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1 **Experimental Quantification of Intrusion Volumes Due to Transients in Drinking**  
2 **Water Distribution Systems**

3  
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16  
17 **ABSTRACT**

18 We are currently unable to fully assess the risks to human health and wellbeing from  
19 contaminant intrusion into drinking water distribution systems due to lack of understanding  
20 and accurate estimation of intrusion volumes during dynamic pressure events. This paper  
21 presents results quantifying such volumes from carefully controlled but representative  
22 physical three dimensional experiments. Results show how the volumes change as a function  
23 of the dynamics of the driving pressure and how these volumes can be estimated from the  
24 time integral of the measured driving head. Results also reveal the complex coupling of  
25 dynamic pressure behaviour interacting with the leak orifice and the exchanged volumes. The  
26 findings of this work can be integrated within assessment frameworks to enable better  
27 estimation of intrusion volumes and hence management of risk to public health.

28 **INTRODUCTION**

29 Water suppliers are legally and morally responsible for the quality of drinking water  
30 that issues from customers' taps, such as set out in drinking water quality standards (EU

31 Drinking Water Directive 98/83/EC). These standards and expectations are becoming  
32 increasingly more stringent and water quality failures are known to occur. Such failures occur  
33 for a number of reasons, such as discoloration of water caused by a change in hydraulic  
34 conditions and contamination of the source water. In many instances failures cannot be  
35 explained. A possible source of such failures is the contamination of drinking water due to  
36 the intrusion of pollutants into the distribution system from the surrounding soil and water.  
37 Leakage apertures provide a possible pathway for this. Leakage is an accepted feature of  
38 distribution systems. It is realised that, due to the ageing asset infrastructure, the elimination  
39 of all leakage is unlikely to be feasible or economically justifiable. In the UK, network  
40 utilities can lose up to 575 million litres per day through leakage (Brydon, 2013). Such  
41 leakage is considered to occur outwards due to the pressure differential between the water in  
42 the pipe and the lower pressure in the surrounding ground. Risks associated with long term  
43 depressurisation, such as to fix a pipe burst, should be mitigated with good working practices.  
44 However, distribution networks are dynamic systems with frequent changes in hydraulic  
45 conditions. Such changes induce transients in the form of pressure waves that move  
46 throughout the network. Transient events may induce low or even negative pressures over  
47 relatively short durations. Hence, the pressure of the water inside the pipe may briefly be  
48 lower than the pressure outside the pipe and there is potential for intrusion. Such intrusion  
49 volumes are likely to be small but may contain harmful contaminants. The smallest traces of  
50 certain contaminants may cause a water quality failure whilst others may seed bacterial  
51 growth, including within biofilms where they may be protected from disinfection residuals,  
52 ultimately impacting on public health.

## 53 **LITERATURE REVIEW**

### 54 **Health Impacts**

55 There is published evidence of water contamination as a possible cause of health  
56 issues. This includes epidemiology studies by Payment et al. (1991 and 1997) and  
57 randomised trials by Hellard et al. (2001). Craun and Calderon (2001) analysed waterborne  
58 disease outbreaks and their origins from 1971-1998 in the United States of America. They  
59 found that in this period 113 out of 619 disease outbreaks were caused by chemical and  
60 microbial contaminants entering public drinking water distribution systems (DWDS),  
61 although it is estimated that the true number might be much higher due to accuracy and  
62 reliability of data collection. From those 113 events, more than 21,000 cases of illness were  
63 reported mostly attributed to Giardia and bacterial pathogens, including 498 hospital and

64 emergency room visits and 13 deaths. In the UK, Hunter et al. (2005) reported results from a  
65 postal questionnaire, finding a strong association between loss of water pressure at the home  
66 tap and the incidence of diarrhoea and estimated that the cost of such illness could exceed  
67 £100 million per annum in England and Wales (15% of the total estimated annual cost of  
68 diarrhoeal disease).

## 69 **Intrusion Mechanisms**

70 Research and evidence exists for the three components of contaminant intrusion risk  
71 as set out by Lindley and Buchberger (2002). Contaminants undesirable in drinking water  
72 have been shown to exist in the soil surrounding pipes (LeChevallier et al. (2003), Karim et  
73 al. (2003), Besner et al. (2006)). Pathways including leaks, cracks, submerged air valves,  
74 badly fitted joints/seals, and cross connections exist throughout distribution systems.  
75 Evidence is emerging which supports the dynamic nature of distribution systems and the  
76 widespread frequent occurrence of transient events (McInnis and Karney, 1995; Ebacher et  
77 al., 2011; Starczewska et al., 2013) while some research directly evidences the occurrence of  
78 low and negative pressure transients (Walski and Lutes 1994, Qaqish et al. 1995, Karim et al.  
79 2003, Gullick et al., 2005, Fleming et al 2006 and Besner et al. 2007). Kirmeyer et al. (2001)  
80 performed transient modelling on the Montreal distribution system, where Payment  
81 conducted his epidemiology studies, and found that more than 90% of nodes would  
82 experience negative pressures under certain scenarios, such as power surges.

## 83 **Laboratory Testing**

84 Boyd et al. (2004a) provided the first experimental confirmation of the potential for  
85 contaminant intrusion into pressurised water mains during transient events, but under  
86 idealised conditions. Their configuration used an external column of water placed above a  
87 manually operated check valve and pre-drilled orifice mounted on the test pipeline. The  
88 transients were generated by a system valve closure, and required a manual synchronised  
89 valve opening on the external column. While this finding provided proof of intrusion for an  
90 idealised condition, their experiments were limited as *“neither the volumetric nor the*  
91 *chemical tracer method provides an accurate estimate of the actual volume of contamination*  
92 *associated with a specific event”*.

93 Research by Fox et al (2015) moved substantially closer to reality using a pipe with  
94 an orifice buried in a gravel media, to show that net intrusion and transport of material  
95 originating external to pipes can occur due to transient conditions. While this experiment did

96 provide repeatable quantification of volume and estimation of the sphere of influence around  
97 the leak aperture, it did not allow for volume to be estimated across a range of transient  
98 conditions, which is essential for risk assessment.

## 99 **Operational Systems**

100 Research reported in Besner et al. (2007 and 2010) conducted experiments to  
101 determine if negative pressure caused by a transient resulted in contaminant intrusion in  
102 operational distribution systems. In the 2007 study a transmission main was rapidly closed  
103 and although sustained negative pressures were recorded, no significant water contamination  
104 was detected. The 2010 study investigated the same distribution system used by Payment et  
105 al (1991 and 1997) and Kirmeyer et al (2001). In the 2010 study, bacterial indicators of faecal  
106 contamination were found more frequently in the water found in flooded air-valve vaults than  
107 in the surrounding soil or water. This suggests that air-valve orifices can provide a critical  
108 pathway for contaminant intrusion. Although the paper does not provide direct evidence, the  
109 authors strongly suggest a link to the negative pressures shown during long-term pressure  
110 monitoring. While the risk for air-valves can be mitigated by good operational management,  
111 Besner et al. (2010) show that bacterial contamination has been found in soil and water  
112 surrounding pipes, hence leaks which cannot be easily managed could provide a pathway for  
113 contaminant intrusion.

## 114 **Modelling**

115 Any attempt to quantify the risks associated with contaminant intrusion requires the  
116 estimation of intrusion volumes. The most common method to do this is via some form of the  
117 Torricelli or orifice equation, Equation 1, such as in Funk et al., (1999); Kirmeyer et al.,  
118 (2001); LeChevallier et al., (2003); Boyd et al (2004b); Fleming and LeChevallier, (2008);  
119 Ebacher et al. (2012).

$$Q = C_D \frac{\pi d_o^2}{4} \sqrt{2g} \sqrt{H_D} \quad \text{Equ. 1}$$

120 Where Q is orifice flow rate,  $C_D$  is coefficient of discharge,  $d_o$  the diameter of the leak orifice  
121 (assumed to be circular) and  $H_D$  the driving head.

122 While the orifice equation has been applied for estimation of intrusion volumes, its  
123 widest application to drinking water distribution systems is in the field of leakage. Farley and  
124 Trow (2003) demonstrated that the exponent for head can vary from 0.5 to 2.79; this was

125 attributed by van Zyl and Clayton (2007) to the orifice expansion or contraction due to  
 126 pressure, which strongly depends on its shape and the on pipe behaviour. However it is now  
 127 suggested that a modified orifice equation using a 0.5 exponent is a more realistic description  
 128 of leakage and intrusion flows for variable pressure (van Zyl et al., 2017). Cassa et al. (2010)  
 129 showed that round holes present the smallest expansion with pressure – a maximum area  
 130 increase of 1.4% for a 12 mm diameter hole in a 110 mm unplasticised Poly Vinyl Chloride  
 131 (uPVC) pipe under a 60 m pressure head. The small change in area for an orifice under  
 132 pressure corresponds to a pressure head exponent close to the historical value of 0.5. Fox et al  
 133 (2016) explored pressure-area-flow rate effects in plastic pipes and concluded that the orifice  
 134 equation, with a constant coefficient of discharge, is suitable for accurately estimating  
 135 dynamic leakage flow rates from longitudinal slits, provided that the leak area is suitably  
 136 incorporated.

137 The coefficient of discharge is also commonly found to vary as a function of  
 138 resistance effects, including due to the orifice shape and local entry and exit conditions.  
 139 Collins and Boxall (2013) developed and verified a modified coefficient of discharge for an  
 140 orifice submerged in porous media experiencing steady state leakage or intrusion. The  
 141 expression incorporated parameters capturing the effects of the surrounding porous media,  
 142 including the inertial resistance,  $B$ , the orifice losses,  $k'$  and a geometric shape factor,  $G$ .

$$Q = \frac{1}{\sqrt{k' + \frac{d_o g \sqrt{GB}}{6}}} \frac{\pi d_o^2}{4} \sqrt{2g} \sqrt{dH} \quad \text{Equ. 2}$$

143 Besner et al (2011) provided a review of the components that should be considered  
 144 and included in a quantitative microbial risk assessment (QMRA) framework for the public  
 145 health risks associated with intrusion events. They conclude that while such risks can be  
 146 estimated, they are based on several assumptions. They particularly note that population  
 147 exposure is dependent upon both the quantity of pathogens entering the system and the  
 148 duration of intrusion - both of which are time integral functions of the intrusion flow rate.

## 149 AIMS

150 The main aim of this research was to experimentally quantify the volume of  
 151 contaminant intrusion through an orifice in a representative physical system when subjected  
 152 to hydraulic transients causing negative pressures. The work sought to investigate how the  
 153 volume intruded changed with respect to the transient conditions as defined by the change in

154 system pressure and flow rate and due to the presence of media external to the orifice. The  
155 work also aimed to explore the application of the orifice equation to quantify these volumes.

## 156 **MATERIALS**

157 The large scale laboratory facility at the University of Sheffield (Collins and Boxall,  
158 2013; Fox et al., 2015) was used. The system comprises 140 m of 50 mm internal diameter  
159 medium-density polyethylene (MDPE) pipeline, configured as a recirculating system. Water  
160 is fed from an upstream reservoir through a 3.5 kW Wilo MVIE variable speed pump. System  
161 flow rate and pressure is controllable through this variable speed pump and a downstream  
162 control valve. Flow rate was measured with an Arkon Flow Systems Mag-900  
163 electromagnetic flow meter. Pressure was measured by four Gems 2000 series Pressure  
164 Sensors, with a manufacturer stated accuracy of  $\pm 0.16$  m. Maximum conditions possible  
165 were 4 l/s and 40 m for flow rate and steady state pressure head respectively, providing  
166 conditions fully representative of operational drinking water distribution systems. Quarter  
167 turn butterfly valves are located throughout the pipeline capable of rapid manual closure to  
168 produce highly repeatable transients.

169 A circular orifice was installed in the pipe invert in a straight section of the pipeline,  
170 approximately 75 m from the reservoir tank using a 2 mm diameter drill bit. Due to residual  
171 stresses of the MDPE material, the actual diameter created was 1.55 mm. A circular hole was  
172 chosen to minimise pressure dependent area effects, as covered in the literature review (Fox  
173 et al, 2016). The size was chosen based on initial experiments to provide measurable  
174 intrusion volumes and to be representative of the type of background leakage that may be  
175 prevalent and go unrepaired within operational systems.

176 In order to measure the volumes exchanged through the leakage orifice the main pipe  
177 line was enclosed within a 400mm length of larger 380mm diameter outer pipe that had a  
178 single relatively unconstrained overflow (see Figure 1). The outer pipe was located centrally  
179 around the inner pipe. The outer pipe was made of stiff acrylonitrile butadiene styrene (ABS)  
180 with an 8 mm wall thickness. The outer pipe was capped at both ends by aluminium plates  
181 secured with bolts, creating a volume surrounding the orifice. This outer pipe and associated  
182 end plates were stiff such that any possible changes in volume due to dynamic pressures  
183 during experiments were minimised. While assumed small, any volume changes of the main  
184 MDPE pipeline due to dynamic pressures are a consistent effect across all tests. This would  
185 also be part of the mechanism driving intrusion in operational systems. The outer volume was

186 sufficient such that the internal flow field within it was not affected for the ranges of flow and  
187 pressure available in the system, based on simulations in computational fluid dynamics  
188 (CFD) by Collins et al (2010).

189 To monitor the net movement from an external source into the system, a clear riser  
190 pipe was fitted above a secondary 12 mm orifice in the external pipe directly above the  
191 primary leakage orifice. This inlet/outlet point creates the sole pathway for fluid from the  
192 riser pipe into the pipeline system. The level in this riser pipe was monitored to quantify  
193 intrusion. The diameter of the riser pipe was designed such that its entry and exit losses were  
194 minimal compared to the primary leak orifice, but such that observable changes in level  
195 occurred in the riser pipe.

## 196 **METHODS**

197 Results are reported here for the intrusion volume measured as the result of complete  
198 instantaneous closure of a butterfly valve immediately upstream of the test section. This  
199 provided a range of transients in the test section each with an initial down surge. Initial  
200 conditions were varied independently to provide a range of transient conditions: for a set  
201 initial pressure of 20 m, flow rates in steps of 1 l/s from 1 l/s to 4 l/s; and for a set initial flow  
202 rate of 2 l/s, pressure heads in steps of 10 m from 10 m to 40 m. These values were chosen to  
203 give conditions representative of operational water distribution systems. Five repeats were  
204 carried out for each initial condition creating 35 experimental cases for two types of media in  
205 the external volume (see Table 1). The order of experiments was randomised and the system  
206 flushed between experiments including removal of any air. Once the desired initial conditions  
207 were set, the system was allowed to stabilise for at least 10 minutes before a transient was  
208 created. The two types of external media were water and pea gravel (diameter 3 to 8 mm and  
209 average porosity of 42 %). In order to ensure that the gravel media remained fully  
210 consolidated and minimise formation of voids, the gravel was rigorously compacted during  
211 filling and a water filled bladder pressurised to 32 m was installed behind one of the end  
212 plates to provide a compressive force on the solid particles. The gravel was periodically  
213 checked and maintained over the experimental period.

214 An SVSi Gigaview high speed video camera was used to record the water level in the  
215 riser pipe at 50 frames per second. The volume of intrusion was assessed by tracking the  
216 locations of the meniscus in the riser pipe. Repeated cycles of drops and rises were found  
217 between maximum and minimum meniscus locations due to the dynamic cyclic nature of



218 transients (see Figure 2). The drops in the meniscus level indicated fluid flowing from the  
219 outer pipe into the orifice through the surrounding media, these were considered as intrusion.  
220 The cumulative drop was calculated, calibrated from an adjacent graduated scale, and then  
221 multiplied by the internal area of the riser pipe to produce a total volume of intrusion in  
222 millilitres. Given the frame rate, image resolution and meniscus detection the average  
223 accuracy of volume estimate was  $\pm 1.3$  ml.

## 224 **RESULTS**

225 Figure 3 shows four examples of the transients created in the system across the  
226 various conditions set out in Table 1. The surrounding material is water in all cases. Each  
227 sub-figure includes five repeats evidencing the repeatability of the system. The time taken for  
228 the system to reach equilibrium after the valve closures ranged from approximately 6 s to 14 s  
229 as a function of the conditions being studied, but irrespective of the surrounding material.  
230 Figures 3 b) and d) show maximum negative pressures ‘flat lining’ at cavitation pressure  
231 around -10 m. Low or negative pressures sufficient to cause intrusion were generated for all  
232 the conditions reported here, i.e. a drop in meniscus level greater than experimental error  
233 indicating net movement of fluid into the main pipeline.

234 Figures 4 a) and b) present results of experimental intrusion volumes for both water  
235 and gravel media external to the leak orifice. Figure 4 a) shows results for an initial flow rate  
236 of 2 l/s and varying initial head. Figure 4 b) shows results for an initial head of 20 m and  
237 varying initial flow rate. For both water and gravel external to the leak orifice it can be seen  
238 that as the initial pressure head increases, the volume of intrusion into the system decreases;  
239 also as the flow rate increases, the volume of intrusion increases. The linear regression lines  
240 shown all demonstrate a good fit with  $R^2$  values above 0.9. In both cases the gradient terms  
241 between water and gravel are similar.

242 Table 2 presents the average volumes of intrusion, from 5 repeats, for each of the  
243 hydraulic conditions set out in Table 1. The table includes direct comparison of how these  
244 volumes change as a function of the external water or gravel media. The results show that,  
245 under the same initial conditions for transient generation, the intrusion volumes are  
246 consistently lower when the orifice is surrounded by gravel rather than water, as also evident  
247 in Figure 4. Tentative trends can be seen in the difference between the two media as a  
248 percentage of the water intrusion volumes – as the flow rate increases, the percentage  
249 difference decreases; as the pressure head increases, the percentage difference increases.

250 **ANALYSIS**

251 An aim of this research was to explore the application of orifice equation based  
252 expressions to estimate intrusion volumes. The approach adopted was to assume that orifice  
253 flow could be estimated by applying Equation 1 at each instantaneous time when the driving  
254 head was negative and that these could be integrated over time to provide an estimate of the  
255 intrusion volume. The intrusion driving head,  $H_D$ , was defined as the external pressure  
256 indicated by the meniscus head in the riser pipe (measured from the meniscus to the point of  
257 intrusion, i.e. the orifice) minus the pressure in the pipeline. Only the negative driving head is  
258 considered for intrusion to occur.

Where

$$Q_O = C_D A_0 \sqrt{2g} \sqrt{H_D} \quad \text{Equation 3}$$

And

$$H_D = H_M - H_S \quad \text{Equation 4}$$

Thus

$$V_I = \int Q_O dt = C_d A_o \sqrt{2g} \int \sqrt{H_D} dt \quad \text{Equation 5}$$

259 Where  $Q_O$  is the instantaneous intrusion flow rate,  $A_0$  the orifice area,  $H_M$  is the  
260 external meniscus head,  $H_S$  the system head, and  $V_I$  the intrusion volume.

261 If the coefficient of discharge, area and acceleration due to gravity are constant, then  
262 from Equation 5 there should be a linear relationship between intrusion volume and the time  
263 integral of the square root of the negative driving head. The system head was measured by  
264 the pressure transducers; however, the meniscus head is a function of the fluid height in the  
265 riser pipe which changed over the duration of the intrusion events as recorded on the video  
266 images (Figure 2). Two methods were applied to assess the meniscus head to determine the  
267 driving head over time. The first using the average meniscus head over the transient duration.  
268 The second involved interpolation of the 50 Hz video data to the 300 Hz of the pressure data  
269 and calculating the driving head at every time point. The difference between the two method  
270 was found for a random sample of 6 transients (9 % of total tests) covering both gravel and  
271 water cases. The difference in calculated volumes was no greater than a maximum of  $\pm 0.18$

272 %. This can be explained by the variation in driving head being negligible compared to the  
273 driving head itself, therefore an approximately linear relationship exists between flow rate  
274 and pressure head. The simpler method was adopted for the complete data set.

275 Figure 5 shows that a linear trend is evident, for the data collected here, between the  
276 time integral of the square root of the negative driving head versus experimental intrusion  
277 volumes, with coefficients of determination,  $R^2$ , of 0.92 for the water and 0.87 for the gravel  
278 cases. Using the trendline gradients the  $C_d$  for water is calculated as 0.55, and for gravel as  
279 0.57. This suggests that there is little difference in the combined coefficient of discharge, area  
280 and gravity effects between the two cases.

281 To further investigate the linear relationship shown in Figure 5, in particular if there  
282 was any association between the coefficient value and the different transient conditions,  
283 individual values of the coefficient of discharge were also calculated. No trend or pattern in  
284 these values could be found despite various ordering and replotting of the data.

## 285 **DISCUSSION**

### 286 **Experimental Methodology and Method**

287 The research reported here has shown that under idealised laboratory conditions  
288 pressure transients can lead to quantifiable intrusion of water through a leak orifice, aligning  
289 with previous literature (Boyd et al, 2004a and b; Fox et al, 2015). While the experimental  
290 configuration used here was full scale and fully three dimensional it required fluid exchange  
291 to occur through the pipe leakage orifice and through the outer pipe volume channelled to the  
292 single riser pipe. The internal diameter of the riser pipe was 12 mm, thus loss effects  
293 associated with this should have been small compared to the main leakage orifice of 1.5 mm  
294 diameter. The flow through the outer pipe was from the leakage orifice in the invert of the  
295 main pipe to the riser pipe at the top of the outer pipe. The outer pipe was sized to be large  
296 enough to avoid edge effects and to allow full three dimensional flow, based on CFD  
297 simulations (not shown). It is likely, however, that the flow paths in the external volume will  
298 have been different between test cases and in particular between cases with gravel and water  
299 media filling the outer volume. Arguably the overflow at the crown of the outer pipe is  
300 similar to leakage flow towards a ground surface, but this is not always the main route of  
301 leakage flows and concentration to a single point is unrealistic. This point overflow will have  
302 induced some additional resistance effects as the flow paths focus to this point, particularly so  
303 in the gravel cases, however due to the larger diameter of the external pipe and the riser pipe

304 this will be substantially smaller than at the leaking orifice. While it is relevant to note these  
305 idealised factors of the experimental set up, they were constant across the experimental  
306 conditions and effects were small compared to the effects of interest.

307 It is possible that the transients could have been altered due to mechanical changes in  
308 the pipe material. Experimental data collected by Gally et al. (1979) shows strong effects of  
309 temperature on transient behaviour – an increase in temperature can decrease pressure  
310 fluctuations due to a lower propagation speed. Additionally, transient damping is affected by  
311 the stress-time history as the pressure waves result in retarded deformation of the pipe wall,  
312 Covas et al. (2004). Both of these effects were controlled and minimised here. The  
313 temperature difference within and between the experiments using different media was less  
314 than 2°C. The order of experiments with different initial conditions was randomised meaning  
315 that any such effects would manifest in scatter of the experimental data, which is low.

316 It is possible that there was movement of the gravel during and between experiments  
317 allowing the creation of a small void immediately external to the leak orifice, despite the use  
318 of a bladder to restrict this. However, experiments were randomised and the pressure in the  
319 bladder checked regularly, hence there should have been no consistent effect of this, with any  
320 impact manifesting as scatter in the data, Figure 3 b). But this scatter is comparable between  
321 media in Figure 4 suggesting any such effects were minimal.

### 322 **Transient Intrusion Mechanisms**

323 The data presented here provides definitive evidence that as the magnitude of the  
324 negative pressure increases so the intrusion volume increases. From Figure 4 a) it can be seen  
325 that for a given change in flow, and hence initial pressure surge, as the initial pressure in the  
326 system is increased the observed intrusion volume decreases. This is because the datum  
327 pressure is effectively increasing so the magnitude of negative pressure decreases, evident by  
328 comparing Figures 3 b) and c). Conversely Figure 4 b) shows that for a fixed initial pressure,  
329 increases in initial flowrate (equivalent to velocity for a fixed diameter) cause an increase in  
330 the observed intrusion volume. This change in pressure transient is evident by comparing  
331 Figures 3 b) and d), although manifest as greater period at cavitation pressure rather than a  
332 greater negative pressure.

### 333 **Application of Orifice Equation**

334 Linear correlations were observed between intrusion volumes and the time integral of  
335 the square root of measured negative head differential, Figure 5. From this is it evident that

336 using a time integral form of the orifice equation it is possible to estimate intrusion volumes,  
337 supporting the use of an orifice theory based equation in this analysis and estimation of  
338 intrusion volumes through fixed area orifices. It should be noted that the calculation of the  
339 time integral of the square root of the measured negative head differential is very sensitive to  
340 the zero datum, i.e. the pressure at which the flow is being driven into or out of the pipe. It is  
341 possible that in particular the dynamic resistive effects in the external media, meant that the  
342 zero datum was not constant throughout a given transient tests. However, the intrusion  
343 volumes calculated here were not significantly different for the average and more detailed  
344 methods explored in Analysis.

345 Collins and Boxall (2013) developed and validated for low (up to +/-10m) head  
346 steady state conditions an equation that accounted for gravel media effects external to a leak  
347 orifice. The gravel was expected to impart additional resistance effects immediately outside  
348 the leakage orifice, which were expected to be made apparent through a reduction in the  
349 coefficient of discharge. Application of this using the properties of the gravel used here yield  
350 a modified coefficient of discharge of 0.56. This value agrees with the average fitted values  
351 calculated from Figure 5 between the gravel and water cases, 0.55 and 0.57, respectively.  
352 From the data presented by Collins and Boxall (2013) it is apparent that the orifice effects  
353 associated with a 1.5 mm orifice are dominant over gravel media effects so this result is  
354 perhaps not surprising.

355 From Figure 4 and Table 2 it can be seen that for transients generated with the same  
356 initial system conditions the volumes of intrusion are consistently lower when there is gravel  
357 surrounding the orifice rather than water. Under steady state conditions the effect of gravel  
358 media external to an orifice is known to reduce the orifice flow rate. Thus the presence of the  
359 gravel media could be expected to reduce the intrusion volume. Under transient conditions  
360 there is a complex coupling of the driving head due to the transient, exchange of volume  
361 through the orifice (both leakage and intrusion) and the dissipation of the transient in the pipe  
362 system. Lower resistance to exchange through an orifice should result in greater intrusion  
363 volumes, but dissipates the transient faster resulting in less overall driving force and hence  
364 lower volumes. Conversely increasing the resistance to flow through an orifice (adding gravel  
365 media externally) should decrease the volume, but it also decreases the dissipation effects and  
366 hence increases the overall driving force.

367 Figure 6 shows a comparison between transients generated by valve closures from  
368 initial conditions of 4 l/s and 20 m for water and gravel. The initial waves in both cases are

369 very similar, suggesting that the changes due to the external conditions were not very  
370 significant, similar to the repeatability evident in Figure 3. Thus there is no significant  
371 change in driving transients, but due to the sensitivity of the calculation of the intrusion  
372 volume to the time integral of the square root of measured negative head differential this  
373 could still be sufficient to explain the change in volumes observed and calculated here.

#### 374 **Practical Implications**

375 Overall the research presented here provides physical evidence from controlled but  
376 realistic experiments of how intrusion volumes change as a function of transient conditions,  
377 within the limits of the experimental setup. The work also shows that the time integral of the  
378 square root of the negative driving head can be used to estimate intrusion volumes, but only if  
379 the driving transient pressure profile is well quantified. This indicates a need to radically  
380 improve our ability to model the propagation of pressure transients in operational systems,  
381 including accounting for all damping / dissipation effects and network uncertainty; from  
382 friction and viscoelastic material effects to network uncertainties such as pipe material,  
383 diameter, connectivity etc. and uncertainties of leakage (location, size, orifice shape, external  
384 media etc.). The research reported has particularly highlighted the complex coupling of the  
385 driving head due to the transient, exchange of volume through the orifice and the dissipation  
386 of the transient.

387 It should be noted that the intrusion volumes reported and estimated here are worst  
388 cases, no consideration is given to push-pull exchange through the orifice; it is simply  
389 assumed that any volume that has been external to the pipe, even if only for a short period, is  
390 a contamination risk. This work better informs the volume estimations integrated into QMRA  
391 frameworks and hence enhances understanding of contamination risks.

#### 392 **CONCLUSIONS**

393 The work presented here supports previous research providing physical evidence that  
394 contaminant intrusion can occur due to dynamic pressure transient events within water  
395 distribution systems. Specifically, the work shows how intrusion volumes change as a  
396 function of the hydraulic conditions within in a full scale laboratory pipeline that replicates  
397 operational environments. Expected underlying trends have been clearly evidenced: as the  
398 change in velocity increases (increasing initial pressure surge) the volumes of intrusion  
399 increase; and as the change in pressure increases (increasing the initial pressure offset) the  
400 volumes of intrusion decrease. Analysis has demonstrated that the time integral of the square

401 root of the negative driving head can be used in an integral form of the orifice equation to  
402 predict observed intrusion volumes. However, the required orifice discharge coefficient is  
403 found to be consistent across cases with gravel and water media surrounding the leak orifice.  
404 This is despite smaller volumes being measured and estimated for the gravel cases. Further  
405 analysis reveals that this is due to the complex coupling between the dynamic pressures and  
406 exchange through the orifice. This paper has improved the understanding of intrusion  
407 volumes. However, in order to make accurate estimates of intrusion volumes and fully assess  
408 the risks of contaminant intrusion, a step change improvement in our ability to model  
409 transients across complex pipe systems is required.

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