

832

833
$$\varphi(t) = \varphi_{Max} \left[1 - \left(1 - \frac{2M_w k}{d_0 \rho_0} t \right)^3 \right] \quad (17)$$

834 where as before ρ_0 and M_w are density and molar weight of lipid, respectively and d_0 the initial droplet
 835 diameter. The model encompassing the above assumption was first proposed by McClements and Li
 836 [131, 134] and later solved by Gaucel *et al.* to yield equation (17) [135]. The model predict a fixed
 837 finite time at which droplets will be completely hydrolyzed (*i.e.* shrank to zero). This time is $\tau =$
 838 $\frac{d_0 \rho_0}{2M_w k}$, beyond which equation (17) is no longer physical. Another aspect of the model is that as
 839 droplets shrink, the surface to volume ratio increases and hence the model predicts a rather rapid upturn
 840 in the rate of hydrolysis towards the end of the process. This is thought to not be all that realistic. A
 841 possible modifications to overcome this issue has been discussed by Gaucel *et al.* [135]. Once again if
 842 one is interested in the half-life ($t_{1/2}$), then using (17) this is found to be

843

844
$$t_{1/2} = \frac{\rho d_0}{2kM_w} \left(1 - \frac{1}{\sqrt[3]{2}} \right) \quad (18)$$

845 In Fig. 5, a schematic representation of the mathematical models applicable to the pathways relevant to
 846 surfactant-stabilised or particle-stabilised emulsions. Herein, we provide the modelling pathways relevant
 847 to the various droplet behavior and interfacial dynamics during digestion. Under the assumptions of rapid
 848 adsorption/desorption of surface enzymes and permissible reduction in droplet size, equations (16) and (17)
 849 are relevant where short time digestion and subsequent asymptotic equilibrium is observable. Under
 850 conditions where the droplet size remains stable during digestion, *i.e.* in the case of Pickering emulsion,
 851 equation (9) is the appropriate modelling route and where equation (10) is selected for rapid interfacial
 852 adsorption and in the cases where interfacial dynamics are anticipated, equation (12) is appropriate. In the
 853 latter case it is notable that interfacial adsorption at short-times results in delayed digestion and that the large-
 854 time behaviour (marked in red) of both equations (10) and (12) asymptotically stable, approach a constant
 855 plateau value.

856 In this section, we have discussed several different models currently being used in the
 857 literature to fit experimental data on digestion of emulsion systems. We have sought to provide
 858 a clearer understanding of the connection between various models, by discussing them as

859 limiting cases of a more generalised situation. In doing so, we highlight the limits of validity
860 and underlying assumption in each case. It is important that some thought be given to the type
861 of model that best captures the situation one is investigating, rather than a forced attempt to fit
862 the data to equations for which the underlying model is not necessarily appropriate. When this
863 is done carefully, these models provide useful means to compare the digestion of emulsion
864 systems that possess different surface properties and will facilitate standard parameters to
865 compare reaction behaviour *e.g.* the case where, particles at interface remain intact or fuse
866 together either with or without heat treatments, respectively. We envisage that the future models
867 will provide closed form equations which will accommodate more complex systems where
868 surface and droplet shrinkage dynamics both occur simultaneously.

869

870 **6. Conclusions**

871 The biophysical aspects of lipid digestion of particle-stabilised emulsions is a rapidly growing
872 research domain owing to its fundamental importance to human biology and numerous
873 industrial applications in food, pharmaceutical, personal care, biomedical sectors, such as,
874 designing systems allowing sustained release of lipophilic molecules. Recently, there has been
875 a substantial improvement in the understanding the role of particle-laden interface on modifying
876 colloidal aspects of lipid digestion. We have provided the first systematic, balanced and
877 comprehensive summary of experimental investigations as well as mathematical models for
878 lipid digestion of Pickering emulsion droplets within this review. The key benefits of using
879 Pickering emulsions is the ability of these particles to resist any competitive displacement by
880 surface active bile salts by virtue of high desorption energies of these particles. Although the
881 gaps between the particles may provide access to the lipolysis enzymes, but the area available
882 for lipase to bind is significantly reduced due to the presence of the particle on the droplet
883 surface, providing further benefits to reduce the kinetics and extent of digestion. Besides intact
884 particles, some attempts have been made in literature to include particle fusion, such as using
885 heat treatments after thermos-labile particles have been adsorbed at the interface in order to

886 reduce those interstitial pores and consequently, delay lipid digestion. Particle shape anisotropy
887 has also been shown to offer interesting features in altering digestion profile by not only
888 influencing interfacial adsorption and surface packing to reduce interfacial porosity but also
889 impacting bulk interactions with key lipid digestion players. In order to adequately compare
890 different mathematical models ranging from simple first order kinetics to those that account for
891 kinetics of lipase-binding and interfacial dynamics, a decision tree has been proposed based on
892 underlying assumptions and boundary conditions to ensure validity of the models. In summary,
893 in order to adequately manipulate lipid digestion kinetics, we propose specific interfacial design
894 strategies for future investigations focussing on particle physics and chemistry as well as the
895 development of closed-loop mathematical models.

896

897

898

899 **7. References**

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1232

1233 **Table 1.** Summary of literature reports on Pickering O/W emulsions where *in vitro* lipid digestion kinetics

1234 was followed.

1235

Type of particles (<i>E</i> = Human enzyme-responsive, <i>U</i> = Human enzyme-unresponsive)	Particle Shape & Size Range (d_p = diameter, l_p = length, h_p = height, t = shell thickness)	Emulsion droplet size (μm)	<i>In vitro</i> digestion regimes	Intestinal lipid digestion with kinetic data			Reference
				k	φ_{max} (%)	$t_{1/2}$ (min)	
Silica nanoparticles (<i>U</i>)	Spherical, d_p = 50-500 nm	4 – 8	Oral, Intestinal	\approx control	\sim 50%*, <control	-	[83, 85]
Nanofibrillated cellulose (NFC) (<i>U</i>)	Fibre, d_p = 57 nm, l_p = Several μm s	9 – 24 μm	Sequential (Oral-Gastric-Intestinal)	7.5-12% FFA/min*, <control	\sim 78-84%*, <control	-	[86]
Chitin nanocrystal (<i>U</i>)	Rod, d_p = 18 nm, l_p = 240 nm	5 – 7 μm	Intestinal	$2.0 \times 10^{-4} \text{ s}^{-1}$, <control	33%, <control	-	[17, 30, 92]
Chitosan-tripolyphosphate nanoparticles (<i>U</i>)	Spherical, d_p = 214–522 nm	19 – 86 μm	Sequential (Oral-Gastric-Intestinal)	-	33%, <control	-	[95, 96]
Flavonoid glycosides from <i>Ginkgo biloba</i> extracts (<i>U</i>)	-	1 μm	Intestinal	$0.13 \mu\text{mol s}^{-1} \text{ m}^{-2}$, <control	33%, <control	9.8, >control	[98]
Starch granules (<i>E</i>)	Polyhedral, d_p = 1.8 μm	27 – 32 μm	Oral,	Relative lipolysis rate: heated < not heated	-	-	[81, 99, 108]
Starch granules with heat treatment (<i>E</i>)			Gastric, Intestinal		-	-	
Whey protein microgel particles (WPM) (<i>E</i>)	Spherical, d_p = 300 nm	43 μm	Sequential (Gastric-Intestinal),	0.31** $\mu\text{mol s}^{-1} \text{ m}^{-2}$, <control	42%, 20%***, <control	6.6, 16.5**, >control	[16]
Whey protein microgel particles with heat treatment (HT-WPM) (<i>E</i>)			Only Intestinal step without proteases**				
Lactoferrin nanoparticles (LFnp)	Spherical, d_p = 200 – 400 nm	1 – 11 μm	Sequential (Oral-Gastric), Intestinal	\approx control	\sim 64%*, \approx control	-	[109, 111, 126]
Lactoferrin nanoparticles complexed with alginate (LF-ALG) (<i>E/ U</i>)		1 – 56 μm		<control	\sim 50%*, <control	-	
Lactoferrin nanoparticles complexed with carrageenan (LF-CAR) (<i>E/ U</i>)		3 – 9 μm		>control	\sim 70%*, >control	-	
Zein particle shell (<i>E</i>)	Spherical, t = 1.5 – 4 μm	30 – 40 μm	Sequential (Gastric-Intestinal I)	<control	\sim 40-100%*, <control	-	[112]
Zein + tannic acid (<i>E</i>)	- , d_p = 96 – 203 nm	25 – 45 μm	Sequential (Gastric-Intestinal)	<control	\sim 4-6%*, <control	-	[113]

Gliadin aproanthocynaidins (E) +	Spherical, $d_p= 87-290$ nm	53-94 μ m	Sequential (Gastric-Intestinal)	<control	~40%, <control	~40*, >control	[114]
Karifin nanoparticles (E)	$d_p= 92 - 434$ nm		Gastric, Intestinal	<control	~38%, <control	-13.23***, > control	[115, 116]

1236 - k = rate of lipid digestion, φ_{max} = maximum extent of FFA release (observed or theoretical), $t_{1/2}$ = time interval

1237 whereby half of the initial concentration of lipids has been converted to FFA (observed or theoretical)

1238 No data (-), Derived data from the graphs (*), Bypassed proteolysis (**), Indicative