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A sustainable chemistry method to improve the wash-off process of reactive dyes on cotton

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Reactive dyes are extensively used for coloration of cellulosic fibers because of their excellent wash fastness (stability to washing with aqueous detergent solutions), which arises from covalent bond formation between dye and fibre. However, up to 40% of the dyestuff may hydrolyze in the dyeing process; this hydrolyzed dye has affinity for the fibre *via* hydrogen bonding and van der Waals interactions, but is not covalently bonded and as such exhibits poor wash fastness. Accordingly, these reactive dyeings require a multi-step ‘wash-off’ process after dyeing,

involving various aqueous rinses and washings, in order for the dyeing to achieve the characteristic very high wash fastness. Wash-off and subsequent effluent treatment can account for up to 50% of the total cost of reactive dyeing and consumes significant amounts of water and energy; from a sustainable chemistry and engineering perspective, consumption of water and energy are arguably the biggest issues in textile dyeing. Existing and developmental dye transfer inhibiting (DTI) polymers were employed to remove unfixed (hydrolyzed) dyes. It was found that the use of DTI in the wash-off of reactive dyes enables a much more efficient, economical and sustainable process to be developed, which significantly reduces operation time, water consumption and energy consumption. Different DTI polymer types varied in their efficacy of dye removal; poly(vinylpyridine-*N*-oxide) polymers were the most effective with respect to the level of hydrolyzed dye removal closely followed by the poly(vinylpyridine betaine) polymers, which were also highly efficient in hydrolyzed dye removal, with poly(vinylpyrrolidone) polymers being the least effective. These differences were attributed to variations in the magnitude and delocalization of positive electrostatic potential of the functional moieties in the polymers and the extent of and propensity for hydrogen bonding with the hydrolyzed reactive dyes.

Introduction

Cotton and other cellulose substrates comprise over 40% of world textile consumption. Of all the dyes employed for coloration of cellulosic fibers, reactive dyes find greatest use with over 50% of world consumption.¹⁻³ Reactive dyes are desirable because of their excellent wash fastness, which arises from covalent bond formation between dye and fibre through either

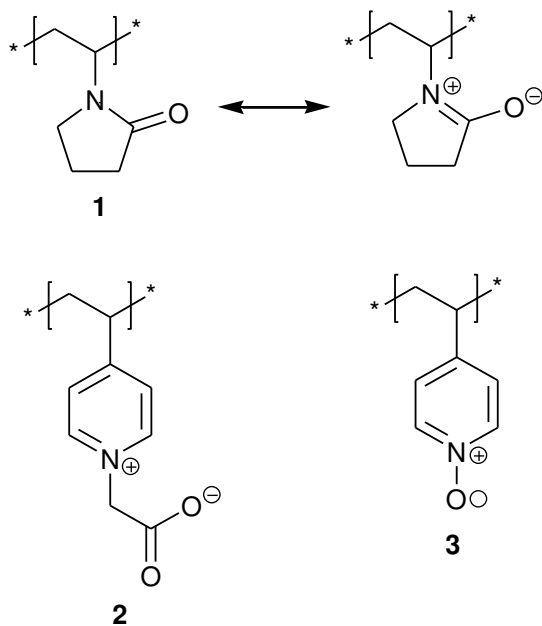
nucleophilic substitution or Michael addition reactions, depending upon the nature of the reactive group in the dye. Reactive dyeing essentially has two stages. In the first stage, the dye adsorbs onto the cellulosic substrate through hydrogen bonding and van der Waals interactions; dyes are applied from aqueous solutions with electrolyte (sodium sulfate or sodium chloride),⁴ which is needed to overcome the long-range repulsion forces operating between anionic dyes (as a result of water-solubilizing sulfonic acid groups) and the negative zeta potential acquired by cotton surface in aqueous media.⁵ Moreover, this repulsive force can be exacerbated through the formation of anionic carboxylic acid (COOH) groups in the cotton substrate, formed *via* oxidation of glucose moieties in cellulose during processing operations such as bleaching or mercerizing,^{6,7} which owing to their relatively low pK_a values will be ionized at the pH values typically encountered during dye application. Without electrolyte addition, adsorption of dye on the fibre will not occur, and with dyes such as reactive dyes, which are very soluble in water, a high amount of electrolyte is required in the dyeing process, often up to 150 g dm^{-3} . Electrolyte also supports dye penetration into the fibre interior (diffusion) which leads to better dye uptake and fixation.^{8,9}

In the second stage, alkali is added to achieve a pH of around 11 in order to generate sufficient cellulosate anions (cell-O^-) within the substrate for covalent bond formation between dye and fibre (fixation); the neutral species (cell-OH) is not sufficiently nucleophilic for reaction between dye and fibre to occur. However, this alkaline environment produces hydroxyl ions in the aqueous dyeing solution with which the reactive dye is able to react, in competition with the cellulosate anions in the fibre, to form hydrolyzed dye. Up to 40% of the dye maybe hydrolyzed in the dyeing process, this hydrolyzed dye has high affinity for the fibre, through hydrogen bonding, van der Waals and ion-dipole forces, but is not covalently bonded.^{5,6,10,11} Accordingly,

these reactive dyeings require a multi-step ‘wash-off’ process after dyeing, involving various aqueous rinses and washings, in order for the dyeing to achieve the characteristic very high wash fastness. This wash-off and subsequent effluent treatment, to remove the resultant color pollution, can account for up to 50% of the total cost of reactive dyeing.⁸

Another extremely important sustainability consideration is the amount of water used in this wash-off process; a process involving over seven separate rinsing stages is not uncommon. High volumes of water and numerous repeated individual wash-off stages are often required to effect a dilution in electrolyte and alkali concentration in the wash-off bath; a wash-off process might include a cold water wash at 25-60 °C; a hot water wash at approximately 60-80 °C; scouring with anionic surfactant at 80-90 °C; followed by subsequent hot and cold water rinses.¹² Electrolyte remains at the end of the dyeing process and, in typical industrial processes, significant amounts are carried over into the wash-off process as the fabric holds at least its own mass of dyeing solution; as a result, the first wash-off stage may contain an electrolyte concentration of up to 15 g dm⁻³. Electrolyte not only increases dye-fibre substantivity, but also can cause dye molecules to aggregate, as a result of which, the hydrolyzed dye molecules become difficult to remove from the fibre. As the electrolyte concentration of the wash-off bath needs to be below 2 g dm⁻³, and ideally below 1 g dm⁻³, in order to achieve effective color removal, the first two stages of the wash-off procedure are mainly employed to reduce electrolyte concentration. Subsequent stages then remove the hydrolyzed dye, and all non-covalently bound dye must be removed to achieve the high level of wash fastness expected. These hot water rinsing and washing stages require high amounts of energy to raise the temperature of large volumes of cold water from ambient temperature to those needed for

efficient washing, and the time taken to empty, fill and heat up washing baths considerably lengthens the total process and reduces productivity.



The use of dye transfer inhibitors (DTI) in domestic laundering detergent compositions is well known. The stain inhibition character of these auxiliaries is effective on both cotton and polyamide fibers in formulations containing non-ionic and/or anionic surfactants. Suitable formulations that reduce the problem of dye staining in domestic laundering have been described¹³ employing cationic and zwitterionic surfactants with a non-ionic detergent. Such DTIs include polymers such as poly(vinylpyrrolidone) (**1**), poly(vinylpyridine betaine)¹⁴ (**2**), and poly(vinylpyridine-*N*-oxide) (**3**). These polymers are permanent dipoles and, as such, can hold soils and vagrant dye, which may be washed from fabric during laundering, in solution and prevent their redeposition onto fabric.¹⁵ Currently, such DTIs are used in domestic washing formulations (powder, liquid, tablet) at concentrations between 0.2 to 1.0 % on mass of the total formulation.¹⁶

From a sustainable chemistry and engineering perspective, consumption of water and energy are arguably the biggest issues in textile dyeing. In this paper, existing and developmental DTIs are employed to remove unfixed (hydrolyzed) dyes following reactive dyeing of cotton, with the objective of gaining a significant cost saving and sustainability benefit as a result of a dramatically reduced wash-off procedure, which will save water, time and energy.

Experimental

Materials

The fabric used was 100% cotton, plain weave, 150 g m⁻². Table 1 shows the DTIs used in this study; all DTIs were supplied by Uniqema, except the two poly(vinylpyridine-*N*-oxide) polymers and the 10,000 Mr poly(vinylpyrrolidone) (PVP) polymer, which were supplied by Reilly Industries, Inc., USA. All DTIs are water soluble and the DTI-dye complex formed in these experiments remains in aqueous solution and does not precipitate. A commercial sample of *Sandozin NIE* was obtained from Clariant, which was included to evaluate the effect of a simple non-ionic surfactant (that may be used in standard wash-off processes) under the novel wash-off method used for the DTIs.

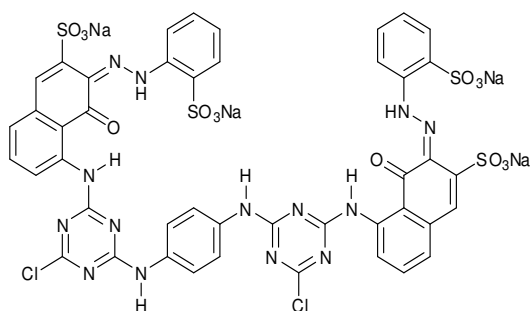
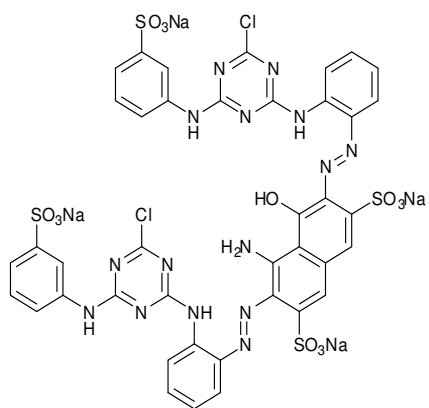
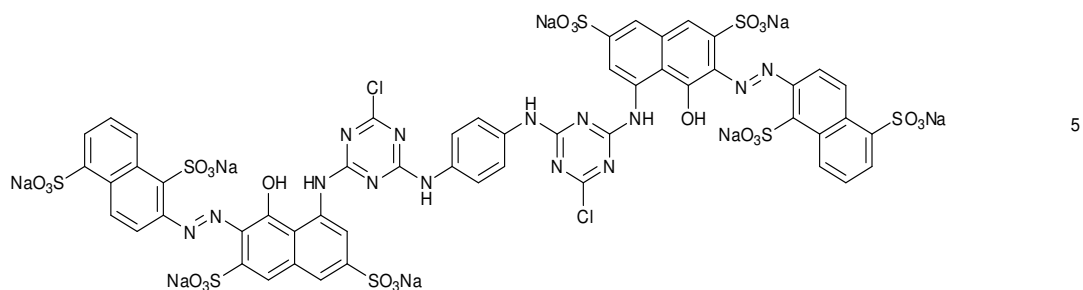
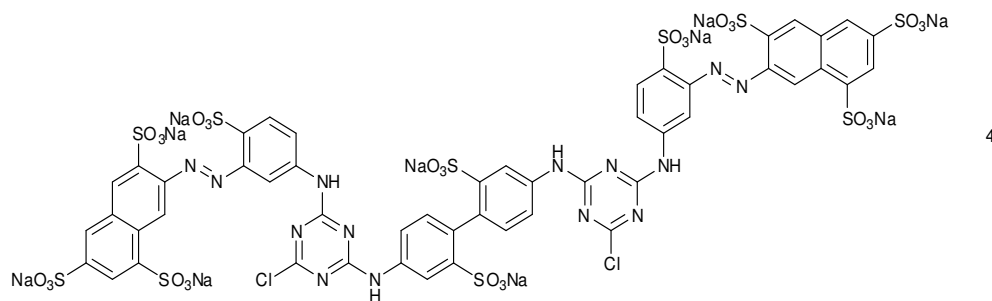
The dyes used were all known to be problematic with respect to removal of hydrolyzed dye, hence, requiring extensive wash-off treatments. Commercial samples of the *Procion H-E* dyes C.I. Reactive Yellow 84 (4), C.I. Reactive Red 141 (5), and C.I. Reactive Blue 171 (6) were kindly supplied by DyStar. Uniqema supplied a sample of 100% cotton, plain weave, 150 g m⁻², dyed on an industrial-scale with C.I. Reactive Red 120 (7), this was given no wash-off treatment

or rinsing prior to supply. Although the applied dye species would be those shown in 4-7, in terms of the dye species that would be removed during the wash-off process, it would be expected that the structure would be the hydrolyzed form (all -Cl substituted with -OH). All other general chemicals were obtained from Aldrich.

Table 1. DTIs used to remove hydrolyzed reactive dye.

Commercial name	Chemical type	M_r (g mol ⁻¹)	Form supplied
PVP	1	10,000	Solid powder
PVP K-15 ^a	1	6,000-15,000	Solid powder
PVP K-30 ^a	1	40,000-80,000	Solid powder
PVP K-90 ^a	1	900,000-1,500,000	Solid powder
PVP K-120 ^a	1	2,000,000-3,000,000	Solid powder
Chromabond S-100	2	35,000	40% (w/w) aqueous solution
Chromabond S-403E	3	30,000	40% (w/w) aqueous solution
PVNO Classic	3	25,000-28,000	40% (w/w) aqueous solution
PVNO Europe	3	11,000-15,000	40% (w/w) aqueous solution

^a The average relative molecular mass may range from 6,000-3,000,000 g mol⁻¹ as distributed by the Grades in terms of Fikentscher K-values.¹⁷



Dyeing

Cotton samples were dyed in sealed stainless steel dye pots of 300 cm³ capacity, housed in a laboratory-scale *Roaches Pyrotec 2000* dyeing machine, according to the dye manufacturer's recommended method.¹⁸ Woven cotton fabric (5 g), the reactive dye (3% on mass of fibre), and

anhydrous sodium sulfate (90 g dm^{-3}) were added to distilled water with a total solution:fibre ratio of 10:1 and the temperature held at $50 \text{ }^{\circ}\text{C}$ for 20 min. The temperature was then raised at a rate of $1.5 \text{ }^{\circ}\text{C min}^{-1}$ to 80°C and held for 30 min. Sodium carbonate (20 g dm^{-3}) was added to achieve a pH of 10.5 for nucleophilic substitution reaction with the dye and held at $80 \text{ }^{\circ}\text{C}$ for a further 60 min. The fibre was removed from the dyeing solution, retaining 200% of its mass of the dyeing solution, this was adopted to mimic dyeing conditions of industrial processes.

Wash-off

Dyed cotton samples were washed-off using the standard wash-off procedure (Figure 1; a six-stage process according to the dye manufacturer's recommended method¹⁸) using sealed stainless steel dyepots of 300 cm^3 capacity, housed in a laboratory-scale *Roaches Pyrotec 2000* dyeing machine. Throughout the wash-off process shown in Figure 1 (and Figure 2) "dyed fabric" is material that is dyed and unrinsed, and wet with twice its weight of original dyebath or preceding wash-off bath; in the case of the dyed and unrinsed C.I. Reactive Red 120, this was the "dyed fabric" used.

In comparison, dyed cotton samples were washed-off in a novel three-stage process using sealed stainless steel dyepots of 300 cm^3 capacity, housed in a laboratory-scale *Roaches Pyrotec 2000* dyeing machine. In the first stage, dyed woven cotton fabric (5 g) was added to distilled water with a total solution:fibre ratio of 10:1 and the temperature held at $20 \text{ }^{\circ}\text{C}$ for 10 min. The bath was then dropped. In the second stage, the samples from the first stage and the DTI polymer (1 g dm^{-3} active solids) were added to distilled water with a total solution:fibre ratio of 10:1 and the temperature held at $40 \text{ }^{\circ}\text{C}$ for 10 min. In the third stage the samples from the second stage

were added to distilled water with a total solution:fibre ratio of 10:1 and the temperature held at 20 °C for 10 min (Figure 2). For comparison to industrial processes, where high electrolyte content carry-over is often observed, the wash-off process detailed above was repeated including anhydrous sodium sulfate (20 g dm^{-3}) at the second stage.

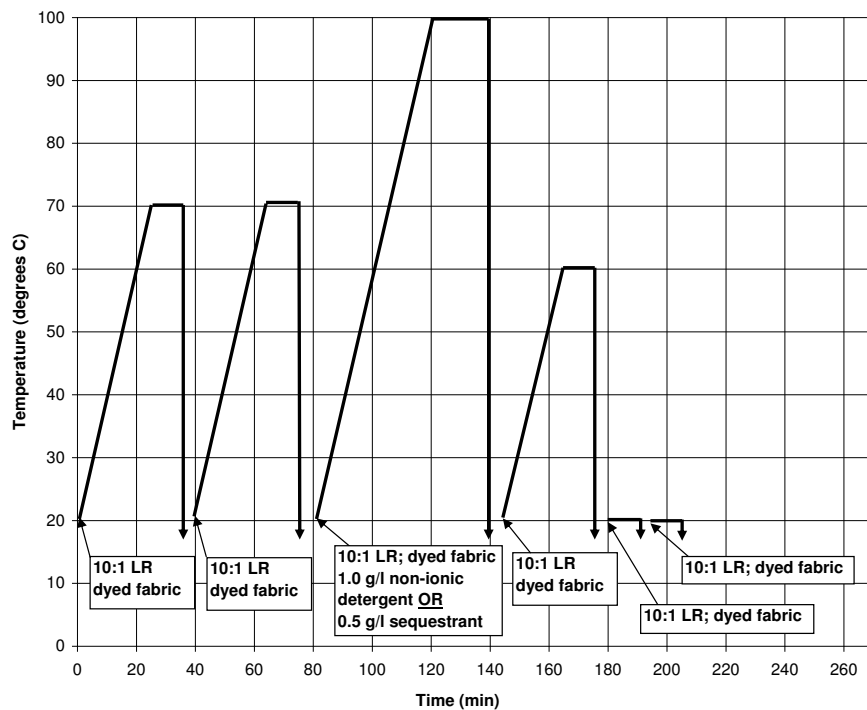


Figure 1. Standard *Procion H-E* wash-off procedure.¹⁸

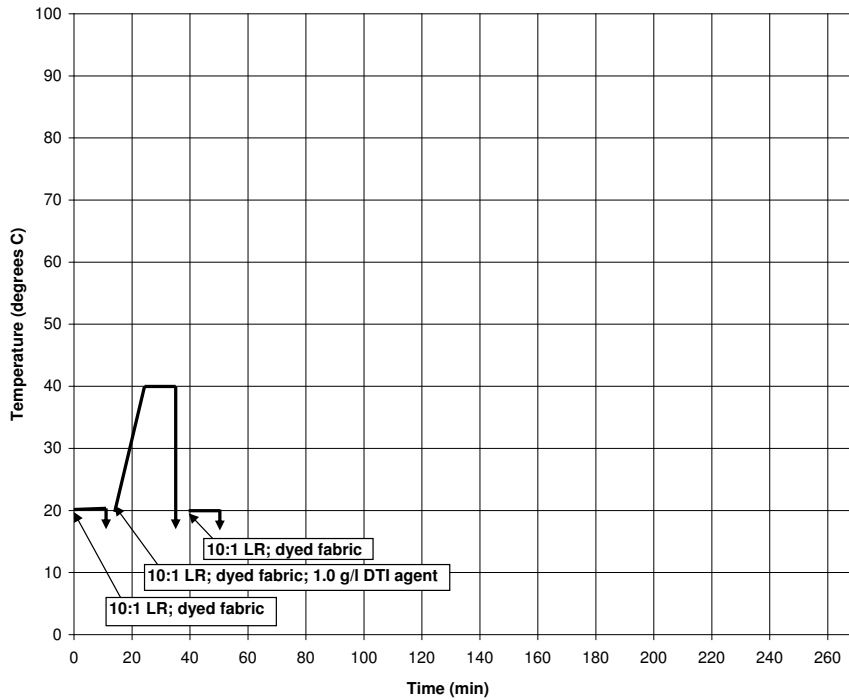


Figure 2. DTI wash-off procedure.

Color measurement

Spectral reflectance factors (taken between 400 and 700 nm wavelengths in 20-nm increments) of the samples were measured using a *Datacolor Spectraflash SF600* reflectance spectrophotometer (Datacolor International Ltd, UK) interfaced to a computer. Each fabric sample was folded twice to give a total of four layers. Four different areas of each sample were measured and the average color value was automatically calculated and saved by the computer.

CIELAB values (under illuminant D65 using the 10° standard observer) were automatically calculated. The color difference ΔE_{ab}^* was calculated from CIELAB coordinates $L^*a^*b^*$ using equation 1:

$$\Delta E_{ab}^* = \sqrt{[(L_r^* - L_t^*)^2 + (a_r^* - a_t^*)^2 + (b_r^* - b_t^*)^2]} \quad (1)$$

in which the subscripts r and t refer to the reference and test samples, respectively.

Wash fastness testing

Samples were subjected to the ISO 105:C06/C2S wash test (60°C) using SDC multifibre fabric as adjacent.¹⁹ The samples were washed five times using the same piece of multifibre strip for each washing. After washing the samples were visually assessed using grey scales according to the ISO 105:A03 test protocol¹⁹ to determine the degree of cross staining. The grey scale ranges from 5 for no stain on the adjacent fibers down to 1 for severe staining, with half points in between. A gray scale stain rating of 3 is suggested in the majority of standard performance specifications published by ASTM as a pass/fail borderline,²⁰ although many retailers set a higher standard at a gray scale rating of 4.

Energy consumption

The amount of energy consumed by the wash-off processes to heat water was calculated by equation 2, where Q is the heat added, c is the specific heat (water = 4.1868 J g⁻¹), m is mass, and ΔT is change in temperature. The total energy consumption for the whole wash-off process was calculated by addition of energy consumption for each stage.

$$Q = cm\Delta T \quad (2)$$

Computational chemistry

The geometry of the methyl capped DTI polymer repeat units (**1-3**) was optimized using a DFT method (B88PW91/DZVP) and the charge distribution calculated by using point charge fitting (PCF) charges and produce plots of the electrostatic potential plotted onto a total electron density isosurface (0.09). Blue is used to represent the strongest negative electrostatic potential on the molecule and red the strongest positive electrostatic potential. The other colors are the values in between, green is neutral. In each case the oxygen atoms are negatively charged. The interaction orientation of these repeat units with functional groups that are usually observed on dye molecules were investigated by using ISOSTAR. Plots were constructed of the interaction of any OH group in the Cambridge Scientific Database (CSD) with the pyridine-*N*-oxide and pyrrolidone groups.

Results and discussion

Table 2 shows the color difference (ΔE_{ab}^*) between dyeings that had received the standard *Procion H-E* wash-off procedure (Figure 1) and the modified DTI wash-off process. It is evident from the data that ΔE_{ab}^* in all cases where a DTI was applied was relatively low, suggesting that the wash-off procedures did not detrimentally effect the final expected visual appearance of the dyeings ($\Delta E_{ab}^* \approx 2.3$ corresponds to a just noticeable difference²¹). Higher ΔE_{ab}^* values are observed where no DTI or non-ionic detergent alone were used in the modified wash-off process, which may suggest that these two processes do not sufficiently remove hydrolyzed dye from the fabric that may result in an observable color difference in comparison with the standard *Procion H-E* wash-off process.

Table 2. Color difference (ΔE^*_{ab}) between dyeings that had received the standard *Procion H-E* wash-off procedure (reference) and the modified DTI wash-off process (no Na₂SO₄ added).

DTI	C.I. Reactive Red 120	C.I. Reactive Yellow 84	C.I. Reactive Red 141	C.I. Reactive Blue 171
None	2.7	2.8	3.2	1.9
Sandozin NIE	2.3	2.1	1.9	1.8
PVP	1.6	1.2	1.3	1.3
PVP K-15	1.0	1.1	1.2	1.0
PVP K-30	1.4	1.5	1.3	1.2
PVP K-90	0.7	1.0	1.2	1.1
PVP K-120	1.3	1.2	1.4	1.3
Chromabond S-100	1.5	1.1	1.2	1.0
Chromabond S-403E	1.4	0.9	0.8	0.8
PVNO Classic	0.5	0.3	0.5	0.2
PVNO Europe	0.5	0.1	0.4	0.3

Table 3 shows the grey-scale ratings for the staining of the cotton portion of the adjacent multifibre as a result of the fastness tests; staining to other fibre types was not observed in any case. The standard *Procion H-E* wash-off procedure (Figure 1) would be expected to give resultant washed-off dyeings that achieved a grey-scale rating of 5, as a result of complete removal of any hydrolyzed dye with only covalently bound dye remaining. From the data it is evident that without the use of a DTI (None) the developed shortened, lower energy and water consumption wash-off procedure (Figure 2) is insufficient to affect the high grey-scale rating required.

Table 3. Grey-scale ratings for staining to adjacent cotton.

DTI	C.I. Reactive Red 120		C.I. Reactive Yellow 84		C.I. Reactive Red 141		C.I. Reactive Blue 171	
	20 g dm ⁻³ Na ₂ SO ₄	No Na ₂ SO ₄	20 g dm ⁻³ Na ₂ SO ₄	No Na ₂ SO ₄	20 g dm ⁻³ Na ₂ SO ₄	No Na ₂ SO ₄	20 g dm ⁻³ Na ₂ SO ₄	No Na ₂ SO ₄
None	2/3	3	2	3	2	3	2/3	3
<i>Sandozin NIE</i>	3/4	4	3/4	4	3	4	3/4	4
PVP	4/5	4/5	4	4/5	4/5	4/5	4/5	4/5
PVP K-15	4/5	5	4	4/5	4/5	4/5	4/5	4/5
PVP K-30	4/5	4/5	4/5	4/5	3/4	4	4	4
PVP K-90	4/5	4/5	4/5	4/5	4	4	4	4
PVP K-120	5	5	4/5	4/5	4	4/5	4	4/5
<i>Chromabond S-100</i>	5	5	5	4/5	4/5	4/5	4/5	4/5
<i>Chromabond S-403E</i>	5	5	5	5	5	5	5	5
<i>PVNO Classic</i>	5	5	5	5	5	5	5	5
<i>PVNO Europe</i>	5	5	5	5	4/5	5	5	5
Standard wash-off (Figure 1)	5	5	5	5	5	5	5	5

The use of a non-ionic detergent (*Sandozin NIE*) does secure an improved wash-off, but it is still significantly below the standard required. The staining rating is generally worse when sodium sulfate is present, this is expected as the high level of electrolyte present in the wash-off bath causes aggregation of dye molecules and pushes the [dye in fibre ↔ dye in solution] equilibrium towards the dye remaining in the fibre, hence an insufficient level of hydrolyzed dye removal was observed. Electrolyte may also reduce the detergency of *Sandozin NIE* by

precipitation. When the DTIs are employed in the developed wash-off procedure, it is clearly evident that, in most cases, they enable the removal of comparatively high levels of hydrolyzed dye removal, which is reflected in higher grey-scale ratings subsequent to wash fastness testing.

From the data it is observed that the different DTI polymer types varied in their efficacy of dye removal in the following order: **3** > **2** > **1**. Poly(vinylpyridine-*N*-oxide) polymers were the most effective with respect to the level of hydrolyzed dye removal closely followed by the poly(vinylpyridine betaine) polymers which were also highly efficient in hydrolyzed dye removal. Although poly(vinylpyrrolidone) polymers did affect improvement in the wash-off of the hydrolyzed dye, their efficacy was notably inferior to type **2** and **3** DTIs. It is also observed that the lowest ΔE_{ab}^* occurred when type 3 DTIs were used in the wash-off process, suggesting these polymers remove similar levels of hydrolyzed dye in comparison with the standard *Procion H-E* wash-off procedure.

It would be expected that the mode of interaction of these polymeric systems with dye molecules would be affected by the distribution of charge around the repeat unit. From the PCF plots on the electron density isosurface (Figure 3) it is observed that the aromatic DTI polymers (**2** and **3**) have greater delocalization of positive electrostatic potential in comparison with the aliphatic DTI polymers (**1**). For poly(vinylpyridine betaine) and poly(vinylpyridine-*N*-oxide) polymers, the positive electrostatic potential extends around the H atoms of the aromatic ring and that potential on the isosurface is 3.1 times the order of magnitude (average PCF 0.171) in comparison with the aliphatic poly(vinylpyrrolidone) polymers (average PCF 0.055). Additionally, with type **2** and **3** DTI polymers positive electrostatic potential is relatively equally delocalized around the four H atoms, whereas with type **1** DTI polymers most positive electrostatic potential is concentrated on the two H atoms of C3 on the pyrrolidone ring. As such,

the stronger overall electrostatic potential of poly(vinylpyridine betaine) and poly(vinylpyridine-*N*-oxide) polymers and the uniform delocalization of that potential would explain why such DTI polymers secure superior removal and association with anionic hydrolyzed reactive dye molecules in comparison with poly(vinylpyrrolidone) polymers.

This superior performance is further evidenced and explained through ISOSTAR predictions of interactions of hydroxyl groups with pyrrolidone and pyridine-*N*-oxide groups (Figure 4). There are a significantly higher number of records relevant to the pyridine-*N*-oxide group as compared to the pyrrolidone unit, which would indicate that the interaction of OH groups, and subsequent hydrogen bonding, of hydrolyzed reactive dyes with type 3 DTI polymers would be significantly greater and more extensive than type 1 DTI polymers.

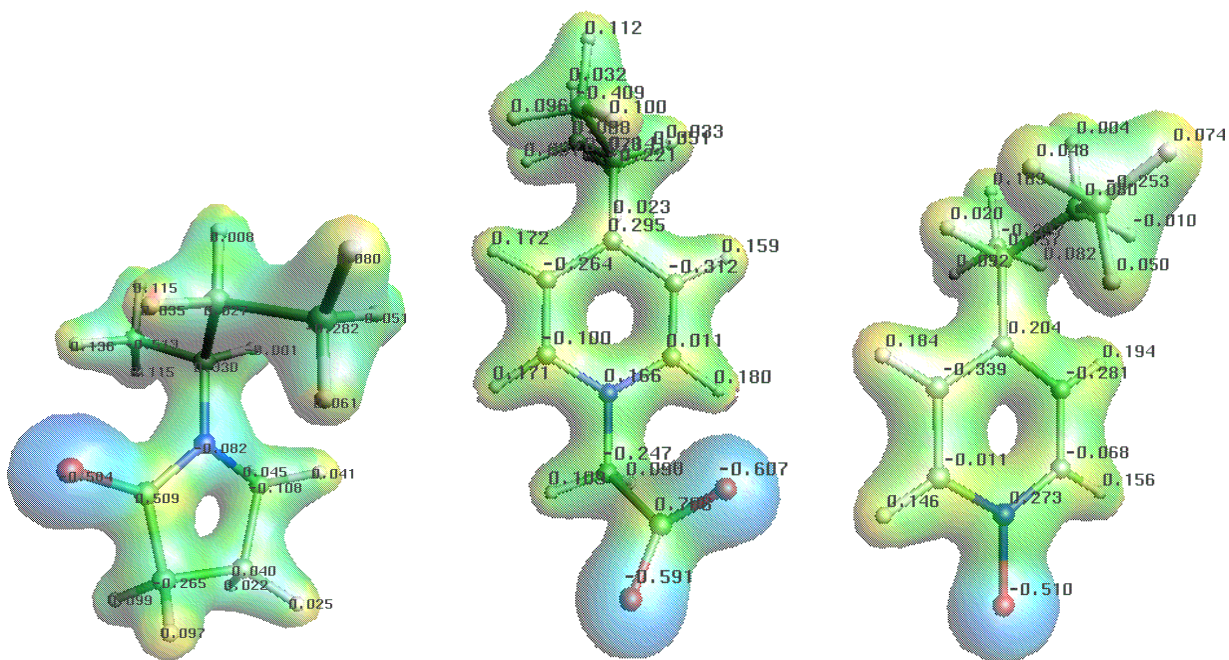


Figure 3. PCF charges plotted onto a total electron density isosurface for DTI polymer repeat units; poly(vinylpyrrolidone) (left), poly(vinylpyridine betaine) (center), poly(vinylpyridine-*N*-oxide) (right)

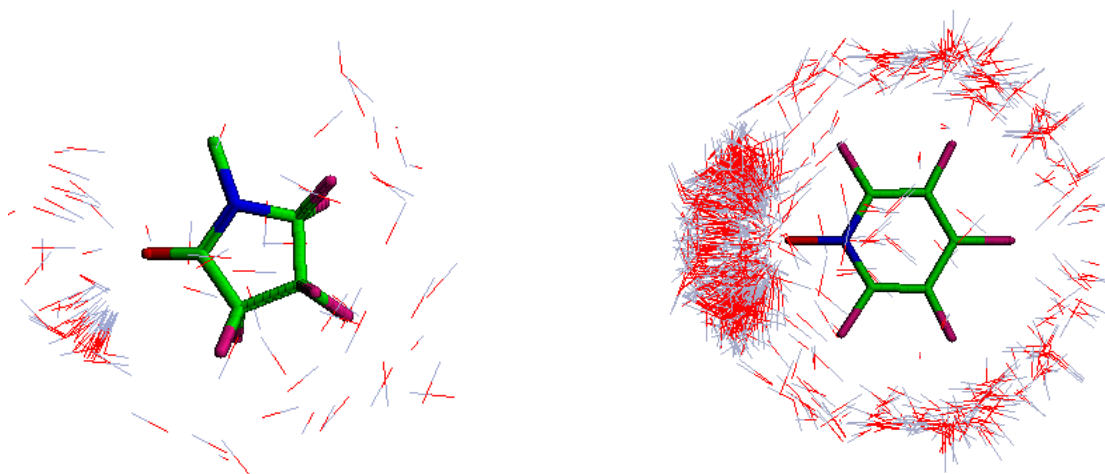


Figure 4. The interaction of pyrrolidone (left) and pyridine-*N*-oxide (right) with any OH group in the CSD. H atoms on the repeat units have been colored purple and H atoms on the OH group are grey.

The experimental results indicated that type **3** DTI polymers were marginally superior in their performance in comparison with type **2** DTI polymers. Although their positive electrostatic potentials and the delocalization of those potentials are relatively similar, the reason for the superior performance of polymers based on vinylpyridine-*N*-oxide may be related to conformation and accessibility of hydrolyzed reactive dye molecules to the polymers. Poly(vinylpyridine-*N*-oxide) is very planar, insofar as the active moiety extends in one axis from the vinyl polymer backbone, whereas poly(vinylpyridine betaine) extends in two axes from the backbone as the carboxyl group extends out of plane. This could lead to some steric effects that could compromise the effectiveness of the type **2** DTI polymers.

The use of DTIs in the wash-off of reactive dyes on cotton enables a much more efficient process to be developed. Table 4 provides a breakdown analysis of the time, water consumption

and energy consumption for the developed DTI procedure in comparison with the standard recommended wash-off procedure. It is evident that the DTI process operation time is <25% that of the standard, the total water consumption is halved, it consumes 9% of the energy of the recommended wash-off process.

Table 4. Comparison of different wash-off procedures.

Procedure	Time (min)	Water (dm³ kg⁻¹)^a	Energy (Q) (MJ kg⁻¹)^a
Recommended wash off	205	60	9.21
DTI wash-off	50	30	0.84

^a per kg fabric processed.

It could be argued that the use of these DTIs would provide additional chemical hazard in the effluent, but these types of polymers are already extensively used in domestic laundering. Considering a 1 kg reactive dyed cotton garment that may have a life of 100 washes, based on an average 3 kg washing load²² using 108 g washing powder per load²³ and with a DTI concentration of 1%,¹⁶ such a garment would consume 36 g DTI in its life after production. Using the concentrations specified in this work, the same 1 kg garment would consume 10 g DTI in the new wash-off process, an additional 27% over its full life cycle. However, the DTI would replace the same mass of detergent in the standard wash-off process, so the total mass of chemicals is equal. Additionally, through further development it may be possible to reduce the concentration of DTI polymer required to enable efficient hydrolyzed reactive dye wash-off. Nevertheless, the additional DTI chemicals are far outweighed from a sustainability perspective

by the saving made in terms of water and energy and economically in terms of time and energy costs, making this novel wash-off system a much greener alternative.

The application of the DTI wash-off process might affect the treatability of the effluent: if the same amount of dye is present in a smaller volume of effluent, the effluent color would be more intense, and hence less acceptable, but this may make the treatment of the effluent more efficient, particularly if sorption treatment techniques are applied.²⁴ However, the DTI process may result in a higher electrolyte content (total dissolved solids) due to the lower volume of water used in the wash-off process, and this would need to be considered in effluent treatment.

The use of DTIs in the wash-off of reactive dyes on cotton enables a much more efficient, economical and sustainable process to be developed, which significantly reduces operation time, water consumption and energy consumption. When the DTIs are employed in the developed wash-off procedure they enable comparatively high levels of hydrolyzed dye removal through formation of a complex with the anionic dye molecules. Different DTI polymer types varied in their efficacy of dye removal; poly(vinylpyridine-*N*-oxide) polymers were the most effective with respect to the level of hydrolyzed dye removal closely followed by the poly(vinylpyridine betaine) polymers which were also highly efficient in hydrolyzed dye removal, with poly(vinylpyrrolidone) polymers being the least effective. These differences were attributed to variations in the magnitude and delocalization of positive electrostatic potential of the functional moieties in the polymers and the extent of and propensity for hydrogen bonding with the hydrolyzed reactive dyes.

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Author Contributions

The manuscript was written through contributions of all authors. All authors contributed equally.

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A sustainable chemistry method to improve the wash-off process of reactive dyes on cotton

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Polymers employed in novel reactive dye wash-off process that reduces operation time, water consumption and energy consumption.

