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Pellis, Alessandro, Comerford, James W. [orcid.org/0000-0002-9977-5695](https://orcid.org/0000-0002-9977-5695), Maneffa, Andrew J. et al. (3 more authors) (2018) Elucidating enzymatic polymerisations : Chain-length selectivity of *Candida antarctica* lipase B towards various aliphatic diols and dicarboxylic acid diesters. *European Polymer Journal*. pp. 79-84. ISSN 0014-3057

<https://doi.org/10.1016/j.eurpolymj.2018.07.009>

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1 Elucidating enzymatic polymerisations: chain-length selectivity of *Candida antarctica* lipase  
2 B towards various aliphatic diols and dicarboxylic acid diesters

3

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6

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12

13 Keywords: enzymatic polymerisation, biobased polyesters, solventless synthesis, *Candida*  
14 *antarctica* lipase B, enzymatic selectivity

15

16 Abstract

17 The sustainable synthesis of polymers is a field with growing interest due to the need of  
18 modern society to preserve the environment whilst making used products and food  
19 sustainable for the future generations. In this work we investigate the possibility of  
20 synthesizing aliphatic polyesters derived from various dicarboxylic acid diesters and diols  
21 in a solvent-free reaction system. *Candida antarctica* lipase B was selected as biocatalyst  
22 and its selectivity towards the carbon and ester chain length were elucidated. The selected  
23 enzyme was able to synthesize various polyesters combining C<sub>4</sub>-C<sub>10</sub> diesters and C<sub>4</sub>-C<sub>8</sub>  
24 diols. All combinations led to monomer conversions above 90% in 24 h with the best  
25 number average molecular weights (M<sub>n</sub>) being obtained through the combination of  
26 dimethyl adipate and 1,8-octanediol leading to a M<sub>n</sub> of 7141 Da. Differential scanning

27 calorimetry analysis shows a clear trend with an increase in melting temperature of the  
28 polymers that correlates with both the increase of the  $M_n$  or of the polymer's constitutional  
29 repeat unit carbon chain length. Thermogravimetric analysis and rheology measurements  
30 performed on selected samples also confirm the trend showing a variation of the polymer's  
31 degradation temperatures and viscosity profiles.

32

### 33 Introduction

34 The application of biocatalysts in organic synthesis offers several advantages compared  
35 with traditional chemo-catalysts such as milder reaction conditions with regards to  
36 temperature (usually  $T < 100$  °C), pressure and pH (normally 3-8). Such conditions often  
37 lead to remarkable energy efficiency, high enantio-, regio- and chemo-selectivities as well  
38 as controlled stereochemistry. These features allow the development of new functional  
39 compounds for pharmaceuticals, agrochemicals and polymers using nontoxic natural  
40 catalysts with a significant "green" appeal having commercial benefits and satisfying  
41 ecological requirements [1].

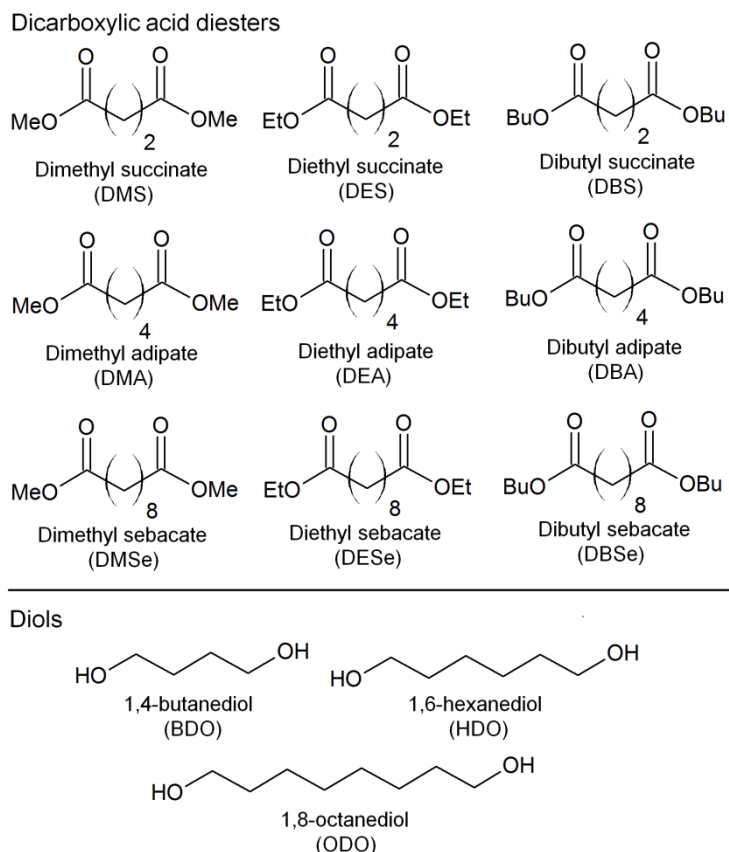
42 Despite studies focused on the use of glycosidases for the synthesis of natural and  
43 unnatural polysaccharides [2], as well as oxidoreductases for the polymerisation of phenol  
44 derivatives [3] and vinyl monomers [1] (mainly using laccases and peroxidases), the most  
45 investigated area of enzymatic synthesis is the production of polyesters via both  
46 polycondensation (transesterification) and ring opening polymerisations (ROPs) [4,5].  
47 These areas have predominantly emerged thanks to the discovery and commercial  
48 availability of *Candida antarctica* lipase B (CaLB). Over recent years the extraordinary  
49 properties of this enzyme were brought to light from several research teams in the kinetic  
50 resolution of organofluorine rac-alcohols [6], the synthesis of glucoside esters [7] and the  
51 enantioselective synthesis of a  $\beta$ -amino acid ester via a solvent-free chemo-enzymatic  
52 reaction among others [8].

53 Further to this, CaLB has been shown to be an active catalyst for the synthesis of a wide  
54 range of aliphatic [9], aliphatic functional [10, 11] (e.g. polyesters containing lateral  
55 functionalities such as vinyl and hydroxy groups) and aliphatic-aromatic polyesters [12,13]  
56 and polyamides [14]. In recent years these polyesters and polyamides have been derived  
57 preferentially from renewable monomers such as 2,5-furandicarboxylic, adipic and succinic  
58 acids and 1,4-butanediol among others [5].

59 Despite several other enzymes belonging to the hydrolases family, namely cutinases from  
60 *Humicola insolens* [15], *Fusarium solani pisi* [16] and *Thermobifida cellulosilytica* [17],  
61 being reported to be active for the synthesis of various polyesters and polyamides in their  
62 lyophilized and immobilized forms (ranging from cross-linked enzyme aggregates to  
63 covalent binding [18, 19]), the choice of the chemist is still often the readily available CaLB  
64 adsorbed on a methacrylic resin known under the tradename of Novozym® 435. This  
65 biocatalyst has been shown to be active and stable in several different conditions ranging  
66 from water-based to anhydrous organic media and up to temperatures of ~100 °C.

67 Among the many synthesis studies both on polycondensation and ROPs that were  
68 performed over the years using this enzyme, we found there is a lack of comparative  
69 studies on the range of monomers shown in Scheme 1 (most of which bio-based) [20] for  
70 the synthesis of aliphatic polyesters.

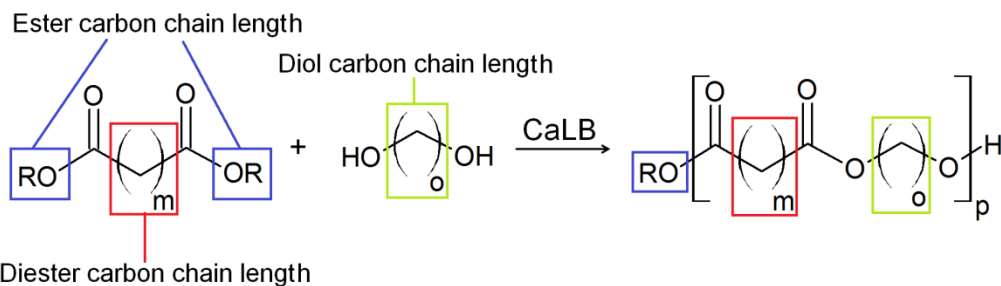
71



72  
73 Scheme 1. Dicarboxylic acid diesters (top) and linear diols (bottom) used in this study for the enzymatic  
74 synthesis of aliphatic polyesters in solvent-free systems using *Candida antarctica* lipase B as biocatalyst.  
75

76 Despite the many studies on the topic, there remains an absence of any detailed  
77 systematic study into the implications of changing the diester and/or diol whilst applying  
78 identical methodologies for the polymerisation. In the present study we investigated the  
79 CaLB-catalyzed polycondensation of various methyl-, ethyl- and butyl- dicarboxylic acid  
80 esters with various linear diols having a carbon chain length of 4, 6 or 8, shedding light on  
81 how reactive different size diesters are when employing enzymatic catalysis in a solvent-  
82 free reaction system (Scheme 2). These results will/help(ed) us to understand the  
83 strengths and weaknesses of using this, until now, sporadically investigated enzyme for  
84 polyester synthesis.

85



86  
87 Scheme 2. The three parameters that were investigated in the present study, namely 1) ester carbon chain  
88 length; 2) diester carbon chain length and 3) diol carbon chain length.  
89

## 90 Materials and methods

### 91 Chemicals and enzymes

92 1,4-butanediol (BDO) was purchased from Alfa Aesar. Dimethyl adipate (DMA) and 1,8-  
93 octanediol (ODO) were purchased from Acros Organics. Dimethyl succinate (DMS) was  
94 purchased from Fluka. All other chemicals and solvents were purchased from Sigma-  
95 Aldrich and used as received if not otherwise specified. *Candida antarctica* lipase B  
96 (CaLB) immobilized onto methacrylic resin was purchased from Sigma-Aldrich (product  
97 code L4777) (N435). The enzyme was dried under vacuum for 96 h at 25 °C and stored in  
98 a desiccator prior to use.

### 99 Enzymatic polycondensation of aliphatic polyesters

100 0.006 mol of dicarboxylic acid ester (A) and 0.006 mol of linear diol (B) (diester:diol ratio=  
101 1.0:1.0) were accurately weighted in a 25 mL round bottom flask. The mixture was then  
102 stirred at 85 °C until a homogeneous melt was obtained. 10% w w<sup>-1</sup> (calculated on the total  
103 amount of the monomers) of N435 was then added and the reaction was run for 6 h at  
104 1 Atm. A vacuum of 20 mbar was subsequently applied for an additional 18 h maintaining  
105 the reaction temperature at 85 °C (total reaction time: 24 h). The reaction product was  
106 recovered by adding THF (or DCM in the case of the 24 h succinate-BDO polymers) in  
107 order to dissolve the solid reaction products. The biocatalyst was then removed via a  
108 filtration step and the solvent evaporated under vacuum. The polymers were then  
109 characterised without additional purification steps.

110 Nuclear Magnetic Resonance (NMR) Spectroscopy

111  $^1\text{H}$ -NMR analyses were performed on a JEOL JNM-ECS400A spectrometer at a frequency  
112 of 400 MHz.  $\text{CDCl}_3$  was used as NMR solvent for all synthesized polymers.

113 Gel Permeation Chromatography (GPC)

114 GPC was carried out using a PSS SDV High set composed of 3 analytical columns ( $300 \times$   
115  $8$  mm, particle diameter  $5 \mu\text{m}$ ) of 1000,  $1000 \times 10^5$  and  $10^6 \text{ \AA}$  pore sizes, plus guard column  
116 (Polymer Standards Service GmbH, PSS) installed in a PSS SECcurity SEC system.  
117 Elution was with THF at  $1 \text{ mL min}^{-1}$  with a column temperature of  $23 \text{ }^\circ\text{C}$  and detection by  
118 refractive index.  $20 \mu\text{L}$  of a  $\sim 2 \text{ mg mL}^{-1}$  sample in THF, adding a drop of toluene as  
119 reference standard, was injected for each measurement and eluted for 50 min. Calibration  
120 was carried out in the molecular weight range 370-2520000 Da using the ReadyCal  
121 polystyrene standards supplied by Sigma Aldrich and referenced to the toluene peak.

122 Differential Scanning Calorimetry (DSC)

123 Traditional DSC analyses were performed on a TA Instruments Q2000 under nitrogen  
124 atmosphere. The heating rate used was  $5 \text{ }^\circ\text{C min}^{-1}$  over a T range of  $-60$ - $200 \text{ }^\circ\text{C}$ . Cooling  
125 rate was set at  $5 \text{ }^\circ\text{C min}^{-1}$  over the same T range. Sample mass was of 5-10 mg for all  
126 measured samples. The polymer's melting ranges were calculated from the second  
127 heating scan using the value at peak maximum option.

128 Thermogravimetric analysis (TGA)

129 TGA was performed on a PL Thermal Sciences STA 625 thermal analyzer.  $\sim 10$  mg of  
130 sample was weighted in an aluminium pan. The sample was then placed into the furnace  
131 with a  $\text{N}_2$  flow of  $100 \text{ mL min}^{-1}$  and heated from 21 to  $625 \text{ }^\circ\text{C}$  at a heating rate of  $10 \text{ }^\circ\text{C}$   
132  $\text{min}^{-1}$ . From the TGA profiles the temperatures at 5% and 50% mass loss (TD5 and TD50)  
133 were subsequently determined.

134 Rheology measurements

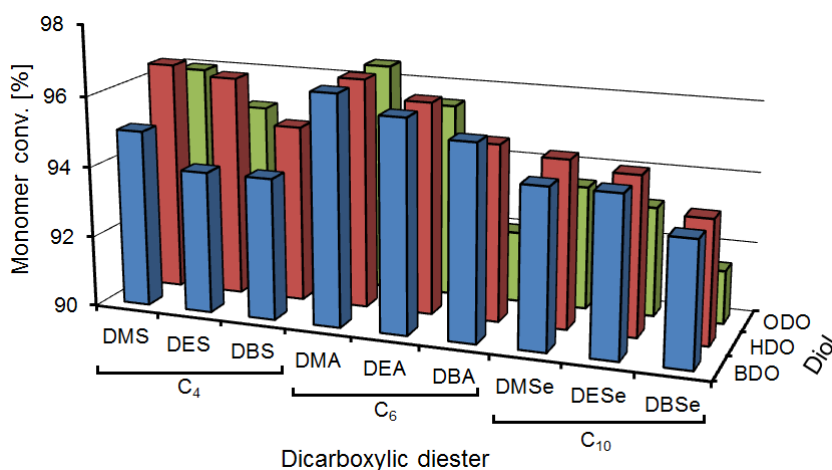
135 Rheological rotational measurement under controlled shear rate were recorded using a  
 136 Brookfield R/S-CPS+ Rheometer fitted with a Peltier P-TS2 temperature controller and  
 137 cone-plate geometry where the cone used had a 25 mm diameter, 2° angle and 0.045 mm  
 138 gap height. The polymer samples were ground with a pestle and mortar prior to being  
 139 loaded onto the pre-heated (80 °C) bottom plate. In all cases, a constant shear rate of 100  
 140 s<sup>-1</sup> was maintained throughout the experiments with each polymer melt being initially held  
 141 at 80 °C (under shear) for 120 s before the temperature was decreased by 0.01 °C s<sup>-1</sup>.

142

### 143 Results and Discussion

144 The CaLB-catalysed polycondensation of methyl-, ethyl- and butyl- succinic (C<sub>4</sub>), adipic  
 145 (C<sub>6</sub>) and sebacic (C<sub>10</sub>) dicarboxylic acids esters with linear diols having a carbon chain  
 146 length of 4, 6 or 8 atoms were investigated. In order to be environmentally friendly, all  
 147 reactions were performed in bulk (i.e. solvent-less). All monomers were melted at 85 °C  
 148 before adding the biocatalyst that allowed the initiation of the step-growth  
 149 polycondensation. From the <sup>1</sup>H-NMR spectra analysis it is possible to observe that for all  
 150 reactions excellent monomer conversion values (>90%) were obtained with the methyl and  
 151 ethyl esters consistently giving slightly higher conversions than the equivalent butyl esters  
 152 for all the dicarboxylic diesters investigated (Figure 1).

153



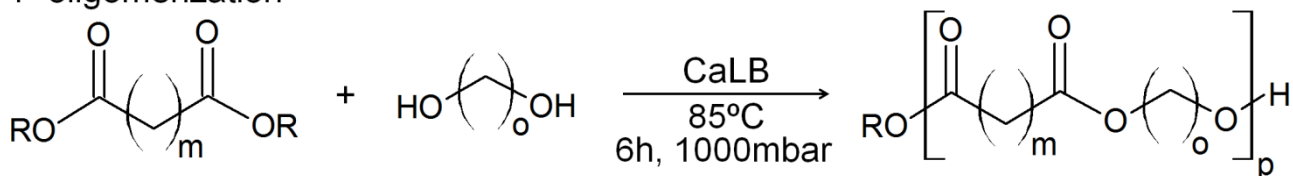
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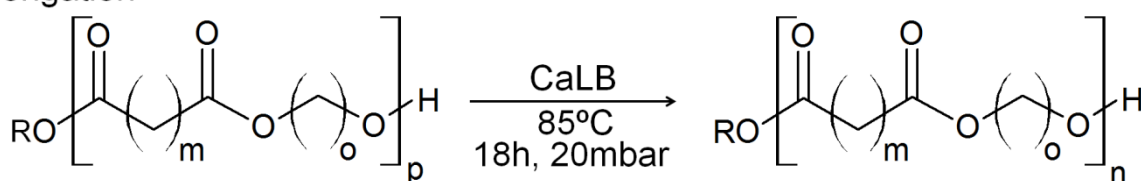
155 Figure 1. <sup>1</sup>H-NMR analysis of the crude polycondensation products after CaLB-catalyzed polycondensation  
 156 reactions after 24 h. Reactions without catalyst led to no detectable transesterification products. All reactions  
 157 were performed in duplicates. Statistical analysis reporting the mean value ± standard deviation for all  
 158 reactions can be found in ESI, Figure S1 and the complete spectra assignment in Figure S5.  
 159

160 The 2-step polycondensation protocol (1st-oligomerization and 2nd-chain elongation)  
 161 reported in Scheme 3 was found suitable for all the reactions (see Table 1). The  
 162 polycondensation reactions occur via transesterification of dicarboxylic acids diesters with  
 163 aliphatic diols and follow a step-growth polymerisation mechanism (the same as some  
 164 other similar synthetic polymers such as polyamides and polyurethanes). In fact with low  
 165 DP (~5-10) the conversion is already >80-90% and further increase in DP (two fold)  
 166 influences only minor the monomer conversion. This allows the initial oligomerisation of  
 167 most of the monomers without loss of any of the starting compounds. After oligomerisation  
 168 is achieved, vacuum is applied to effectively remove the alcohol by-product and enables  
 169 the elongation of the polymeric chain length. The biocatalyst is indeed able to catalyse  
 170 synthetic reactions starting from long polymeric chains as recently reported by Vastano et  
 171 al. who coupled dimethyl itaconate and poly(ethylene glycol) to poly(hydroxyalkanoates)  
 172 having M<sub>n</sub> of 50188 Da and M<sub>w</sub> of 117720 Da produced using an engineered strain of  
 173 Escherichia Coli [21].  
 174

#### 1- oligomerization



#### 2- elongation



R= -methyl, -ethyl or -butyl

o= C<sub>4</sub>, C<sub>6</sub> or C<sub>8</sub>

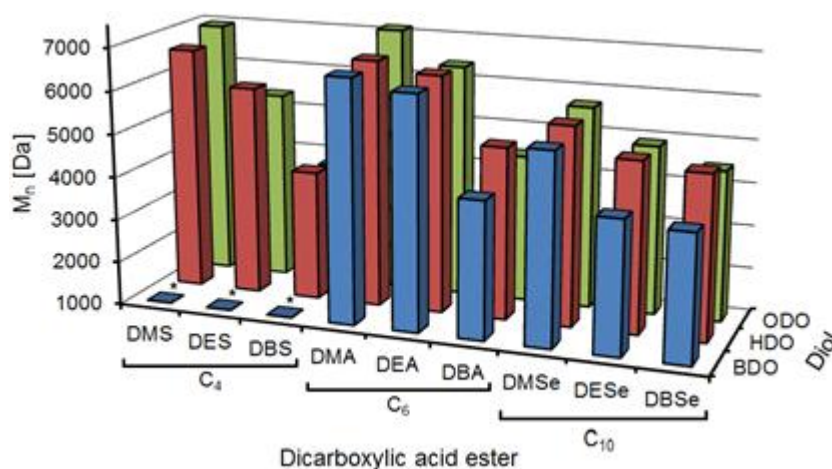
m= C<sub>2</sub>, C<sub>4</sub> or C<sub>8</sub>

175 Scheme 3. The 2-step polycondensation protocol used for the synthesis of various aliphatic-aliphatic  
 176 polyesters via enzymatic catalysis in bulk (n>p).  
 177

178

179 The number average molecular weight ( $M_n$ ) (Figure 2) and the weight average molecular  
180 weight ( $M_w$ ) (see Figure S2 in ESI) of the polymers were determined via GPC analysis.  
181 The  $M_n$  trend reported in Figure 2 agreed well with the  $^1\text{H-NMR}$  spectroscopy monomer  
182 conversion analysis reported in Figure 1. The methyl and ethyl diesters lead to the  
183 synthesis of polymers having higher molecular weight relative to the butyl diesters. This  
184 effect of the size of the alkyl group of the diester (-methyl, -ethyl and -butyl) becomes less  
185 marked when increasing the diester internal chain length from  $C_6$  to  $C_{10}$ . The lower  
186 conversions and molecular masses obtained using butyl diesters is most probably due to  
187 the relative boiling points of the alcohol by-products with methanol (BP= 64.7 °C) and  
188 ethanol (BP= 78.4 °C) being significantly less volatile than butanol (BP= 117.7 °C) and  
189 therefore easier to remove from the reaction system, especially when considering a  
190 reaction temperature of 85 °C was used. The polymers synthesized using the shortest  
191 dicarboxylic esters, dimethyl succinate (DMS), diethyl succinate (DES) and dibutyl  
192 succinate (DBS) together with 1,4-butanediol (BDO) were not soluble in the GPC mobile  
193 phase (THF) and therefore were not characterised using this technique.

194



195  
196 Figure 2. Number average molecular weights ( $M_n$ ) calculated via GPC analysis of the crude  
197 polycondensation products using a 370-2520000 Da polystyrene calibration curve. Reactions without  
198 catalyst did not lead to detectable polyesterification products. All reactions were performed in duplicates.  
199 Statistical analysis reporting the mean value  $\pm$  standard deviation for all reactions can be found in ESI,  
200 Figure S2. \*=reactions non soluble in the GPC mobile phase (THF).

201

202 The generally observed trend for the synthesised polymers based on HDO and ODO  
203 having higher molecular masses than the BDO equivalents (with the exception of the  
204 adipate-based polyesters that showed similar molecular masses) reflects very well the  
205 data reported by Feder and Gross for the polycondensation of sebacic acid and various  
206 diols using N435 at 70 °C. [15] In this previous work, a comparison between adipic and  
207 sebacic acid was made and fully agrees with our observation that the adipic acid diesters  
208 lead to higher molecular weight products than the sebacic diesters when methyl and ethyl  
209 esters were used while no significant differences were observed when butyl esters were  
210 used. It was noticed that CaLB, when operating in a solventless reaction system, led to  
211 smaller differences between the different ester chains than when using cutinases and  
212 serin-hydrolase enzymes belonging to the same family. [22] In fact, whereas CaLB leads  
213 to similar conversions with BDO, HDO and ODO, cutinases have a preferred substrate.  
214 Cutinase from *Humicola insolens* (70 °C, in bulk, diol diacid 1:1 mol/mol, 1% w/w of  
215 enzyme-to monomer, application of vacuum after 2 h) produces polyesters with higher  
216 molecular weight when ODO is used as a diol [15] while cutinase 1 from *Thermobifida*  
217 *cellulosilytica* (Thc\_cut1) (70 °C, in bulk, diol diacid 1:1 mol/mol, 10% w w<sup>-1</sup> CaLB  
218 immobilized onto methacrylic resin-to monomer, application of vacuum for 24 h) prefers  
219 BDO, leading to only short oligomers when HDO and ODO are used in combination with  
220 dimethyl adipate. [23] For Thc\_cut1, it was recently reported that the structure of the diol is  
221 relevant for the chain length, but the conversion is not much affected. [17]

222 In order to be able to analyze the differences between all reactions, including the formation  
223 of aforementioned insoluble poly(butylene succinate), some selected reactions (reported in  
224 Table 1) were run for only 6 h at 85 °C and atmospheric pressure in order to stop the  
225 reaction after the initial oligomerisation phase.

226

Table 1. Comparison of the CaLB-catalyzed polycondensation reactions after 6 h at 85 °C and 1000 mbar and 24 h.

Diester	Diol	Time [h]	Conv. [%] <sup>#</sup>	M <sub>n</sub> <sup>*</sup> [Da]	M <sub>w</sub> <sup>*</sup> [Da]	Đ <sup>*</sup>	M <sub>0</sub>	DP <sub>n</sub>	
DES	BDO	6	89	851	1094	1.29	172.2	4.9	
		24	94	ns	ns	ns		x	
	HDO	6	92	2164	2398	1.26	200.2	9.8	
		24	96	5853	10439	1.79		29.2	
DMA	BDO	6	89	2227	2843	1.31		200.2	10.1
		24	97	6626	11549	1.71			33.1
DBA	HDO	6	83	2018	2247	1.07	228.3	9.5	
		24	95	4978	8018	1.62		21.8	

<sup>#</sup> Calculated via <sup>1</sup>H-NMR based on the conversion of the diol.

<sup>\*</sup> Calculated via GPC using a - Da polystyrene calibration curve and toluene as internal standard.

ns= non soluble in THF

227

228 From the collected data it is possible to see that the insolubility of poly(butylene succinate)  
 229 in THF, even after stirring for several days, is not due to the high molecular weight of the  
 230 polymers. It is well known that the dissolution of polymers depends not only on their  
 231 physical properties, but also on their polarity, molecular weight, branching, crosslinking  
 232 degree and crystallinity. [24] In this particular instance, given the crystalline nature of all  
 233 produced polymers it is probable that the insolubility of the succinate-based aliphatic  
 234 oligoesters after 24 h reaction was indeed a result of high crystallinity rather than the  
 235 oligomers as evidenced by the molecular masses data reported in Table 1 (and the DSC  
 236 data reported later). The calculation of the DP of the reactions after 6 and 24 h fully  
 237 confirms the trend previously reported via <sup>1</sup>H-NMR spectroscopy and GPC for all of the  
 238 other reactions carried out (Table 1).

239 In addition to monomer conversion and molecular weight analysis, differential scanning  
 240 calorimetry analysis for the determination of the polymers' melting points and  
 241 thermogravimetric analysis for the determination of the mass loss were performed. Figure  
 242 3 reports the melting temperatures of all the synthesized polymers when the standard  
 243 protocol (6 h at 1000 mbar, 18 h at 20 mbar, 85 °C, 10% w w<sup>-1</sup> CaLB, 24 h total reaction  
 244 time) was applied. It is possible to observe a general trend where an increase in polymer  
 245 melting point aligns with increasing carbon chain length of the diester, where C<sub>4</sub>-based

246 polymers have lower melting points than the C<sub>10</sub>-based polymers. This is due to the  
 247 crystallinity of the C<sub>4</sub>-based polymers as discussed above. A similar increase is also  
 248 observed when increasing the diol carbon chain length from C<sub>4</sub> (BDO, blue) to C<sub>8</sub> (ODO,  
 249 green). In this case, increasing the dicarboxylic ester length from C<sub>4</sub> to C<sub>8</sub> reduces the  
 250 melting point differences among the produced polymers, analogous to number average  
 251 molecular weight observations plotted in Figure 2.

252

Table 2. Calculated percentage of M<sub>n</sub> reduction for any diethyl ester chain in relation to the alkyl group in relation to 1,8-octanediol.

		Diester end group		
		Me	Et	Bu
Diester carbon chain length	C4	6959 g mol <sup>-1</sup> * 100%	5380 g mol <sup>-1</sup> * 23%	3796g mol <sup>-1</sup> * 45%
	C6	7141g mol <sup>-1</sup> * 100%	6390 g mol <sup>-1</sup> * 11%	4413 g mol <sup>-1</sup> * 38%
	C10	5677 g mol <sup>-1</sup> * 100%	4908 g mol <sup>-1</sup> * 14%	4478 g mol <sup>-1</sup> * 21%

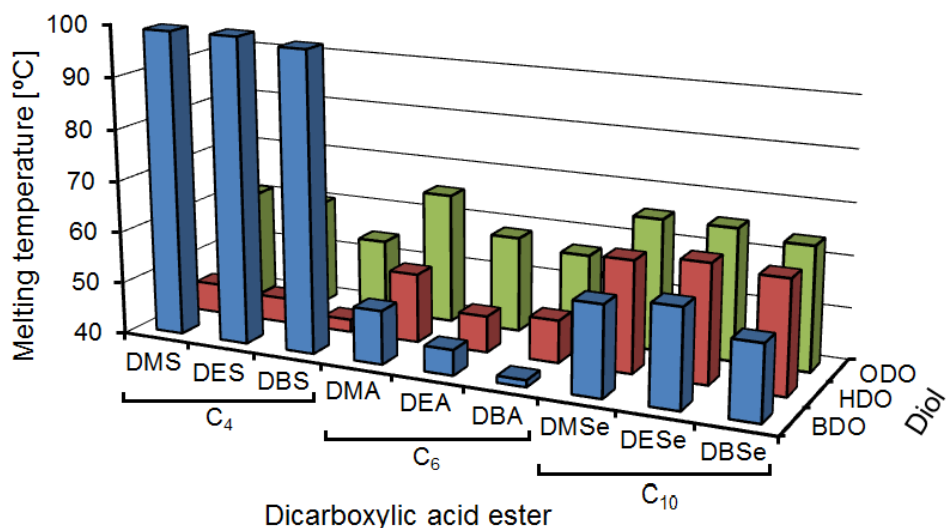
\* Calculated via GPC using a - Da polystyrene calibration curve and toluene as internal standard.

253

254 In Table 2 we reported the % of M<sub>n</sub> reduction for any diethyl ester chain in relation to the  
 255 alkyl group in relation to 1,8-octanediol. As we can see from the collected data, the methyl  
 256 ester (Me) (taken as 100%) is always the best performing one, followed by the diethyl (Et)  
 257 and the dibutyl (Bu) ones. Also to notice that the differences in the M<sub>n</sub>s decrease for the  
 258 Bu end group are lower with the increase of the carbon chain length of the diester for the  
 259 considered reaction.

260 Further to this, the difference in polymer melting temperature between the different diol  
 261 chain lengths becomes less pronounced when increasing the diester chain length (Figure  
 262 3).

263

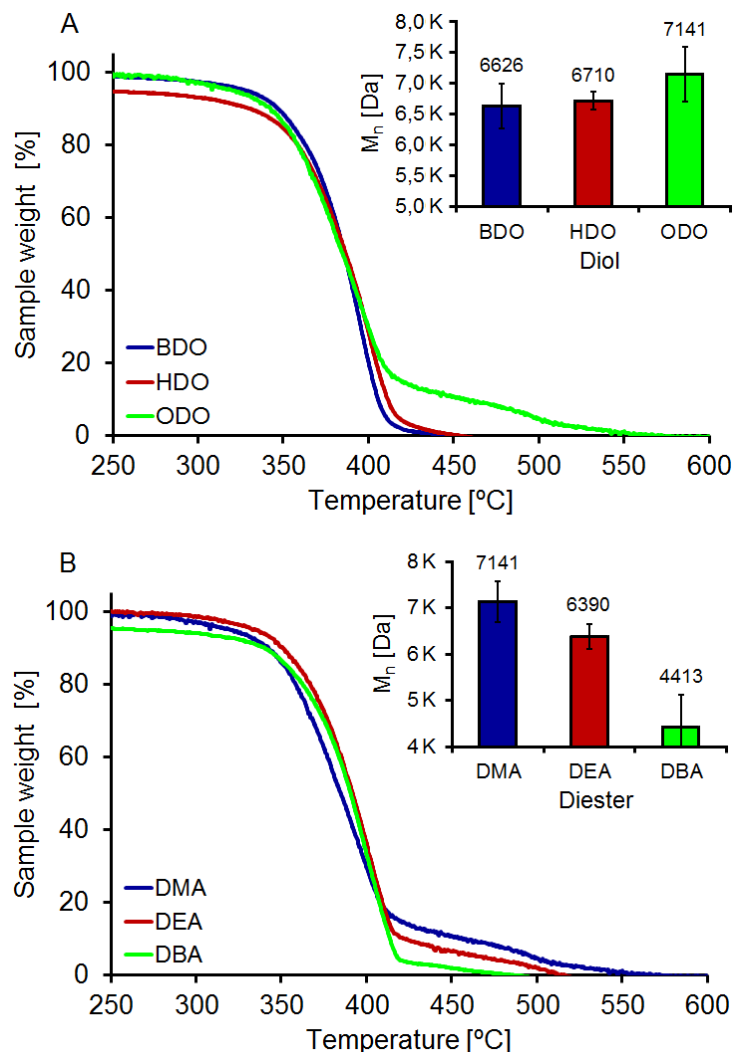


264 Figure 3. DSC determination of the polymer's melting points (see Table S1 for details).  
 265  
 266

267 The inert atmosphere (N<sub>2</sub>) thermogravimetric profile of the polymers presented in Figure 4  
 268 is also consistent with the previously discussed molecular mass data. In fact, with the  
 269 increase of the polymer's M<sub>n</sub> and the increase of the diol's carbon chain length (see Figure  
 270 4a insert) the degradation temperature increases accordingly (Figure 4a).

271 A comparison of the polymerisations conducted using the same diol (1,8-octanediol, ODO,  
 272 C<sub>8</sub>) with three different diesters having methanol, ethanol or butanol alkyl groups on the  
 273 monomers also show a remarkable difference in the obtained M<sub>n</sub> (see discussion above  
 274 and Figure 4b insert), with the dimethyl adipate-derived polyester proving more thermally  
 275 stable than the diethyl equivalent, with this being more stable than the dibutyl. This  
 276 indicates that the selection of the diester remains highly important for these  
 277 transesterification reactions since the volatility of the leaving group proved to be a key  
 278 point in determining the extent to the which the polyester chain grows. From the TGA  
 279 profiles the temperatures at 5% and 50% mass loss (TD5 and TD50) were subsequently  
 280 determined and are reported in Table S2 in ESI.

281



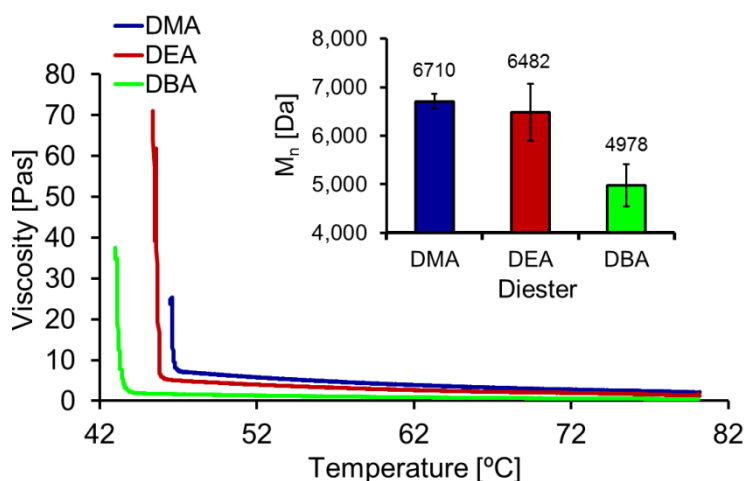
282  
 283 Figure 4. TGA analysis of A) polymers obtained from the polycondensation of dimethyl adipate and the three  
 284 different aliphatic diols 1,4-butanediol (C4, BDO), 1,6-hexanediol (C6, HDO) and 1,8-octanediol (C8, ODO)  
 285 and B) polymers obtained from the polycondensation of ODO with three different diesters dimethyl adipate  
 286 (DMA), diethyl adipate (DEA) and dibutyl adipate (DBA).  
 287

288 Rheology was used to further characterise the polymers and identify differences in their  
 289 viscosity. Figure 5 shows the viscosity change of the polymer melts based on a decrease  
 290 of temperature for poly(1,6-hexylene adipate) synthesized from dimethyl adipate (blue),  
 291 diethyl adipate (red) and dibutyl adipate (green). In all cases, viscosity steadily rose with  
 292 decreasing temperature until the onset of freezing was reached, at which point viscosity  
 293 increased rapidly. This further exemplifies how the differing molecular weights (see Fig.5  
 294 insert) lead to different viscosity profiles. The shorter chain polymer behaves remarkably  
 295 different compared with the other two polymers with similar  $M_n$  values. Comparative  
 296 studies of the presented reactions in organic media are needed in order to better elucidate

297 the effect of viscosity on the reaction progression. Moreover, we noted that the viscosity of  
298 any initial mixture appeared to be below the lower detection limit (ca. <0.2 Pa.s) of the  
299 apparatus when used under the same conditions.

300 The produced polyesters can find applications that range from the biomedical field (as  
301 carriers in protein- and peptide-delivery systems) [25] and, if further coupled with  
302 poly(ethylene glycol), for the production of eco-friendly water-soluble polymers and  
303 coatings [26].

304



305

306 Figure 5. Change of the polymer's viscosity relative to the temperature decrease over time for different  
307 poly(hexamethylene adipate) polyesters whose chain length alters due to the chose dialkyl adipate monomer  
308 (dimethyl adipate – DMA, diethyl adipate – DEA and dibutyl adipate – DBA).  
309

## 310 Conclusions

311 From the collected data we can conclude that CaLB is an effective catalyst for the  
312 synthesis of a range of aliphatic polyesters using a solventless reaction system. Polyesters  
313 based on diesters with an internal carbon chain length between 4 (succinate) and 10  
314 (sebacate) and diols with a carbon chain length between 4 (1,4-butanediol) and 8 (1,8-  
315 octanediol) were successfully synthesized via transesterification. A strong effect of the  
316 selected alkyl group of the diester (dimethyl, diethyl and dibutyl) was observed for all  
317 polyesters. Lower molecular weights and monomer conversions were obtained using  
318 dibutyl esters since it proved more difficult to remove the butanol by-product during the



319 reaction due to its higher boiling point (relative to methanol and ethanol). DSC, TGA and  
320 rheology measurements confirm the trend showing a large difference in degradation  
321 temperatures and viscosity of the melts due to the polymers' molecular weight. This work  
322 has sets the basis for efficient biocatalyzed syntheses of aliphatic polyesters having  $M_n$  of  
323  $\sim 6$  and  $M_w$  of  $\sim 13$  KDa and with monomers conversions  $>94\%$ . This also represents the  
324 first systematic study of different dialkyl aliphatic diesters with various diols under identical  
325 reaction conditions.

326

#### 327 Conflicts of interest

328 The authors declare no conflicts of interest.

329

#### 330 Acknowledgements

331 A. P. thanks the FWF Erwin Schrödinger fellowship (grant agreement J 4014-N34) for  
332 financial support. M. H. S. thanks Academy of Finland for funding (grant #296547). T. J. F.,  
333 J. H. C. and J. W. C. would like to thank the UK Engineering and Physical Sciences  
334 Research Council (EPSRC, grant EP/L017393/1) and the Biotechnology and Biological  
335 Sciences Research Council (BBSRC, grant BB/N023595/1) for funding their involvement in  
336 this research.

337

#### 338 Notes and references

339 Electronic Supplementary Information (ESI) available: Details of:  $^1\text{H-NMR}$  spectroscopy  
340 conversions (Fig. S1),  $M_n$  (Fig.S3) and  $M_w$  (Fig. S2 and S4) GPC data, DSC-determined  
341 polymer's melting temperatures (Table S1) and TD5 and 50 (Table S2) are reported in  
342 ESI. All data gathered via funding from grants EP/L017393/1 and BB/N023595/1 is  
343 contained within the manuscript or the ESI.

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