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### **Carbon sequestration in biogenic magnesite and other magnesium carbonate minerals**

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# Carbon sequestration in biogenic magnesite and other magnesium carbonate minerals

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## 1 **Abstract**

2 The stability and longevity of carbonate minerals make them an ideal sink for surplus atmospheric  
3 carbon dioxide. Biogenic magnesium carbonate mineral precipitation from the magnesium-rich  
4 tailings generated by many mining operations could offset net mining greenhouse gas emissions,  
5 while simultaneously giving value to mine waste products. In this investigation, cyanobacteria in  
6 a wetland bioreactor enabled the precipitation of magnesite ( $\text{MgCO}_3$ ), hydromagnesite  
7  $[\text{Mg}_5(\text{CO}_3)_4(\text{OH})_2 \cdot 4\text{H}_2\text{O}]$ , and dypingite  $[\text{Mg}_5(\text{CO}_3)_4(\text{OH})_2 \cdot 5\text{H}_2\text{O}]$  from a synthetic wastewater  
8 comparable in chemistry to what is produced by acid leaching of ultramafic mine tailings. These  
9 precipitates occurred as micrometer-scale mineral grains and microcrystalline carbonate coatings  
10 that entombed filamentous cyanobacteria. This provides the first laboratory demonstration of low  
11 temperature, biogenic magnesite precipitation for carbon sequestration purposes. These findings  
12 demonstrate the importance of extracellular polymeric substances in microbially enabled  
13 carbonate mineral nucleation. Fluid composition was monitored to determine carbon sequestration  
14 rates. The results demonstrate that up to 238 t of  $\text{CO}_2$  could be stored per hectare of wetland/year  
15 if this method of carbon dioxide sequestration was implemented at an ultramafic mine tailing  
16 storage facility. The abundance of tailings available for carbonation and the anticipated global  
17 implementation of carbon pricing make this method of mineral carbonation worth further  
18 investigation.

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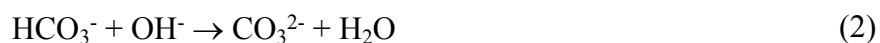
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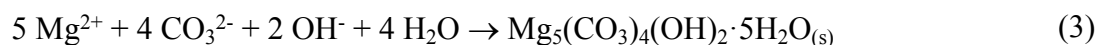
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## 24 1. Introduction

25 Microbially-mediated carbonate mineral precipitation reactions, commonly referred to as  
26 microbial carbonation, have been documented in numerous environments, induced by organisms  
27 including cyanobacteria (1-3), sulfate reducing bacteria (4, 5), ureolytic bacteria (6, 7), and  
28 oxalotrophic bacteria (8, 9). This biogeochemical process has potential to produce stable, long-  
29 term sinks for atmospheric carbon dioxide (CO<sub>2</sub>) (10-13). Stable carbonate minerals are a desirable  
30 sink for atmospheric CO<sub>2</sub>, prompting the investigation of a range of carbon sequestration strategies  
31 that aim to precipitate carbonate minerals (10, 11, 14-24).

32 Passive carbonate mineral formation from ultramafic tailings produced by nickel, diamond,  
33 and asbestos mining operations has been studied at active and historic mine sites (15, 25-28). The  
34 high surface area of tailing minerals allows for greater weathering and carbonation reaction rates  
35 than those typically observed for natural bedrock (29). The ability of cyanobacteria to mediate the  
36 precipitation of hydrated magnesium carbonate minerals has been previously documented (30-32),  
37 and could be stimulated by utilizing soluble magnesium derived from dissolution of ultramafic  
38 tailings (13, 33). Cyanobacterial photosynthesis produces hydroxyl (OH<sup>-</sup>) anions that promote  
39 carbonate mineral precipitation by increasing the pH value and thus the proportion of dissolved  
40 carbonate (CO<sub>3</sub><sup>2-</sup>) species, as outlined in Reactions 1-3 (34). The extracellular surfaces of bacteria  
41 and their encapsulating exopolymer are negatively charged due to the presence of functional  
42 groups, such as carboxyls (35). These functional groups can bind divalent cations, thereby  
43 generating microenvironments with high cation concentrations that favor carbonate mineral  
44 precipitation reactions.





### Dypingite

45

46 The present study characterizes the ability of a phototrophic microbial consortium to drive  
47 Mg-carbonate mineral formation using atmospheric CO<sub>2</sub> in a wetland bioreactor (Figure 1). The  
48 bioreactor was inoculated with microbial mats predominantly composed of filamentous  
49 cyanobacteria that were collected from a natural wetland associated with a hydromagnesite-  
50 magnesite playa near Atlin, British Columbia, Canada (32, 36, 37). In addition to cyanobacteria,  
51 the microbial mats host abundant diatoms that remove dissolved silica from solution. The mats  
52 overlie anoxic sediments known to host sulfate reducing bacteria that have been previously shown  
53 to precipitate iron sulfide minerals (37). An Mg-rich synthetic mine wastewater, the chemistry of  
54 which was based on a tailings leaching experiment completed by McCutcheon et al. (33), was  
55 added to the bioreactor. Spatial and temporal changes in water chemistry and mineral precipitates  
56 were used to calculate the rate of carbon storage, thereby demonstrating this carbon sequestration  
57 strategy on a scale at least one order of magnitude greater than typical laboratory experiments.

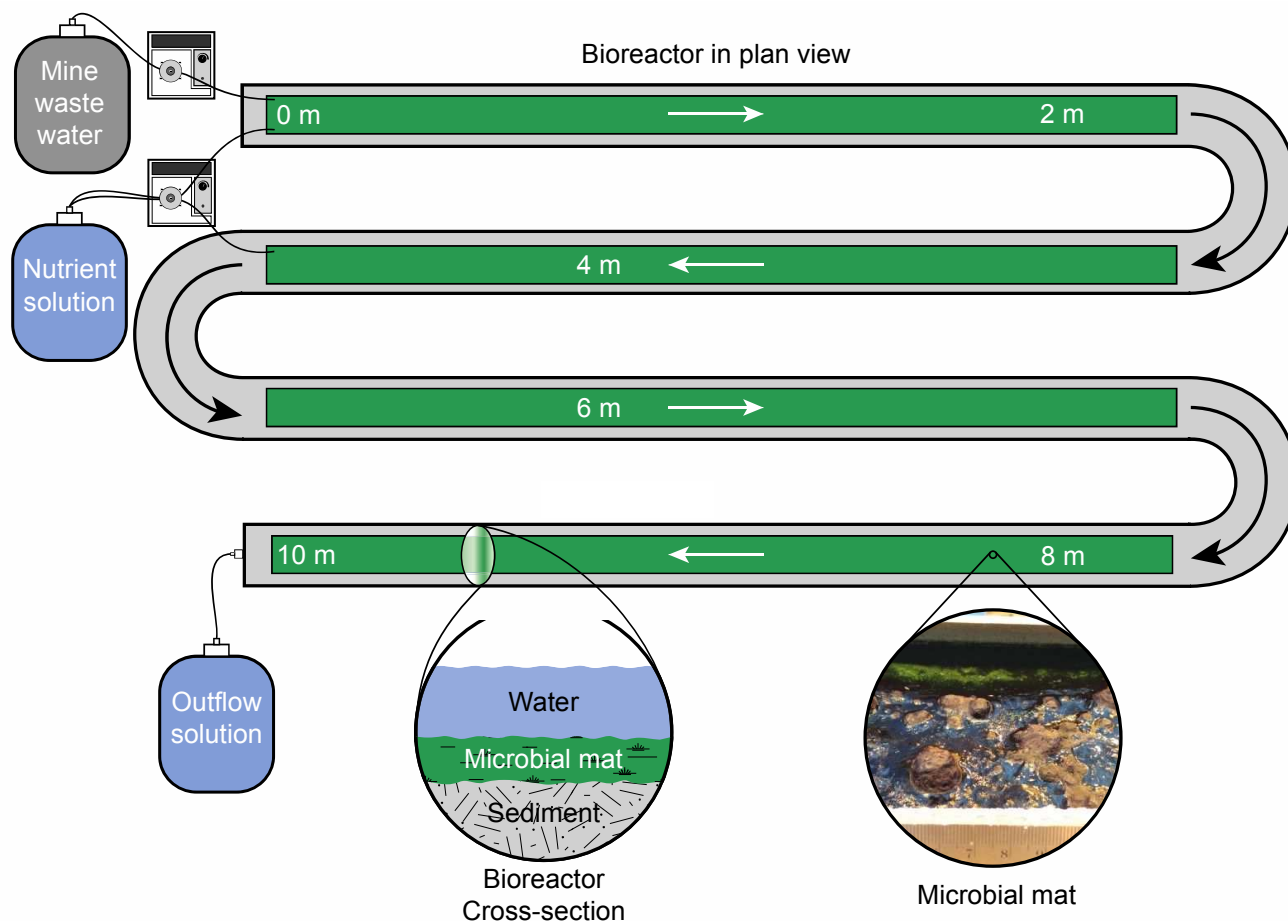
## 58 2. Methods

### 59 2.1 Bioreactor design

60 In this 67-day experiment, synthetic mine wastewater and nutrient solutions were added to  
61 a 10 m long flow-through bioreactor constructed of 15 cm diameter polyvinyl chloride pipe (see  
62 Supplementary Information (SI) for details). The bioreactor was initially constructed for the  
63 experiment presented in McCutcheon et al. (13), in which the natural biogeochemical conditions  
64 of the wetland associated with the hydromagnesite-magnesite playa near Atlin were modelled.  
65 Prior to the present study, the microbial mats in the bioreactor were culled to allow for growth of

66 second generation mats containing no Mg-carbonate minerals (confirmed using electron  
67 microscopy). Rather than modelling the natural wetland, the present study targeted the  
68 biogeochemical conditions of an engineered mine site bioreactor wetland for the purposes of  
69 maximizing carbon sequestration in Mg-carbonate minerals. A critical experimental parameter by  
70 which the present study differs from its precursor is that an inorganic carbon source was not  
71 provided, which is crucial as the ingress of CO<sub>2</sub> into mineral carbonation reactors is a known  
72 limiting factor (38), and must be overcome for large-scale implementation of mineral carbonation.  
73 Additionally, the synthetic mine wastewater added to the bioreactor contained 5000 ppm (205.8  
74 mM) Mg<sup>2+</sup>. This value, which is five times greater than that used in the 2014 study, was based on  
75 the results of a tailings leaching experiment (33) in order to better represent an industrial tailing  
76 leachate. With dypingite as the target mineral (Reaction 3), the number of cycles of carbon fixation  
77 (Reaction 1) required to make the necessary hydroxyl and carbonate anions (Reaction 3) per  
78 molecule of dypingite produced was calculated as ten (13). The classic phytoplankton biomass  
79 formula [(CH<sub>2</sub>O)<sub>106</sub>(NH<sub>4</sub>)<sub>16</sub>(H<sub>3</sub>PO<sub>4</sub>)] was used as a guideline to determine the phosphorous and  
80 nitrogen required in the nutrient solution (39). The synthetic mine wastewater solution chemistry  
81 was used to calculate the nutrient requirements of the microbes in the bioreactor using modified  
82 BG-11 growth medium (SI Tables S1 and S2) (40). The solutions were added to one end of the  
83 bioreactor (0 m), from which they could passively flow through the gravity-driven system and  
84 drain out the other end. A second nutrient solution inflow was located at 5 m. The inflow rate of  
85 both solutions was increased over time to determine the response of the bioreactor to a high influx  
86 of soluble magnesium (Table 1). The bioreactor was housed in greenhouse with an average air  
87 temperature of 23.5°C, as documented at all sampling time points, and subject to diurnal 12 h

88 light/dark conditions. The experiment took place in southern Canada from December to March,  
 89 and thus the light was provided by a combination of natural and artificial sources.



90  
 91 Figure 1. Plan view schematic of the bioreactor inoculated with microbial mats for the carbonation experiment. The  
 92 synthetic mine wastewater was added at one end of the channel (0 m), while the nutrient solution was added at 0 m  
 93 and 5 m. The gravity driven system allowed for the solution to flow passively through the bioreactor and out a valve  
 94 in the other end. Arrows indicate the direction of flow. The four straight segments of the bioreactor were open to the  
 95 air and contained the active microbial mats (green segments in the schematic), while the bends were covered. A cross-  
 96 section of the bioreactor contents is shown, along with a photograph of the pellicle that formed at the air-water  
 97 interface.  
 98

99 After 21 days, a pellicle, a biofilm at the air-water interface, developed as sections of mat  
 100 were buoyed up to the water surface by trapped photosynthetically-generated oxygen bubbles. The  
 101 pellicle was removed because it was restricting the photosynthesis of the benthic microbial mats  
 102 and causing a decrease in dissolved oxygen concentration in the bioreactor water. At this time, the



103 addition of the wastewater solution was ceased and the growth medium concentration was halved  
 104 to moderate microbial activity (Table 1). The bioreactor outflow volume was measured to quantify  
 105 evaporation, which indicated that 45% of the added water evaporated during the experiment. This  
 106 water loss was taken into account for mass balance calculations for the system and when  
 107 interpreting conductivity, inductively coupled plasma-atomic emission spectroscopy (ICP-AES),  
 108 ion chromatography (IC), and dissolved inorganic carbon (DIC) results (SI Table S3).

109

110 Table 1. Fluid composition for the nutrient and synthetic mine wastewater solutions added to the  
 111 bioreactor during the carbonation experiment. Summary of the timeline for solution addition to the  
 112 bioreactor at the 0 and 5 m locations. Note, the experiment was paused between day 21 and 32 due  
 113 to the formation of the pellicle.

Solution type	Fluid composition measurements			Cation and anion concentrations (mM)					
	pH	DO (mg/mL)	Conductivity (mS/cm)	Mg <sup>2+</sup>	Ca <sup>2+</sup>	DIC	PO <sub>4</sub> <sup>3-</sup>	NO <sub>3</sub> <sup>-</sup>	NO <sub>2</sub> <sup>-</sup>
100% nutrient solution	5.91	4.20	6.64	0.01	0.78	0.20	6.10	74.9	0.00
50% nutrient solution	5.91	6.11	3.65	0.00	0.34	0.20	2.28	30.7	0.00
Wastewater	8.10	7.37	18.1	196	8.16	0.21	0.00	0.00	0.00

Solution addition timeline				
Day	0 m solution addition point		5 m solution addition point	
	Solution	Flow rate (L/day)	Solution	Flow rate (L/day)
1-21	100% nutrients	1	100% nutrients	1
	Wastewater	1		
21	Experiment paused and the pellicle removed			
22-31	Standard BG-11	1	Standard BG-11	1
32	Experiment resumed			
32-38	50% nutrients	1	100% nutrients	1
	Wastewater	1		
39-45	50% nutrients	2	50% nutrients	2
	Wastewater	2		
46-52	100% nutrients	3		
	Wastewater	3		
53-59	100% nutrients	4		
	Wastewater	4		
60-67	50% nutrients	5		
	Wastewater	5		

114

## 115 **2.2 Mineral and microbe characterization**

116 Microbial mat samples collected at 0 m prior to the experiment, and at 0 m, 5 m, and 10 m  
 117 on days 28 and 67 were analyzed using X-ray diffraction (XRD). The mats were air dried in petri  
 118 dishes and powdered using a mortar and pestle. The samples were analyzed using a Bruker D8

119 Focus Bragg-Brentano diffractometer and mineral phases were determined using DIFFRAC<sup>plus</sup>  
120 Eva software (see SI for details). Additional microbial mat samples were collected on days 14 and  
121 28 from the same locations representing upstream, midstream, and downstream mats for analysis  
122 using scanning electron microscopy and energy dispersive spectroscopy (SEM-EDS; see SI for  
123 details). After 67 days, microbial mats were sampled at 1 m increments for SEM-EDS. A sample  
124 of microbial mat collected from the 10 m location in the bioreactor on day 67 was fixed using  
125 2%<sub>(aq)</sub> glutaraldehyde, and stained using 2%<sub>(aq)</sub> OsO<sub>4</sub>, 1.5%<sub>(aq)</sub> ferricyanide, and 1%<sub>(aq)</sub>  
126 thiocarbohydrazide prior to being dehydrated using acetone, and embedded in Epon Embed 812  
127 resin, described in detail in McCutcheon and Southam (41) as a protocol adapted for use on natural  
128 microbial biofilms (42). Ultrathin sections of the embedded sample were characterized using  
129 transmission electron microscopy (TEM) in conjunction with selected area electron diffraction  
130 (SAED) and EDS (see SI for details).

### 131 **2.3 Fluid composition analyses**

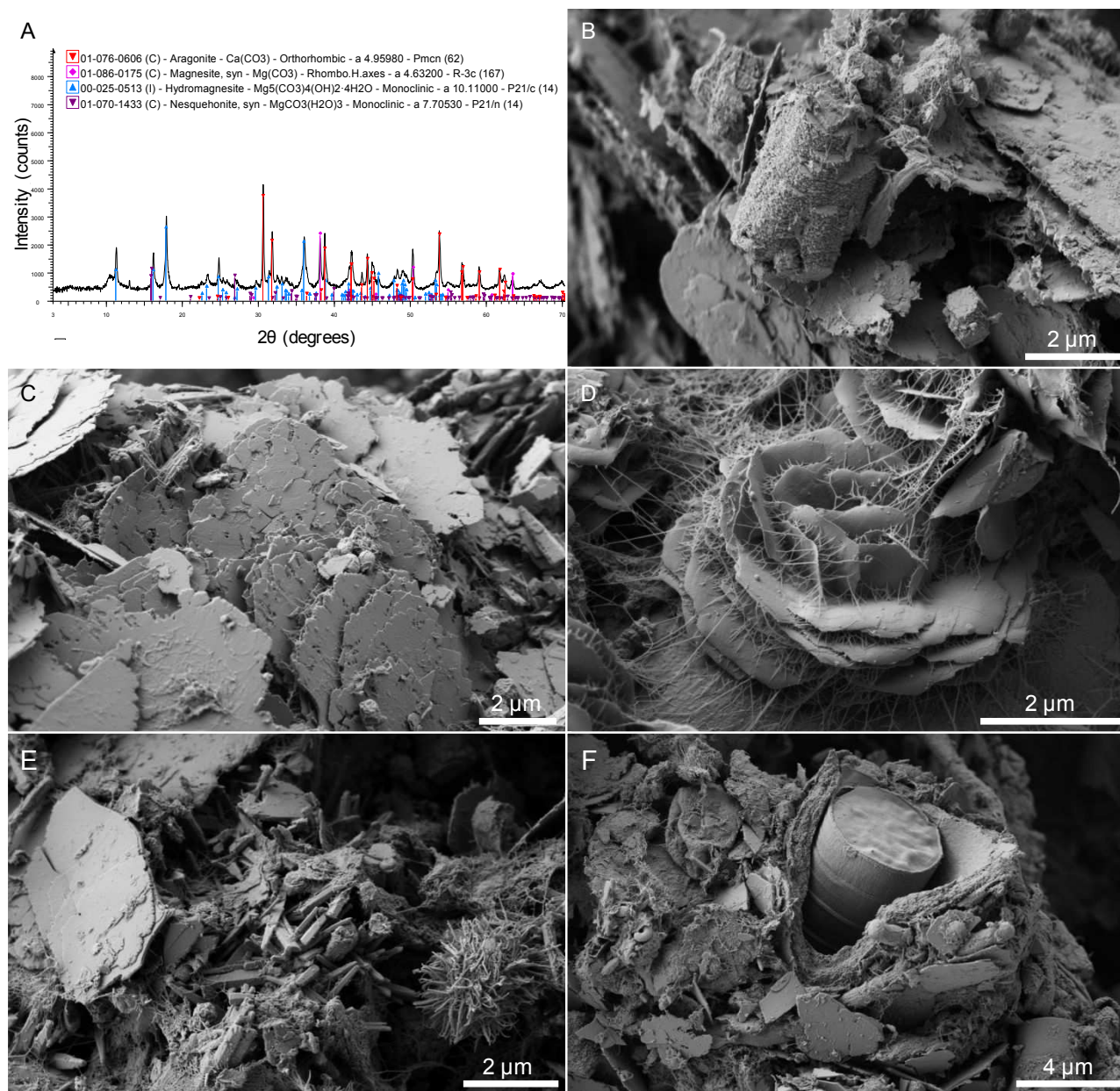
132 Fluid composition was monitored weekly at 1 m increments along the length of the  
133 bioreactor. Dissolved oxygen (DO), pH, and conductivity were measured using probes (see SI for  
134 details). Water samples were collected and filtered (0.1 μm pore-size) to determine DIC, and major  
135 cation (ICP-AES) and anion (IC) concentrations at each location (see SI for details). Due to the  
136 high concentration, magnesium was analysed using IC instead of ICP-AES. Stable carbon isotopic  
137 measurements of DIC is another means of determining whether a solution is at equilibrium with  
138 atmospheric CO<sub>2</sub> (25). Stable carbon, oxygen, and hydrogen isotope analysis was conducted on  
139 water samples collected 1 week after the experiment concluded (see SI for details). Saturation  
140 indices (*SI*) for possible mineral products were determined using PHREEQC (43) and the fluid

141 composition data were used to evaluate how pH, and the availability of  $Mg^{2+}$  and DIC species  
142 influence carbonate mineralization (see SI for PHREEQC details).

### 143 **3. Results**

#### 144 ***3.1 Carbonate mineral precipitation***

145 XRD analysis of the pre-experiment microbial mat sample identified thenardite ( $Na_2SO_4$ )  
146 and aragonite ( $CaCO_3$ ) (SI Figure S1A), neither of which were observed with SEM (SI Figure  
147 S2A). Magnesite, hydromagnesite, dypingite, aragonite ( $CaCO_3$ ), and nesquehonite  
148 [ $Mg(HCO_3)(OH) \cdot 2H_2O$ ] were identified as mineral precipitates in the bioreactor microbial mats  
149 using XRD (Figure 2, SI Figure S1B,C). Subhedral rhombohedral magnesite crystals were  
150 predominantly observed between 4 and 10 m in the bioreactor and were identified using TEM-  
151 EDS and SAED (Figure 3A,B, SI Table S4). The magnesite often occurred at convergent points  
152 between multiple hydromagnesite plates (Figure 3C-E), a relationship documented in natural  
153 samples by Power et al. (36). Note the tendency of magnesite crystals to fall out of the ultrathin  
154 sections, as seen in Figure 3E. For those that were retained, SAED confirms that these precipitates  
155 are hexagonal, and indicates that they are polycrystalline in nature (Figure 3A,B).

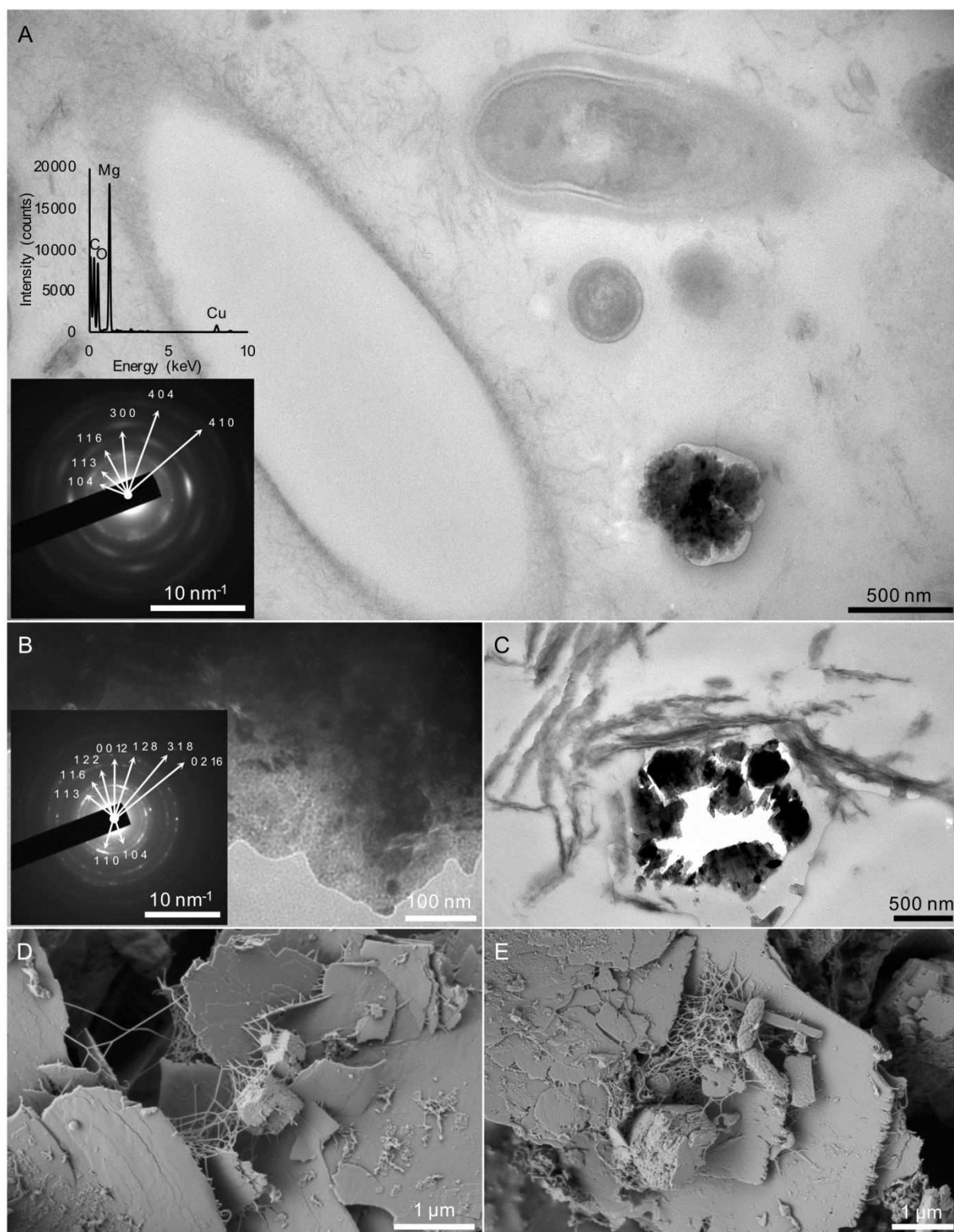


156  
 157 Figure 2. X-ray diffraction and SEM results for the key mineral precipitates produced in this study. A: Pattern  
 158 produced by XRD analysis of a sample of microbial mat collected at 5 m on day 67 of the carbonate precipitation  
 159 experiment. Scanning electron micrographs depicting: B: rhombohedral magnesite crystals found between 4 and 10  
 160 m in the bioreactor; C: platy hydromagnesite or dypingite crystals formed throughout the bioreactor; D: a rosette of  
 161 hydromagnesite or dypingite covered in EPS (day 67, 1 m); E: platy hydromagnesite or dypingite crystal (left),  
 162 disarticulated aragonite crystals (centre), and mineral coated coccoid bacterium (right); and F: cyanobacterium  
 163 filament encased in Mg-carbonate encrusted EPS (day 14, 10 m).  
 164

165 Hydromagnesite or dypingite crystals were the most abundant precipitates and occurred as  
 166 plates and rosettes, often associated with large amounts of extracellular polymeric substances  
 167 (EPS; Figure 2C,D). The EPS exhibits the collapsed, mesh-like morphology commonly observed

168 when biofilms are prepared for SEM via solvent dehydration and critical point drying (41). The  
169 platy hydromagnesite or dypingite precipitates visible using SEM (Figure 4A) can also be observed  
170 using TEM, oriented tangential to the filamentous cells such that only the edge of the platy crystals  
171 can be observed (Figure 4B). The platy precipitates can be observed nucleating on EPS  
172 surrounding filamentous cyanobacteria (Figure 4B,C), as demonstrated by McCutcheon and  
173 Southam (41). In addition to crystalline precipitates, cells and surrounding EPS often appear coated  
174 in microcrystalline precipitates (Mg-C-O based on EDS), resulting in cells becoming entombed  
175 (Figure 2F), likely interfering with microbial metabolism. Many empty Mg-carbonate casts  
176 exhibiting the morphology of cyanobacterium filaments were observed using TEM (Figure 4D)  
177 and SEM (Figure 4E,F), appearing to encase a framework of EPS. Poorly crystallized ~100 nm-  
178 scale pseudo-acicular precipitates composed of Ca-Mg-C-O-P formed directly on coccoid  
179 microbial cells (Figure 2E, 4G,H), much like the extracellular precipitate morphology observed by  
180 Shuster et al. (44).

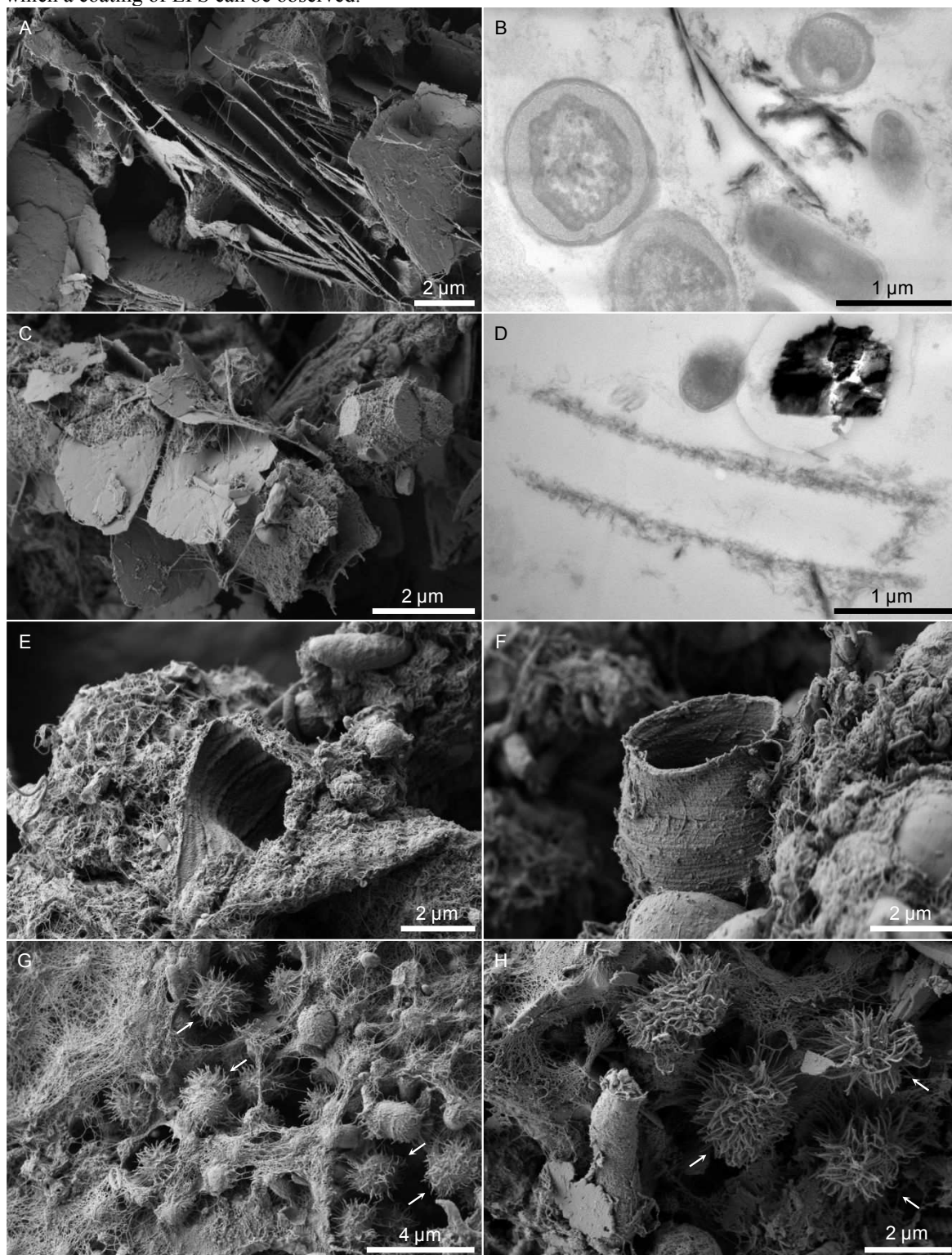
181 Aragonite was observed as prismatic crystals (SI Figure S2B,C), similar to those  
182 documented by Power et al. (37) from sediments in the Atlin wetland (See SI for aragonite and  
183 nesquehonite results). Struvite ( $\text{NH}_4\text{MgPO}_4 \cdot 6\text{H}_2\text{O}$ ) was identified in the samples collected from  
184 the bioreactor, with this mineral phase being most abundant at 0 m and 5 m (SI Figure S2E,F).



185  
186 Figure 3. Transmission electron micrographs showing A: the microbial biofilm in ultrathin section, including a  
187 magnesite grain (corresponding SAED pattern and spectrum on left) adjacent to the EPS outline of a cell; B:  
188 a magnesite grain in ultrathin section with corresponding SAED (inlay); and C: a magnesite grain (centre)  
189 at the junction between platy hydromagnesite crystals. Note the tendency of magnesite to fall out of the ultrathin section (C). D and



190 E: Secondary electron micrographs depicting the same magnesite-hydromagnesite relationship visible in (C), over  
 191 which a coating of EPS can be observed.



192  
 193 Figure 4. A: Secondary electron micrograph showing the platy hydromagnesite crystals. B: Transmission electron  
 194 micrograph showing platy hydromagnesite crystals as they nucleate on EPS adjacent to filamentous cyanobacteria  
 195 (visible here in cross-section). EPS-nucleated hydromagnesite and mineral encrusted EPS outlining cyanobacterium  
 196 filaments visible using C: SEM and D: TEM. Note the magnesite crystal visible in the top right corner of both C and

197 D, E and F: Casts of filamentous bacteria composed of magnesium carbonate. Scanning electron micrographs of G:  
198 the large amount of EPS generated in the bioreactor along with the microcrystalline pseudo-acicular mineral  
199 precipitate (H) found coating coccoid cells within the microbial mat (coated cells indicated by arrows in G and H).  
200

### 201 **3.2 Fluid composition**

202 The pH and DO concentrations both decreased during the first 21 days of the experiment,  
203 coincident with the formation of the pellicle, from respective system averages of 9.8 and 15.2 mg/L  
204 on day 0, to 9.4 and 5.9 mg/L on day 21 (Figure 5A,B; SI Table S5). The conductivity, and  $Mg^{2+}$   
205 and  $Ca^{2+}$  concentrations increased over time with the increase in flow rate from day 39 to 67, while  
206 spatially, these three parameters decreased down the length of the bioreactor (Figure 5C-E). With  
207 a wastewater inflow rate of 1 - 3 L/day, the bioreactor precipitated carbonate minerals at a rate that  
208 reduced the conductivity and magnesium concentration to equal or less than the Time = 0 values  
209 (Figure 5C-E). Conductivity (Figure 5C) and magnesium concentration (Figure 5D) values  
210 increased with inflow rates of 4 and 5 L/day despite magnesium continuously being removed from  
211 the water, suggesting the influx exceeded the rate of removal via precipitation. The average  
212 magnesium concentration of the entire bioreactor increased from 2.6 mM to 68.8 mM over time,  
213 owing to the increased inflow rate (Figure 5D, SI Table S5).

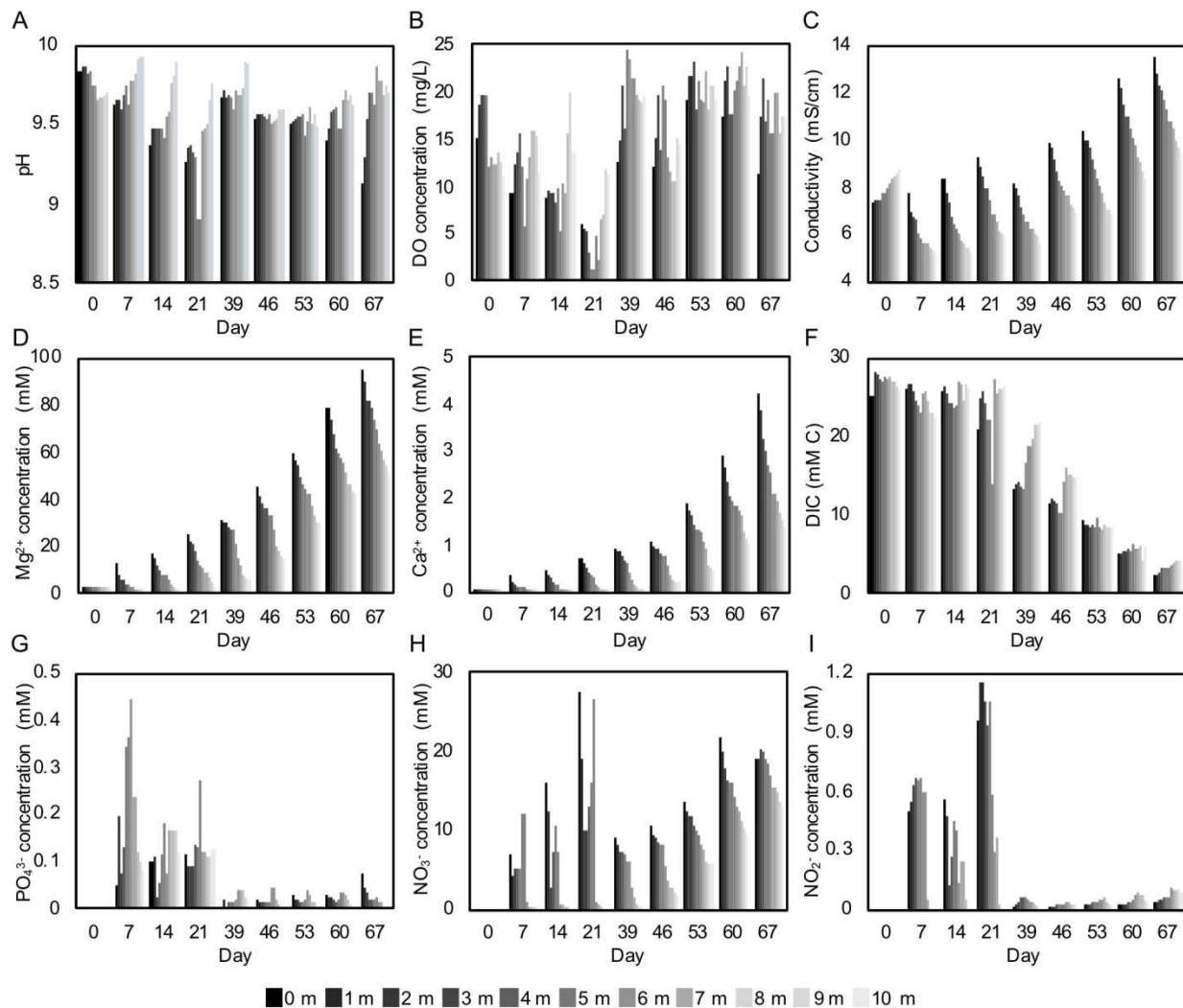
214 The DIC was relatively constant during the first 21 days, after which it decreased as the  
215 wastewater inflow rate was increased (Figure 5F; SI Table S5). DIC concentrations increased with  
216 distance from the source of nutrient and synthetic mine wastewater input at 0 m and 5 m. Higher  
217 nutrient availability at these locations may have caused localized increases in heterotrophy;  
218 however, it appears that autotrophy dominated the microbial activity beyond 5 m, resulting in a  
219 pH value increase due to photosynthesis driven  $CO_2$  consumption and  $OH^-$  generation. The DIC  
220 concentration on day 67 was 64% of what was measured on day 60, indicating rapid removal of



221 DIC from solution via carbonate precipitation (SI Table S5). Note, approximately 11% of this  
222 decrease is due to the increase in flow rate.

223 The phosphate concentration showed no clear trend during the first 21 days of the  
224 experiment, apart from a clear increase in concentration at the 5 m sampling location,  
225 corresponding to the second nutrient addition point (Figure 5G; SI Table S5). From day 39 to 67,  
226 the phosphate concentration approached 0, and never increased above 0.1 mM. The nitrate  
227 concentration was irregular during the first 21 days, after which nitrate accumulated over time to  
228 a system average concentration of 17.3 mM on day 67 (Figure 5H). The nitrate concentration  
229 decreased down the length of the bioreactor. No nitrite was measured in the nutrient solution or  
230 mine wastewater (Table 1). The nitrite concentration was irregular in the bioreactor during the first  
231 21 days, fluctuating between 0.04 and 1.15 mM (Figure 5I). From day 39 to 67, the nitrite  
232 concentration decreased markedly to less than 0.1 mM (Figure 5I; SI Table S5).

233



234  
 235 Figure 5. Change in the fluid composition parameters down the length of the bioreactor over the  
 236 duration of the experiment. A) pH, B) dissolved oxygen, C) conductivity, D)  $\text{Mg}^{2+}$ , E)  $\text{Ca}^{2+}$ , F)  
 237 DIC, G) phosphate, H) nitrate, and I) nitrite. Note, no phosphate, nitrate, or nitrite data is available  
 238 for day 0.  
 239

240 On day 67, the  $\delta^{2}\text{H}$  and  $\delta^{18}\text{O}$  values of the water increased with distance down the  
 241 bioreactor length (Table 2). The equilibrium fractionation between  $\text{CO}_{2(\text{g})}$  and  $\text{HCO}_3^-$ , the  
 242 dominant DIC species at the experimental pH, is +7.9% at 25°C (45), and the  $\delta^{13}\text{C}$  value of  
 243 atmospheric  $\text{CO}_2$  is approximately -8.3% (46). The stable carbon isotope analysis indicated that  
 244 the  $\delta^{13}\text{C}_{\text{DIC}}$  was -6.76% at 0 m and decreased down the length of the bioreactor to -9.04% at 10

245 m (Table 2), while the DIC concentration increased from 2.42 to 4.16 mM over the same distance  
 246 (SI Table S5).

247  
 248 Table 2. Stable isotope data for water samples collected following the carbonate precipitation  
 249 experiment.

Sample location	$\delta^{13}\text{C}$ (‰)	$\delta^2\text{H}$ (‰)	$\delta^{18}\text{O}$ (‰)
0 m	-6.76	-27.3	-0.32
1 m	-7.17	-31.12	0.08
2 m	-7.99	-28.93	0.12
3 m	-9.15	-23.38	0.27
4 m	-8.97	-27.3	0.47
5 m	-9.35	-23.3	0.24
6 m	-8.99	-26.57	1.25
7 m	-8.59	-27.28	1.43
8 m	-8.77	-23.7	2.09
9 m	-8.92	-20.62	2.64
10 m	-9.04	-14.9	2.43

250  
 251 Carbonate mineral Saturation Indices (*SI*) were calculated using the fluid composition data  
 252 and PHREEQC (SI Tables S6-24). The synthetic mine wastewater had *SI*s for hydromagnesite and  
 253 magnesite of -10.07 and -0.65, respectively. On day 0, the sampling locations in the bioreactor had  
 254 hydromagnesite and magnesite *SI*s ranging between -0.36 and 0.51, and 1.39 and 1.45,  
 255 respectively. The average hydromagnesite *SI* for the bioreactor increased from 0.05 (day 0) to 3.64  
 256 (day 39) followed by a decrease over the remainder of the experiment. The system average *SI* for  
 257 magnesite increased over time from 1.43 on day 0 to 2.09 on day 39, followed by a decrease to  
 258 1.62 by day 67 (SI Table S23). The average magnesite *SI* by sampling location changed little over  
 259 time, remaining between 1.72 and 1.86. On the final day of the experiment (day 67), the magnesite  
 260 *SI* increased down the length of the bioreactor from 1.2 (0 m) to 1.81 (10 m). The bioreactor did  
 261 not reach equilibrium with atmospheric  $p\text{CO}_{2(\text{g})}$  at any point during the experiment (SI Table S19).  
 262 The calculated  $p\text{CO}_2$  in equilibrium with the measured DIC values was in the range of 1.0 to 158  
 263 ppm (SI Table S19).

264

265 **4. Discussion**266 **4.1 Microbial magnesium carbonate mineral precipitation**

267 The trends observed between Mg-carbonate type and location in the bioreactor can be  
268 explained using Ca-carbonate precipitation kinetics (47-50), as carbonate crystal size and  
269 abundance is dependent on the balance between crystal nucleation rate and crystal growth rate.  
270 Higher degrees of supersaturation promote mineral nucleation, resulting in a greater abundance of  
271 individual crystals (48, 50), a relationship observed in the upper 5 m of the bioreactor as rapid  
272 nucleation of the microcrystalline coatings on microbial cells. In contrast, crystal growth is favored  
273 over crystal nucleation in solutions with a low degree of supersaturation and results in fewer, larger  
274 crystals. This relationship is evident in the downstream 5 m of the bioreactor, where micrometer-  
275 scale hydromagnesite and magnesite grains were the prevailing precipitates.

276 Microbial mats aid carbonate mineral nucleation, in part, by assisting the dehydration of  
277 divalent cations. This is a particularly critical precursor in the case of Mg-carbonates, which are  
278 more difficult to precipitate than their calcium counterparts.  $Mg^{2+}$  ions in solution are enclosed in  
279 a stable hydration shell composed of two layers of water molecules (51, 52). The inner layer  
280 consists of an octahedrally coordinated shell of six water molecules, around which a second shell  
281 of twelve water molecules is bound by hydrogen-bonds (52-54). The hydration energy of  
282 magnesium (1926 kJ/mol) compared to calcium (1579 kJ/mol) results in water molecule exchange  
283 in calcium's hydration shell occurring  $\sim 1000\times$  faster than around magnesium (55, 56), resulting in  
284 much lower precipitation rates of anhydrous Mg-carbonates compared to Ca-carbonates, and thus  
285 the tendency to form hydrated Mg-carbonates at low temperature. The biogenic process by which  
286 the magnesite identified using TEM-SAED-EDS formed explains why the lattice spacings for

287 these precipitates do not precisely match reference values (57) (Figure 3, SI Table S4). Biogenic  
288 carbonate minerals tend to exhibit a higher degree of crystal lattice disorder than their abiotically  
289 synthesized counterparts (58, 59), a characteristic that is detectable using SAED (60).

290 Abiotic precipitation of magnesite at temperatures below 80°C is typically inhibited by the  
291 energy required for the spiral step crystal growth pattern by which magnesite forms (61).  
292 However, Power et al. (51) demonstrated that the hydration shell surrounding  $Mg^{2+}$  ions can be  
293 disrupted by binding to carboxyl-coated polystyrene microspheres, thereby inducing low  
294 temperature magnesite precipitation. The results of the present study demonstrate that the  
295 negatively charged cell exteriors and EPS in cyanobacterial mats are capable of facilitating  $Mg^{2+}$   
296 dehydration through a similar mechanism (32). As much as 90% of the total organic carbon in  
297 biofilms is found in the EPS, which comprises a matrix of water, polysaccharides, lipids, proteins,  
298 and nucleic acids (62). Extracellular polysaccharides provide a large proportion of the stability of  
299 biofilms (63), which is influenced by the prevalence of cation binding. Cross-linking of  
300 polysaccharides in the EPS with cations can increase biofilm stability, while simultaneously  
301 generating localized microenvironments of high cation concentrations (64). The EPS becomes a  
302 cation reservoir to which low molecular weight (LMW) organic compounds can attach.  
303 Heterotrophic metabolic processes oxidize these LMW compounds to product bicarbonate, which  
304 can subsequently react with the cations to form carbonate minerals (64). Mineral precipitates may  
305 remain attached to the EPS, as in the case of the cellular carbonate coatings (Figure 4C), or be  
306 released like many of the hydromagnesite plates observed using SEM (Figure 4A). The apparent  
307 tendency for hydromagnesite to nucleate on, and subsequently be shed from, EPS was  
308 demonstrated by McCutcheon and Southam (41), and highlights that microbial mats must be  
309 actively producing and metabolizing EPS to provide carbonate mineral nucleation sites.

310 Carbonate precipitation can lead to mat lithification, a process demonstrated in the rock  
311 record and many contemporary environments (4, 65-67). For the reasons outlined above, calcium,  
312 rather than magnesium, carbonate minerals are the predominant deposits found in natural settings  
313 and throughout the rock record. The formation of magnesite, versus less stable, hydrated Mg-  
314 carbonate mineral phases is likely dependant on the optimization of a number of factors, namely:  
315 the efficiency of the biogeochemical process of cation dehydration described above, development  
316 of EPS-hosted microenvironments of high  $Mg^{2+}$  concentration, and alkalinity generation via  
317 microbial metabolism. Hydrated Mg-carbonate minerals, such as hydromagnesite, typically  
318 dominate known Mg-carbonate deposits because the magnesium ions need not be completely  
319 dehydrated (61, 68), thus making the successful demonstration of low temperature, microbially-  
320 aided magnesite precipitation in the present study noteworthy.

#### 321 ***4.2 Microbial activity and fluid composition***

322 Some of the  $CO_2$  used in carbonate precipitation may have been generated by heterotrophic  
323 oxidation of photosynthetically-derived organic compounds, and contributed to DIC by producing  
324 dissolved  $CO_2$  or  $HCO_3^-$  (12, 69). Organic matter in microbial mat systems is largely derived from  
325 atmospheric carbon fixed by phototrophs, which can be oxidized by heterotrophs, providing an  
326 indirect pathway for transferring atmospheric  $CO_2$  into water (12). Heterotrophic activity,  
327 therefore, may have been partially responsible for the patterns observed in the DIC, a possibility  
328 supported by the depletion in  $^{13}C_{DIC}$  (70). Phototrophic metabolism preferentially removes  $^{12}C_{DIC}$   
329 thereby enriching the remaining DIC pool in  $^{13}C$  while decreasing DIC concentrations (71).  
330 Carbonate precipitation may decrease both DIC concentration and  $\delta^{13}C_{DIC}$  values (25). However,  
331 for the majority of the bioreactor length,  $\delta^{13}C_{DIC}$  values and DIC generally co-vary, likely due to  
332 dissolution of atmospheric  $CO_2$ , as this will increase both DIC and  $\delta^{13}C$  values. Progressive

333 increases in  $\delta^2\text{H}$  and  $\delta^{18}\text{O}$  from -27.3‰ and -0.3‰ to -14.9‰ and 2.4‰, respectively, can be  
334 attributed to evaporation along the length of the bioreactor (Table 2) (72).

335 Saturation indices cannot be used as strict indicators of Mg-carbonate precipitation, given  
336 kinetic limitations to precipitation; however, the following interpretations regarding the  
337 relationship between fluid composition, *SI*, and mineral precipitation can be made (13). The  
338 changes in magnesium concentration indicated that the greatest carbonation rate was achieved  
339 from day 60 - 67 and carbonate precipitation was pervasive throughout the bioreactor. The low  
340 hydromagnesite *SI* values calculated for day 67 are consistent with rapid mineral precipitation and  
341 may be responsible for the observed cyanobacteria entombment. The pH and DO measurements  
342 from days 60 and 67 suggest that this mineralization caused a decline in photosynthesis, with the  
343 system average pH value decreasing from 9.59 to 6.21, and system average DO from 21.0 mg/L  
344 to 17.4 mg/L (SI Table S5). Addition of 5000 ppm magnesium at a rate of 5 L/day was likely  
345 approaching the limit of the bioreactor's ability to consume magnesium; therefore, reducing the  
346 flow rate or the magnesium concentration would be necessary for long-term maintenance of the  
347 biogeochemical conditions required for carbonation.

348 The pellicle likely limited gas exchange between the atmosphere and bioreactor water, as  
349 well as photosynthesis in the submerged microbial mats. Reduced photosynthesis plus  
350 heterotrophic consumption of oxygen resulted in a suboxic environment that potentially stimulated  
351 sulfate reducing-bacteria (SRB) activity, organisms previously found in the anoxic sediments used  
352 to line the bottom of the bioreactor (37). These organisms use sulfate ( $\text{SO}_4^{2-}$ ) as a terminal electron  
353 acceptor to oxidize organic compounds, producing hydrogen sulfide ( $\text{H}_2\text{S}$ ) (73, 74), which can  
354 consume oxygen, support anoxygenic photosynthesis, and/or be toxic to cyanobacteria (75-77).  
355 The metabolic activity of SRBs would have increased as DO decreased, especially at night (75).

356 While SRBs can enable carbonate precipitation by driving the water chemistry conditions towards  
357 carbonate supersaturation and generating EPS (4, 5), the toxicity of H<sub>2</sub>S towards cyanobacteria  
358 was likely detrimental to the overall bioreactor function (78). Thus, the pellicle formation  
359 demonstrates the need to regulate nutrient input, microbial growth, and carbonate precipitation,  
360 such that biofilm formation does not outpace the bioreactor's capabilities.

361 The elevated concentration of nitrite during the initial 21 days of the experiment (Figure  
362 5I) is consistent with nitrate consumption by denitrifying bacteria in anaerobic biofilms (79),  
363 which would be enabled by the low DO conditions caused by the pellicle. Nitrite is part of active  
364 nitrogen fixation-nitrification-denitrification reaction pathway common in cyanobacteria-  
365 dominated microbial mats. The nitrite depletion that occurred following the removal of the pellicle  
366 and corresponding reoxygenation of the water suggests that anaerobic denitrification was the  
367 source of the nitrite (80). The disappearance of nitrite after day 21, corresponding to the loss of  
368 the pellicle and re-oxygenation of the bioreactor suggests that denitrification was the source of the  
369 nitrite.

#### 370 ***4.3 Quantifying mineral precipitation rate and application to carbon sequestration***

371 This study demonstrated that atmospheric CO<sub>2</sub> can be sequestered via microbial  
372 carbonation in an engineered system, which is important because dissolution of atmospheric CO<sub>2</sub>  
373 into water is typically the rate-limiting step in mineral carbonation experiments and in mine  
374 tailings (14, 25). The water chemistry data, flow rate, and microbial mat surface area were used to  
375 calculate mineral precipitation and carbon storage rates. Carbon storage in biomass is considered  
376 in addition to storage in mineral phases; as its presence was minimal, aragonite was excluded from  
377 the storage calculation. See SI for details regarding how struvite precipitation was accounted for  
378 in the biomass calculation.



379           The first week (day 0-7; inflow: 1 L/day) of the experiment exhibited the highest proportion  
380 of magnesium removed (98%); however, the greatest mass of carbonate precipitated occurred  
381 during the final week of the experiment (day 60-67; inflow: 5 L/day) with 73% of the added  
382 magnesium being used for carbonate precipitation. During the final week, 5.05 mol or ~123 g of  
383 Mg was used to produce carbonate minerals. A carbon sequestration rate can be calculated for each  
384 of hydromagnesite and magnesite, providing a range for mineral carbonation. It was calculated  
385 that 472 g of hydromagnesite or 426 g of magnesite could have formed in the bioreactor during  
386 the final week. Extrapolating this process to the scale of a microbial carbonation wetland at a mine  
387 tailings storage facility, these values translate to combined biomass and mineralogical carbon  
388 storage rates of 222 and 238 t of CO<sub>2</sub>/ha of wetland/year for hydromagnesite and magnesite,  
389 respectively. The hydration of hydromagnesite results in a slightly greater precipitate mass when  
390 compared to magnesite, but makes it slightly less efficient in terms of carbon stored per magnesium  
391 atom.

392           The undersaturation of the bioreactor water with respect to atmospheric CO<sub>2</sub> suggests that  
393 sequestration rates could be increased by providing additional carbon. Harrison et al. (14)  
394 demonstrated that supplying gas containing 10% CO<sub>2</sub>, similar to power plant flue gas, causes a  
395 240-fold increase in the rate of Mg-carbonate mineral precipitation in brucite [Mg(OH)<sub>2</sub>]-bearing  
396 slurries. Limited availability of water in dry tailings can also inhibit hydrated magnesium  
397 carbonate mineral precipitation (81). An in situ microbial mineral carbonation experiment by  
398 McCutcheon et al. (82) demonstrated the challenge of water limitation, in which a microbial  
399 inoculum, cultured from biofilms naturally occurring at the mine site, was added to chrysotile mine  
400 tailings for the purpose of producing a Mg-carbonate crust. Those results indicated that  
401 constructing microbial carbonation wetlands, similar to the one implemented in the present study,

402 is likely the best strategy for integrating microbial carbonation technology for industrial carbon  
403 sequestration at tailing storage facilities (82). A potential deployment strategy would include the  
404 production Mg-rich fluids via large-scale leaching of mafic or ultramafic mine tailings, which  
405 would act as a feedstock for carbonation wetlands that could be constructed in the open pits  
406 remaining from mining activity (82). Carbonate mineral precipitation in the wetlands could utilize  
407 atmospheric CO<sub>2</sub>, while simultaneously sequestering first row transition metals that may be  
408 released from the tailings during acid leaching, thus reducing the risk of toxic metal contamination  
409 of the surrounding environment (83, 84). Similar to the wetland near Atlin, which hosts sulfate  
410 reducing bacteria in the underlying anoxic sediments, any sulfate accumulating in the system  
411 could be consumed through iron sulphide mineral generation by SRBs (37).

412         Microbial mat lithification would occur as a more laterally extensive variation of the  
413 cementation observed in naturally occurring stromatolites, exhibiting progressive growth and  
414 cementation over time. The mats would grow upwards as lithification progresses, maintaining an  
415 active layer of microbial mat into which the ion-rich leach solution can infiltrate, thereby receiving  
416 the reactants required for carbonate precipitation. Through this process, the pit would gradually  
417 become infilled with the resulting precipitates, forming a carbonate deposit. The stability of the  
418 deposit should be monitored in order to ensure safe mine site reclamation.

419         As a measure of scale for the deployment of this carbon sequestration strategy, applying  
420 this technology to the Mount Keith Nickel Mine (Western Australia) would require a 1900 ha  
421 bioreactor, a size comparable to the existing tailings facility. Such a wetland could sequester  
422 000 to 450 000 t of CO<sub>2</sub>/year, which is ~10% of the estimated 4 Mt CO<sub>2</sub>/year sequestration capacity  
423 of the Mount Keith tailings facility (85). The remaining capacity could be satisfied using other  
424 acceleration strategies, such as flue gas injection (14). In 2004, the Mount Keith Mine emitted

425 ~382 000 t of CO<sub>2</sub> equivalent, demonstrating that the proposed carbon storage strategy is capable  
426 of sequestering mine-scale quantities of CO<sub>2</sub> (12). With the correct balance of nutrients, e.g., the  
427 limiting phosphate concentrations encountered in this study (Fig. 5), microbial growth and mine  
428 wastewater input, the carbonate precipitation rate could be increased. If successful, this technology  
429 could fulfil a portion of the ~175 Mt CO<sub>2</sub>/year total carbon sequestration capacity estimated for  
430 the ~419 Mt of mafic and ultramafic tailings that are generated worldwide each year (86, 87).

431 The lack of a global carbon price is a fundamental limiting condition for the development  
432 of mineral carbonation strategies beyond laboratory demonstrations for large-scale industrial  
433 implementation (86), however, estimates by the High-Level Commission on Global Carbon Prices  
434 indicate that meeting the temperature target of the Paris Agreement will necessitate carbon prices  
435 of \$50-100 USD/t CO<sub>2</sub> by 2030 (88). At a conservative price of \$50 USD/t, economic valuation  
436 of microbial carbonation of nickel mine tailings, considering past production and reserve ore at  
437 major ultramafic nickel mine sites worldwide (excluding other ultramafic mine tailings), puts the  
438 prospective worth of this microbial carbon storage technology at \$20.5 billion USD (89, 90). Such  
439 a valuation is encouraging, as it will be necessary for many countries to increase their carbon price  
440 to achieve their emission reduction targets (88). For instance, the fuel levy rates currently  
441 implemented in Canada as part of the federal carbon pricing backstop equate to \$10 CAD/t  
442 CO<sub>2(equivalent)</sub> for 2018, and are due to increase by \$10 CAD/year until a price of \$50 CAD/t  
443 CO<sub>2(equivalent)</sub> is reached in 2022 (91). Meeting the International Energy Agency (IEA) '2°C  
444 Scenario' may result in global marginal abatement costs reaching \$130-160 USD/t CO<sub>2</sub> by 2050  
445 (88, 92), providing incentive for pursuing cost-effective implementation of various mineral  
446 carbonation technologies. Additional value could be gained during the implementation of

447 microbial carbonation wetland bioreactors by integrating the biomass component of this carbon  
448 sequestration method with biofuel production technologies (93, 94).

449

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461

## 462 **Supporting Information**

463 The supplementary information file contains details about the experimental design and the  
464 composition of the nutrient and synthetic mine wastewater solutions added to the bioreactor. It  
465 reports the errors for the fluid composition measurements and analyses. It also contains additional  
466 methods and results for the fluid composition, X-ray diffraction, and electron microscopy analyses,  
467 and tables of PHREEQC input data and saturation index outputs.

468

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