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26 ABSTRACT

Aiming to achieve heavy metal adsorption in water and soil environments, a montmorillonite 27 rich bentonite was graft-copolymerized with chitosan, and the obtained composite material 28 29 was evaluated as a metal immobilizing agent for remediating metal contaminated soil. The graft-copolymerization reaction in the composite was confirmed by scanning electron 30 microscopy (SEM), X-ray diffraction (XRD) and Fourier transform infrared spectroscopy 31 (FTIR) techniques. Batch adsorption studies with varying experimental conditions, such as 32 adsorbent amount, pH and metal concentration, were conducted to assess the metal 33 34 adsorption capacity of the composite. The adsorption pattern followed the Langmuir isotherm model, and maximum monolayer capacity was 88.5, 72.9, 51.5 and 48.5 mg g⁻¹ for Cu, Zn, 35 Cd and Ni, respectively. Amendment of a contaminated soil with the composite enhanced the 36 37 metal retention capacity by 3.4, 3.2, 4.9 and 5.6-fold for Cu, Zn, Cd and Ni, respectively, 38 over unamended soil. The desorption percentage of metals from the composite treated soil was significantly lower than the unamended contaminated soil. The findings indicated that 39 40 immobilization of heavy metals in soils could be achieved by the chitosan-bentonite, which would potentially be an inexpensive and sustainable environmental remediation technology. 41

42

43 Key words: Chitosan, Bentonite, Characterization, Adsorption, Metal contaminated soil,

- 44 Remediation
- 45

46 1. Introduction

Heavy metal pollution by the discharge of metal laden effluents into the environment
is one of the most serious environmental problems of modern society due to the toxic effects
of metals on the ecosystem, agriculture, and human health. Removal of heavy metals from
effluents before their disposal into the environment is essential since the metals are non-

51 biodegradable, may undergo chemical transformations and bio-magnification at different52 trophic levels.

Efficient, rational and economically feasible treatment technologies should be 53 developed to overcome the issue of heavy metal pollution in the environment. Among the 54 physico-chemical methods of heavy metal remediation, adsorption is easy to operate, and can 55 treat waste effluents with high as well as very low metal loadings (Bolan et al. 2014; Gupta 56 57 and Bhattacharya 2016). Biopolymers such as chitosan, cellulose and starch have been tested for removal of metals from effluents with varying degree of success. Chitosan with chelating 58 59 hydroxyl (-OH) and amino (-NH) functional groups has been studied extensively for the treatment of metal laden wastewaters, but the material has poor mechanical stability (Azarova 60 et al. 2016; Zhang et al. 2016). To overcome the weak mechanical stability, chitosan has been 61 62 immobilized on an array of supporting materials (e.g., bentonite, zeolite) (Abdel Khalek et al. 2012; Liu et al. 2015; Ngah et al. 2013). In this regard, clay minerals with metal binding sites, 63 mechanical stability, larger surface area and low cost could be used as potential support 64 65 materials for improving chitosan stability and simultaneously enhancing metal removal performance of the composite materials (El-Dib et al. 2016; Grisdanurak et al. 2012; Futalan 66 et al. 2011; Pestov and Bratskaya, 2016; Rusmin et al., 2015). 67

In the recent past, significant efforts have also been extended for the remediation of 68 metal contaminated soils. Bringing down the risk level of contaminated soils to an acceptable 69 70 limit (risk-based land management practices) can be a more rational method of soil remediation than expensive ex-situ and in-situ treatments (Naidu, 2013; Kumararaja et al., 71 2017). Stabilization of heavy metals in soils by immobilizing agents can reduce the 72 73 availability of metals and their risk to a desired level (Lim et al., 2016; Sarkar et al., 2012). Due to their low costs, waste materials have been evaluated as soil metal stabilizers in 74 numerous studies. However, many of these materials hold low 75 metal

adsorption/immobilization capacities. Soil amendments with chelating functional groups,
such as those delivered through natural polymers, are efficient for metal immobilization
because of their ability to bind or complex the metal ions tightly (Etemadi et al. 2003; Kamari
et al. 2011a; 2011b; Zhang et al. 2016; Shaheen et al. 2015a; Shaheen and Rinklebe, 2015;
Yin et al. 2015).

Chitosan is a biopolymer that is easily available at cheap price from seafood wastes. 81 Similarly, clay minerals are also abundantly available in almost all the continents. The 82 objective of this work is therefore to improve the metal binding capacity of bentonite clay by 83 84 synthesizing a chitosan-bentonite composite material through graft copolymerization method, and to evaluate the potential of the synthesized material as a metal immobilizing agent in 85 water and soil. The chitosan-bentonite composite was characterized by X-ray diffraction 86 87 (XRD), Fourier transform infrared (FTIR) and scanning electron mesoscopic (SEM) techniques, and its metal (Zn, Cu, Cd and Ni) adsorption capacity was evaluated by batch 88 studies. Adsorption-desorption studies were also done to evaluate the composite material as 89 90 an amendment for the remediation of contaminated soils by metal immobilization.

91

92 **2.** Materials and methods

93 2.1 Materials

Chitosan of low molecular weight (50-190 KDa) was procured from Sigma Aldrich Ltd., Mumbai, India. Ammonium per sulphate, acrylic acid, acetic acid and methylenebisacrylamide were purchased from Sisco Research Laboratories Pvt Ltd, India, and used without any purification. Bentonite was purchased from Minerals Ltd., New Delhi, India. Na-bentonite was prepared by adding NaCl solution (0.25 M) drop-wise to a 10% (w/v) bentonite suspension in deionized water (Kumararaja et al., 2017). Appropriate amount of analytical reagent (AR) grade salts of metals [Ni(NO₃)₂.6H₂O, Cd(NO₃)₂.6H₂O, 101 Cu(SO₄)₂.5H₂O, and Zn(SO₄)₂.7H₂O] were dissolved in deionized water to obtain stock solutions of metals (Zn, Cu, Ni and Cd) containing 1000 mg L⁻¹ metal ions. The stock 102 solution was diluted serially in deionized water to get the working standard solutions of 103 104 metals. To evaluate the efficiency of chitosan-bentonite composite as an amendment for immobilizing metals, batch study was conducted using a metal contaminated soil. The soil 105 106 was collected from agricultural fields continuously irrigated for more than two decades with the canal water of Bandi River, Rajasthan, India. The water was loaded with heavy metals 107 discharged through untreated textile, tanning and electroplating effluents from the industries 108 109 harbored in Pali industrial area, Rajasthan, India (Krishna and Govil, 2004; Dutta and Singh, 2014). The physico-chemical properties of the contaminated soil were determined by 110 standard methods (Table 1). 111

113	Table 1.	Physico-chemical	properties	of	the	industrial	effluent	irrigated	heavy	metal
114	contamina	ited soil								

containinated bon	
Soil property	Value
Mechanical composition	
Sand (%)	57.00
Silt (%)	22.10
Clay (%)	20.90
Soil Texture	Sandy clay loam
pH (1:2)	8.65
$EC (1:2) (dS m^{-1})$	0.79
$CEC (cmol (p^+) kg^{-1})$	10.20
Soil organic carbon (%)	0.44
Available soil N (mg kg ^{-1})	102.00
Available soil P (mg kg ^{-1})	4.20
Available soil K (mg kg ⁻¹)	142.00
DTPA Extractable metal	
$Zn (mg kg^{-1})$	18.20
$Cu (mg kg^{-1})$	14.12
Ni (mg kg ⁻¹)	1.03
Total metal content	
$Zn (mg kg^{-1})$	158.70
$Cu (mg kg^{-1})$	48.40
Ni (mg kg ⁻¹)	33.60

116 **2.2 Preparation of chitosan-g-poly(acrylic acid)-bentonite composite**

Chitosan-g-poly(acrylic acid)-bentonite composite was prepared using graft co-117 polymerization method with minor modification of what was described previously (Zhang et 118 al., 2007). Chitosan solution was prepared by dissolving 5 g of chitosan in 300 mL of 1% 119 acetic acid with continuous stirring. The slurry was kept at 90°C for 5 h. After cooling to 120 60°C, N₂ was purged for 30 min. Aqueous solution of ammonium persulfate (APS) was 121 added (0.94 g in 10 mL distilled water), and the reaction temperature was maintained at 60°C 122 for 15 min. After cooling to 50°C, mixtures of 360 mL of acrylic acid, 1.198 g of N,N'-123 124 methylenebisacrylamide (MBA) and 4.79 g of Na-bentonite was added. The temperature was maintained at 70°C for 3 h under continuous stirring for the completion of grafting and 125 polymerization reactions. Then the mixture was neutralized by the dropwise addition of 2 M 126 127 sodium hydroxide. The completion of neutralization reaction was indicated by the appearance of a brown color. The whole procedure was done in a four-way neck reaction kettle. The final 128 granular product was washed with distilled water, dried at 70°C, ground, sieved and 129 desiccated to obtain the final chitosan-bentonite composite powder. 130

131

132 2.3 Characterization of chitosan-g-poly(acrylic acid)-bentonite composite

133

134 2.3.1 Cation retention capacity

Cation retention capacity of the composite was determined by Ca-Mg exchange method. The composite (200 mg) saturated with 0.25 M CaCl₂ was washed with 0.25 M MgCl₂ thrice to release the adsorbed Ca²⁺. The supernatant was collected, and the volume was made up to 100 mL by distilled water. The Ca²⁺ concentration in the supernatant was determined by flame atomic absorption spectroscopy (ZEEnit 700, Analytic, Jena, Germany).

141 2.3.2 X-ray diffraction (XRD) analysis

142 XRD of the composite was performed at room temperature using Philips model 143 PW1710 diffractometer to determine the changes in crystallinity of minerals. The 144 diffractometer was fitted with a Cu tube (λ =1.5418 Å), and operated at 40 kV and 20 mA. 145 The diffractograms were collected from 3° to 35° 20 at a step size of 0.1° and counting rate of 146 5s per step using APD (automated powder diffraction) software.

147

148 2.3.3 FTIR spectroscopy

FTIR analyses were performed at room temperature by KBr disc method using a FTIR spectrophotometer; model SPECTRUM 1000, Perkin Elmer. KBr discs were prepared by mixing the chitosan-bentonite composite with IR grade KBr in pestle and mortar in the ratio of 1 mg composite per 100 mg of KBr. The mixture was pulverized to powder, and made into disc by a hydraulic press. The FTIR spectrum was recorded in the spectral range of $4000 - 600 \text{ cm}^{-1}$ with a resolution of 4 cm⁻¹ over 60 cumulative scans.

155

156 2.3.4 Scanning electron microscopy

To examine changes in the surface morphology of the composite, scanning electron microscopy (SEM) was used (EVO/MA10, CARL ZEISS Instruments). Prior to analysis the composite was coated with palladium in vacuum (10⁻³ Torr)

160

161 **2.4 Batch adsorption and desorption experiments in water and soil**

162 The metal adsorption capacity of the composite was examined using batch 163 equilibrium experiments conducted at room temperature. The initial and equilibrium 164 concentrations of metals in the aqueous solutions were analyzed by atomic adsorption

spectroscopy (AAS) as described earlier. Standard metal solutions procured from Merck(Darmstadt, Germany) was used to calibrate the spectrometer.

167

168 2.4.1 Effect of adsorbent dose

The dose of the composite was optimized by adding different masses of the material (0.01, 0.025, 0.05, 0.1, and 0.2 g) to 50 mL of 25 mg L⁻¹ metal solution in polypropylene bottle. The mixture was equilibrated for 24 h based on a preliminary experiment in an agitating shaker. The metal solution pH was adjusted to pH=6 for Cu and Cd, pH=7 for Zn, and pH=8 for Ni with 0.01 M HCl or NaOH. The supernatant was obtained by filtration using Whatman No.42 filter paper at the end of the equilibration time.

175

176 2.4.2 Effect of pH

The effect of pH on metal adsorption was studied by shaking 0.1 g composite with 50 mL of 25 mg L^{-1} metal solutions adjusted at different pH values (1, 2, 3, 4, 5, 6, 7 and 8) for 24 h in polypropylene bottles.

180

181 2.4.3 Adsorption isotherm

Adsorption isotherms were obtained by shaking 50 mL of metal solutions of varying initial concentrations (0 to 100 mg L^{-1}) with 0.1 g of composite for 24 h on an end-to-end shaker at room temperature. Clear filtrate was obtained after the equilibration time by filtering through Whatman No.42 filter paper. Similar procedure was followed to obtain the metal adsorption capacity of unamended (1g soil) and amended soils (1g soil + 0.1g composite) with varying metal concentrations. A control (soil without added metal but only deionized water) was used, and the metal extracted in the control sample was deducted from the others for calculating the final concentration to get adsorption isotherms (Forjan et al.2016).

The metal adsorption capacity (q), the amount of ions adsorbed per unit mass of
composite (mg g⁻¹) was determined by Eq. 1:

193
$$q_e = [(C_i - C_e)/m] V$$
 (Eq. 1)

where, q_e is the amount of metal ions adsorbed onto unit amount of the adsorbent (mg g⁻¹), C_i and C_e are the initial and equilibrium concentrations of metal in solution (mg L⁻¹), V is the volume of solution (L) and m is the mass of the adsorbent (g), respectively.

197 The metal removal efficiency, R, (%) of the chitosan-bentonite composite was calculated by198 Eq. 2:

199
$$R(\%) = [C_i - C_e/C_i] \times 100$$
 (Eq.

200 The distribution coefficient for adsorption was calculated using Eq. 3:

201 Distribution coefficient (K_d, mL
$$g^{-1}$$
): = [C_i-C_e/C_i] * V / m (Eq. 3)

To study the effect of biopolymer-bentonite composite addition on heavy metal 202 adsorption by soils, a procedure (Xiong et al. 2005; Tsadilas et al. 2009; Uchimiya et al. 203 2011; Li et al. 2016; Bogusz et al. 2017) similar to the aqueous system was followed. To 1 g 204 soil, 0.05 g chitosan-bentonite composite was added, and the mixture was incubated for a 205 fortnight at room temperature (25°C). Following incubation, 1g of amended soil was added to 206 30 mL of metal solutions (0.05 M CaCl₂ as the background electrolyte) with varying 207 concentrations (5-50 mg L⁻¹), shaken for 24 h, and centrifuged at 8000 rpm for 15 min. After 208 centrifugation, 15 mL of the supernatant was withdrawn and replaced with 15 mL of 209 desorbing agents (0.05 M Ca(NO₃)₂, 0.05 M eethylenediaminetetraacetic acid or 0.05 M 210 diethylenetriaminepentaacetic acid) to elucidate the desorption pattern. A similar procedure 211 was followed for an unamended soil without addition of the composite. 212

213

2)

214 **2.5 Statistical analysis**

The isotherm data of metal adsorption were fitted to the Langmuir and Freundlich models by nonlinear regression using least square method. The correlation coefficients (\mathbb{R}^2) obtained from the regression analyses were used to evaluate the applicability of the isotherm equations.

219

220 **3. Results and discussion**

221 **3.1** Characterization of chitosan grafted acrylic acid bentonite composite (chit-AA-bent)

222 Cation retention capacity is an important property of an adsorbent which determines its contaminant adsorption capacity. The cation retention capacity of chit-AA-bent composite 223 was 95.5 cmol (p^+) kg⁻¹ higher than that of bentonite (83.3 cmol (p^+) kg⁻¹). The XRD pattern 224 (Fig. 1a) of bentonite showed a strong reflection at $2\theta = 6.8^{\circ}$ which corresponded to a basal 225 spacing of 12.2Å. This characteristic reflection corresponded to montmorillonite which is the 226 predominant clay mineral (85%) in the bentonite clay. The XRD pattern shows the 227 dominance of montmorillonite $(2\theta = 10.4^{\circ}, 12.6^{\circ}, 19.4^{\circ})$ and impurities such as Quartz 228 $(2\theta = 26.3^{\circ}, 29.4^{\circ})$ (JCPDS card No 13-0135). The intensity of the primary reflection of 229 montmorillonite was reduced significantly following preparation of the chit-AA-bent 230 composite (Fig. 1b). The shape of the typical montmorillonite reflection got flattened in case 231 of the composite as against a sharp reflection in pristine bentonite, and the peak position was 232 slightly shifted to the left $(2\theta = 5.9^{\circ} \text{ and } d = 14.9 \text{ Å})$ in the composite compared to the 233 bentonite $(2\theta = 6.8^{\circ})$ (Fig. 1b). The XRD patterns thus indicated that intercalation of the 234 polymer into the stacked silicate galleries of bentonite (montmorillonite) led to an exfoliation 235 236 of the clay mineral in the polymer matrix to form a composite structure (Sarkar 2009; El-Sherif and El-Masry 2011; Liu et al. 2015). Many studies indicate the disappearance of 237

characteristic montmorillonite peak and appearance of other peaks in the composites (Yadavand Rhee, 2012; Ma et al., 2012)

240







Fig. 1. Randomly oriented XRD pattern of (a) bentonite, and (b) chitosan grafted bentonitecomposite

245

To obtain further evidence on clay exfoliation and composite formation, FTIR spectra 246 of raw bentonite, chitosan and chit-AA-bent composite were recorded in the region of 4000 -247 600 cm⁻¹ (Fig. 2). Disappearance of characteristic absorption bands of amide I (1653cm⁻¹) 248 and N-H (1596 cm⁻¹) in the spectrum of the composite confirmed that these reactive 249 functional groups (-NH₂ and -NHCO) in chitosan took part in the graft reaction with acrylic 250 acid (Sarkar 2009; Xie and Wang, 2009; Abdel Kalek et al., 2012). The absorption bands at 251 1558 and 1414 cm⁻¹ in the spectrum of the composite were arisen from acrylic acid, and 252 could be assigned to asymmetric and symmetric -COO- stretching vibrations, respectively 253

(Bulut and Karaer, 2014; Raifei et al., 2016). The characteristic bands in the spectrum of Nabentonite at 3697 and 1637 cm⁻¹ (stretching and bending vibrations of -OH) also disappeared in the spectrum of the composite. The polymerization reaction between chitosan, AA and bentonite in the composite was confirmed by the disappearance of Si-O stretching vibration at 1032 cm⁻¹, and appearance of a new band at 1022 cm⁻¹. Overall, FTIR spectra of the materials indicated that Na-bentonite participated in the grafting copolymerization reaction through its active Si-OH groups (Paluszkiewicz et al. 2011; Luo et al. 2015).

261





264

Fig. 2 FTIR spectra of chitosan, bentonite, and chitosan grafted bentonite composite

The scanning electron micrograph of the composite (Fig. 3) revealed a more extensive unfolded 3D network of the material, which could be attributed to the cross-linking reaction leading to the formation of closely packed chain rearrangement of polymer and clay particles (Abdel Kalek et al., 2012; Hafida et al., 2014). The SEM image of the composite verified that the material contained a porous structure (Lewandowska et al. 2014; Costa et al. 2016).



Figure 3. Scanning Electron Microscopy images of (a) bentonite, and (b) chitosan grafted
bentonite composite

276 **3.2 Adsorption of heavy metals**

277 3.2.1 Effect of adsorbent dose

Results indicated that percentage removal of metals increased from 60% to 95%, 35% 278 to 95%, 20% to 85% and 30% to 70% in case of Cu(II), Zn(II), Cd(II) and Ni(II), 279 respectively, with the increasing adsorbent doses (Fig. 4a). An increase in the effective 280 surface area and exchangeable sites for metal ions with increasing dose of the adsorbent 281 resulted in higher percentage of metal removal. Contrarily, as the composite dose increased, 282 the metal adsorption capacity decreased (Fig. 4b). In this case, the concentration of metal ions 283 284 became a limiting factor to cover the available exchangeable sites leading to a large number of unoccupied sites. Reduced efficiency of metal adsorption by the composite at higher dose 285 might also arise from the decreased total surface area and increased diffusional path due to 286 287 aggregation of composite particles (Ngah et al. 2013; Wang et al. 2014; Tsai et al. 2016).

288



Figure 4. Effect of adsorbent dose on percentage removal (a) and sorption capacity (b) of Zn,
Cu, Ni and Cd by chitosan grafted bentonite composite

290

294 3.2.2 Effect of pH

The speciation and distribution of metal ions, degree of ionization of the composite 295 296 and the counter ion concentration can be influenced by the solution pH, and thereby it can control the adsorption process. Depending on the pH, the active sites (OH, COOH, NH₂) on 297 298 chit-AA-bent composite could either be protonated or deprotonated. Adsorption of metals at equilibrium was low at acidic pH, and it increased with increasing pH of the solution up to a 299 critical pH level (Fig. 5). Results indicated that Cu(II) and Cd(II) were adsorbed at maximum 300 levels onto the composite at pH 6, whereas maximum Zn(II) and Ni(II) adsorption occurred 301 at pH 7 and 8, respectively. Increased levels of H^+ and hydronium (H₃O⁺) ions at lower pH 302 values would decrease metal adsorption by the composite due to a competition among cations 303 for the adsorption sites (Rusmin et al., 2016). The repulsive electrostatic force induced 304 towards the approaching cations by the positively charged surface arisen from the protonated 305 amino groups (-NH₃⁺) of the composite at acidic pH would thus result in a reduced metal 306 uptake (Grisdanurak et al. 2012; Zhang et al. 2016; Duan et al. 2016). The following reaction 307 (Eq. 4) shows the influence of pH on metal adsorption by the chit-AA-bent composite: 308

309

$$Composite-NH_3^+ + M^{2+} \longrightarrow Composite-NH_2 - M^{2+} + H^+$$
(Eq. 4)





Figure 5. Effect of pH on percentage removal (a) and sorption capacity (b) of Zn, Cu, Ni and
Cd by chitosan grafted bentonite composite

On the other hand, development of negative charges at higher pH by deprotonation of surface functional groups attracted the metal cations by electrostatic interaction. The smothering of the inhibitory effect of H^+ ions also resulted in enhanced metal adsorption. However, precipitation of metals as metal hydroxides above the critical pH value (> 6 for Cu and Cd) resulted in a decreased adsorption. The mechanism of metal adsorption by an adsorbent with functional groups at different pH can be represented by Eq. 5.

320
$$M^{2+} + RNH_2 \longrightarrow M (RNH_2)^{2+}$$
 (Eq. 5)

321

322 The amino group of the composite might react with hydrogen ions (H^+) as in Eq. 6:

323
$$H^+ + RNH_2 \longrightarrow H (RNH_2)^+$$
 (Eq. 6)

$$324 \quad OH^{-} + RNH_{2} \longrightarrow (RNH) + H_{2}O \tag{Eq. 7}$$

325 3.2.3 Adsorption isotherms

326 The Langmuir isotherm (Eq. 8) describes the adsorption onto a homogenous surface.

327
$$q_m K_L C_e$$

328 $q_e = ------- (Eq. 8)$

where, q_e is the equilibrium adsorption capacity (mg g⁻¹), C_e is the equilibrium concentration 330 of metal (mg L⁻¹), q_m is the maximum amount of metal adsorbed per unit weight of the 331 composite, K_L is the Langmuir constant (L mg⁻¹) is measure of energy of adsorption. q_m and 332 K_L are obtained from the slope and intercept of linear plot of C_e/q_e against C_e. A 333 dimensionless constant (known as separation factor or equilibrium factor; RL) (Foo and 334 Hameed, 2010; Wang et al., 2014) calculated from the Langmuir constants (Eq. 9) can be 335 used to predict whether the adsorption process is unfavorable $(R_L > 1)$, linear $(R_L = 1)$ 336 favorable ($0 < R_L < 1$) or irreversible ($R_L = 0$). 337

341 The Freundlich isotherm is an empirical equation (Eq. 10) which describes the heterogeneous342 surface adsorption.

$$q_e = K_f \times C^{1/n} \tag{Eq. 10}$$

where, q_e is the amount of metal ion adsorbed (mg g⁻¹) onto the composite. The Freundlich parameters K_f and n represent the adsorption capacity and intensity, respectively. Slope and intercept of the linear plots of log q_e versus log C_e (log $q_e = \log K_f + 1/n \log C_e$) gives K_f and n. The favorability of the adsorption process is indicated by the Freundlich constant n value; values < 1 for poor adsorption, 1-2 for moderately good, and 2-10 represent the beneficial adsorption (Foo and Hameed, 2010; Sarkar et al., 2012).

Langmuir isotherm model fitted well with the adsorption data for the studied metals with R^2 values ≥ 0.98 (Table 2). This suggested the occurrence of monolayer adsorption on an energetically uniform surface (Pereira et al. 2013; Moussout et al. 2016). The Langmuir maximum monolayer adsorption capacity (q_m) of the composite were in the following order: Cu: 88.49, Zn: 72.99, Cd: 51.55 and Ni: 48.54 mg g⁻¹. The adsorption capacity of the composite was higher than that of the raw bentonite (Cu:13.95, Zn:11.41, Cd:9.41, Ni:13.95 356 mg g⁻¹) (Kumararaja et al., 2014; Kumararaja and Manjajah, 2015). The sequence of metal adsorption by the composite is in agreement with previous results (Ngah et al. 2011; Kamari 357 et al., 2012a&b). The intrinsic nature of metal ions has an important influence on their 358 adsorption performance. High electronegativity, high softness value and easy hydrolyzability 359 would result in preferential adsorption of Cu (II) over other ions. The metal adsorption 360 sequence followed negative log of the first hydrolysis dissociation constant of the metals [Cu 361 (8.0); Zn (9.0); Ni (9.9) and Cd (10.1)]. Metals with low hydrolysis constant easily form 362 hydroxo-complex which is adsorbed to the composite more strongly than the free ions. 363 364 Similar to hydrolysis constant, the adsorption of metals also followed the electronegativity parameters [Cu (2.0); Ni (1.91); Cd (1.69) and Zn (1.65)] of metals except for Zn. 365 Electronegativity of a metal ion is the ability to attract electrons towards itself to form a bond 366 367 with another atom or ion. As the difference in electronegativity is large for Cu, it is preferentially adsorbed onto the composite. Metals with large softness value has a higher 368 affinity for forming electrostatic and inner sphere complexes with an adsorbent. The higher 369 the covalent index of metal ions, higher is the affinity for the adsorption site. Metals having 370 high hardness index (5.55, 5.40 and 4.12 for Cu, Zn and Cd, respectively) are easily 371 polarizable, and have high affinity for ligand molecules. The dominance of Cu in the affinity 372 sequence reinforced the role of specific binding mechanisms such as covalent binding to 373 composite surfaces with high stability and binding energy in the behaviour of this metal. Ni, 374 375 Zn and Cd are more affected by the electrostatic interactions with the surface exchange sites. The K_L related to the affinity of binding sites showed the highest value for Cu (Usman 2008; 376 Jalali and Moradi 2013; Tsai et al., 2016). Chit-AA-Bent metal sorption capacity is compared 377 378 with previously reported chitosan-based adsorbents (Supplementary)

Table 2. Isotherm constants and correlation coefficients for metal sorption on chitosan
 biopolymer bentonite composite in aqueous system
 381

Parameters	Zn	Cu	Ni	Cd
Langmuir adsorption i	sotherm			
$q_{\rm m} ({\rm mg} {\rm g}^{-1})$	72.99	88.49	48.54	51.55
$K_L (L mg^{-1})$	0.66	0.45	0.18	0.17
\mathbb{R}^2	0.99	0.98	0.99	0.98
Freundlich adsorption	isotherm			
K_{f} (mg g ⁻¹) (L g ⁻¹) ^{1/n}	21.86	30.62	10.66	10.77
Ν	2.92	6.21	2.42	2.62
\mathbf{R}^2	0.77	0.93	0.98	0.97

The R_L values (Table 3) varied between 0.60 to 0.04 for Zn, 0.69 to 0.05 for Cu, 0.88 to 0.13 for Cd and 0.85 to 0.12 for Ni. The R_L values at metal concentrations of 5-50 mg L⁻¹ were in the range of $0 < R_L < 1$, which indicated that the adsorption of Zn, Cu, Ni and Cd ions onto the composite was favorable. It implied that the composite was an efficient adsorbent for the removal of Cu(II), Zn(II), Cd(II) and Ni(II) (Futalan et al. 2011; Saravanan et al. 2011; Azzam et al., 2016).

Table 3. Langmuir isotherm dimensionless separation factor (R_L) values

Initial metal	R _L values				
concentration	Zn	Cu	Ni	Cd	
$(mg L^{-1})$					
5	0.60	0.69	0.85	0.85	
10	0.23	0.31	0.53	0.54	
20	0.13	0.18	0.34	0.37	
30	0.07	0.10	0.22	0.23	
40	0.05	0.07	0.16	0.16	
50	0.04	0.05	0.12	0.13	

391

The Freundlich parameters along with the correlation coefficients are given in Table 392 2. Copper (II) had the highest K_f and n values over Zn(II), Cd(II) and Ni(II). Higher n value 393 394 for Cu (II) indicated that the functional groups of the composite had greater affinity towards it, and the larger K_f values could be ascribed to the strong binding of Cu(II) by the composite. 395 The n values for the studied metals lie between 1 and 10 indicating beneficial adsorption of 396 metals by the chit-AA-bent composite. The order of n for the metals was Cu(II) > Zn(II) >397 Cd(II) > Ni(II) corresponding to the adsorbability or adsorption affinity sequence, which was 398 399 also in agreement with the adsorption data. Isotherms with n > 1 are classified as L-type

isotherms reflecting high affinity between adsorbate and adsorbent, which is indicative of
chemisorption (Duan et al., 2016). Higher n values indicated that the adsorption sites were
more of heterogeneous in nature (Liu et al. 2015; El-Dib et al. 2016; Moussout et al. 2016).

403

404 3.2.4 Distribution coefficients

405 The K_d values over the studied initial metal concentrations are shown in Fig. 6. The 406 K_d values indicate a preference of the adsorbent towards the adsorbate (metal ions), the higher is the K_d value, greater is the adsorbent-adsorbate affinity. The K_d values were found 407 408 to be the highest for Cu(II) followed by Zn(II), Cd(II), and the least for Ni(II). Cu and Zn were adsorbed strongly, whereas Cd and Ni showed a weaker affinity. As the nature of 409 adsorption sites changes with the metal concentrations, the K_d values also decrease at higher 410 metal concentrations. Sites with strong binding energies exhibit high selectivity towards the 411 metals at a lower concentration. As the metal concentration increases, the K_d values decreases 412 due to specific sites are continuously occupied by the metals resulting in non-specific 413 adsorption (Gomes et al. 2001; Shaheen et al. 2013; Sastre et al. 2006; Souza Baraz et al. 414 2013). 415



417 **Figure 6.** Distribution coefficients of metals with varying initial metal concentrations

418 3.2.5 Desorption of metals

Desorption study was conducted with three different desorbing agents, namely 419 calcium nitrate [Ca(NO₃)₂], EDTA and DTPA at 0.05 M concentrations. Among the 420 421 desorbing agents, the electrolyte, Ca(NO₃)₂, was found to be ineffective in removing the adsorbed metals from the composite (Fig. 7). Contrarily, owing to their metal chelating 422 functional groups, the organic desorbing agents were able to remove up to 90% of the 423 adsorbed metals. Hence, either EDTA or DTPA could be utilized for regenerating the 424 composite when applied for water purification (Ngah et al. 2013; Pereira et al. 2013; Davari 425 426 et al. 2015; Luo et al. 2015). On the other hand, a lower desorption of adsorbed metals from the composite in the presence of Ca(NO₃)₂ makes the material suitable for immobilizing 427 metals in contaminated soils where an environmental electrolyte concentration always exists. 428

429







433

434 3.2.6 Metal immobilization in soils

435 The contaminated soil used for the adsorption study was alkaline in reaction (pH in

1:2 soil: water =8.65), sandy clay loam in texture, with oxidizable organic carbon content of 436 4.43 mg kg⁻¹ (Table 1). The Langmuir parameters and correlation coefficients of metal 437 adsorption (Zn, Cu, Ni and Cd) by contaminated soil in the absence and presence of chit-AA-438 439 bent are shown in Table 4. The Langmuir model described the adsorption data better than Freundlich model for all the metals in case of the unamended contaminated soil. Langmuir 440 maximum monolayer adsorption capacity of the contaminated soil (unamended) was 0.85, 441 0.94, 0.45 and 0.42 mg g⁻¹ for Zn(II), Cu(II), Cd(II) and Ni(II), respectively, and the affinity 442 of metals was in the order Cu(II) > Zn(II) > Ni(II) > Cd(II). Application of the chit-AA-bent 443 444 composite increased the monolayer maximum adsorption capacity of the contaminated soil by 3.4, 3.2, 4.9 and 5.6 times for Zn, Cu, Ni and Cd, respectively. The maximum adsorption 445 capacity of contaminated soil for the studied metals increased in the presence of the 446 447 composite due to the increased adsorption sites available for the metals on the composite surfaces. The relative increase of Cd and Ni adsorption was higher than that of Cu. The effect 448 of the chit-AA-bent composite treatment increased the adsorption capacity of weakly 449 450 adsorbing heavy metals such as Ni, Cd and Zn compared to the strongly adsorbing metal such as Cu. This might be due to the inherent high adsorption capacity of the contaminated soil for 451 Cu because of the higher organic matter content with the different chelating functional groups 452 (Ye et al., 2013; Rinklebe and Shaheen 2015). The large difference in q_m value between 453 water and soil is due to the lower metal adsorption capacity of soil (0.85, 0.94, 0.45 and 0.42 454 mg g⁻¹) for Zn(II), Cu(II), Cd(II) and Ni(II), respectively). In soil, only 10% of sites 455 (composite) are with higher metal adsorption capacity and remaining 90% are with lower 456 adsorption capacity. Similarly, Fernández-Pazos et al (2016) reported that the Cr adsorption 457 capacity of mussel shell was 121,878 mg kg⁻¹, but the same in soil amended with mussel shell 458 was only 677 mg kg⁻¹. The Langmuir parameter K_L represents the binding energy coefficient 459 which corresponds to adsorbate concentration at which the amount of metal bound to the 460

461	adsorbent is equal to $q_m/2$ (Sastre et al. 2006). The K _L values for the contaminated soil were
462	1.09, 0.24, 0.16 and 0.10 for Cu, Zn, Ni and Cd, respectively, indicating a significantly
463	stronger affinity of the soil for Cu than other metals. The Freundlich model described the
464	adsorption data better for the contaminated soils that were amended with the chit-AA-bent
465	composite (Table 4). The K_f and N values were 15.53, 15.11, 12.16, 10.81, and 3.09, 2.17,
466	2.04, 1.59, respectively, for Cu, Zn, Cd and Ni. The N values for all the metals studied was
467	greater than 1, reflecting a favorable adsorption (Kamari et al. 2011a; 2011b; Ming et al.
468	2016).

Table 4. Isotherm constants and correlation coefficients for metal sorption on contaminated
 soil treated with chitosan biopolymer bentonite composite

Langmuir adsorption isotherm								
Soil								
	Zn	Cu	Ni	Cd				
$Qm (mg g^{-1})$	0.85	0.94	0.42	0.45				
$K_{L} (L g^{-1})$	0.24	1.09	0.10	0.16				
\mathbb{R}^2	0.99	0.99	0.99	0.99				
Soil + Chit-AA-bent co	omposite							
$Qm (mg g^{-1})$	2.91	3.06	2.09	2.53				
$K_{L} (L g^{-1})$	0.07	0.10	0.02	0.06				
\mathbb{R}^2	0.97	0.91	0.95	0.95				
Freundlich adsorption	isotherm							
Soil								
$K_{f} (mg g^{-1}) (L g^{-1})^{1/n}$	5.05	8.41	1.58	4.71				
Ν	1.42	1.53	1.27	1.41				
\mathbb{R}^2	0.95	0.97	0.91	0.90				
Soil+ Chit-AA-bent co	mposite							
$K_{f} (mg g^{-1}) (L g^{-1})^{1/n}$	15.11	15.53	10.81	12.16				
Ν	2.17	3.09	1.59	2.04				
R ²	0.99	0.99	0.99	0.99				

472

The term 'adsorption intensity' is the ratio of the quantity adsorbed in the solid phase to the initial solution quantity of the adsorbate. The adsorption intensities of metals on the composite-amended or unamended soils (Table 5) showed a decreasing trend with the increasing initial metal concentrations. At a lower initial metal loading, there was insignificant difference in adsorption intensities between the amended and unamended soils. 478 It was because of the sufficient unoccupied adsorption sites available for metals. But at a higher initial metal loading, a higher concentration of metals remained in the solution in the 479 unamended soils that resulted in a lower adsorption intensity. Composite addition to the soil 480 481 increased the adsorption sites that resulted in more amount of metals in the solid phase leading to a higher adsorption intensity than that of the untreated soil. Among the metals 482 studied, Cu maintained a higher adsorption intensity due to higher affinity for adsorption sites 483 than that of Zn, Cd and Ni in the treated and untreated soils (Shaheen et al. 2013; 484 Srinivasarao et al. 2014; Shaheen et al. 2015a &b; Kang et al. 2016). 485

Table 5. Sorption intensities of metals on contaminated soil with and without chit-AA-bentcomposite

Ci	Cu		Zn		Ni		Cd	
$(mg L^{-1})$	Soil + chit-	Soil						
	A A-bent		A A-bent		A A-bent		A A-bent	
	· · ·		· · ·		· ·		· ·	
	composite		composite		composite		composite	
5	97.4	88.8	90.2	71.8	88.0	55.9	86.8	78.0
10	98.4	87.4	87.6	62.6	86.5	50.8	86.1	63.1
20	93.5	78.0	87.0	53.6	80.5	46.8	82.6	54.3
30	85.2	74.7	82.2	46.9	73.5	37.2	80.4	43.5
40	81.6	68.4	81.6	46.6	75.3	28.3	81.6	33.8
50	79.5	60.8	78.6	39.1	74.5	27.0	77.5	26.5

489

488

490 Desorption rate can be used to characterize the degree of metal binding to the 491 adsorbent. Higher the percentage of desorption, the weak the binding. The desorption of all 492 the metals were decreased in the presence of the chit-AA-bent composite from the contaminated soil compared to the unamended soil (Fig. 8). The desorption percentage was 493 higher at a higher metal loading for all the studied metals both in the presence and absence of 494 495 the composite. Desorption percentages at all initial metal concentrations were lower for the 496 strongly adsorbed metal Cu (0.02% at 5 ppm to 0.27% at 50 ppm) than that of Zn (0.07% at 5 ppm to 3.03% at 50 ppm), Cd (0.2% at 5 ppm to 6.41% at 50 ppm), Ni (0.62% at 5 ppm to 497 23

498 5.58% at 50 ppm) in the amended soil. The percentage desorption sequence followed the same trend as in the unamended soil, and the percentage desorption was 4.26% at 5 ppm to 499 16.9% at 50 ppm, 6.66% at 5 ppm to 26.8% at 50 ppm, 10.5% at 5 ppm to 31.12% at 50 ppm 500 501 and 10.6% at 5 ppm to 37.3% at 50 ppm for Cu, Zn, Cd and Ni, respectively. Lowered desorption of metals in the composite amended soil might be due to the strong binding of 502 503 metals by the chelating functional groups of the composite. The lower percentage of desorption of Cu might be because of the formation of multinuclear complexes with the 504 composite. Increased desorption at higher loading might be due to adsorption at edges of the 505 506 composite (Futalan et al., 2012; Arabyarmohammadi et al., 2016). For the studied metals, the desorption sequence followed their relative stability of the ligand complexes. 507





Figure 8. Desorption percentage of metals from (a) unamended contaminated soil and (b)chitosan grafted bentonite composite-amended contaminated soil

513

514 4. Conclusions

XRD and SEM analyses confirmed that the layers of montmorillonite in bentonite 515 were mostly exfoliated and dispersed in the organic matrix to form a porous composite 516 structure of chit-AA-bent. Similarly, the FTIR spectra confirmed the participation of 517 montmorillonite particles in the grafting copolymerization reaction through its active Si-OH 518 519 groups to form the biopolymer composite of desired properties. The Cu, Zn, Cd and Ni adsorption capacities of the chit-AA-bent composite were higher than that of the pristine 520 bentonite. Amongst the adsorption isotherms, Langmuir equation fitted well, and the study 521 522 demonstrated the usefulness of biopolymer composite in removing metals from aqueous solutions by adsorption mechanism, i.e., through chelating interaction between functional 523 groups of composite and metals. The Freundlich adsorption model was fitted well to the 524 adsorption data of the composite-amended metal contaminated soil. The biopolymer 525 composite enhanced the adsorption intensity of metals in the contaminated soil and lowered 526 desorption of metals. Thus, the composite material could be used as a potential immobilizing 527 agent for remediating heavy metals in contaminated soils. 528

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534

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- 755 Chitosan-g-poly(acrylic acid)-bentonite composite: a potential immobilizing agent of
- 756 heavy metals in soil
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 SI Table 1: Comparison of metal adsorption capacities of chitosan bentonite composites

Material	Metal	Adsorption capacity (mg g ⁻¹)	Reference
Chitosan-montmorillonite beads	Cu	100	Pereira et al. 2013
Cross-linked chitosan/Al ₁₃ -pillared montmorillonite	Cu	53.3	Duan et al. 2014
PMAA/ grafted chitosan-bentonite	Cd	83	Abdel Khalek et al. 2012
Chitosan/vermiculite bio composite	Cd	58.5	Chen et al. 2018
Chitosan-clay composite	Ni	32.4	Futalan et al. 2011
Chitosan immobilized bentonite	Ni	18.7	Tirtom et al. 2012
Chitosan-GLA	Zn	37.7	Kamari et al. 2011
Chitosan-AA-bentonite composite	Zn	73.0	Present study
	Cu	88.5	
	Ni	48.5	
	Cd	51.6	

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