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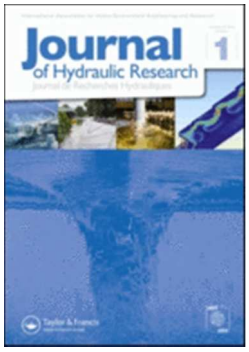

The frictional resistance induced by bacterial based biofouling within drainage pipelines

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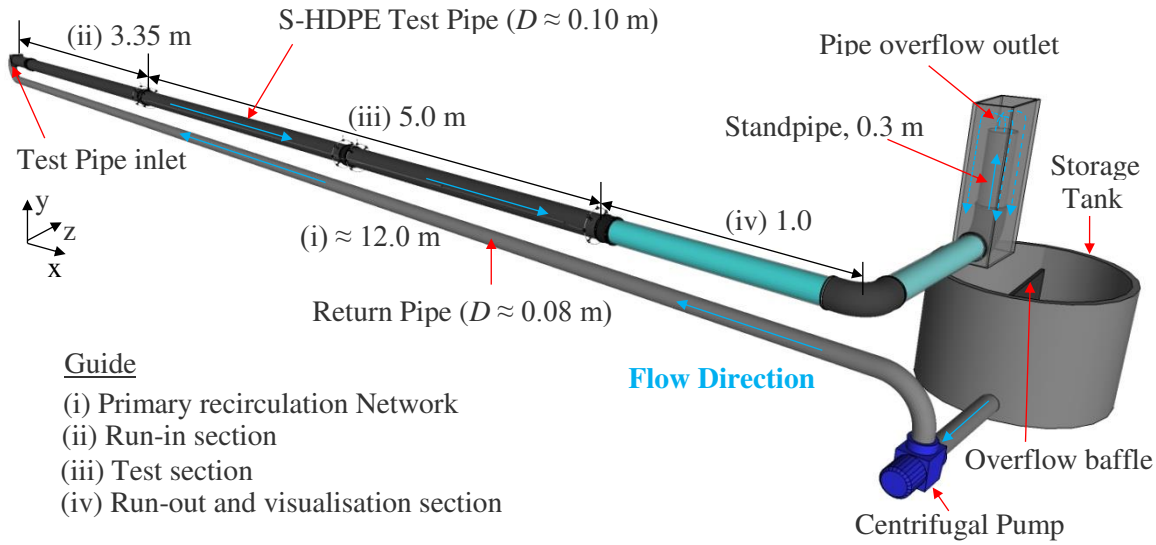
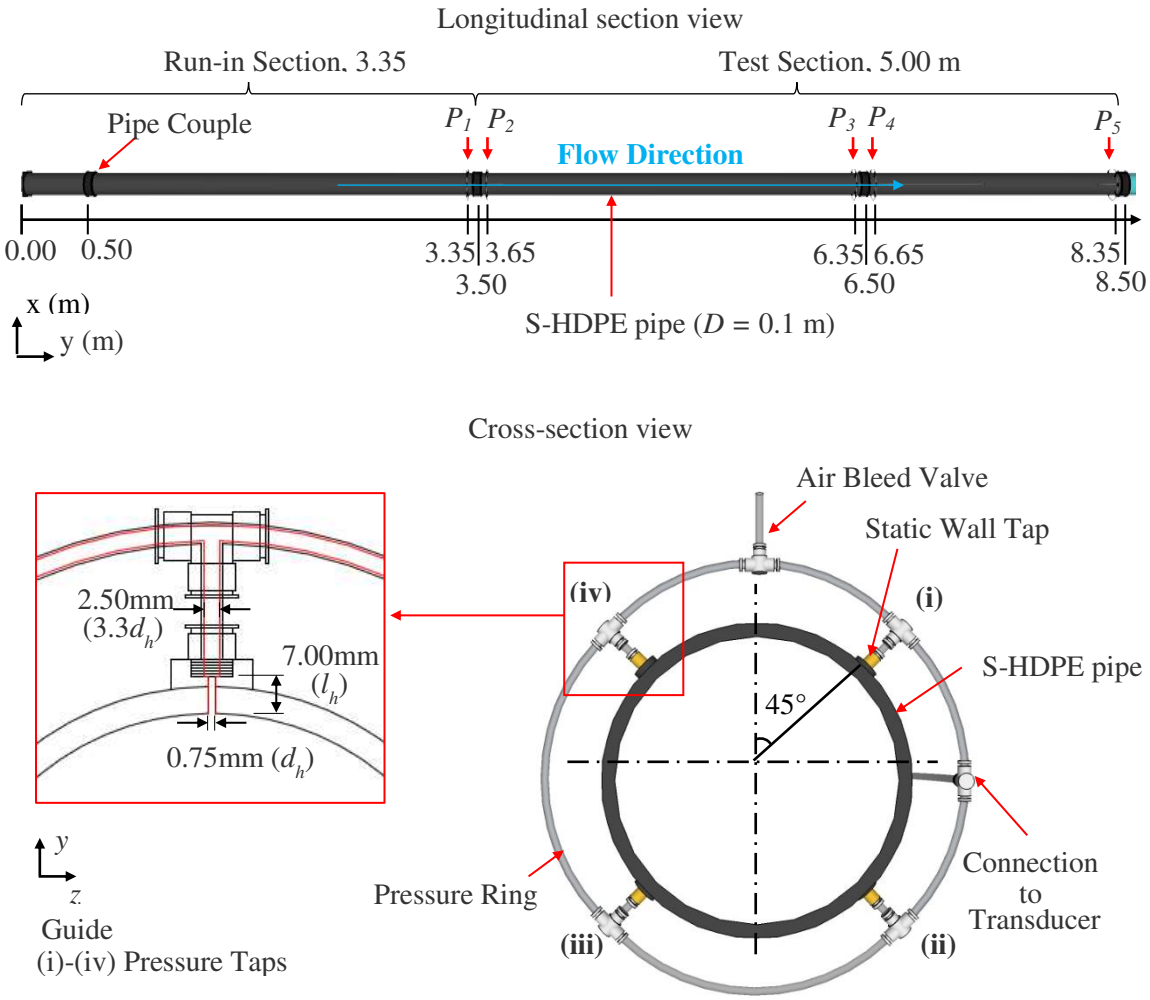
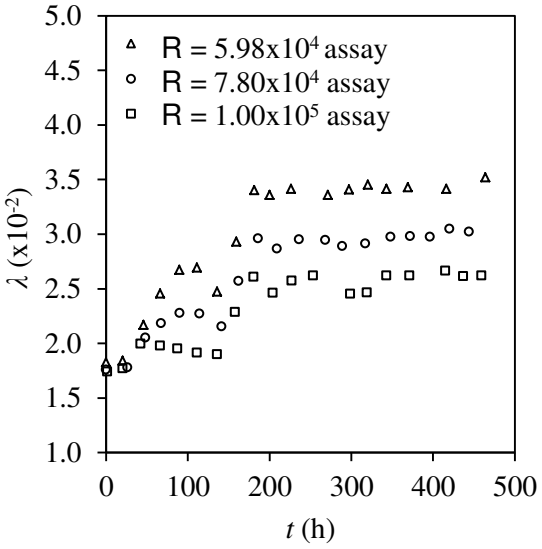
Assay		R ($x10^4$)	$\bar{U}$ (ms^{-1})	Temperature ($^{\circ}C$)	ν ($x10^7$) (m^2s^{-1})	ρ (kgm^{-2})	COD (mgl^{-1})	TOC (mgl^{-1})	DOC (mgl^{-1})	TN (mgl^{-1})	TP (mgl^{-1})	Ammonium (mgl^{-1})	Nitrate (mgl^{-1})	Iron (mgl^{-1})	Manganese (mgl^{-1})
	Av.	5.98	0.58	21.3	9.70	998.0	536.4	238.2	211.5	49.5	12.1	0.41	0.50	0.11	0.13
$R = 5.98x10^4$	σ	0.12	0.01	0.6	0.00	0.2	40.5	16.1	14.3	0.6	1.20	0.23	0.28	0.05	0.06
	n	60	60	60	60	60	20	10	10	2	2	6	6	6	6
	Av.	7.81	0.76	21.2	9.72	998.0	545.6	251.2	-	50.3	10.8	0.25	0.33	0.10	0.30
$R = 7.82x10^4$	σ	0.17	0.01	0.7	0.00	0.2	21.2	9.5	-	0.4	0.8	0.23	0.28	0.07	0.20
	n	60	60	60	60	60	20	20	-	2	4	4	4	4	4
	Av.	1.01	0.96	21.8	9.59	997.9	548.1	241.6	190.6	51.2	11.0	0.75	1.09	0.15	0.39
$R = 1.00x10^5$	σ	0.29	0.02	0.6	0.00	0.2	23.4	12.2	9.6	0.9	0.8	0.02	0.11	0.09	0.10
	n	60	60	60	60	60	20	9	9	11	3	4	4	5	5

Parameter	Symbol	Uncertainty (%)	
		Av.	Max.
Fluid density	ρ	0.02	0.03
Fluid kinematic viscosity	ν	2.39	4.14
Reynolds Number (Flowmeter)	R	10.01	15.99
Reynolds Number (Pitot Probe)		6.43	11.61
Local velocity, near wall region ($y^+ < 50$)	u	3.85	4.40
Local velocity, Log-Law region ($50 < y^+ < 300$)		1.21	1.79
Local velocity, wake region ($300 < y^+ < R^+$)		0.70	1.08
Friction factor	λ	5.15	7.30
Shear velocity	u_*	6.49	14.27
Wall shear stress	τ_w	13.44	28.53
Skin friction coefficient	c_f	4.53	15.36

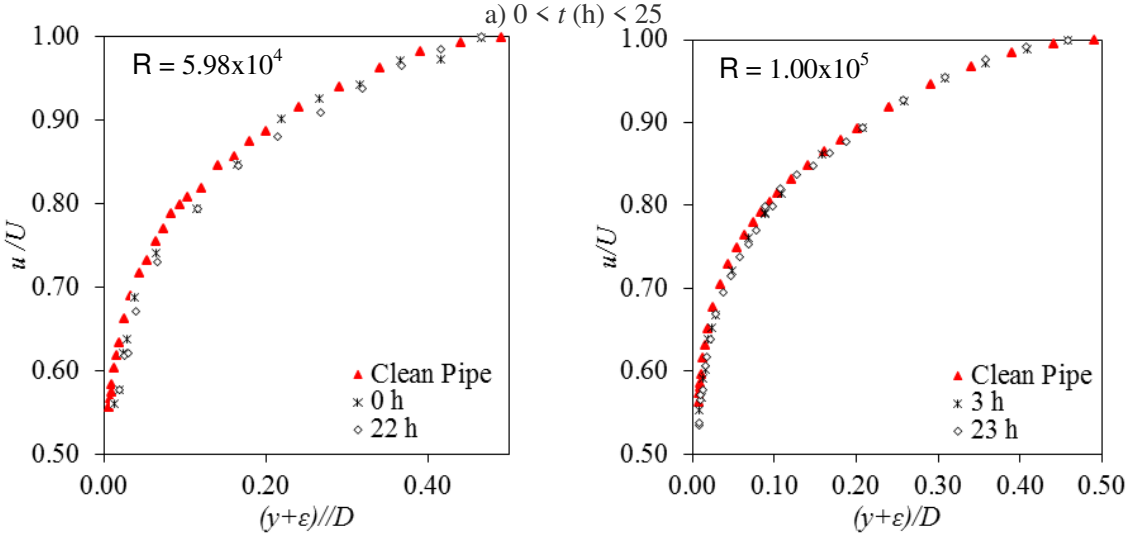
Assay		λ	$\boldsymbol{u}_*$ (ms^{-1})	τ_w (Nm^{-2})	c_f ($x10^{-3}$)	k_s (mm)	k_s^+
$R = 5.98x10^4$	Av.	0.034	0.038	1.42	8.54	0.637	25.05
	σ	0.000	0.001	0.07	0.12	0.023	1.76
$R = 7.82x10^4$	Av.	0.030	0.045	2.15	7.57	0.445	20.94
	σ	0.001	0.001	0.05	0.18	0.031	1.34
$R = 1.00x10^5$	Av.	0.026	0.054	2.95	6.44	0.223	12.79
	σ	0.001	0.001	0.07	0.19	0.027	1.41


(ii) 3.35 m
S-HDPE Test Pipe ($D \approx 0.10$ m)
Pipe overflow outlet
(iii) 5.0 m
Standpipe, 0.3 m
Storage Tank
Test Pipe inlet
y
z
x
(i) ≈ 12.0 m
(iv) 1.0
Return Pipe ($D \approx 0.08$ m)
Guide
(i) Primary recirculation Network
(ii) Run-in section
(iii) Test section
(iv) Run-out and visualisation section
Flow Direction
Overflow baffle
Centrifugal Pump

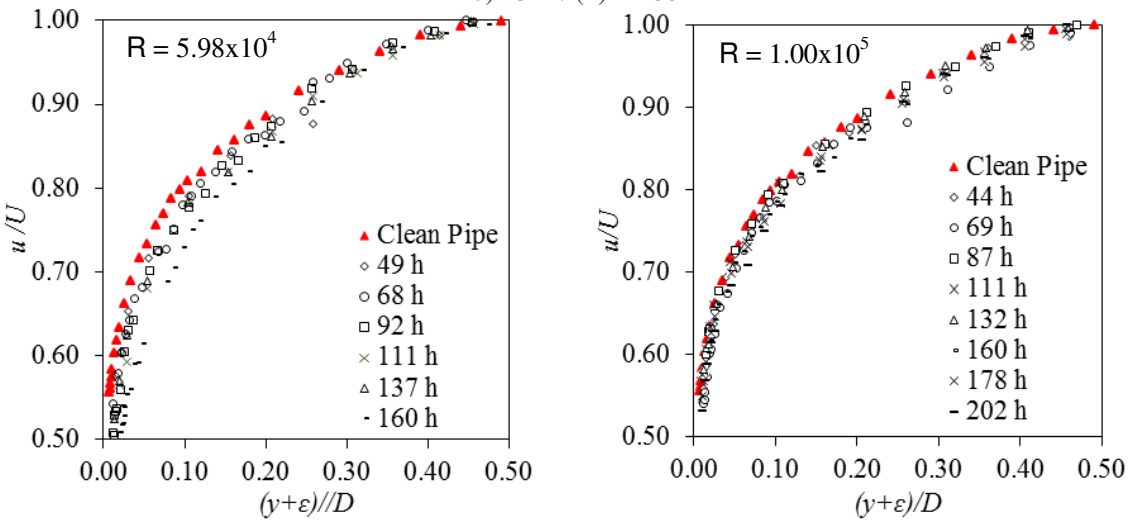

Longitudinal section view
Run-in Section, 3.35
Test Section, 5.00 m
Pipe Couple
P_1 P_2
P_3 P_4
P_5
Flow Direction
0.00 0.50
3.35 3.65
3.50
6.35 6.65
6.50
8.35
8.50
x (m)
y (m)
S-HDPE pipe (D = 0.1 m)
Cross-section view
Air Bleed Valve
Static Wall Tap
(iv)
(i)
S-HDPE pipe
45°
2.50mm
($3.3d_h$)
7.00mm
(l_h)
0.75mm (d_h)
y
z
Guide
(i)-(iv) Pressure Taps
Pressure Ring
Connection
to
Transducer
(iii)
(ii)


R = 5.98x10^4 assay
R = 7.80x10^4 assay
R = 1.00x10^5 assay
λ (x10^-2)
t (h)
5.0
4.5
4.0
3.5
3.0
2.5
2.0
1.5
1.0
0
100
200
300
400
500

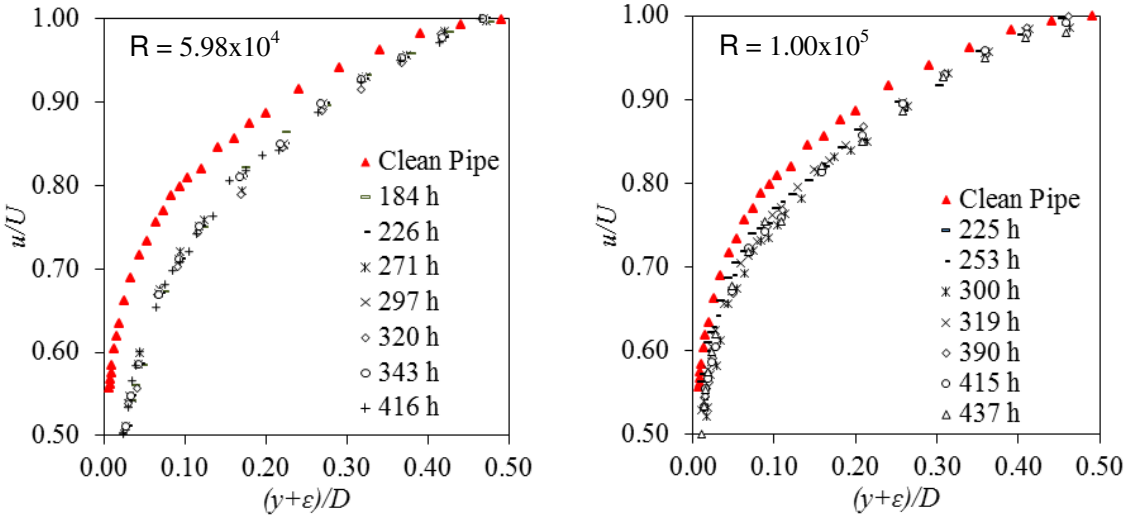
a) 0 < *t* (h) < 25

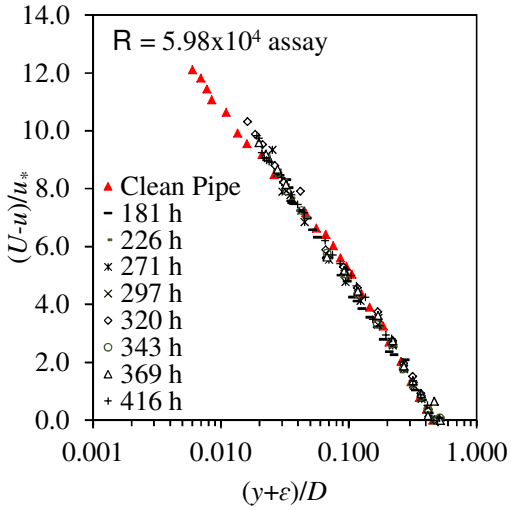


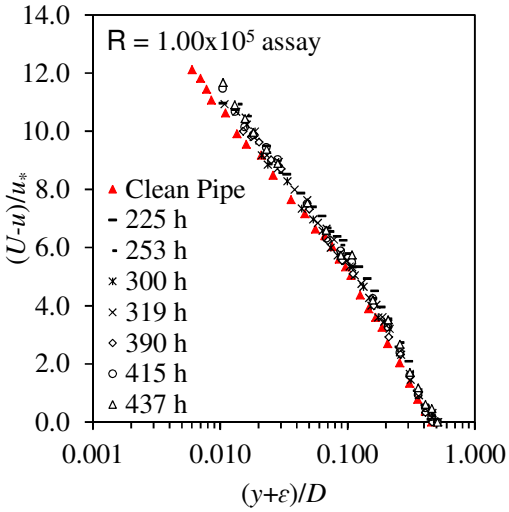
b) 25 < *t* (h) < 180

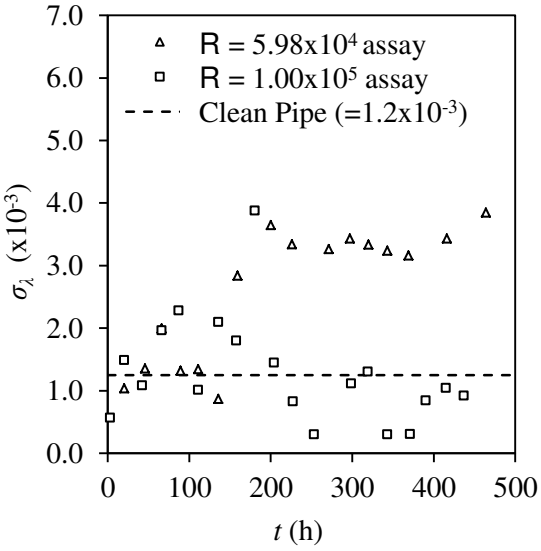


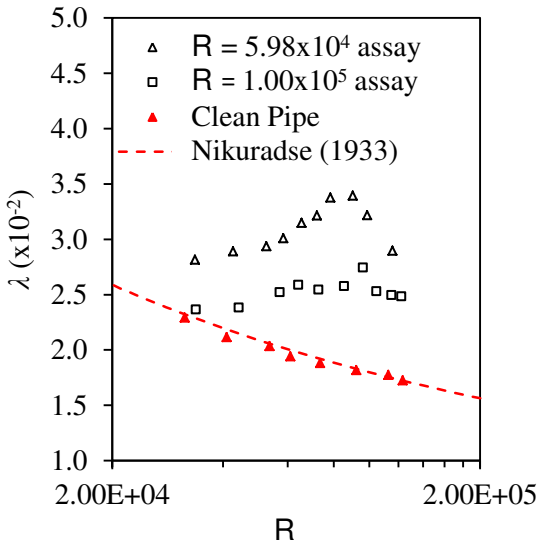
c) *t* (h) > 180

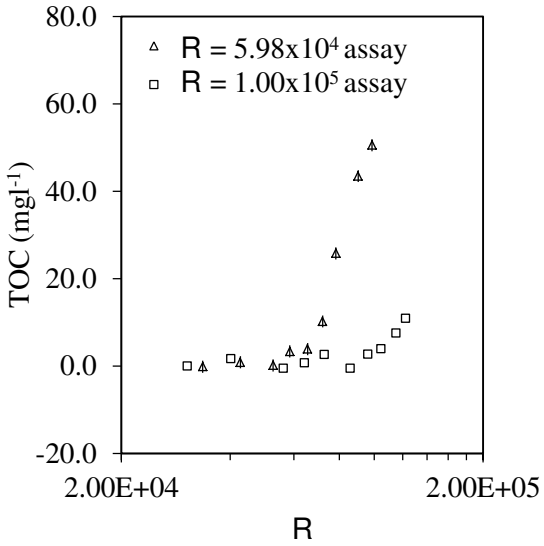


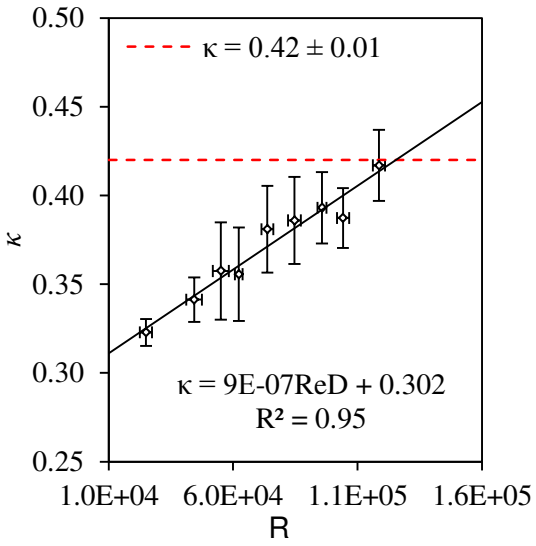

R = 5.98x10^4 assay
Clean Pipe
181 h
226 h
271 h
297 h
320 h
343 h
369 h
416 h
(U-u)/u*
(y+ε)/D
14.0
12.0
10.0
8.0
6.0
4.0
2.0
0.0
0.001
0.010
0.100
1.000

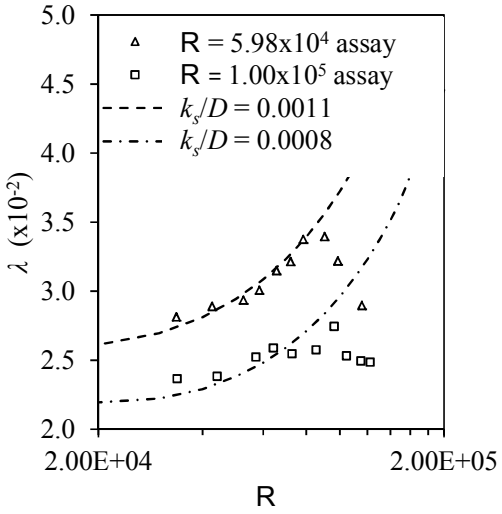

R = 1.00x10^5 assay
Clean Pipe
225 h
253 h
300 h
319 h
390 h
415 h
437 h
(U-u)/u*
(y+ε)/D
14.0
12.0
10.0
8.0
6.0
4.0
2.0
0.0
0.001
0.010
0.100
1.000

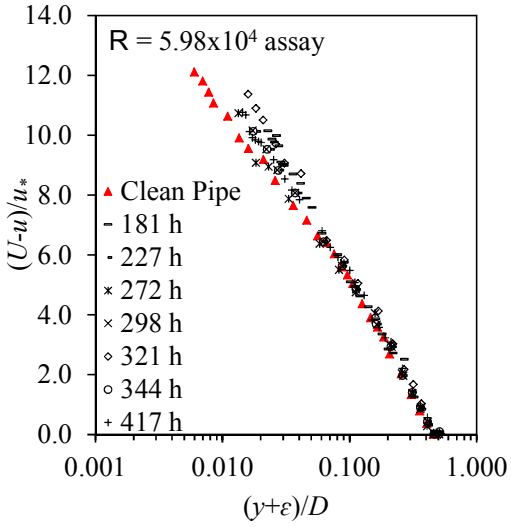

R = 5.98x10^4 assay
R = 1.00x10^5 assay
Clean Pipe (=1.2x10^-3)
σλ (x10^-3)
t (h)
7.0
6.0
5.0
4.0
3.0
2.0
1.0
0.0
0
100
200
300
400
500

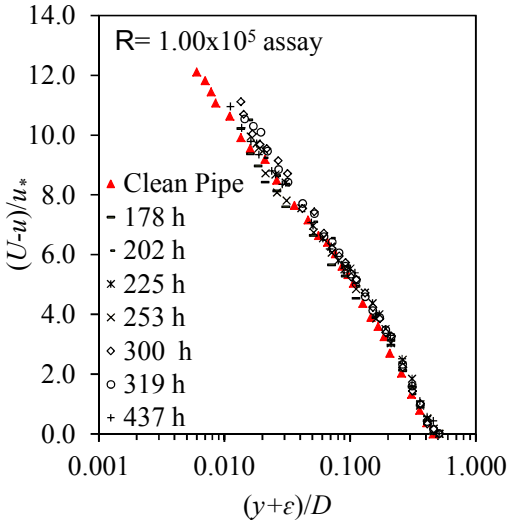

5.0
4.5
4.0
3.5
3.0
2.5
2.0
1.5
1.0
λ (x10-2)
R = 5.98x10⁴ assay
R = 1.00x10⁵ assay
Clean Pipe
Nikuradse (1933)
2.00E+04
2.00E+05
R


80.0
60.0
40.0
20.0
0.0
-20.0
TOC (mgl-1)
R = 5.98x10^4 assay
R = 1.00x10^5 assay
2.00E+04
2.00E+05
R


0.50
0.45
0.40
0.35
0.30
0.25
κ
κ = 0.42 ± 0.01
κ = 9E-07ReD + 0.302
R² = 0.95
1.0E+04
6.0E+04
1.1E+05
1.6E+05
R


5.0
4.5
4.0
3.5
3.0
2.5
2.0
λ (x10-2)
R = 5.98x10^4 assay
R = 1.00x10^5 assay
ks/D = 0.0011
ks/D = 0.0008
2.00E+04
2.00E+05
R


R = 5.98x10^4 assay
Clean Pipe
181 h
227 h
272 h
298 h
321 h
344 h
417 h
(U-u)/u*
(y+ε)/D
14.0
12.0
10.0
8.0
6.0
4.0
2.0
0.0
0.001
0.010
0.100
1.000


R= 1.00x10^5 assay
Clean Pipe
178 h
202 h
225 h
253 h
300 h
319 h
437 h
(U-u)/u*
(y+ε)/D
14.0
12.0
10.0
8.0
6.0
4.0
2.0
0.0
0.001
0.010
0.100
1.000

The frictional resistance induced by bacterial based biofouling in drainage pipelines

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Running Head: The frictional resistance induced by bacterial biofouling

The frictional resistance induced by bacterial based biofouling in drainage pipelines

ABSTRACT

This paper aims at improving the current understanding of bacterial-based biofouling in drainage pipelines. Using a purpose built pipeline facility consisting of a high density polyethylene pipe, biofilms were incubated with synthetic wastewater for 20 days at three steady-state flow regimes. The results obtained have shown that the presence of a biofilm can cause a significant increase in frictional resistance. The magnitude of a biofilm's frictional resistance is a function of the shear conditions under which the biofilm is incubated. In particular, the lower the conditioning shear, the higher the frictional resistance imparted by the biofilm. This is attributed to the thickness and roughness distribution induced by such conditions, and it serves to highlight the problem of characterising a biofilm's effective roughness using a single roughness scale. The study has also supported the earlier funding that the von Kármán constant is non-universal, and is dependent on Reynolds number for biofouled pipes.

Keywords: Biofilm; bacterial based biofouling; drainage pipelines; equivalent roughness; flows in pipes; von Kármán constant

1 Introduction

It is widely acknowledged that population growth, urbanisation and climate change will put significant pressure on pipeline infrastructure over the next century. In particular, the magnitude and intensity of precipitation in extreme events is predicted to increase as a direct result of climate change. The increased runoff and storm water discharge expected has the potential to increase the frequency and magnitude of surcharge and flooding, particularly in highly populated urban areas. Global population growth is likely to further exacerbate the impacts of climate change on sewer systems, especially in urbanised areas where it is predicted that the majority of the growth will be absorbed. The effective management of Drainage Networks (DNs) is therefore of paramount importance to the water industry; and it represents one of the industry's greatest challenges from both an operational and public health standpoint. This challenge is exacerbated by the environmental complexities of DNs, which are characterised by highly diverse and variable flow rates, temperatures and their contents. Fouling mechanisms such as bacterial based biofouling, contribute to, and are governed by these inherent complexities. Bacterial based biofouling refers to the natural, albeit sometimes undesirable process through which a complex microbiological slime layer – known as a biofilm – forms upon a surface. Biofilms in pipelines are generally classified on the macro-scale as either low-form gelatinous or filamentous. Their presence can cause a significant

increase in boundary shear stresses and surface roughness (Barton, 2006; Barton Sargison, Buia, Walker, 2008).

The magnitude of the change in surface roughness caused by biofouling is a function of the physical nature of a biofilm (Barton, 2006). Biofilms are viscoelastic in nature and through a vibrating and oscillating action, they have the ability to remove significant amount of energy from a flow field (Andrewartha, 2010; Walker, Sargison, & Henderson, 2013). As a result, a biofilm's effective roughness can be significantly higher than that predicted based upon traditional wall similarity hypothesis, i.e. using the classical Nikuradse-type equivalent sandgrain roughness, k_s as defined in the Colebrook-White (C-W) equation:

$$\frac{1}{\sqrt{\lambda}} = -2.00 \log\left(\frac{k_s}{3.7D} + \frac{2.51}{\mathrm{R}\sqrt{\lambda}}\right) \quad (1)$$

where D is the internal pipe diameter, R is Reynolds number (=$\overline{U}D/\nu$; where $\overline{U}$ is the area-averaged axial flow velocity, and ν is kinematic viscosity (=μ/ρ; where μ is dynamic viscosity and ρ is the specific density)), and λ is the Darcy-Weisbach friction factor:

$$\lambda = \frac{2gDS_f}{\overline{U}^2} \quad (2)$$

where g is the acceleration due to gravity (i.e. 9.81 ms^{-2}), and S_f is the friction slope or pressure gradient (=dH_f/dx; where H_f is hydraulic headloss (=$\Delta P/\rho g$, where ΔP is pressure drop) and x is the characteristic length scale (in the streamwise direction). Solving Eq. (1) for k_s yields:

$$k_s = 3.7D\left(10^{\frac{-1}{2\sqrt{\lambda}}} - \frac{2.51}{\mathrm{R}\sqrt{\lambda}}\right) \quad (3)$$

The mechanisms by which a biofilm interacts with a fluid along with its physical morphology are governed by the conditions under which it is grown (Stoodley, Dodds, Boyle, & Lappin-Scott, 1998a; Stoodley, Lewandowski, Boyle, & Lappin-Scott, 1998b). There is compelling evidence to suggest that flow hydrodynamics and nutrient availability are the two most influential factors governing biofilm development in pipelines (Stoodley et al., 1998a, Lauchlan, Forty, & May, 2005). However, in DNs where it is likely that sufficient nutrients would be available; flow hydrodynamics will be the primary controlling factor due to its potential to remove existing biofilms, and/or counteract further growth. Nonetheless, there is an inherent link between flow hydrodynamics and nutrient availability on biofilm development; and this is due to their combined influence on mass transfer and diffusion. The mass transfer and diffusion potential of a system is predominantly controlled by the level of turbulence in the flow (i.e. R).

The prevailing conditions in a typical DN imply that the presence of a biofilm is realistically unavoidable. Consequently, the accurate assessment of a biofouled surface is

imperative for efficient pipeline design and effective control strategies. However, this is not possible through the application of conventional design approaches which utilise traditional frictional relationships and roughness scales. In particular, in their current forms Eq. (1) and k_s have been deemed inadequate for biofouled surfaces (Barton, 2006; Lambert, Edwards, Howie, Gilio, & Quinn, 2009; Perkins, Henderson, Walker, Sargison, & Li, 2014). It has been widely suggested that the complex surface dynamics of a biofilm cannot be adequately defined by a single one-dimensional parameter, such as k_s (Andrewartha, 2010; Barton, 2006). However, as such a parameter (or series of parameters) has yet to be successfully formulated, the Nikuradse equivalent sandgrain height was used within this study to define k_s.

Lambert et al. (2009) used experimental observations on freshwater biofilms to obtain a modified C-W equation (Eq. (4)), which is aimed at addressing the inadequacy of Eq. (1), i.e.:

$$\frac{1}{\sqrt{\lambda}} = -\frac{1}{\sqrt{8.08\kappa}} \ln\left(\frac{k_s}{0.85D} + \frac{2.51}{\mathrm{R}\sqrt{\lambda}}\right) \tag{4}$$

Lambert et al. (2009) found that for biofouled pipes, the von Kármán constant κ, which is a fundamental part of the Eq. (1), was non-universal, dependant on R, and lower than the conventional value (i.e. $\kappa = 0.42$). Solving Eq. (4) for k_s yields:

$$k_s = 0.85D\left(e^{\frac{-1\sqrt{8.08\kappa}}{\sqrt{\lambda}}} - \frac{2.51}{\mathrm{R}\sqrt{\lambda}}\right) \tag{5}$$

Similar observations were reported by Perkins et al. (2014) for biofilms incubated in a hydropower system. However, these studies assessed a very specific set of environmental conditions; and in the case of Lambert et al. (2009), a very limited range of flow regimes (at low R values). Furthermore, the environmental conditions in a hydropower or freshwater system are inherently different to those found in DNs; and this would be reflected in the respective system's biofilm. This ultimately affects the broader application of the reported observations, particularly with respect to DNs. Nonetheless, the existence of a non-universal log-law is not a new concept, as there is debate within the classical theory as to whether κ is truly independent of R (Wei, Schmidt, & McMurtry, 2005). The highly dynamic nature of a biofouled surface will undoubtedly add an additional layer of complexity to the debate. The implication of a non-universal κ on roughness and flow rate determination (using Eq. (1)) could be considerable. This would be reflected in pipeline design through pipe sizing; and this could have financial and environmental implications especially if the pipe is oversized as a result (Cowle, Babatunde, Rauen, & Bockelmann-Evans, 2014). The impact of a non-universal κ would also be detrimental to wall similarity techniques, particularly with respect to their ability to effectively establish the local roughness for biofouled surfaces. This is

because these techniques which are commonly used to determine parameters such as wall shear velocity u_* by fitting experimental data to the law of the wall (Eq. (6)), are reliant on the existence of a universal log-law:

$$\frac{u}{u_*} = \frac{1}{\kappa}\ln(\mathsf{Y}^+) + B$$

or

$$\frac{u}{u_*} = \frac{1}{\kappa}\ln(\mathsf{Y}^+) + 5.6 - \Delta\mathsf{U}^+ \quad (6)$$

where u is the local mean velocity, Y^+ is the normalised wall distance (=u_*y/ν, where y is the wall distance), B is Nikuradse's roughness function which assumes different values depending on the flow regime (for fully rough flow B = 8.48), and $\Delta\mathsf{U}^+$ is the roughness function which represents the shift in the velocity profile from the smooth wall profile, and increases with increasing surface roughness. As a result, the frictional data derived from wall similarity techniques are highly sensitive to κ (Wei et al., 2005). The current prevailing understanding of biofilm-flow interactions is predominantly based upon observations established from wall similarity techniques, and thus a universal log-law (Andrewartha, 2010; Barton, 2006; Walker et al., 2013). The potential non-universality of κ could bring the conclusions of these studies into question.

Ultimately, the inadequacies in current design practices and hydraulic theory are a reflection of the current state of scientific understanding of biofouling in DNs (Cowle et al., 2014). The increasing awareness and emphasis on sustainability within the water industry, with respect to both the capacity and efficiency of existing networks and future installations, means that it is now more important than ever to change the perception of biofouling and address the inadequacies in current pipe design approaches.

The aim of this study was to evaluate the impact of biofouling on the surface roughness of a drainage pipe within a controlled laboratory environment. This would provide a platform through which the inadequacies in current pipe design approaches could be addressed. To this effect, the specific objectives of the study were to comprehensively determine the impact of biofouling on surface roughness and mean-velocity; investigate the impact of flow shear on biofilm development; and examine whether κ is non-universal for biofouled pipes.

2 Material and methods

2.1 Experimental facility

The experiments reported herein were conducted in a purpose built pilot scale pipeline facility, located in the Hydraulics Laboratory, at Cardiff University School of Engineering. The facility was designed and developed as an open loop, recirculating system for the specific

purpose of studying biofilm-flow interaction in DNs, over a wide range of flow conditions. It was fabricated mainly from high density polyethylene (HDPE), and it consisted of a storage tank (350 l), working and recirculation parts. The fluid in the pipeline was recirculated by a 2.25 kW single phase centrifugal water pump (*Clarke* CPE30A1). The pump is capable of operating over the range of 0.3 $ms^{-1} < \overline{U} < 1.3$ ms^{-1} (or $3.0x10^4 < R < 1.30x10^5$, based on a fluid temperature of 20ºC). The fluid temperature in the system was maintained by an external cooling unit (*D&D*, DC-750), and it was measured by two universal temperature probes (model: *LabJack* EI-1034). The probes had a typical accuracy of ±0.22 ºC at room temperature, and they were calibrated under non-flow and flow conditions using a mercury thermometer which had an accuracy of ±0.10ºC. Temperature control is essential in both biofilm and boundary layer investigations, for the purpose of environmental and R control. The fluid temperature in the facility was maintained at 21.5 ± 0.9°C and this is representative of the temperature found in typical European DNs during the summer (i.e. 18-22°C) (Cipolla & Maglionico, 2014).

[Insert Fig. 1]

The working part of the facility was 9.5 m in length and it consisted of a test pipe (8.5 m) and a visualisation pipe (1.0 m). The test pipe comprised of four individual solid wall high density polyethylene (S-HDPE) pipe segments. The discrete pipe segments were carefully aligned and connected by flexible pipe coupling in a way that ensures a smooth transition between the segments. Nonetheless, it was inevitable that the joints would cause some disruption to the velocity fields in the system. An S-HDPE pipe was selected due to its extensive use in the water industry, especially within the UK and modern projects. The inner diameter of the test pipe was measured at 8 axial locations and at 6 different positions along the length of the pipeline. The inner diameter was determined to be 102.08 ± 0.44 mm.

[Insert Fig. 2]

As shown in Fig. 2, the test pipe consisted of a run-in section and a test section. The run-in section was 3.35 m (or 34 *D*) long and it corresponded to the region of 0.00 m < *x* < 3.35 m. Using the criteria outlined by Zagarola and Smits (1998), the length of the run-in section was deemed sufficient for fully developed mean flow to be obtained in the test section. The test section was 5.0 m in length and was located between 3.35 m < *x* < 8.35 m.

A hydrodynamic evaluation of the test pipe under non-fouled conditions over the range of $3.15x10^4 < R < 1.23x10^5$ indicated that it had a k_s value of 0.01 mm. A surface is considered hydraulically smooth if the roughness Reynolds number, k_s^+ ($=k_s v/u_*$) is less than

or equal to five (Nikuradse, 1933). The maximum value of k_s^+, which corresponds to the maximum R investigated (i.e. $R = 1.23 \times 10^5$) was found to be 0.51. Consequently, the test pipe was considered to be hydraulically smooth.

2.2 Measurements and instrumentation

Volumetric flow rate

The volumetric flow rate in the facility was recorded using a "time of flight" ultrasonic flowmeter (*Nixon* CU100). The meter had a reading accuracy of ±1.5% and it was located in the recirculation part of the system. The flow rate, Q recorded by the ultrasonic flowmeter was verified against the Q values established from local mean-velocity data using a Pitot probe and conservation of mass principles. The diameter of the Pitot probe, d_p (=1.0 mm) used to measure the mean-velocity data limited the spatial resolution near the wall to approximately 0.5 mm. Consequently, a near wall correction was required, especially for high R values (Zagarola, 1996). The values of Q determined from the flowmeter and Pitot probe were found to have a strong correlation, with a coefficient of determination R^2 of 0.92.

Pressure gradient

As the flow in the test section was fully developed, the frictional resistance of the pipe can be accurately determined from the system's pressure gradient (PG) by applying simple equilibrium considerations. The test section's PG was measured using a series of static wall tappings located at various circumferential and longitudinal positions as shown in Fig. 2. In order to minimise the impact of the wall tappings on the external flow field, the tappings were designed in accordance with the recommendations outlined by McKeon and Smits (2002). The key size characteristics of the wall tappings were $d_h = 0.75$ mm, $d_h/D = 7.35 \times 10^{-3}$, $l_h = 7.0$ mm, $l_h/d_h = 9.3$, $d_c = 2.5$ mm and $d_c/d_h = 3.33$; where d_h is the wall tappings' diameter, l_h is the wall tappings' length and d_c is the diameter of the connection to pressure gauge.

Four wall tappings linked in a pressure ring arrangement were located at five streamwise locations (i.e. P_1, P_2, P_3, P_4, P_5, as shown in Fig. 2) along the test section. The pressure ring arrangement allowed a circumferential average pressure to be determined at each location; this reduced potential errors caused by uneven and unstable flow distributions (Barton, 2006). During a typical PG traverse, the time-averaged static pressure at each of the five streamwise locations was recorded at least 4 times and an average value determined. The wall tapping correction criteria outlined by McKeon and Smits (2002) was applied to all static pressure measurements recorded within the study.

Local velocity measurements

A Pitot probe located at P_5 (i.e. x = 8.35 m) was used to obtain all time-averaged velocity profile traverses within the test pipe. The probe's aperture was square ended and 1.0 mm in diameter; and it was located in the same plane as the wall tappings at P_5. However, the main body of the probe was offset from the plane by 30.0 mm in a downstream direction; and this minimised any potential flow disruptions caused by the probe. A watertight gland allowed the probe to freely traverse 93% of the pipe's vertical plane. A wall origin, y = 0, was chosen at the invert side of the pipe. The distance along the pipe's vertical centreline relative to the wall origin was accurately determined using a digital height gauge (*Rapid* AK9636D), which had an accuracy of ±0.01 mm. A typical velocity traverse consisted of at least 45 logarithmically spaced wall-normal positions. Several corrections were applied to all pressure measurements recorded by the Pitot probe and static wall tapping to account for the effects of viscosity, velocity gradient, the presence of the wall, and turbulence (McKeon, Li, Jiang, Morrison, & Smits, 2003).

The wall similarity technique outlined by Perry and Li (1990) – referred to herein as the PL method – was used to determine the local frictional conditions at P_5. The PL method has been used to evaluate biofouled surfaces (Andrewartha, 2010; Walker et al., 2013), and it is known to consistently produce highly accurate values of local u_* (Walker, 2014). The von Kármán constant applied during this analysis was 0.42. The Nikuradse's roughness function was determined using the procedure outlined by Ligrami and Moffat (1986). To establish u_* using the PL method, the exact location of the wall must be known. However, this was difficult to achieve given the position of the probe within the test pipe. Consequently, a wall origin correction, ε, was applied. An adaptation of the method proposed by Perry and Joubert (1963) was integrated into the PL method in order to solve for ε and u_* simultaneously using an iterative approach.

Pressure transducers and data acquisition

All pressure measurements were obtained using three high accuracy pressure transducers (*Omega* PXM409-070HG10V), designated 1 to 3; all of which had a full scale accuracy (including effects of linearity, hysteresis and repeatability) of ±0.08% (or ±0.57 mmH_2O (at 20ºC)). The pressure transducers were regularly calibrated to within ± 0.5 mm using individual wall mounted water manometers. Transducers 1 and 2 were used to record the pressure measurements required for each of the PG and velocity profile traverses. Transducer 3 always recorded the static pressure at location P_1 during each of the respective traverses; for the purpose of removing any temporal variations observed during testing.

For each measurement interval within each of the PG and velocity profile traverses; the pressure, temperature and flow rate were simultaneously recorded by their respective devices and streamed to a desktop PC at a frequency of 100 Hz using a multifunction 24-bit datalogger (*LabJack* U6-Pro). Appropriate sampling times were derived for each of the variables using a cumulative time-averaged approach. For each discrete measurement, a setting time of 30 s and an acquisition time of 24 s was used to ensure transients had settled, and accurate time averaged pressure measurements could be attained.

2.3 Operating conditions

Biofilms were incubated in the facility with a synthetic wastewater under full bore and steady state conditions within three separate flow regime assays, namely: the $R = 5.98x10^4$ (or $\overline{U} = 0.60$ ms^{-1}) assay; $R = 7.82x10^4$ (or $\overline{U} = 0.75$ ms^{-1}) assay; and $R = 1.00x10^4$ (or $\overline{U} = 1.00$ ms^{-1}) assay. The flow conditions within the respective assays are common in DNs in the UK, particularly in pumping/force mains which typically operate full bore and between the range of 0.6 ms^{-1} < $\overline{U}$ < 1.0 ms^{-1} (Lauchlan et al., 2005). The maximum recorded variation in R was ±3%, this indicates that the flow conditions within the respective assays were reasonably homogenous. The shear stress, τ_w acting on the biofilm was $\tau_w = 1.42$ Nm^{-2} for the $R = 5.98x10^4$ assay, $\tau_w = 2.15$ Nm^{-2} for the $R = 7.82x10^4$ assay, and $\tau_w = 2.95$ Nm^{-2} for the $R = 1.00x10^4$ assay. These values are based upon the initial conditions (i.e. without fouling) and the principle that the primary force acting on the biofilm was the shear force generated by the flow (Stoodley, Cargo, Rupp, Wilson, & Klapper, 2002). The internal hydraulic retention time in the facility during the three flow assays was at least 73 s and therefore the systems were considered to be well-mixed.

The synthetic wastewater was prepared according to the specification outlined by the Organisation for Economic Cooperation and Development (OCED, 1984), which provided nutrient conditions that are representative of those found in typical DNs in Europe. The wastewater had the following composition: 320 mgl^{-1} of Peptone; 220 mgl^{-1} of meat extract (540 mgl^{-1} as Chemical Oxygen Demand (COD)); 30 mgl^{-1} of Urea (CH_4N_2O) (50 mgl^{-1} as Total Nitrogen, (TN)); 12 mgl^{-1} of di-potassium hydrogen phosphate (KH_2PO_4) (10 mgl^{-1} as Total Phosphorus (TP)); 7 mgl^{-1} of sodium chloride, 4 mgl^{-1} of Calcium Chloride Dihydrate ($CaCl_2.2H_2O$); and 2 mgl^{-1} of Magnesium Sulfate Heptahydrate ($MgSO_4.7H_2O$). The pH, Total Organic Carbon (TOC) and Dissolved Organic Carbon (DOC) of the prepared wastewater was 7.95 ± 0.15, 244 mgl^{-1} and 201 mgl^{-1}, respectively. The physico-chemical properties of the wastewater within the three flow assays are presented in Table 1.

The three flow assays ran for 20 d (480 h). Based on the nutrient conditions, this was deemed sufficient for the biofilms to reach a state of equilibrium, at least in terms of their

frictional resistance (Andrewartha, 2010; Lambert et al., 2009). Prior to the experimental work, the entire facility was disinfected using a concentrated chlorine solution, and sodium thiosulfate was used to neutralise any residual chlorine in the facility post disinfection.

[Insert Table 1]

2.4 Experimental uncertainty

The uncertainties associated with the friction parameters measured and calculated within the current study are given in Table 2. The uncertainties were determined from repeatability test and they represent a 95% confidence interval. The repeatability tests were undertaken under non-fouled conditions over the range of $3.15x10^4 < R < 1.23x10^5$ (at increments of $R \approx 1.00x10^4$). Each R increment included a PG and velocity profile traverse and was repeated at least three times.

[Insert Table 2]

The uncertainties listed in Table 2 for the non-fouled pipe represent the worst case conditions for the facility; and this was due to the smoothness of the non-fouled pipe and the R values assessed. Higher Reynolds numbers, i.e. in excess of $R = 1.30x10^5$ which would have improved the experimental uncertainties listed in Table 2 could not be achieved using the facility in its current arrangement. Similarly, a test section with a greater overall length which could also have improved the experimental uncertainties, could not be achieved due to laboratory restrictions.

3 Results and discussion

3.1 General description of fouled pipes

The biofilms incubated with synthetic wastewater within the current study displayed a predominantly low-form gelatinous structure. Filamentous type development was observed but very rarely, with filaments seldom exceeding 10 mm. The fouled pipes showed various amounts of microbial material with very different morphologies depending on the conditioning. Typically, the biofilm incubated at high shear (i.e. in the $R = 1.00x10^5$ assay) had a seemingly more uniform coverage than the biofilm incubated at low shear (i.e. in the $R = 5.98x10^4$ assay), which had a more isolated structure. Molecular analysis of the biofilms showed that they were diverse arrays of microbial cells, embedded within an extracellular polymer matrix of which carbohydrates dominated. Polymerase Chain Reaction-Denaturing

Gradient Gel Electrophoresis (PCR-DGGE) indicated that the biofilms were dominated by *Bacteria* and in particular, members of the phyla *Alphaproteobacteria, Betaproteobacteria, Actinobacteria, Bacteroidetes* and *Firmicutes*. These species are commonly found in DNs and as a result, the biofilms were considered representative of those found in real systems, at least in terms of bacterial dominance (Santo Domingo, Revetta, Iker, Gomez-Alvarez, Garcia, Sullivan, & Weast, 2011).

3.2 Impact on frictional resistance

A complete set of PG and mean-velocity traverses were taken at least 3 times a day during each of the biofilm incubation phases, with the exception of the $R = 7.82x10^4$ assay where only PG data was collected. A total of 60 PG and mean-velocity (if applicable) profiles were taken during the incubation phase of three flow assays. The influence of biofilm development on frictional resistance in the form of λ over time t is depicted in Fig. 3. The values of λ presented in Fig.3 for the three flow assays were determined from the system's PG using Eq. (2), where S_f was derived from a linear fit of the profiles of static pressure and therefore, it represents the space-averaged conditions over the entire test section. The static pressure profiles recorded within this study for all the fouled pipes, at all flow rates and time intervals were always a linear function.

[Insert Fig. 3]

The increase in frictional resistance, as indicated by the increase in λ caused by the biofilm development was significant, particularly with respect to the initial non-fouled conditions. This is consistent with the findings outlined previously within the literature (Barton et al., 2008). The observed increases in frictional resistance would have potentially resulted in a reduction in Q of between 15-22% had the pressure drop been held constant in each of the respective flow assays. It is evident from Fig. 3 that λ begins to depart from the non-fouled value after just 25 h of incubation. The biofilms reached a state of equilibrium, in terms of their frictional development after approximately 180 h (see Fig. 3). A summary of the frictional conditions recorded after the biofilms had reached a state of equilibrium is presented in Table 3, where c_f is the skin friction coefficient. The values of k_s presented in Table 3 were determined using the traditional C-W equation (i.e. Eq. (3)) and therefore, they should be viewed with caution as a result of the equation's documented inadequacies in evaluating biofouled surface (as discussed previously in section 1).

[Insert Table 3]

It is evident from Table 3 and Fig. 3 that the highest values of λ were measured in the $R = 5.98x10^4$ assay where λ plateaued at 0.034. The lowest values of λ were measured in the $R = 1.00x10^5$ assay where λ plateaued at 0.026. The $R = 7.82x10^4$ assay represented the intermediate. Single factor analysis of variances (ANOVAs) conducted on the three flow assay datasets indicated that the differences in λ between the respective assays were statistically significant, within the experimental uncertainty. The significance level of all ANOVAs was set at $\alpha = 0.05$.

Dimensionless mean-velocity profiles are presented in Fig. 4 for the range of $0 \leq (y+\varepsilon) \leq r$ (where r is the pipe radius ($=D/2$)). It can be seen that the biofilms caused a gradual shift in the velocity profiles associated with increasing surface roughness. This is in agreement with observations of Walker et al. (2013) for biofilms incubated in a hydropower channel for between 2-52 weeks, at $\overline{U} \approx 1.0$ ms^{-1}. Once the biofilms had reached a state of equilibrium, the respective profiles appeared to collapse well onto a single curve (see Fig. 4c). Varying degrees of roughness can be observed in Fig. 4; and typically, the biofilm cultivated in the $R = 5.98x10^4$ assay had the greatest influence on roughness, as exhibited by the greatest shift away from the non-fouled data. The mean-velocity data is presented in velocity defect form in Fig. 5. It is evident from Fig. 5 that the non-fouled and fouled data collapsed well onto a single curve in the outer region of the boundary layer. This suggests that the presence of a biofilm did not affect the mean-flow structure in the outer region and therefore it provides support for Townsend's wall similarity hypothesis. This has also been observed within the literature for freshwater and marine biofilms (Walker et al., 2013).

[Insert Fig. 4]

[Insert Fig. 5]

It is evident that the frictional resistance induced by a biofilm is a function of the biofilm's conditioning. In particular, the lower the conditioning R, the greater the frictional resistance imposed by the biofilm. This is to be expected, as the overall thickness of a biofilm is heavily dependent on the shear conditions in which it is incubated; and typically, the higher the conditioning shear the thinner the biofilm (Barton, 2006; Celmer, Oleszkiewicz, Cicek, 2008). As a biofilm's thickness defines to some extent the physical and effective roughness of a biofouled surface, the thinner the biofilm, the lower the frictional resistance expected (Andrewartha, 2010; Barton, 2006). Naturally, the opposite is true of thicker biofilms.

Furthermore, the mass transfer and drag limitation potentials associated with lower R values would typically foster a more isolated and irregularly distributed biofilm (Stoodley et

al., 1998a). Such a roughness distribution would induce a higher overall frictional resistance than that imposed by a uniformly distributed structure (Andrewartha, 2010; Stoodley et al., 2002). This could further explain the relatively high nature of the frictional data recorded in the $R = 5.98x10^4$ assay. Alternatively, the increased mass transfer and diffusion potentials associated with higher R values would have induced a more uniformly distributed biofilm (Celmer et al., 2008; Stoodley et al., 2002). The increased uniformity coupled with the limits imposed on maximum thickness by the inherently high drag could explain the low values of λ recorded in the $R = 1.00x10^5$ assay.

The irregularity of the biofilm's space-averaged roughness distribution was evaluated by examining each part of the test section discreetly (i.e. P_1-P_5, P_1-P_4, P_1-P_3 etc.). Figure 6 illustrates the standard deviation in λ for the $R = 5.98x10^4$ and $R = 1.00x10^5$ assays. The average standard deviation in λ determined under non-fouled conditions of $1.25x10^3$ is also presented in Fig. 6 for reference purposes. It is evident from Fig. 6 that the variation in space-averaged conditions along the test section after the biofilms had reached a state of equilibrium, was far greater in the $R = 5.98x10^4$ assay than in the $R = 1.00x10^5$ assay. This was supported by single factor ANOVAs conducted on the respective flow assays (where $\alpha = 0.05$) which indicated that the differences in the values of λ recorded along the test section in the $R = 5.98x10^4$ assay were statistically significant, whereas the ANOVAs performed on the $R = 1.00x10^5$ assay data showed that the differences in values of λ were statistically insignificant. The observed variations in the space-averaged values of λ supports the assumption that biofilm's overall coverage in the $R = 5.98x10^4$ assay was more irregular and thus less uniform (over the length of the system), than the respective coverage in the $R = 1.00x10^5$ assay. The observed heterogeneity of a biofilm's roughness serves to highlight the problem of characterising a biofilm's effective roughness using a single scale, i.e. k_s.

[Insert Fig. 6]

3.3 Influence of Reynolds number on mature biofilm development

Once the biofilms incubated in the $R = 5.98x10^4$ and $R = 1.00x10^5$ assays had reached a state of equilibrium in terms of their frictional resistance, they were subjected to varying flow regimes (over the range of $3.05x10^4 < R < 1.23x10^5$). A total of 10 R increments were assessed within this phase which will be referred to as the mature testing phase. A complete set of PG and mean-velocity traverses were recorded for each of the fouled pipes at each R increment. A total of 62 PG and mean-velocity profiles were recorded during the mature testing phase. This took place after approximately 480-500 h of incubation, and it lasted for

about 12-15 h. An unforeseen complication which led to the death of the biofilm incubated in the $R = 7.82x10^4$ assay prior to the 500 h mark precluded it from this phase of testing.

The influence of R on λ is illustrated in Fig. 7. The relationships between R and λ depicted in Fig. 7 for the respective fouled pipes are evidently different to that expected based on standard convention (i.e. Eq. (1)). In particular, it is evident from Fig. 7 that λ increases with increasing R. For the $R = 5.98x10^4$ assay, λ increased to a maximum of $3.34x10^{-3}$ at $R = 9.02x10^4$; whereas for the $R = 1.00x10^5$ assay, λ increased to a maximum of $2.74\ x10^{-3}$ at $R = 9.61x10^4$. Consequently, the current study is in agreement with the general consensus that λ for a biofouled surface does not follow the traditional C-W relationship (Barton, 2006).

[Insert Fig. 7]

The degree at which λ increases with R is seemingly a function of the biofilm's overall effective roughness (and thus its roughness distribution). In particular, the greater the roughness, the greater the increase in λ. Lambert et al. (2009) reported a similar phenomenon for biofouling, albeit for smaller diameter pipes (i.e. D = 25-50 mm).

Once the local maximum was reached, λ begins to decrease with increasing R. In the case of the $R = 5.98x10^5$ assay, this decrease was significant; whereas the equivalent decrease in the $R = 1.00x10^5$ assay was far more gradual. Similar trends have been reported within the literature (Barton et al., 2008; Lambert et al., 2009; Perkins et al., 2014). For instance, Perkin et al. (2014) found that the λ of a biofilm incubated in a hydropower pipeline increased gradually with increasing R between $9.32x10^4 < R < 1.57x10^5$, to a maximum of 0.033, before decreasing significantly with increasing R between $1.57x10^4 < R < 2.66x10^5$. The biofilm assessed by Perkin et al. (2014) was conditioned at $\overline{U} = 1.30\ ms^{-1}$. The evident reduction in λ with R after the local maximum was reached could be explained by a reduction in biofilm thickness caused by the biofilm compressing itself under loading (Percival, Knapp, Wales, & Edyyean, 1999), or by it being sheared from the surface (Andrewartha, 2010; Barton, 2006). The usual reduction in λ with R could also explain the evident trend (Perkin et al., 2014).

The concentration of TOC in the bulk water was measured at each R increment to indirectly determine whether the increase in flow shear could actively remove the biofilm from the surface. Bulk water samples were taken directly from the storage tank and stored at -20ºC before being analysed. Due to the relatively short time it took to complete each of the mature testing phases (i.e. < 15 h), any changes in water chemistry during this phase would have likely been caused by biofilm detachment. The concentrations of TOC recorded in the bulk water for the $R = 5.98x10^5$ and $R = 1.00x10^5$ assays is presented in Fig. 8. It is evident from Fig. 8 that the concentration of TOC increased significantly in the $R = 5.98x10^4$ assay as

flow shear increased. In particular, a significant increase in TOC was evident when R exceeded $6.54x10^4$. The equivalent increase was less extreme in the $R = 1.00x10^5$ assay, although an increase was evident when R exceeded $9.60x10^4$. The observed increases in organic content in each assays' bulk water suggests that biofilm detachment was likely to have occurred. However, based on the magnitude of the respective increases, the degree of detachment will have varied between the assays. For instance, the concentration of TOC in the bulk water of the $R = 5.98x10^4$ assay following the increase in flow shear was 62.5 mgl^{-1}, whereas the equivalent concentration in the bulk water of the $R = 1.00x10^5$ assay was 10.9 mgl^{-1}. Therefore, it could be suggested that greater biofilm detachment was likely to have occurred in the $R = 5.98x10^4$ assay than in the $R = 1.00x10^5$ assay. The presumed detachment point for the $R = 1.00x10^5$ assay's biofilm, as suggested by the increase in bulk water organic content, is the same point at which a reduction in λ was first recorded (see Fig. 7).

[Insert Fig. 8]

The gradual reduction in λ combined with the relatively low increase in TOC with R, which was observed in the $R = 1.00x10^5$ assay, could potentially suggest that the respective biofilm was merely thinned and/or compressed by the increase in flow shear. Alternatively, the considerable changes in λ and TOC observed in $R = 5.98x10^4$ assay, would suggest that large scale detachment occurred in the respective assay. However, as λ did not approach the non-fouled curve post shear, it was unlikely that the biofilm was completely removed. The point at which λ began to decrease with R in the $R = 5.98x10^4$ assay did not coincide with the detachment point implied by the changes in bulk water chemistry (i.e. $R > 6.54x10^4$). In fact, λ continued to increase beyond this presumed detachment point; and this suggests that biofilm detachment did not occur. However, it is possible that the initial detachment which gave rise to the increases in bulk water organic content had a negligible effect on the biofilm's frictional capacity. Conversely, it is equally possible that the initial biofilm detachment could have given rise to a more heterogeneous roughness distribution, which could have directly contributed to, or be the reason for the observed λ relationship.

3.4 Determining κ for biofouled surfaces

The von Kármán constant's dependence on R was assessed using the PG and mean-velocity data recorded during the mature testing phase. In particular, a linear regression line of best fit was fitted to the log-law region of U^+ against $\ln((y+\varepsilon)/k_s)$ plot. The inverse of the slope of this regression line was equal to κ (i.e. $\kappa = 1/[d(U^+)/d(\ln((y+\varepsilon)\, u_*/\nu)]$). The location of the log-law region within the boundary layer was determined experimentally using the method outlined

by Saleh (2005), and it was found to be unaffected by the presence of a biofilm. The location of the log-law region was taken as $50 < yu_*/\nu < 0.18\mathrm{r}^+$ ($= r\nu/u_*$) which is also where standard convention states that it should be (George, 2007).

Wall similarity techniques, such as the PL method are typically used to determine local frictional conditions at a particular streamwise location from mean-velocity data. However, such techniques are inherently dependent on a universal log-law in which κ is a known constant and typically equal to 0.42. As κ is the unknown in this instance, wall similarity techniques cannot be applied. Therefore, with no other means of determining the local frictional data, the global data determined from the system's PG was used. In particular, the frictional data determined between P_3 and P_5 was applied in this case. It should be noted that although the global values of u_* were unaffected by κ, the global values of k_s required re-calculation using Eq. (5). This was an iterative process that typically required 3-4 iterations for a suitable convergence to be obtained.

Despite the fact that the applied global data represents the frictional conditions for the section at which the mean-velocity data was recorded, it may not be a true reflection of the local frictional conditions at P_5 (i.e. where the mean-velocity data was recorded). This is because a biofilm's roughness distribution is generally heterogenetic, as highlighted by the biofilm incubated in the $\mathrm{R} = 5.98\text{x}10^4$ assay. Furthermore, although the biofilm incubated in the $\mathrm{R} = 1.00\text{x}10^5$ assay displayed a seemingly uniform roughness distribution, it is still highly unlikely that it was truly homogeneous over the whole system. Any error in the frictional data used to determine κ would naturally result in errors in established values κ (Wei et al., 2005). Consequently, the results presented herein should be viewed accordingly and with caution.

The relationship between κ and R is presented in Fig. 9 which illustrates the combined data measured in the two fouled pipes. As it was not possible to distinguish between the two fouled pipe's datasets, the two datasets were combined. It is evident from Fig. 9 that κ has a dependency on R, and in particular, a trend of increasing κ with increasing R can be observed. The elastic nature of a biofilm may have contributed to these trends. The lowest value of κ was measured for $\mathrm{R} = 2.50\text{x}10^5$ and it was equal to 0.32. The reduction in κ from the conventional value lessened as R increased. This may have been as a result of the assumed biofilm detachment and the smoothening of the pipe's surface under loading. This is supported by the fact that the value of κ approaches the canonical value as R increases.

[Insert Fig. 9]

The relationship of κ with R was found to be a linear function ($R^2 > 0.95$), as given by:

$$\kappa = 9.443 \times 10^{-7}\mathrm{R} + 0.302 \quad (7)$$

The trend observed within the current study for κ is consistent with the findings of Perkins et al. (2014) and Lambert et al. (2009). However, the values of κ found within the current study were generally higher than the equivalent values reported by Perkins et al. (2014), who assessed the impact of biofouling on κ in a pipe with similar diameter to that used within the current study (i.e. D = 101.6mm). Nonetheless, the biofilms observed by Perkins et al. (2014) had a significant filamentous component. Visually, the filaments pictured by Perkins et al. (2014) were considerably more abundant than those observed within the current study. Filamentous type development is known to induce a considerable amount of drag on a system, and it can alter the mean flow structure in the outer region of the boundary layer in some extreme cases (Andrewartha, 2010; Barton et al., 2006). However, as a result of the inherently dark conditions in a DN, it is unlikely that the filaments observed by Perkins et al. (2014) would have been as long as those reported in the extreme cases, which typically relate to biofilms incubated in open channels. Nevertheless, the interactions between the filaments and the fluid may have contributed to the lower values of κ observed by Perkins et al. (2014). Consequently, the degree and type of biofouling may have had a greater influence on κ than was first thought, based on the observations reported within this study.

The observed non-universality of κ means that as expected, the values of k_s derived using Eq. (3), and presented in Table 3 are unrepresentative of the actual conditions. The equilibrium state values of k_s as derived from Eq. (5) (where κ is defined by Eq. 7) for the $\mathrm{R} = 5.98\text{x}10^4$ and $\mathrm{R} = 1.00\text{x}10^5$ assays were 0.11mm and 0.08mm, respectively. Therefore, the traditionally derived k_s values (see Table 3) are significantly higher than those derived using the modified C-W equation. Nevertheless, although the magnitude of the k_s values may have changed, the influence of conditioning shear on biofilm induced k_s remained the same. Figure 10 presents the experimentally determined mature phase values of λ recorded in the $\mathrm{R} = 5.98\text{x}10^4$ and $\mathrm{R} = 1.00\text{x}10^5$ assays, along with theoretically determined values derived from Eq. (5) and (7). It is evident from Fig. 10 that prior to the local maximums being reached, the modified C-W curves established using Eq. (5) and (7) were in good agreement with the experimentally determined values of λ. In particular, it was found that the maximum discrepancy between the measured and predicted values was ±7.21%. The average discrepancy between the respective values of λ was ±2.82%. These discrepancies are within the experimental uncertainty in λ presented in Table 2.

[Insert Fig. 10]

The suggestion that wall similarity applies to biofouled pipes (i.e. as indicated by Fig. 5) can also be questioned by the observed non-universality of κ. This is because the velocity defect plots presented in Fig. 5 were scaled by values of u_* derived from the PL method. Velocity defect plots, which have been scaled by values of u_* determined directly from the system's PG are presented in Fig. 11 for the $R = 5.98 \times 10^4$ and $R = 1.00 \times 10^5$ assay. The observed collapses of the non-fouled and fouled profiles suggest that wall similarity is valid for biofouled surfaces, irrespective of the non-universality of the log-law constants.

[Insert Fig. 11]

4 Conclusions and recommendations

4.1 Conclusions

Biofouling in drainage networks is realistically unavoidable. Therefore, the frictional properties of a biofilm, which are characterised by their highly dynamic and case-specific nature, should represent the "true" underlying surface roughness of all pipelines in service. However, such an understanding is currently not recognised within conventional design practices, and this is detrimental to efficient and sustainable operation given that:

- a biofilm has an inherent ability to induce an effective roughness which is well in excess of what its physical structure would traditionally suggest; and
- traditional frictional relationships fail to adequately account for the true nature of a biofouled surface in their current manifestation.

The current study has comprehensively evaluated the impact of biofouling on frictional resistance of a high density polyethylene drainage pipe**.** The finding of the study with regards to the influence of flow hydrodynamics on biofilm frictional development over time, have gone beyond that previously documented within the literature.

An initial increase in roughness caused by biofilm development was observed after just 25 h of incubation, and it continued to increase until a statistically steady state was achieved. The time at which the biofilms reached a state of equilibrium was found to be independent of the conditioning shear and equal to 180 h. The magnitude of a biofilm's frictional resistance was evidently a function of the shear conditions under which the biofilm was incubated. Most notably, it was found that the lower the conditioning shear, the higher the frictional resistance imparted by the biofilm. This is attributed to the thickness and roughness distribution induced by such conditions, and it serves to highlight the problem of

characterising a biofilm's effective roughness using a single roughness scale. A biofilm's impact on frictional resistance is further compounded by its influence over the von Kármán constant. In particular, the current study has provided conclusive evidence that the von Kármán constant for biofouled surfaces is non-universal, dependent on Reynolds number, and lower than the conventionally accepted value. As a consequence of the non-universality of the von Kármán constant, the traditional Colebrook-White equation is not applicable to biofouled pipes. The Darcy-Weisbach friction factor for a biofouled surface was shown to increase with increasing Reynolds number, until a critical threshold was reached. Thereafter, the Darcy-Weisbach friction factor decreased with increasing Reynolds number. This decrease was partly attributed to the biofilm becoming detached under loading. Changes in bulk water chemistry, and in particular organic content supported this assumption.

A modified Colebrook-White equation (i.e. Eq. (3)) can be applied to drainage networks, provided the von Kármán constant is defined by Eq. (7). Furthermore, it was found that, although wall similarity is valid and applicable to biofouled surfaces, it is reliant on either the von Kármán constant or shear velocity being known, without which the results are likely to be unrepresentative of the actual conditions.

4.2 Recommendations for further research

The incubation conditions used within the current study were purposely designed to be representative of those found within natural sewer systems, albeit for those operating at full bore. The resultant biofilms incubated and evaluated within this study can therefore be considered equivalent to those found in real systems. However, wastewater systems with the exception of rising mains are rarely operated at full bore, and drainage networks as a whole are generally unsteady in nature. Consequently, although the study has provided much needed data on biofouling in DNs, further research is still required in order for biofouling to be truly incorporated in pipeline design practices. Such research should ideally expand on the fundamental ideas and concepts outlined within this study. In particular, it is recommended that biofilm development over time is evaluated for a greater range of conditions including a broader range of flow regimes, nutrient levels, operating depths and temperatures. Similarly, given the highly variable nature of real systems, it would be beneficial to incorporate and evaluate typical daily and seasonal variations in operational and environmental conditions within future studies. This study has however provided the platform and methodology needed for such future investigations to be achieved

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Notation

B = Nikuradse's roughness function

c_f = local skin friction coefficient

D = pipe diameter (mm)

d_c = diameter of the pressure transducer connection tube (mm)

d_h = wall tapping hole diameter (mm)

d_p = Pitot Probe diameter (mm)

g = gravity acceleration constant (ms^{-2})

h = hours

H_f = hydraulic head (mm)

k_s = Nikuradse-type equivalent sandgrain roughness (mm)

L = streamwise Length (m)

ΔP = pressure drop (Nm^{-2})

Q = volumetric flow rate (m^3s^{-1})

r = pipe radius (mm)

R^2= coefficient of determination

R = Reynolds number

S_f = friction slope

T = temperature (ºC)

t = time (h)

$\overline{U}$ = area-averaged axial velocity (ms^{-1})

u = local mean streamwise velocity (ms^{-1})

U^+ = normalised velocity

u_* = wall shear velocity (ms^{-1})

ΔU^+ = Hama's (1954) roughness function

x = characteristic length scale

y = distance from the wall (mm)

Δ = change in a variable

ε = wall origin error (mm)

κ = von Kármán constant

λ = Darcy-Weisbach friction factor

μ = dynamic viscosity ($Nm^{-2}s$)

ρ = density (kgm^{-2})

τ_w = wall shear stress (Nm^{-2})

v = kinematic viscosity (m^2s^{-1})

$^+$ = normalised by u_* or u_*/v

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Table Captions

Table 1 Physico-chemical properties of the synthetic wastewater used within the $R = 5.98x10^4$, $R = 7.82x10^4$ and $R = 1.00x10^5$ assays.

Table 2 Uncertainty estimates derived from the evaluation of the non-fouled pipe over the range of $3.15x10^4 < R < 1.23x10^5$.

Table 3 Average frictional data determined from the system's PG at $t > 180$ h (i.e. during the equilibrium stage).

Figure Captions

Figure 1 Perspective 3-D view of the pilot scale pipeline (the flow direction is clockwise).

Figure 2 Schematic of the 8.5 m test section of the pilot scale pipeline, highlighting the pressure tapping locations and general arrangement.

Figure 3 Influence of biofilm development over time on λ within the $R = 5.98x10^4$, $R = 7.82x10^4$ and $R = 1.00x10^5$ assays.

Figure 4 Normalised mean-velocity profiles for the $R = 5.98x10^4$ and $R = 1.00x10^5$ assays at (a) $0 < t$ (h) < 25, (b) $25 < t$ (h) < 180 and (c) t (h) > 180.

Figure 5 Velocity defect plots for the $R = 5.98x10^4$ and $R = 1.00x10^5$ assays at $t > 180$ h (i.e. the during equilibrium stage).

Figure 6 Standard deviation in space-averaged λ along the length of the Test Section for the $R = 5.98x10^4$ and $Re_D = 1.00x10^5$ assays.

Figure 7 The influence of R on λ, for the mature biofilms incubated within $R = 5.98x10^4$ and $R = 1.00x10^5$ assays.

Figure 8 Concentration of TOC within the bulk water against R, for $R = 5.98x10^4$ and $R = 1.00x10^5$ assays.

Figure 9 Relationship of κ with R for the biofouled pipes.

Figure 10 Experimentally and theoretically determined values λ against R for the biofilm incubated within the $R = 5.98x10^4$ and $R = 1.00x10^5$ assay. The theoretically determined values were derived from the Eq. (3) and Eq. (7).

Figure 11 Velocity defect plots scaled using the global values of u_* for the R = 5.98×10^4 and R = 1.00×10^5 assays, at t > 180 h (i.e. during the equilibrium stage).